

For more than 100 years, Armstrong has been providing utility system solutions and optimization for our global partners through products, education, training aids and service. Because we know our customers are always looking for ways to make their facilities more efficient, we offer total system solutions for steam, air and hot water.

In addition to energy- and cost-saving products, Armstrong provides comprehensive services. We offer turn-key installation, operation and maintenance services; steam and compressed air system audits; steam trap management; process drying optimization; condensate system improvement; insect heat treatment; and hot-water solutions for process, safety, sanitation and domestic applications—all of which can be customized to help improve your bottom line.

Customers have been turning to Armstrong for more than 100 years because of a continuing need to optimize the efficiency of their industrial, institutional and commercial facilities. It is our intelligence and experience that separate us from other companies.

We're proud of the tradition we've established at Armstrong—merging energy and environment while sharing our vast knowledge, so future generations can benefit from a healthier, cleaner world.

Armstrong offers the following utility system and service solutions:

- Steam and Condensate Solutions Steam trapping and steam tracing equipment, testing and monitoring, strainers, air vents, liquid drainers, and condensate recovery equipment
- Hot Water Solutions Hot water heaters, balancing valves, radiator products, mixing valves and hose stations
- Heat Transfer Solutions Heating and cooling coils, unit heaters, and tank heaters
- **Humidification Solutions** Conditioned steam humidifiers, gas fired humidifiers, electric steam humidifiers and fogging systems
- Pressure/Temperature Control Solutions Pressure reducing valves and temperature regulators
- Armstrong Service Solutions Armstrong Service offers complete utility system
 optimization services for industrial, institutional and commercial facilities worldwide. We
 provide steam system audits and utility system performance evaluations;
 long-term operation and maintenance to ensure best-in-class performance; turn-key
 sustaining engineering that includes installation and continuing engineering solutions;
 utility optimization, which allows us to identify energy-saving projects within your utility
 system; and utility monetization, whereby we purchase your utility assets to free up
 cash for use elsewhere in your organization.





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Bringing Energy Down to Earth

Say energy. Think environment. And vice versa.

Any company that is energy conscious is also environmentally conscious. Less energy consumed means less waste, fewer emissions and a healthier environment.

In short, bringing energy and environment together lowers the cost industry must pay for both. By helping companies manage energy, Armstrong products and services are also helping to protect the environment.

Armstrong has been sharing know-how since we invented the energy-efficient inverted bucket steam trap in 1911. In the years since, customers' savings have proven again and again that knowledge not shared is energy wasted.

Armstrong's developments and improvements in steam trap design and function have led to countless savings in energy, time and money. This section has grown out of our decades of sharing and expanding what we've learned. It deals with the operating principles of steam traps and outlines their specific applications to a wide variety of products and industries. You'll find it a useful complement to other Armstrong literature and the Armstrong Steam-A-ware software program for sizing and selecting steam traps, pressure reducing valves and water heaters, which can be requested through Armstrong's Web site, **armstrong**international.com.

This section also includes Recommendation Charts that summarize our findings on which type of trap will give optimum performance in a given situation and why.

IMPORTANT: This section is intended to summarize general principles of installation and operation of steam traps, as outlined above. Actual installation and operation of steam trapping equipment should be performed only by experienced personnel. Selection or installation should always be accompanied by competent technical assistance or advice. This data should never be used as a substitute for such technical advice or assistance. We encourage you to contact Armstrong or its local representative for further details.



Instructions for Using the Recommendation Charts

A quick reference Recommendation Chart appears throughout the "HOW TO TRAP" sections of this catalog, pages CG-19 to CG-45

A feature code system (ranging from A to Q) supplies you with "at-a-glance" information.

The chart covers the type of steam traps and the major advantages that Armstrong feels are superior for each particular application.

For example, assume you are looking for information concerning the proper trap to use on a gravity drained jacketed kettle. You would:

- 1. Turn to the "How to Trap Jacketed Kettles" section, pages CG-37 to CG-38, and look in the lower right-hand corner of page CG-37. The Recommendation Chart located there is reprinted below for your convenience. (Each section has a Recommendation Chart.)
- 2. Find "Jacketed Kettles, Gravity Drain" in the first column under "Equipment Being Trapped" and read to the right for Armstrong's "1st Choice and Feature Code." In this case, the first choice is an IBLV and the feature code letters B, C, E, K, N are listed.

- 3. Now refer to Chart CG-2 below, titled "How Various Types of Steam Traps Meet Specific Operating Requirements" and read down the extreme left-hand column to each of the letters B, C, E, K, N. The letter "B," for example, refers to the trap's ability to provide energy-conserving operation.
- **4.** Follow the line for "B" to the right until you reach the column that corresponds to our first choice, in this case the inverted bucket. Based on tests and actual operating conditions, the energy-conserving performance of the inverted bucket steam trap has been rated "Excellent." Follow this same procedure for the remaining letters.

Abbreviations

IB Inverted Bucket Trap

IBLV Inverted Bucket Large Vent

BM Bimetallic Trap

F&T Float and Thermostatic Trap

CD Controlled Disc Trap

DC Automatic Differential Condensate Controller

CV Check Valve

T Thermic Bucket

PRV Pressure Reducing Valve

Chart CG-1. Recommendation Chart (See chart below for "Feature Code" References.)								
Equipment Being Trapped 1st Choice and Feature Choice Code								
Jacketed Kettles Gravity Drain	IBLV B, C, E, K, N	F&T or Thermostatic						
Jacketed Kettles Syphon Drain	DC B, C, E, G, H, K, N, P	IBLV						

Chart CG-2. How Various Types of Steam Traps Meet Specific Operating Requirements								
Feature Code		IB	ВМ	F&T	Disc	Thermostatic Wafer	DC	Orifice
А	Method of Operation	(1) Intermittent	(2) Intermittent	Continuous	Intermittent	(2) Intermittent	Continuous	Continuous
В	Energy Conservation (Time in Service)	Excellent	Excellent	Good	Poor	Fair	(3) Excellent	Poor
С	Resistance to Wear	Excellent	Excellent	Good	Poor	Fair	Excellent	Poor
D	Corrosion Resistance	Excellent	Excellent	Good	Excellent	Good	Excellent	Good
Е	Resistance to Hydraulic Shock	Excellent	Excellent	Poor	Excellent	(4) Poor	Excellent	Good
F	Vents Air and CO2 at Steam Temperature	Yes	No	No	No	No	Yes	Poor
G	Ability to Vent Air at Very Low Pressure (1/4 psig)	Poor	(5) NR	Excellent	(5) NR	Good	Excellent	Poor
Н	Ability to Handle Start-Up Air Loads	Fair	Excellent	Excellent	Poor	Excellent	Excellent	Poor
- 1	Operation Against Back Pressure	Excellent	Excellent	Excellent	Poor	Excellent	Excellent	Poor
J	Resistance to Damage From Freezing	(6) Good	Good	Poor	Good	Good	Good	Excellent
K	Ability to Purge System	Excellent	Good	Fair	Excellent	Good	Excellent	Poor
L	Performance on Very Light Loads	Excellent	Excellent	Excellent	Poor	Excellent	Excellent	Poor
М	Responsiveness to Slugs of Condensate	Immediate	Delayed	Immediate	Delayed	Delayed	Immediate	Poor
N	Ability to Handle Dirt	Excellent	Fair	Poor	Poor	Fair	Excellent	Poor
0	Comparative Physical Size (7)	Large	Small	Large	Small	Small	Large	Small
Р	Ability to Handle"Flash Steam"	Fair	Poor	Poor	Poor	Poor	Excellent	Poor
Q	Mechanical Failure (Open or Closed)	Open	Open	Closed	(8) Open	(9)	Open	NA

- (1) Drainage of condensate is continuous. Discharge is intermittent.
- (2) Can be continuous on low load.
- (3) Excellent when "secondary steam" is utilized.
- (4) Bimetallic and wafer traps good.
- (5) Not recommended for low pressure operations.

- (6) Cast iron traps not recommended.
- (7) In welded stainless steel construction medium.
- (8) Can fail closed due to dirt.
- (9) Can fail either open or closed, depending upon the design of the bellows.

Armstrong® Steam Tables

What They Are...How to Use Them

The heat quantities and temperature/ pressure relationships referred to in this section are taken from the Properties of Saturated Steam table.

Definitions of Terms Used

Saturated Steam is pure steam at the temperature that corresponds to the boiling temperature of water at the existing pressure.

Absolute and Gauge Pressures

Absolute pressure is pressure in pounds per square inch (psia) above a perfect vacuum. Gauge pressure is pressure in pounds per square inch above atmospheric pressure, which is 14.7 pounds per square inch absolute. Gauge pressure (psig) plus 14.7 equals absolute pressure. Or, absolute pressure minus 14.7 equals gauge pressure.

Pressure/Temperature Relationship (Columns 1, 2 and 3). For every pressure of pure steam there is a corresponding temperature. Example: The temperature of 250 psig pure steam is always 406°F.

Heat of Saturated Liquid (Column 4). This is the amount of heat required to raise the temperature of a pound of water from 32°F to the boiling point at the pressure and temperature shown. It is expressed in British thermal units (Btu).

Latent Heat or Heat of Vaporization (Column 5). The amount of heat (expressed in Btu) required to change a pound of boiling water to a pound of steam. This same amount of heat is released when a pound of steam is condensed back into a pound of water. This heat quantity is different for every pressure/temperature combination, as shown in the steam table.

Total Heat of Steam (Column 6). The sum of the Heat of the Liquid (Column 4) and Latent Heat (Column 5) in Btu. It is the total heat in steam above 32°F.

Specific Volume of Liquid (Column 7). The volume per unit of mass in cubic feet per pound.

Specific Volume of Steam (Column 8). The volume per unit of mass in cubic feet per pound.

How the Table Is Used

In addition to determining pressure/

temperature relationships, you can compute the amount of steam that will be condensed by any heating unit of known Btu output. Conversely, the table can be used to determine Btu output if steam condensing rate is

known. In the application portion of this section, there are several references to the use of the steam table.

Table CG-1. Properties of Saturated Steam
(Abstracted from Keenan and Keyes, THERMODYNAMIC PROPERTIES OF STEAM,
by permission of John Wiley & Sons, Inc.)

	Col. 1	Col. 2		Col. 4	0-1-5	Col. 6	Col. 7	Col. 8
			Col. 3		Col. 5	Total	Specific	Specific
	Gauge	Absolute	Steam	Heat of	Latent	Heat of	Volume of	Volume of
	Pressure	Pressure	Temp. (°F)	Sat. Liquid	Heat	Steam	Sat. Liquid	Sat. Steam
i I	riessuie	(psia)	remp. (1)	(Btu/lb)	(Btu/lb)	(Btu/lb)	(cu ft/lb)	(cu ft/lb)
	29.743	0.08854	32.00	0.00	1075.8	1075.8	0.016022	3306.00
ا ۽ ا	29.515	0.08834	53.14	21.21	1063.8	1075.0	0.016022	1526.00
=	27.886	1.0	101.74	69.70	1036.3	1106.0	0.016027	333.60
acı	19.742	5.0	162.24	130.13	1001.0	1131.0	0.016407	73.52
nches of Vacuum	9.562	10.0	193.21	161.17	982.1	1143.3	0.016590	38.42
0	7.536	11.0	197.75	165.73	979.3	1145.0	0.016620	35.14
ě	5.490	12.0	201.96	169.96	976.6	1146.6	0.016647	32.40
딛	3.454	13.0	205.88	173.91	974.2	1148.1	0.016674	30.06
-	1.418	14.0	209.56	177.61	971.9	1149.5	0.016699	28.04
	0.0	14.696	212.00	180.07	970.3	1150.4	0.016715	26.80
l h	1.3	16.0	216.32	184.42	967.6	1152.0	0.016746	24.75
	2.3	17.0	219.44	187.56	965.5	1153.1	0.016768	23.39
	5.3	20.0	227.96	196.16	960.1	1156.3	0.016830	20.09
	10.3	25.0	240.07	208.42	952.1	1160.6	0.016922	16.30
l h	15.3	30.0	250.33	218.82	945.3	1164.1	0.017004	13.75
l h	20.3	35.0	259.28	227.91	939.2	1167.1	0.017078	11.90
	25.3	40.0	267.25	236.03	933.7	1169.7	0.017078	10.50
	30.3	45.0	274.44	243.36	928.6	1172.0	0.017140	9.40
	40.3	55.0	287.07	256.30	919.6	1175.9	0.017205	7.79
	50.3	65.0	297.97	267.50	911.6	1179.1	0.017323	6.66
l h	60.3	75.0	307.60	277.43	904.5	1181.9	0.017123	5.82
	70.3	85.0	316.25	286.39	897.8	1184.2	0.017613	5.17
	80.3	95.0	324.12	294.56	891.7	1186.2	0.017696	4.65
	90.3	105.0	331.36	302.10	886.0	1188.1	0.017775	4.23
	100.0	114.7	337.90	308.80	880.0	1188.8	0.017775	3.88
i i	110.3	125.0	344.33	315.68	875.4	1191.1	0.017922	3.59
İ	120.3	135.0	350.21	321.85	870.6	1192.4	0.017991	3.33
	125.3	140.0	353.02	324.82	868.2	1193.0	0.018024	3.22
lσ	130.3	145.0	355.76	327.70	865.8	1193.5	0.018057	3.11
PSIG	140.3	155.0	360.50	333.24	861.3	1194.6	0.018121	2.92
-	150.3	165.0	365.99	338.53	857.1	1195.6	0.018183	2.75
İ	160.3	175.0	370.75	343.57	852.8	1196.5	0.018244	2.60
	180.3	195.0	379.67	353.10	844.9	1198.0	0.018360	2.34
	200.3	215.0	387.89	361.91	837.4	1199.3	0.018470	2.13
İ	225.3	240.0	397.37	372.12	828.5	1200.6	0.018602	1.92
İ	250.3	265.0	406.11	381.60	820.1	1201.7	0.018728	1.74
İ		300.0	417.33	393.84	809.0	1202.8	0.018896	1.54
		400.0	444.59	424.00	780.5	1204.5	0.019340	1.16
		450.0	456.28	437.20	767.4	1204.6	0.019547	1.03
ĺ		500.0	467.01	449.40	755.0	1204.4	0.019748	0.93
İ		600.0	486.21	471.60	731.6	1203.2	0.02013	0.77
İ		900.0	531.98	526.60	668.8	1195.4	0.02123	0.50
ן ו		1200.0	567.22	571.70	611.7	1183.4	0.02232	0.36
[1500.0	596.23	611.60	556.3	1167.9	0.02346	0.28
		1700.0	613.15	636.30	519.6	1155.9	0.02428	0.24
ן וֹ		2000.0	635.82	671.70	463.4	1135.1	0.02565	0.19
ן ו		2500.0	668.13	730.60	360.5	1091.1	0.02860	0.13
[2700.0	679.55	756.20	312.1	1068.3	0.03027	0.11
[3206.2	705.40	902.70	0.0	902.7	0.05053	0.05

Steam Tables



Flash Steam (Secondary)

What is flash steam? When hot condensate or boiler water, under pressure, is released to a lower pressure, part of it is re-evaporated, becoming what is known as flash steam.

Why is it important? This flash steam is important because it contains heat units that can be used for economical plant operation—and which are otherwise wasted.

How is it formed? When water is heated at atmospheric pressure, its temperature rises until it reaches 212°F, the highest temperature at which water can exist at this pressure. Additional heat does not raise the temperature, but converts the water to steam.

The heat absorbed by the water in raising its temperature to boiling point is called "sensible heat" or heat of saturated liquid. The heat required to convert water at boiling point to steam at the same temperature is called "latent heat." The unit of heat in common use is the Btu, which is the amount of heat required to raise the temperature of one pound of water 1°F at atmospheric pressure.

If water is heated under pressure, however, the boiling point is higher than 212°F, so the sensible heat required is greater. The higher the pressure, the higher the boiling temperature and the higher the heat content. If pressure is reduced, a certain amount of sensible heat is released. This excess heat will be absorbed in the form of latent heat, causing part of the water to "flash" into steam.

Condensate at steam temperature and under 100 psig pressure has a heat content of 308.8 Btu per pound. (See Column 4 in Steam Table.) If this condensate is discharged to atmospheric pressure (0 psig), its heat content instantly drops to 180 Btu per pound. The surplus of 128.8 Btu re-evaporates or flashes a portion of the condensate. The percentage that will flash to steam can be computed using the formula:

% flash steam =
$$\frac{SH - SL}{H}$$
 x 100

SH = Sensible heat in the condensate at the higher pressure before discharge.

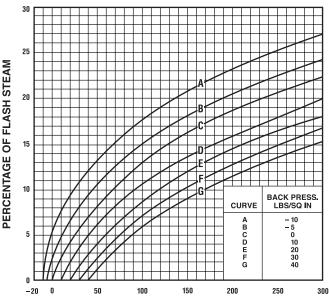
SL = Sensible heat in the condensate at the lower pressure to which discharge takes place.

H = Latent heat in the steam at the lower pressure to which the condensate has been discharged.

Chart CG-3 shows the amount of secondary steam that will be formed when discharging condensate to different pressures.

Chart CG-3.

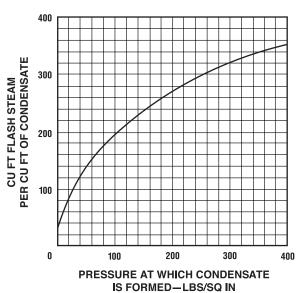
Percentage of flash steam formed when discharging condensate to reduced pressure.



PSI FROM WHICH CONDENSATE IS DISCHARGED

Chart CG-4.

Volume of flash steam formed when one cubic foot of condensate is discharged to atmospheric pressure.





Armstrong Steam...Basic Concepts

Steam is an invisible gas generated by adding heat energy to water in a boiler. Enough energy must be added to raise the temperature of the water to the boiling point. Then additional energy—without any further increase in temperature—changes the water to steam.

Steam is a very efficient and easily controlled heat transfer medium. It is most often used for transporting energy from a central location (the boiler) to any number of locations in the plant where it is used to heat air, water or process applications.

As noted, additional Btu are required to make boiling water change to steam. These Btu are not lost but stored in the steam ready to be released to heat air, cook tomatoes, press pants or dry a roll of paper.

The heat required to change boiling water into steam is called the heat of vaporization or latent heat. The quantity is different for every pressure/temperature combination, as shown in the steam tables.

Steam at Work... How the Heat of Steam Is Utilized

Heat flows from a higher temperature level to a lower temperature level in a process known as heat transfer. Starting in the combustion chamber of the boiler, heat flows through the boiler tubes to the water. When the higher pressure in the boiler pushes steam out, it heats the pipes of the distribution system. Heat flows from the steam through the walls of the pipes into the cooler surrounding air. This heat transfer changes some of the steam back into water. That's why distribution lines are usually insulated to minimize this wasteful and undesirable heat transfer.

When steam reaches the heat exchangers in the system, the story is different. Here the transfer of heat from the steam is desirable. Heat flows to the air in an air heater, to the water in a water heater or to food in a cooking kettle. Nothing should interfere with this heat transfer.

Condensate Drainage... Why It's Necessary

Condensate is the by-product of heat transfer in a steam system. It forms in the distribution system due to unavoidable radiation. It also forms in heating and process equipment as a result of desirable heat transfer from the steam to the substance heated. Once the steam has condensed and given up its valuable latent heat, the hot condensate must be removed immediately. Although the available heat in a pound of condensate is negligible as compared to a pound of steam, condensate is still valuable hot water and should be returned to the boiler.

Definitions

- The Btu. A Btu—British thermal unit—is the amount of heat energy required to raise the temperature of one pound of cold water by 1°F. Or, a Btu is the amount of heat energy given off by one pound of water in cooling, say, from 70°F to 69°F.
- **Temperature.** The degree of hotness with no implication of the amount of heat energy available.
- **Heat.** A measure of energy available with no implication of temperature. To illustrate, the one Btu that raises one pound of water from 39°F to 40°F could come from the surrounding air at a temperature of 70°F or from a flame at a temperature of 1 000°F.

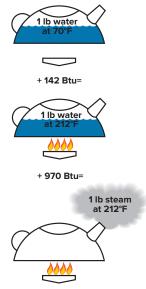


Figure CG-1. These drawings show how much heat is required to generate one pound of steam at atmospheric pressure. Note that it takes 1 Btu for every 1°F increase in temperature up to the boiling point, but that it takes more Btu to change water at 212°F to steam at 212°F.

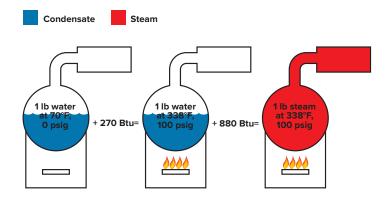


Figure CG-2. These drawings show how much heat is required to generate one pound of steam at 100 pounds per square inch pressure. Note the extra heat and higher temperature required to make water boil at 100 pounds pressure than at atmospheric pressure. Note, too, the lesser amount of heat required to change water to steam at the higher temperature.

Steam...Basic Concepts



The need to drain the distribution system. Condensate lying in the bottom of steam lines can be the cause of one kind of water hammer. Steam traveling at up to 100 miles per hour makes "waves" as it passes over this condensate (Fig. CG-4). If enough condensate forms, high-speed steam pushes it along, creating a dangerous slug that grows larger and larger as it picks up liquid in front of it. Anything that changes the direction—pipe fittings, regulating valves, tees, elbows, blind flanges—can be destroyed. In addition to damage from this "battering ram," high-velocity water may erode fittings by chipping away at metal surfaces.

The need to drain the heat transfer unit. When steam comes in contact with condensate cooled below the temperature of steam, it can produce another kind of water hammer known as thermal shock. Steam occupies a much greater volume than condensate, and when it collapses suddenly, it can send shock waves throughout the system. This form of water hammer can damage equipment, and it signals that condensate is not being drained from the system.

Obviously, condensate in the heat transfer unit takes up space and reduces the physical size and capacity of the equipment. Removing it quickly keeps the unit full of steam (Fig. CG-5). As steam condenses, it forms a film of water on the inside of the heat exchanger. Non-condensable gases do not change into liquid and flow away by gravity. Instead, they accumulate as a thin film on the surface of the heat exchanger—along with dirt and scale. All are potential barriers to heat transfer (Fig. CG-3).

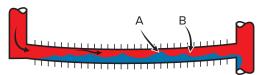


Figure CG-4. Condensate allowed to collect in pipes or tubes is blown into waves by steam passing over it until it blocks steam flow at point **A**. Condensate in area **B** causes a pressure differential that allows steam pressure to push the slug of condensate along like a battering ram.

The need to remove air and CO_2 . Air is always present during equipment start-up and in the boiler feedwater. Feedwater may also contain dissolved carbonates, which release carbon dioxide gas. The steam velocity pushes the gases to the walls of the heat exchangers, where they may block heat transfer. This compounds the condensate drainage problem, because these gases must be removed along with the condensate.

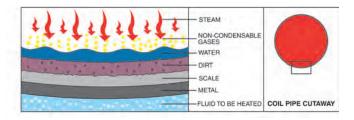


Figure CG-3. Potential barriers to heat transfer: steam heat and temperature must penetrate these potential barriers to do their work.

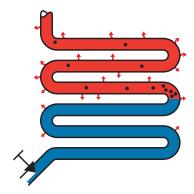


Figure CG-5. Coil half full of condensate can't work at full capacity.

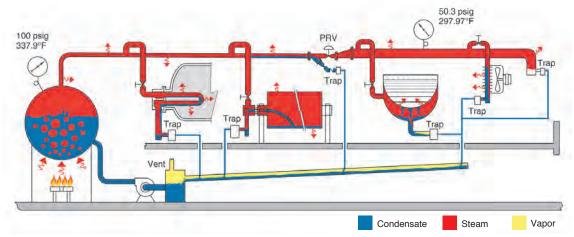


Figure CG-6. Note that heat radiation from the distribution system causes condensate to form and, therefore, requires steam traps at natural low points or ahead of control valves. In the heat exchangers, traps perform the vital function of removing the condensate before it becomes a barrier to heat transfer. Hot condensate is returned through the traps to the boiler for reuse.

Armstrong Steam...Basic Concepts

Effect of Air on Steam Temperature

When air and other gases enter the steam system, they consume part of the volume that steam would otherwise occupy. The temperature of the air/steam mixture falls below that of pure steam. Figure CG-7 explains the effect of air in steam lines. Table CG-2 and Chart CG-5 show the various temperature reductions caused by air at various percentages and pressures.

Effect of Air on Heat Transfer

The normal flow of steam toward the heat exchanger surface carries air and other gases with it. Since they do not condense and drain by gravity, these non-condensable gases set up a barrier between the steam and the heat exchanger surface. The excellent insulating properties of air reduce heat transfer. In fact, under certain conditions as little as 1/2 of 1% by volume of air in steam can reduce heat transfer efficiency by 50% (Fig. CG-8).

Table CG-2. Temperature Reduction Caused by Air								
Pressure (psig)	Temp. of Steam, No Air Present (°F)	Temp. of Steam Mixed With Various Percentages of Air (by Volume) (°F)						
		10%	20%	30%				
10.3	240.1	234.3	228.0	220.9				
25.3	267.3	261.0	254.1	246.4				
50.3	298.0	291.0	283.5	275.1				
75.3	320.3	312.9	304.8	295.9				
100.3	338.1	330.3	321.8	312.4				

When non-condensable gases (primarily air) continue to accumulate and are not removed, they may gradually fill the heat exchanger with gases and stop the flow of steam altogether. The unit is then "air bound."

Corrosion

Two primary causes of scale and corrosion are carbon dioxide (CO_2) and oxygen. CO_2 enters the system as carbonates dissolved in feedwater and, when mixed with cooled condensate, creates carbonic acid. Extremely corrosive, carbonic acid can eat through piping and heat exchangers (Fig. CG-9). Oxygen enters the system as gas dissolved in the cold feedwater. It aggravates the action of carbonic acid, speeding corrosion and pitting iron and steel surfaces (Fig. CG-10).

Eliminating the Undesirables

To summarize, traps must drain condensate because it can reduce heat transfer and cause water hammer. Traps should evacuate air and other non-condensable gases because they can reduce heat transfer by reducing steam temperature and insulating the system. They can also foster destructive corrosion. It's essential to remove condensate, air and CO_2 as quickly and completely as possible. A steam trap, which is simply an automatic valve that opens for condensate, air and CO_2 and closes for steam, does this job. For economic reasons, the steam trap should do its work for long periods with minimum attention.

Figure CG-7. Chamber containing air and steam delivers only the heat of the partial pressure of the steam, not the total pressure.



Steam chamber 100% steam Total pressure 100 psia Steam pressure 100 psia Steam temperature 327.8°F



Steam chamber 90% steam and 10% air Total pressure 100 psia Steam pressure 90 psia Steam temperature 320.3°F

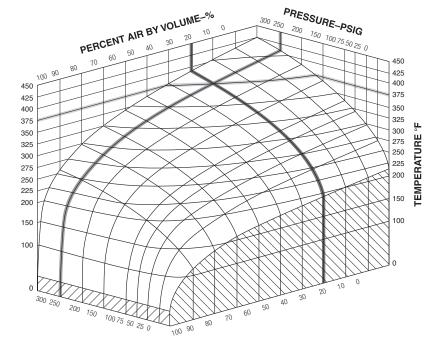


Chart CG-8. Air Steam Mixture

Temperature reduction caused by various percentages of air at differing pressures. This chart determines the percentage of air with known pressure and temperature by determining the point of intersection between pressure, temperature and percentage of air by volume. As an example, assume system pressure of 250 psig with a temperature at the heat exchanger of 375°F. From the chart, it is determined that there is 30% air by volume in the steam.+

Steam...Basic Concepts



What the Steam Trap Must Do

The job of the steam trap is to get condensate, air and CO_2 out of the system as quickly as they accumulate. In addition, for overall efficiency and economy, the trap must also provide:

- Minimal steam loss. Table CG-3 shows how costly unattended steam leaks can be.
- 2. Long life and dependable service. Rapid wear of parts quickly brings a trap to the point of undependability. An efficient trap saves money by minimizing trap testing, repair, cleaning, downtime and associated losses.
- **3. Corrosion resistance.** Working trap parts should be corrosion-resistant in order to combat the damaging effects of acidic or oxygen-laden condensate.
- 4. Air venting. Air can be present in steam at any time and especially on start-up. Air must be vented for efficient heat transfer and to prevent system binding.
- 5. CO₂ venting. Venting CO₂ at steam temperature will prevent the formation of carbonic acid. Therefore, the steam trap must function at or near steam temperature since CO₂ dissolves in condensate that has cooled below steam temperature.
- **6. Operation against back pressure.** Pressurized return lines can occur both by design and unintentionally. A steam trap should be able to operate against the actual back pressure in its return system.

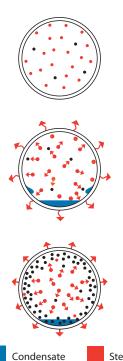
7. Freedom from dirt problems. Dirt is an ever-present concern since traps are located at low points in the steam system. Condensate picks up dirt and scale in the piping, and solids may carry over from the boiler. Even particles passing through strainer screens are erosive and, therefore, the steam trap must be able to operate in the presence of dirt.

A trap delivering anything less than all these desirable operating/design features will reduce the efficiency of the system and increase costs. When a trap delivers all these features the system can achieve:

- 1. Fast heat-up of heat transfer equipment
- Maximum equipment temperature for enhanced steam heat transfer
- 3. Maximum equipment capacity
- 4. Maximum fuel economy
- 5. Reduced labor per unit of output
- 6. Minimum maintenance and a long trouble-free service life

Sometimes an application may demand a trap without these design features, but in the vast majority of applications the trap which meets all the requirements will deliver the best results.

Figure CG-8. Steam condensing in a heat transfer unit moves air to the heat transfer surface, where it collects or "plates out" to form effective insulation.



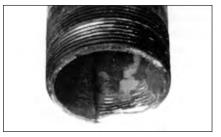


Figure CG-9. CO₂ gas combines with condensate allowed to cool below steam temperature to form carbonic acid, which corrodes pipes and heat transfer units. Note groove eaten away in the pipe illustrated.

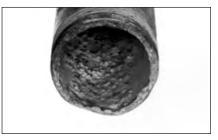


Figure CG-10. Oxygen in the system speeds corrosion (oxidation) of pipes, causing pitting such as shown here. Figs. CG-9 and CG-10 courtesy of Dearborn Chemical Company.

Table CG-3. Cost of Various Sized Steam Leaks at 100 psi (Assuming steam costs \$10.00/1,000 lbs)									
Size of Orifice Lbs Steam Wasted Per Month (USD) Total Cost I (USD) (USD)									
1/2"	12, 7 mm	553,000	\$5,530.00	\$66,360.00					
7/16"	11, 2 mm	423,500	4,235.00	50,820.00					
3/8"	9, 5 mm	311,000	3,110.00	37,320.00					
5/16"	7, 9 mm	216,000	2,160.00	25,920.00					
1/4"	6, 4 mm	138,000	1,380.00	16,560.00					
3/16"	4, 8 mm	78,000	780.00	9,360.00					
1/8"	3, 2 mm	34,500	345.00	4,140.00					

The steam loss values assume typical condensate load for drip trap applications.

Armstrong methodology for steam trap management and condensate return is sanctioned by the Clean Development

Mechanism of the United Nations Framework Convention on Climate Change.



The Inverted Bucket Steam Trap

The Armstrong inverted submerged bucket steam trap is a mechanical trap that operates on the difference in density between steam and water. See Fig. CG-11. Steam entering the inverted submerged bucket causes the bucket to float and close the discharge valve. Condensate entering the trap changes the bucket to a weight that sinks and opens the trap valve to discharge the condensate. Unlike other mechanical traps, the inverted bucket also vents air and carbon dioxide continuously at steam temperature.

This simple principle of condensate removal was introduced by Armstrong in 1911. Years of improvement in materials and manufacturing have made today's Armstrong inverted bucket traps virtually unmatched in operating efficiency, dependability and long life.

Long, Energy-Efficient Service Life

At the heart of the Armstrong inverted bucket trap is a unique leverage system that multiplies the force provided by the bucket to open the valve against pressure. There are no fixed pivots to wear or create friction. It is designed to open the discharge orifice for maximum capacity. Since the bucket is open at the bottom, it is resistant to damage from water hammer. Wearing points are heavily reinforced for long life.

An Armstrong inverted bucket trap can continue to conserve energy even in the presence of wear. Gradual wear slightly increases the diameter of the seat and alters the shape and diameter of the ball valve. But as this occurs, the ball merely seats itself deeper—preserving a tight seal.

Reliable Operation

The Armstrong inverted bucket trap owes much of its reliability to a design that makes it virtually free of dirt problems. Note that the valve and seat are at the top of the trap. The larger particles of dirt fall to the bottom, where they are pulverized under the up-and-down action of the bucket. Since the valve of an inverted bucket is either closed or fully open, there is free passage of dirt particles. In addition, the swift flow of condensate from under the bucket's edge creates a unique self-scrubbing action that sweeps dirt out of the trap. The inverted bucket has only two moving parts—the valve lever assembly and the bucket. That means no fixed points, no complicated linkages—nothing to stick, bind or clog.

Corrosion-Resistant Parts

The valve and seat of Armstrong inverted bucket traps are high chrome stainless steel, ground and lapped. All other working parts are wear- and corrosion-resistant stainless steel.

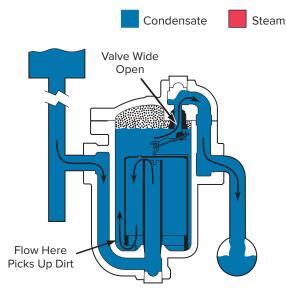
Operation Against Back Pressure

High pressure in the discharge line simply reduces the differential across the valve. As back pressure approaches that of inlet pressure, discharge becomes continuous just as it does on the very low pressure differentials.

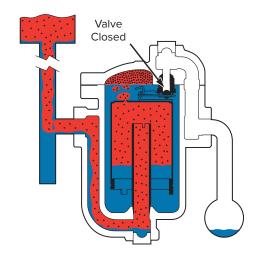
Back pressure has no adverse effect on inverted bucket trap operation other than capacity reduction caused by the low differential. There is simply less force required by the bucket to pull the valve open, cycling the trap.

Flashing Condensate

Figure CG-11. Operation of the Inverted Bucket Steam Trap (at pressures close to maximum)



1. Steam trap is installed in drain line between steam-heated unit and condensate return header. On start-up, bucket is down and valve is wide open. As initial flood of condensate enters the trap and flows under bottom of bucket, it fills trap body and completely submerges bucket. Condensate then discharges through wide-open valve to return header.



2. Steam also enters trap under bottom of bucket, where it rises and collects at top, imparting buoyancy. Bucket then rises and lifts valve toward its seat until valve is snapped tightly shut. Air and carbon dioxide continually pass through bucket vent and collect at top of trap. Any steam passing through vent is condensed by radiation from trap.

The Inverted Bucket Steam Trap

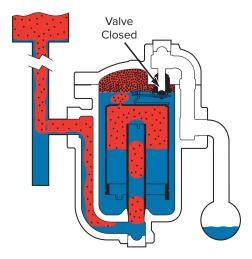


Types of Armstrong Inverted Bucket Traps Available to Meet Specific Requirements

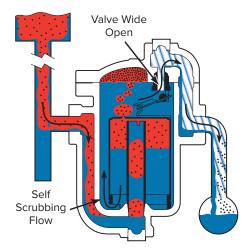
The availability of inverted bucket traps in different body materials, piping configurations and other variables permits flexibility in applying the right trap to meet specific needs. See Table CG-4.

- All-Stainless Steel Traps. Sealed, tamper-proof stainless steel bodies enable these traps to withstand freeze-ups without damage. They may be installed on tracer lines, outdoor drips and other services subject to freezing. For pressures to 650 psig and temperatures to 800°F.
- **2. Cast Iron Traps.** Standard inverted bucket traps for general service at pressures to 250 psig and temperatures to 450°F. Offered with side connections, side connections with integral strainers and bottom inlet—top outlet connections.
- **3. Forged Steel Traps.** Standard inverted bucket traps for high pressure, high temperature services (including superheated steam) to 2,700 psig at 1,050°F.
- Cast Stainless Steel Traps. Standard inverted bucket traps for high capacity, corrosive service. Repairable. For pressures to 700 psig and temperatures to 506°F.

Table CG-4. Typical Design Parameters for Inverted Bucket Traps									
Body and Cap Materials	Cast Iron	Stainless Steel	Forged Steel	Cast Steel	Cast Stainless Steel				
Connections	1/2" thru 2-1/2"	3/8" thru 1"	1/2" thru 2"	1/2" thru 1"	1/2" thru 2"				
Type Connections	Screwed	Screwed, Socketweld	Screwed, Socketweld or Flanged	Screwed, Socketweld or Flanged	Screwed, Socketweld or Flanged				
Operating Pressure (psig)	0 thru 250	0 thru 650	0 thru 2,700	0 thru 600	0 thru 700				
Capacity (lbs/hr)	To 20,000	To 4,400	To 20,000	To 4,400	To 20,000				



3. As the entering condensate starts to fill the bucket, the bucket begins to exert a pull on the lever. As the condensate continues to rise, more force is exerted until there is enough to open the valve against the differential pressure.



4. As the valve starts to open, the pressure force across the valve is reduced. The bucket then sinks rapidly and fully opens the valve. Accumulated air is discharged first, followed by condensate. The flow under the bottom of the bucket picks up dirt and sweeps it out of the trap. Discharge continues until more steam floats the bucket, and the cycle repeats.



The Float and Thermostatic Steam Trap

The float and thermostatic trap is a mechanical trap that operates on both density and temperature principles. The float valve operates on the density principle: A lever connects the ball float to the valve and seat. Once condensate reaches a certain level in the trap the float rises, opening the orifice and draining condensate. A water seal formed by the condensate prevents live steam loss.

Since the discharge valve is under water, it is not capable of venting air and non-condensables. When the accumulation of air and non-condensable gases causes a significant temperature drop, a thermostatic air vent in the top of the trap discharges it. The thermostatic vent opens at a temperature a few degrees below saturation so it's able to handle a large volume of air—through an entirely separate orifice—but at a slightly reduced temperature.

Armstrong F&T traps provide high air-venting capacity, respond immediately to condensate and are suitable for both industrial and HVAC applications.

Reliable Operation on Modulating Steam Pressure

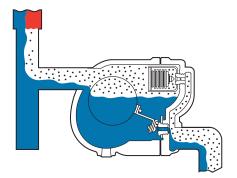
Modulating steam pressure means that the pressure in the heat exchange unit being drained can vary anywhere from the maximum steam supply pressure down to vacuum under certain conditions. Thus, under conditions of zero pressure, only the force of gravity is available to push condensate through a steam trap. Substantial amounts of air may also be liberated under these conditions of low steam pressure. The efficient operation of the F&T trap meets all of these specialized requirements.

High Back Pressure Operation

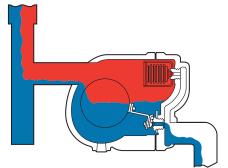
Back pressure has no adverse effect on float and thermostatic trap operation other than capacity reduction due to low differential. The trap will not fail to close and will not blow steam due to the high back pressure.

Table CG-5. Typical Design Parameters for Float and Thermostatic Traps					
Body and Cap Materials	Cast Iron	Cast Steel			
Connections	1/2" thru 3"	1/2" thru 3"			
Type Connections	Screwed or Flanged	Screwed, Socketweld or Flanged			
Operating Pressure (psig)	0 thru 250	0 thru 465			
Capacity (lbs/hr)	To 208 000	To 280 000			

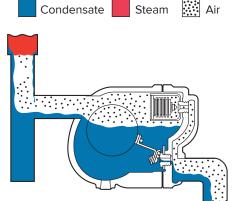
Figure CG-12. Operation of the F&T Steam Trap



1. On start-up, low system pressure forces air out through the thermostatic air vent. A high condensate load normally follows air venting and lifts the float, which opens the main valve. The remaining air continues to discharge through the open vent.



2. When steam reaches the trap, the thermostatic air vent closes in response to higher temperature. Condensate continues to flow through the main valve, which is positioned by the float to discharge condensate at the same rate that it flows to the trap.



3. As air accumulates in the trap, the temperature drops below that of saturated steam. The balanced pressure thermostatic air vent opens and discharges air.

NOTE: These operational schematics of the F&T trap do not represent actual trap configuration.



The Controlled Disc Steam Trap



The controlled disc steam trap is a time-delayed device that operates on the velocity principle. It contains only one moving part, the disc itself. Because it is very lightweight and compact, the CD trap meets the needs of many applications where space is limited. In addition to the disc trap's simplicity and small size, it also offers advantages such as resistance to hydraulic shock, the complete discharge of all condensate when open and intermittent operation for a steady purging action.

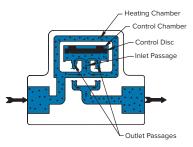
Operation of controlled disc traps depends on the changes in pressures in the chamber where the disc operates. The Armstrong CD trap will be open as long as cold condensate is flowing. When steam or flash steam reaches the inlet orifice, velocity of flow increases, pulling the disc toward the seat. Increasing pressure in the control chamber snaps the disc closed. The subsequent pressure reduction, necessary for the trap to open, is controlled by the heating chamber in the cap and a finite machined bleed groove in the disc. Once the system is up to temperature, the bleed groove controls the trap cycle rate.

Unique Heating Chamber

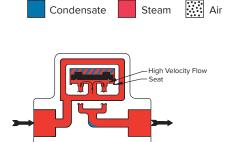
The unique heating chamber in Armstrong's controlled disc traps surrounds the disc body and control chamber. A controlled bleed from the chamber to the trap outlet controls the cycle rate. That means that the trap design—not ambient conditions—controls the cycle rate. Without this controlling feature, rain, snow and cold ambient conditions would upset the cycle rate of the trap.

Table CG-6. Typical Design Parameters for Controlled Disc Traps				
Body and Cap Materials	Steel			
Connections	3/8" thru 1"			
Type Connections	Screwed, Socketweld or Flanged			
Operating Pressure (psig)	10 thru 600			
Capacity (lbs/hr)	To 2 850			

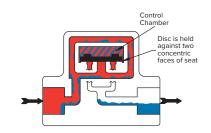
Figure CG-13. Design and Operation of Controlled Disc Traps



1. On start-up, condensate and air entering the trap pass through the heating chamber, around the control chamber and through the inlet orifice. This flow lifts the disc off the inlet orifice, and the condensate flows through to the outlet passages.



Steam enters through the inlet passage and flows under the control disc. The flow velocity across the face of the control disc increases, creating a low pressure that pulls the disc toward the seat.



Condensate and Steam Mixture

3. The disc closes against two concentric faces of the seat, closing off the inlet passage and also trapping steam and condensate above the disc. There is a controlled bleeding of steam from the control chamber; flashing condensate helps maintain the pressure in the control chamber. When the pressure above the disc is reduced, the incoming pressure lifts the disc off the seat. If condensate is present, it will be discharged, and the cycle repeats.

The Bimetallic Steam Trap

Bimetallic steam traps have the ability to handle large start-up loads. As the trap increases in temperature, its stacked nickel-chrome bimetallic elements start to expand, allowing for tight shutoff as steam reaches the trap, thus preventing steam loss. In addition to its light weight and compact size, it offers resistance to water hammer. Titanium valve and seat on high-pressure bimetallic traps ensure extremely long service life in the harsh environment of superheated steam systems.

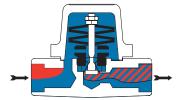
Figure CG-14. Design and Operation of Bimetallic Steam Traps

Table CG-7. Typical Design Parameters for Bimetallic Traps						
Body and Cap Materials	Carbon Steel Stainless Steel					
Connection Sizes	1/2", 3/4", 1"					
Type Connections	Screwed, Socketweld, Flanged	Screwed, NPT, BSPT, Socketweld, Buttweld, Flanged				
Operating (psig)	0 - 250 200 - 900					
Cold Water Capacity lb/hr	up to 11 000					

Steam



1. On start-up, the trap is cold, so the elements are flat and the valve is wide open, which results in air and condensate being easily removed from the system by working pressure.



Condensate

2. With increasing temperature of the condensate, the bimetallic elements will start to expand and flex.



Flashing Steam

3. When set temperature is reached, the force of the elements is high enough to close the valve completely against the system pressure working on the valve.



The Thermostatic Steam Trap

Armstrong thermostatic steam traps are available with balanced pressure bellows or wafer-type elements and are constructed in a wide variety of materials, including stainless steel, carbon steel and bronze. These traps are used on applications with very light condensate loads.

Thermostatic Operation

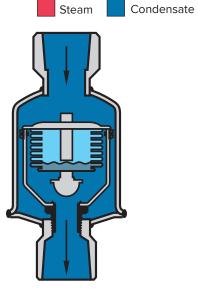
Thermostatic steam traps operate on the difference in temperature between steam and cooled condensate and air. Steam increases the pressure inside the thermostatic element, causing the trap to close. As condensate and non-condensable gases back up in the cooling leg, the temperature begins to drop, and the thermostatic element contracts and opens the valve. The amount of condensate backed up ahead of the trap depends on the load conditions, steam pressure and size of the piping. It is important to note that an accumulation of non-condensable gases can occur behind the condensate backup.

Table CG-8. Design Parameters for Thermostatic Traps						
	Balanced Bello		Balan	ced Pressure \	Wafer	
Body and Cap Materials	Stainless Steel	Bronze	Stainless Steel	Carbon Steel	Bronze	
Connections	1/2", 3/4"	1/2", 3/4"	1/4" thru 1"	1/2", 3/4"	1/2", 3/4", 1"	
Type Connections	Screwed, Socketweld	NPT Straight, Angle	Screwed, Socketweld	Screwed, Socketweld	NPT Straight, Angle	
Operating Pressure (psig)	0 - 300	0 - 50	0 - 400	0 - 600	0 - 65	
Capacity (lbs/hr)	To 3 450	To 1 600	To 70	To 85	To 960	

NOTE: Thermostatic traps can also be used for venting air from a steam system. When air collects, the temperature drops and the thermostatic air vent automatically discharges the air at slightly below steam temperature throughout the entire operating pressure range.

Condensate and Air

Figure CG-15. Operation of the Thermostatic Steam Trap

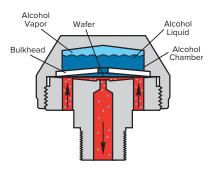


1. On start-up, condensate and air are pushed ahead of the steam directly through the trap. The thermostatic bellows element is fully contracted, and the valve remains wide open until steam approaches the trap.



2. As the temperature inside the trap increases, it quickly heats the charged bellows element, increasing the vapor pressure inside. When pressure inside the element becomes balanced with system pressure in the trap body, the spring effect of the bellows causes the element to expand, closing the valve. When temperature in the trap drops a few degrees below saturated steam temperature, imbalanced pressure contracts the bellows, opening the valve.

Figure CG-16.
Operation of Thermostatic Wafer



Balanced Pressure Thermostatic Wafer operation is very similar to balanced pressure bellows described in Fig. CG-15. The wafer is partially filled with a liquid. As the temperature inside the trap increases, it heats the charged wafer, increasing the vapor pressure inside. When the pressure inside the wafer exceeds the surrounding steam pressure, the wafer membrane is forced down on the valve seat, and the trap is closed. A temperature drop caused by condensate or non-condensable gases cools and reduces the pressure inside the wafer, allowing the wafer to uncover the seat.



The Automatic Differential Condensate Controller

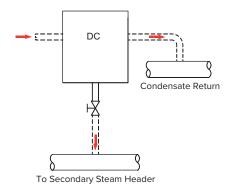
Armstrong automatic differential condensate controllers (DC) are designed to function on applications where condensate must be lifted from a drain point or in gravity drainage applications where increased velocity will aid in drainage.

Lifting condensate from the drain point—often referred to as syphon drainage—reduces the pressure of condensate, causing a portion of it to flash into steam. Since ordinary steam traps are unable to distinguish flash steam and live steam, they close and impede drainage.

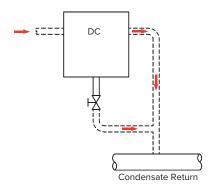
Increased velocity with gravity drainage will aid in drawing the condensate and air to the DC. An internal steam by-pass controlled by a manual metering valve causes this increased velocity. Therefore, the condensate controller automatically vents the by-pass or secondary steam. This is then collected for use in other heat exchangers or discharged to the condensate return line.

Capacity considerations for draining equipment vary greatly according to the application. However, a single condensate controller provides sufficient capacity for most applications.

Figure CG-17.



For the most efficient use of steam energy, Armstrong recommends this piping arrangement when secondary steam is collected and reused in heat transfer equipment.



Piping arrangement when flash steam and non-condensables are to be removed and discharged directly to the condensate return line.

Condensate Controller Operation

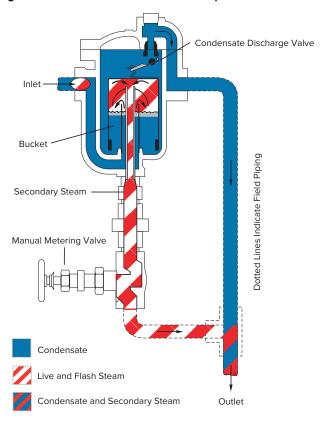
Condensate, air and steam (live and flash) enter through the controller inlet. At this point flash steam and air are automatically separated from the condensate. Then they divert into the integral by-pass at a controlled rate, forming secondary steam (See Fig. CG-18).

The valve is adjustable so it matches the amount of flash present under full capacity operation or to meet the velocity requirements of the system. The condensate discharges through a separate orifice controlled by the inverted bucket.

Because of the dual orifice design, there is a preset controlled pressure differential for the secondary steam system, while maximum pressure differential is available to discharge the condensate.

Table CG-9. Typical Design Parameters for the Automatic Differential Condensate Controller					
Body and Cap Materials Cast Iron Steel					
Connections	1/2" thru 2"	1" thru 2"			
Type Connections	Screwed	Screwed			
Operating Pressure (psig)	0 thru 250	0 thru 650			
Capacity (lbs/hr)	To 20 000	To 20 000			

Figure CG-18. Condensate Controller Operation





Steam Trap Selection

To obtain the full benefits from the traps described in the preceding section, it is essential to select traps of the correct size and pressure for a given job and to install and maintain them properly. One of the purposes of this section is to supply the information to make that possible. Actual installation and operation of steam trapping equipment should be performed only by experienced personnel. Selection or installation should always be accompanied by competent technical assistance or advice. This section should never be used as a substitute for such technical advice or assistance. We encourage you to contact Armstrong or its local representative for further details.

Basic Considerations

Unit trapping is the use of a separate steam trap on each steam-condensing unit including, whenever possible, each separate chest or coil of a single machine. The discussion under the Short Circuiting heading explains the "why" of unit trapping versus group trapping.

Rely on experience. Select traps with the aid of experience—either yours, the know-how of your Armstrong Representative or what others have learned in trapping similar equipment.

Do-it-yourself sizing. Do-it-yourself sizing is simple with the aid of Steam-A-ware, Armstrong's sizing and selection software program, which can be downloaded at: **armstrong**international.com.

Even without this computer program, you can easily size steam traps when you know or can calculate:

- 1. Condensate loads in lbs/hr
- 2. The safety factor to use
- 3. Pressure differential
- 4. Maximum allowable pressure
- Condensate load. Each "How To" portion of this section contains formulas and useful information on steam condensing rates and proper sizing procedures.
- 2. Safety factor or experience factor to use. Users have found that they must generally use a safety factor in sizing steam traps. For example, a coil condensing 500 lbs/hr might require a trap that could handle up to 1 500 lbs/hr for best overall performance. This 3:1 safety factor takes care of varying condensate rates, occasional drops in pressure differential and system design factors.

Safety factors will vary from a low of 1.5:1 to a high of 10:1. The safety factors in this book are based on years of user experience.

Configuration affects safety factor. More important than ordinary load and pressure changes is the design of the steam-heated unit itself. Refer to Figs. CG-21, CG-22 and CG-23 showing three condensing units each producing 500 pounds of condensate per hour, but with safety factors of 2:1, 3:1 and 8:1.

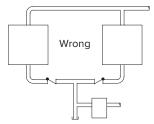


Figure CG-19. Two steam-consuming units drained by a single trap, referred to as group trapping, may result in short circuiting.

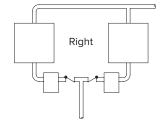


Figure CG-20. Short circuiting is impossible when each unit is drained by its own trap. Higher efficiency is assured.

Short Circuiting

If a single trap connects more than one drain point, condensate and air from one or more of the units may fail to reach the trap. Any difference in condensing rates will result in a difference in the steam pressure drop. A pressure drop difference too small to register on a pressure gauge is enough to let steam from the higher pressure unit block the flow of air or condensate from the lower pressure unit. The net result is reduced heating, output and fuel waste (see Figs. CG-19 and CG-20).

Identical Condensing Rates, Identical Pressures With Differing Safety Factors

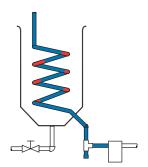


Figure CG-21. Continuous coil, constant pressure gravity flow to trap. 500 lbs/hr of condensate from a single copper coil at 30 psig. Gravity drainage to trap. Volume of steam space very small. 2:1 safety factor.

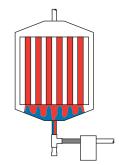


Figure CG-22. Multiple pipes, modulated pressure gravity flow to trap. 500 lbs/hr of condensate from unit heater at 80 psig. Multiple tubes create minor short-circuiting hazard. Use 3:1 safety factor at 40 psig.

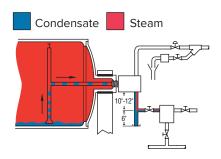


Figure CG-23. Large cylinder, syphon drained. 500 lbs/hr from a 4' diameter, 10' long cylinder dryer with 115 cu ft of space at 30 psig. The safety factor is 3:1 with a DC and 8:1 with an IB.

Steam Trap Selection



Economical steam trap/orifice selection. While an adequate safety factor is needed for best performance, too large a factor causes problems. In addition to higher costs for the trap and its installation, a needlessly oversized trap wears out more quickly. And in the event of a trap failure, an oversized trap loses more steam, which can cause water hammer and high back pressure in the return system.

3. Pressure differential. Maximum differential is the difference between boiler or steam main pressure or the downstream pressure of a PRV and return line pressure. See Fig. CG-24. The trap must be able to open against this pressure differential.

NOTE: Because of flashing condensate in the return lines, don't assume a decrease in pressure differential due to static head when elevating.

Operating differential. When the plant is operating at capacity, the steam pressure at the trap inlet may be lower than steam main pressure. And the pressure in the condensate return header may go above atmospheric.

If the operating differential is at least 80% of the maximum differential, it is safe to use maximum differential in selecting traps.

Modulated control of the steam supply causes wide changes in pressure differential. The pressure in the unit drained may fall to atmospheric or even lower (vacuum). This does not prevent condensate drainage if the installation practices in this handbook are followed.

IMPORTANT: Be sure to read the discussion to the right, which deals with less common but important reductions in pressure differential.

4. Maximum allowable pressure. The trap must be able to withstand the maximum allowable pressure of the system or design pressure. It may not have to operate at this pressure, but it must be able to contain it. As an example, the maximum inlet pressure is 350 psig and the return line pressure is 150 psig. This results in a differential pressure of 200 psi; however, the trap must be able to withstand 350 psig maximum allowable pressure. See Fig. CG-24.

Factors Affecting Pressure Differential

Except for failures of pressure control valves, differential pressure usually varies on the low side of the normal or design value. Variations in either the inlet or discharge pressure can cause this.

Inlet pressure can be reduced below its normal value by:

- 1. A modulating control valve or temperature regulator.
- "Syphon drainage." Every 2' of lift between the drainage point and the trap reduces the inlet pressure (and the differential) by one psi. See Fig. CG-25.

Discharge pressure can be increased above its normal value by:

- 1. Pipe friction.
- Other traps discharging into a return system of limited capacity.
- 3. Elevating condensate. Every 2' of lift increases the discharge pressure (and the differential) by one psi when the discharge is only condensate. However, with flash present, the extra back pressure could be reduced to zero. See Fig. CG-26, noting the external check valve.

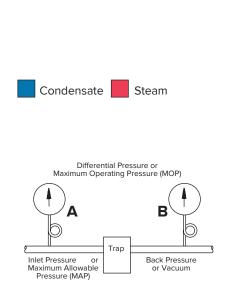


Figure CG-24. "A" minus "B" is Pressure Differential: If "B" is back pressure, subtract it from "A". If "B" is vacuum, add it to "A".

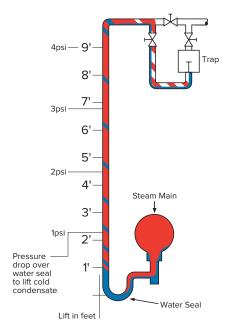


Figure CG-25. Condensate from gravity drain point is lifted to trap by a syphon. Every 2' of lift reduces pressure differential by 1 psi. Note seal at low point and the trap's internal check valve to prevent backflow.

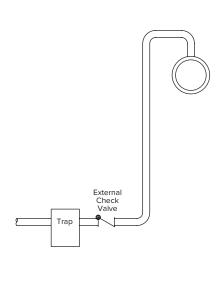


Figure CG-26. When trap valve opens, steam pressure will elevate condensate. Every 2' of lift reduces pressure differential by 1 psi.



How to Trap Steam Distribution Systems

Steam distribution systems link boilers and the equipment actually using steam, transporting it to any location in the plant where its heat energy is needed.

The three primary components of steam distribution systems are boiler headers, steam mains and branch lines. Each fulfills certain requirements of the system and, together with steam separators and steam traps, contributes to efficient steam use.

Drip legs. Common to all steam distribution systems is the need for drip legs at various intervals (Fig. CG-27). These are provided to:

- Let condensate escape by gravity from the fast-moving steam.
- Store the condensate until the pressure differential can discharge it through the steam trap.

Figure CG-27. Drip Leg Sizing

The properly sized drip leg will capture condensate. Too small a drip leg can actually cause a venturi "piccolo" effect where pressure drop pulls condensate out of the trap. See Table CG-13 on page CG-19.



Chart CG-6. Recommendation Chart (See Page CG-4 for "Feature Code" References.)				
Equipment Being Trapped	Alternate Choice			
Boiler Header	IBLV M, E, L, N, B, Q	*F&T		

*On superheated steam never use an F&T type trap.

Always use an IB with internal check valve and burnished valve and seat.

Chart CG-7. Recommendation Chart						
Equipment Being Trapped	1st Choice, Feature Code and Alternate Choice(s)	0 - 30 psig	Above 30 psig			
Steam Mains and Branch Lines Non-	B, M, N, L, F, E, C, D, Q	*IB	*IB			
freezing Conditions	Alternate Choice	F&T	**F&T			
Steam Mains and	B, C, D, E, F, L, M, N, Q, J	*IB	*IB			
Branch Lines Freezing Conditions	Alternate Choice	Therm	nostatic or CD			

^{*}Provide internal check valve when pressures fluctuate. **Use IBLV above F&T pressure/temperature limitations.

Boiler Headers

A boiler header is a specialized type of steam main that can receive steam from one or more boilers. It is most often a horizontal line which is fed from the top and in turn feeds the steam mains. It is important to trap the boiler header properly to assure that any carryover (boiler water and solids) is removed before distribution into the system.

Steam traps that serve the header must be capable of discharging large slugs of carryover as soon as they are present. Resistance to hydraulic shock is also a consideration in the selection of traps.

Trap selection and safety factor for boiler headers (saturated steam only). A 1.5:1 safety factor is recommended for virtually all boiler header applications. The required trap capacity can be obtained by using the following formula: Required Trap Capacity = Safety Factor x Load Connected to Boiler(s) x Anticipated Carryover (typically 10%).

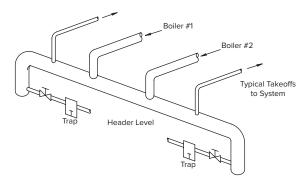
EXAMPLE: What size steam trap will be required on a connected load of 50,000 lbs/hr with an anticipated carryover of 10%? Using the formula:

Required Trap Capacity = 1.5 x 50 000 x 0.10 = 7 500 lbs/hr.

The ability to respond immediately to slugs of condensate, excellent resistance to hydraulic shock, dirt-handling ability and efficient operation on very light loads are features that make the inverted bucket the most suitable steam trap for this application.

Installation. If steam flow through the header is in one direction only, a single steam trap is sufficient at the downstream end. With a midpoint feed to the header (Fig. CG-28), or a similar two-directional steam flow arrangement, each end of the boiler header should be trapped.

Figure CG-28. Boiler Headers



Drip leg same as the header diameter up to 4." Above 4", 1/2 header size, but never less than 4."

NOTE: On superheated steam, use an IB with internal check valve and burnished valve and seat.





Steam Mains

One of the most common uses of steam traps is the trapping of steam mains. These lines need to be kept free of air and condensate in order to keep steam-using equipment operating properly. Inadequate trapping on steam mains often leads to water hammer and slugs of condensate that can damage control valves and other equipment.

There are two methods used for the warm-up of steam mains—supervised and automatic. Supervised warm-up is widely used for initial heating of large-diameter and/or long mains. The suggested method is for drip valves to be opened wide for free blow to the atmosphere before steam is admitted to the main. These drip valves are not closed until all or most of the warm-up condensate has been

discharged. Then the traps take over the job of removing condensate that may form under operating conditions. Warm-up of principal piping in a power plant will follow much the same procedure.

Automatic warm-up is when the boiler is fired, allowing the mains and some or all equipment to come up to pressure and temperature without manual help or supervision.

CAUTION: Regardless of warm-up method, allow sufficient time during the warm-up cycle to minimize thermal stress and prevent any damage to the system.

Trap selection and safety factor for steam mains (saturated steam only). Select trap to discharge condensate produced by radiation losses at running load. Sizing for start-up loads results in oversized traps, which may wear prematurely. Size drip legs to collect condensate during low-pressure, warm-up conditions. (See Table CG-13 on page CG-21.) Condensate loads of insulated pipe can be found in Table CG-10. All figures in the table assume the insulation to be 75% effective. For pressures or pipe sizes not included in the table, use the following formula:

$$C = \frac{A \times U \times (T_1 - T_2)E}{H}$$

Where:

 T_2

C = Condensate in lbs/hr-foot

A = External area of pipe in square feet (Table CG-10, Col. 2)

U = Btu/sq ft/degree temperature difference/hr from Chart CG-7 (page CG-19)

 T_1 = Steam temperature in °F

E = 1 minus efficiency of insulation (Example: 75% efficient insulation:

Air temperature in °F

1 - .75 = .25 or E = .25)

H = Latent heat of steam(See Steam Table on page CG-5)

Pressure, psig	Table CG-10. Condensation in Insulated Pipes Carrying										
Pipe Size (in) sq ft Per Lineal ft Pounds of Condensate Per Hour Per Lineal Foot 1 344 .05 .06 .07 .10 .12 .14 .186 .221 .285 1-1/4 .434 .06 .07 .09 .12 .14 .17 .231 .273 .355 1-1/2 .497 .07 .08 .10 .14 .16 .19 .261 .310 .400 2 .622 .08 .10 .13 .17 .20 .23 .320 .379 .490 2-1/2 .753 .10 .12 .15 .20 .24 .28 .384 .454 .599 3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .714 3-1/2 1.047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 1.178 .15 .18 <	in Quiet Air	in Quiet Air at 70°F (Insulation assumed to be 75% efficient.)									
Cin Lineal ft Pounds of Condensate Per Hour Per Lineal Foot	Pressur	e, psig	15	30	60	125	180	250	450	600	900
1	Pipe Size	sq ft Per		Pour	de of C	`onden	cate D	or Hou	r Dor I in	eal Eoot	.
1-1/4 .434 .06 .07 .09 .12 .14 .17 .231 .273 .359 1-1/2 .497 .07 .08 .10 .14 .16 .19 .261 .310 .400 2 .622 .08 .10 .13 .17 .20 .23 .320 .379 .490 2-1/2 .753 .10 .12 .15 .20 .24 .28 .384 .454 .590 3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .714 3-1/2 .1047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 .1178 .15 .18 .22 .27 .37 .44 .51 .698 .826 .89 5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.05	(in)	Lineal ft		Foun	ius oi c	Jonaen	sate F	ei i iou	rei Liii	ear i oot	
1-1/2 .497 .07 .08 .10 .14 .16 .19 .261 .310 .400 2 .622 .08 .10 .13 .17 .20 .23 .320 .379 .498 2-1/2 .753 .10 .12 .15 .20 .24 .28 .384 .454 .596 3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .712 3-1/2 .1047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 .1178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 .1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 1.25	1	.344	.05	.06	.07	.10	.12	.14	.186	.221	.289
2 .622 .08 .10 .13 .17 .20 .23 .320 .379 .498 2-1/2 .753 .10 .12 .15 .20 .24 .28 .384 .454 .590 3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .714 3-1/2 .1047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 .1,178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 1,456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1,735 .20 .25 .32 .44 .51 .59 .809 .959 1.25 8 2,260 .27 .32 .41 .55 .66 .76 1.051 1,244 .162	1-1/4	.434	.06	.07	.09	.12	.14	.17	.231	.273	.359
2-1/2 .753 .10 .12 .15 .20 .24 .28 .384 .454 .590 3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .714 3-1/2 1.047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 1.178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 .125 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 .162 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01	1-1/2	.497	.07	.08	.10	.14	.16	.19	.261	.310	.406
3 .916 .12 .14 .18 .24 .28 .33 .460 .546 .714 3-1/2 1.047 .13 .16 .20 .27 .32 .38 .520 .617 .80 4 1.178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 .125 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39	2	.622	.08	.10	.13	.17	.20	.23	.320	.379	.498
3-1/2 1.047 13 16 .20 .27 .32 .38 .520 .617 .80 4 1.178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 1.25 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62 <td>2-1/2</td> <td>.753</td> <td>.10</td> <td>.12</td> <td>.15</td> <td>.20</td> <td>.24</td> <td>.28</td> <td>.384</td> <td>.454</td> <td>.596</td>	2-1/2	.753	.10	.12	.15	.20	.24	.28	.384	.454	.596
4 1.178 .15 .18 .22 .30 .36 .43 .578 .686 .89 5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 1.25 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	3	.916	.12	.14	.18	.24	.28	.33	.460	.546	.714
5 1.456 .18 .22 .27 .37 .44 .51 .698 .826 1.07 6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 1.25 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	3-1/2	1.047	.13	.16	.20	.27	.32	.38	.520	.617	.807
6 1.735 .20 .25 .32 .44 .51 .59 .809 .959 1.25 8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	4	1.178	.15	.18	.22	.30	.36	.43	.578	.686	.897
8 2.260 .27 .32 .41 .55 .66 .76 1.051 1.244 1.62 10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	5	1.456	.18	.22	.27	.37	.44	.51	.698	.826	1.078
10 2.810 .32 .39 .51 .68 .80 .94 1.301 1.542 2.01 12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	6	1.735	.20	.25	.32	.44	.51	.59	.809	.959	1.253
12 3.340 .38 .46 .58 .80 .92 1.11 1.539 1.821 2.39 14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	8	2.260	.27	.32	.41	.55	.66	.76	1.051	1.244	1.628
14 3.670 .42 .51 .65 .87 1.03 1.21 1.688 1.999 2.62	10	2.810	.32	.39	.51	.68	.80	.94	1.301	1.542	2.019
	12	3.340	.38	.46	.58	.80	.92	1.11	1.539	1.821	2.393
	14	3.670	.42	.51	.65	.87	1.03	1.21	1.688	1.999	2.624
<u> 16 4.200 .47 .57 .74 .99 1.19 1.38 1.927 2.281 2.99</u>	16	4.200	.47	.57	.74	.99	1.19	1.38	1.927	2.281	2.997
18 4.710 .53 .64 .85 1.11 1.31 1.53 2.151 2.550 3.35	18	4.710	.53	.64	.85	1.11	1.31	1.53	2.151	2.550	3.351
20 5.250 .58 .71 .91 1.23 1.45 1.70 2.387 2.830 3.72	20	5.250	.58	.71	.91	1.23	1.45	1.70	2.387	2.830	3.725
24 6.280 .68 .84 1.09 1.45 1.71 2.03 2.833 3.364 4.43	24	6.280	.68	.84	1.09	1.45	1.71	2.03	2.833	3.364	4.434

Table CG-1	1. The Warm	ing-Up Lo	oad from 7	70°F, Scho	edule 40 F	Pipe		
Pressu	ıre, psig	2	15	30	60	125	180	250
Pipe Size (in)	wt of Pipe Per ft (lbs)		Pound	ds of Con	densate	Per Linea	al Foot	
1	1.69	.030	.037	.043	.051	.063	.071	.079
1-1/4	2.27	.040	.050	.057	.068	.085	.095	.106
1-1/2	2.72	.048	.059	.069	.082	.101	.114	.127
2	3.65	.065	.080	.092	.110	.136	.153	.171
2-1/2	5.79	.104	.126	.146	.174	.215	.262	.271
3	7.57	.133	.165	.190	.227	.282	.316	.354
3-1/2	9.11	.162	.198	.229	.273	.339	.381	.426
4	10.79	.190	.234	.271	.323	.400	.451	.505
5	14.62	.258	.352	.406	.439	.544	.612	.684
6	18.97	.335	.413	.476	.569	.705	.795	.882
8	28.55	.504	.320	.720	.860	1.060	1.190	1.340
10	40.48	.714	.880	1.020	1.210	1.500	1.690	1.890
12	53.60	.945	1.170	1.350	1.610	2.000	2.240	2.510
14	63.00	1.110	1.370	1.580	1.890	2.340	2.640	2.940
16	83.00	1.460	1.810	2.080	2.490	3.080	3.470	3.880
18	105.00	1.850	2.280	2.630	3.150	3.900	4.400	4.900
20	123.00	2.170	2.680	3.080	3.690	4.570	5.150	5.750
24	171.00	3.020	3.720	4.290	5.130	6.350	7.150	8.000

Table CG-12. Pip	e Weights Per Foo	t in Pounds		
Pipe Size (in)	Schedule 40	Schedule 80	Schedule 160	XX Strong
1	1.69	2.17	2.85	3.66
1-1/4	2.27	3.00	3.76	5.21
1-1/2	2.72	3.63	4.86	6.41
2	3.65	5.02	7.45	9.03
2-1/2	5.79	7.66	10.01	13.69
3	7.57	10.25	14.32	18.58
3-1/2	9.11	12.51	-	22.85
4	10.79	14.98	22.60	27.54
5	14.62	20.78	32.96	38.55
6	18.97	28.57	45.30	53.16
8	28.55	43.39	74.70	72.42
10	40.48	54.74	116.00	-
12	53.60	88.60	161.00	-
14	63.00	107.00	190.00	-
16	83.00	137.00	245.00	-
18	105.00	171.00	309.00	-
20	123.00	209.00	379.00	-
24	171.00	297.00	542.00	-



How to Trap Steam Distribution Systems

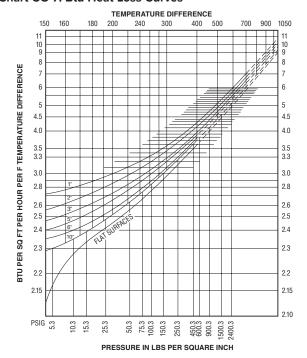
For traps installed between the boiler and the end of the steam main, apply a 2:1 safety factor. Apply a 3:1 safety factor for traps installed at the end of the main or ahead of reducing and shutoff valves that are closed part of the time.

The inverted bucket trap is recommended because it can handle dirt and slugs of condensate and resists hydraulic shock. In addition, should an inverted bucket fail, it usually does so in the open position.

Installation. Both methods of warm-up use drip legs and traps at all low spots or natural drainage points such as:

Ahead of risers End of mains Ahead of expansion joints or bends Ahead of valves or regulators

Chart CG-7. Btu Heat Loss Curves



Install drip legs and drain traps even where there are no natural drainage points (See Figs. CG-29, CG-30 and CG-31). These should normally be installed at intervals of about 300' and never longer than 500'.

On a supervised warm-up, make drip leg length at least 1-1/2 times the diameter of the main, but never less than 10". Make drip legs on automatic warm-ups a minimum of 28" in length. For both methods, it is a good practice to use a drip leg the same diameter as the main up to 4" pipe size and at least 1/2 of the diameter of the main above that, but never less than 4". See Table CG-13.

M	D	н		
		Drip Leg Ler	ngth Min. (in)	
Steam Main Size (in)	Drip Leg Diameter (in)	Supervised Warm-Up	Automatic Warm-Up	
1/2	1/2	10	28	
3/4	3/4	10	28	
1	1	10	28	
2	2	10	28	
3	3	10	28	
4	4	10	28	
6	4	10	28	
8	4	12	28	
10	6	15	28	
12	6	18	28	
14	8	21	28	
16	8	24	28	
18	10	27	28	
20	10	30	30	
24	12	36	36	

	CG-8. Recommendation Chart age CG-4 for "Feature Code" References.				
Equipment Being Trapped	1st Choice and Feature Code	Alternate Choice			
Steam Separator	IBLV B, M, L, E, F, N, Q	*DC			

^{*}DC is 1st choice where steam quality is 90% or less.

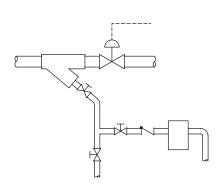


Figure CG-29. Trap draining strainer ahead of PRV.

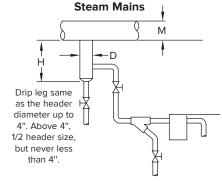


Figure CG-30. Trap draining drip leg on main.

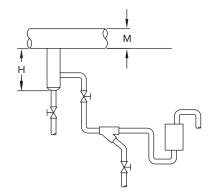
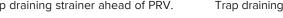


Figure CG-31. Trap draining drip leg at riser. Distance "H" in inches ÷ 28 = psig static head for forcing water through the trap.



How to Trap Steam Distribution Systems



Branch Lines

Branch lines are take-offs from the steam mains supplying specific pieces of steam-using equipment. The entire system must be designed and hooked up to prevent accumulation of condensate at any point.

Trap selection and safety factor for branch lines. The formula for computing condensate load is the same as that used for steam mains. Branch lines also have a recommended safety factor of 3:1.

Installation. Recommended piping from the main to the control is shown in Fig. CG-32 for runouts under 10' and Fig. CG-33 for runouts over 10'. See Fig. CG-34 for piping when control valve must be below the main.

Install a full pipe-size strainer ahead of each control valve as well as ahead of the PRV, if used. Provide blowdown valves, preferably with IB traps. A few days after starting the system, examine the strainer screens to see if cleaning is necessary.

Separators

Steam separators are designed to remove any condensate that forms within steam distribution systems. They are most often used ahead of equipment where especially dry steam is essential. They are also common on secondary steam lines, which by their very nature have a large percentage of entrained condensate.

Branch Lines

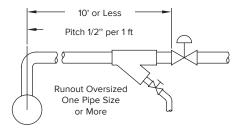


Figure CG-32. Piping for runout less than 10 ft. No trap required unless pitch back to supply header is less than 1/2" per ft.

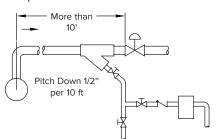


Figure CG-33. Piping for runout greater than 10'. Drip leg and trap required ahead of control valve. Strainer ahead of control valve can serve as drip leg if blowdown connection runs to an inverted bucket trap. This will also minimize the strainer cleaning problem. Trap should be equipped with an internal check valve or a swing check installed ahead of the trap.

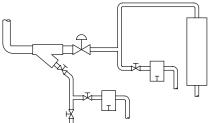


Figure CG-34. Regardless of the length of the runout, a drip leg and trap are required ahead of the control valve located below steam supply. If coil is above control valve, a trap should also be installed at downstream side of control valve.

Trap selection and safety factors for separators. Apply

a 3:1 safety factor in all cases, even though different types of traps are recommended, depending on condensate and pressure levels.

Use the following formula to obtain the required trap capacity:

Required trap capacity in lbs/hr = safety factor x steam flow rate in lbs/hr x anticipated percent of condensate (typically 10% to 20%).

EXAMPLE: What size steam trap will be required on a flow rate of 10 000 lbs/hr? Using the formula:

Required trap capacity = $3 \times 10000 \times 0.10 = 3000$ lbs/hr.

The inverted bucket trap with large vent is recommended for separators. When dirt and hydraulic shock are not significant problems, an F&T type trap is an acceptable alternative.

An automatic differential condensate controller may be preferred in many cases. It combines the best features of both of the above and is recommended for large condensate loads that exceed the separating capability of the separator.

Installation

Connect traps to the separator drain line 10" to 12" below the separator with the drain pipe running the full size of the drain connection down to the trap take-off (Fig. CG-35). The drain pipe and dirt pocket should be the same size as the drain connection.

Steam Separator

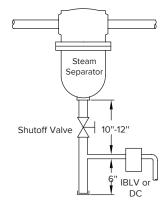


Figure CG-35. Drain downstream side of separator. Full-size drip leg and dirt pocket are required to ensure positive and fast flow of condensate to the trap.

How to Trap Steam Tracer Lines

Steam tracer lines are designed to maintain the fluid in a primary pipe at a certain uniform temperature. In most cases, these tracer lines are used outdoors, which makes ambient weather conditions a critical consideration.

The primary purpose of steam traps on tracer lines is to retain the steam until its latent heat is fully utilized and then discharge the condensate and non-condensable gases. As is true with any piece of heat transfer equipment, each tracer line should have its own trap. Even though multiple tracer lines may be installed on the same primary fluid line, unit trapping is required to prevent short circuiting. See page CG-15.

In selecting and sizing steam traps, it's important to consider their compatibility with the objectives of the system, as traps must:

- Conserve energy by operating reliably over a long period of time.
- 2. Provide abrupt periodic discharge in order to purge the condensate and air from the line.
- 3. Operate under light load conditions.
- 4. Resist damage from freezing if the steam is shut off.

The cost of steam makes wasteful tracer lines an exorbitant overhead no industry can afford.

Trap Selection for Steam Tracer Lines.

The condensate load to be handled on a steam tracer line can be determined from the heat loss from the product pipe by using this formula:

$$Q = \frac{L \times U \times \Delta T \times E}{S \times H}$$

Where:

Q = Condensate load, lbs/hr

L = Length of product pipe between tracer line traps in ft

U = Heat transfer factor in Btu/sq ft/°F/hr (from Chart CG-7, page CG-21)

 ΔT = Temperature differential in °F

E = 1 minus efficiency of insulation (example: 75% efficient insulation or 1 - .75 = .25 or E = .25)

S = Lineal feet of pipe line per sq ft of surface (from Table CG-29, page CG-55)

H = Latent heat of steam in Btu/lb (from Steam Table, page CG-5)

Typical Tracer Installation

Figure CG-36.

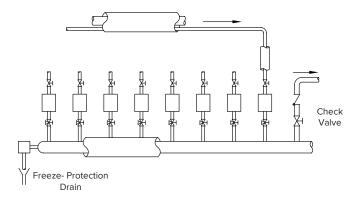


Figure CG-37.

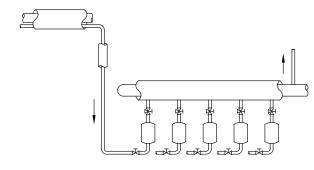


Chart CG-9. Recommendation Chart (See Page CG-4 for "Feature Code" References.)							
Equipment Being Trapped	Alternate Choice						
Tracer Lines	*IB A, B, C, L, J, N, I, K	Thermostatic or CD					

^{*}Select a 5/64" steam trap orifice to conserve energy and avoid plugging with dirt and scale.

Table CG-14. Pipe Size Conversion Table (Divide lineal feet of
pipe by factor given for size and type of pipe to get square feet of
surface.)

Pipe Size (in)	Iron Pipe	Copper or Brass Pipe
1/2	4.55	7.63
3/4	3.64	5.09
1	2.90	3.82
1-1/4	2.30	3.05
1-1/2	2.01	2.55
2	1.61	1.91
2-1/2	1.33	1.52
3	1.09	1.27
4	.848	.954





EXAMPLE: Three tracer lines at 100 psig steam pressure are used on a 20" diameter, 100' long insulated pipe to maintain a temperature of 190°F with an outdoor design temperature of -10°F. Assume further that the pipe insulation is 75% efficient. What is the condensate load?

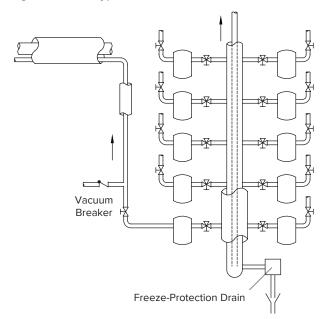
Using the formula:

$$Q = \frac{100 \text{ ft x } 2.44 \text{ Btu/sq ft } \text{-°F - hr x } 200 \text{°F x } .25}{0.191 \text{ lin ft/sq ft x } 880 \text{ Btu/lb}} = 72 \text{ lbs/hr}$$

Now divide by three in order to get the load per tracer line - 24 lbs/hr.

On most tracer line applications, the flow to the steam trap is surprisingly low; therefore, the smallest trap is normally adequate. Based on its ability to conserve energy by operating reliably over a long period of time, handle light loads, resist freezing and purge the system, an inverted bucket trap is recommended for tracer line service.

Figure CG-38. Typical Tracer Installation



Safety factor. Use a 2:1 safety factor whether exposure to ambient weather conditions is involved or not. Do not oversize steam traps or tracer lines. Select a 5/64" steam trap orifice to conserve energy and avoid plugging with dirt and scale.

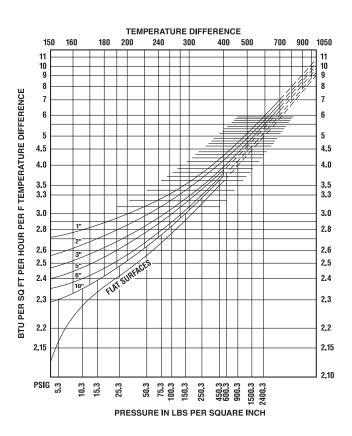
Installation

Install distribution or supply lines at a height above the product lines requiring steam tracing. For the efficient drainage of condensate and purging of non-condensables, pitch tracer lines for gravity drainage and trap all low spots. This will also help avoid tracer line freezing. (See Figs. CG-36, CG-37 and CG-38.)

To conserve energy, return condensate to the boiler. Use vacuum breakers immediately ahead of the traps to ensure drainage on shutdown on gravity drain systems. Freeze-protection drains on trap discharge headers are suggested where freezing conditions prevail.

Chart CG-10. Btu Heat Loss Curves

Unit heat loss per sq ft of surface of uninsulated pipe of various diameters (also flat surface) in quiet air at 75°F for various saturated steam pressures or temperature differences.





How to Trap Superheated Steam Lines

At first glance, this may seem confusing due to the idea that superheated steam produces no condensate; therefore, the steam lines carrying superheated steam should not have any condensate in them. This is true once the system is up to temperature and pressure, but condensate removal is necessary up to this point. This section will explain what superheated steam is and the applications for its use.

The specific heat of any substance (using Btu standards) is the quantity of heat required to raise the temperature of 1 pound by 1 degree F. With this definition, the specific heat of water is 1, and the specific heat of superheated steam varies according to temperature and pressure. Specific heat decreases as the temperature rises but increases as the pressure goes up.

Superheated steam is customarily made by the addition of an extra set of coils inside the boiler or in the exhaust area of the boiler so as to use the "waste" heat from the boiler. Or, by the addition of a superheat chamber somewhere after the boiler, attached to the steam main. A schematic diagram of a steam generator with a superheated section of coil is shown below.

Properties of Superheated Steam

Superheated steam has several properties that make it unsuitable as a heat energy exchange medium yet ideal for work and mass transfer. Unlike saturated steam, the pressure and temperature of superheated steam are independent. As superheat is formed at the same pressure as the saturated steam, the temperature and volume increase.

In high heat release boilers with relatively small drums, separation of steam from water is extremely difficult. The combination of the small volume of water in the drums and rapid load swings produces severe shrink and swell conditions in the drum, which promotes water carryover.

This water can be removed with separators and traps in the steam outlets, but they are not 100% efficient. In

applications where dry steam is a necessity, additional superheating coils are placed in the boiler furnace as convection passes. More heat is added to the steam to vaporize the water carryover, which adds a small amount of superheat to guarantee absolutely dry steam.

Because superheated steam can give up so little heat before it converts back to saturated steam, it is not a good heat-transfer medium. Some processes, such as power plants, require a dry heat in order to do work. Whatever the type of power unit, superheat helps reduce the amount of condensation when starting from cold. Superheat also increases the power output by delaying condensation during the expansion stages in the equipment. Having drier steam at the exhaust end will increase the life of turbine blades.

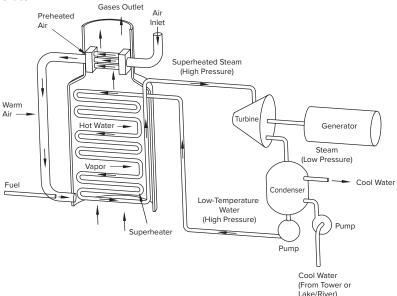
Superheated steam can lose heat without condensing whereas saturated steam cannot. Therefore, superheated steam can be transported through very long steam lines without losing sufficient heat to condense. This permits the delivery of dry steam throughout the entire steam system.

Why Trap Superheated Systems?

The primary reason for traps on superheat systems is the start-up load. It can be heavy because of the large size of the mains. On start-up, manual valves will most likely be used since time is available to open and to close the valves. This is known as supervised start-up. A second reason for steam traps is to handle emergencies such as superheater loss or by-pass, which might require operation on saturated steam. In these unscheduled events, there is no time available for manually opening valves; therefore, steam traps are a necessity.

These are the situations for which proper trap sizing is a must. Condensate must be removed as it forms in any steam system to keep efficiency high and to minimize damaging water hammer and erosion.

Figure CG-39. Steam Generator



Stack

How to Trap Superheated Steam Lines



Sizing Superheat Loads to Traps

The condensate load to a trap used on superheat will vary widely from severe start-up loads to virtually no load during operation. Consequently, this is a demanding application for any steam trap.

During start-up, very large lines are being filled with steam from cold conditions. At this time, only saturated steam at low pressure is in the lines until the line temperature can be increased. This is done slowly over a long period so the lines are not stressed. Large condensate flow combined with low pressure is the start-up condition that requires the use of large capacity traps. These oversized traps are then required to operate at very high pressures with very low capacity requirements during normal superheat operation.

Typical start-up loads can be roughly calculated as follows:

Using:

$$C = \frac{0.114 \text{ Wp (t2-t1)}}{H}$$

Where:

C = Amount of condensate in pounds

Wp = Total weight of pipe (from Table CG-12 on page CG-20)

Total heat of X pressure minus Sensible heat of Y Pressure (Latent heat of steam. For long warm-up times, use the total heat of saturated steam at the superheat steam supply pressure (X) minus the sensible heat of saturated steam at the average pressure (Y) during the warm-up time involved.)

0.114 = Specific heat of steel pipe in btu/lb °F

EXAMPLE:

Assuming a 100°F/hr (37°C/hr) heat-up

14" (35 cm) diameter Schedule 80 line

Supply superheated steam at 1 200 psig 1070°F (85 bar, 577°C)

Ambient temperature is 70°F (21°C)

200 feet (61 m) of run between traps

For the first two hours:

W = (200 ft) (107 lb/ft) = 21 400 lb (9727 kg) $t(2) - t(1) = 270 - 70 = 200^{\circ}\text{F} (93^{\circ}\text{C})$ H = 1.184.8 btu/lb - 196.27 btu/lb = 988.5 btu/lb = (474 kJ)

 $C = \frac{(0.114 \text{ btu/lb °F}) (21 400 \text{ lb}) (200 \text{°F})}{988.5 \text{ btu/lb}} = 493 \text{ lb } (224 \text{ kg})$

For the second two hours:

The only thing that changes is the sensible heat of the saturated steam at average pressure during the time involved.

$$C = \frac{(0.114 \text{ btu/lb }^{\circ}\text{F}) (21 400 \text{ lb}) (200^{\circ}\text{F})}{851.1 \text{ btu/lb}} = 573 \text{ lb } (260 \text{ kg})$$

Table CG-15. Time Period Table									
Time Period	Average Pressure psig (barg)	Temperature at End of Time Period °F (°C)	14" Line Condensation Rate lb/hr (kg/hr)						
1 st 2 hours	5 (.35)	270 (132)	247 (112)						
2 nd 2 hours	140 (9.8)	470 (243)	286 (130)						
3 rd 2 hours	700 (49)	670 (354)	352 (160)						
4 th 2 hours	1 200 (85)	870 (465)	288 (131)						
5 th 2 hours	1 200 (85)	1 070 (577)	260 (118)						

NOTE: For the average pressure of 1,200 psig (85 bar), assume H to be the latent heat of 1,200 psig (85 bar) steam plus superheat at temperature at the end of the period.

To ensure the condensate is removed efficiently, proper drip leg sizing and piping recommendations should also be followed when installing traps on superheat systems. The Table CG-13 on page CG-21 lists the proper drip leg size for given pipe sizes.

The question arises whether insulation should be used on the drip leg, piping leading to the trap, and the trap. The answer is no; unless it is mandatory for safety reasons, this section of the steam system should not be insulated. This ensures that some condensate is continuously being formed ahead of the trap and going to it, thus prolonging the trap's life.

Types of Superheat Traps

Bimetallic

A bimetallic trap is set to not open until condensate has cooled to a temperature below saturation. For the existing pressure, it will remain closed whenever steam of any temperature is in the trap. As the steam temperature rises, the pull of the bimetallic element becomes greater, providing a greater sealing force on the valve. Superheated steam tends to seal the valve better. The bimetallic trap also has the ability to handle large start-up loads. For these reasons, this trap is a good choice for superheat.

During superheat operation, the condensate in the trap must cool to a temperature below the saturation temperature before the trap can open. Condensate may back up into the line and cause damage to the lines, valves and equipment if drip leg size and length before the trap are insufficient.

Inverted Bucket

A water seal prevents steam from getting to the valve, promoting no live steam loss and long life. The valve at the top makes it impervious to dirt and permits removal of air. Large start-up loads can be handled, and the trap can still accommodate small running loads. There are problems associated with its application on superheat, mostly associated with the necessity of maintaining its water seal or "prime." Proper piping is necessary to maintain a prime in the IB.

For proper inverted bucket piping on superheat, refer to Figure CG-31 on page CG-21. When sizing a superheat trap, size for start-up load with no safety factor. Body materials should be selected on the basis of maximum pressure and temperature, including superheat.



How to Trap Space Heating Equipment

Space heating equipment such as unit heaters, air handling units, finned radiation and pipe coils is found in virtually all industries. This type of equipment is quite basic and should require very little routine maintenance. Consequently, the steam traps are usually neglected for long periods of time. One of the problems resulting from such neglect is residual condensate in the heating coil, which can cause damage due to freezing, corrosion and water hammer.

Trap Selection and Safety Factors

Different application requirements involving constant or variable steam pressure determine which type and size of trap should be used. There are two standard methods for sizing traps for coils.

1. Constant Steam Pressure.

INVERTED BUCKET TRAPS AND F&T TRAPS—Use a 3:1 safety factor at operating pressure differentials.

2. Modulating Steam Pressure.

F&T TRAPS AND INVERTED BUCKET TRAPS WITH THERMIC BUCKETS

- 0-15 psig steam—2:1 safety factor at 1/2 psi pressure differential
- 16-30 psig steam—2:1 at 2 psi pressure differential
- Above 30 psig steam—3:1 at 1/2 of maximum pressure differential across the trap.

INVERTED BUCKET TRAPS WITHOUT THERMIC BUCKETS Above 30 psig steam pressure only—3:1 at 1/2 of maximum pressure differential across the trap.

Trap Selection for Unit Heaters and Air Handling Units

You may use three methods to compute the amount of condensate to be handled. Known operating conditions will determine which method to use.

1. Btu method. The standard rating for unit heaters and other air coils is Btu output with 2 psig steam pressure in the heater and entering air temperature of 60°F. To convert from standard to actual rating, use the conversion factors in Table CG-16 (page CG-29). Once the actual operating conditions are known, multiply the condensate load by the proper safety factor.

2. CFM and air temperature rise method. If you know only CFM capacity of fan and air temperature rise, find the actual Btu output by using this simple formula: Btu/hr = CFM x 1.08 x temperature rise in °F.

EXAMPLE: What size trap will drain a 3 500 CFM heater that produces an 80°F temperature rise? Steam pressure is constant at 60 psig.

Using the formula:

 $3500 \times 1.08 \times 80 = 302400 \text{ Btu/hr}.$

Now divide 302 400 Btu/hr by 904.5 Btu (from the Steam Tables) to obtain 334 lbs/hr and then multiply by the recommended safety factor 3. The application needs a trap with a 1 002 lbs/hr capacity.

Derive the 1.08 factor in the above formula as follows: 1 CFM \times 60 = 60 CFH 60 CFH \times .075 lbs of air/cu ft = 4.5 lbs of air/hr 4.5 \times 0.24 Btu/lb -°F (specific heat of air) = 1.08 Btu/hr °F - CFM.

3. Condensate method.

Once you determine Btu output:

- a. Divide Btu output by latent heat of steam at steam pressure used. See Column 2 of Table CG-16 (page CG-29) or the Steam Table (page CG-5). This will give the actual weight of steam condensed. For a close approximation, a rule of thumb could be applied in which the Btu output is simply divided by 1,000.
- Multiply the actual weight of steam condensing by the safety factor to get the continuous trap discharge capacity required.

Chart CG-11. Multipliers for Sizing Traps for Multiple Coils

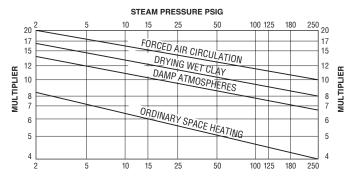


Chart CG-12. Recommendation Chart (See Page CG-4 for "Feature Code" References.)									
Equipment Being	1st Choice and	Constan	t Pressure	1st Choice and	Variat	ole Pressure			
Trapped	Feature Code	0-30 psig	Above 30 psig	Feature Code	0-30 psig	Above 30 psig			
I lait I la atava	B, C, E, K, N	IBLV	IBLV	B, C, G, H, L	F&T	*F&T			
Unit Heaters	Alternate Choice	F&T	*F&T	Alternate Choice	IBLV	IBLV			
Air Handling Haite	B, C, E, K, N, O	IBLV	IBLV	B, C, G, H, L	F&T	*F&T			
Air Handling Units	Alternate Choice	F&T	*F&T	Alternate Choice	IBT	IBLV			
Finned Radiation &	B, C, E, K, N	IBLV	IBLV	B, C, G, H, L	F&T	F&T			
Pipe Coils	Alternate Choice	Thermostatic	Thermostatic	Alternate Choice	IBLV	IBLV			

^{*}Use IBLV above F&T pressure/temperature limitations.

PLEASE NOTE: 1. Provide vacuum breaker wherever subatmospheric pressures occur.

2. Do not use F&T traps on superheated steam.

How to Trap Space Heating Equipment



Trap Selection for Pipe Coils and Finned Radiation

Pipe coils. Insofar as possible, trap each pipe individually to avoid short circuiting.

Single pipe coils. To size traps for single pipes or individually trapped pipes, find the condensing rate per linear foot in Table CG-18 (page CG-29). Multiply the condensing rate per linear foot by the length in feet to get the normal condensate load.

For quick heating, apply a trap selection safety factor of 3:1 and use an inverted bucket trap with a thermic vent bucket. Where quick heating is not required, use a trap selection safety factor of 2:1 and select a standard inverted bucket trap.

Multiple pipe coils. To size traps to drain coils consisting of multiple pipes, proceed as follows:

- Multiply the lineal feet of pipe in the coil by the condensing rate given in Table CG-18. This gives normal condensate load.
- From Chart CG-11 (page CG-27), find the multiplier for your service conditions.
- Multiply normal condensate load by multiplier to get trap required continuous discharge capacity.
 Note that the safety factor is included in the multiplier.

Finned radiation. When Btu output is not known, condensing rates can be computed from Tables CG-17 and CG-19 (page CG-29) with sufficient accuracy for trap selection

Figure CG-40. Trapping and Venting Air Heat Coil

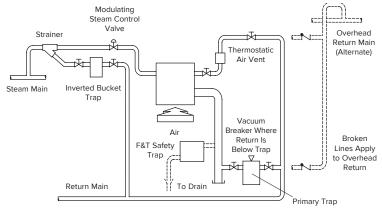
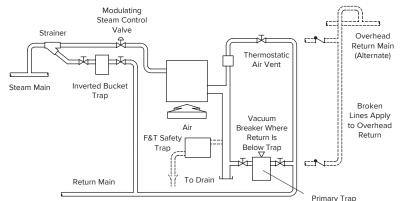


Figure CG-41. Trapping and Venting Air Heat Coil



purposes. To enter Table CG-19, observe size of pipe, size of fins, number of fins and material. Determine condensing rate per foot under standard conditions from Table CG-19. Convert to actual conditions with Table CG-17.

Safety factor recommendations are to:

- Overcome the short circuiting hazard created by the multiple tubes of the heater.
- Ensure adequate trap capacity under severe operating conditions. In extremely cold weather the entering air temperature is likely to be lower than calculated, and the increased demand for steam in all parts of the plant may result in lower steam pressures and higher return line pressures—all of which cut trap capacity.
- 3. Ensure the removal of air and other non-condensables.

WARNING: For low-pressure heating, use a safety factor at the actual pressure differential, not necessarily the steam supply pressure, remembering that the trap must also be able to function at the maximum pressure differential it will experience.

Installation

In general, follow the recommendations of the specific manufacturer. Figs. CG-40, CG-41, CG-42 and CG-43 represent the consensus of space heating manufacturers.

NOTE: For explanation of safety drain trap, see Fig. CG-66 (page CG-49).

Figure CG-42. Generally approved method of piping and trapping high-pressure (above 15 psi) horizontal discharge heaters. Figs. CG-40 and CG-41 drip leg should be 10"-12" minimum.

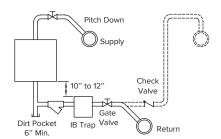
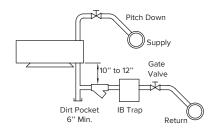


Figure CG-43. Generally approved method of piping and trapping low-pressure (under 15 psi) vertical discharge heaters.





How to Trap Space Heating Equipment

Table CG-16. A Table of Constants for determining the Btu output of a unit heater with conditions other than standard — standard being with 2 lbs steam pressure at 60°F entering air temperature. To apply, multiply the standard Btu capacity rating of heater by the indicated constant. (Reprinted from• ASHRAE Guide by special permission.)

Steam Pressure	Latent Heat	Entering Air Temperature °F											
Ibs Per sq in of Steam	of Steam	-10	0	10	20	30	40	50	60	70	80	90	100
2	966.3	_	_	_	_	_	1.155	1.078	1.000	0.926	0.853	0.782	0.713
5	960.7	1.640	1.550	1.456	1.370	1.289	1.206	1.127	1.050	0.974	0.901	0.829	0.760
10	952.4	1.730	1.639	1.545	1.460	1.375	1.290	1.211	1.131	1.056	0.982	0.908	0.838
15	945.5	1.799	1.708	1.614	1.525	1.441	1.335	1.275	1.194	1.117	1.043	0.970	0.897
20	939.3	1.861	1.769	1.675	1.584	1.498	1.416	1.333	1.251	1.174	1.097	1.024	0.952
30	928.5	1.966	1.871	1.775	1.684	1.597	1.509	1.429	1.346	1.266	1.190	1.115	1.042
40	919.3	2.058	1.959	1.862	1.771	1.683	1.596	1.511	1.430	1.349	1.270	1.194	1.119
50	911.2	2.134	2.035	1.936	1.845	1.755	1.666	1.582	1.498	1.416	1.338	1.262	1.187
60	903.9	2.196	2.094	1.997	1.902	1.811	1.725	1.640	1.555	1.472	1.393	1.314	1.239
70	897.3	2.256	2.157	2.057	1.961	1.872	1.782	1.696	1.610	1.527	1.447	1.368	1.293
75	893.8	2.283	2.183	2.085	1.990	1.896	1.808	1.721	1.635	1.552	1.472	1.392	1.316
80	891.1	2.312	2.211	2.112	2.015	1.925	1.836	1.748	1.660	1.577	1.497	1.418	1.342
90	885.4	2.361	2.258	2.159	2.063	1.968	1.880	1.792	1.705	1.621	1.541	1.461	1.383
100	880.0	2.409	2.307	2.204	2.108	2.015	1.927	1.836	1.749	1.663	1.581	1.502	1.424

Table CG-17. Finned Radiation Conversion Factors for steam pressures and air temperatures other than 65°F air and 215°F steam.								
Steam	Steam	Entering Air Temperature °F						
Pressure (psig)	Temp. (°F)	45	55	65	70	75	80	90
.9	215.0	1.22	1.11	1.00	.95	.90	.84	.75
5	227.1	1.34	1.22	1.11	1.05	1.00	.95	.81
10	239.4	1.45	1.33	1.22	1.17	1.11	1.05	.91
15	249.8	1.55	1.43	1.31	1.26	1.20	1.14	1.00
30	274.0	1.78	1.66	1.54	1.48	1.42	1.37	1.21
60	307.3	2.10	2.00	1.87	1.81	1.75	1.69	1.51
100	337.9	2.43	2.31	2.18	2.11	2.05	2.00	1.81
125	352.9	2.59	2.47	2.33	2.27	2.21	2.16	1.96
175	377.4	2.86	2.74	2.60	2.54	2.47	2.41	2.21

Table CG-18. Condensing Rates in Bare Pipe Carrying Saturated Steam								
	ssure (psig) e From 70°	Pound	ds of Co	ndensa	te Per h	r Per Li	neal ft	
Pipe Size (in)	sq ft Per Lineal ft	15 30 60 125 180 250 180 204 237 283 310 336						
1/2	.220	.13	.15	.19	.26	.30	.35	
3/4	.275	.15	.19	.24	.33	.38	.45	
1	.344	.19	.23	.28	.39	.46	.54	
1-1/4	.434	.23	.28	.36	.49	.57	.67	
1-1/2	.497	.26	.32	.41	.55	.65	.76	
2	.622	.33	.40	.50	.68	.80	.93	
2-1/2	.753	.39	.47	.59	.81	.95	1.11	
3	.916	.46	.56	.70	.96	1.13	1.31	
3-1/2	1.047	.52	.63	.80	1.08	1.27	1.50	
4	1.178	.58	.70	.89	1.21	1.43	1.72	

Table CG-19. Finned Radiation Condensing Rates with 65°F air and 215°F steam (for trap selection purposes only).							
	Pipe Size (in)	Fin Size (in)	Fins Per Inch	No. of Pipes High on 6" Centers	Condensate lbs/hr Per Foot of Pipe		
				1	1.1		
Steel Pipe, Steel Fins Painted	1-1/4	3-1/4	3 to 4	2	2.0		
				3	2.6		
	1-1/4	4-1/4	3 to 4	1	1.6		
				2	2.4		
Black				3	3.1		
	2	4-1/4	2 to 3	1	1.5		
				2	2.4		
				3	3.1		
				1	1.6		
Copper Pipe	1-1/4	3-1/4	4	2	2.2		
Aluminum				3	2.8		
Fins				1	2.2		
Unpainted	1-1/4	4-1/4	5	2	3.0		
				3	3.6		

How To Trap Process Air Heaters



Process air heaters are used for drying paper, lumber, milk, starch and other products as well as preheating combustion air for boilers.

Common examples of this type of equipment are process dryers, tunnel dryers, and combustion air preheaters. Compared with air heaters for space heating, process air heaters operate at very high temperature, 500°F not being uncommon. These extremely high-temperature applications require high pressure (and occasionally superheated) steam.

Trap Selection and Safety Factor

Determine the condensate load for process air heaters with the following formula:

 $Q = \frac{F \times Cp \times d \times 60 \text{ min/hr} \times \Delta T}{H}$

Where:

Q = Condensate load in lbs/hr
F = Cubic feet of air per minute
Cp = Specific heat of air in Btu/lb—°F
(from Table CG-34, page CG-57)
d = Density of air—.075 lbs/cu ft

 ΔT = Temperature rise in °F H = Latent heat of steam in Btu/lb

(Steam Table, page CG-5)

EXAMPLE: What would be the condensate load on a tunnel dryer coil handling 2 000 CFM of air and requiring a 100°F temperature rise? The steam pressure is 45 psig. Using the formula:

 $O = 2000 \times .24 \times .075 \times 60 \times 100$

915

Q = 236 lbs/hr

Multiplying by a safety factor of 2—which is recommended for all constant pressure process air heaters—indicates that a trap with a capacity of 472 lbs/hr will be required. This is based on one coil. For higher air temperature rises, additional coils in series may be required.

Safety Factors

For constant steam pressure, use a safety factor of 2:1 at operating pressure differential. For modulating steam pressure, use a safety factor of 3:1 at 1/2 of maximum pressure differential across the trap.

Installation

Give piping for an entire piece of process air heating equipment—including all steam trap connections—adequate allowance for expansion due to the wide temperature variations. Mount traps 10"-12" below the coils with a dirt pocket of at least 6". On both constant and modulated pressure heaters, install a vacuum breaker between the coil and the steam trap. Install an air vent on each coil to remove air and other non-condensables that can cause rapid corrosion.

See Fig. CG-44.

Consider a safety drain if condensate is elevated after the trap or if back pressure is present. See page CG-49 for piping diagram and explanation.

Figure CG-44. Process Air Heater

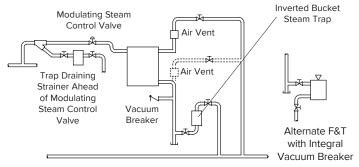


Chart CG-13. Recommendation Chart (See Page CG-4 for "Feature Code" References.)								
F	1st Choice	Constant Pressure		1st Choice	Variable Pressure			
Equipment Being Trapped	and Feature Code	0-30 psig	Above 30 psig	and Feature Code	0-30 psig	Above 30 psig		
Dunnen Air	A, B, F, I, K, M	IB	IB	B, C, G, H, L	F&T	*F&T		
Process Air Heaters	Alternate Choice	F&T	IBLV	Alternate Choice	IBLV	IBLV		

^{*}Use IBLV above F&T pressure temperature limitations.

PLEASE NOTE:

Provide vacuum breaker wherever subatmospheric pressures occur.

^{2.} Do not use F&T traps on superheated steam.

How To Trap - Shell & Tube Heat Exchangers & Submerged Coils

Submerged coils are heat transfer elements that are immersed in the liquid to be heated, evaporated or concentrated. This type of coil is found in virtually every plant or institution that uses steam. Common examples are water heaters, reboilers, suction heaters, evaporators and vaporizers. These are used in heating water for process or domestic use, vaporizing industrial gases such as propane and oxygen, concentrating in-process fluids such as sugar, black liquor and petroleum, and heating fuel oil for easy transfer and atomization.

Different application requirements involving constant or variable steam pressure determine which type of trap should be used. Trap selection factors include the ability to handle air at low differential pressures, energy conservation and the removal of dirt and slugs of condensate. Three standard methods of sizing help determine the proper type and size traps for coils.

Safety Factor

- Constant Steam Pressure. INVERTED BUCKET TRAPS OR F&T TRAPS—use a 2:1 safety factor at operating pressure differentials.
- Modulating Steam Pressure. F&T TRAPS OR INVERTED BUCKET TRAPS.
 - 1. 0-15 psig steam—2:1 at 1/2 psi pressure differential.
 - 2. 16-30 psig steam—2:1 at 2 psi pressure differential.
 - 3. Above 30 psig steam—3:1 at 1/2 of maximum pressure differential across the trap.
- Constant or Modulating Steam Pressure with Syphon Drainage. An automatic differential condensate controller with a safety factor of 3:1 should be used. An alternate is an IBLV with a 5:1 safety factor.

Apply the safety factor at full differential on constant steam pressure. Apply the safety factor at 1/2 maximum differential for modulating steam pressure.

Shell and Tube Heat Exchangers

One type of submerged coil is the shell and tube heat exchanger (Fig. CG-45). In these exchangers, numerous tubes are installed in a housing or shell with confined free area. This ensures positive contact with the tubes by any fluid flowing in the shell. Although the term submerged coil implies that steam is in the tubes and the tubes are submerged in the liquid being heated, the reverse can also be true, where steam is in the shell and a liquid is in the tubes.

Trap Selection for Shell and Tube Heat Exchangers

To determine the condensate load on shell and tube heaters, use the following formula when actual rating is known.* (If heating coil dimensions alone are known, use formula shown for embossed coils. Be sure to select applicable "U" factor):

$$Q = \frac{L \times \Delta T \times C \times 500 \times sg}{H}$$

Where:

Q = Condensate load in lbs/hr

L = Liquid flow in GPM ΔT = Temperature rise in °F

C = Specific heat of liquid in Btu/lb-°F (Table CG-33,

page CG-57)

500 = 60 min/hr x 8.33 lbs/gal

sg = Specific gravity of liquid (Table CG-33)

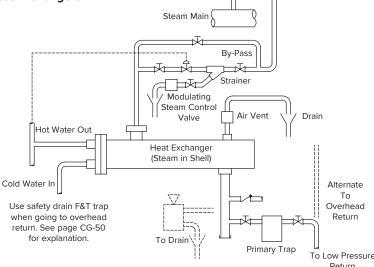
H = Latent heat of steam in Btu/lb (Steam Table, page CG-5)

EXAMPLE: Assume a water flow rate of 50 GPM with an entering temperature of 40°F and a leaving temperature of 140°F. Steam pressure is 15 psig. Determine the condensate load.

Using the formula:

$$Q = \frac{50 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb} \cdot \text{F} \times 500 \times 1.0 \text{ sg}}{945 \text{ Btu/lb}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 1 \text{ Btu/lb}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F} \times 100^{\circ}\text{F}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F}}{100 \text{ GPM}} = \frac{100 \text{ GPM} \times 100^{\circ}\text{F}}{100 \text{ GPM}} = \frac{100 \text{ GPM}}{100 \text{ GPM}} =$$

Figure CG-45. Shell And Tube Heat Exchangers (Typical Piping Diagram)





^{*} Size steam traps for reboilers, vaporizers and evaporators (processes that create vapor) using the formula for EMBOSSED COILS on page CG-32.



How To Trap – Shell & Tube Heat Exchangers & Submerged Coils

Rule of Thumb for Computing Condensing Rate for Water Heaters: Raising the temperature of 100 gallons of water 1°F will condense one pound of steam.

Embossed Coils

Very often open tanks of water or chemicals are heated by means of embossed coils (Fig. CG-46). Upsetting grooves in the sheet metal of the two halves produce the spaces for the steam. When welded together, the halves form the passages for steam entry, heat transfer and condensate evacuation.

Trap Selection for Embossed Coils

Calculate the condensate load on embossed coils with the following formula:

 $Q = A \times U \times Dm$

Where:

Q = Total heat transferred in Btu per hour A = Area of outside surface of coil in sq ft

U = Overall rate of heat transfer in Btu per hr-sq ft-°F. See Tables CG-20 and CG-21.

Dm = Logarithmic mean temperature difference between steam and liquid (as between inlet and outlet of a heat exchanger) in °F

 $Dm = \frac{D1-D2}{Log_{e}\frac{(D1)}{(D2)}}$

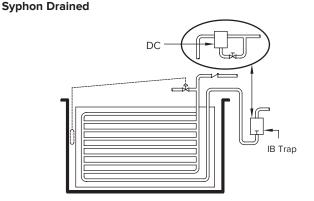
D1 = Greatest temperature difference D2 = Least temperature difference

Logarithmic mean temperature difference can be determined with slightly less accuracy using the nomograph, Chart CG-16 (page CG-36).

U values are determined by tests under controlled conditions.

Table CG-20. Pipe Coil U Values in Btu/hr-sq ft-°F						
Tyme of Comice	Circulation					
Type of Service	Natural	Forced				
Steam to Water	50-200	150-1 200				
1-1/2" Tube Heaters	180	450				
3/4" Tube Heaters	200	500				
Steam to Oil	10-30	50-150				
Steam to Boiling Liquid	300-800	-				
Steam to Boiling Oil	50-150	-				

Figure CG-46. Thermostatic Controlled Embossed Coil,



Tables CG-20 and CG-21 show the commonly accepted range for submerged embossed coils. For trap selection purposes, use a U value that is slightly greater than the conservative U value selected for estimating actual heat transfer.

EXAMPLE:

A = 20 sq ft of coil surfaceU = $175 \text{ Btu/sq ft-hr-}^{\circ}\text{F}$

Conditions:

Water in: 40°F Water out: 150°F

Steam pressure: 125 psig or 353°F

D1 = 353 - 40, or 313 D2 = 353 - 150, or 203

Dividing by 4 to get within range of Chart CG-16 (page CG-36), we have:

D1 = 78.25

D1 = 78.25 D2 = 50.75

Mean difference from chart is 63°F.

Multiplying by 4, the mean temperature difference for the original values is 252°F. Substituting in the equation:

Q = 20 x 175 x 252 = 882 000 Btu/hr

Btu transferred per hour.

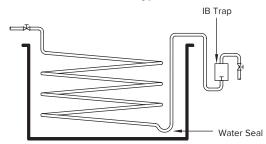
Latent heat of steam at 125 psig = 867.6

 $\frac{882\ 000}{867.6}$ = 1 016 lbs condensate per hr

To determine trap capacity required, multiply condensing rate by the recommended safety factor.

Table CG-21. Embossed Coil U Values in Btu/hr-sq ft-°F						
Time of Service	Circulation					
Type of Service	Natural	Forced				
Steam to Watery Solutions	100-200	150-275				
Steam to Light Oil	40-45	60-110				
Steam to Medium Oil	20-40	50-100				
Steam to Bunker C	15-30	40-80				
Steam to Tar Asphalt	15-25	18-60				
Steam to Molten Sulphur	25-35	35-45				
Steam to Molten Paraffin	25-35	40-50				
Steam to Molasses or Corn Syrup	20-40	70-90				
Downtherm to Tar Asphalt	15-30	50-60				

Figure CG-47. Continuous Coil, Syphon Drained





How To Trap - Shell & Tube Heat Exchangers & Submerged Coils

Pipe Coils

Pipe coils are heat transfer tubes immersed in vessels that are large in volume compared to the coils themselves (Fig. CG-47, page CG-32). This is their primary difference when compared to shell and tube heat exchangers. Like embossed coils, they may be drained by gravity or syphon drained, depending on the conditions prevailing at the installation site. Unlike embossed coils, most pipe coils are installed in closed vessels.

Trap Selection for Pipe Coils

Determine the condensate load for pipe coils by applying one of the formulas, depending on known data. If capacity is known, use the formula under shell and tube heat exchangers. When physical dimensions of coil are known, use the formula under embossed coils.

Installation

When gravity drainage is utilized on shell and tube heat exchangers, embossed coils and pipe coils, locate the steam trap below the heating coil. Under modulating pressure, use a vacuum breaker. This can be integral in F&T traps or mounted off the inlet piping on an inverted bucket trap. Place an ample drip leg ahead of the trap to act as a reservoir. This ensures coil drainage when there is a maximum condensate load and a minimum steam pressure differential.

Avoid lifting condensate from a shell and tube heat exchanger, embossed coil or pipe coil under modulated control. However, if it must be done, the following is suggested:

- Do not attempt to elevate condensate more than 1' for every pound of normal pressure differential, either before or after the trap.
- 2. If condensate lift takes place after the steam trap, install a low-pressure safety drain. (See page CG-49).
- If condensate lift takes place ahead of the steam trap (syphon lift), install an automatic differential condensate controller to efficiently vent all flash steam.

For Pounds of Steam Condensed Per sq ft Per Hour of Submerged Coil Surface, see Chart CG-17 (page CG-36).

Equipment Being	1st Choice and	Constant Pressure		1st Choice and	Variable	Pressure
Equipment Being Trapped	Feature Code	0-30 psig	Above 30 psig	Feature Code	0-30 psig	Above 30 psig
Shell and Tube	B, C, E, F G, I, K N, Q	IBLV	IBLV	B, C, G, H, I, L	F&T [†]	F&T [†]
Heat Exchangers	Alternate Choice	DC F&T	DC *F&T	Alternate Choice	DC IBT	DC IBLV
Embossed Coils and Pipe Coils	B, C, E, F, G, H, I K, N, Q	DC	DC	B, C, G, H, I, L	DC	DC
Syphon Drain	Alternate Choice	IBLV	IBLV	Alternate Choice	F&T [†]	*F&T [†]
Embossed Coild	B, C, E, F, G, I, K N, Q	IBLV	IBLV	B, C, G, H, I, L	F&T [†]	*F&T [†]
and Pipe Coils Gravity Drain	Alternate Choice	DC F&T	DC F&T	Alternate Choice	DC IBT	DC IBLV

^{*}Use IBLV above pressure/temperature limitations.

Please Note:

- Provide vacuum breaker wherever subatmospheric pressures occur.
- 2. Provide a safety drain when elevating condensate on modulating service.



If dirt and large volumes of air must be handled, an inverted bucket trap with an external thermostatic air vent can be used effectively.

How to Trap Evaporators



Evaporators reduce the water content from a product through the use of heat. They are very common to many industries, especially paper, food, textiles, chemical and steel.

An evaporator is a shell and tube heat exchanger where the steam is normally in the shell and the product is in the tubes and in motion. Depending upon the type of product and the desired results, more than one stage or effect of evaporation may be required. The triple effect is the most common, although as many as five or six can be found on some applications.

Single Effect

While the product is being forced through the tubes of the evaporator, heat is added to remove a specific amount of moisture. After this is completed, both the product vapor and the concentrated product are forced into the separating chamber where the vapor is drawn off and may be used elsewhere. The concentrate is then pumped off to another part of the process (Fig. CG-48).

Multiple Effect

In using the multiple effect method, there is a conservation of heat as steam from the boiler is used in the first effect, and then vapor generated from the product is used as the heat source in the second effect. The vapor generated here is then used as the heat source in the third effect and finally heats water for some other process or preheats the incoming feed (Fig. CG-49).

There are many variables in the design of evaporators due to their wide application to many different products. The steam capabilities for evaporators can vary from approximately 1 000 lbs per hour to 100 000 lbs per hour, while steam pressures may vary from a high of 150 psig in the first effect to a low of 24" mercury vacuum in the last effect.

Because evaporators are normally run continuously, there is a uniform load of condensate to be handled. It's important to remember that traps must be selected for the actual pressure differential for each effect.

The three major considerations when trapping evaporators are:

- 1. Large condensate loads.
- 2. Low pressure differentials in some effects.
- 3. The evacuation of air and contaminants.

Safety Factor

- When load is fairly constant and uniform, a 2:1 safety factor should be adequate when applied to an actual condensing load in excess of 50,000 lbs/hr.
- Below 50 000 lbs/hr, use a 3:1 safety factor.

For single and multiple effect evaporators, automatic differential condensate controllers are recommended. In addition to offering continuous operation, DC traps vent air and $\rm CO_2$ at steam temperature, handle flash steam and respond immediately to slugs of condensate.

Figure CG-48. Single Effect Evaporator System

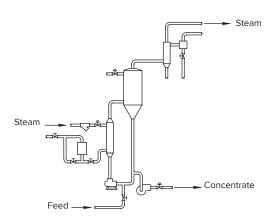


Figure CG-49. Triple Effect Evaporator System

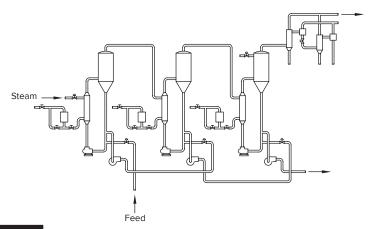


Chart CG-15. Recommendation Chart (See Page CG-4 for "Feature Code" References.)							
Equipment Being Trapped	0-30 psig	Above 30 psig					
Evaporator Single	A, F, G, H, K, M, P	DC	DC				
Effect	Alternate Choices	IBLV F&T	IBLV F&T				
Evaporator	A, F, G, H, K, M, P	DC	DC				
Multiple Effect	Alternate Choices	IBLV F&T	IBLV F&T				



How to Trap Evaporators

Installation

Because an evaporator is basically a shell and tube heat exchanger with the steam in the shell, there should be separate steam air vents on the heat exchanger. Place these vents at any area where there is a tendency for air to accumulate, such as in the quiet zone of the shell. Install a separate trap on each effect. While the condensate from the first effect may be returned to the boiler, condensate from each successive effect may not be returned to the boiler due to contamination from the product.

Trap Selection for Evaporators

When calculating the condensate load for evaporators, take care in selecting the U value (Btu/hr-sq ft-°F). As a general rule, the following U values can be used:

- 300 for natural circulation evaporators with low pressure steam (up to 25 psig)
- 500 on natural circulation with high pressure (up to 45 psig)
- 750 with forced circulation evaporators

Use the following formula to compute heat transfer for constant steam pressure continuous flow heat exchangers.

 $Q = A \times U \times Dm$

Where:

Q = Total heat transferred in Btu per hour

A = Area of outside surface of coil in sq ft

U = Overall rate of heat transfer in Btu/hr-sq ft-°F (See Tables CG-20 and CG-21 on page CG-32)

Dm = Logarithmic mean temperature difference between steam and liquid (as between inlet and outlet of a heat exchanger) in °F

 $Dm = \frac{D1-D2}{Log_{e}\frac{(D1)}{(D2)}}$

Where:

D1 = Greatest temperature difference D2 = Least temperature difference

Logarithmic mean temperature difference can be estimated by using the nomograph, Chart CG-16 (page CG-36).

EXAMPLE:

A = Heat transfer tubes: eight 3/4" OD tubes 12' long

 $\frac{8 \times 12'}{5.09} = 20 \text{ sq ft of coil surface}$

 $U = 500 \text{ Btu/hr-sq ft-}^{\circ}\text{F}$

Conditions:

Water in: 40°F Water out: 150°F

125 psig or 353°F steam pressure:

D1 = 353°F - 40°F, or 313°F D2 = 353°F - 150°F, or 203°F

Dividing by 4 to get within range of Chart CG-16, we have:

D1 = 78.25°F D2 = 50.75°F

Mean difference from chart is 63°F. Multiplying by 4, the mean temperature difference for the original value is 252°F. Substituting in the equation:

Q = 20 x 500 x 252 = 2 520 000 Btu/hr transferred per hour

Latent heat of steam at 125 psig = 867.6

 $\frac{2\ 520\ 000}{867.69}$ = 2 900 lbs condensate per hour

To determine trap capacity required, multiply the condensing rate by the recommended safety factor.

How to Trap Evaporators



Table CG-22. Pipe Coil U Values in Btu/hr-sq ft-°F						
Tyme of Service	Circulation					
Type of Service	Natural	Forced				
Steam to Water	50-200	150-200				
1-1/2" Tube Heaters	180	450				
3/4" Tube Heaters	200	500				
Steam to Oil	10-30	50-150				
Steam to Boiling Liquid	300-800	-				
Steam to Boiling Oil	50-150	-				

able CG-24. Pipe Size Conversion Table. (Divide lineal feet of pipe by factor given for size and type of pipe to get square feet of surface)							
Pipe Size (in)	Iron Pipe	Copper or Brass Pipe					
1/2	4.55	7.63					
3/4	3.64	5.09					
1	2.90	3.82					
1-1/4	2.30	3.05					
1-1/2	2.01	2.55					
2	1.63	1.91					
2-1/2	1.33	1.52					
3	1.09	1.27					
4	.848	.954					

Table CG-23. Embossed Coil U Values in Btu/hr-sq ft-°F						
Time of Service	Circu	Circulation				
Type of Service	Natural	Forced				
Steam to Watery Solutions	100-200	150-275				
Steam to Light Oil	40-45	60-110				
Steam to Medium Oil	20-40	50-100				
Steam to Bunker C	15-30	40-80				
Steam to Tar Asphalt	15-25	18-60				
Steam to Molten Sulphur	25-35	35-45				
Steam to Molten Paraffin	25-35	40-50				
Steam to Molasses or Corn Syrup	20-40	70-90				
Downtherm to Tar Asphalt	15-30	50-60				

Chart CG-17. Pounds of Steam Condensed Per sq ft Per Hour of Submerged Coil Surface

(See "Conditions" conversion factors below chart)

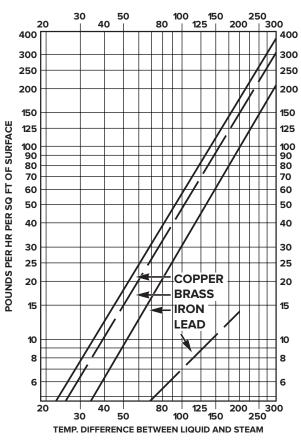
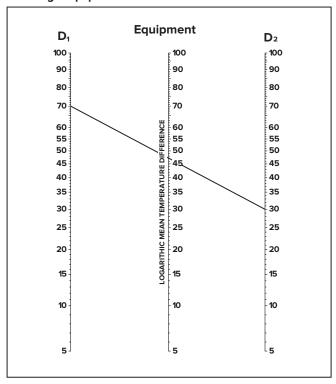


Chart CG-16. Mean Temperature Difference Chart for Heat Exchange Equipment



Condition Factors
(Divide chart figures by proper factor)

CONDITIONS	ACTOR
Will remain bright	_ 1
Moderate scale	_ 2
Liquid contains up to 25% solids	3-5
Thick viscous liquids	4-8

Connect greatest temperature difference on scale D_1 with least temperature difference on scale D_2 to read logarithmic mean temperature difference on center scale.



Armstrong How to Trap Jacketed Kettles

Steam jacketed kettles are essentially steam jacketed cookers or concentrators. They are found in all parts of the world and in almost every kind of application: meat packing, paper and sugar making, rendering, fruit and vegetable processing and food preparation—to name a few.

There are basically two types of steam jacketed kettles—fixed gravity drain and tilting syphon drain. Each type requires a specialized method for trapping steam, although the major problems involved are common to both.

The most significant problem encountered is air trapped within the steam jacket, which adversely affects the temperature. Jacketed kettles usually perform batch operations, and maintaining a uniform or "cooking" temperature is critical. With an excessive amount of air, wide variations in temperature occur and may result in burnt product and/or slow production. To be more specific, under certain conditions as little as 1/2 of 1% by volume of air in steam can form an insulating film on the heat transfer surface and reduce efficiency as much as 50%. See pages CG-9 and CG-10.

A second basic concern in the use of steam jacketed kettles is the need for a steady, thorough removal of condensate. Accumulation of condensate in the jacket leads to unreliable temperature control, reduces the output of the kettle and causes water hammer.

Trap Selection for Jacketed Kettles

Table CG-25 gives the required trap capacities for various size kettles based on the following assumptions: $U = 175 \text{ Btu/hr-sq ft-}^{\circ}\text{F}$

Safety factor of 3 included.

EXAMPLE: What would be the recommended trap capacity for a 34" gravity drained kettle at 40 psig steam? Reading directly from the chart, a trap with a capacity of 1 704 lbs/hr at the operating pressure is required.

For an alternative method of determining condensate, use the following formula:

$$Q = \frac{G \times sg \times Cp \times \Delta T \times 8.3}{H \times t}$$

Where:

Q = Condensate loads (lbs/hr) G = Gallons of liquid to be heated

sg = Specific gravity of the liquid Cp = Specific heat of the liquid

 ΔT = Temperature rise of the liquid °F

8.3 = lbs/gal of water

H = Latent heat of the steam (Btu/lb)t = Time in hours for product heating

EXAMPLE: Select a trap for a 250-gallon kettle using 25 psig steam to heat a product with a specific gravity of 0.98 and a specific heat of 0.95 Btu/lb-°F. Starting at room temperature of 70°F, the product will be heated to 180°F in 1/2 hour. (Assume 3:1 safety factor.) Using the formula:

$$Q = \frac{250 \text{ gal} \times 0.98 \times 0.95 \text{ Btu/lb-}^{\circ}\text{F} \times 110^{\circ}\text{F} \times 8.3 \text{ lbs/gal}}{933 \text{ Btu/lb} \times 0.5 \text{ hr}}$$

 $= \frac{212\ 500}{466.5}$

= 455 lbs/hr

Now simply multiply by a safety factor of 3 to get 1,365 lbs/hr of condensate and select the proper type and capacity trap.

Based on the standard requirements and problems involved with fixed gravity drained kettles, the most efficient type trap to use is the inverted bucket.

The inverted bucket trap vents air and CO_2 at steam temperature and provides total efficiency against back pressure. The primary recommendation for tilting syphon drained kettles is the automatic differential condensate controller. In addition to providing the same features as the IB, the DC offers excellent air venting ability at very low pressure and excellent flash steam handling ability. If an IB trap is selected for syphon drained service, use a trap one size larger.

General Recommendations for Maximum Efficiency

Desirable Cooking Speed. Because the product cooked has such an important bearing on trap selection, a plant with many jacketed kettles should conduct experiments using different sizes of traps to determine the size giving best results.

Steam Supply. Use steam lines of ample size to supply steam to the kettles. Locate the inlet nozzle high up on the jacket for best results. It should be slotted so as to give steam flow around the entire jacket area.

Installation

Install traps close to the kettle. You can further increase the dependability and air-handling capability by installing a thermostatic air vent at high points in the jacket. See Figs. CG-50 and CG-51.

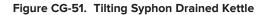
Never drain two or more kettles with a single trap. Group drainage will invariably result in short circuiting.

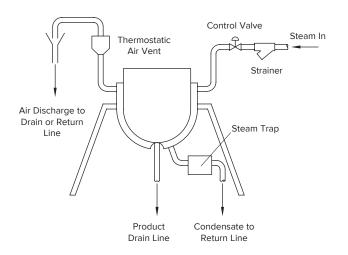
Chart CG-18. Recommendation Chart (See Page CG-4 for "Feature Code" References.)							
Equipment Being Trapped	1st Choice and Feature Code	Alernate Choices					
Jacketed Kettles Gravity Drain	IBLV B, C, E, H, K, N	F&T or Thermostatic					
Jacketed Kettles Syphon Drain	DC B, C, E, G, H, K, N, P	IBLV					

How to Trap Jacketed Kettles



Figure CG-50. Fixed Gravity Drained Kettle





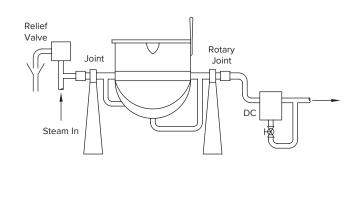


Table CG-25. Condensate Rates in lbs/hr for Jacketed Kettles—Hemispherical Condensing Surface	
Safety factor 3:1 is included. Assume $II = 175 \text{ Rtu/hr-sq ft-}^\circ\text{F} = 50^\circ\text{F}$ starting temperature.	

Kettle		U.S. Gallons	U.S. Gals. Water per	Steam Pressure					S Gals Water per		Steam Pressure	
Diameter (in)	Heat Transfer Surface (sq ft)	of Water in Hemisphere	in. of Height Above Hemisphere	5 psig 227°F	10 psig 240°F	15 psig 250°F	25 psig 267°F	40 psig 287°F	60 psig 307°F	80 psig 324°F	100 psig 338°F	125 psig 353°F
18	3.50	7	1.10	339	366	387	426	474	522	564	603	642
19	3.90	8	1.20	378	408	432	477	528	582	630	669	714
20	4.35	9	1.35	420	456	483	531	588	651	702	747	798
22	5.30	12	1.65	513	555	588	648	717	792	855	912	972
24	6.30	16	1.95	609	660	699	768	852	942	1 017	1083	1 155
26	7.40	20	2.30	717	774	822	903	1 002	1 107	1 194	1 272	1 356
28	8.50	25	2.65	822	891	942	1 038	1 149	1269	1 371	1 461	1 557
30	9.80	31	3.05	948	1026	1 089	1 197	1326	1464	1 581	1686	1797
32	11.20	37	3.50	1 086	1 173	1 242	1 368	1 515	1 674	1 809	1 926	2 052
34	12.60	45	3.95	1 221	1320	1398	1539	1704	1 881	1944	2 166	2 310
36	14.10	53	4.40	1365	1 476	1566	1722	1908	2 106	2 277	2 424	2 586
38	15.70	62	4.90	1 521	1 644	1 743	1 917	2 124	2 346	2 535	2 700	2 877
40	17.40	73	5.45	1 686	1 821	1932	2 124	2 355	2 601	2 808	2 991	3 189
42	19.20	84	6.00	1860	2 010	2 130	2 343	2 598	2 868	3 099	3 300	3 519
44	21.10	97	6.60	2 043	2 208	2 343	2 577	2 856	3 153	3 405	3 627	3 867
46	23.00	110	7.20	2 229	2 409	2 553	2 808	3 111	3 435	3 711	3 954	4 215
48	25.30	123	7.85	2 451	2 649	2 808	3 087	3 423	3 780	4 083	4 350	4 638
54	31.70	178	9.90	3 076	3 324	3 523	3 875	4 296	4 743	5 125	5 458	5 820
60	39.20	245	12.30	3 798	4 104	4 350	4 785	5 304	5 856	6 327	6 738	7 185
72	56.40	423	17.70	5 469	5 910	6 264	6 890	7 638	8 433	9 111	9 703	10 346

How to Trap – Closed, Stationary Steam Chamber Equipment

Closed, stationary steam chamber equipment includes platen presses for the manufacture of plywood and other sheet products, steam jacketed molds for rubber and plastic parts, autoclaves for curing and sterilizing and retorts for cooking.

Product Confined in Steam Jacketed Press

Molded plastic and rubber products such as battery cases, toys, fittings and tires are formed and cured, and plywood is compressed and glue-cured in equipment of this type. Laundry flatwork ironers are a specialized form of press with a steam chamber on one side of the product only.

Trap Selection and Safety Factor

The condensate load for closed, stationary steam chamber equipment is determined by use of the following formula:

 $Q = A \times R \times S$

Where:

Q = Condensate load in lbs/hr

A = Total area of platen in contact with product in sq ft

R = Condensing rate in lbs/sq ft-hr (For purposes of sizing steam traps, a 3 lbs/sq ft-hr condensing rate may be used)

S = Safety factor

EXAMPLE: What is the condensate load for a mid platen on a press with 2' x 3' platens, upper and lower? Using the formula:

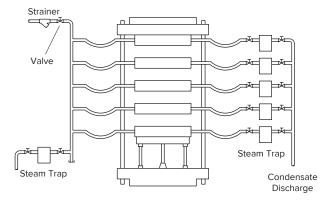
Q = 12 sq ft x 3 lbs/sq ft-hr x 3 = 108 lbs/hr

End platens would have half this load.

The safety factor recommended for all equipment of this type is 3:1.

The inverted bucket trap is the recommended first choice on steam jacketed chambers, dryers and ironers because it can purge the system, resist hydraulic shock and conserve energy. Disc and thermostatic type traps may be acceptable alternatives.

Figure CG-52. Product Confined In Steam Jacketed Press



Installation

Although the condensate load on each platen is small, individual trapping is essential to prevent short circuiting, Fig. CG-52. Individual trapping ensures maximum and uniform temperature for a given steam pressure by efficiently draining the condensate and purging the non-condensables.

Direct Steam Injection Into Product Chamber

This type of equipment combines steam with the product in order to cure, sterilize or cook. Common examples are autoclaves used in the production of rubber and plastic products, sterilizers for surgical dressings and gowns, and retorts for cooking food products already sealed in cans.

Trap Selection and Safety Factor

Calculate the condensate load using the following formula:

$$Q = \frac{W \times C \times \Delta T}{H \times t}$$

Where:

Q = Condensate load in lbs/hr

W = Weight of the material in lbs

C = Specific heat of the material in Btu/lb-°F

(See page CG-57)

 ΔT = Material temperature rise in °F

H = Latent heat of steam in Btu/lb

(See Steam Tables on page CG-5)

t = Time in hours

EXAMPLE: What will be the condensate load on an autoclave containing 300 lbs of rubber product which must be raised to a temperature of 300°F from a starting temperature of 70°F? The autoclave operates at 60 psig steam pressure and the heat-up process takes 20 minutes. Using the formula:

$$Q = \frac{300 \text{ lbs x .42 Btu/lb-°F x 230°F}}{904 \text{ Btu/lb x .33 hr}} = 96 \text{ lbs/hr}$$

Multiply by a recommended safety factor of 3:1 to get the required capacity—288 lbs/hr.



How to Trap – Closed, Stationary Steam Chamber Equipment

Since steam is in contact with the product, you can anticipate dirty condensate. In addition, the vessel is a large volume chamber that requires special consideration in the purging of condensate and non-condensables. For these reasons, an inverted bucket trap with an auxiliary thermostatic air vent installed at the top of the chamber is recommended.

Where no remote thermostatic air vent can be installed, incorporate the large volume air purging capabilities in the steam trap itself. An automatic differential condensate controller should be considered a possible first choice on large chambers. As an alternative, an F&T or thermostatic trap should be used and be preceded by a strainer, the latter receiving regular checks for free flow.

Installation

Because the steam and condensate is in contact with the product, the trap discharge should almost always be disposed of by some means other than return to the boiler. In virtually all cases this equipment is gravity drained to the trap. However, very often there is a condensate lift after the trap. Because steam pressure is usually constant, this does not present a problem. For thorough air removal and quicker warm-up, install a thermostatic air vent at a high point of the vessel. See Fig. CG-53.

Product in Chamber—Steam in Jacket

Autoclaves, retorts and sterilizers are also common examples of this equipment; however, the condensate is not contaminated from actual contact with the product and can be returned directly to the boiler. Steam traps with purging ability and large volume air venting are still necessary for efficient performance.

Trap Selection and Safety Factor

Size steam traps for "product in chamber—steam in jacket equipment" by using the same formula outlined for direct steam injection. The safety factor is also 3:1.

The inverted bucket trap is recommended because it conserves steam, purges the system and resists hydraulic shock.

Use the IB trap in combination with a thermostatic air vent at the top of the chamber for greater air-handling capability. As an alternative, an F&T or thermostatic trap could be used. On large chambers, where it's not possible to install the air vent, an automatic differential condensate controller should be considered a possible first choice.

Installation

With "product in chamber—steam in jacket equipment," the steam and condensate do not come in contact with the product and can be piped to the condensate return system. Where possible, install an auxiliary thermostatic air vent at a remote high point on the steam chamber. See Fig. CG-54.

Chart CG-19. Recommendation Chart (See Page CG-4 for "Feature Code" References.)							
Equipment Being Trapped	1st Choice and Feature Code	Alternate Choices					
Product Confined Steam Jacketed Press	IB A, B, E, K	CD and Thermostatic					
Direct Steam Injection into Product Chamber	*IB A, B, E, H, K, N, Q	**DC					
Product in Chamber—Steam in Jacket	*IB A, B, E, H, K	Thermostatic and F&T and **DC					

^{*}An auxiliary air vent is recommended.

Figure CG-53. Direct Steam Injection Into Product Chamber

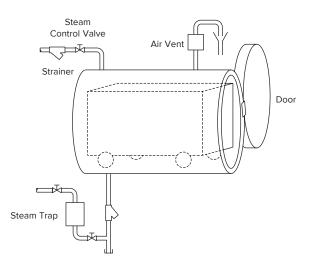
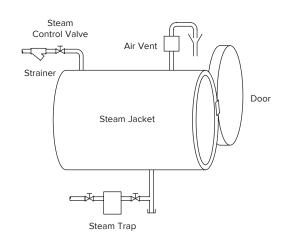


Figure CG-54. Product in Chamber—Steam in Jacket



^{**}First choice on large volume vessels.



How to Trap – Rotating Dryers Requiring Syphon Drainage

There are two classifications of rotating dryers which vary significantly in both function and method of operation. The first dries a product by bringing it into contact with the outside of a steam-filled cylinder. The second holds the product inside a rotating cylinder where steam-filled tubes are used to dry it through direct contact. In some applications a steam jacket surrounding the cylinder is also used.

Safety Factor

The safety factor for both kinds of dryers depends on the type of drainage device selected.

- If an automatic differential condensate controller (DC) is installed, use a safety factor of 3:1 based on the maximum load. This will allow sufficient capacity for handling flash steam, large slugs of condensate, pressure variations and the removal of non-condensables. The DC performs these functions on both constant and modulated pressure.
- If an inverted bucket trap with large vent is used, increase the safety factor in order to compensate for the large volume of non-condensable and flash steam that will be present. Under constant-pressure conditions, use a safety factor of 8:1. On modulated pressure increase it to 10:1.

Rotating Steam Filled Cylinder with Product Outside

These dryers are used extensively in the paper, textile, plastic and food industries, where common examples are dry cans, drum dryers, laundry ironers and paper machine dryers. Their speed of operation varies from 1 or 2 rpm to surface velocities as high as 5 000 rpm. Operating steam pressure ranges from subatmospheric to more than 200 psig. Diameters can vary from 6" or 8" to 14' or more. In all cases syphon drainage is required and flash steam will accompany the condensate.

Trap Selection

Condensate loads can be determined by use of the following formula:

 $Q = 3.14D \times R \times W$

Where:

Q = Condensate load in lbs/hr

D = Diameter of the dryer in ft

R = Rate of condensation in lbs/sq ft-hr

W = Width of dryer in ft

EXAMPLE: Determine the condensate load of a dryer 5 ft in diameter, 10 ft in width and with a condensing rate of 7 lbs/sq ft-hr. Using the formula:

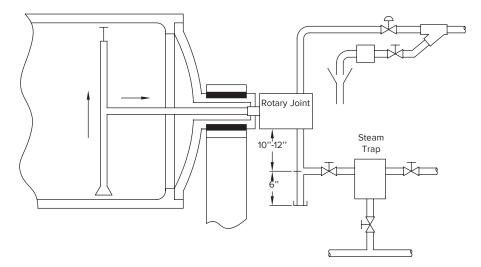
Condensate load = $3.14(5) \times 7 \times 10 = 1100 \text{ lbs/hr}$

Based on its ability to handle flash steam, slugs of condensate and purge the system, a DC is the recommended first choice. An IBLV may be adequate if proper sizing procedures are followed.

Chart CG-20. Recommendation Chart (See Page CG-4 for "Feature Code" References.)						
Equipment Being Trapped	1st Choice and Feature Code	Alternate Choice				
Rotating Dryers	DC A, B, K, M, P, N	IBLV*				

^{*}On constant pressure use 8:1 safety factor, and on modulated pressure use 10:1.

Figure CG-55. Product Outside Dryer



A revolving cylinder drained with a syphon—an internal syphon surrounded by steam. Some condensate flashes back to steam due to the steam jacketed syphon pipe and syphon lifting during evacuation.



Armstrong

How to Trap – Rotating Dryers Requiring Syphon Drainage

Product Inside a Rotating Steam Heated Dryer

This type of dryer finds wide application in meat packing as well as food processing industries. Common examples are grain dryers, rotary cookers and bean conditioners.

Their speed of rotation is relatively slow, usually limited to a few rpm, while steam pressure may range from 0-150 psig. These slower rotating speeds permit the condensate to accumulate in the bottom of the collection chamber in practically all cases. Again, syphon drainage is required and flash steam is generated during condensate removal.

Trap Selection

The condensate load generated by these dryers can be determined through use of the following formula:

$$Q = \frac{N \times L \times R}{P}$$

Where:

Q = Condensate in lbs/hr

N = Number of tubes

L = Length of tubes in ft

R = Condensing rate in lbs/sq ft-hr

(typical 6-9 lbs/sq ft-hr)

P = Lineal ft of pipe per sq ft of surface

(see Table CG-26)

EXAMPLE: What will be the condensate load on a rotary cooker containing 30 1-1/4" steel pipes 12' in length with a condensing rate of 8 lbs/sq ft-hr?
Using the formula:

$$Q = \frac{30 \times 12 \times 8}{2.30} = 1252 \text{ lbs/hr}$$

A differential controller is recommended on these dryers for its purging and flash steam handling ability.

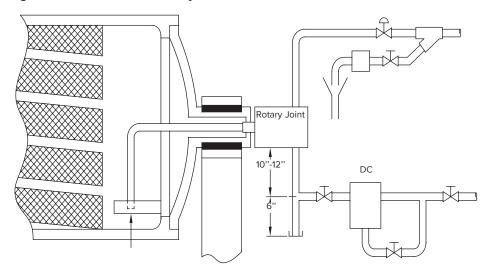
The IBLV again requires proper sizing for certain applications.

Installation

In all cases, condensate drainage is accomplished through a rotary joint, Figs. CG-55 and CG-56. The DC should then be located 10"-12" below the rotary joint with an extended 6" dirt pocket. These provide a reservoir for surges of condensate and also a pocket for entrained scale.

Table CG-26. Pipe Size Conversion Table (Divide lineal feet of pipe by factor given for size and type of pipe to get square feet of surface)							
Pipe Size (in)	Iron Pipe	Copper or Brass Pipe					
1/2	4.55	7.63					
3/4	3.64	5.09					
1	2.90	3.82					
1-1/4	2.30	3.05					
1-1/2	2.01	2.55					
2	1.61	1.91					
2-1/2	1.33	1.52					
3	1.09	1.27					
4	.848	.954					

Figure CG-56. Product Inside Dryer



A revolving cylinder drained with a syphon—an internal syphon surrounded by steam. Some condensate flashes back to steam due to the steam jacketed syphon pipe and syphon lifting during evacuation.



How to Trap Flash Tanks

When hot condensate or boiler water, under pressure, is released to a lower pressure, part of it is re-evaporated, becoming what is known as flash steam. The heat content of flash is identical to that of live steam at the same pressure, although this valuable heat is wasted when allowed to escape through the vent in the receiver. With proper sizing and installation of a flash recovery system, the latent heat content of flash steam may be used for space heating; heating or preheating water, oil and other liquids; and low pressure process heating.

If exhaust steam is available it may be combined with the flash. In other cases, the flash will have to be supplemented by live make-up steam at reduced pressure. The actual amount of flash steam formed varies according to pressure conditions. The greater the difference between initial pressure and pressure on the discharge side, the greater the amount of flash that will be generated.

To determine the exact amount, as a percentage, of flash steam formed under certain conditions, refer to page CG-6 for complete information.

Trap Selection

The condensate load can be calculated using the following formula:

$$Q = L - \frac{L \times P}{100}$$

Where:

Q = Condensate load in lbs/hr (to be handled by steam trap)

L = Condensate flow into flash tank in lbs/hr

P = Percentage of flash

EXAMPLE: Determine the condensate load of a flash tank with 5,000 lbs/hr of 100 psig condensate entering the flash tank held at 10 psig. From page CG-6, the flash percentage is P = 10.5%. Using the formula:

$$Q = 5000 - (5000 \times 10.5) = 4475 \text{ lbs/hr}$$

$$100$$

Due to the importance of energy conservation and operation against back pressure, the trap best suited for flash steam service is the inverted bucket type with large bucket vent. In addition, the IB operates intermittently while venting air and CO_2 at steam temperature.

In some cases, the float and thermostatic type trap is an acceptable alternative. One particular advantage of the F&T is its ability to handle heavy start-up air loads.

Chart CG-21. Recomme (See Page CG-4 for "Fea		
Equipment Being Trapped	Alternate Choice	
Flash Tanks	IBLV B, E, M, L, I, A, F	F&T or *DC

^{*}Recommended where condensate loads exceed the separating capability of the flash tank.

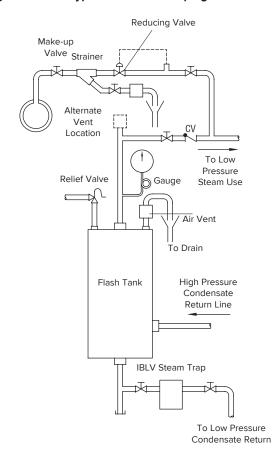
Refer to Chart CG-3 (page CG-6) for percentage of flash steam formed when discharging condensate to reduced pressure.

A third type of device that may be the preferred selection in many cases is the automatic differential condensate controller. It combines the best features of both the IB and F&T and is recommended for large condensate loads that exceed the separating capability of the flash tank.

Safety Factor

The increased amount of condensate at start-up and the varying loads during operation accompanied by low pressure differential dictates a safety factor of 3:1 for trapping flash tanks.

Figure CG-57. Typical Flash Tank Piping Sketch



Flash steam tank with live steam make-up, showing recommended fittings and connections. The check valves in the incoming lines prevent waste of flash when a line is not in use. The by-pass is used when flash steam cannot be used. Relief valves prevent pressure from building up and interfering with the operation of the high pressure steam traps. The reducing valve reduces the high pressure steam to the same pressure as the flash, so they can be combined for process work or heating.

How to Trap Flash Tanks



Installation

Condensate return lines contain both flash steam and condensate. To recover the flash steam, the return header runs to a flash tank, where the condensate is drained, and steam is then piped from the flash tank to points of use, Fig. CG-57. Since a flash tank causes back pressure on the steam traps discharging into the tank, these traps should be selected to ensure their capability to work against back pressure and have sufficient capacity at the available differential pressures.

Condensate lines should be pitched toward the flash tank, and where more than one line feeds into a flash tank, each line should be fitted with a swing check valve. Then, any line not in use will be isolated from the others and will not be fed in reverse with resultant wasted flash steam. If the trap is operating at low pressure, gravity drainage to the condensate receiver should be provided.

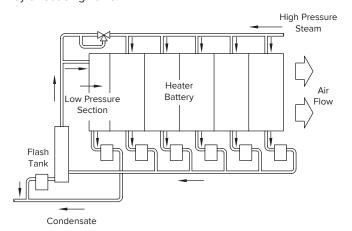
Generally, the location chosen for the flash tank should meet the requirement for maximum quantity of flash steam and minimum length of pipe.

Condensate lines, the flash tank, and the low pressure steam lines should be insulated to prevent waste of flash through radiation. The fitting of a spray nozzle on the inlet pipe inside the tank is not recommended. It may become choked, stop the flow of condensate, and produce a back pressure to the traps.

Low pressure equipment using flash steam should be individually trapped and discharged to a low pressure return. Large volumes of air need to be vented from the flash tank; therefore, a thermostatic air vent should be used to remove the air and keep it from passing through the low pressure system.

Figure CG-58. Flash Steam Recovery from an Air Heater Battery

Flash is taken from the flash tank and combined with live steam, the pressure of which is reduced to that of the flash by a reducing valve.



Flash Tank Dimensions

The flash tank can usually be conveniently constructed from a piece of large diameter piping with the bottom ends welded or bolted in position. The tank should be mounted vertically. A steam outlet is required at the top and a condensate outlet at the bottom. The condensate inlet connection should be 6"-8" above the condensate outlet.

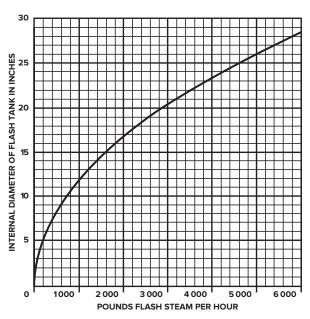
The important dimension is the inside diameter. This should be such that the upward velocity of flash to the outlet is low enough to ensure that the amount of water carried over with the flash is small. If the upward velocity is kept low, the height of the tank is not important, but good practice is to use a height of 2'-3'.

It has been found that a steam velocity of about 10' per second inside the flash tank will give good separation of steam and water. On this basis, proper inside diameters for various quantities of flash steam have been calculated; the results are plotted in Chart CG-22. This curve gives the smallest recommended internal diameters. If it is more convenient, a larger tank may be used.

Chart CG-22 does not take into consideration pressure—only weight. Although volume of steam and upward velocity are less at a higher pressure, because steam is denser, there is an increased tendency for priming. Thus it is recommended that, regardless of pressure, Chart CG-22 be used to find the internal diameter.

Chart CG-22. Determination of Internal Diameter of Flash Tank to Handle a Given Quantity of Flash Steam

Find amount of available flash steam (in pounds per hour) on bottom scale, read up to curve and across to vertical scale, to get diameter in inches.





How to Trap Absorption Machines

An absorption refrigeration machine chills water for air conditioning or process use by evaporating a water solution, usually lithium bromide. Steam provides the energy for the concentration part of the cycle and, except for electric pumps, is the only energy input during the entire cycle.

A steam trap installed on a steam absorption machine should handle large condensate loads and purge air at low pressure, modulated conditions.

Trap Selection and Safety Factor

Determine the condensate load produced by a low pressure (normally 15 psig or less) single-stage steam absorption machine by multiplying its rating in tons of refrigeration by 20, the amount of steam in lbs/hr required to produce a ton of refrigeration. This represents consumption at the rated capacity of the machine.

EXAMPLE: How much condensate will a single-stage steam absorption machine with a rated capacity of 500 tons produce?

Multiply the 500-ton machine capacity rating \times 20 lbs/hr to get the condensate load—10 000 lbs/hr.

A 2:1 safety factor should be applied to the full capacity condensate load, and the steam trap must be capable of draining this load, at a 1/2 psi differential. In other words, the machine in the example would require a trap capable of handling 20 000 lbs/hr of condensate at 1/2 psi, and the capability of functioning at the maximum pressure differential, usually 15 psi.

In comparison, two-stage absorption machines operate at a higher steam pressure of 150 psig. They have an advantage over single-stage units in that their energy consumption per ton of refrigeration is less (12.2 lbs steam/hr/ton of refrigeration at rated capacity).

EXAMPLE: How much condensate will a two-stage steam absorption machine with a rated capacity of 300 tons produce?

Multiply the 300-ton machine capacity rating x 10 lbs/hr to get the condensate load—3 000 lbs/hr.

Chart CG-23. Recommendation Chart (See Page CG-4 for "Feature Code" References.						
Equipment Being Trapped	Alternate Choice					
Steam Aborption Machine	F&T A, B, G	*IB				

NOTE: Vacuum breaker and standby system should be provided.

On two-stage steam absorption machines, a 3:1 safety factor should be used. Therefore, the example requires a steam trap with a capacity of 9 000 lbs/hr. At pressures above 30 psig, the trap capacity must be achieved at 1/2 maximum pressure differential, which in the example is 75 psi. At pressures below 30 psig, trap capacity must be achieved at 2 psi differential pressure. However, the trap must still be capable of operating at a maximum inlet pressure of 150 psig.

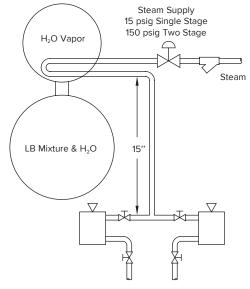
The F&T trap with an integral vacuum breaker is ideally suited for draining both single- and double-stage steam absorption machines. It provides an even, modulated condensate flow and energy-conserving operation. An inverted bucket trap with an external thermostatic air eliminator may also be acceptable.

Installation

Mount the steam trap below the steam coil of the absorption machine with a drip leg height of at least 15" (Fig. CG-59). This ensures a minimum differential pressure across the trap of 1/2 psi. Whichever trap is used, a standby trapping system is recommended for this service. In the event that a component in the drainage system needs maintenance, the absorption machine can operate on the standby system while the repairs are being made. This ensures continuous, uninterrupted service.

In some cases, very heavy condensate loads may require the use of two traps operating in parallel to handle the normal load.

Figure CG-59. Generally approved method of piping steam absorption machine with standby trapping system.



F&T Trap w/Integral Vacuum Breaker Draining to Gravity Return



^{*}With external thermostatic air vent.





This table provides recommendations for traps likely to be most effective in various applications. The recommended safety factors ensure proper operation under varying conditions. For more specific information on recommended traps and safety factors, contact your Armstrong Representative.

Table CG-27.			
Application	1st Choice	2nd Choice	Safety Factor
Boiler Header	IBLV	F&T	1.5:1
(Superheat)	IBCV Burnished	Wafer	Start-Up Load
Steam Mains & Branch Lines			2:1, 3:1 if @ end of main,
(Non-Freezing)	15 (6) (16		ahead of valve, or on
	IB (CV if pressure varies)	F&T	branch
(Freezing) Steam Separator	IB IBLV	Thermostatic or Disc DC	Same as above
Steam quality 90% or less	DC		3:1
Tracer Lines	IB	Thermostatic or Disc	2:1
Unit Heaters and Air Handlers			
(Constant Pressure)	IBLV	F&T	3:1
(0-15 Variable Pressure)			2:1 @ 1/2 psig Differential
(16-30 Variable Pressure)	F&T	IBLV	2:1 @ 2 psig Differential
(>30 Variable Pressure)			3:1 @ 1/2 Max. Pressure Differential
Finned Radiation & Pipe Coils			3:1 for guick heating
(Constant Pressure)	IB	Thermostatic	2:1 normally
(Variable Pressure)	F&T	IB	·
Process Air Heaters			
(Constant Pressure)	IB	F&T	2:1
(Variable Pressure)	F&T	IBLV	3:1 @ 1/2 Max. Pressure Differentia
Steam Absorption Machine (Chiller)	F&T	IB Ext. Air Vent	2:1 @ 1/2 psig Differential
Shell & Tube Heat Exchangers, Pipe & Embossed Coils			
(Constant Pressure)	IB	DC or F&T	2:1
(Variable Pressure)	F&T	DC or IBT (If >30 psig IBLV)	<15 psig 2:1 @ 1/2 psig 16-30 psig 2:1 @ 2 psig >30 psig 3:1 @ 1/2 Max. Pressure Differential
Evaporator Single Effect & Multiple Effect	DC	IBLV or F&T	2:1, If load 50 000 lbs/hr use 3:1
Jacketed Kettles			
(Gravity Drain)	IBLV	F&T or Thermostatic	3:1
(Syphon Drain)	DC	IBLV	
Rotating Dryers	DC	IBLV	3:1 for DC, 8:1 for IB variable pressure, 10:1 for IB variable pressure
Flash Tanks	IBLV	DC or F&T	3:1

IBLV = Inverted Bucket Large Vent
IBCV = Inverted Bucket Internal Check Valve
IBT = Inverted Bucket Thermic Vent
F&T = Float & Thermostatic

DC = Differential Condensate Controller

Use an IB with external air vent above the F&T pressure limitations or if the steam is dirty. All safety factors are at the operating pressure differential unless otherwise noted.



Before Installing

Run pipe to trap. Before installing the trap, clean the line by blowing down with steam or compressed air. (Clean any strainer screens after this blowdown.)

Trap Location ABCs

Accessible for inspection and repair.

Below drip point whenever possible.

Close to drip point.

Trap Hookups. For typical hookups, see Figs. CG-60 (below) through CG-71, pages CG-47 through CG-50.

Shutoff Valves ahead of traps are needed when traps drain steam mains, large water heaters, etc., where system cannot be shut down for trap maintenance. They are not needed for small steam-heated machines—a laundry press, for example. Shutoff valve in steam supply to machine is usually sufficient.

Shutoff Valves in trap discharge line are needed when trap has a by-pass. It is a good idea when there is high pressure in discharge header. See also Check Valves.

Figure CG-60. Typical IB Hookup

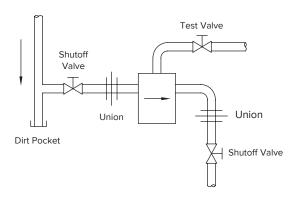
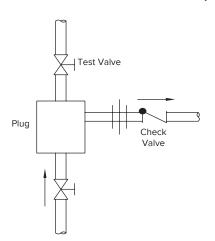


Figure CG-62.

Typical IB Bottom Inlet—Side Outlet Hookup



By-passes (Figs. CG-64 and CG-65) are discouraged, for if left open, they will defeat the function of the trap. If continuous service is absolutely required, use two traps in parallel, one as a primary, one as a standby.

Unions. If only one is used, it should be on discharge side of trap. With two unions, avoid horizontal or vertical in-line installations. The best practice is to install at right angles as in Figs. CG-60 and CG-64, or parallel as in Fig. CG-65.

Standard Connections. Servicing is simplified by keeping lengths of inlet and outlet nipples identical for traps of a given size and type. A spare trap with identical fittings and half unions can be kept in storeroom. In the event a trap needs repair, it is a simple matter to break the two unions, remove the trap, put in the spare and tighten the unions. Repairs can then be made in the shop and the repaired trap, with fittings and half unions, put back in stock.

Test Valves (Fig. CG-60) provide an excellent means of checking trap operation. Use a small plug valve. Provide a check valve or shutoff valve in the discharge line to isolate trap while testing.

Figure CG-61.

Typical IB Bottom Inlet—Top Outlet Hookup

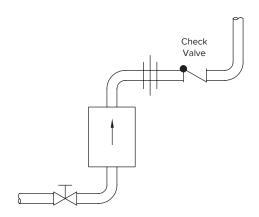
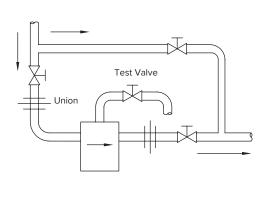


Figure CG-63.
Typical IB By-pass Hookup





Strainers. Install strainers ahead of traps if specified or when dirt conditions warrant their use. Some types of traps are more susceptible to dirt problems than others—see Recommendation Chart on page CG-4.

Some traps have built-in strainers. When a strainer blowdown valve is used, shut off steam supply valve before opening strainer blowdown valve. Condensate in trap body will flash back through strainer screen for thorough cleaning. Open steam valve slowly.

Dirt Pockets are excellent for stopping scale and core sand, and eliminating erosion that can occur in elbows when dirt pockets are not provided. Clean periodically.

Syphon Installations require a water seal and, with the exception of the DC, a check valve in or before the trap. Syphon pipe should be one size smaller than nominal size of trap used but not less than 1/2" pipe size.

Figure CG-64.
Possible Check Valve Locations

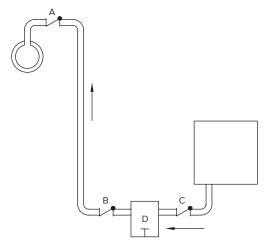
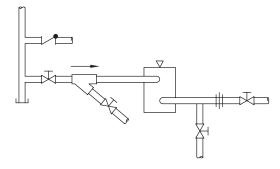


Figure CG-66.
Typical F&T Hookup



Elevating Condensate. Do not oversize the vertical riser. In fact, one pipe size smaller than normal for the job will give excellent results.

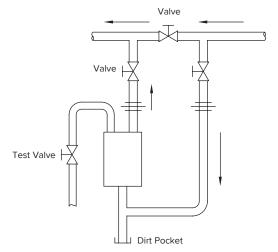
Check Valves are frequently needed. They are a must if no discharge line shutoff valve is used. Fig. CG-63 shows three possible locations for external check valves—Armstrong inverted bucket traps are available with internal check valves, while disc traps act as their own check valve. Recommended locations are given in Fig. CG-63.

Discharge Line Check Valves prevent backflow and isolate trap when test valve is opened. Normally installed at location B, Fig. CG-63. When return line is elevated and trap is exposed to freezing conditions, install check valve at location A.

Inlet Line Check Valves prevent loss of seal if pressure should drop suddenly or if trap is above drip point in IB traps. Armstrong Stainless Steel Check Valve in trap body, location D, Fig. CG-63, is recommended. If swing check is used, install at location C.

Figure CG-65.

Typical IB By-pass Hookup, Bottom Inlet—Top Outlet





Protection Against Heat Exchanger Stall

Stall occurs when the inlet pressure will fall below the outlet pressure of a steam trap. In these situations, a condensate pump should be used to covercome the back pressure. return the condnesate adequately, and avoid stalling the heat exchanger. When a condensate pump is not practical, a Safety Drain Trap should be used whenever there is a likelihood that the inlet pressure will fall below the outlet pressure of a primary steam trap, especially in the presence of freezing air. One such application would be on a modulated pressure heating coil that must be drained with an elevated return line. In the event of insufficient drainage from the primary trap, condensate rises into the safety drain and is discharged before it can enter the heat exchanger. An F&T trap makes a good safety drain because of its ability to handle large amounts of air and its simplicity of operation. Safety drain trap should be same size (capacity) as primary trap.

The proper application of a safety drain is shown in Fig. CG-66. The inlet to the safety drain must be located on the heat exchanger drip leg, above the inlet to the primary trap. It must discharge to an open sewer. The drain plug of the safety drain is piped to the inlet of the primary trap. This prevents the discharge of condensate formed in the safety drain by body radiation when the primary trap is active. The safety drain has an integral vacuum breaker to maintain operation when pressure in the heat exchanger falls below atmospheric. The inlet of the vacuum breaker should be fitted with a gooseneck to prevent dirt from being sucked in when it operates. The vacuum breaker inlet should be provided with a riser equal in elevation to the bottom of the heat exchanger to prevent water leakage when the vacuum breaker is operating, but the drip leg and trap body are flooded.

Protection Against Freezing

A properly selected and installed trap will not freeze as long as steam is coming to the trap. If the steam supply should be shut off, the steam condenses, forming a vacuum in the heat exchanger or tracer line. This prevents free drainage of the condensate from the system before freezing can occur. Therefore, install a vacuum breaker between the equipment being drained and the trap. If there is not gravity drainage through the trap to the return line, the trap and discharge line should be drained manually or automatically by means of a freeze protection drain. Also, when multiple traps are installed in a trap station, insulating the traps can provide freeze protection.

Anti-Freeze Precautions.

- 1. Do not oversize trap.
- 2. Keep trap discharge lines very short.
- 3. Pitch trap discharge lines down for fast gravity discharge.
- 4. Insulate trap discharge lines and condensate return lines.
- 5. Where condensate return lines are exposed to ambient weather conditions, tracer lines should be considered.
- If the return line is overhead, run vertical discharge line adjacent to drain line to top of return header and insulate drain line and trap discharge line together. See Fig. CG-67.

NOTE: A long horizontal discharge line invites trouble. Ice can form at the far end, eventually sealing off the pipe. This prevents the trap from operating. No more steam can enter the trap, and the water in the trap body freezes.

Figure CG-67. Typical Safety Drain Trap Hookup.

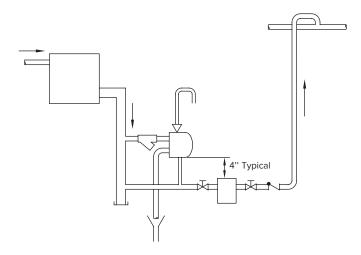


Figure CG-68.

Typical Condensate Pump Hookup.

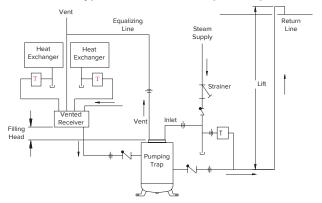
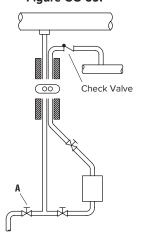


Figure CG-69.



Outdoor installation to permit ground level trap testing and maintenance when steam supply and return lines are high overhead. Drain line and trap discharge line are insulated together to prevent freezing. Note location of check valve in discharge line and blowdown valve **A** that drains the steam main when trap is opened for cleaning or repair.





Testing Armstrong Steam Traps

Testing Schedule.

For maximum trap life and steam economy, a regular schedule should be set up for trap testing and preventive maintenance. Trap size, operating pressure and importance determine how frequently traps should be checked.

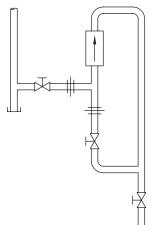
Table CG-28. Suggested Yearly Trap Testing Frequency									
Operating Pressure		Application							
(psig)	Drip	Tracer	Coil	Process					
0-100	1	1	2	3					
101-250	2	2	2	3					
251-450	2	2	3	4					
451 and above	3	3	4	12					

How to Test

The test valve method is best. Fig. CG-60 (page CG-47) shows correct hookup, with shutoff valve in return line to isolate trap from return header. Here is what to look for when test valve is opened:

- 1. Condensate Discharge—Inverted bucket and disc traps should have an intermittent condensate discharge. F&T traps should have a continuous condensate discharge, while thermostatic traps can be either continuous or intermittent, depending on the load. When an IB trap has an extremely small load it will have a continuous condensate discharge which causes a dribbling effect. This mode of operation is normal under this condition.
- 2. Flash Steam—Do not mistake this for a steam leak through the trap valve. Condensate under pressure holds more heat units-Btu-per pound than condensate at atmospheric pressure. When condensate is discharged, these extra heat units re-evaporate some of the condensate. See description of flash steam on page CG-6. How to Identify Flash: Trap users sometimes confuse flash steam with leaking steam. Here's how to tell the difference: If steam blows out continuously, in a "blue" stream, it's leaking steam. If steam "floats" out intermittently (each time the trap discharges) in a whitish cloud, it's flash steam.

Figure CG-69.
Typical DC Hookup



3. Continuous Steam Blow—Trouble. Refer to page CG-51.

4. No Flow—Possible trouble. Refer to page CG-51.

Listening Device Test. Use a listening device or hold one end of a steel rod against the trap cap and the other end against your ear. You should be able to hear the difference between the intermittent discharge of some traps and the continuous discharge of others. This correct operating condition can be distinguished from the higher velocity sound of a trap blowing through. Considerable experience is required for this method of testing, as other noises are telegraphed along the pipe lines.

Pyrometer Method of Testing. This method may not give accurate results, depending on the return line design and the diameter of the trap orifice. Also, when discharging into a common return, another trap may be blowing through, causing a high temperature at the outlet of the trap being tested. Better results can be obtained with a listening device. Request Armstrong Bulletin 310.

Figure CG-70.
Typical Disc Trap Hookup

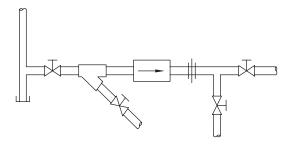
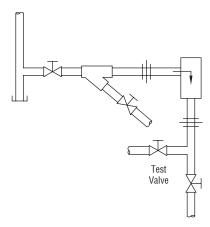


Figure CG-71.

Typical Thermostatic Hookup





Troubleshooting Armstrong Steam Traps

The following summary will prove helpful in locating and correcting nearly all steam trap troubles. Many of these are actually system problems rather than trap troubles.

More detailed troubleshooting literature is available for specific products and applications—consult factory.

Whenever a trap fails to operate and the reason is not readily apparent, the discharge from the trap should be observed. If the trap is installed with a test outlet, this will be a simple matter—otherwise, it will be necessary to break the discharge connection.

Cold Trap-No Discharge

If the trap fails to discharge condensate, then:

- A. Pressure may be too high.
 - 1. Wrong pressure originally specified.
 - 2. Pressure raised without installing smaller orifice.
 - 3. PRV out of order.
 - 4. Pressure gauge in boiler reads low.
 - 5. Orifice enlarged by normal wear.
 - 6. High vacuum in return line increases pressure differential beyond which trap may operate.
- B. No condensate or steam coming to trap.
 - 1. Stopped by plugged strainer ahead of trap.
 - 2. Broken valve in line to trap.
 - 3. Pipe line or elbows plugged.
- **C.** Worn or defective mechanism. Repair or replace as required.
- **D.** Trap body filled with dirt. Install strainer or remove dirt at source.
- E. For IB, bucket vent filled with dirt. Prevent by:
 - 1. Installing strainer.
 - 2. Enlarging vent slightly.
 - 3. Using bucket vent scrubbing wire.
- F. For F&T traps, if air vent is not functioning properly, trap will likely air bind.
- **G.** For thermostatic traps, the bellows element may rupture from hydraulic shock, causing the trap to fail closed.
- **H.** For disc traps, trap may be installed backward.

Hot Trap—No Discharge

- A. No condensate coming to trap.
 - 1. Trap installed above leaky by-pass valve.
 - 2. Broken or damaged syphon pipe in syphon drained cylinder.
 - Vacuum in water heater coils may prevent drainage. Install a vacuum breaker between the heat exchanger and the trap.

Steam Loss

If the trap blows live steam, the trouble may be due to any of the following causes:

- **A.** Valve may fail to seat.
 - 1. Piece of scale lodged in orifice.
 - 2. Worn parts.

- B. IB trap may lose its prime.
 - If the trap is blowing live steam, close the inlet valve for a few minutes. Then gradually open. If the trap catches its prime, chances are the trap is all right.
 - Prime loss is usually due to sudden or frequent drops in steam pressure. On such jobs, the installation of a check valve is called for—location D or C in Fig. CG-63 (page CG-48). If possible, locate trap well below drip point.
- C. For F&T and thermostatic traps, thermostatic elements may fail to close.

Continuous Flow

If an IB or disc trap discharges continuously, or an F&T or thermostatic trap discharges at full capacity, check the following:

- A. Trap too small.
 - A larger trap, or additional traps, should be installed in parallel.
 - High pressure traps may have been used for a low pressure job. Install right size of internal mechanism.
- Abnormal water conditions. Boiler may foam or prime, throwing large quantities of water into steam lines.
 A separator should be installed or else the feed water conditions should be remedied.

Sluggish Heating

When trap operates satisfactorily, but unit fails to heat properly:

- **A.** One or more units may be short-circuiting. The remedy is to install a trap on each unit. See page CG-17.
- **B.** Traps may be too small for job even though they may appear to be handling the condensate efficiently. Try next larger size trap.
- C. Trap may have insufficient air-handling capacity, or the air may not be reaching trap. In either case, use auxiliary air vents.

Mysterious Trouble

If trap operates satisfactorily when discharging to atmosphere, but trouble is encountered when connected with return line, check the following:

- A. Back pressure may reduce capacity of trap.
 - 1. Return line too small—trap hot.
 - 2. Other traps may be blowing steam—trap hot.
 - Atmospheric vent in condensate receiver may be plugged—trap hot or cold.
 - 4. Obstruction in return line—trap hot.
 - 5. Excess vacuum in return line—trap cold.

Imaginary Troubles

If it appears that steam escapes every time trap discharges, remember: Hot condensate forms flash steam when released to lower pressure, but it usually condenses quickly in the return line. See Chart CG-4 on page CG-6.





Pipe Sizing – Steam Supply & Condensate Return Lines

Sizing Charts

Chart CG-25, page CG-53, is the basic chart for determining the flow rate and velocity of steam in Schedule 40 pipe for various values of pressure drop per 100 ft, based on 0 psig saturated steam. Using the multiplier chart (Chart CG-24), Chart CG-25 can be used at all saturation pressures between 0 and 200 psig (see Example).

These Charts are based on the Moody Friction Factor, which considers the Reynolds number and the roughness of the internal pipe surfaces.

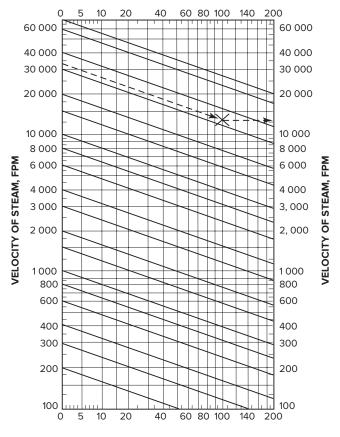
Notes: Based on Moody Friction Factor where flow of condensate does not inhibit the flow of steam. See Chart CG-24 for obtaining flow rates and velocities of all saturation pressures between 0 to 200 psig: see Example.

Pipe Sizing

Two principal factors determine pipe sizing in a steam system:

The initial pressure at the boiler and the allowable pressure drop of the total system. The total pressure drop in the system should not exceed 20% of the total maximum pressure at the boiler. This includes all drops—line loss, elbows, valves, etc. Remember, pressure drops are a loss of energy.

Chart CG-24. Velocity Multiplier Chart for CG-25.



2. Steam velocity. Erosion and noise increase with velocity. Reasonable velocities for process steam are 6 000 to 12 000 fpm, but lower pressure heating systems normally have lower velocities. Another consideration is future expansion. Size your lines for the foreseeable future. If ever in doubt, you will have less trouble with oversized lines than with ones that are marginal.

Use of Basic and Velocity Multiplier Charts

Example.

Given a flow rate of 6 700 lb/hr, an initial steam pressure of 100 psig, and a pressure drop of 11 psi/100 ft, find the size of Schedule 40 pipe required and the velocity of steam in the pipe.

Solution: The following steps are illustrated by the broken line on Chart CG-25 and Chart CG-24.

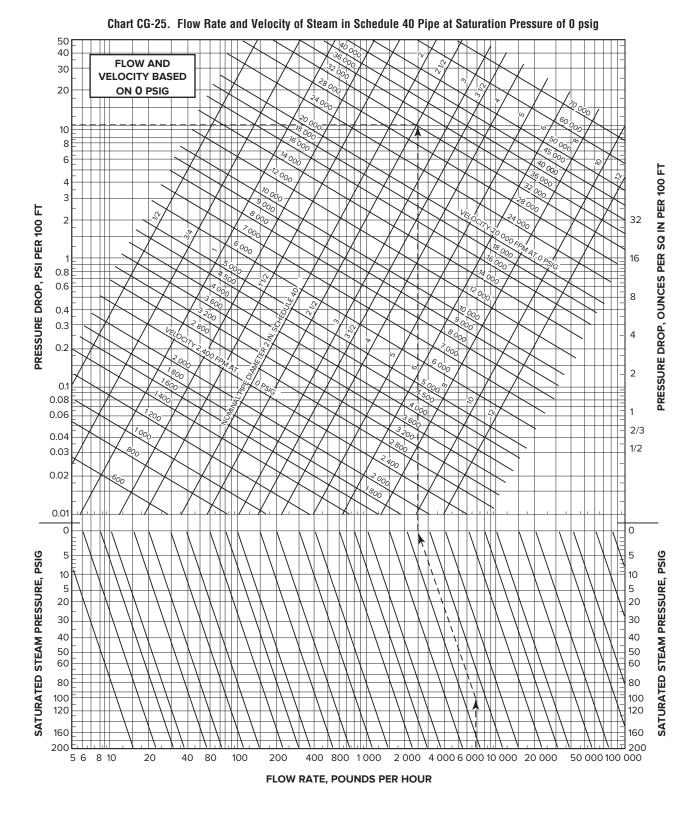
- 1. Enter Chart CG-25 at a flow rate of 6 700 lb/hr, and move vertically to the horizontal line at 100 psig.
- Follow inclined multiplier line (upward and to the left) to horizontal 0 psig line. The equivalent mass flow at 0 psig is about 2 500 lb/hr.
- 3. Follow the 2 500 lb/hr line vertically until it intersects the horizontal line at 11 psi per 100 ft pressure drop. Nominal pipe size is 2-1/2 in. The equivalent steam velocity at 0 psig is about 32 700 fpm.
- 4. To find the steam velocity at 100 psig, locate the value of 32 700 fpm on the ordinate of the velocity multiplier chart (Chart CG-24) at 0 psig.
- Move along the inclined multiplier line (downward and to the right) until it intersects the vertical 100 psig pressure line. The velocity as read from the right (or left) scale is about 13 000 fpm.

NOTE: Steps 1 through 5 would be rearranged or reversed if different data were given.

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SATURATED STEAM PRESSURE, PSIG

Pipe Sizing – Steam Supply & Condensate Return Lines





How to Size Condensate Return Lines

The sizing of condensate return lines presents several problems that differ from those of sizing steam or water lines. The most significant of these is the handling of flash steam. Although a return line must handle both water and flash steam, the volume of flash steam is many times greater than the volume of condensate. For the values in Chart CG-26 the volume of flash steam is 96% to 99% of the total volume. Consequently, only flash steam is considered in Chart CG-26.

Condensate return lines should be sized to have a reasonable velocity at an acceptable pressure drop. Chart CG-26 is based on having a constant velocity of 7 000 feet per minute or below, using Schedule 40 pipe. Additional factors that should also be considered—depending on water conditions—are dirt, fouling, corrosion and erosion.

For a given supply pressure to the trap and a return line pressure, along with an assumed pressure drop per 100 feet of pipe ($\Delta P/L$) and knowing the condensate flow rate, the proper pipe diameter can be selected from Chart CG-26.

How to Use Chart CG-26

Example 1: A condensate system has the steam supply at 30 psig. The return line is non-vented and at 0 psig. The return line is to have the capacity for returning 2 000 lbs/hr of condensate. What must be the size of the return line?

Solution: Since the system will be throttling the condensate from 30 psig to 0 psig, there will be flash steam (assuming no subcooling), and the system will be a dry-closed (not completely full of liquid and not vented to atmosphere) return. The data in Chart CG-26 can be used. A pressure of 1/4 psig per 100 feet is selected. In Chart CG-26 for a 30 psig supply and a 0 psig return for $\Delta P/L = 1/4$, a pipe size for the return line of 2" is selected.

Example 2: A condensate return system has the steam supply at 100 psig and the return line is non-vented and at 0 psig. The return line is horizontal and must have a capacity of 2 500 lbs/hr. What size pipe is required?

Solution: Since the system will be throttling non-subcooled condensate from 100 psig to 0 psig, there will be flash steam, and the system will be a dry-closed return. Selecting a pressure drop of 1 psi per 100 feet yields from Chart CG-26 a non-recommended situation (a). Select a pressure drop of 1/4 psi per 100 feet and then a 2-1/2" pipe can be used for this system.

Chart CG-26. Flow Rate (lbs/hr) for Dry-Closed Returns													
ΔP/L	Supply Pressure = 5 psig			Supply Pressure = 15 psig			Supply F	Supply Pressure = 30 psig			Supply Presssure = 50 psig		
psi/100'	Return Pressure = 0 psig		Return I	Pressure =	0 psig	Return	Return Pressure = 0 psig		Return Pressure = 0 psig				
D, in	1/16	1/4	1	1/16	1/4	1	1/16	1/4	1	1/16	1/4	1	
1/2	240	520	1 100	95	210	450	60	130	274	42	92	200	
3/4	510	1120	2 400	210	450	950	130	280	590	91	200	420	
1	1 000	2 150	a	400	860	а	250	530	1 120	180	380	а	
1-1/4	2 100	4 500	а	840	1800	а	520	1 110	а	370	800	а	
1-1/2	3 170	6 780	а	1 270	2 720	а	780	1670	а	560	1200	а	
2	6 240	13 300	а	2 500	5 320	а	1 540	3 270	а	1 110	2 350	а	
2-1/2	10 000	21 300	а	4 030	8 520	а	2 480	5 250	а	1780	3 780	а	
3	18 000	а	а	7 200	а	а	4 440	9 360	а	3 190	а	а	
4	37 200	а	а	14 900	а	а	9 180	а	а	6 660	а	а	
6	110 500	а	а	44 300	а	а	27 300	а	а	19 600	а	а	
8	228 600	а	а	91 700	а	а	56 400	а	а	40 500	а	а	

Chart CG-26. Flow	Chart CG-26. Flow Rate (lbs/hr) for Dry-Closed Returns											
ΔP/L	Supply Pressure = 100 psig			Supply P	ressure =	150 psig	Supply P	ressure = 1	100 psig	Supply Presssure = 150 psig		
psi/100'	Return P	ressure =	0 psig	Return I	Pressure =	0 psig	Return I	Pressure =	15 psig	Return F	ressure =	15 psig
D, in	1/16	1/4	1	1/16	1/4	1	1/16	1/4	1	1/16	1/4	1
1/2	28	62	133	23	51	109	56	120	260	43	93	200
3/4	62	134	290	50	110	230	120	260	560	93	200	420
1	120	260	a	100	210	а	240	500	а	180	390	800
1-1/4	250	540	а	200	440	а	500	1060	а	380	800	а
1-1/2	380	810	а	310	660	а	750	1600	а	570	1 210	а
2	750	1 590	а	610	1 300	а	1 470	3 100	а	1 120	2 350	а
2-1/2	1200	2 550	а	980	2 100	а	2 370	5 000	а	1800	3 780	а
3	2 160	а	а	1760	3 710	а	4 230	а	а	3 200	6 710	а
4	4 460	а	а	3 640	7 630	а	8 730	a	а	6 620	а	а
6	13 200	а	а	10 800	а	а	25 900	а	а	19 600	а	а
8	27 400	а	а	22 400	а	а	53 400	а	а	40 500	а	а

^a For these sizes and pressure losses the velocity is above 7 000 fpm. Select another combination of size and pressure loss. Reprinted by permission from ASHRAE Handbook - 1985 Fundamentals.



Armstrong Useful Engineering Tables

	Di	Diameters		Circum	ference	Tra	ansverse Are	eas	_	f Pipe Per ft	Length of Pipe Containing		Veight Per oot	Number of
Size (in)	External	Approximate	Thickness (in)	External	Internal	External	Internal	Metal	External Surface	Internal Surface	One Cubic Foot	Plain Ends	Threaded and	Threads Per Inch of Screw
	(in)	Internal (in)		(in)	(in)	(sq in)	(sq in)	(sq in)	Feet	Feet	Feet	Enas	Coupled	Screw
1/8	0.405	0.269	0.068	1.272	0.845	0.129	0.057	0.072	9.431	14.199	2533.775	0.244	0.245	27
1/4	0.540	0.364	0.088	1.696	1.114	0.229	0.104	0.125	7.073	10.493	1383.789	0.424	0.425	18
3/8	0.675	0.493	0.091	2.121	1.549	0.358	0.191	0.167	5.658	7.747	754.360	0.567	0.568	18
1/2	0.840	0.622	0.109	2.639	1.954	0.554	0.304	0.250	4.547	6.141	473.906	0.850	0.852	14
3/4	1.050	0.824	0.113	3.299	2.589	0.866	0.533	0.333	3.637	4.635	270.034	1.130	1.134	14
1	1.315	1.049	0.133	4.131	3.296	1.358	0.864	0.494	2.904	3.641	166.618	1.678	1.684	11-1/2
1-1/4	1.660	1.380	0.140	5.215	4.335	2.164	1.495	0.669	2.301	2.767	96.275	2.272	2.281	11-1/2
1-1/2	1.900	1.610	0.145	5.969	5.058	2.835	2.036	0.799	2.010	2.372	70.733	2.717	2.731	11-1/2
2	2.375	2.067	0.154	7.461	6.494	4.430	3.355	1.075	1.608	1.847	42.913	3.652	3.678	11-1/2
2-1/2	2.875	2.469	0.203	9.032	7.757	6.492	4.788	1.704	1.328	1.547	30.077	5.793	5.819	8
3	3.500	3.068	0.216	10.996	9.638	9.621	7.393	2.228	1.091	1.245	19.479	7.575	7.616	8
3-1/2	4.000	3.548	0.226	12.566	11.146	12.566	9.886	2.680	0.954	1.076	14.565	9.109	9.202	8
4	4.500	4.026	0.237	14.137	12.648	15.904	12.730	3.174	0.848	0.948	11.312	10.790	10.889	8
5	5.563	5.047	0.258	17.477	15.856	24.306	20.006	4.300	0.686	0.756	7.198	14.617	14.810	8
6	6.625	6.065	0.280	20.813	19.054	34.472	28.891	5.581	0.576	0.629	4.984	18.974	19.185	8
8	8.625	7.981	0.322	27.096	25.073	58.426	50.027	8.399	0.442	0.478	2.878	28.554	28.809	8
10	10.750	10.020	0.365	33.772	31.479	90.763	78.855	11.908	0.355	0.381	1.826	40.483	41.132	8
12	12.750	11.938	0.406	40.055	37.699	127.640	111.900	15.740	0.299	0.318	1.288	53.600	_	_
14	14.000	13.125	0.437	43.982	41.217	153.940	135.300	18.640	0.272	0.280	1.069	63.000	_	_
16	16.000	15.000	0.500	50.265	47.123	201.050	176.700	24.350	0.238	0.254	0.817	78.000	_	_
18	18.000	16.874	0.563	56.548	52.998	254.850	224.000	30.850	0.212	0.226	0.643	105.000	-	_
20	20.000	18.814	0.593	62.831	59.093	314.150	278.000	36.150	0.191	0.203	0.519	123.000	_	_
24	24.000	22.626	0.687	75.398	71.063	452.400	402.100	50.300	0.159	0.169	0.358	171.000	_	_

Table CG-30. Equivalent Length of Pipe to Be Added for Fittings–Schedule 40 Pipe							
Pipe	Le	ngth in Fee	et to Be A	dded Ru	n		
Size (in)	Standard Elbow	Side Outlet Tee	Gate Valve*	Globe Valve*	Angle Valve*		
1/2	1.3	3	0.3	14	7		
3/4	1.8	4	0.4	18	10		
1	2.2	5	0.5	23	12		
1-1/4	3.0	6	0.6	29	15		
1-1/2	3.5	7	0.8	34	18		
2	4.3	8	1.0	46	22		
2-1/2	5.0	11	1.1	54	27		
3	6.5	13	1.4	66	34		
3-1/2	8.0	15	1.6	80	40		
4	9.0	18	1.9	92	45		
5	11.0	22	2.2	112	56		
6	13.0	27	2.8	136	67		
8	17.0	35	3.7	180	92		
10	21.0	45	4.6	230	112		
12	27.0	53	5.5	270	132		
*Valve ir	full open	nosition					

Table CG-31. Thermal Expansion of Pipe							
	Elongation	in Inches Pe	er 100 ft From	n -20°F Up			
Temp (°F)	Cast Iron Pipe	Steel Pipe	Wrought Iron Pipe	Copper Pipe			
-20	0.000	0.000	0.000	0.000			
0	0.127	0.145	0.152	0.204			
20	0.255	0.293	0.306	0.442			
40	0.390	0.430	0.465	0.655			
60	0.518	0.593	0.620	0.888			
80	0.649	0.725	0.780	1.100			
100	0.787	0.898	0.939	1.338			
120	0.926	1.055	1.110	1.570			
140	1.051	1.209	1.265	1.794			
160	1.200	1.368	1.427	2.008			
180	1.345	1.528	1.597	2.255			
200	1.495	1.691	1.778	2.500			
240	1.780	2.020	2.110	2.960			
280	2.085	2.350	2.465	3.422			
320	2.395	2.690	2.800	3.900			
360	2.700	3.029	3.175	4.380			
400	3.008	3.375	3.521	4.870			
500	3.847	4.296	4.477	6.110			
600	4.725	5.247	5.455	7.388			

From Piping Handbook, by Walker and Crocker, by special permission. Table CG-31 gives the expansion from -20°F to temperature in question. To obtain the amount of expansion between any two temperatures, take the difference between the figures in the table for those temperatures. For example, if cast iron pipe is installed at a temperature of 80°F and is operated at 240°F, the expansion would be 1.780 - 0.649 = 1.131 in.

*\/alva	in	full	anan	nosition	

valve in full o	pen position										
Table CG-32. Diameters and Areas of Circles and Drill Sizes											
Drill Size	Diameter	Area	Drill Size	Diameter	Area	Drill Size	Diameter	Area	Drill Size	Diameter	Area
3/64	.0469	.00173	27	.1440	.01629	С	.2420	.04600	27/64	.4219	.13920
55	.0520	.00212	26	.1470	.01697	D	.2460	.04753	7/16	.4375	.15033
54	.0550	.00238	25	.1495	.01705	1/4	.2500	.04909	29/64	.4531	.16117
53	.0595	.00278	24	.1520	.01815	E	.2500	.04909	15/32	.4688	.17257
1/16	.0625	.00307	23	.1540	.01863	F	.2570	.05187	31/64	.4844	.18398
52	.0635	.00317	5/32	.1562	.01917	G	.2610	.05350	1/2	.5000	.19635
51	.0670	.00353	22	.1570	.01936	17/64	.2656	.05515	33/64	.5156	.20831
50	.0700	.00385	21	.1590	.01986	H	.2660	.05557	17/32	.5312	.22166
49	.0730	.00419	20	.1610	.02036	I	.2720	.05811	9/16	.5625	.24850
48	.0760	.00454	19	.1660	.02164	J	.2770	.06026	19/32	.5937	.27688
5/64	.0781	.00479	18	.1695	.02256	K	.2810	.06202	5/8	.6250	.30680
47	.0785	.00484	11/64	.1719	.02320	9/32	.2812	.06213	21/32	.6562	.33824
46	.0810	.00515	17	.1730	.02351	L	.2900	.06605	11/16	.6875	.37122
45	.0820	.00528	16	.1770	.02461	M	.2950	.06835	23/32	.7187	.40574
44	.0860	.00581	15	.1800	.02545	19/64	.2969	.06881	3/4	.7500	.44179
43	.0890	.00622	14	.1820	.02602	N	.3020	.07163	25/32	.7812	.47937
42	.0935	.00687	13	.1850	.02688	5/16	.3125	.07670	13/16	.8125	.51849
3/32	.0938	.00690	3/16	.1875	.02761	0	.3160	.07843	27/32	.8437	.55914
41	.0960	.00724	12	.1890	.02806	P	.3230	.08194	7/8	.8750	.60132
40	.0980	.00754	11	.1910	.02865	21/64	.3281	.08449	29/32	.9062	.64504
39	.0995	.00778	10	.1935	.02941	Q	.3320	.08657	15/16	.9375	.69029
38	.1015	.00809	9	.1960	.03017	R	.3390	.09026	31/32	.9687	.73708
37	.1040	.00850	8	.1990	.03110	11/32	.3438	.09281	1	1.0000	.78540
36	.1065	.00891	7	.2010	.03173	S	.3480	.09511	1-1/16	1.0625	.88664
7/64	.1094	.00940	13/64	.2031	.03241	T	.3580	.10066	1-1/8	1.1250	.99402
35	.1100	.00950	6	.2040	.03268	23/64	.3594	.10122	1-3/16	1.1875	1.1075
34	.1110	.00968	5	.2055	.03317	U	.3680	.10636	1-1/4	1.2500	1.2272
33	.1130	.01003	4	.2090	.03431	3/8	.3750	.11045	1-5/16	1.3125	1.3530
32	.1160	.01039	3	.2130	.03563	V	.3770	.11163	1-3/8	1.3750	1.4849
31	.1200	.01131	7/32	.2188	.03758	w	.3860	.11702	1-7/16	1.4375	1.6230
1/8	.1250	.01227	2	.2210	.03836	25/64	.3906	.11946	1-1/2	1.5000	1.7671
30	.1285	.01242	1	.2280	.04083	X	.3970	.12379	1-5/8	1.6250	2.0739
29	.1360	.01453	Α	.2340	.04301	Y	.4040	.12819	1-3/4	1.7500	2.4053
28	.1405	.01550	15/64	.2344	.04314	13/32	.4062	.12962	1-7/8	1.8750	2.7612
9/64	.1406	.01553	В	.2380	.04449	Z	.4130	.13396	2	2.0000	3.1416

Conversion Factors



Power				
Multiply	Ву	To Get		
Boiler hp	33 472	Btu/hr		
Boiler hp	34.5	lbs H₂O evap. at 212°F		
Horsepower	2 540	Btu/hr		
Horsepower	550	ft-lbs/sec		
Horsepower	33 000	ft-lbs/min		
Horsepower	42.42	Btu/min		
Horsepower	0.7457	Kilowatts		
Kilowatts	3 415	Btu/hr		
Kilowatts	56.92	Btu/min		
Watts	44.26	ft-lbs/min		
Watts	0.7378	ft-lbs/sec		
Watts	0.05692	Btu/min		
Tons refrig.	12 000	Btu/hr		
Tons refrig.	200	Btu/min		
Btu/hr	0.00002986	Boiler hp		
lbs H₂O evap. at 212°F	0.0290	Boiler hp		
Btu/hr	0.000393	Horsepower		
ft-lbs/sec	0.00182	Horsepower		
ft-lbs/min	0.0000303	Horsepower		
Btu/min	0.0236	Horsepower		
Kilowatts	1.341	Horsepower		
Btu/hr	0.000293	Kilowatts		
Btu/min	0.01757	Kilowatts		
ft-lbs/min	0.02259	Watts		
ft-lbs/sec	1.355	Watts		
Btu/min	1.757	Watts		
Btu/hr	0.0000833	Tons Refrig.		
Btu/min	0.005	Tons Refrig.		

Energy				
Multiply	Ву	To Get		
Btu	778	ft-lbs		
Btu	0.000393	hp-hrs		
Btu	0.000293	kw-hrs		
		{lbs H₂O		
		evap.)		
Btu	0.0010307	at 212°F		
Btu	0.293	Watt-hrs		
ft-lbs	0.3765	Watt-hrs		
latent heat} of ice	143.33	Btu/lb H₂O		
lbs H₂O evap.} at 212°F	0.284	kw-hrs		
lbs H₂O evap.} at 212°F	0.381	hp-hrs		
ft-lbs	0.001287	Btu		
hp-hrs	2 540	Btu		
kw-hrs	3 415	Btu		
lbs H₂O evap.} at 212°F	970.4	Btu		
Watt-hrs	3.415	Btu		
Watt-hrs	2 656	ft-lbs		
Btu/lb H₂O	0.006977	{Latent heat of ice		
kw-hrs	3.52	{lbs H₂O evap. at 212°F		
hp-hrs	2.63	{lbs H₂O evap. at 212°F		

	Pressure	
Multiply	Ву	To Get
		{in Mercury
atmospheres	29.92	(at 62°F)
		{in H₂O
atmospheres	406.8	(at 62°F)
		{ft. H₂O
atmospheres	33.90	(at 62°F)
atmospheres	14.70	lbs/in²
atmospheres	1.058	ton/ft²
in. H₂O}		{in. Mercury
(at 62°F)	0.0737	(at 62°F)
ft H₂O}		{in. Mercury
(at 62°F)	0.881	(at 62°F)
ft H ₂ O}		
(at 62°F)	0.4335	lbs/in²
ft H ₂ O}		
(at 62°F)	62.37	lbs/ft²
in. Mercury}		
(at 62°F)	70.73	lbs/ft²
in. Mercury}		
(at 62°F)	0.4912	lbs/in ²
in. Mercury}	0.00040	
(at 62°F)	0.03342	atmosphere
in. H₂O}	0.000450	
(at 62°F)	0.002458	atmosphere
ft. H₂O} (at 62°F)	0.0295	atmaanhara
lbs/in ²	0.0295	atmosphere:
ton/ft²	0.0000	atmosphere
in. Mercury}	0.945	{in. H ₂ O
(at 62°F)	13.57	(at 62°F)
in. Mercury}	15.57	(at 02 1) {ft H ₂ O
(at 62°F)	1.131	(at 62°F)
(ft H₂O	1.151	(dt 02 1)
lbs/in²	2.309	(at 62°F)
{ft H₃O)	2.505	(dt 02 1)
lbs/ft ²	0.01603	(at 62°F)
{in. Mercury	0.01000	(41 02 1)
lbs/ft²	0.014138	(at 62°F)
{in Mercury		(== 02 .)
lbs/in²	2.042	(at 62°F)
lbs/in²	0.0689	Barg
lbs/in²	0.0703	kg/cm²

Velocity of Flow					
Multiply By To Get					
ft/min	0.01139	miles/hr			
ft/min	0.01667	ft/sec			
cu ft/min	0.1247	gal/sec			
cu ft/sec	448.8	gal/min			
miles/hr	88	ft/min			
ft/sec	60	ft/min			
gal/sec	8.02	cu ft/min			
gal/min	0.002228	cu ft/sec			

Temperature	
°F = (°C x 1.8) + 32	
°C = (°F - 32) ÷ 1.8	

Weight					
Multiply	Ву	To Get			
lbs	7 000	grains			
lbs H₂O					
(60°F)	0.01602	cu ft H₂O			
lbs H₂O					
(60°F)	0.1198	gal H₂O			
tons (long)	2 240	lbs			
tons (short)	2 000	lbs			
grains	0.000143	lbs			
lbs H₂O					
cu ft H₂O	62.37	(60°F)			
lbs H₂O					
gal H₂O	8.3453	(60°F)			
lbs	0.000446	tons (long)			
lbs	0.000500	tons (short)			

Circular Measure				
Multiply	Ву	To Get		
Degrees	0.01745	Radians		
Minutes	0.00029	Radians		
Diameter	3.142	Circumference		
Radians	57.3	Degrees		
Radians	3 438	Minutes		
Circumference	0.3183	Diameter		

Volume					
Multiply	Ву	To Get			
Barrels (oil)	42	gal (oil)			
cu ft	1728	cu in			
cu ft	7.48	gal			
cu in	0.00433	gal			
gal (oil)	0.0238	barrels (oil)			
cu in	0.000579	cu ft			
gal	0.1337	cu ft			
gal	231	cu in			

Heat Transmission					
Multiply By To Get					
Btu/in}		{Btu/ft			
/sq ft	0.0833	/sq ft			
/hr/°F		/hr/°F			
Btu/ft}		{Btu/in			
/sq ft	12	/sq ft			
/hr/°F		/hr/°F			

Fractions and Decimals					
Multiply	Ву	To Get			
Sixty-fourths	0.015625	Decimal			
Thirty-seconds	0.03125	Decimal			
Sixteenths	0.0625	Decimal			
Eighths	0.125	Decimal			
Fourths	0.250	Decimal			
Halves	0.500	Decimal			
Decimal	64	Sixty-fourths			
Decimal	32	Thirty- seconds			
Decimal	16	Sixteenths			
Decimal	8	Eighths			
Decimal	4	Fourths			
Decimal	2	Halves			

Gallons shown are U.S. standard.



Armstrong[®] Specific Heat—Specific Gravity

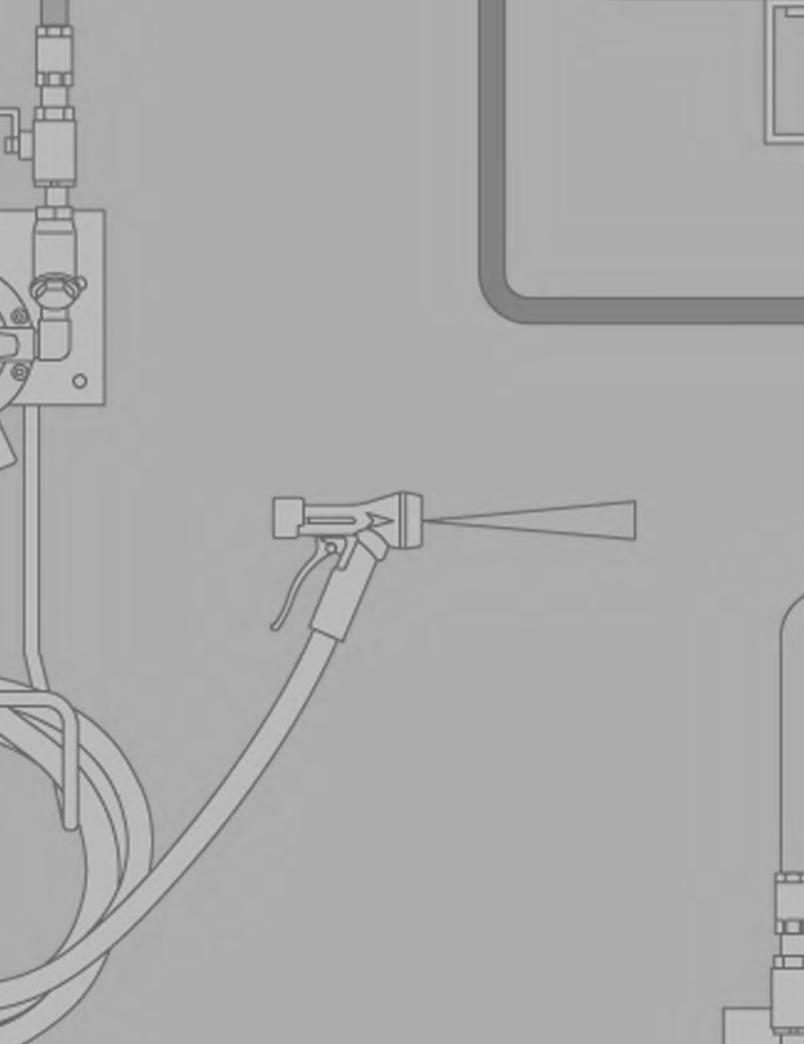
Liquid (L) or Solid (S)	Table CG-33. Physical Propertie	s of Liquids	and Solids	
Acetic acid 100%	,			
Solid (S) 60-70°F Btu/lb-°F				
Acetic acid 10%			60-70°F	
Acetone, 100%	Acetic acid 100%	L	1.05	0.48
Alcohol, ethyl, 95%	Acetic acid 10%	L	1.01	0.96
Alcohol, methyl, 90%	Acetone, 100%	L	0.78	0.514
Aluminum	Alcohol, ethyl, 95%	L	0.81	0.60
Ammonia, 100%	Alcohol, methyl, 90%	L	0.82	0.65
Ammonia, 26%	Aluminum	S	2.64	0.23
Aroclor L 1.44 0.28 Aspbalt L 1.00 0.42 Asphalt, solid S 1.1-1.5 0.22-0.4 Benzene L 0.84 0.41 Brickwork & Masonry S 1.6-2.0 0.22 Brine - calcium chloride, 25% L 1.19 0.786 Clay, dry S 1.9-2.4 0.224 Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.20 0.35@40 Coke, solid S 1.0-1.4 0.265 Coke, solid S 1.0-1.4 0.265 Cotk, solid S 1.50 0.35@40 Cotkon, cloth S 1.50 0.32 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cotton, cloth S 1.50 0.32 Cotton, cloth L 0.99 0.63 Dowtherm A L 0.99 0.63	Ammonia, 100%	L	0.61	1.10
Asbestos board Asphalt Asphalt, solid Benzene L Brickwork & Masonry Brine - calcium chloride, 25% Brine - sodium chloride, 25% Clay, dry Coal Coal Coal Coke, solid S Cotton, cloth Cotton, cloth Dowtherm A Dowtherm A Dowtherm C Ethylene glycol Fish, fresh, average Gasoline Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Pyrex Glass, Ryrex Glass	Ammonia, 26%	L	0.90	1.00
Asphalt, solid L 1.00 0.42 Asphalt, solid S 1.1-1.5 0.22-0.4 Benzene L 0.84 0.41 Brickwork & Masonry S 1.6-2.0 0.22 Brine - calcium chloride, 25% L 1.19 0.786 Clay, dry S 1.9-2.4 0.224 Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.20 0.35@40 Coke, solid S 1.0-1.4 0.265 Coke, solid S 1.50 0.35 Cotk, solid S 1.50 0.35 Cotk, solid S 1.50 0.32 Cotkon, cloth S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cotton, cloth S 1.50 0.32 <td>Aroclor</td> <td>L</td> <td>1.44</td> <td>0.28</td>	Aroclor	L	1.44	0.28
Asphalt, solid S 1.1-1.5 0.22-0.4 Benzene L 0.84 0.41 Brickwork & Masonry S 1.6-2.0 0.22 Brine - calcium chloride, 25% L 1.23 0.689 Brine - sodium chloride, 25% L 1.19 0.786 Clay, dry S 1.9-2.4 0.224 Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.2-1.8 0.26-0.37 Coke, solid S 1.0-1.4 0.265 Copper S 8.82 0.10 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cotton, cloth S 1.50 0.32 Cotton, cloth S 1.50 0.32 Cotton, cloth L 0.99 0.63 Dowtherm A L 0.99 0.63 Dowtherm A L 0.95 0.47 Dottine Stack L 1.11 0.5	Asbestos board	S	0.88	0.19
Benzene	Asphalt	L	1.00	0.42
Brickwork & Masonry S 1.6-2.0 0.22 Brine - calcium chloride, 25% L 1.23 0.689 Brine - sodium chloride, 25% L 1.19 0.786 Clay, dry S 1.9-2.4 0.224 Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.20 0.35@40 Coke, solid S 1.0-1 0.265 Coke, solid S 1.0-1 0.265 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cotton, cloth S 0.25 0.48 Cottonsed oil L 0.99 0.63 Cottonsea L 1.10 0.	Asphalt, solid	S	1.1-1.5	0.22-0.4
Brine - calcium chloride, 25% L 1.23 0.689 Brine - sodium chloride, 25% L 1.19 0.786 Clay, dry S 1.9-2.4 0.224 Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.2-1.8 0.26-0.37 Coke, solid S 1.0-1.4 0.265 Copper S 8.82 0.10 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.95 0.47 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.75-0.82 0.75-0.82 Fruit, fresh, average S 0.75-0.82 0.75-0.82 Glass, Pyrex S 2.25 0.20 0.75-0.82 Glass, P	Benzene	L	0.84	0.41
Brine - sodium chloride, 25% L	Brickwork & Masonry	S	1.6-2.0	0.22
Clay, dry	Brine - calcium chloride, 25%	L	1.23	0.689
Coal S 1.2-1.8 0.26-0.37 Coal tars S 1.20 0.35@40 Coke, solid S 1.0-1.4 0.265 Copper S 8.82 0.10 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.99 0.63 Dowtherm A L 0.99 0.63 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.85 0.653 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.653 0.53 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.073 0.53 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 1.09 <td< td=""><td>Brine - sodium chloride, 25%</td><td>L</td><td>1.19</td><td>0.786</td></td<>	Brine - sodium chloride, 25%	L	1.19	0.786
Coal tars	Clay, dry	1	1.9-2.4	
Coke, solid S 1.0-1.4 0.265 Copper S 8.82 0.10 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.99 0.63 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.84 0.550 Fatty acid - stearic L 0.84 0.550 Fatty acid - stearic L 0.84 0.550 Fruit, fresh, average S 0.84 0.550 Gasoline L 0.73 0.53 Gassoline L 0.73 0.53 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 1.09 0.89 Honey L 1.26 0.58 Honey L 1.15 0.60 <tr< td=""><td>Coal</td><td></td><td>1.2-1.8</td><td>0.26-0.37</td></tr<>	Coal		1.2-1.8	0.26-0.37
Copper S 8.82 0.10 Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.99 0.63 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.85 0.653 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.75-0.82 0.75-0.82 Fruit, fresh, average S 0.73 0.53 Gasoline L 0.73 0.53 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Hydrochloric acid, 31.5% (muriatic) L		1	1.20	-
Cork S 0.25 0.48 Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.95 0.47 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.84 0.550 Fatty acid - stearic L 0.84 0.550 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.80-0.88 0.80-0.88 Gasoline L 0.73 0.53 Gass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Lee S 0.99 0.50	Coke, solid	1	1.0-1.4	0.265
Cotton, cloth S 1.50 0.32 Cottonseed oil L 0.995 0.47 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.85 0.653 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.80-0.88 0.80-0.88 Gasoline L 0.73 0.53 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice Cream S 0.92 0.64 <td< td=""><td>Copper</td><td>S</td><td>8.82</td><td>0.10</td></td<>	Copper	S	8.82	0.10
Cottonseed oil L 0.95 0.47 Dowtherm A L 0.99 0.63 Dowtherm C L 1.10 0.35-0.65 Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.84 0.550 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.80-0.88 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice Cream S 0.90 0.50 Lead S 0.90 0.50 <td< td=""><td>Cork</td><td>S</td><td>0.25</td><td>0.48</td></td<>	Cork	S	0.25	0.48
Dowtherm A	Cotton, cloth	S	1.50	0.32
Dowtherm C	Cottonseed oil	L	0.95	0.47
Ethylene glycol L 1.11 0.58 Fatty acid - palmitic L 0.85 0.653 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.75-0.82 Fruit, fresh, average S 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice Cream S 0.90 0.50 Lead S 11.34 0.031 Lead S 11.34 0.031 Lead L 0.93 0		L	0.99	0.63
Fatty acid - palmitic L 0.85 0.653 Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice Cream S 0.90 0.50 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Mall L 1.03 0.90-0.93 Nickel S 8.90<	Dowtherm C	L	1.10	0.35-0.65
Fatty acid - stearic L 0.84 0.550 Fish, fresh, average S 0.75-0.82 Fruit, fresh, average S 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 1.09 0.89 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice S 0.90 0.50 Ice S 0.90 0.50 Ice S 0.92 0.64 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Meat, fresh	, ,	L		0.58
Fish, fresh, average S 0.75-0.82 Fruit, fresh, average S 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice S 0.90 0.50 Ice S 0.90 0.50 Ice S 0.90 0.50 Ice S 0.92 0.64 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Me	Fatty acid - palmitic	L	0.85	0.653
Fruit, fresh, average S 0.80-0.88 Gasoline L 0.73 0.53 Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 0.34 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 0.75 Ice S 0.90 0.50 0.75 0.75 0.75 0.70 0.70 0.70 0.70 0.70 0.70 0.70 0.64 0.20 0.64 0.20 0.64 0.20 0.64 0.20 0.20 0.64 0.20 0.20 0.20 0.20 0.20 0.27 0.44 0.208 0.27 0.44 0.48 0.20 0.27 0.48 0.29 0.44 0.48 0.29 0.44 0.20 0.20 0.27 0.20			0.84	1
Gasoline	•	1		0.75-0.82
Glass, Pyrex S 2.25 0.20 Glass, wool S 0.072 0.157 Glue, 2 parts water 1 part dry glue L 1.09 0.89 Glycerol, 100% (glycerin) L 1.26 0.58 Honey L 1.15 0.60 Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice S 0.90 0.50 Ice Cream S 0.90 0.50 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37				0.80-0.88
Glass, wool S 0.072 0.157		1		1
Glue, 2 parts water 1 part dry glue L 1.09 0.89				
1 part dry glue	•	S	0.072	0.157
Glycerol, 100% (glycerin)		L	1.09	0.89
Honey			4.00	0.50
Hydrochloric acid, 31.5% (muriatic) L 1.15 0.60 1.05 0.75 0.75 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.70 0.50 0.50 0.70 0.50 0.50 0.50 0.70 0.50		1	1.26	
Hydrochloric acid, 10% (muriatic) L 1.05 0.75 Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice Ice	,	1	445	
Ice S 0.90 0.50 Ice Cream S 0.70 0.70 Lard S 0.92 0.64 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 0.48 Meat, fresh, average S 0.780 0.11 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
Ice Cream S 0.70 Lard S 0.92 0.64 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 Meat, fresh, average S 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 60% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41	1 -	1		
Lard S 0.92 0.64 Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 0.48 Meat, fresh, average S 0.780 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1	0.90	
Lead S 11.34 0.031 Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 Meat, fresh, average S 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1	0.03	
Leather S 0.86-1.02 0.36 Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 0.48 Meat, fresh, average S 0.780 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		1
Linseed oil L 0.93 0.44 Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 0.48 Meat, fresh, average S 0.780 0.90-0.93 Nilk L 1.03 0.90-0.93 Nikric acid, 95% L 1.50 0.50 Nitric acid, 95% L 1.37 0.64 Nitric acid, 60% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1	i	i
Magnesia, 85% L 0.208 0.27 Maple syrup L 0.48 Meat, fresh, average S 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
Maple syrup L 0.48 Meat, fresh, average S 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
Meat, fresh, average S 0.780 Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1	0.208	
Milk L 1.03 0.90-0.93 Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
Nickel S 8.90 0.11 Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41			102	
Nitric acid, 95% L 1.50 0.50 Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41			i .	
Nitric acid, 60% L 1.37 0.64 Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41			i .	
Nitric acid, 10% L 1.05 0.90 No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41	· ·	1	i .	
No. 1 Fuel Oil (kerosene) L 0.81 0.47 No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
No. 2 Fuel Oil L 0.86 0.44 No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41	•			
No. 3 Fuel Oil L 0.88 0.43 No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41				
No. 4 Fuel Oil L 0.90 0.42 No. 5 Fuel Oil L 0.93 0.41		1		
No. 5 Fuel Oil L 0.93 0.41				
	No. 6 Fuel Oil	Ĺ	0.95	0.40

Table CG-33. (cont.) Physical Pro	perties of L	iquids and	Solids
	Liquid (L) or Solid (S)	sp gr @ 60-70°F	sp ht @ 60°F Btu/lb-°F
API Mid-continent crude	L	.085	0.44
API gas oil	L	0.88	0.42
Paper	S	1.7-1.15	0.45
Paraffin	S	0.86-0.91	0.62
Paraffin, melted	L	0.90	0.69
Phenol (carbolic acid)	L	1.07	0.56
Phosphoric acid, 20%	L	1.11	0.85
Phosphoric acid, 10%	L	1.05	0.93
Phthalic anhydride	L	1.53	0.232
Rubber, vulcanized	S	1.10	0.415
SAE - SW (#8 machine lube oil)	L	0.88	
SAE - 20 (#20 machine lube oil)	L	0.89	
SAE - 30 (#30 machine lube oil)	L	0.89	
Sand	S	1.4-1.76	0.19
Sea water	L	1.03	0.94
Silk	S	1.25-1.35	0.33
Sodium hydroxide, 50% (caustic acid)	L	1.53	0.78
Sodium hydroxide, 30%	L	1.33	0.84
Soybean oil	L	0.92	0.24-0.33
Steel, mild @ 70	S	7.90	0.11
Steel, stainless, 300 series	s	8.04	0.12
Sucrose, 60% sugar syrup	Ĺ	1.29	0.74
Sucrose, 40% sugar syrup	L	1.18	0.66
Sugar, cane & beet	s	1.66	0.30
Sulfur	S	2.00	0.203
Sulfuric acid, 110% (fuming)	Ĺ		0.27
Sulfuric acid, 98%	L	1.84	0.35
Sulfuric acid, 60%	L	1.50	0.52
Sulfuric acid. 20%	L	1.14	0.84
Titanium (commercial)	s	4.50	0.13
Toluene	Ĺ	0.86	0.42
Trichloroethylene	Ī	1.62	0.215
Tetrachloride carbon	Ĺ	1.58	0.21
Turpentine, spirits of	Ī	0.86	0.42
Vegetables, fresh, average	S	0.00	0.73-0.94
Water	Ĺ	1.00	1.00
Wines, table, dessert, average	Ē	1.03	0.90
Woods, vary from	S	0.35-0.9	0.90
Wool	S	1.32	0.325
Zinc	S	7.05	0.095

	sp gr @ 60-70°F	spht@60°FBtu/lb-°F
Air	1.00	0.24
Ammonia	0.60	0.54
Benzene		0.325
Butane	2.00	0.455
Carbon dioxide	1.50	0.21
Carbon monoxide	0.97	0.255
Chlorine	2.50	0.118
Ethane	1.10	0.50
Ethylene	0.97	0.45
Freon - 12		0.16
Hydrogen	0.069	3.42
Hydrogen sulfide	1.20	0.25
Methane	0.55	0.60
Nitrogen	0.97	0.253
Oxygen	1.10	0.225
Propane	1.50	0.46
Sulfur dioxide		0.162
Water vapor (steam)	2.30	0.453







Steam Trapping and Steam Tracing Equipment

Armstrono





Steam Traps

Pay less money for energy and more attention to the environment.

It's pretty obvious, really. An efficient steam trap wastes less energy, which means you burn less fuel and reduce emissions. The results are energy savings and a cleaner, healthier environment. By helping companies manage energy, Armstrong steam traps are also helping protect the world we all share.

As a steam trap wears, it loses efficiency and begins to waste energy. But Armstrong inverted bucket traps last years longer than other traps. They operate more efficiently longer because the inverted bucket is the most reliable steam trap operating principle known.

Clearly, the longer an efficient trap lasts, the more it reduces energy wasted, fuel burned and pollutants released into the air. It's an all-around positive situation that lets the environment win, too. Bringing energy down to earth in your facility could begin with a renewed focus on your steam system, especially your steam traps. Said another way: Zeroing in on your steam traps is an easy way to pay less money for energy—and more attention to the environment.

Companies around the world are beginning to realize that rather than being separate challenges, energy and the environment are and have always been a single mission. And that quality management in one area will surely impact the other



Armstrong Steam Trap ID Charts

		Flow	Connection	Max. Allow.				Max. Oper.			Coi	nection	ı Size			Located
Illustration	Туре	Direction	Туре	Press. psig	TMA °F	Body Material	Model	Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	2-1/2"	on Page
	Series 200 Inverted Bucket	^				ASTM A48	211 212 213	250 250 250	•	•						
	Capacities to 20 000 lb/hr		Screwed	250	450	Class 30 Cast Iron	213 214 215 216	250 250 250 250	•	•	•	•	•	•		74
	Series 800 Inverted Bucket					ASTM A48	800 811 812	150 250 250	•	•	•					76
	Capacities to 20 000 lb/hr		Screwed	250	450	Class 30 Cast Iron	813 814 815 816	250 250 250 250		•	•	•	•	•	•	78
	Series 880 Inverted Bucket Capacities to 4 400 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	880 881 882 883	150 250 250 250	•	•	•	•				80
	Series 980 Inverted Bucket		Screwed Socketweld	600	650	ASTM A216 WCB	981	600	•	•						82
	Capacities to 4 400 lb/hr		Flanged †			Carbon Steel	983	600		•	•					

[†] Operating pressure and temperature may be limited depending on the class of flange selected.

Armstrong Steam Trap ID Charts



Illustration Se	Туре	Flow Direction						O	l			nectio				Located
Se		Direction	Connection Type	Allow. Press. psig	TMA °F	Body Material	Model	Oper. Press. psig	3/8"	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	on Page
Ca	Series EM nverted Bucket Capacities to 058 lb/hr		Screwed Socketweld Flanged †	464	482	Forged Carbon Steel	ЕМ	464		•	•					84
In	Series 300 Inverted Bucket Capacities to	1	Screwed Socketweld Flanged †	** 700 600 1 080 1 130 965 1 050	** 700	ASTM A105 Forged Steel	310 312 313 314 315 316	400 600 650 650 650		•	•	•	•	•	•	86
Inv	Series 411G Inverted Bucket Capacities to 300 lb/hr	↑	Screwed Socketweld Flanged †	** 1000	** 700	ASTM A105 Forged Steel	411G	1000		•	•					88
In	Series 521 Inverted Bucket Capacities to 300 lb/hr	→	Screwed NPT & BSPT Socketweld, Flanged †	1 000	700	ASTM A105 Forged Steel	521	1 000		•	•					90
Inv	Series 400 nverted Bucket Capacities to 20 000 lb/hr	↑	Screwed Socketweld Flanged †	** 1050 1080 1350	** 850	ASTM A182 F22 Forged Steel	413 415 416	1 000 1 000 1 000		•	•	•	•	•	•	92
Inv	Series 401-SH Inverted Bucket Capacities to 170 lb/hr		Screwed Socketweld Flanged †	1 000	800	Carbon Steel ASTM A106 Gr. B	401-SH	1 000		•	•					94
Inv	Series 501-SH Inverted Bucket Capacities to 050 lb/hr	†	Screwed Socketweld Flanged †	1 540	850	316L Stainless Steel ASTM A312	501-SH	1540		•	•					94
Ca	Series 5000 Inverted Bucket Capacities to 5 150 lb/hr		Socketweld Flanged †	** 1730 ** 2 070	** 900	ASTM A182 F22 Forged Steel	5133G 5155G	1 500		•	•	•	•			96
See Inv	Series 6000 nverted Bucket Capacities to 5 500 lb/hr	↑	Socketweld Flanged †	** 3 090	* * 900	ASTM A182 F22 Forged Steel	6155G	2 700					•	•		98
Inv	Series 1000 Inverted Bucket Capacities to	1	Screwed Socketweld	400 400 650 450	800 800 800	304L Stainless Steel	1010 1011 1022 1013	150 400 650 450		•	•	•				102
Ca	Series 1800 Inverted Bucket Capacities to 802 lb/hr		Screwed Socketweld	400 650	800	304L Stainless Steel	1810 1811 1822	200 400 650	•	•	•	•				104

 $[\]star\star$ See tables on pages 86, 89 and 91 for complete temperature/pressure rating information.

 $[\]dagger$ Operating pressure and temperature may be limited depending on the class of flange selected.



Armstrong Steam Trap ID Charts

		Flow	Connection	Max. Allow.	тма	Dadu		Max.							1
Illustration	Туре	Direction	Туре	Press. psig	°F	Body Material	Model	Oper. Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	- Located on Page
	Series 2000 Inverted Bucket	*	Screwed	400	800	304L	2010 2011	200 400	•	•	•				106
	Capacities to 1 300 lb/hr	\	Socketweld	650	600	Stainless Steel	2022	650	•	•	•				
	Series 4000 Inverted Bucket		Screwed NPT	400	800	ASTM-A 240	4010 4011	200 400	•	•	•				
	Capacities to 1 300 lb/hr	\	Socketweld Flanged	650	600	Grade 304L	4022	650	•	•	•				108
	1811N and 2011N Inverted Bucket non-metallic seat Capacities to 900 lb/hr	*	Screwed Socketweld	400	800	304L Stainless Steel	1811N 2011N	200 200	•	•	•				110
	Series 20-DC Automatic Differential Condensate Controllers Capacities to 20 000 lb/hr	1	Screwed	250	450	ASTM A48 Class 30 Cast Iron	21-DC 22-DC 23-DC 24-DC 25-DC 26-DC	250 250 250 250 250 250 250	•	•	•	•	•	•	112
	Series 80-DC Automatic Differential Condensate Controllers Capacities to 20 000 lb/hr	*	Screwed	250	450	ASTM A48 Class 30 Cast Iron	81-DC 82-DC 83-DC 84-DC 85-DC 86-DC	250 250 250 250 250 250 250		•	•	•		•	114
	Series TVS 80-DC Automatic Differential Condensate Controllers Capacities to 4 400 lb/hr	*	Screwed	250	450	ASTM A48 Class 30 Cast Iron	TVS 81-DC TVS 82-DC TVS 83-DC	250 250 250	•	•	•				116
	Series 30-DC Automatic Differential Condensate Controllers Capacities to 20 000 lb/hr		Screwed	1 080 1 130 1 015 1 100	700	ASTM A105 Forged Steel	33-DC 34-DC 35-DC 36-DC	650 650 650 650			•	•	•	•	118
	Series B & BI F&T Capacities to 8 900 lb/hr		Screwed	125 175	353 377	ASTM A48 Class 30 Cast Iron	B2, B12 B3, B13 B4, B14 B5 B6 B8	30 30 30 30 30 30	••	•4	• 🛦	•	•	•	122
	Series A & AI F&T Capacities to 8 900 lb/hr		Screwed	175	377	ASTM A48 Class 30 Cast Iron	AI2 A3, AI3 A4, AI4 A5 A6 A8	175 175 175 175 175 175	• • •	••	•	•	•	•	124

 $[\]blacktriangle \textsc{Series}$ Al and BI for in-line connection.

[†] Operating pressure and temperature may be limited depending on the class of flange selected.

Steam Trap ID Charts



	Пар			Max.				Connection Size									
Illustration	Туре	Flow Direction	Connection Type	Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	2-1/2"	3"	Located on Page
	Series AIC F&T Capacities to 60 000 lb/hr	*	Screwed Flanged	580	572	ASTM A395 Ductile Iron	AICV AICFH	465					•	•			126
	Series JD & KD F&T Capacities to 142 000 lb/hr		Screwed Flanged	300	650	ASTM A395 Ductile Iron	15-JD 20-JD 30-JD 75-JD 125-JD 175-JD 250-JD 300-JD 30-KD 50-KD	15 20 30 75 125 175 250 300 30 50 300						•	•	•	128
	Series L & M F&T Capacities to 208 000 lb/hr		Screwed Flanged † (screw on)	250	450	ASTM A48 Class 30 Cast Iron	L8 L10 M12	250 250 250						•	•	•	130
	Series FT-4000 F&T Capacities to 1 080 lb/hr	*	Screwed Socketweld	485	600	ASTM A240 Grade 304L	FT-4075 FT-4150 FT-4225 FT-4300 FT-4465	75 150 225 300 465	•	•	•						132
	Series FF-4000 F&T Capacities to 1 050 lb/hr	*	Screwed Socketweld	600	800	ASTM A240 Grade 304L	FF-4250 FF-4450	250 450	•	•							134
	Series ICS F&T Capacities to 60 000 lb/hr		Screwed Socketweld Flanged †	580	572	Carbon Steel	ICS	465	•	•	•	•	•	•			136
	Series LS & MS F&T Capacities to 280 000 lb/hr		Screwed Socketweld Flanged †	450	650	ASTM A216 WCB Carbon Steel	LS8 LS10 MS-12	450 450 450						•	•	•	138
	TVS 800 Trap Valve Station Capacities to 4 400 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	TVS 811 TVS 812 TVS-813	250 250 250	•	•	•						142
	TVS 4000 Trap Valve Station	*	Screwed Socketweld	650	600	ASTM A351 Gr. CF8M	TVS 4000	650	•	•							146
	TVS 4000F Trap Valve Station	*	Flanged †	650	600	ASTM A351 Gr. CF8M	TVS 4000F	650		•	•						148
	TVS 5000 Trap Valve Station	*	Screwed Socketweld Flanged †	650	600	ASTM A350 LF2	TVS 5000	650	•	•							152

[†] Operating pressure and temperature may be limited depending on the class of flange selected.



Armstrong[®] Steam Trap ID Charts

				Max.				Max.			Co	nnecti	on Si	ze			Located
Illustration	Туре	Flow Direction	Connection Type	Allow. Press. psig	°F	Body Material	Model	Oper. Press. psig	1/4"	3/8"	1/2"	3/4"	1"	2"	2-1/2"	3"	on Page
	TVS 1100 Trap Valve Station	← →	Screwed Socketweld Flanged †	580	662	ASTM A105 Carbon Steel	TVS 1100	319			•	•					150
	Series CD-33 Disc Capacities to 2 428 lb/hr	←→				ASTM	CD-33L			•	•	•	•				158
	Series CD-33S Disc w/Integral Strainer Capacities to		Screwed	915	752	A743 Gr. CA40	CD-33S	600			•	•	•				156
	2 428 lb/hr Series CD-3300 Disc Capacities to	^	Screwed Socketweld	720	750	Stainless Steel	CD-3300	450			•	•	•				159
	800 lb/hr Series CD-40 Controlled Disc Capacities to 2 850 lb/hr	*	Screwed	600	500	Carbon Steel	CD-41 CD-42 CD-43	600 600 600		•	•	•	•				160
	Series CD-60 Controlled Disc Capacities to 2 850 lb/hr	*	Screwed Socketweld	600	750	Forged Carbon Steel	CD-61 CD-62 CD-63	600 600		•	•	•	•				160
	Series CD-72SR Controlled Disc Capacities to 3 900 lb/hr	***	Screwed NPT BSPT Socketweld Flanged †	1 010	750	ASTM A105N/ A350 LF2 Cl.1	CD-72S/ SL	600			•	•	•				162
	Series CD-82S Controlled Disc Capacities to 750 lb/hr	$\bigg \bigoplus_{\begin{subarray}{c} \begin{subarray}{c}	Screwed NPT BSPT Socketweld, Buttweld	1 500	650	ASTM A182 F11 Cl.2	CD-80S	100			•	•					163
	Series WMT Thermostatic Wafer Cold Water Start-Up Capacities to 1 000 lb/hr	,	Flanged † Screwed	250	400	F22 Cl.3 304L Stainless Steel	WMT-1	250	•	•	•						
	Series WT Thermostatic Wafer	←	Screwed	400	650	304L Stainless Steel	WT-1	400			•	•					
	Cold Water Start-Up Capacities to	*	Screwed Socketweld	600 400	750 650	C1018 Carbon Steel	WT-3	600 400			•	•	•				167
	1 600 lb/hr Model SH Thermostatic Wafer	↓ .	Screwed NPT BSPT Socketweld Flanged [†]	580	662	Stainless Steel ASTM A105	SH-300	319			•	•	•				
		*	Screwed NPT BSPT Socketweld Buttweld Flanged †	900	900	Stainless Steel	SH-900	L=650* H=900*			•	•	•				169
	Cold Water Start-Up Capacities to 1 600 lb/hr	↓	Flanged † Socketweld Buttweld Flanged †	1800	1 050	ASTM 217 Cer. C12A	SH-1500	1 800				•	•				

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Steam Trap ID Charts



	_	Flow	Connection	Max. Allow.	TMA	Body		Max. Oper.	Соі	Located		
Illustration	Туре	Direction	Туре	Press. psig	°F	Material	Model	Press. psig	1/2"	3/4"	1"	on Page
	Model SH-2000 Cold Water Start-Up Capacities to 4 800 lb/hr	$\qquad \qquad ewed Socketweld	400	800	Stainless Steel	SH-2000	400	•	•	•	171	
	Model SH-2500 Cold Water Start-Up Capacities to 6 000 lb/hr	*	Screwed Socketweld	650	600	ASTM A351 Gr. CF8M	SH-2500	650	•	•	•	172
	Model AB-3000 Bimetallic Capacities to 4 000 lb/hr	*	Screwed Socketweld Flanged †	319	650	ASTM - A240 304L	AB-3000	319	•	•	•	173
	Model SH-4000 Cold Water Start-Up Capacities to 6 000 lb/hr	*	Screwed Socketweld	1 245	900	Stainless Steel	SH-4000	1 245		•	•	174
HOL	Model TC-300 Cold Water Start-Up Capacities to 1 000 lb/hr	←→	Screwed Socketweld Flanged †	465	662	ASTM A15 Carbon Steel	TC-300	250	•	•	•	166
	Series TT Thermostatic Bellows	*					TTF-1		•	•		
			Screwed	300	450	304L Stainless Steel	TTF-1R	300	•	•		175
	Capacities to 3 450 lb/hr	*	Screwed Socketweld				TT-2000		•	•	•	
	TAVB Thermostatic Bellows w/Integral Vacuum Breaker	^	Straight-Thru Screwed	300	365	304L Stainless Steel	TAVB-2 TAVB-3	150	•	•		177
	Series TS-2/TS-3 Radiator	\downarrow	Threaded	50	300	Durana	TS-2	50	•	•		470
	Capacities to 1 600 lb/hr	\	Inreaded	65	315	Bronze	TS-3	65	•	•	•	178
	Series TC Thermostatic Clean Steam Clamped Capacities to 3 450 lb/hr		Sanitary	120	350	Stainless Steel	тс-с	100	•	•	•	
	Series TC Thermostatic Clean Steam		Sanitary						•	•	•	
	Sealed Capacities to		Threaded	150	366	Stainless Steel	TC-S	120	•	•		179
	3 775 lb/hr Series TC	•	Tube End						•	•		
	Thermostatic Clean Steam Repairable		Sanitary						•	•	•	
		\downarrow	Threaded	120	356	Stainless Steel	TC-R	100	•	•		
	Capacities to 3 775 lb/hr	*	Tube End						•	•		

 $[\]ensuremath{\dagger}$ Operating pressure and temperature may be limited depending on the class of flange selected.



The Inverted Bucket Steam Trap

Energy Efficient Because It's So Reliable

The inverted bucket is the most reliable steam trap operating principle known. The heart of its simple design is a unique leverage system that multiplies the force provided by the bucket to open the valve against pressure. Since the bucket is open at the bottom, it resists damage from water hammer, and wear points are heavily reinforced for long life.

The inverted bucket has only two moving parts—the valve lever assembly and the bucket. That means no fixed points, no complicated linkages. Nothing to stick, bind or clog.

closes tightly. No buildup of dirt or close

clearances to be affected by scale.

Wear and corrosion Virtually no steam loss resistance Free-floating guided lever valve Steam does not reach the watermechanism is "frictionless," and all sealed discharge valve. wear points are heavily reinforced. All working parts are stainless steel. Valve and seat are stainless steel, individually ground and lapped together in matched **Purging action** Snap opening of the valve creates a momentary pressure drop and turbulence in the unit drained. This breaks up films of condensate and air and Continuous air speeds their flow to the trap. and CO₂ venting Vent in top of bucket provides continuous automatic air and CO₂ venting with no cooling lag or threat of air binding. Steam passing through vent is less than that required to compensate for radiation losses from the trap so it's not wasted. Dependable operation Simple, direct operation with nothing to stick, bind or clog. Only two moving parts—the valve lever and the bucket. **Excellent operation** against back pressure Freedom from dirt problems Since trap operation is governed by Condensate flow under the bottom edge the difference in density of steam of the bucket keeps sediment and sludge and water, back pressure in the in suspension until it is discharged with the return line has no effect on the ability condensate. Valve orifice opens wide and

Resistance to damage from water hammer

Open bucket or float will not collapse as a result of water hammer.

of the trap to open for condensate

and close against steam.

Inverted Bucket Steam Trap



Conserves Energy Even in the Presence of Wear

Armstrong inverted bucket steam traps open and close based on the difference in density between condensate and steam—the inverted bucket principle. They open and close gently, minimizing wear. This simple fact means that inverted buckets are subject to less wear than some other types of traps.

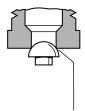
In fact, as an Armstrong inverted bucket trap wears, its tight seal actually improves. The ball valve and seat of the Armstrong trap provide essentially line contact—resulting in a tight seal because the entire closing force is concentrated on one narrow seating ring.

An Armstrong inverted bucket trap continues to operate efficiently with use. Gradual wear slightly increases the diameter of the seat and alters the shape and diameter of the ball valve. But, as this occurs, a tight seal is still preserved—the ball merely seats itself deeper.

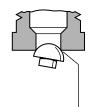
Corrosion-Resistant Parts

The stainless steel valve and seat of the Armstrong inverted bucket steam trap are individually ground and lapped together in matched sets. All other working parts are wear- and corrosion-resistant stainless steel.

Armstrong IB Valve Seating/Ball Valve



Line Contact— Single Seat



Infinite Number of Center Lines and Seating Circumferences

Venting of Air and CO₂

The Armstrong inverted bucket provides continuous automatic air and CO₂ venting with no cooling lag or threat of air binding.

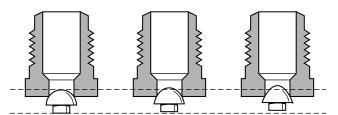
Operation Against Back Pressure

The Armstrong inverted bucket has excellent performance against back pressure. It has no adverse effect on inverted bucket operation other than to reduce its capacity by the low differential. The bucket simply requires less force to pull the valve open and cycle the trap.

Freedom From Dirt Problems

Armstrong designed its inverted bucket to be virtually free of dirt problems. The valve and seat are at the top of the trap, far away from the larger particles of dirt, which fall to the bottom. Here the up-and-down action of the bucket pulverizes them. Since the valve of an inverted bucket is either fully closed or open, dirt particles pass freely. And the swift flow of condensate from under the bucket's edge creates a unique self-scrubbing action that sweeps dirt out of the trap.

IB Valve Wear Characteristics



Armstrong IB ball valve continues to seat itself deeper, providing a tight seal even in the presence of wear.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Armstrong How to Use the IB Trap Summary Capacity Chart

This catalog should be utilized as a guide for the installation and operation of steam trapping equipment by experienced personnel. Selection or installation should always be accompanied by competent technical assistance or advice. Armstrong and its local representatives are available for consultation and technical assistance. We encourage you to contact your Armstrong Representative for complete details.

The summary capacity chart plots actual trap capacity vs. inlet pressure on a log-log grid. The trap capacities become **straight lines** on this grid. The **small numbers** along the pressure axis identify the subdivisions; for example, between the large 10 and 100, the numbers 2, 3, 5, and 7 represent 20, 30, 50 and 70 psig.

The summary chart combines many trap families into one chart by presenting only a portion of the capacity line for each orifice size. For charts that give capacity over a wide range of pressures, see the specific trap model pages.

Individual capacity charts for various traps are given throughout this catalog. Those charts show capacity lines for each orifice, with pressures usually from 1 psig up to the maximum rated pressure of that orifice.

To select an inverted bucket steam trap using the summary capacity chart, you must know the condensate load, safety factor, inlet pressure and outlet pressure. Remember, the object is to select a trap that can 1) operate at the maximum inlet pressure, and 2) handle the capacity at the minimum differential pressure. Consider the following typical problems.

Example 1. Constant pressure, condensing rate. Given:

Maximum inlet pressure
Normal operating differential pressure 60 psig
Required capacity = 300 lb/hr condensate load
times 3:1 safety factor, or900 lb/hr

Enter the chart at the 60 psig line and go up to 900 lb/hr capacity. This is directly on the 5/32" orifice line for models 211, 811 and 881 (and other traps). Now follow this line to the right, to the vertical drop at 70 psig. This means the orifice will work, in these traps, up to a maximum differential of 70 psig. Assuming a cast iron trap is suitable, the 5/32" orifice in a Model 211, 811 or 881 trap will meet all the operating requirements.

Example 2. Constant condensing rate but with possible reduced inlet pressure.

	۰
Given:	

Maximum inlet pressure
Minimum inlet pressure40 psig
Required capacity = 400 lb/hr condensate load
times 3:1 safety factor, or

Consider the maximum operating pressure first. Enter the chart at the 100 psig line and find the first capacity line above 1 200 lb/hr. This is the 5/32" orifice in a Model 212, 812 or 882, and it has a capacity of 1 800 lb/hr at 100 psig. Now extend this straight line to the left until it intersects the 40 psig pressure line. At 40 psig, read a capacity of 1 300 lb/hr. (You could also refer to the individual capacity charts for Models 212, 812 or 882.) Assuming cast iron is suitable,

this is the desired trap selection to meet the requirements of opening at the maximum pressure, and also having the needed capacity at the minimum pressure.

This example points out how the capacity is influenced by the trap size. Example 1 also used the same orifice size, but in a physically smaller trap. In the larger trap the same diameter orifice not only has a higher capacity, it will work at higher pressures.

Example 3. Constant condensing rate but high back pressure.

Given:

0.1.0.11
Inlet pressure100 psig
Normal outlet (back) pressure 50 psig
Required capacity = 1800 lb/hr condensate load
times 3:1 safety factor, or 5 400 lb/hr

Traditional method:

Since the differential pressure is only 50 psig, enter the chart at 50 psig and go up to a capacity of 5 400 lb/hr. This is just under the capacity lines for Models 214 and 814. However, the 5/16" orifice is the largest orifice that will operate at 100 psig inlet pressure. (Remember that the back pressure may not always be there!) Extend the capacity line for the 5/16" orifice to the left, and read a capacity of 4 800 lb/hr at 50 psig. Since this is too low, go up to the 215/815 capacity lines and repeat the process. The selection will end up being a Model 215 or 815 with a 3/8" orifice*

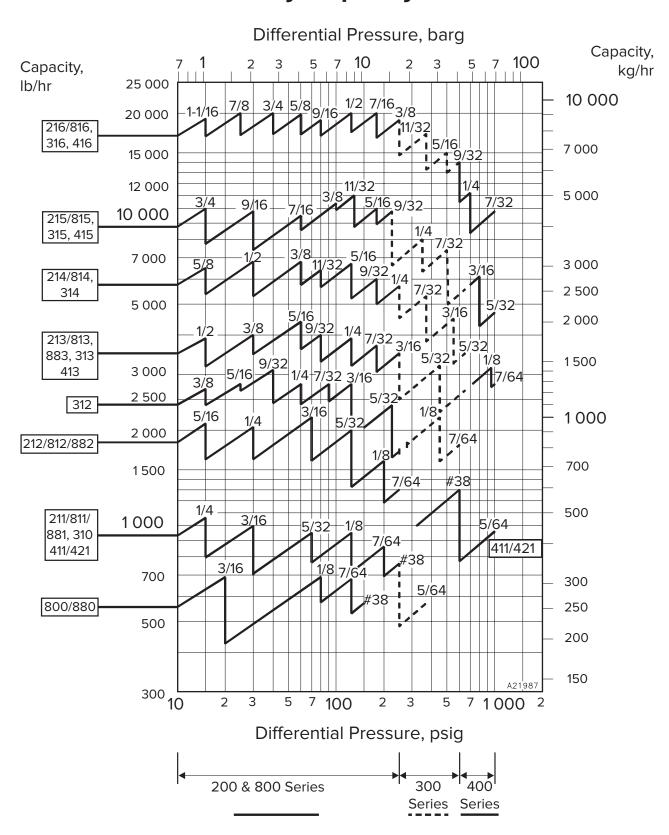
About this chart ...

The Armstrong capacity chart shows continuous discharge capacities of Armstrong traps under actual operating conditions, as determined by many hundreds of tests made over the years. In these tests, **hot condensate** was used, at or near the steam temperature corresponding to the test pressure. The choking effect of flash steam in the orifice and the back pressure created by this flash steam were therefore automatically taken into account. The test setups were similar to an actual installation hookup, so that pipe friction in both inlet and discharge lines was reflected in the results.

* This method is conservative. While it will always select a workable trap, it may select a larger trap than necessary. Consult Armstrong Application Engineering for further information about the effects of back pressure.



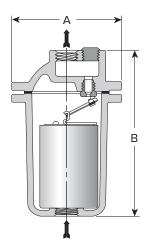
Summary Capacity Chart





Cast Iron for Vertical Installation

For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)



Description

The most reliable steam trap known—the inverted bucket—provides efficient condensate drainage of virtually all types of steam-using equipment. Put the inverted bucket to work in a tough cast iron package, and you have the best of both worlds. Because they operate efficiently for longer periods of time, Armstrong cast iron inverted buckets add solid energy savings to lower replacement/labor costs.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and ${\rm CO}_2$ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, allowing no condensate backup. They are also resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

250 psig @ 450°F (17 barg @ 232°C) Model 211-216: 250 psig (17 barg)

Maximum operating pressure:

Connections

Screwed NPT and BSPT



Materials

ASTM A48 Class 30 Body: Internals All stainless steel-304 Valve and seat: Stainless steel—17-4PH Test plug: Carbon steel

Options

- · Stainless steel internal check valve
- · Thermic vent bucket
- Scrub wire

Specification

Inverted bucket steam trap, type ... in cast iron, with continuous air venting at steam temperature, free floating stainless steel mechanism, and discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

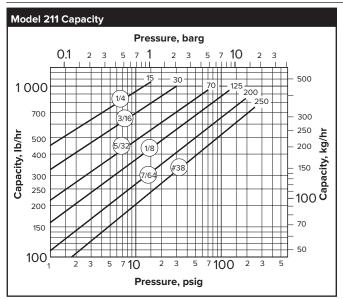
For a fully detailed certified drawing, refer to CD #1001.

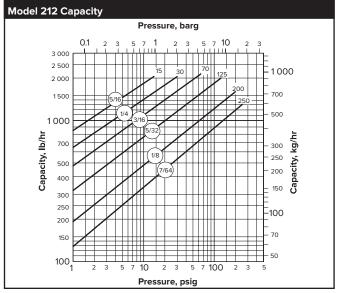
200 Series, Bottom Inlet, Top Outlet Traps Add suffix "CV" to model number for internal check valve, "T" for thermic vent bucket.												
Model No.	Model No. 211 212			2	213		4	215		216		
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1, 1-1/4	25, 32	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50
Test Plug	1/8	3	3/8	10	1/2	15	1/2	15	3/4	20	1	25
"A" (Flange Diameter)	4-1/4	108	5-1/4	133	6-3/8	162	7-1/2	190	8-1/2	216	10-3/16	259
"B" (Height)	6-7/16	164	8-5/8	218	11-1/2	292	12-3/8	314	14-3/16	360	18	457
Number of Bolts	6	5	8	8		6			8		12	
Weight Ib (kg)	6 (2	2.7)	11-1/2	(5.2)	20-1/4	4 (9.2)	33 (15.0) 44-3/4 (20.3)			77-1/2	(35.2)	

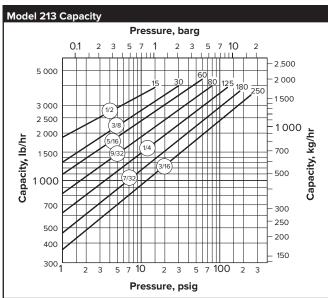
Cast Iron for Vertical Installation

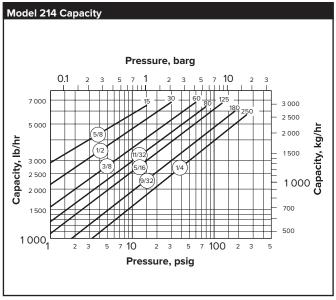
For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

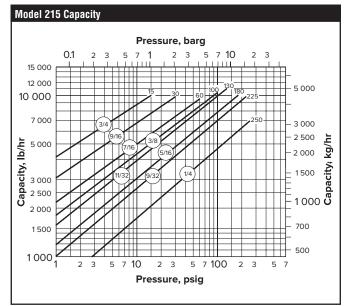


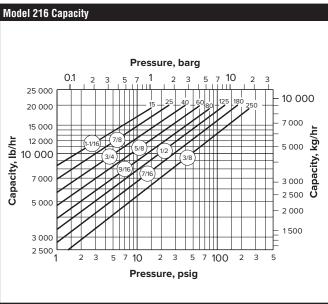












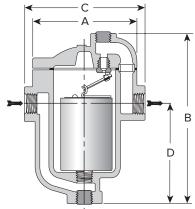
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

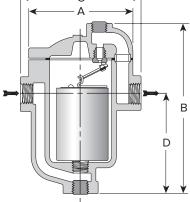
Armstrong®

800-813 Series Inverted Bucket Steam Trap

Cast Iron for Horizontal Installation

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)





Description

The most reliable steam trap known—the inverted bucket—provides efficient condensate drainage of virtually all types of steam-using equipment. Put the inverted bucket to work in a tough cast iron package, and you have the best of both worlds. Because they operate efficiently for longer periods of time, Armstrong cast iron inverted buckets add solid energy savings to lower replacement/labor costs. All Armstrong cast iron inverted bucket steam traps are repairable for even bigger maintenance savings.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat.

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and CO₂ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, allowing no condensate backup. They are also resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Maximum operating pressure:

250 psig @ 450°F (17 barg @ 232°C) Model 800: 150 psig (10 barg) Model 811-813: 250 psig (17 barg)

Connections

Screwed NPT and BSPT



Materials

ASTM A48 Class 30 Body: Internals All stainless steel-304 Valve and seat: Stainless steel—17-4PH Test plug: Carbon steel

Options

- · Stainless steel internal check valve
- · Thermic vent bucket
- · Stainless steel pop drain
- Probe connection · Thermo drain
- Scrub wire

Specification

Inverted bucket steam trap, type ... in cast iron, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and discharge orifice at the top of the trap.

How to Order

Specify:

- · Model number
- · Size and type of pipe connection
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

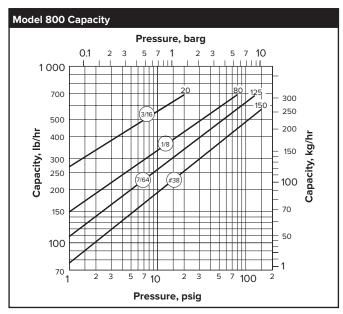
800-813 Series Side Inlet, Side Outlet Traps. Add suffix "CV" to model number for internal check valve, "T" for thermic vent bucket.										
Model No.	800*		8	11	8	12	813			
	in	mm	in	mm	in	mm	in	mm		
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1	20, 25		
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20		
"A" (Flange Diameter)	3-3/4	95.2	3-3/4	95.2	5-5/8	143	7	178		
"B" (Height)	5-7/16	138	6-7/8	175	9-1/16	230	11-3/4	298		
"C" (Face-to-Face)	5	127	5	127	6-1/2	165	7-3/4	197		
"D" (Bottom to C Inlet)	2-3/4	70	4-1/4	108	5-3/8	137	7-1/32	179		
Number of Bolts		6								
Weight lb (kg)	5 (2	2.3)	6 (2.7)	15 (6.8)	27-1/2	2 (12.5)		

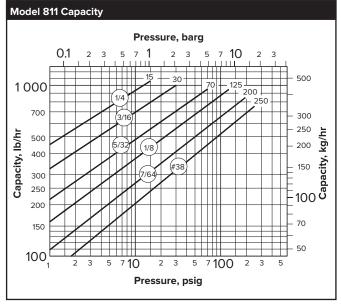
^{*}Cannot be furnished with both thermic vent bucket and check valve.

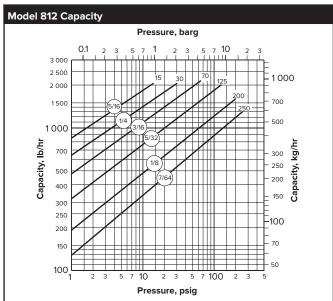
Cast Iron for Horizontal Installation

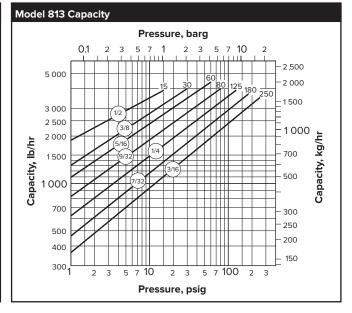
For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)









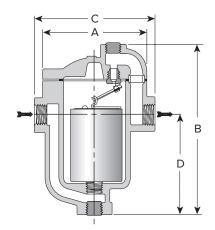


Armstrong®

814-816 Series Inverted Bucket Steam Trap

Cast Iron for Horizontal Installation

For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)





Description

The most reliable steam trap known—the inverted bucket—provides efficient condensate drainage of virtually all types of steam-using equipment. Put the inverted bucket to work in a tough cast iron package, and you have the best of both worlds. Because they operate efficiently for longer periods of time, Armstrong cast iron inverted buckets add solid energy savings to lower replacement/labor costs. All Armstrong cast iron inverted bucket steam traps are repairable for even bigger maintenance savings.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat.

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and $\ensuremath{\text{CO}}_2$ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, allowing no condensate backup. They are also resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure

(vessel design):

250 psig @ 450°F (17 barg @ 232°C) Model 814-816: 250 psig (17 barg) Maximum operating pressure:

Connections

Screwed NPT and BSPT

Materials

Internals: Valve and seat: Test plug:

ASTM A48 Class 30 All stainless steel-304 Stainless Steel-17-4PH Carbon steel

Options

- Stainless steel internal check valve
- · Thermic vent bucket
- · Stainless steel pop drain
- · Probe connection
- · Thermo drain · Scrub wire

Specification

Inverted bucket steam trap, type ... in cast iron, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and discharge orifice at the top of the trap.

How to Order

Specify:

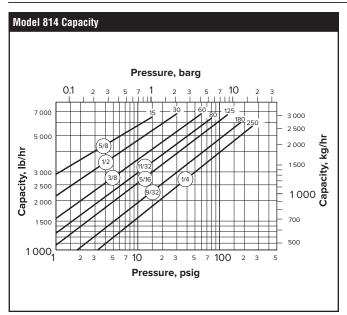
- Model number
- Size and type of pipe connection
- Maximum working pressure that will be encountered or orifice size
- · Any options required

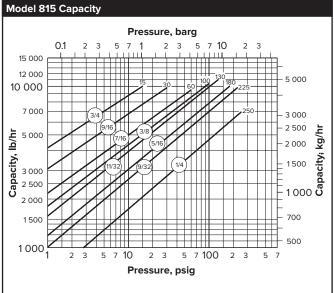
814-816 Series Side Inlet, Side Outlet Traps. Add suffix "CV" to model number for internal check valve, "T" for thermic vent bucket.										
Model No.	81	14	8:	15	816					
	in	mm	in	mm	in	mm				
Pipe Connections	1, 1-1/4	25, 32	1, 1-1/4, 1-1/2, 2	25, 32, 40, 50	2, 2-1/2	50, 65				
Test Plug	1	25	1-1/2	40	2	50				
"A" (Flange Diameter)	8	203	9	229	11-1/2	292				
"B" (Height)	13-5/8	346	16-1/4	413	21-5/16	541				
"C" (Face-to-Face)	9	229	10-1/4	260	13	330				
"D" (Bottom to Q Inlet)	7-13/16	198	8-1/16	205	11	279				
Number of Bolts	8									
Weight lb (kg)	44 (2	44 (20.0) 71 (32.2) 131 (59.4)								

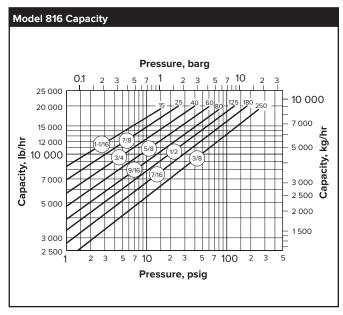
Cast Iron for Horizontal Installation

For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)







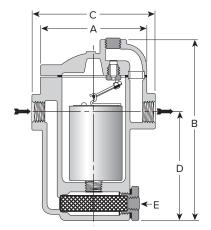


Armstrong®

880 Series Inverted Bucket Steam Traps

Cast Iron for Horizontal Installation With Integral Strainer

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)





The most reliable steam trap known—the inverted bucket—provides efficient condensate drainage of virtually all types of steam-using equipment. Put the inverted bucket to work in a tough cast iron package with an integral strainer, and you have the best of both worlds. Because they operate efficiently for longer periods of time, Armstrong cast iron inverted buckets add solid energy savings to lower replacement/labor costs. All Armstrong cast iron inverted bucket steam traps are repairable for even bigger maintenance savings.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat.

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and CO₂ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, allowing no condensate backup. They are also resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Maximum operating pressure:

250 psig @ 450°F (17 barg @ 232°C) Model 880: 150 psig (10 barg) Model 881-883: 250 psig (17 barg)



Connections

Screwed NPT and BSPT

Materials

Body: ASTM A48 Class 30 Internals All stainless steel-304 Valve and seat: Stainless steel-17-4PH Test plug: Carbon steel Strainer: Stainless steel-304

Options

- · Stainless steel internal check valve
- · Thermic vent bucket
- · Scrub wire

Specification

Inverted bucket steam trap, type \dots in cast iron with integral strainer, with continuous air venting at steam temperature, with free-floating stainless steel mechanism, and discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection
- Maximum working pressure that will be encountered or orifice size
- · Any options required

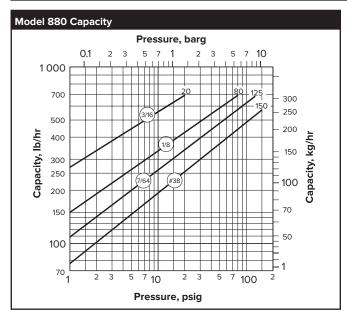
880 Series Side Inlet, Side Outlet Traps With Integral Strainers. Add suffix "CV" to model number for internal check valve, "T" for thermic vent bucket.										
Model No.	880*		8	81	8	82	883			
	in	mm	in mm		in	mm	in	mm		
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1, 1-1/4	20, 25, 32		
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20		
"A" (Flange Diameter)	3-3/4	95.2	3-3/4	95.2	5-5/8	142.9	7	177.8		
"B" (Height)	6-1/16	154	7-1/16	179	9-3/8	244	12-3/8	314		
"C" (Face-to-Face)	5	127	5	127	6-1/2	165	7-7/8	200		
"D" (Bottom to Q Inlet)	3-7/16	87.3	4-7/16	113	5-3/4	146	7-3/8	187		
"E" (Blowdown Connection)	3/8	9	3/8	9	3/8	9	1/2	15		
Number of Bolts					6					
Weight lb (kg)	5-1/2	5-1/2 (2.5) 6 (2.7) 15-1/2 (7.0) 31 (14.1)								

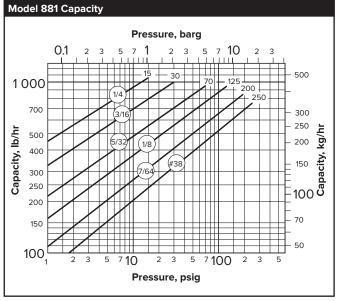
^{*}Cannot be furnished with both thermic vent bucket and check valve.

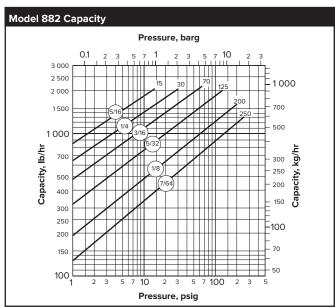
Cast Iron for Horizontal Installation With Integral Strainer

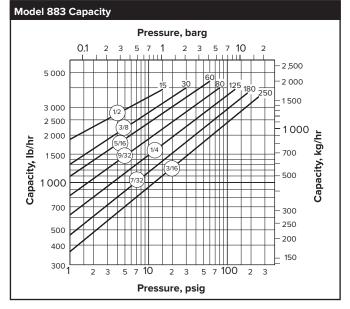
For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)







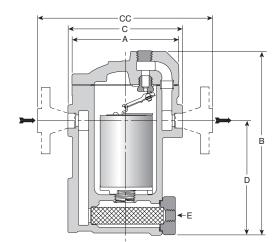






Cast Steel for Horizontal Installation With Integral Strainer

For Pressures to 600 psig (41 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)





Armstrong offers two sizes of cast steel traps with in-line horizontal pipe connections and integral strainers with a choice of screwed, socketweld or flanged connections.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and CO₂ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, allowing no condensate backup. They are also resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

600 psig @ 650°F (41 barg @ 343°C) 600 psig (41 barg)

Maximum operating pressure:

Connections

Screwed NPT and BSPT Socketweld Flanged

See page 187 for dimensional information for flanged and socketweld connections.

Materials

Body: ASTM A216 WCB Internals: All stainless steel-304 Stainless steel-17-4PH Valve and seat: Strainer: Stainless steel-304 Test plug: Carbon steel



Options

- · Stainless steel internal check valve
- · Thermic vent bucket (983 only) maximum operating pressure 250 psig (17 bara)
- Scrub wire

Specification

Inverted bucket steam trap, type ... in cast steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, integral strainer, and discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection. When flanges are required, specify type of
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

For a fully detailed certified drawing, refer to CD #1007.

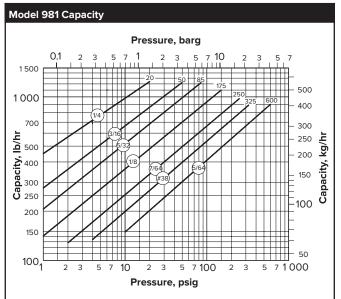
980 Series Traps					
Model No.	9	81	983		
Dina Connections	in	mm	in	mm	
Pipe Connections	1/2, 3/4	15, 20	3/4, 1	20, 25	
Test Plug	1/2	15	3/4	20	
"A" (Flange Diameter)	4-1/2	114	7-1/4	184	
"B" (Height)	8-5/8	219	12-5/16	313	
"C" (Face-to-Face, Scr or SW)	5-3/8	137	7-3/4	197	
"CC" (Face-to-Face, Class 600 ANSI Flanges*)					
1/2" (15 mm) connection	9-3/8	238	_	_	
3/4" (20 mm) connection	9-1/2	241	11-3/4	298	
1" (25 mm) connection	_	_	12-1/8	308	
"D" (Bottom to Q Inlet)	4-13/16	122	7-9/16	192	
"E" (Blowdown Connection)	3/8	9	3/4	20	
Weight, Scr or SW lb (kg)	11-1/2	(5.2)	43 (19.5)		
Weight, 600 Class Flanges Ib (kg) 1/2" connection	18 (8.2)	50 (22.7)	

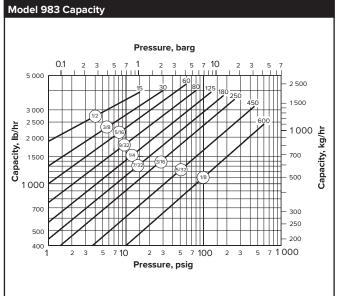
^{*}Face-to-face, other flanges on request. Also available with ANSI raised face, flat face or ring joint flanges.

Cast Steel for Horizontal Installation With Integral Strainer

For Pressures to 600 psig (41 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)









Forged Carbon Steel for Horizontal Installation

For Pressures to 454 psig (32 barg)...Capacities to 1 058 lb/hr (480 kg/hr)

Description

Armstrong's type EM forged steel inverted bucket steam trap combines the most reliable steam trap operating principle known in a body, which can be opened for Easy Maintenance.

High resistance to wear, corrosion and water hammer.

The free-floating guided lever valve mechanism is "frictionless" with all wear points heavily reinforced. All working parts are stainless steel; valve and seat are hardened chrome steel, individually ground and lapped.

Freedom from dirt problems. Condensate flow under bottom edge of bucket keeps sediment and "sludge" in suspension until discharged by full differential purging action. Valve orifice opens wide - closes tight. There is no buildup of dirt, no close clearances to be affected by scale. Under normal conditions of reasonably "clean steam", a strainer is not necessary. However, this is left to the user's discretion.

Air handling ability. Vent in bucket top provides continuous automatic air and CO2 venting with no cooling leg and prevents air binding. Wiggle wire ensures clean vent hole at all times. Any steam passing through vent is condensed and discharged as liquid.

No steam loss. Steam does not reach the water sealed valve.

Inverted bucket traps require no adjustment and no live steam to operate.

Maximum operating conditions

Maximum allowable pressure

(vessel design): 464 psig @ 482°F

(32 barg @ 250°C)

Maximum operating pressure: 464 psig (32 barg)
Maximum back pressure: 99% of inlet pressure

Connections

Screwed BSPT and NPT Socketweld Flanged DIN or ANSI (welded)

Materials

Body: Forged carbon steel
Internals: All stainless steel – 304
Valve and seat: Stainless steel – 440F
Gasket: Spiral wound graphite

Bolts: 24 CrMo5

Options

- · Bucket vent scrubbing wire for heavy dirt/oil conditions
- · For superheated steam we advise stellited valve and seat

How to order

Specify:

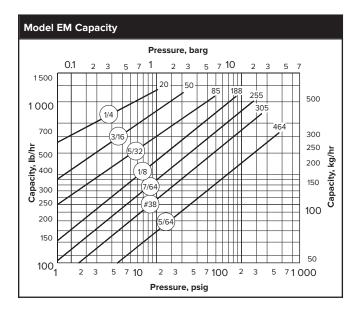
- · Size and type of pipe connection
- Max. working pressure that will be encountered or orifice size
- · Max. condensate load
- Any options required

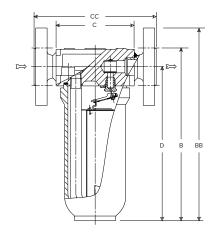


Forged Carbon Steel for Horizontal Installation

For Pressures to 454 psig (32 barg)...Capacities to 1 058 lb/hr (480 kg/hr)







Model EM Side Inlet, Side Outlet Trap (dimensions in mm)									
Pipe Connections	in	mm	in	mm	in	mm			
	1/2	15	3/4	20	1	25			
"C" Face-to-Face (screwed & SW)	3-5/8	92	3-5/8	92	-	-			
"CC" Face-to-Face (flanged ANSI CL150)	6-3/4	171	7	178	7-1/4	184			
"CC" Face-to-Face (flanged ANSI CL300)	7	178	7-3/8	187	7-3/4	197			
"D" Bottom to C Inlet	7-7/16	189	7-7/16	189	7-7/16	189			
"B" Height (screwed & SW)	8-1/4	210	8-1/4	210		-			
"BB" Height (flanged*)	9-1/4	235	9-7/16	240	9-5/8	245			
Weight, screwed, lb (kg)	6.8	(3.1)	6.8	(3.1)	_				
Weight, flanged, lb (kg)	12 (5.5)	15.7	(7.1)	18 (8.1)				



Forged Carbon Steel for Vertical Installation

For Pressures to 650 psig (45 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

Description

Armstrong offers its 300 Series forged carbon steel traps for vertical installation with a choice of screwed, socketweld or flanged connections.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating, and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket, which provides continuous automatic air and CO_2 venting at steam temperature.

Inverted bucket traps drain continuously, allowing no condensate backup. They are also resistant to water hammer.

For Superheat Service:

- 1. Don't oversize the orifice; a restricted orifice may be advisable.
- 2. Specify an internal check valve.
- 3. Provide a drip leg of adequate diameter and length.
- 4. Provide a generous length (2'-3') of inlet piping, with the trap below the main.
- 5. Don't insulate the trap or the inlet piping.

Connections

Screwed NPT and BSPT Socketweld Flanged

See page 187 for dimensional information for flanged and socketweld connections.

Materials

Body: ASTM A105

Models 312, 313, 316 are also available with cast 316 stainless steel bodies and all stain-

less steel internals

Internals:

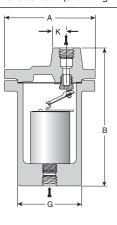
All stainless steel—304 (Models 314, 315 and 316 have cast iron bucket weights)

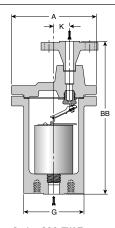
Valve and seat:

Stainless steel—17-4PH or Titanium

Options

- Stainless steel internal check valve
- Thermic vent bucket 250 psig (17 barg) maximum
- Scrub wire





Series 300 Trap

Series 300-FW Trap

Specification

Inverted bucket steam trap, type ... in forged carbon steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- Size and type of pipe connection. When flanges are required, specify type of flange in detail
- Maximum working pressure that will be encountered or orifice size
- · Any options required

Pressu	Pressure-Temperature Rating for Forged Steel Traps										
	May	Oper.			Allowa		,				
Model		sure,	°F	°C	°F	°C	°F	°C	°F	°C	
No.	Sat. Steam		-20/ +650	-28/ +343	700	371	750	399	800	427	
	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	
310	400	27.5	770	48	770	48	730	50	600	41	
312	600	41	600	41	600	41	560	38.5	500	34.5	
313	650	45	1080	74	1 080	74	970	67	780	54	
314	650	45	1 130	78	1120	77	990	68	810	56	
315	650	45	1 015	70	965	66.5	860	59	690	47.5	
316	650	45	1 100	76	1050	72	940	65	760	52	

NOTES: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used. Maximum allowable pressures shown in boldface will be marked on nameplate, unless otherwise requested. Traps with flanges may have different pressure-temperature ratings.

300 Series Bottom Inlet, Top Outlet Traps. Add suffix "CV" to trap number for internal check valve.													
Model No. Screwed or SW Model No. Flanged	310 310-FW		312 312-FW		313 313-FW		314 314-FW		315 315-FW		316 316-FW		
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1, 1-1/4	25, 32	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	
"A" (Diameter)	4-5/8	117	6-3/4	171	8	203	8-5/8	219	9-3/4	248	11-7/8	302	
"B" (Height, Screwed or SW)	7-15/16	202	10-3/16	259	11-1/2	292	13-11/16	348	15	381	17-1/8	435	
"BB"	12-1/16*	306*	12-5/16	313	13-7/8	352	16-1/16	408	17-9/16	446	19-11/16	500	
"G" (Body OD)	3-1/16	78	4-3/4	121	5-1/8	130	5-3/4	146	6-5/8	168	8-3/8	213	
"K" (@ Outlet to @ Inlet)	9/16	14.3	1-1/4	31.7	1-7/16	36.5	1-7/16	36.5	1-3/4	44.4	2-1/8	54.0	
Number of Bolts	6				8			9		10			
Weight Scr. or SW lb (kg)	10 (4.5) 30 (13.6)		50 (22.7)		70 (31.8)		98 (44.5)		179 (81.2)				
Weight, Flanged lb (kg)	12 (5	.4)	32 ((14.5)	51 (2	51 (23.1)		3.1)	103 (46.7)		184 (8	184 (83.5)	

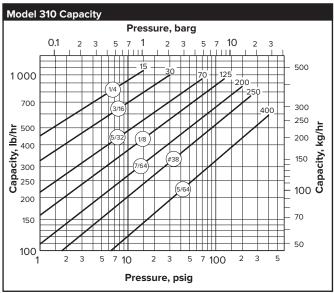
[&]quot;"BB" dimensions shown are for 3/4" conn., Class 600 flanged No. 310-FW. Consult factory for dimensions of models with other connection sizes and/or flanges.

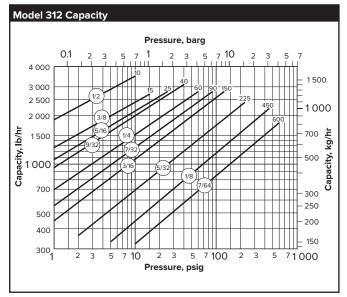
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

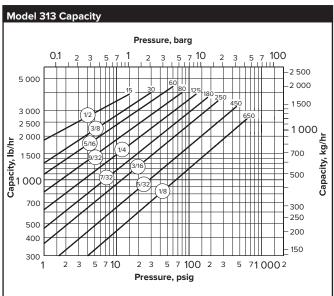
Forged Carbon Steel for Vertical Installation

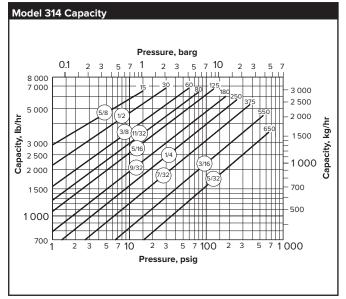
For Pressures to 650 psig (45 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

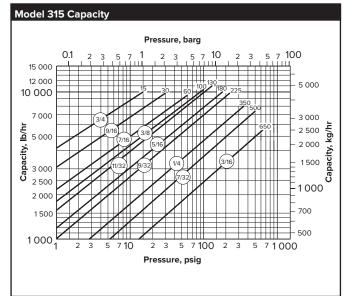


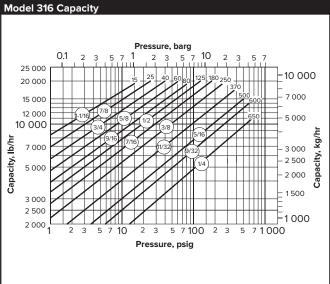










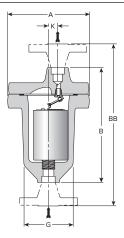


Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Forged Carbon Steel for Vertical and Horizontal Installation

For Pressures to 1 000 psig (69 barg)...Capacities to 1 300 lb/hr (590 kg/hr)



Model 411G Trap

Description

Armstrong Model 411G vertical installation offers smaller capacities at higher pressures.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat.

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket.

Inverted bucket traps drain continuously to prevent condensate backup. They are also resistant to water hammer.

411G Bottom Inlet, Top Outlet Traps Add suffix "CV" to trap number for internal check valve.										
Model No. Screwed or SW Model No. Flanged	411G 411G-FW									
Dina Cannastiana	in	mm								
Pipe Connections	1/2, 3/4	15, 20								
"A" (Diameter)	6-5/16	160								
"B" (Height, Screwed or SW)	8-13/16	224								
"G" (Body OD)	4-1/16	103								
"K" (@ Outlet to @ Inlet)	3/4	19.0								
Number of Bolts	3	3								
Weight Scr. or SW lb (kg)	25 (11.3)								
Weight, Flanged lb (kg)	35 (5 (15.9)								

Consult factory for "BB" dimensions.



Connections

Screwed NPT and BSPT Socketweld Flanged

See page 187 for dimensional information for flanged and socketweld connections.

Materials

Body: ASTM A105 411G cap: ASTM A105

Internals: All stainless steel—304

Valve and seat: Titanium

Options

Stainless steel internal check valve

Specifications

Inverted bucket steam trap, type ... in forged carbon steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, with the discharge orifice at the top of the trap.

How to Order

Specify:

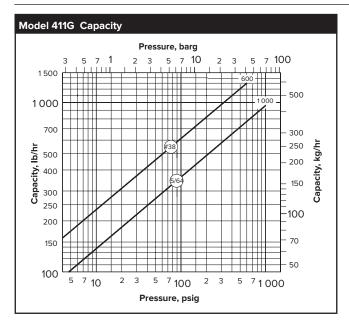
- Model number
- Size and type of pipe connection. When flanges are required, specify type of flange in detail
- Maximum working pressure that will be encountered or orifice size
- Any options required

For a fully detailed certified drawing, refer to CD #1105.

Forged Carbon Steel for Vertical and Horizontal Installation

For Pressures to 1 000 psig (69 barg)...Capacities to 1 300 lb/hr (590 kg/hr)





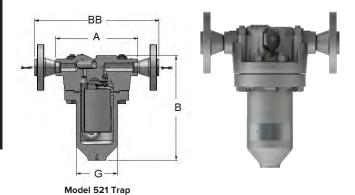
Pressure	Pressure-Temperature Rating for Forged Steel Traps												
	Max. 0		Maximum Allowable Pressure (Vessel Design) of Pressure-Containing Parts at Indicated Temperature										
Model	Press	/							°F	°C			
No.	Sat. 3	team	-20/+650	-28/+343	700	371	750	399	800	427			
	psig barg		psig	barg	psig	barg	psig	barg	psig	barg			
411G	1000	69	1000	69	1000	69	950	65.5	840	58			

NOTE: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used. Maximum allowable pressures shown in boldface will be marked on nameplate, unless otherwise requested. Traps with flanges may have different pressure-temperature ratings.



Forged Carbon Steel for Horizontal Installation

For Pressures to 1 000 psig (69 barg)...Capacities to 1 300 lb/hr (590 kg/hr)



Description

Armstrong $\dot{\text{M}}$ Model 521 horizontal installation offers smaller capacities at higher pressures.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating and has no fixed pivots to create wear or friction, because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat. The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket. Inverted bucket traps drain continuously to prevent condensate backup. They are also resistant to water hammer. Model 521 adds the convenience and savings of in-line repairability and is designed to meet today's energy-management requirements efficiently and economically over a long, trouble-free service life. Model 521 also has an integral strainer to protect from dirt and scale

Connections

Screwed NPT and BSPT Socketweld Flanged

Materials

Body: ASTM A105N
Cap: ASTM A105N
Internals: All stainless steel—304
Valve and seat: Titanium
Strainer Screen Stainless Steel

Bolt/Nut ASTM A193 Gr B7 / ASTM A194 Gr 2H

Specifications

Inverted bucket steam trap with integral strainer, type ... in forged carbon steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, with the discharge orifice at the top of the trap.

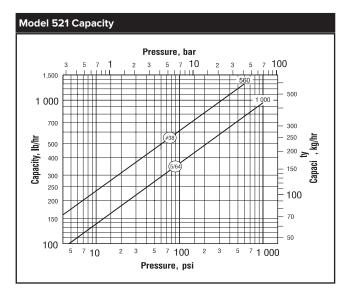
How to Order

Specify:

- Model number
- Size and type of pipe connection. When flanges are required, specify type
 of flange in detail
- Maximum working pressure that will be encountered or orifice size
- · Any options required

521 Side Inlet, S	521 Side Inlet, Side Outlet Traps										
Model No. Screwed or SW Model No. Flanged	52 521-										
	in	mm									
Pipe Connections	1/2, 3/4	15, 20									
"A"	8	203									
"B" (Height, Screwed or SW)	10-5/16	263									
"G" (Body OD)	4	102									
Number of Bolts	8										
Weight Scr. or SW lb (kg)	30 (1	3.4)									

Consult factory for "BB" dimensions.



NOTE: #38 orifice in Model 521 is limited to 560 psig (39 barg).

Pressure	Pressure-Temperature Rating for Forged Steel Traps												
	Max. (Maximum Allowable Pressure (Vessel Design) of Pressure-Containing Parts at Indicated Temperature										
Model	Pressure, Sat. Steam		°F	°C	°F	°C	°F	°C	°F	ů			
No.	Sat. Steam		-20/+650	-28/+343	700	371	750	399	800	427			
	psig barg		psig	barg	psig	barg	psig	barg	psig	barg			
521	1000	69	1000	69	1000	69	950	65.5	840	58			

NOTE: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used. Traps with flanges may have different pressure-temperature ratings.

Armstrong
Steam Tracing Equipment
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Notes



Forged Chrome-moly Steel for Vertical Installation

For Pressures to 1 000 psig (69 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

Description

Armstrong offers its 400 Series forged chrome-moly steel traps for vertical installation with a choice of screwed, socketweld or flanged connections.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat.

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket. This provides continuous automatic air and CO_2 venting at steam temperature.

Inverted bucket traps drain continuously to prevent condensate backup. They are also resistant to water hammer.

Operation on Superheat. A normally operating bucket trap is filled with saturated steam and condensate. Superheated steam can enter only as fast as the steam inside can condense. As a result, the temperature of the trap is at (or slightly below) saturated steam temperature, regardless of the degree of superheat.

Trap Selection. The pressure-containing parts of the steam trap should safely withstand the maximum pressure and temperature conditions of the system. For example, a trap is required for a 900 psig (62 barg) main at 900°F (482°C). The normal operating temperature of the trap will be about 532°F (278°C). A Model 415 trap should be selected, even though several smaller traps are capable of handling the working pressure.

For Superheat Service:

- 1. Don't oversize the orifice; a restricted orifice may be advisable.
- 2. Specify an internal check valve.
- 3. Provide a drip leg of adequate diameter and length.
- 4. Provide a generous length (2'-3') of inlet piping, with the trap below the main.
- 5. Don't insulate the trap or the inlet piping.

Connections

Screwed NPT and BSPT Socketweld Flanged

See page 187 for dimensional information for socketweld connections.

Materials

Body: ASTM A182 F22 Class 3

Models 413 and 415 are available with cast 316 stainless steel bodies and all stainless

steel internals

Internals: All stainless steel—304

Valve and seat: Stainless steel—17-4PH or Titanium

Options

Stainless steel internal check valve

Specification

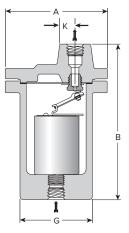
Inverted bucket steam trap, type ... in forged chrome-moly steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, with the discharge orifice at the top of the trap.

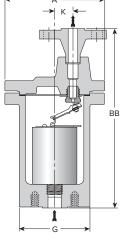
How to Order

Specify:

- · Model number
- Size and type of pipe connection. When flanges are required, specify type of flange in detail
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

For a fully detailed certified drawing, refer to CD #1002.





Series 400 Trap

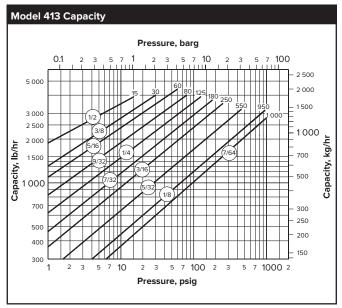
Series 400-FW Trap

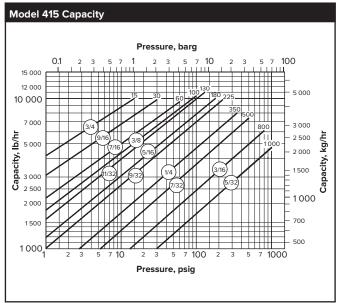
400 Series, Bottom Inlet, Top O		•	1		1			
Model No. Screwed or SW	=	13	-	15	-	416		
Model No. Flanged	413	-FW	415	-FW	416	-FW		
Dia a Canna asti ana	in	in mm		in mm		mm		
Pipe Connections	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50		
"A" (Diameter)	8-5/8	219	10-3/4	273	12-1/2	317		
"B" (Height, Screwed or SW)	12-3/16	310	14-15/16	379	17-5/8	448		
"BB"	14-7/8	378	18-1/16	459	459 21-1/2			
"G" (Body OD)	5-3/8	137	6-7/8	175	8-1/2	216		
"K" (Ç Outlet to Ç Inlet)	1-7/16	36.5	1-3/4	44.4	2-1/8	54.0		
Number of Bolts	_	8	Ç	9	1	2		
Weight Scr. or SW lb (kg)	65 (29.5) 126 (57.2) 205 (93.0)			
Weight, Flanged lb (kg)	70 (31.8)	132 (59.9)	211 (95.7)		

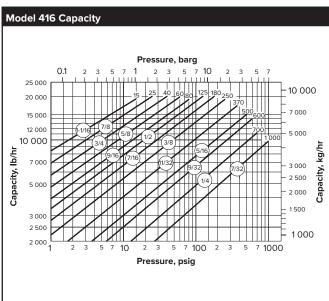
Forged Chrome-moly Steel for Vertical Installation

For Pressures to 1 000 psig (69 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)









Pressure-	-Temperat	ture Ratin	g for Forge	d Steel Tra	ps									
	Max.	K. Oper. Maximum Allowable Pressure (Vessel Design) of Pressure-Containing Parts at Indicated Temporary											Temperat	ture
Model	<u> </u>		°F	°C	°F	°C	°F	°C	°F	°C	°F	°C	°F	°C
No	Ste	am	-20/+650	-28/+343	700	371	750	399	800	427	850	454	900	482
	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
413	1000	69	1200	83	1200	83	1200	83	1200	83	1050	72	780	54
415	1000	69	1 100	76	1100	76	1 100	76	1 100	76	1 080	74.5	965	66.5
416	1000	69	1700	117	1700	117	1700	117	1660	114	1350	93	990	68

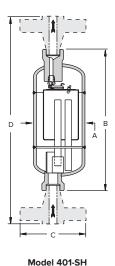
NOTES: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used. Maximum allowable pressures shown in boldface will be marked on nameplate, unless otherwise requested. Traps with flanges may have different pressure-temperature ratings.

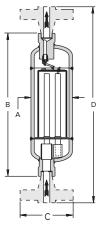


401-SH/501-SH Series Inverted Bucket Superheat Steam Trap

Carbon Steel or Stainless Steel for Vertical Installation

For Pressures to 1 540 psig (105 barg)...Capacities to 950 lb/hr (432 kg/hr)









Description

Armstrong's 401-SH/501-SH Series inverted bucket steam trap line is made for overcoming the difficult combination of superheat and high pressure/low load

To survive this most severe steam service, Armstrong created an inverted bucket trap with a unique accumulation chamber. The chamber collects sufficient condensate to ensure full discharge cycles. A cup in the chamber floats up and down on the steam inlet tube, sealing it off as the condensate level rises. At the same time as the chamber collects condensate, steam continues to flow under the bucket, making sure that the discharge valve closes tightly until the condensate rises into the trap body and the bucket falls down. The operation is on/off, no throttling or dribbling.

Furthermore, it combines all the advantages of an inverted bucket steam trap:

- · High resistance to wear, corrosion and water hammer with no gaskets.
- A unique leverage system multiplies the force provided by the bucket, to open the valve against system pressure.
- · The mechanism is located at the top. No dirt can collect on the orifice. Small particles of dirt will be held in suspension until discharged by the full differential purging action.
- The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small hole in the bucket.
- Inverted bucket traps require no adjustment. They do not allow condensate backup and are resistant to water hammer.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model 401-SH: 1 000 psig @ 800°F (69 barg @ 427°C) Model 501-SH: 1 540 psig @ 850°F (105 barg @ 454°C)

Maximum operating pressure:

Model 401-SH: 1 000 psig Model 501-SH: 1 540 psig

Connections

Screwed NPT and BSPT (401-SH only) Socketweld Flanged

See page 187 for dimensional information for flanged and socketweld connections.

Materials

Body:

Model 401-SH Carbon steel ASTM A106 Gr. B Sch. 80 pipe Stainless steel 316L ASTM A312 Sch. 80 pipe Model 501-SH Internals: Stainless steel-304

Valve and seat: Titanium Connections:

> Model 401-SH Stainless steel-304 Model 501-SH Stainless steel-316L

Specification

Inverted bucket steam trap, type ... in carbon steel (stainless steel), with accumulation chamber, continuous air venting at steam temperature, stainless steel leverage system, with the discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection. When flanges are required, specify type of flange in detail
- · Maximum working pressure that will be encountered or orifice size

For a fully detailed certified drawing, refer to: 401-SH CD #1011 501-SH CD #1012

401-SH and 501-SH Series	Steam 1	Traps							
Model	401	-SH	501-SH						
	in	mm	in	mm	in	mm			
Pipe Connections	1/2, 3/4	15, 20	1/2	15	3/4	20			
"A" Diameter (NPT, BSPT or SW)	4	100	4	100	4	100			
"B" Height (NPT, BSPT or SW)	11	275	13-9/16	344	13-9/16	344			
"C" Diameter (Flanged)*	4-5/8	117	4-3/4	121	5-1/8	130			
"D" Height (Flanged)*	15-1/8	384	18-3/16	462	18-11/16	475			
Weight NPT, BSPT or SW lb (kg)	12 (5.5)		15					
Weight Flanged lb (kg)	15 (6.7)		29	9 (13)				

^{*401-}SH 600 lb RF shown. 501-SH 900/1500 lb RF shown.

401-SH/501-SH Series Inverted Bucket Superheat Steam Trap

Carbon Steel or Stainless Steel for Vertical Installation

For Pressures to 1 540 psig (105 barg)...Capacities to 950 lb/hr (432 kg/hr)



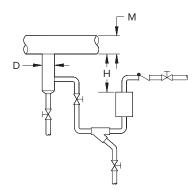
Installation Recommendations

What little condensate there is on superheat and high pressure/low load service usually forms in drip legs and in the traps themselves. Therefore proper piping and drip legs of adequate size and diameter are essential for the successful operation of the Armstrong superheat trap.

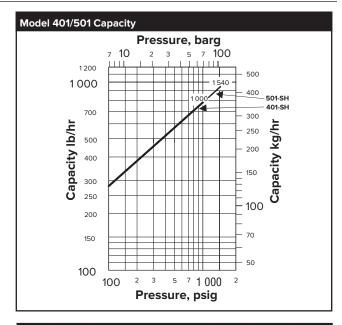


Drip Leg Sizing

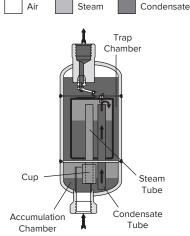
The properly sized drip leg will capture condensate. Too small a drip leg can actually cause a venturi "piccolo" effect where pressure drop pulls condensate out of the drip leg and trap.



Trap Draining Drip Leg on Steam Main



Recomn	nended St	eam Mair	and Brai	nch Line I	Orip Leg 1	racing	
ı	M	ı	D	H Dr	ip Leg Le	ngth Mini	mum
	eam n Size		Leg neter		rvised m-Up		ic Warm- Jp
in	mm	in	mm	in	mm	in	mm
1/2	15	1/2	15	10	250	28	710
3/4	20	3/4	20	10	250	28	710
1	25	1	25	10	250	28	710
2	50	2	50	10	250	28	710
3	75	3	75	10	250	28	710
4	100	4	100	10	250	28	710
6	150	4	100	10	250	28	710
8	200	4	100	12	300	28	710
10	250	6	150	15	380	28	710
12	300	6	150	18	450	28	710
14	350	8	200	21	530	28	710
16	400	8	200	24	600	28	710
18	450	10	250	27	685	28	710
20	500	10	250	30	760	30	760
24	600	12	300	36	910	36	910



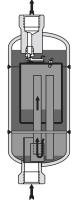
Cycling—Discharge Valve Wide Open

With the steam feed tube to the trap chamber sealed, condensate flows through the condensate feed tube (from accumulation chamber) into the trap chamber. This sinks the inverted bucket, which opens the discharge valve, cycling the trap.



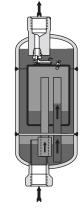
Cycle Ending

As the level of condensate in the accumulation chamber falls, the cup sealing the steam feed tube moves downward, opening a passage for steam to flow into trap chamber.



Trap Closed

As steam begins to flow through the accumulation chamber and up the steam feed tube under the inverted bucket in the trap chamber, the discharge valve closes tightly.



Cycle About to Repeat

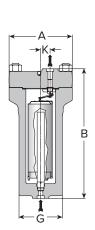
As the level of condensate rises in the accumulation chamber, the cup floats up until it again seals the steam feed tube, and the cycle repeats.

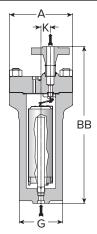
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Forged Chrome-moly Steel for Vertical Installation

For Pressures to 1 800 psig (124 barg)...Capacities to 5 150 lb/hr (2 336 kg/hr)





Series 5133G-5155G Traps

Series 5133G-FW & 5155G-FW Traps

Description

Armstrong offers its 5000 Series forged chrome-moly steel traps for vertical installation with a choice of screwed, socketweld or flanged connections.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket. This provides continuous automatic air and CO2 venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, to prevent condensate backup. They are also resistant to water hammer.

Operation on Superheat. A normally operating bucket trap is filled with saturated steam and condensate. Superheated steam can enter only as fast as the steam inside can condense. As a result, the temperature of the trap is at (or slightly below) saturated steam temperature, regardless of the degree of superheat.

Trap Selection. The pressure-containing parts of the steam trap should safely withstand the maximum pressure and temperature conditions of the system. For example, a trap is required for a 1 000 psig (68 barg) main at 950°F (510°C). The normal operating temperature of the trap will be about 546°F (286°C). A Model 5133G trap should be selected, even though several smaller traps are capable of handling the working pressure.



For Superheat Service:

- Don't oversize the orifice; a restricted orifice may be advisable.
- Specify an internal check valve.
- Provide a drip leg of adequate diameter and length.
- 4. Provide a generous length (2'-3') of inlet piping, with the trap below the main.
- 5. Don't insulate the trap or the inlet piping.

Connections

Screwed NPT and BSPT Socketweld Flanged

See page 187 for dimensional information for flanged and socketweld

Materials

Bodv: ASTM A182 F22 Class 3 All stainless steel-304 Internals:

Valve and seat: Titanium

Options

· Stainless steel internal check valve

For a fully detailed certified drawing, refer to: 5133 CD #1069 5155 CD #1096

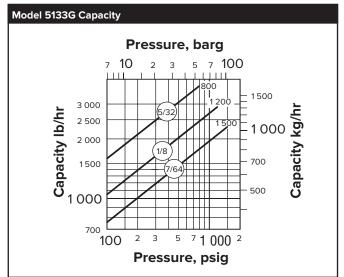
Model No. Screwed or SW Model No. Flanged		33G G-FW	5155G 5155G-FW			
Dina Cannastiana	in	mm	in	mm		
Pipe Connections	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4	20, 25, 32		
"A" (Diameter)	8-1/2	216	10-3/8	264		
"B" (Height, Screwed or SW)	14-1/4	362	16-7/32	412		
"BB"	18-7/8*	479*	20-7/8*	530*		
"G" (Body OD)	5-3/4	146	7-5/8	194		
"K" (டி Outlet to டி Inlet)	1-5/16	33.3	1-3/4	44.4		
Number of Bolts		8	10			
Weight Scr. or SW lb (kg)	113 (44.5)	171 (77.6)			
Weight, Flanged Ib (kg)	120	(47.6)	185 (83.9)		

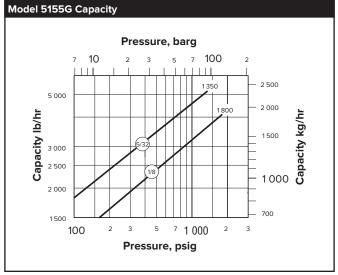
^{*&}quot;BB" dimensions shown are for 1" conn. Class 1500 flanged No. 5133G-FW and 1-1/4" conn. Class 1500 flanged No. 5155G-FW. Consult factory for dimensions of models with other connection sizes and/or flanges.

Forged Chrome-moly Steel for Vertical Installation

For Pressures to 1 800 psig (124 barg)...Capacities to 5 150 lb/hr (2 336 kg/hr)







Pressure-	Pressure-Temperature Rating for Forged Steel Traps																	
	Max.	Oper.		Maximum Allowable Pressure (Vessel Design) of Pressure-Containing Parts at Indicated Temperature											•			
Model	Pressu	re, Sat.	°F											°C				
No.	Ste	am	-20/+650	-28/+343	700	371	750	399	800	427	850	454	900	482	950	510	1000	538
	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
5133G	1500	103	2 120	146	2 120	146	2 120	146	2 120	146	1990	137	1730	119	1350	93	930	64
5155G	1800	124	2 520	174	2 520	174	2 520	174	2 520	174	2 370	163	2 070	143	1 610	111	1 110	76.5

NOTES: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used.

Maximum allowable pressures shown in boldface will be marked on nameplate, unless otherwise requested. Traps with flanges may have different pressure-temperature ratings.

Options

Internal Check Valves are spring loaded stainless steel and screw into an extended inlet tube having a pipe coupling at the top to save fittings, labor and money. Internal check valves may result in slightly reduced capacities.

Screwed Connections are available in all sizes for pressures of 900 psig or less. Traps for pressures of 900 psig or higher are available with socketweld or flanged connections.

Specification

Inverted bucket steam trap, type ... in forged chrome-moly steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, with the discharge orifice at the top of the trap.

How to Order

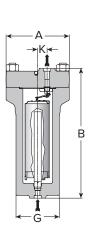
Specify:

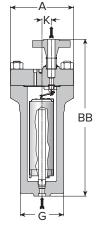
- Model number
- Size and type of pipe connection. When flanges are required, specify type of flange in detail
- Maximum working pressure that will be encountered or orifice size
- Any options required



Forged Chrome-moly Steel for Vertical Installation

For Pressures to 2 700 psig (186 barg)...Capacities to 6 500 lb/hr (2 948 kg/hr)





Model 6155G Traps

Model 6155G-FW Traps

Description

Armstrong offers its 6000 Series forged chrome-moly steel traps for vertical installation with a choice of socketweld or flanged connections.

A unique leverage system multiplies the force provided by the bucket to open the valve against system pressure. The mechanism is free-floating and has no fixed pivots to create wear or friction.

Because the mechanism is located at the top of the trap, no dirt can collect on the orifice. Small particles of dirt are held in suspension until discharged by the full differential purging action when the bucket sinks, pulling the valve off the seat

The discharge orifice is surrounded by a water seal, preventing live steam loss. Automatic air venting is provided by a small vent hole in the bucket. This provides continuous automatic air and CO₂ venting at steam temperature.

Inverted bucket traps drain continuously, although discharging intermittently, to prevent condensate backup. They are also resistant to water hammer.

Operation on Superheat. A normally operating bucket trap is filled with saturated steam and condensate. Superheated steam can enter only as fast as the steam inside can condense. As a result, the temperature of the trap is at (or slightly below) saturated steam temperature, regardless of the degree of superheat.

Trap Selection. The pressure-containing parts of the steam trap should safely withstand the maximum pressure and temperature conditions of the system. For example, a trap is required for a 1500 psig (102 barg) main at 1000°F (538°C). The normal operating temperature of the trap will be about 596°F (299°C). A Model 6155G trap should be selected, even though several smaller traps are capable of handling the working pressure.

For Superheat Service:

- 1. Don't oversize the orifice; a restricted orifice may be advisable.
- Specify an internal check valve.
- 3. Provide a drip leg of adequate diameter and length.
- 4. Provide a generous length (2'-3') of inlet piping, with the trap below the main.
- 5. Don't insulate the trap or the inlet piping.

6000 Series Bottom Inlet, Top Outlet Traps Add suffix "CV" to trap number for internal check valve.									
Model No. Screwed or SW 6155G Model No. Flanged 6155G-FW									
Dina Campastiana	in	mm							
Pipe Connections	1, 1-1/4	25, 32							
"A" (Diameter)	11-3/4	298							
"B" (Height, Screwed or SW)	24-1/8	613							
"BB"	29-11/16*	724*							
"G" (Body OD)	8-3/8	213							
"K" (C Outlet to C Inlet)	1-3/4	44.4							
Number of Bolts	1	0							
Weight Scr. or SW lb (kg)	325 (147.4)								
Weight, Flanged lb (kg)	340 (154.2)								

^{*&}quot;BB" dimensions shown are for Class 2500 flanged No. 6155G-FW traps. Consult factory for dimensions of models with other connection sizes and/or flanges.

Connections

Socketweld

Flanged

See page 187 for dimensions information for flanged and socketweld connections.

Materials

ASTM A182 F22 Class 3 Internals: All stainless steel-304

Valve and seat: Titanium

Options

Stainless steel internal check valve

Screwed connections are available in all sizes for pressures of 900 psig or less. Traps for pressures of 900 psig or higher are available with socketweld or flanged connections.

Specification

Inverted bucket steam trap, type ... 6155G in forged chrome-moly steel, with continuous air venting at steam temperature, free-floating stainless steel mechanism, with the discharge orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection. When flanges are required, specify type of flange in detail
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

For a fully detailed certified drawing, refer to CD #1092.

Forged Chrome-moly Steel for Vertical Installation

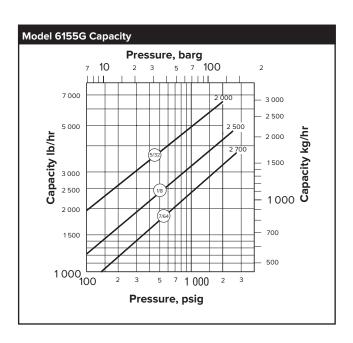
For Pressures to 2 700 psig (186 barg)...Capacities to 6 500 lb/hr (2 948 kg/hr)



Pressure	Pressure-Temperature Rating for Forged Steel Traps																	
Max. Oper. Maximum Allowable Pressure (Vessel Design) of Pressure-Containing Parts at Indicated Temp										peratur	е							
Model										°F	°C							
No.	Stea	am	-20/+650	-28/+343	700	371	750	399	800	427	850	454	900	482	950	510	1 000	538
	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
6155G	2 700	186	3 500	241	3 500	241	3 500	241	3 500	241	3 500	241	3 090	213	2 410	166	1650	114

NOTES: Maximum operating pressure to be marked on nameplate will be determined by actual orifice used.

Maximum allowable pressures shown in boldface will be marked on nameplate, unless otherwise requested. Traps with flanges may have different pressure-temperature ratings.



Options

Internal Check Valves are spring loaded stainless steel and screw into an extended inlet tube having a pipe coupling at the top to save fittings, labor and money. Internal check valves may result in slightly reduced capacities.



2000 Series Stainless Steel Traps

The Armstrong stainless steel traps—Series 1000, Series U-1000, Series 1800 and Series 2000—have high resistance to damage from freeze-ups. They also offer high resistance to wear and corrosion for longer service reliability, and they provide continuous air venting.

Armstrong stainless steel traps provide maximum ease and economy of installation, inspection or replacement. What's more, an Armstrong stainless steel trap is the ideal solution for trapping applications such as tracer lines, steam mains, and heating and processing applications.

Wear and corrosion resistance

Free-floating guided lever valve mechanism is "frictionless," and all wear points are heavily reinforced. All working parts are stainless steel. Valve and seat are stainless steel, individually ground and lapped together in matched sets.

360° universal 304 stainless steel connector

Provides quick, easy in-line renewability along with all the proven advantages of an inverted bucket operation. Also available with optional IS-2 integral strainer connector with 20 x 20 mesh stainless steel strainer.

Virtually no steam loss

Steam does not reach the water-sealed discharge valve.

Purging action

Snap opening of the valve creates a momentary pressure drop and turbulence in the unit drained. This breaks up films of condensate and air and speeds their flow to the trap.

Sealed, tamperproof 304-L stainless steel package

Able to withstand freeze-ups without damage.

Excellent operation against back pressure

Since trap operation is governed by the difference in density of steam and water, back pressure in the return line has no effect on the ability of the trap to open for condensate and close against steam.

Continuous air and CO₂ venting Vent in top of bucket provides continuous automatic air and CO₂ venting with no cooling lag or threat of air

binding. Steam passing through vent is less than that

required to compensate for radiation losses from the

operation
Simple, direct operation with
nothing to stick, bind or clog.
Only two moving parts—the
valve lever and the bucket.

Dependable

trap, so it's not wasted.

Freedom from dirt problems

Condensate flow under the bottom edge of the bucket keeps sediment and sludge in suspension until it is discharged with the condensate. Valve orifice opens wide and closes tightly. No buildup of dirt or close clearances to be affected by scale.

Resistance to damage from water hammer

Open bucket or float will not collapse as a result of water hammer.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

2000 Series Stainless Steel Traps



For Pressures to 650 (45 barg) psig... Capacities to 1 300 lbs/hr (590 kg/hr)

With the Series 2000 360° universal connector, you can install inverted bucket efficiency and long service life in any piping configuration with little or no repiping. You get the reliability of the inverted bucket operating principle, plus all the benefits of all-stainless steel construction:

- A sealed, tamperproof package
- · A compact, lightweight trap
- The ability to withstand freeze-ups without damage
- Exceptional corrosion resistance
- A three-year guarantee against defective materials or workmanship

Series 2000 steam traps combine savings in three important areas: energy, installation and replacement. The 360° universal connector provides quick, easy in-line renewability along with all the proven advantages of an inverted bucket operation. Choice of NPT or BSPT screwed connections, or socketweld connections.

Also available with IS-2 integral strainer connector.



Available with Standard Connector Material: 304 stainless steel



Available with
IS-2 Integral Strainer Connector
(shown with optional blowdown
valve)

Material: 304 stainless steel



IS-4 Connector

Material: ASTM A351 Gr. CF8M





All Stainless Steel for Vertical Installation

For Pressures to 650 psig (45 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)

Description

Armstrong 1000 Series stainless steel inverted bucket steam traps normally last three to four times longer than conventional traps used in identical services. Heat-treated stainless steel valves and seats are of the same design, material and workmanship as those used in traps for pressures up to 900 psig and temperatures to 900°F. More compact than cast iron or carbon steel equivalents, 1000 Series traps are ideal for trapping applications such as tracer lines, steam mains and heating/process applications.

The 1000 Series are guaranteed for three years.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

400 psig @ 800°F (28 barg @ 427°C) Model 1010, 1011: 650 psig @ 600°F (45 barg @ 316°C) Model 1022:

627 psig @ 700°F (43 barg @ 371°C) 604 psig @ 800°F (41.6 barg @ 427°C)

450 psig @ 800°F (31 barg @ 427°C) Model 1013:

Maximum operating pressure:

Model 1010: 150 psig (10 barg) Model 1011: 400 psig (28 barg) Model 1022: 650 psig (45 barg) Model 1013: 450 psig (31 barg)

Connections

Screwed NPT and BSPT

Socketweld

Materials

ASTM A240 Grade 304L Body: Internals: All stainless steel-304

Stainless steel—17-4PH or Titanium Valve and seat:

Options

- Stainless steel internal check valve
- · Thermic vent bucket 250 psig (17 barg) maximum;
- for Model 1022 15 psig (1 barg) maximum
- Wiggle wire
- 316 stainless steel valve and seat

Specification

Inverted bucket steam trap, type ... in all stainless steel, freeze resistant, without gaskets, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and orifice at the top of the trap.

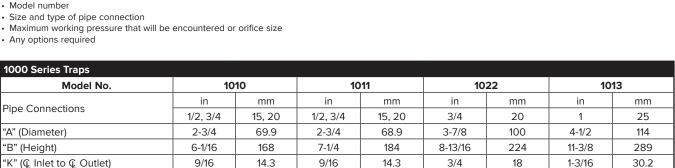
1-1/2 (0.7)

How to Order

Specify:

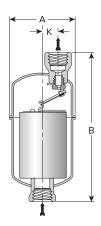
Model number

Weight lb (kg)



1-3/4 (0.8)





Model 1010 Trap

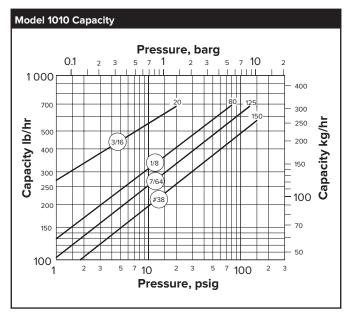
4 (2)

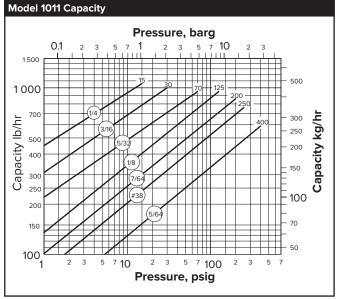
7-1/2 (3.4)

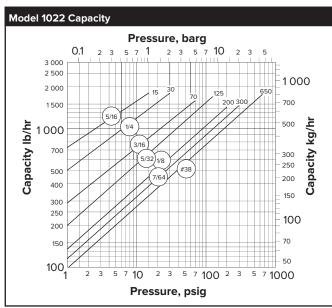
All Stainless Steel for Vertical Installation

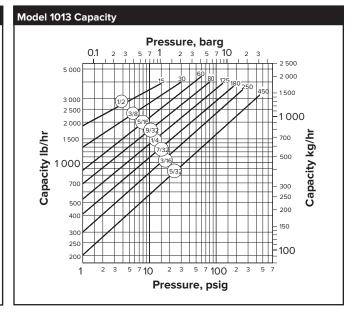
For Pressures to 650 psig (45 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)





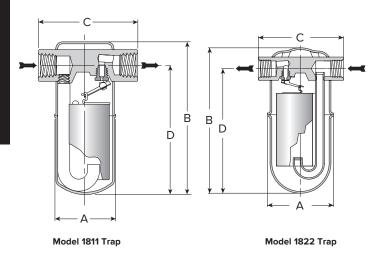






All Stainless Steel for Horizontal Installation

For Pressures to 650 psig (45 barg)...Capacities to 1 802 lb/hr (817 kg/hr)





Description

A quick and easy "in-line" replacement for other types of side inlet/side outlet traps, the Armstrong 1800 Series brings together all the benefits of energy-efficient inverted bucket operation. Side inlet/outlet all-welded construction means an inverted bucket trap that will operate efficiently on applications such as tracer lines, drips, heating, processing and similar applications.

With the 1800 Series you get freeze-resistant, all-stainless steel construction, with a three-year guarantee, plus all the benefits of inverted bucket operation:

Long, trouble-free service life

- Excellent purging action
- Continuous air venting
- · Ease and flexibility of in-line installation

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model 1810, 1811: 400 psig @ 800°F (28 barg @ 427°C)
Model 1822: 650 psig @ 600°F (45 barg @ 315°C)
627 psig @ 700°F (43 barg @ 371°C)
604 psig @ 800°F (41.6 barg @ 427°C)

Maximum operating pressure:

 Model 1810:
 200 psig (14 barg)

 Model 1811:
 400 psig (28 barg)

 Model 1822:
 650 psig (45 barg)

Connections

Screwed NPT and BSPT Socketweld Flanged (consult factory)

Materials

Body: ASTM A240 Grade 304L Internals: All stainless steel—304

Valve and seat: Stainless steel—17-4PH or Titanium

Options

- Insu-Pak[™] insulation for Models 1810/1811
- Stainless steel pop drain for Models 1811/1822
- Probe connection for Models 1811/1822
- · Restricted orifice
- Wiggle wire
- 316 stainless steel valve and seat

Specification

Inverted bucket steam trap, type ... in all stainless steel, freeze resistant, without gaskets, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and orifice at the top of the trap.

How to Order

Specify:

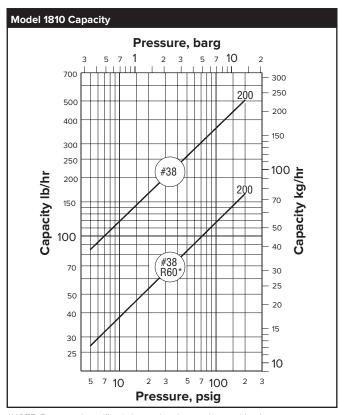
- Model number
- Size and type of pipe connection
- $\bullet\,$ Maximum working pressure that will be encountered or orifice size
- · Any options required

1800 Series Traps											
Model No.	18	1810 1811 1822									
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	
	3/8, 1/2	10, 15	1/2	15	3/4	20	1/2, 3/4	15, 20	1	25	
"A" (Diameter)	2-11/16	68	2-11/16	68	2-11/16	68	3-7/8	99	3-7/8	99	
"B" (Height)	5-5/16	135	6-5/16	160	6-9/16	167	8-1/2	218	8-1/2	218	
"C" (Face to Face)	4-5/16	110	4-5/16	110	4-5/16	110	5	127	5	127	
"D" (Bottom to Q Inlet)	4-7/16	113	5-7/16	138	5-9/16	141	7-3/8	187	7-1/8	181	
Weight lb (kg)	1-3/4	1-3/4 (0.8) 2 (0.9) 2-3/8 (1.1) 7 (3)				(3)					

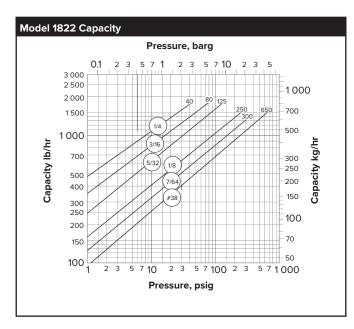
All Stainless Steel for Horizontal Installation

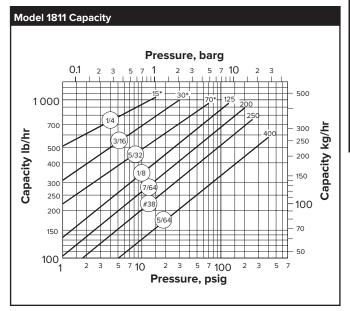
For Pressures to 650 psig (45 barg)...Capacities to 1802 lb/hr (817 kg/hr)





*NOTE: Because the orifice is located at the top, inverted bucket steam traps handle dirt and scale better than other types of traps. However, in applications where extremely dirty conditions exist, care should be exercised in the use of all types of restricted-orifice, reduced-capacity traps.



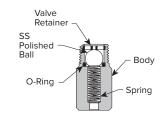


*Orifices available only with 3/4" connections.

Options

Pop Drain for Freeze Protection

In general, a properly selected and installed Armstrong trap will not freeze as long as steam is coming to the trap. If the steam supply is shut off, a pop drain should be used to automatically drain the trap. Stainless steel pop drain available for Models 1811 and 1822.



Maximum Operating Conditions

Pressure: 600 psig (41 barg) Temperature: 350°F (177°C)

nsu-Pak™

Now you can insulate the in-line traps in your plant without complicating regular trap maintenance. Insu-Pak, a simple reusable insulation package, cuts the time and cost of in-field installation because it goes on in a snap. And it comes off just as easily. Insu-Pak can prevent trap freezeup when used with a properly designed condensate manifold. Designed for use with Model 1810 and Model 1811 traps.

Probe connections are available for trap monitoring on Models 1811 and 1822.





All Stainless Steel With 360° Connector/IS-2/TVS-4000

For Pressures to 650 psig (45 barg)...Capacities to 1300 lb/hr (590 kg/hr)

Description

With the 2000 Series' 360° universal connector, you can install inverted bucket efficiency and long service life in any piping configuration with little or no repiping. You get the reliability of the inverted bucket operating principle, plus all the benefits of all-stainless steel construction:

- A sealed, tamperproof package
- · A compact, lightweight trap
- · The ability to withstand freeze-ups without damage
- · Exceptional corrosion resistance
- A three-year guarantee against defective materials, defective workmanship.

2000 Series steam traps combine savings in three important areas: energy, installation and replacement. The 360° universal connector provides quick, easy in-line replacement along with all the proven advantages of inverted bucket operation.

Also available with optional IS-2 integral strainer connector.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model 2010, 2011: 400 psig @ 800°F (28 barg @ 427°C) Model 2022: 650 psig @ 600°F (45 barg @ 315°C)

627 psig @ 700°F (43 barg @ 371°C) 600 psig @ 800°F (41 barg @ 427°C)

Maximum operating pressure:

 Model 2010:
 200 psig (14 barg)

 Model 2011:
 400 psig (28 barg)

 Model 2022:
 650 psig (45 barg)

Connections

Screwed NPT and BSPT Socketweld Flanged (consult factory)

Materials

Body: ASTM-A 240 Grade 304L
Internals: All stainless steel—304
Valve and seat: Stainless steel—17-4PH or Titanium
Connector body (std & IS-2): Stainless steel—304
Flange ASTM A105 Zinc plated

Options

- Insu-Pak[™] insulation for Models 2010/2011
- Stainless steel pop drain for Models 2011/2022
- Probe connection for Models 2011/2022
- · Strainer blowdown valve for IS-2 connector
- · Wiggle wire
- 316 stainless steel valve and seat

360° Connector Styles

- · Standard connector
- IS-2 connector with integral strainer
- IS-2 connector with integral strainer with blowdown valve

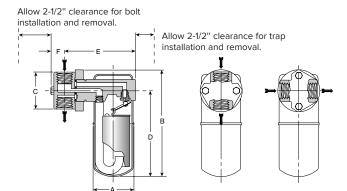
Specification

Inverted bucket steam trap, type ... in all stainless steel, freeze resistant, with 360° universal connector, having continuous air venting at steam temperature, free-floating stainless steel mechanism, and orifice at the top of the trap.

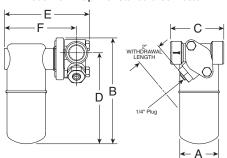
How to Order

Specify:

- Model number
- Size and type of pipe connection
- Type of 360° connector (with or without strainer)
- Maximum working pressure that will be encountered or orifice size
- · Any options required



Model 2011 Trap With Standard Connector



Series 2010-2022 With IS-2 Connector

Model No.	Model No. 2010				2022						
2000 Series Traps With Standard Connector											
	in	mm	in	mm	in	mm					
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20	3/8, 1/2, 3/4	10, 15, 20	3/8, 1/2, 3/4	10, 15, 20					
"A" (Diameter)	2-11/16	68	2-11/16	68	3-7/8	98					
"B" (Height)	6	152	6-15/16	176	8-11/16	221					
"C" (Face to Face)	2-3/8	60	2-3/8	60	2-3/8	60					
"D" (Bottom to Q)	4-19/32	117	5-9/16	141	7-3/8	187					
"E" (டு to Outside)	4-9/16	115	4-9/16	115	5-3/4	146					
"F" (Ç to Bolt)	1	25	1	25	1	25					
Weight lb (kg)	4-1/4 (1.9) 4-1/2 (2.0)			7 (3)							

Model No.		20	10		2011				2022			
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20	1	25
"A" (Diameter)	2-11/16	68	2-11/16	68	2-11/16	68	2-11/16	68	3-7/8	98	3-7/8	98
"B" (Height)*	6	152	6	152	6-15/16	176	6-15/16	176	8-11/16	221	8-11/16	221
"C" (Face to Face)	3-1/2	89	4	102	3-1/2	89	4	102	3-1/2	89	4	102
"D" (Bottom to ℚ)*	5	127	5	127	6	152	6	152	7-3/4	197	7-3/4	197
"E" (Outside to Bolt)	5-1/2	140	5-11/16	144	5-1/2	140	5-11/16	144	6-11/16	170	6-7/8	175
"F" (Ç to Outside)	4-5/8	117	4-13/16	122	4-5/8	117	4-13/16	122	5-13/16	148	6	152
Weight Ib (kg)	4-3/4	(2.2)	5-1/4	(2.4)	5 (2	2.3)	5-1/2	(2.5)	7 (3)			•

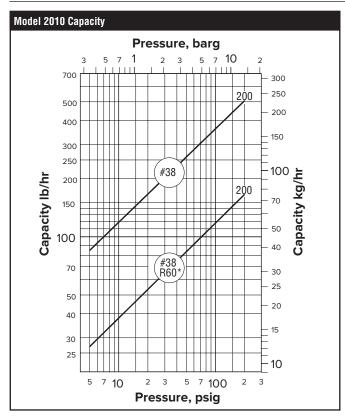
^{*}Add 1/2" (15 mm) to "B" and "D" dimensions when optional probe connection is required.

2000 Series Inverted Bucket Steam Trap

All Stainless Steel With 360° Connector/IS-2/TVS-4000

For Pressures to 650 psig (45 barg)...Capacities to 1 300 lb/hr (590 kg/hr)





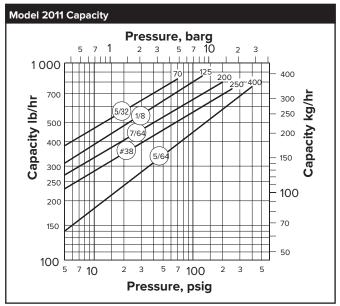
*NOTE: Because the orifice is located at the top, inverted bucket steam traps handle dirt and scale better than other types of traps. However, in applications where extremely dirty conditions exist, care should be exercised in the use of all types of restricted-orifice, reduced-capacity traps.

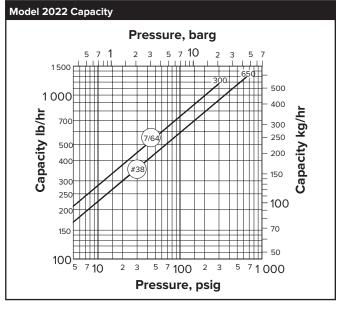
Connectors

Besides the inverted bucket traps, the standard connector, IS-2 connector, and TVS-4000 connector with integral strainer can also be used on thermostatic, thermostatic wafer and disc traps.



CD-3300 Disc Trap With IS-2 Integral Strainer Connector





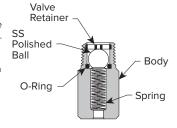
Options

Pop Drain for Freeze Protection

In general, a properly selected and installed Armstrong trap will not freeze as long as steam is coming to the trap. If the steam supply is shut off, a pop drain should be used to automatically drain the trap. Stainless steel pop drain available for Models 2011 and 2022.

Maximum Operating ConditionsPressure: 600 psig (41 barg)

Temperature: 350°F (177°C)



Insu-Pak

Now you can insulate the in-line traps in your plant without complicating regular trap maintenance. Insu-Pak, a simple reusable insulation package, cuts the time and cost of in-field installation because it goes on in a snap. And it comes off just as easily. The Insu-Pak can prevent trap freeze-up when used with a properly designed condensate manifold. Designed for use with Model 2010 and Model 2011 traps.

Probe connections are available for trap monitoring for Models 2011 and 2022.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



4000 Series Inverted Bucket Steam Trap

All Stainless Steel With IS-4 4-Bolt Connector

For Pressures to 650 psig (45 barg)...Capacities to 1 300 lb/hr (590 kg/hr)

Description

With the 4000 Series IS-4 connector, you can install 4-bolt compatible inverted bucket efficiency and long service life in any piping configuration with little or no repiping. You get the reliability of the inverted bucket operating principle, plus all the benefits of all-stainless steel construction:

- · A sealed, tamperproof package
- · A compact, lightweight trap
- · The ability to withstand freeze-ups without damage
- · Exceptional corrosion resistance
- · A three-year guarantee against defective materials, defective workmanship.

4000 Series steam traps combine savings in three important areas: energy, installation and replacement. The 4-bolt connector provides quick, easy in-line replacement along with all the proven advantages of inverted bucket operation.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model IB4011: 400 psig @ 800°F (28 barg @ 427°C)
Model IB4022: 650 psig @ 600°F (45 barg @ 315°C)
627 psig @ 700°F (43 barg @ 371°C)
600 psig @ 800°F (41 barg @ 427°C)

Maximum operating pressure:

Model IB4011: 400 psig (28 barg) Model IB4022: 650 psig (45 barg)

Connections

Screwed NPT Socketweld

Flanged (consult factory)

Materials

Body: ASTM-A 240 Grade 304L Internals: All stainless steel—304

Valve and seat: Stainless steel—17-4PH or Titanium

Connector body: ASTM A351 Gr. CF8M

Options

- Stainless steel pop drain for Models 4011/4022
- Probe connection for Models 4011/4022
- Wiggle wire
- 316 stainless steel valve and seat

Connector Styles

- Standard with strainer
- With strainer blowdown valve
- With block/bleed valves

Specification

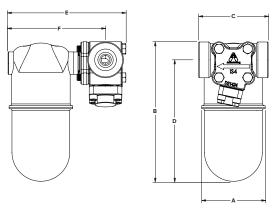
Inverted bucket steam trap, type ... in all stainless steel, freeze resistant, with 360° universal connector, having continuous air venting at steam temperature, free-floating stainless steel mechanism, and orifice at the top of the trap.

How to Order

Specify:

- Model number
- · Size and type of pipe connection
- Maximum working pressure that will be encountered or orifice size
- · Any options required





Model IB4022 Trap With IS-4 Connector

4000 Series Traps With Stand	lard IS-4 Connec	tor								
Model No.		IB4	011		IB4022					
Dina Cannastiana	in	mm in		mm	in mm		in	mm		
Pipe Connections	3/4	20	1	25	3/4	20	1	25		
"A" (Diameter)	2-11/16	68	2-11/16	68	3-7/8	98	3-7/8	98		
"B" (Height)*	6-15/16	176	6-15/16	176	8-11/16	221	8-11/16	221		
"C" (Face to Face)	4-1/4	108	4-1/4	108	4-1/4	108	4-1/4	108		
"D" (Bottom to Ç)*	6	152	6	152	7-3/4	197	7-3/4	197		
"E" (Outside to Bolt)	6-1/8	156	6-1/8	156	7-5/16	186	7-5/16	186		
"F" (Ç to Outside)	4-15/16	125	4-15/16	125	6-1/8	156	6 -1/8	156		
Weight lb (kg)		7-3/4	(3.5)			10-3/-	4 (4.9)			

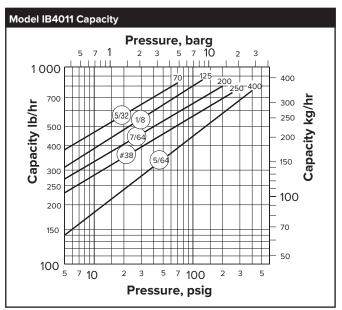
^{*}Add 1/2" (15 mm) to "B" and "D" dimensions when optional probe connection is required.

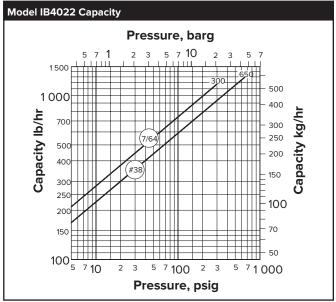
4000 Series Inverted Bucket Steam Trap

All Stainless Steel With IS-4 4-Bolt Connector

For Pressures to 650 psig (45 barg)...Capacities to 1 300 lb/hr (590 kg/hr)



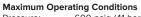




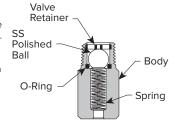
Options

Pop Drain for Freeze Protection

In general, a properly selected and installed Armstrong trap will not freeze as long as steam is coming to the trap. If the steam supply is shut off, a pop drain should be used to automatically drain the trap. Stainless steel pop drain available for Models 4011 and 4022.



Pressure: 600 psig (41 barg) Temperature: 350°F (177°C)





1811N and 2011N Inverted Bucket Steam Trap

All stainless steel, non-metallic seat for tracer service

For pressure to 200 psig (14 barg)... capabilities to 900 lbs/hr (410 kg/hr)

Description

With the 2000N Series' 360° universal connector or the in-line 1800N Series inverted bucket, copper oxide plugging problems can be eliminated. High pressure steam and condensate will dissolve copper tracing without proper amine treatment. The copper in solution precipitates out as copper oxide when it flashes through the steam trap orifice, depositing and eventually plugging the opening. The non-metallic seat eliminates the electrolytic attraction between the dissimilar metals. The copper oxide stays in suspension and flushes away with the condensate return. In addition, you get the reliability and energy efficiency of the inverted bucket design with the benefits of all-stainless steel construction.

- · A sealed, tamperproof package
- · A compact, lightweight trap
- · Ability to withstand freeze-ups without mechanical failure
- · Exceptional corrosion resistance
- A three-year guarantee against defective materials and workmanship

Maximum Operating Conditions

Maximum allowable pressure

Model 1811N 400 psig @ 800°F (28 barg @ 427°C) Model 2011N 400 psig @ 800°F (28 barg @ 427°C)

Maximum operating pressure:

Model 1811N 200 psig @ 450°F (14 barg @ 232°C) Model 2011N 200 psig @ 450°F (14 barg @ 232°C)

Materials

Body: ASTM A240 Grade 304L Internals: All stainless steel
Valve: Stainless steel—17-4PH
Seat: Non-metallic

2011N 360° Universal, 2-bolt, Connector Styles

- Standard 2-bolt connector
- IS-2 connector including integral strainer with optional blowdown valve
- TVS 4000 Trap Valve Station

1811N Connections

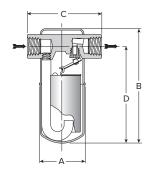
• 1/2" or 3/4", NPT or SW

Specification

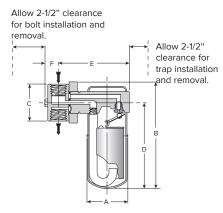
Inverted bucket steam trap. Stainless steel construction, stainless steel valve with non-metallic seats, freeze resistant, continuous air venting.

How to order

- · Specify model
- Select connection size or type of connector
- Maximum working pressure or orifice size



Model 1811N Trap



Model 2011N Trap With Standard Connector

1811N Dimensions and Weight				
Model No.		18	311N	
Dina Cannastiana	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20
"A" (Diameter)	2-11/16	68	2-11/16	68
"B" (Height)	6-5/16	160	6-9/16	167
"C" (Face to Face)	4-5/16	110	4-5/16	110
"D" (Bottom to Q Inlet)	5-7/16	138	5-9/16	141
Weight lb (kg)	2 (0	.9)	2-3/8	(1.1)

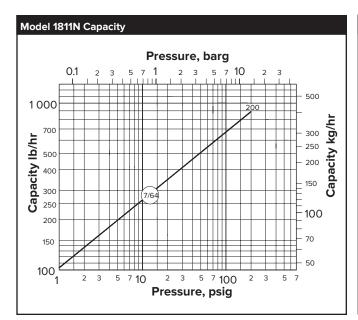
2011N Dimensions and Weight										
Model No.	2011									
Dina Cannactions	in	mm								
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20								
"A" (Diameter)	2-11/16	68								
"B" (Height)	6-15/16	176								
"C" (Face to Face)	2-3/8	60								
"D" (Bottom to Q)	5-9/16	141								
"E" (@ to Outside)	4-9/16	115								
"F" (Ç to Bolt)	1	25								
Weight lb (kg)	4-1/2	(2.0)								

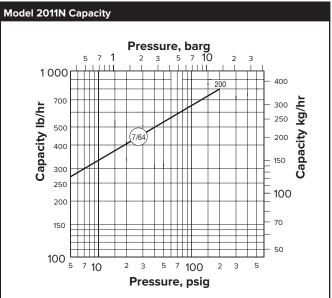
1811N and 2011N Inverted Bucket Steam Trap

All stainless steel, non-metallic seat for tracer service

For pressure to 200 psig (14 barg)... capabilities to 900 lbs/hr (410 kg/hr)

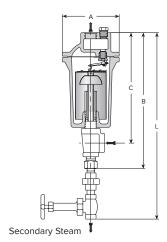








For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)



Description

Armstrong automatic differential condensate controllers (DC) are designed to function on applications where condensate must be lifted from a drain point or in gravity drainage applications where increased velocity will aid in condensate drainage.

When lifting from the drain point, often referred to as syphon drainage, the reduction in pressure that occurs when the condensate is elevated causes a portion of it to flash back into steam.

Ordinary steam traps, unable to differentiate between flash steam and live steam, close and impede drainage. Increased velocity with gravity drainage will aid in drawing the condensate and air to the DC. This increased velocity is caused by an internal steam by-pass, controlled by a manual metering valve, so the condensate controller will automatically vent the by-pass or secondary steam. This is then directed to the condensate return line or collected for use in other heat exchangers.

Maximum Operating Conditions

Maximum allowable pressure

250 psig @ 450°F (17 barg @ 232°C) (vessel design):

Maximum operating pressure: 250 psig (17 barg)



Connections

Screwed NPT and BSPT

Materials

ASTM A48 Class 30 Body: Internals: All stainless steel-304 Valve and seat: Stainless steel—17-4PH Fittings metering valve:

Metering valve—Bronze with stainless steel

trim. Fittings 250# malleable iron

Specification

Automatic differential condensate controller, type ... in cast iron.

How to Order

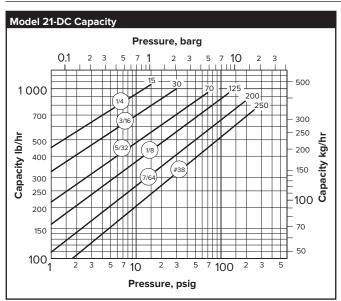
- · Specify model number
- · Specify size and type of pipe connection
- · Specify maximum working pressure that will be encountered or orifice size
- Specify any options required

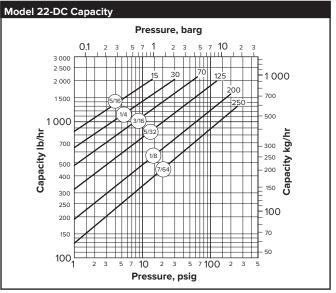
For a fully detailed certified drawing, refer to CD #1008.

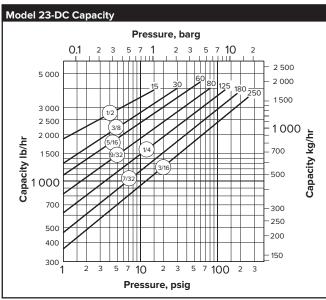
20-DC Series Differential Condensate Controllers													
Model No.	21-	DC	22-	DC	23-	DC	24-	DC	25-	DC	26-	DC	
Inlet & Outlet Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	
illet & Outlet Confections	1/2	15	3/4	20	1	25	1-1/4	32	1-1/2	40	2	50	
Secondary Steam Connection	3/8	10	1/2	15	1/2	15	3/4	20	1	25	1	25	
"A" (Diameter)	4-1/4	108	5-1/4	133	6-3/8	162	7-1/2	190	8-1/2	216	10-3/16	259	
"B" (Height)	9-3/4	248	12-1/4	311	15-1/2	394	18	457	20-1/4	514	23-1/2	597	
"C"	7-3/4	197	9-1/2	241	12-3/4	324	15	381	16-3/4	425	19-3/4	502	
"L"	14-7/8	378	18-1/8	460	21-3/8	543	23-7/8	606	26-3/4	679	31	787	
Weight lb (kg)	7 (3	3.2)	14 (6.4)	24 (10.9)	38 (17.2)	53 (2	24.0)	86 (3	39.0)	

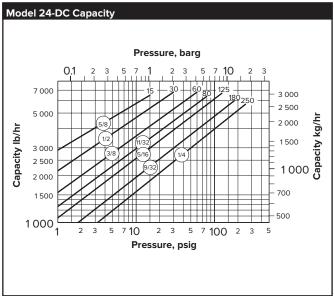
For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

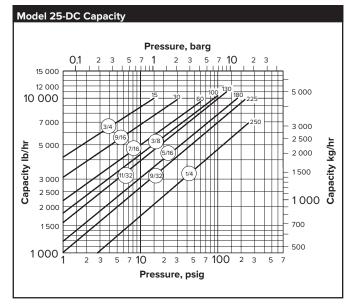


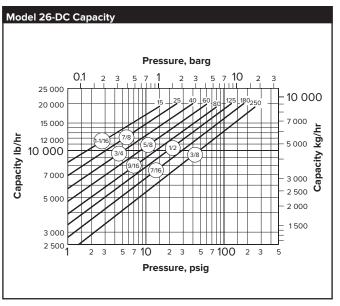








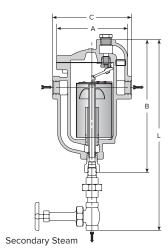




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For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)



Description

Armstrong automatic differential condensate controllers (DC) are designed to function on applications where condensate must be lifted from a drain point or in gravity drainage applications where increased velocity will aid in

When lifting from the drain point, often referred to as syphon drainage, the reduction in pressure that occurs when the condensate is elevated causes a portion of it to flash back into steam.

Ordinary steam traps, unable to differentiate between flash steam and live steam, close and impede drainage. Increased velocity with gravity drainage will aid in drawing the condensate and air to the DC. This increased velocity is caused by an internal steam by-pass, controlled by a manual metering valve, so the condensate controller will automatically vent the by-pass or secondary steam. This is then directed to the condensate return line or collected for use in other heat exchangers.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

250 psig @ 450°F (17 barg @ 232°C) Maximum operating pressure: 250 psig (17 barg)



Connections

Screwed NPT and BSPT

Materials

Body: ASTM A48 Class 30 Internals: All stainless steel-304 Valve and seat: Stainless steel-17-4PH

Fittings metering valve: Metering valve—Bronze with stainless steel

trim. Fittings 250# malleable iron.

Specification

Automatic differential condensate controller, type ... in cast iron.

How to Order

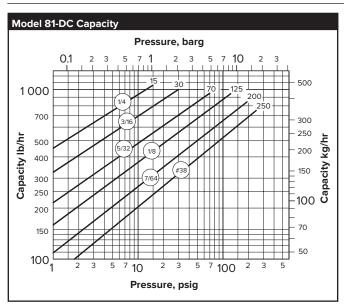
- · Specify model number
- · Specify size and type of pipe connection
- · Specify maximum working pressure that will be encountered or orifice size
- · Specify any options required

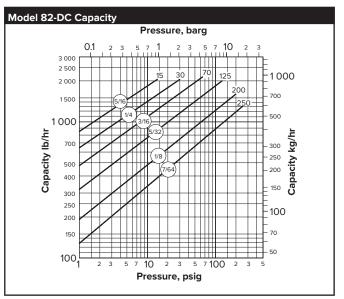
For a fully detailed certified drawing, refer to CD #1008.

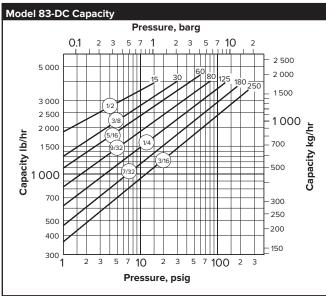
80-DC Series Differential Co	30-DC Series Differential Condensate Controllers													
Model No.	81-	DC	82-	DC	83-	DC	84-	DC	85-DC		86-DC			
Inlet & Outlet Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm		
	3/4	20	3/4	20	1	25	1-1/4	32	1-1/2, 2	50	2	50		
Secondary Steam Conn.	3/8	10	1/2	15	1/2	15	3/4	20	1	25	1-1/2	40		
"A" (Diameter)	3-3/4	95	5-5/8	143	7	178	8	203	9	229	11-1/2	292		
"B" (Height)	8	203	10-1/2	267	13	330	15	381	17-1/2	445	23	584		
"C"	5	127	16-5/8	422	7-3/4	197	9	229	10-1/4	260	13	330		
"L"	13-1/4	337	17-1/2	445	18-3/4	476	21-3/4	552	24	610	32	813		
Weight lb (kg)	7-1/2	(3.4)	17-1/2	2 (7.9)	30-1/2	2 (13.7)	47 (21.3)	75 (34)	139	(63)		

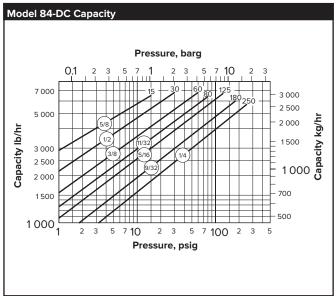
For Pressures to 250 psig (17 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

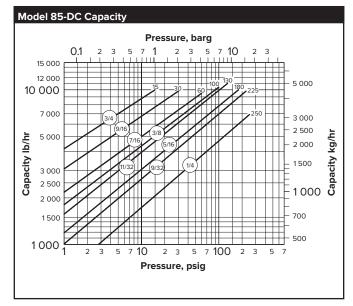


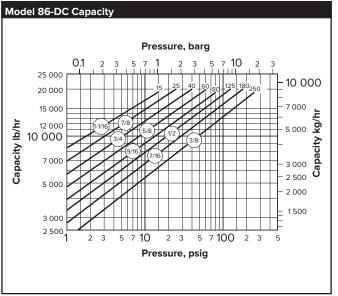






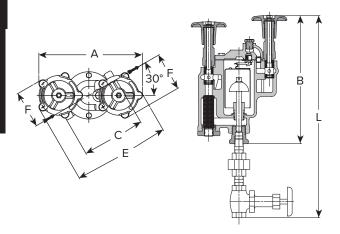


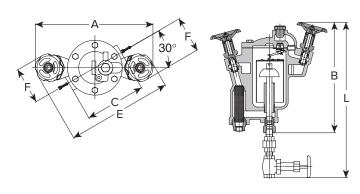




Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)





TVS 81-DC

TVS 82-DC & TVS 83-DC

Description

Armstrong automatic differential condensate controllers (DC) are designed to function on applications where condensate must be lifted from a drain point or in gravity drainage applications where increased velocity will aid in condensate drainage.

When lifting from the drain point, often referred to as syphon drainage, the reduction in pressure that occurs when the condensate is elevated causes a portion of it to flash back into steam.

Ordinary steam traps, unable to differentiate between flash steam and live steam, close and impede drainage. Increased velocity with gravity drainage will aid in drawing the condensate and air to the DC. This increased velocity is caused by an internal steam by-pass, controlled by a manual metering valve, so the condensate controller will automatically vent the by-pass or secondary steam. This is then directed to the condensate return line or collected for use in other heat exchangers.

Maximum Operating Conditions

Maximum allowable pressure

(vessel design):

250 psig @ 450°F (17 barg @ 232°C)

Maximum operating pressure: 250 psig (17 barg)

Connections

Screwed NPT and BSPT

Materials

Body: ASTM A48 Class 30
Internals: All stainless steel—304
Valve and seat: Stainless steel—17-4PH

Fittings metering valve: Metering valve—Bronze with stainless steel

trim. Fittings 250# malleable iron.

Handwheel: Ductile iron TVS 80 Series

Piston valve internals: Stainless steel and graphite

Specification

Automatic differential condensate controller, type TVS in cast iron complete with integral piston valves on the inlet, and outlet with strainer.

How to Order

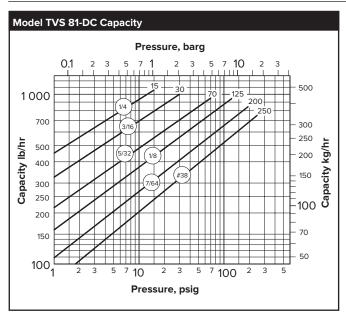
- · Specify model number
- · Specify size and type of pipe connection
- · Specify maximum working pressure that will be encountered or orifice size
- Specify any options required

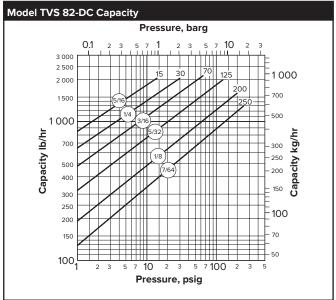
For a fully detailed certified drawing, refer to: TVS 81-DC CD #1088
TVS 82-DC and TVS 83-DC CD #1089

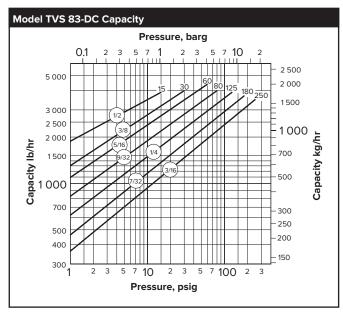
TVS 80-DC Series							
Model No.	TVS 8	B1-DC	TVS 8	2-DC	TVS 83-DC		
Inlet & Outlet Connections	in	mm	in	mm	in	mm	
Innet & Outlet Connections	1/2, 3/4	15, 20	1/2, 3/4	15, 20	3/4, 1	20, 25	
Secondary Steam Connections	3/8	9	1/2	15	1/2	15	
Test Plug	1/4	6	1/2	15	3/4	20	
"A" Width Across Handwheels	8-1/4	210	13-3/4	349	15-1/8	384	
"B" Outlet Valve Open	11	279	12-5/8	320	15-1/8	384	
"C" Face to Face	5	127	6-1/2	165	7-3/4	197	
"E"	7-5/8	194	13	330	14-3/8	365	
"F"	3	76	4-1/2	114	4-7/8	124	
"L"	16-3/4	425	18-3/8	467	20-3/4	527	
Number of Bolts	6	6	6	6	6	6	
Weight lb (kg)	13-1/2	6	27-1/2	12.5	50	23	
Maximum Allowable Pressure (Vessel Design)		250	psig @ 450°F	(17 barg @ 23	32°C)		
Maximum Operating Pressure psig (barg) 250 (17)							

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)











For Pressures to 650 psig (45 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)

Description

Armstrong automatic differential condensate controllers (DC) are designed to function on applications where condensate must be lifted from a drain point or in gravity drainage applications where increased velocity will aid in condensate drainage.

When lifting from the drain point, often referred to as syphon drainage, the reduction in pressure that occurs when the condensate is elevated causes a portion of it to flash back into steam.

Ordinary steam traps, unable to differentiate between flash steam and live steam, close and impede drainage. Increased velocity with gravity drainage will aid in drawing the condensate and air to the DC. This increased velocity is caused by an internal steam by-pass, controlled by a manual metering valve, so the condensate controller will automatically vent the by-pass or secondary steam. This is then directed to the condensate return line or collected for use in other heat exchangers.

Connections

Screwed NPT and BSPT

Materials

Body: ASTM A105

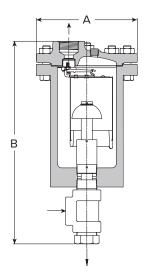
Internals: All stainless steel—304
Valve and seat: Stainless steel—17-4PH
Fittings: 3000# Carbon steel

Specification

Automatic differential condensate controller, type ... in carbon steel.

How to Order

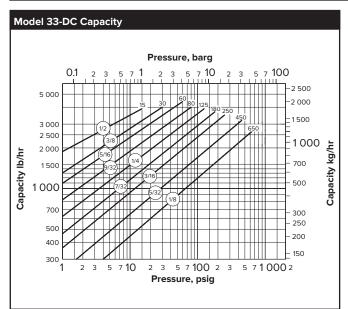
- · Specify model number
- · Specify size and type of pipe connection
- Specify maximum working pressure that will be encountered or orifice size
- · Specify any options required

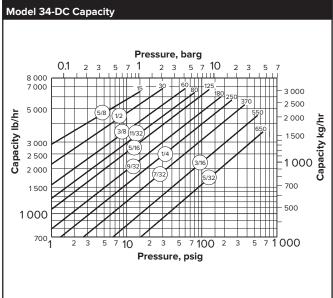


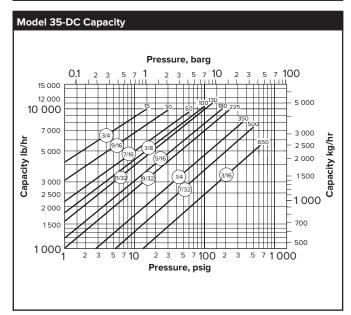
Model No.	33-	DC	34	-DC	35-	DC	36	-DC		
lates a Country Course of the sec	in	mm	in	mm	in	mm	in	mm		
Inlet & Outlet Connections	1	25	1-1/4	32	1-1/2	40	2	50		
Secondary Steam Conn.	1/2	15	3/4	20	1	25	1	25		
"A" (Diameter)	8	203	8-5/8	219	9-3/4	248	11-7/8	302		
"B" (Height)	16-9/16	420	19-1/4	489	21-7/16	544	23-7/8	607		
Weight lb (kg)	53 ((24)	73	(33)	102	(46)	184	(83)		
Maximum Operating Pressure, Sat. Steam, psig (barg)		650 (44)								
Maximum Allowable Pressure (Vessel Design)							g @ 650°F @ 343°C)			

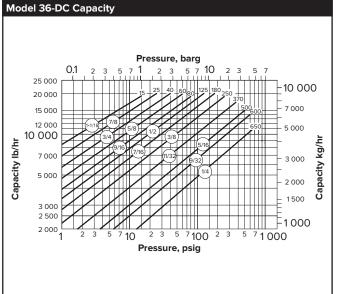
For Pressures to 650 psig (45 barg)...Capacities to 20 000 lb/hr (9 072 kg/hr)













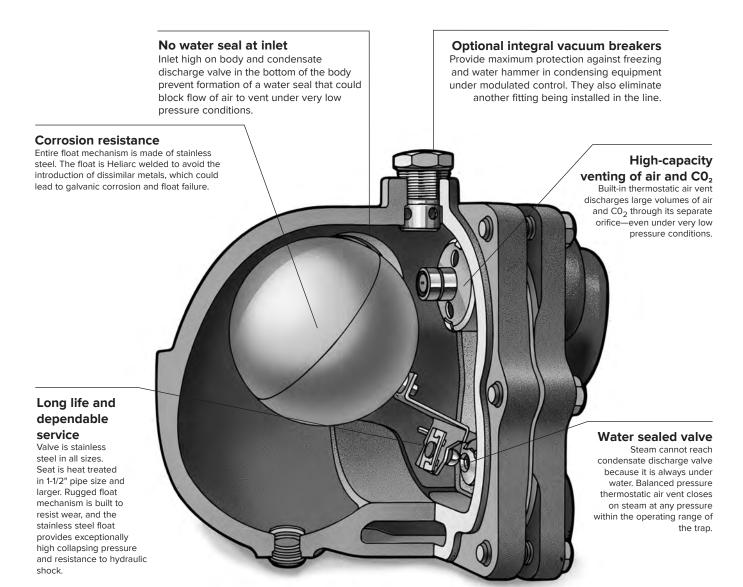
Float & Thermostatic Steam Trap

The More Your Steam Pressure Varies, the More You Need Armstrong F&T Traps

When steam pressure may vary from maximum steam supply pressure to vacuum, Armstrong F&Ts are your most energy-efficient choice. Our line of F&Ts brings Armstrong performance, dependability and long life to trapping services requiring continuous drainage with high air venting capacity. Thanks to separate orifices for condensate and air, they provide continuous condensate drainage and air venting—even

under conditions of zero pressure.

All the benefits detailed below have been designed into Armstrong F&Ts through long experience in the manufacture of pressure float-type drain traps. They assure you of optimum operating efficiency for long periods with minimum trouble.



Operation against back pressure

Trap operation is governed solely by the condensate level in the trap. Back pressure in the return line will not render the trap inoperative as long as there is any pressure differential to force condensate through the discharge valve.

Continuous drainage

No pressure fluctuations due to intermittent condensate drainage. Condensate is discharged at very close to steam temperature. No priming needed.

Float & Thermostatic Steam Trap



Built as Tough as the Jobs They Do

Armstrong float and thermostatic traps are unique in their super heavy duty construction. Armstrong uses high quality ASTM A48 Class 30 cast iron or ASTM A216 WCB cast steel—normally found in pressure vessels rated to 250 psig or 465 psig. Internal mechanisms are made from stainless steel and are heavily reinforced. No brass cotter pins here. Valves and seats are stainless steel, hardened, ground and lapped to withstand the erosive forces of flashing condensate.

Why go to all this trouble on traps normally recommended for low-pressure, modulating service? The answer is in the word modulating. Modulating pressures mean widely varying loads, thermal cycling and high air and non-condensable gas loads.

In other words, tough service. Inferior, lightweight construction is a mistake waiting to happen. Trap failures on modulating pressure may lead to water hammer, corrosion and even heat exchanger damage.

Armstrong's published capacities are based on actual measurements of traps handling hot, flashing condensate. Competitive F&Ts may utilize theoretical calculated capacities. Armstrong uses its own steam lab to give you actual capacity—especially important on high-capacity traps such as those in our ultra-capacity line. Not only does Armstrong offer super heavy duty construction for long life and reliability, but we also supply the data to back up performance. Here's a simple, easy-to-remember summary: The more your pressure varies, the more you need Armstrong F&Ts.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



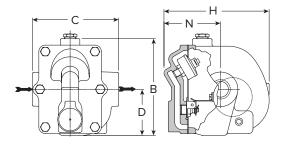
B and BI Series Float & Thermostatic Steam Trap

Cast Iron for Horizontal Installation, With Thermostatic Air Vent

For Pressures From Vacuum to 30 psig (2 barg)...Capacities to 8 900 lb/hr (4 037 kg/hr)

Alternate Inlet

Drain Plug



Model BI Traps

Description

Armstrong B and BI Series F&T traps combine high standards of performance and long life with economy for heating service where continuous drainage with high air-venting capacity is required.

Model B Traps

Because of the wide use of vacuum returns in systems of this type, the thermostatic air vent element is charged to give it the capability of compensated response to the pressure-temperature curve of steam at any pressure from less than 20" (500 mm) Hg vacuum to 30 psig (2 barg) gauge. B and BI Series F&T traps will vent air at slightly below steam temperature throughout this entire range of operation.

All B Series traps, except the 1/2" (15 mm) and 3/4" (20 mm), have inlet connections on both sides of the body to provide flexibility in piping. The BI Series F&T traps in sizes 1/2", 3/4" and 1" feature the convenience of in-line connections with the same internals as the B Series.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model B2-B3: 125 psig @ 353°F (8.5 barg @ 178°C) Model B4-B8: 175 psig @ 377°F (12 barg @ 191°C)

Maximum operating pressure:

15B, Bl:15 psig (1 barg) saturated steam30B, Bl:30 psig (2 barg) saturated steam

NOTE: Cast iron traps should not be used in systems where excessive hydraulic or thermal shock are present.

Connections

Screwed NPT and BSPT

Materials

Body and cap: ASTM A48 Class 30
Internals: All stainless steel—304
Valve: Stainless steel—303 or 17-4PH
Seat: Stainless steel—303 (ASTM A582)
Stainless steel—17-4PH in 1-1/2" and 2"
Thermostatic air vent: Stainless steel and bronze with phosphor

Options

Integral vacuum breaker. Add suffix VB to model number.

CAUTION: Do not use a conventional vacuum breaker open to the atmosphere in any system that incorporates a mechanical return system that carries pressure less than atmospheric pressure. This includes all return systems designated as vacuum returns, variable vacuum returns or subatmospheric returns. If a vacuum breaker must be installed in such a system, it should be of the type that is loaded to open only when the vacuum reaches a calibrated level well in excess of the design characteristics of the system.

Specification

Float and thermostatic steam trap, type ... in cast iron, with thermostatic air vent.

How to Order

Pressure	Model	Connection Size	Option
15	В	2	VB
15 30	B = Standard Connection	*2 = 1/2" *3 = 3/4" 4 = 1" 5 = 1-1/4" 6 = 1-1/2" 8 = 2"	VB = Vacuum Breaker
	BI = In-line Connection	2 = 1/2" 3 = 3/4" 4 = 1"	

^{*}No alternate inlet available.

B and BI Series Traps											,	
Trap Series		B Model									BI Model	
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4	15, 20	1	25	1-1/4	32	1-1/2	40	2	50	1/2, 3/4, 1	15, 20, 25
"B" (Height)	4-7/8	124	5-1/2	140	5-1/2	140	7-7/16	189	9-5/8	244	5-5/8	143
"C" (Face to Face)	3-7/8	98	4-7/8	124	4-5/8	117	5-3/4	146	7-5/8	194	5	127
"D" (Bottom to Q)	7/8	22.2	1	25.4	1-7/32	31.0	1-7/16	36.5	1-11/16	42.9	2-11/16	68
"H" (Width)	5-3/8	137	6	152	7-3/4	197	8-7/16	214	11-5/8	295	6-5/8	168
"K" (Connection Offset)	1/8	3.2	3/8	9.5	_	_	_	_	_	_	_	_
"M" (Ç to Ç)	2-3/4	69.8	3	76.2	3	76.2	4-3/16	106	6	152	_	_
"N" (Top to Q)	2-9/16	65.1	3	76.2	3-3/8	85.7	3-3/4	95.2	5	127	3-9/32	83
Weight Ib (kg)	6 (2	2.7)	8-1/2	(3.9)	11 (5	5.0)	19 (8.6)	40 ('	18.1)	9-3/4	(4.4)

NOTE: Cast iron traps should not be used in systems where excessive hydraulic or thermal shock are present.

bronze bellows, caged in stainless steel

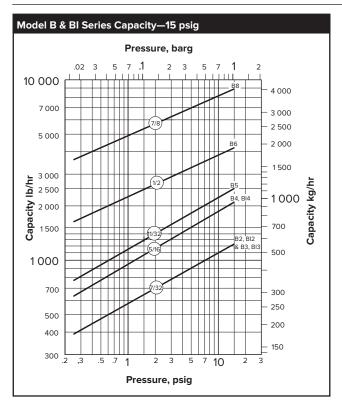
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

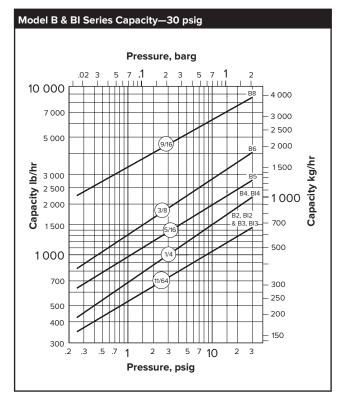
B and **BI** Series Float & Thermostatic Steam Trap

Cast Iron for Horizontal Installation, With Thermostatic Air Vent

For Pressures From Vacuum to 30 psig (2 barg)...Capacities to 8 900 lb/hr (4 037 kg/hr)







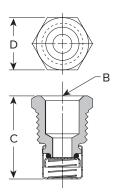
Options

Vacuum Breakers 3/8" (10 mm) and 1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in condensing equipment under modulated control, vacuum breakers are recommended. Armstrong B and BI Series F&T traps are available with integral vacuum breakers. Maximum pressure is 150 psig (10 barg).

Vacuum Breakers										
Size	in	mm	in	mm						
Size	1/2 NPT	15 3/8	NPT	10						
"B" Pipe Connections	3/8 NPT	10	1/4 NPT	6						
"C" Height	1-1/4	32	1-3/32	28						
"D" Width	7/8 Hex	22 Hex	11/16 Hex	17 Hex						



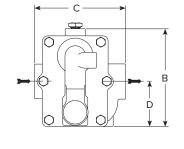


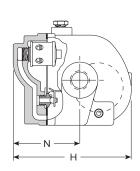
A & Al Series Float & Thermostatic Steam Trap

Cast Iron for Horizontal Installation, With Thermostatic Air Vent

For Pressures to 175 psig (12 barg)...Capacities to 8 600 lb/hr (3 900 kg/hr)

Alternate Inlet 2 Drain Plug





Model A Traps

Model Al Traps

Description

Armstrong A & Al Series F&T traps are for industrial service from 0 to 175 psig and feature a balanced pressure phosphor-bronze type bellows caged in stainless steel. Armstrong A & Al Series F&T traps are designed for service on heat exchange equipment where there is a need to vent air and noncondensable gases quickly.

The Al Series F&T traps feature the convenience of in-line connections with the same rugged internals found in the A Series.

Maximum Operating Conditions

Maximum allowable pressure (vessel design): 175 psig @ 377°F (12 barg @ 191°C)

Maximum operating pressure:

Model30-A, Al:30 psig (2 barg) saturated steamModel75-A, Al:75 psig (5 barg) saturated steamModel125-A, Al:125 psig (8.5 barg) saturated steamModel175-A, Al:175 psig (12 barg) saturated steam

NOTE: Cast iron traps should not be used in systems where excessive hydraulic or thermal shock are present.

Connections

Screwed NPT and BSPT

Materials

Body and cap: ASTM A48 Class 30 Internals: All stainless steel—304 Valve: Stainless steel—17-4PH

Seat: Stainless steel—303 (ASTM A582)

Stainless steel—17-4PH in 1-1/2" and 2"
Thermostatic air vent: Stainless steel and bronze with phosphor

bronze bellows, caged in stainless steel

Options

Integral vacuum breaker. Add suffix VB to model number.

CAUTION: Do not use a conventional vacuum breaker open to the atmosphere in any system that incorporates a mechanical return system that carries pressure less than atmospheric pressure. This includes all return systems designated as vacuum returns, variable vacuum returns or subatmospheric returns. If a vacuum breaker must be installed in such a system, it should be of the type that is loaded to open only when the vacuum reaches a calibrated level well in excess of the design characteristics of the system.

Specification

Float and thermostatic steam trap, type ... in cast iron, with thermostatic air vent.

How to Order

Pressure	Model	Connection Size	Option
75	Al	2	VB
30 75 125	A = Standard Connection	3 = 3/4" 4 = 1" 5 = 1-1/4" 6 = 1-1/2" 8 = 2"	VB = Vacuum Breaker
175	AI = In-line Connection	2 = 1/2" 3 = 3/4" 4 = 1"	

A & Al Series Traps												
Trap Series					Mode	el A					Model Al	
Dina Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	3/4	20	1	25	1-1/4	32	1-1/2	40	2	50	1/2, 3/4, 1	15, 20, 25
"B" (Height)	5-1/8	130	5-1/8	130	5-13/16	148	7-7/16	189	9-3/4	248	5-1/2	140
"C" (Face to Face)	4-7/8	124	4-7/8	124	4-5/8	117	5-3/4	146	7-5/8	194	5	127
"D" (Bottom to Q)	1	25.4	1	25.4	1-7/32	31.0	1-13/32	35.7	1-11/16	42.9	2-9/16	65.1
"H" (Width)	6-7/16	164	6-7/8	164	8-1/8	206	8-7/16	214	11-5/8	295	6-1/2	165
"K" (Connection Offset)	3/8	95.2	3/8	95.2	_	_	_	_	_	_	_	_
"М" (Ç to Ç)	3	76.2	3	76.2	3	76.2	4-3/16	106	6	152	_	_
"N" (Top to ℚ)	3-3/8	85.7	3-3/8	85.7	3-3/4	95.2	3-3/4	95.2	5	127	3-11/16	93.7
Weight lb (kg)	9-1/2	(4.3)	8-1/4	(3.7)	11 (!	5.0)	18-3/4	(8.5)	40 (18.1)	9-3/	4 (4.4)

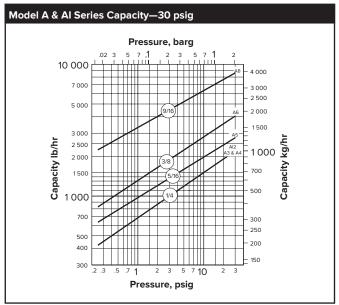
NOTE: Cast iron traps should not be used in systems where excessive hydraulic or thermal shock are present.

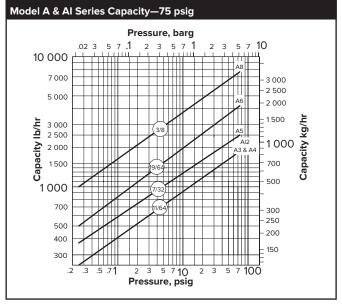
A & Al Series Float & Thermostatic Steam Trap

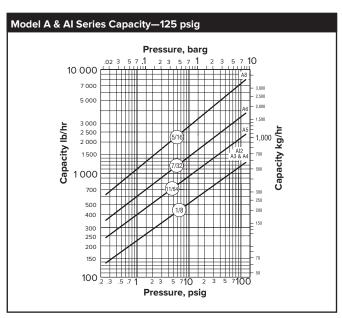
Cast Iron for Horizontal Installation, With Thermostatic Air Vent

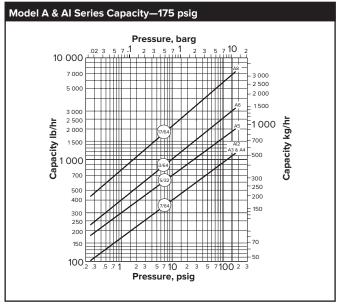
For Pressures to 175 psig (12 barg)...Capacities to 8 600 lb/hr (3 900 kg/hr)











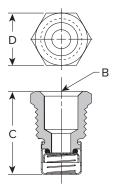
Options

Vacuum Breaker-3/8" (10 mm) and 1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in condensing equipment under modulated control, vacuum breakers are recommended. Armstrong A and Al Series F&T Traps are available with integral vacuum breakers. Maximum service pressure is 150 psig (10 barg).

Vacuum Breaker							
Size	in	mm	in	mm			
Size	1/2 NPT	15	3/8 NPT	10			
"B" Pipe Connections	3/8 NPT	10	1/4 NPT	6			
"C" Height	1-1/4	32	1-3/32	28			
"D" Width	7/8 Hex	22 Hex	11/16 Hex	17 Hex			





AIC Series Float & Thermostatic Steam Trap

Ductile Iron for Horizontal & Vertical Installation with Thermostatic Air Vent

For Pressures to 465 psig (32 barg)...Capacities to 60 075 lb/hr (27 250 kg/hr)



Description

Armstrong AIC Series F&T traps are designed for industrial service up to 465 psig (32 barg). They feature all the benefits of Armstrong F&T traps, such as operation against back pressure, continuous drainage, high-capacity venting of air and $\rm CO_2$, long life and dependable service and enjoys the convenience of in-line connections.

Armstrong AIC Series F&T traps are the perfect solution for applications where there is a need to vent air and non-condensable gases quickly under varying loads.

Maximum Operating Conditions

Maximum allowable pressure (vessel design)*: 580 psig @ 572°F

40 barg @ 300°C
Maximum Allowable Pressure: 580 psig (40 barg)
Maximum Allowable Temperature: 572°F (300°C)
Maximum Operating Pressure: 465 psig (32 barg)

Note: Caution should be used when Float and Thermostatic steam traps are applied in systems where freezing or excessive hydraulic shock can occur.

Connections

Screwed NPT and BSPT Flanged ANSI and DIN

Materials

Body & Cap Ductile Iron

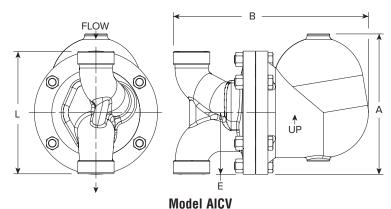
EN1563 EN-GJS-400-18U (ASTM A395)

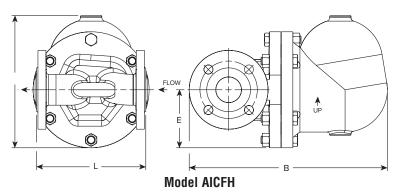
Gasket Graphite

Seat Stainless Steel 17-4PH Internals Stainless Steel Valve Stainless Steel 17-4PH Thermostatic Air Vent Hastelloy Wafer

Options

Integral vacuum breaker (Maximum pressure is 150 psig (10 barg)). Add suffix VB to model number.

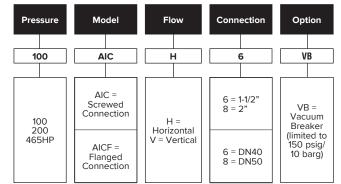




Flow Direction

Right to Left (Horizontal). Top to Bottom (Vertical).

How to Order



Available Connections and Face-To-Face Dimensio		4/0"	1		
Pipe Connections	1 1/2" DN40		2" DN50		
•	in	mm	in	mm	
"A" Height	10-15/16	278	10-15/16	278	
"B" (Length Screwed)	12-27/32	326	13-1/8	333	
"B" (Length Flanged)	16-1/8	410	16-27/64	417	
"L" (Face-to-face Screwed)	10-5/8	270	11-13/16	300	
"L" (Face-to-face Flanged PN40 ANSI CL150)	9-1/16	230	9-1/16	230	
"L" (Face-to-face Flanged ANSI CL300)	9-3/32	231	9-1/4	235	
"E" (Bottom to Q of inlet)	4-13/16	122	4-13/16	122	
Vacuum Breaker (optional)	1/2"	DN15	1/2"	DN15	
Weight screwed lb (kg)	70-1/2	70-1/2 lb (32 kg)		b (32 kg)	
Weight flanged lb (kg)	75 lb (34 kg)		75 lb	(34 kg)	

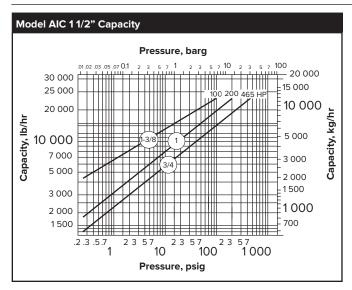
[†] May be derated depending on flange rating and type.

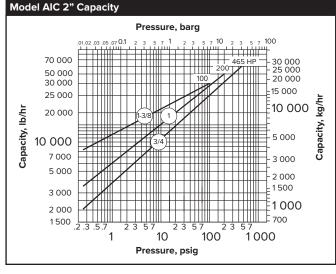
AIC Series Float & Thermostatic Steam Trap

Ductile Iron for Horizontal & Vertical Installation with Thermostatic Air Vent

For Pressures to 465 psig (32 barg)...Capacities to 60 075 lb/hr (27 250 kg/hr)







Options

Vacuum Breaker 1/2" NPT (DN15)

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

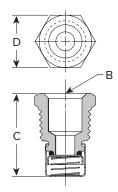
For maximum protection against freezing and water hammer in condensing equipment under modulated control, vacuum breakers are recommended. Armstrong AIC Series F&T Traps are available with integral vacuum breakers. Maximum service pressure is 150 psig (10 barg).

Vacuum Breaker			
Ci	in	mm	Max. allow. pres.
Size	1/2 NPT	DN15	
"B" Pipe Connections	3/8 NPT	DN10	150 psig
"C" Height	1-1/4	32	(10 barg)
"D" Width	7/8 Hex	22 Hex	

CAUTION: Do not use a conventional vacuum breaker open to the atmosphere in any system that incorporates a mechanical return system that carries pressure less than atmospheric pressure. This includes all return systems designated as vacuum returns, variable vacuum returns or subatmospheric returns. If a vacuum breaker must be installed in such a system, it should be of the type that is loaded to open only when the vacuum reaches a calibrated level well in excess of the design characteristics of the system.

Specification

The steam trap shall be an Armstrong model AIC (AICF) float & thermostatic type. Cap and body shall be EN1563 EN-GJS-400-15U (ASTM A395) Ductile Iron. Inline connections shall be integral to the cap as well as the internal mechanism. The valve and seat mechanism and float shall be stainless steel and repairable without disturbing the piping. The thermostatic Air Vent shall be a balanced pressure Hastelloy wafer with chrome steel seat. Maximum allowable back pressure should be 99% of the inlet pressure.





JD & KD Series Ultra-Capacity Float & Thermostatic Steam Trap

Ductile Iron for Horizontal Installation. With Thermostatic Air Vent

For Pressures to 300 psig (21 barg)...Capacities to 142 000 lb/hr (64 400 kg/hr)

Series JD & KD Cap

Series KD, F&T shown

Series JD, F&T shown

Description

The simple, yet rugged, ductile iron construction of the JD & KD Series Ultra-Capacity F&T steam traps offers long, trouble-free service. All floats, valves and seats, and lever mechanisms are constructed of stainless steel.

The integral thermostatic air vent is a balanced-pressure phosphor bronze bellows caged in stainless steel. It is designed especially for heavy-duty industrial applications where highly efficient, uninterrupted service is essential. This balanced-pressure-type air vent will respond to the pressure-temperature curve of steam at any pressure from zero to 300 psig (21 barg). Thus—up to 300 psig (21 barg)—air is vented at slightly below steam temperature.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model JD:	300 psig @ 650°F (21 barg @ 343°C)
Model KD:	300 psig @ 650°F (21 barg @ 343°C)
imum operating pressure:	

Maximum operating pressure: Model 15-JD:

15 psig (1 barg) saturated steam Model 20-JD: 20 psig (1.3 barg) saturated steam Model 30-JD: 30 psig (2 barg) saturated steam Model 75-JD: 75 psig (5.1 barg) saturated steam Model 125-JD: 125 psig (8.6 barg) saturated steam Model 175-JD: 175 psig (12 barg) saturated steam Model 250-JD: 250 psig (17.2 barg) saturated steam Model 300-JD: 300 psig (20.6 barg) saturated steam Model 30-KD: 30 psig (2 barg) saturated steam Model 50-KD: 50 psig (3.4 barg) saturated steam Model 300-KD: 300 psig (20.6 barg) saturated steam

Maximum operating temperature bellows: 422°F (217°C)

Connections

Screwed NPT and BSPT Flanged (screw on)

Materials

Body and cap: ASTM A395 ductile iron Internals: All stainless steel
Valve(s) and seat(s): Stainless steel
Drain plug: Carbon steel

Thermostatic air vent: Stainless steel and bronze with phosphor bronze bellows, caged in stainless steel

Options

- Integral vacuum breaker 150 psig (10 barg) maximum. Add suffix VB to model number
- No internal thermostatic air vent for liquid drainer service. Add suffix LD to model number
- Integral flash release for syphon drainage service. Add suffix CC to model number
- Flanged
- Armored gauge glass 310 psig @ 400°F (21 barg @ 204°C)

Specification

Float and thermostatic steam trap, type ... in ductile iron, with thermostatic air vent.

For a fully detailed certified drawing, refer to CD #1302.

How to Order

Pressure	Model	Connection Size	Option	
75	JD	8	VB	
15				
20				
30			VD Various Breaker	
75	ID	0 2"	VB = Vacuum Breaker	
125	JD	8 = 2"	LD = Liquid Drainer	
175			CC = Condensate Controller	
250			FLG = Specify type and class of flange	
300			GG = Gauge Glass	
30	KD	8 = 2"	OG Gauge Glass	
50	KD	10 = 2-1/2"		
300	KD	10 = 2-1/2", 12 = 3"		

Special Configurations

Condensate controller with flash release for syphon drainage.

The condensate controller (CC) configuration was developed especially to meet very large capacity needs in applications where condensate must be lifted from the drain point to the trap. Under such conditions—often referred to as syphon drainage—the reduction in pressure that occurs when the condensate is elevated causes a portion of the condensate to flash into steam. Ordinary traps, unable to differentiate between flash steam and live steam, close and impede drainage.

The JD & KD Series condensate controllers (CC) are equipped with a fixed, restricted orifice near the top of the body to bleed off the flash steam (and all air present). This permits the trap to function properly on flashing condensate.

Liquid drainer with back vent for exceptionally high-capacity drainage of liquid from gas under pressure. The liquid drainer (LD) configuration was developed to meet very large capacity needs in draining water and other liquids from air or other gases under pressure. To prevent air or gas binding, the access port in the top of the body serves as a back vent connection to the equipment being drained. For capacity data, consult Armstrong International or your Armstrong Representative.

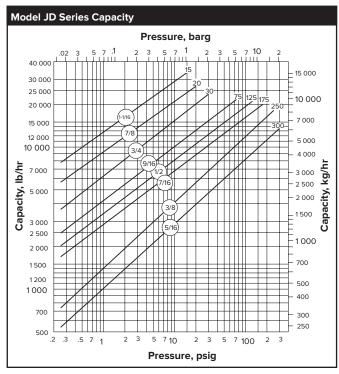
JD and KD Series Traps							
Trap Series	JD		KD				
Dina Canaction	in	mm	in	mm			
Pipe Connection	2	50	2, 2-1/2, 3	50, 65, 80			
"B" (Height)	13-1/16	332	13-1/16	332			
"C" (Width)	9-11/16	246	9-11/16	246			
"D" (Bottom to Q)	2-15/16	75	3-9/16	90			
"H" (Length)	13-11/16	348	14-11/16	373			
"M" (ℚ to ℚ)	6-5/8	168	6	152			
"P" (Trap Top to Bellows Cap Top)	1-13/16	46	1-13/16	46			
"S" (Gauge Glass width)	4-1/2	114	4-1/2	114			
"T" (Gauge Glass height)	8-3/4	222	8-3/4	222			
Weight lb (kg)	80 (3	39)	100 (45)				

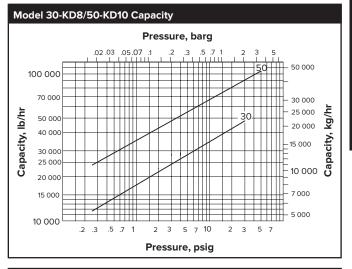
JD & KD Series Ultra-Capacity Float & Thermostatic Steam Trap

Ductile Iron for Horizontal Installation, With Thermostatic Air Vent

For Pressures to 300 psig (21 barg)...Capacities to 142 000 lb/hr (64 400 kg/hr)







Model 300-KD10 Capacity Pressure, barg 23 571 5 710 250 000₁ 100 000 200 000 300 70 000 150 000 kg/hr <u>부</u> 100 000 50 000 30 000 25 000 20 000 15 000 Cabacity, 70 000 50 000 40 000 15 000 30 000 25 000 10 000 20 000 15 000 Pressure, psig

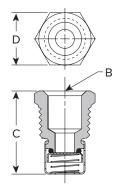
Options

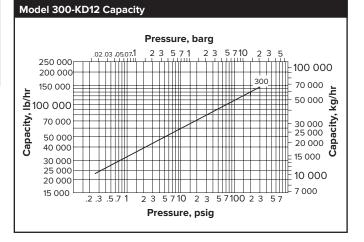
Vacuum Breaker-1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in heating coils under modulated control, for example, vacuum breakers are recommended in conjunction with freeze protection devices.

Vacuum Breaker							
Size	in	mm	Max. allow. pres.				
Size	1/2 NPT	15					
"B" Pipe Connections	3/8 NPT	10	150 psig				
"C" Height	1-1/4	32	(10 barg)				
"D" Width	7/8 Hex	22 Hex					





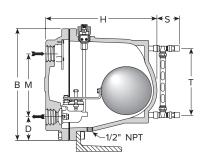


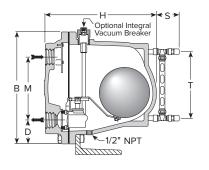
L & M Series Ultra-Capacity Float & Thermostatic Steam Trap

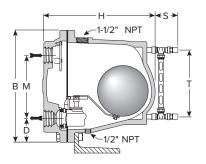
Cast Iron for Horizontal Installation. With Thermostatic Air Vent

For Pressures to 250 psig (17 barg)...Capacities to 208 000 lb/hr (94 348 kg/hr)

For Pressures to 250 psig (17 barg)...Capacities to 208 000 lb/nr (94 348 kg/ni







Series L, F&T shown

Series M, CC shown

Series M. LD shown

Description

The simple vet rugged cast iron construction of the L & M Series Ultra-Capacity F&T steam traps offers long, trouble-free service. All floats, valves and seats, and lever mechanisms are constructed of stainless steel.

The integral thermostatic air vent is a balanced-pressure phosphor bronze bellows caged in stainless steel. It is designed especially for heavy-duty industrial applications where highly efficient, uninterrupted service is essential. This balanced pressure type air vent will respond to the pressure-temperature curve of steam at any pressure from zero to 250 psig (17 barg). Thus—up to 250 psig (17 barg)—air is vented at slightly below steam temperature.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model L: 250 psig @ 450°F (17 barg @ 232°C) Model M: 250 psig @ 450°F (17 barg @ 232°C)

Maximum operating pressure:

Model 30-L:30 psig (2 barg) saturated steamModel 100-L:100 psig (7 barg) saturated steamModel 150-L:150 psig (10 barg) saturated steamModel 250-L:250 psig (17 barg) saturated steamModel 250-M:250 psig (17 barg) saturated steam

Maximum operating temperature bellows: 422°F (217°C)

Connections

Screwed NPT and BSPT Flanged (screw on)

Materials

Body and cap: ASTM A48 Class 30 Internals: All stainless steel—304 Valve(s) and seat(s): Stainless steel

Valve(s) and seat(s): Stainless stee
Drain plug: Carbon steel

Thermostatic air vent: Stainless steel and bronze with phosphor bronze bellows, caged in stainless steel

Options

- Integral vacuum breaker 150 psig (10 barg) maximum. Add suffix VB to model number
- No internal thermostatic air vent for liquid drainer service. Add suffix LD to model number
- Integral flash release for syphon drainage service. Add suffix CC to model number
- Armored gauge glass 310 psig @ 400°F (21 barg @ 204°C)
- · L and M Series available with floor mounting bracket. Consult factory.

Specification

Float & thermostatic steam trap, type ... in cast iron, with thermostatic air vent.

For a fully detailed certified drawing, refer to CD #1010.

How to Order

Pressure	Model	Connection Size	Option
250	M	12	GG
30 100 150 250	L	8 = 2" 10 = 2-1/2"	VB = Vacuum Breaker LD = Liquid Drainer CC = Condensate Controller G/G = Gauge Glass
250	М	12 = 3"	FLG = Specify type and class of flange

Special Configurations

Condensate controller with flash release for syphon drainage and/or cascade service. The condensate controller (CC) configuration was developed especially to meet very large capacity needs in applications where condensate must be lifted from the drain point to the trap. Under such conditions—often referred to as syphon drainage—the reduction in pressure that occurs when condensate is elevated causes a portion of the condensate to flash into steam. Ordinary traps, unable to differentiate between flash steam and live steam, close and impede drainage.

The L & M Series condensate controllers (CC) are equipped with a fixed, restricted orifice near the top of the body to bleed off the flash steam (and all air present). This permits the trap to function properly on condensate.

Liquid drainer with back vent for exceptionally high capacity drainage of liquid from gas under pressure. The liquid drainer (LD) configuration was developed to meet very large capacity needs in draining water and other liquids from air or other gases under pressure. To prevent air or gas binding, the access port in the top of the body serves as a back vent connection to the equipment being drained. For capacity data, see pages 501 and 520 or consult your Armstrong Representative.

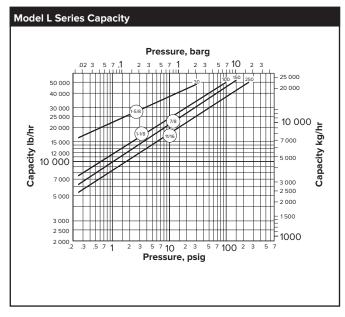
L and M Series Traps					
Trap Series	L	М	L	M	
Pipe Connection	in	1	m	mm	
	2, 2-1/2	3	50, 65	80	
"B" (Height)	20-	20-1/4		514	
"C" (Width)	14-3	14-3/4		375	
"D"(Bottom to Q)	4-3/	4-3/16		106	
"H" (Length)	19-3/4 502)2		
"M" (Ç to Ç)	11-5	11-5/16 23		37	
"S" (Gauge Glass Width)	3-3	3-3/4		5.2	
"T" (Gauge Glass Height)	12	12 305)5	
Weight lb (kg)		196 (88.9)			

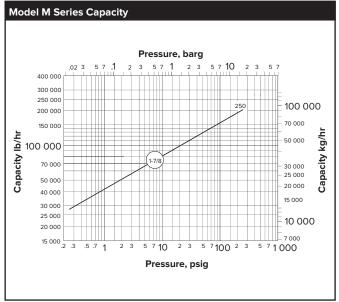
L & M Series Ultra-Capacity Float & Thermostatic Steam Trap

Cast Iron for Horizontal Installation, With Thermostatic Air Vent

For Pressures to 250 psig (17 barg)...Capacities to 208 000 lb/hr (94 348 kg/hr)







Installation Notes

Under conditions where the load may approach the maximum capacity of the trap, it is recommended that the size of the discharge line be increased one size as close to the trap cap as is practical. When L and M Series units are used in severe service conditions or at pressures exceeding 30 psig, use an anchoring bracket or other supportive measures to minimize stress on piping.

Ultra-Capacity L and M Series units MUST BE WARMED UP in the proper sequence and gradually. Recommended warm-up rate—not to exceed 100° F/8 minutes.

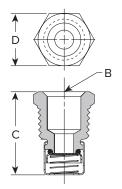
See your Armstrong Representative.

Vacuum Breaker—1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in heating coils under modulated control, for example, vacuum breakers are recommended in conjunction with freeze protection devices.

Vacuum Breaker							
6:	in	mm	Max. allow. pres.				
Size	1/2 NPT	15					
"B" Pipe Connections	3/8 NPT	10	150 psig				
"C" Height	1-1/4	32	(10 barg)				
"D" Width	7/8 Hex	22 Hex					





FT-4000 Series Float and Thermostatic Steam Trap

All Stainless Steel

For Pressures to 465 psig (32 barg)... Capacities to 1080 lb/hr (490 kg/hr)

Description

With the FT-4000 Series, you can install a float and thermostatic trap in any piping configuration with little or no repiping. You get the reliability of the float and thermostatic operating principle, plus all the benefits of all-stainless steel construction

- A sealed, tamperproof package
- · A compact, lightweight trap
- · Exceptional corrosion resistance
- · A one-year guarantee against defective materials and workmanship

FT-4000 Series Float & Thermostatic steam traps combine savings in three important areas: energy, installation and replacement. Mounting the FT-4000 on universal connectors with integral strainers provides quick, easy in-line replacement with added protection from dirt and scale.

Maximum Operating Conditions

Maximum allowable pressure (vessel design): 485 psig @ 600°F (33 barg @ 315°C)

Maximum operating pressure:

Model FT-4075:75 psig (5 barg) saturated steamModel FT-4150:150 psig (10 barg) saturated steamModel FT-4225:225 psig (16 barg) saturated steamModel FT-4300:300 psig (21 barg) saturated steamModel FT-4465:465 psig (32 barg) saturated steam

Materials

Flange

Body: ASTM A240 Grade 304L Internals: All stainless steel—304 Valve and seat: Stainless steel

Thermostatic air vent: Wafer type-stainless steel with

Hastelloy element ASTM A105 Zinc plated

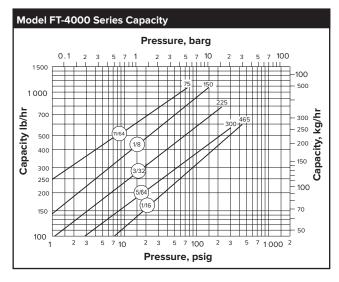
Specification

Steam trap shall be float and thermostatic type having stainless steel construction, stainless steel valve, seat and float, for use on an IS-2 connector with integral strainer or TVS 4000 trap valve station. Integral thermostatic element shall be wafer type constructed of Hastelloy and stainless steel. Thermostatic element shall be capable of withstanding 45°F (25°C) of superheat and be resistant to water hammer damage.

How to order

- · Specify model number
- Select 360° connector style (IS-2 or TVS 4000)
- Specify maximum working pressure that will be encountered or orifice size
- Specify any options required

For a fully detailed certified drawing, refer to CD #1298 and CD #1299.







TVS 4000 Trap Valve Station With FT-4000 Float and Thermostatic Trap



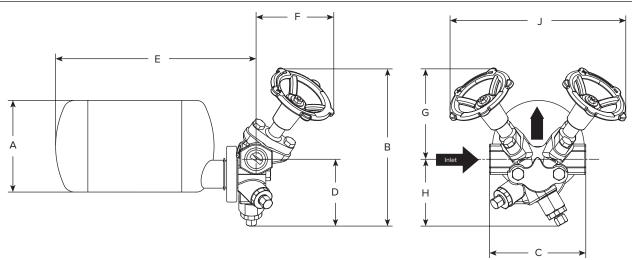
IS-2 Connector With FT-4000 Float and Thermostatic Trap

FT-4000 Series Float and Thermostatic Steam Trap

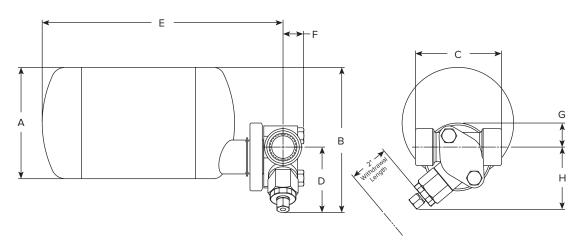
All Stainless Steel

For Pressures to 465 psig (32 barg)... Capacities to 1 080 lb/hr (490 kg/hr)





Series FT-4000 With TVS 4000 Trap Valve Station



Series FT-4000 With IS-2 Connector With Integral Strainer and Optional Blowdown Valve

Trap Series			FT-4	1000		
Madal	IS-2 Connector With Integral Strainer				TVS 4000	Connector
Model	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20
"A" Trap Diameter	4-1/2	114	4-1/2	114	4-1/2	114
"B" Total Height	5-7/8	149	5-7/8	149	7-7/8	198
"C" Face-to-Face	3-1/2	89	4	101	4-3/4	120
"D" Connection Q to Bottom	2-5/8	67	2-5/8	67	3-1/4	83
"E" Connection & to Outside of Trap	10	255	10-1/4	259	9-7/8	250
"F" Connection Q to Front of Connector	7/8	22	7/8	22	3-7/8	98
"G" Connection & to Top	1	25	1	25	4-1/2	114
"H" Connection Q to Bottom of Connector	2-1/2	64	2-1/2	64	3-1/4	83
"J" Width across Handwheels (valve open)		N	/A		8-11/16	221
Test Port Connection		N	/A		1/4 NPT	6
Maximum Operating Pressure (saturated steam)	465 psig (32 barg)					
Maximum Allowable Pressure (vessel design)	485 psig @ 600°F (33 barg @ 315°C)					
Trap Only Weight, lb (kg)	6-1/4 (2.8)					
Trap and Connector Weight, lb (kg)		8-3/	/4 (4)		12-3/4	(5.8)



FF-4000 Series Float and Thermostatic Steam Trap with freely floating ball All Stainless Steel

For Pressures to 250 psig (17 barg)... Capacities to 1 050 lb/hr (476 kg/hr)

Description

With the FF-4000 Series' 360° universal connector, you can install the float and thermostatic trap to fit any piping configuration. You get the reliability of the freely floating ball and thermostatic design plus all the benefits of all-stainless steel construction.

- · A sealed, tamperproof package
- A compact, lightweight trap
- Exceptional corrosion resistance
- A three-year guarantee against defective materials and workmanship

FF-4000 Series Float and Thermostatic steam traps combine savings in three important areas: energy, installation and replacement. Mounting the FF-4000 on universal connectors provide quick and easy in-line replacement.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model FF-4250 270 psig @ 650°F (20.7 barg @ 343°C) Model FF-4450 600 psig @ 800°F (41.4 barg @ 427°C)

Maximum operating pressure:

Model FF-4250 250 psig @ 650°F (17 barg @ 343°C) Model FF-4450 450 psig @ 800°F (31 barg @ 427°C)

Materials

Body: ASTM A240 Grade 304L Internals: All stainless steel-304
Ball seat: Stainless Steel
Float: Stainless Steel
Air Vent: Bimetal

360° Universal Connector Styles

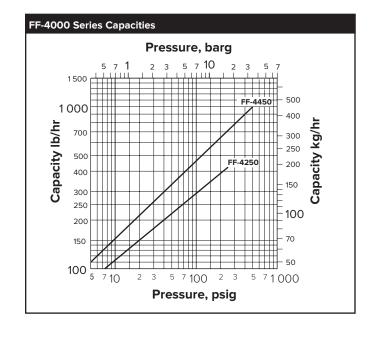
- Standard 2-bolt connector
- IS-2 connector with integral strainer and optional blowdown valve
- Trap Valve Station

How to order

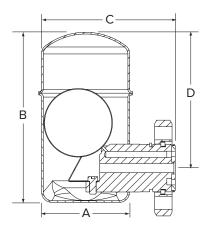
- Specify model number
- Size and type of pipe connection, style of 360° universal connector.



FF-4250 with TVS-4000



FF-4000 Series						
Model No. FF-4250 FF-4450						
Pipe	1/2, 3/4	1/2, 3/4 15, 20		15, 20		
Connection	in	mm	in	mm		
"A" Diameter	2-11/16	68	3-7/8	98		
"B" Height	4-7/8	124	6-3/16	157		
"C" Outside to Flange"D"	3-7/8	98	4-15/16	125		
"D" C Flange to Top	4	102	4-15/16	125		
Trap Only Weight, lb (kg)	2 (0	0.9)	4 (1.8)		



Notes	Armstrong



ICS Series Float & Thermostatic Steam Traps

Carbon Steel for Horizontal or Vertical Installation, With Thermostatic Air Vent

For Pressures to 465 psig (32 barg)... Capacities to 60 000 lb/hr (27 215 kg/hr)

Description

Armstrong ICS Series F&T traps are for industrial service from 0 to 465 psig (32 barg). The simple yet rugged construction of the ICS series carbon steel float and thermostatic trap is designed to assure long, trouble-free service.

Materials

Body: ASTM A352 LCB
Internals: All stainless steel
Valve(s) and Seat(s): Stainless Steel
Thermostatic Air Vent: Wafer type stainless steel

with Hastelloy element

Connections

Flanged Socketweld ASME B16.5 Class 150 - 300

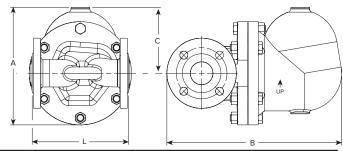
Options

Integral vacuum breaker. Add suffix VB to model number. Condensate controller. Add suffix CC to model number.

Flow			
	in	mm	Flow Direction
Horizontal	1/2, 3/4, 1	15, 20, 25	Left-to-Right
Horizontal	1-1/2, 2	40, 50	Right-to-Left
Vertical	All	All	Down

Note: For vertical applications and dimensions, please consult factory.





Face-to-Face Dimensions - NPT and	Socketwel	d								
Pina Commontions	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1	25	1-1/2	40	2	50
"A" Height	7-11/16	196	7-11/16	196	8-5/16	211	11-5/16	288	11-5/16	288
"B" Length	10-15/16	278	11	279	12-3/8	314	14-3/4	374	14-15/16	380
"C" Cap Q to Top	4-15/16	126	4-15/16	126	5-3/16	131	6-9/16	166	6-9/16	166
"L" Face-to-Face	7-1/4	184	7	178	7-3/8	188	10-1/2	266	10-3/4	273
Weight lb (kg)	21	(10)	21	(10)	28	(13)	76	(35)	76	(35)
Maximum Allowable Pressure (Vessel Design)		580 psig @ 650°F (40 barg @ 343°C)								
Maximum Operating Pressure					465 psia	(32 barg)				

Dia a Cananatiana	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1	25	1-1/2	40	2	50
"A" Height	7-11/16	196	7-11/16	196	8-5/16	211	11-5/16	288	11-5/16	288
"B" Length	11-7/8	301	12-1/16	306	13-9/16	344	15-11/16	399	16-3/16	412
"C" Cap Q to Top	4-15/16	126	4-15/16	126	5-3/16	131	6-9/16	166	6-9/16	166
"L" Face-to-Face	8	203	8-1/16	205	8-3/16	208	12-5/8	321	12-1/4	312
Weight lb (kg)	23	(11)	25	(11)	33	(15)	83	(38)	84 (3	8)
Maximum Allowable Pressure (Vessel Design)				200 psig	@ 400°F (13	.6 barg @ 2	205°C)			
Maximum Operating Pressure					200 psia (13	.6 bara)				

Face-to-Face Dimensions - ASME B	6.5 Class	300#								
Dina Cannastiana	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1	25	1-1/2	40	2	50
"A" Height	7-11/16	196	7-11/16	196	8-5/16	211	11-5/16	288	11-5/16	288
"B" Length	11-15/16	304	12-5/16	314	13-13/16	352	16-5/16	414	16-1/2	419
"C" Cap & to Top	4-15/16	126	4-15/16	126	5-3/16	131	6-9/16	166	6-9/16	166
"L" Face-to-Face	8-1/4	209	8-1/4	209	8-3/8	212	12-7/8	327	12-5/8	320
Weight lb (kg)	24	(11)	26	(12)	35	(16)	88	(40)	88(40)
Maximum Allowable Pressure (Vessel Design)		585 psig @ 500°F (40.4 barg @ 260°C)								
Maximum Operating Pressure					465 psig	(32 barg)				

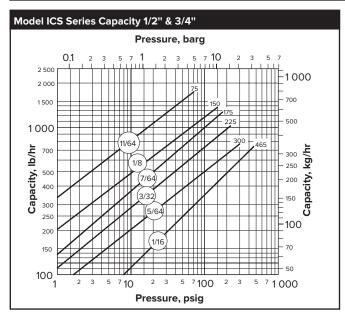
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

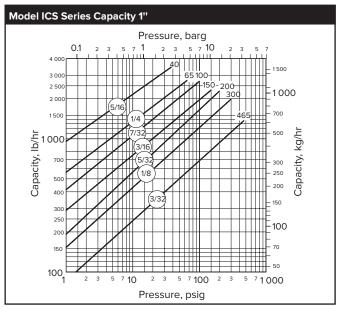
ICS Series Float & Thermostatic Steam Traps

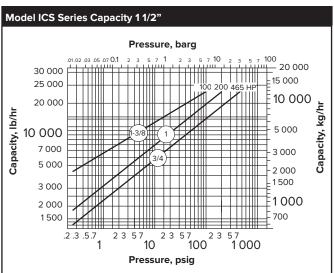
Carbon Steel for Horizontal or Vertical Installation, With Thermostatic Air Vent

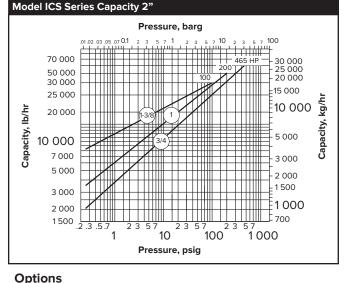
For Pressures to 465 psig (32 barg)... Capacities to 60 000 lb/hr (27 215 kg/hr)

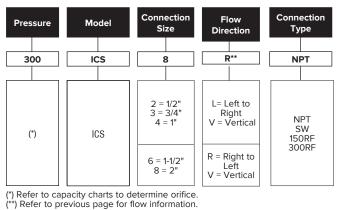












Vacuum Breaker 1/2" NPT (DN15)

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in condensing equipment under modulated control, vacuum breakers are recommended. Armstrong ICS Series F&T Traps are available with integral vacuum breakers. Maximum service pressure is 150 psig (10 barg).

Vacuum Breaker			
Size	in	mm	Max. allow. pres.
Size	1/2 NPT	DN15	
"B" Pipe Connections	3/8 NPT	DN10	150 psig at 366°F
"C" Height	1-1/4	32	(10 barg at 184°C)
"D" Width	7/8 Hex	22 Hex	

CAUTION: Do not use a conventional vacuum breaker open to the atmosphere in any system that incorporates a mechanical return system that carries pressure less than atmospheric pressure. This includes all return systems designated as vacuum returns, variable vacuum returns or subatmospheric returns. If a vacuum breaker must be installed in such a system, it should be of the type that is loaded to open only when the vacuum reaches a calibrated level well in excess of the design

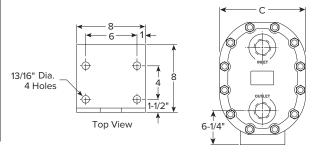
characteristics of the system.



LS & MS Series Ultra-Capacity Float & Thermostatic Steam Trap

Cast Steel for Horizontal Installation, With Thermostatic Air Vent

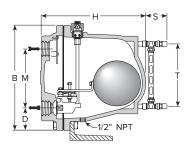
For Pressures to 450 psig (31 barg)...Capacities to 280 000 lb/hr (127 000 kg/hr)



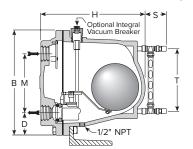
LS and MS Floor Mounting Bracket

LS & MS Series Traps						
Trap Series	LS & MS					
Pipe Connection	in	mm				
Pipe Connection	2, 2-1/2, 3*	50, 65, 80*				
"B" (Height)	20	508				
"C" (Width)	15-1/4	387				
"D" (Bottom to Q)	4-3/16	106				
"H" (Length)	20-1/4	508				
"M" (Ç to Ç)	11-5/16	287				
"S" (Gauge Glass Width)	4-5/8	95.2				
"T" (Gauge Glass Height)	12	305				
Weight lb (kg)	290	(131.5)				

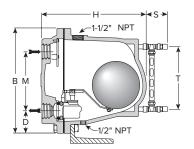
*MS Series 3" (80 mm) only.



Series LS, F&T shown



Series MS, CC shown



Series MS, LD shown

Description

The simple yet rugged cast steel construction of the LS & MS Series Ultra-Capacity F&T steam traps offers long, trouble-free service. All floats, valves and seats, and lever mechanisms are constructed of stainless steel.

The integral thermostatic air vent is a balanced-pressure phosphor bronze bellows caged in stainless steel. It is designed especially for heavy-duty industrial applications where highly efficient, uninterrupted service is essential. This balanced-pressure air vent will respond to the pressure-temperature curve of steam at any pressure from zero to 250 psig (17 barg). Thus—up to 250 psig (17 barg)—air is vented at slightly below steam temperature.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

450 psig @ 650°F (31 barg @ 343°C) Model LS: Model MS 450 psig @ 650°F (31 barg @ 343°C)

Maximum operating pressure:

Model 30-LS: Model 100-LS: 30 psig (2 barg) saturated steam 100 psig (7 barg) saturated steam Model 150-LS: 150 psig (10 barg) saturated steam Model 250-LS 250 psig (17 barg) saturated steam Model 250-MS 250 psig (17 barg) saturated steam Model 450-LS: 450 psig (31 barg) saturated steam Model 450-MS 450 psig (31 barg) saturated steam

Maximum operating temperature bellows: 422°F (217°C)

NOTE: For pressures above 250 psig (17 barg), the thermostatic vent should be removed and only a CC or LD version should be used.

Connections

- Screwed NPT and BSPT
- Socketweld
- Flanged (weld neck)

Materials

Body and cap: ASTM A216 WCB Internals: All stainless steel-304 Valve(s) and seat(s): Stainless steel Drain plug: Carbon steel

Thermostatic air vent: Stainless steel and bronze with phosphor bronze bellows, caged in stainless steel

Options

- Integral vacuum breaker 150 psig (10 barg) maximum. Add suffix VB to
- · No internal thermostatic air vent for liquid drainer service. Add suffix LD to model number.
- · Integral flash release for syphon drainage service. Add suffix CC to model number.
- Armored gauge glass 310 psig @ 400°F (21 barg @ 204°C)
- · LS and MS Series available with floor mounting bracket. Consult factory.

Specification

Float and thermostatic steam trap, type ... in cast steel, with thermostatic

For a fully detailed certified drawing, refer to CD #1010.

How to Order

Pressure	Model	Connection Size	Option			
100	LS	10	VB			
30 100 150 250 450*	LS	8 = 2" 10 = 2-1/2"	VB = Vacuum Breaker LD = Liquid Drainer CC = Condensate Controller G/G = Gauge Glass			
250 450*	MS	12 = 3"	FLG = Specify type and class of flange			

^{*} Orifice only available for CC and LD versions.

Special Configurations

Condensate controller with flash release for syphon drainage and/or cascade service. The condensate controller (CC) configuration was developed especially to meet very large capacity needs in applications where condensate must be lifted from the drain point to the trap. Under such conditions—often referred to as syphon drainage—the reduction in pressure that occurs when condensate is elevated causes a portion of the condensate to flash into steam. Ordinary traps, unable to differentiate between flash steam and live steam, close and impede drainage.

The LS & MS Series condensate controllers (CC) are equipped with a fixed, restricted orifice near the top of the body to bleed off the flash steam (and all air present). This permits the trap to function properly on condensate.

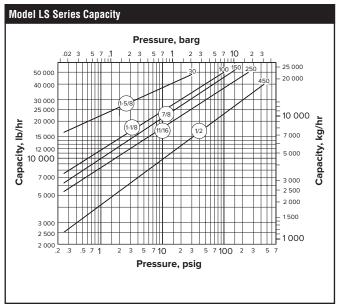
Liquid drainer with back vent for exceptionally high capacity drainage of liquid from gas under pressure. The liquid drainer (LD) configuration was developed to meet very large capacity needs in draining water and other liquids from air or other gases under pressure. To prevent air or gas binding, the access port in the top of the body serves as a back vent connection to the equipment being drained. For capacity data, see pages 501 and 520 or consult your Armstrong Representative.

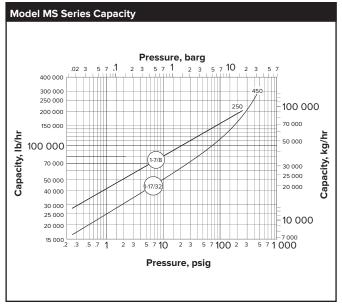
LS & MS Series Ultra-Capacity Float & Thermostatic Steam Trap

Cast Steel for Horizontal Installation, With Thermostatic Air Vent

For Pressures to 450 psig (31 barg)...Capacities to 280 000 lb/hr (127 000 kg/hr)







Installation Notes

Under conditions where the load may approach the maximum capacity of the trap, it is recommended that the size of the discharge line be increased one size as close to the trap cap as is practical.

When LS and MS Series units are used in severe service conditions or at pressures exceeding 30 psig, use an anchoring bracket or other supportive measures to minimize stress on piping.

Ultra-Capacity LS and MS Series units MUST BE WARMED UP in the proper sequence and gradually. Recommended warm-up rate not to exceed 100°F/8 minutes.

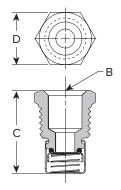
See your Armstrong Representative.

Vacuum Breaker-1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in heating coils under modulated control, for example, vacuum breakers are recommended in conjunction with freeze protection devices.

Vacuum Breaker	Vacuum Breaker								
Size	in	mm	Max. allow. pres.						
Size	1/2 NPT	15							
"B" Pipe Connections	3/8 NPT	10	150 psig						
"C" Height	1-1/4	32	(10 barg)						
"D" Width	7/8 Hex	22 Hex							



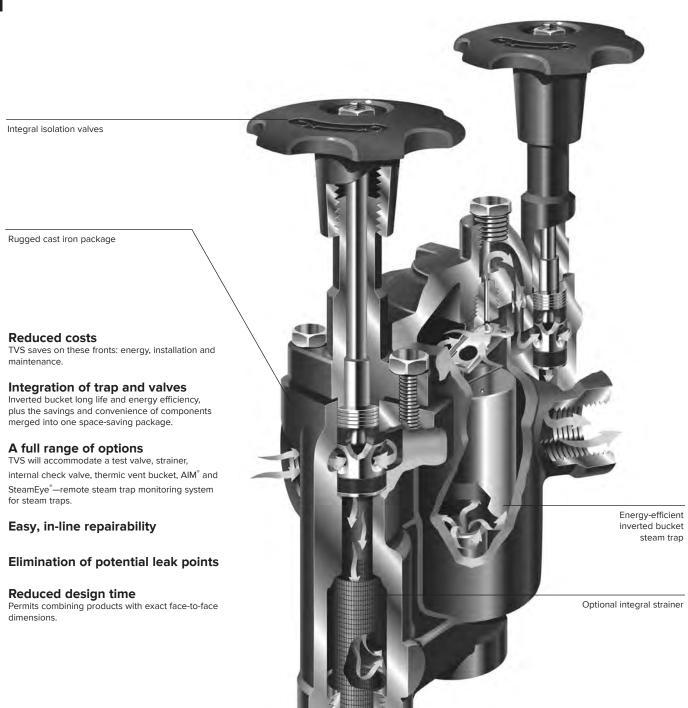
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



TVS 800 Series Cast Iron Trap Valve Station

Put the principle of the inverted bucket to work in a tough cast iron package and you have the best of both worlds—energy efficiency and long-lasting reliability. Add the advantages of valves integrated into one compact trap/valve casting, and you extend the benefits into installation, trap testing and maintenance.

All the components are concentrated in a single, accessible package and can be dealt with in-line. And if you have existing Armstrong cast iron traps in-line, identical face-to-face dimensions will make retrofitting with the patented* Armstrong Trap Valve Station (TVS) a snap. You'll also reduce your inventory requirements. So you'll eliminate what you're paying just to keep parts on hand.

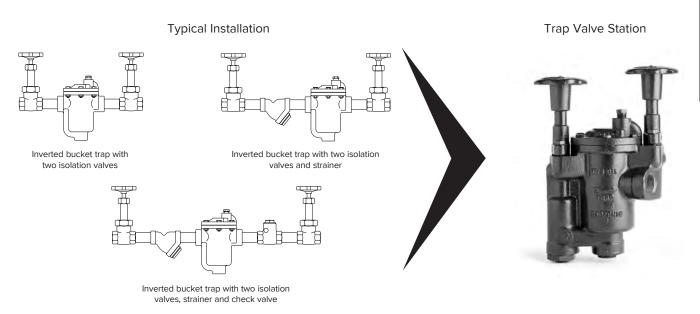


*U.S. Patent 5.947.145

TVS 800 Series Cast Iron Trap Valve Station



TVS makes a long story...short.



The Innovation Is Integration

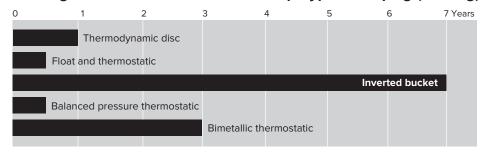
The Armstrong TVS makes what used to be long, complicated steam installation stories simple and compact. It shortens installations by integrating components—specifically an inverted bucket steam trap with two or more valves.

For example, here's an old description for a typical installation: valve-nipple-strainer-nipple-trap-nipple-valve. It's a long tale, even for this simple piping arrangement.

The Trap Valve Station rewrites this steam story: pipe-TVS-pipe. In other words, the TVS makes it all one, delivering the functions of multiple components in a dramatically smaller unit. It integrates two high-value products in a package of revolutionary versatility.

Look above to see how the Armstrong cast iron Trap Valve Station has rewritten these typical steam installations.

Average Service Life for Different Trap Types 200 psig (14 barg)



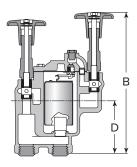
Above data from ICI Engineer January 1993 special issue with permission from ICI Engineering.

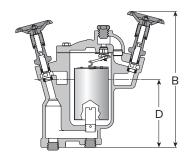


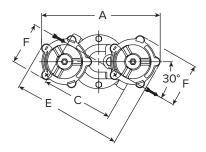
TVS 800 Series Trap Valve Station

Cast Iron for Horizontal Installation, With Integral Piston Valves

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)







Model TVS 811

Series TVS 812/813

Series TVS 811/812/813 - Top View

Same principle. Different package. Now the energy-saving performance and reliability of the inverted bucket steam trap are available in a versatile new package.

You'll still enjoy all the familiar benefits. And the same efficient condensate drainage from virtually every kind of steam-using equipment. But what you'll find new are all the benefits of a piston valve integrated into the same space-saving package.

Maximum Operating Conditions

Maximum allowable pressure

(vessel design): 250 psig @ 450°F (17 barg @ 232°C)

Maximum operating pressure: 250 psig (17 barg)

Connections

Screwed NPT and BSPT

Materials

Cap and body: ASTM A48 Class 30
Internals: All stainless steel—304
Valve and seat: Stainless steel—17-4PH

Handwheel: Ductile iron Internals: Stainless steel

Valve sealing rings: Graphite and stainless steel

Blowdown valve Stainless steel

Options

- Stainless steel internal check valve
- · Thermic vent bucket
- · Stainless steel pop drain
- Integral strainer
- · Scrub wire
- · Probe connection
- · Blowdown valve (TVS 811 and TVS 812 only)

Specification

Inverted bucket steam trap, type ... in cast iron, with continuous air venting at steam temperature, free-floating stainless steel mechanism, and discharge orifice at the top of the trap. Integral upstream and downstream shutoff piston style valves in same dimensional space as standard bucket trap.

How to Order

Specify:

- Model number
- Size and type of pipe connection
- · Maximum working pressure that will be encountered or orifice size
- · Any options required

For a fully detailed certified drawing, refer to:

TVS 811 CD #1099 TVS 812/813 CD #1100

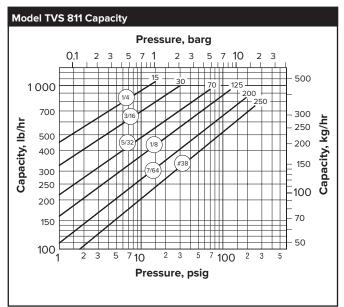
Model No.	TVS	TVS 811			TVS 813	
Dia - Consortion	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4	15, 20	3/4, 1	20, 25
Test Plug	1/4	6	1/2	15	3/4	20
"A" Width Across Handwheels	8-1/4	210	13-3/4	349	15-1/8	384
"B" Outlet Valve Open	10-1/4	260	11-3/4	298	14-1/4	362
"C" Face to Face	5	127	6-1/2	165	7-3/4	197
"D" Connection Q to Bottom	3-11/16	94	4-3/4	121	7-1/4	184
"E"	7-5/8	194	13	330	14-3/8	365
"F"	3	76	4-1/2	114	4-7/8	124
Number of Bolts	6	6	6	6	6	6
Weight lb (kg)	12 (5.4)	25 (1	1.3)	47	(24)

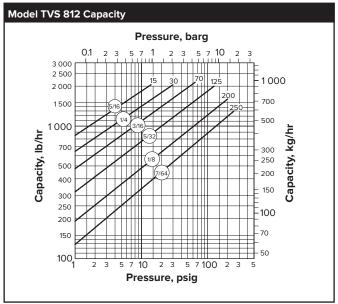
TVS 800 Series Trap Valve Station

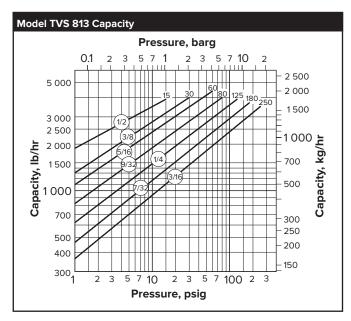
Cast Iron for Horizontal Installation, With Integral Piston Valves

For Pressures to 250 psig (17 barg)...Capacities to 4 400 lb/hr (2 000 kg/hr)









Options

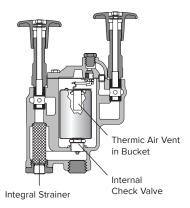
Internal Check Valves are spring-loaded stainless steel and screw directly into the trap inlet or into an extended inlet tube having a pipe coupling at the top to save fittings, labor and money.

Thermic Vent Buckets have a bimetal controlled auxiliary air vent for discharging large amounts of air on start-up.

Integral Strainer is made from 20×20 stainless steel screen.

Probe Connections are available for trap monitoring.

Blowdown Valve for clearing strainers of dirt and debris.

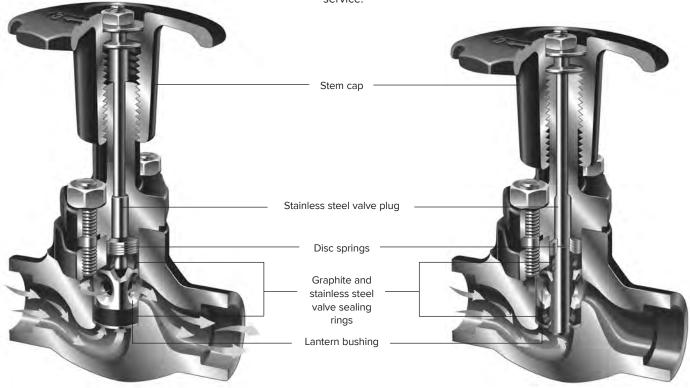




TVS 4000 Series Stainless Steel Trap Valve Station

The Piston Valve

Armstrong Steam Distribution Manifolds (MSD/SMSD) and TVS 4000 Trap Valve Stations incorporate advanced piston sealing technology for safer, longer lasting steam isolation service.



Open Position

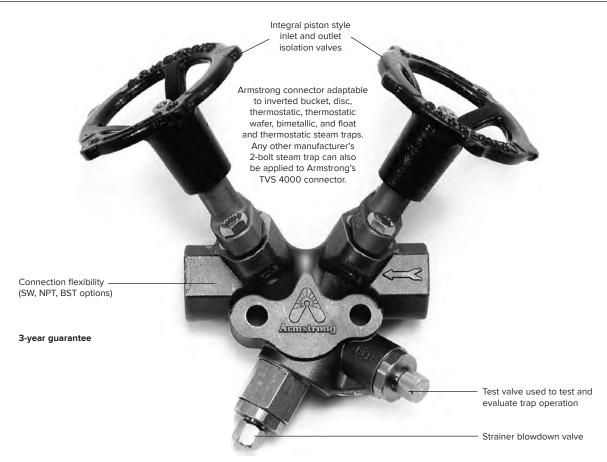
Closed Position

- Dual sealing action. The piston valve is a seatless valve that includes two graphite and stainless steel valve sealing rings that seal the stem and function as a seat. This combination provides long-term protection against leaks to the atmosphere and downstream piping.
- Self-cleaning action. Stainless steel piston slides without rotating between the two valve sealing rings, preventing dirt from damaging the surfaces.
- Sealing integrity. Flexible disc springs automatically provide leak tightness by exerting pressure, which keeps the upper and lower valve sealing rings compressed at all times. Sealing tightness is ensured by the compression of the sealing rings against the piston and valve body. This

- combination of disc springs and dual valve seal rings protects against expansion and contraction due to heating and cooling. This ensures dependable operation, even after years of service.
- Protected valve stem. The valve stem and sealing surfaces are completely protected from dirt and corrosion by the stem cap, whether in an open or closed position.
- In-line repairability. All sealing valve components may be easily replaced in-line.
- Long-term operation. Piston valve design ensures actuation even after many years without operation.

TVS 4000 Series Stainless Steel Trap Valve Station





Description

Same principle. Different package with two piston-style isolation valves, test valve and integral stainless steel strainer with blowdown valve. What you'll find new are all the benefits of a piston valve integrated into the same space-saving package.

Maximum Operating Conditions

Maximum allowable pressure: 830 psig (57.2 barg) @ 800°F (427°C)

Materials—TVS 4000 Connector

Connector: ASTM A351 Gr. CF8M Strainer screen: Stainless steel Test valve: Stainless steel Blowdown valve: Stainless steel

Isolation Valve Components

All wetted parts: Stainless steel

Valve sealing rings: Graphite and stainless steel

Handwheel: Ductile iron

Weight

6-1/2 lb (2.9 kg)

Features

- Reduced costs. TVS saves on these fronts: reduced leak points, installation and maintenance time.
- A full range of features. TVS has test and strainer blowdown valves. When installed with Armstrong Model 2011 and 2022 steam traps, it will also accommodate the Armstrong pop drain as well as AIM® and SteamEye®—remote steam trap monitoring and testing devices.
- Reduced design time. Permits combining products with exact face-to-face dimensions.
- Three-year guarantee. The TVS 4000 is guaranteed for three years.
- Easy, in-line repairability with maximum safety. TVS allows isolation at point of service with upstream/downstream depressurization.
- Installation versatility. The connector design makes the TVS adaptable to any manufacturer's 2-bolt steam trap and piping configuration.
- Simplified trap testing. TVS enhances your capability to check trap operation and offers a built-in method to block and bleed traps.

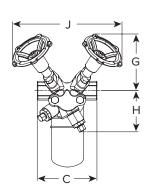
How to Order

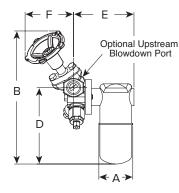
Model	Connection	Type of Connection Inlet/Outlet	Flow Direction	Trap Type
TVS 4000	1/2" 3/4"	NPT SW BSPT Flanged*	R = Right to Left L = Left to Right	Inverted Bucket Disc Thermostatic wafer Bimetallic Float and Thermostatic

*Consult factory.
U.S. Patent 6,467,503

TVS 4000 Series Stainless Steel Trap Valve Station

For Pressures to 830 psig (57.2 barg)...Capacities to 1300 lb/hr (590 kg/hr) (Using 2000 Series Inverted Bucket Steam Traps)





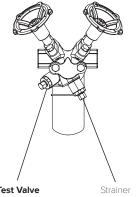
Model TVS 4000 With 2000 Series SS Trap Front View

Model TVS 4000 With 2000 Series SS Trap Side View

Test Valve

Test Port Connection

Model TVS 4000 With 2000 Series SS Trap Bottom View



Test Valve
Used to test and
evaluate trap
operation

Strainer Blowdown Valve

Same principle. Different package with two piston-style isolation valves, test valve and integral stainless steel strainer with blowdown valve. Now the energy-saving performance and reliability of the inverted bucket steam trap are available in a versatile new package. You'll still enjoy all the familiar benefits. And the same efficient condensate drainage from virtually every kind of steam-using equipment. What you'll find new are all the benefits of a piston valve integrated into the same space-saving package.

Materials—TVS 4000 Connector

Connector: ASTM A351 Gr. CF8M
Strainer screen: Stainless steel
Screen retainer: Stainless steel
Gasket: Stainless steel
Retainer unit: Stainless steel
Test valve: Stainless steel
Blowdown valve: Stainless steel

Isolation Valve Components

Handwheel: Ductile iron
Nut: Stainless steel
Stem, washers: Stainless steel
Bonnet: ASTM A351 Gr. CF8M

Bonnet, bolts: DIN 933, Gr. A2 Class 70 per DIN 267

Valve plug: Stainless steel
Disc springs: Stainless steel

Valve sealing rings: Graphite and stainless steel

Lantern bushing: Stainless steel Valve washers: Stainless steel

Materials—Series 2000 Traps

Body: ASTM A240 Gr. 304L Internals: All stainless steel—304 Valve and seat: Stainless steel—17-4PH

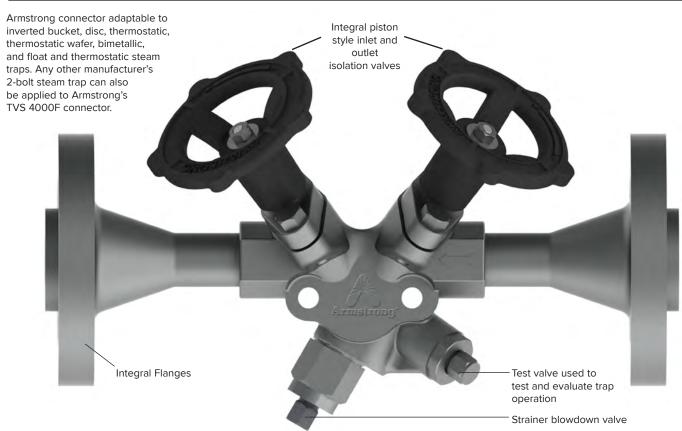
Model No.	20	2010		2011		2022	
Dina Compostions	in	mm	in	mm	in	mm	
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20	1/2, 3/4	15, 20	1/2, 3/4	15, 20	
"A" Trap Diameter	2-11/16	68	2-11/16	68	3-7/8	98	
"B" Height (Valve Open)	8	203	10-1/2	268	12-1/2	318	
"C" Face to Face	4-3/4	120	4-3/4	120	4-3/4	120	
"D" Connection & to Bottom	4-3/4	120	6	154	8	203	
"E" Connection Q to Outside of Trap	4-1/2	114	4-13/16	122	5-7/8	149	
"F" Connection & to Front of Handwheel (Valve Open)	3-1/2	89	3-7/8	98	3-7/8	98	
"G" Connection & to Top of Handwheel (Valve Open)	3-1/4	83	4-1/2	114	4-1/2	114	
"H" Connection & to Bottom of Connector	1-7/8	47	3-1/4	83	3-1/4	83	
"J" Width Across Handwheels (Valve Open)	9-1/4	235	8-3/4	222	8-3/4	222	
Test Port Connection	1/4 NPT	6	1/4 NPT	6	1/4 NPT	6	
Weight lb (kg)	9	4	9-1/2	4.3	12	5.4	
Maximum Operating Pressure (Trap)	200 psig (14 barg) 400 psig (28 barg) 650 psig (4		(45 barg)				
Maximum Operating Conditions (Connector)		830 psig (57.2 barg) @ 800°F (427°C) 1400 psig (96.5 barg) @ 100°F (38°C)					
Maximum Allowable Pressure (Trap)	400	400 psig (28 barg) @ 750°F (399°C) 650 psig @ 600° (45 barg @ 315°C)					

U.S. Patent 6,467,503

TVS 4000F Series Stainless Steel Trap Valve Station

For Pressures to 830 psig (57.2 barg)...Capacities to 1 300 lb/hr (590 kg/hr) (Using 2000 Series Inverted Bucket Steam Traps)





Description

A complete package featuring two piston-style isolation valves, test valve and integral stainless steel strainer with blowdown valve. You'll realize all the benefits of a piston valve integrated into the same space-saving package.

Maximum Operating Conditions

Maximum allowable pressure: 830 psig (57.2 barg) @ 800°F (427°C)

Materials—TVS 4000F Connector

Connector	. ASTM A351 Gr. Cl
Strainer screen	. Stainless steel
Test valve	. Stainless steel
Blowdown valve	. Stainless steel

Isolation Valve Components

All wetted parts	Stainless steel
Valve sealing rings	Graphite and stainless steel
Handwheel	Ductile iron

Weight

14 lb (6.4 kg)

Features

- Reduced costs. TVS saves on these fronts: reduced leak points, installation and maintenance time.
- A full range of features. TVS has test and strainer blowdown valves. When installed with Armstrong Model 2011 and 2022 steam traps, it will also accommodate the Armstrong pop drain as well as TrapAlert and SteamEye —remote steam trap monitoring and testing devices.
- Reduced design time. Permits combining products with exact face-to-face dimensions.
- Three-year guarantee. The TVS 4000F is guaranteed for three years.
- Easy, in-line repairability with maximum safety. TVS allows isolation at point of service with upstream/downstream depressurization.
- Installation versatility. The connector design makes the TVS adaptable to any manufacturer's 2-bolt steam trap and piping configuration.
- Simplified trap testing. TVS enhances your capability to check trap operation and offers a built-in method to block and bleed traps.
- Integral Flanges. The body and connections are of one piece construction, free of welds and other potential leak paths.

How to Order

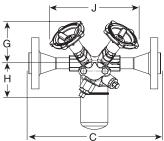
Model	Connection	Type of Connection Inlet/Outlet	Flow Direction	Trap Type
TVS 4000F	3/4"	Flanged ASME B16.5 Class 150, 300, 600	R = Right to Left L = Left to Right	Inverted Bucket • Disc • Thermostatic wafer Bimetallic • Float and Thermostatic
	1"	Flanged ASME B16.5 Class 150, 300		

U.S. Patent 6,467,503



TVS 4000F Series Stainless Steel Trap Valve Station

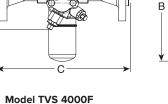
For Pressures to 830 psig (57.2 barg)...Capacities to 1 300 lb/hr (590 kg/hr) (Using 2000 Series Inverted Bucket Steam Traps)

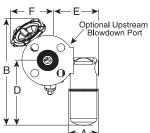


with

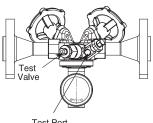
2000 Series SS Trap

Front View



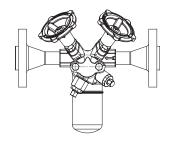


Model TVS 4000F with 2000 Series SS Trap Side View









Strainer Blowdown Valve

Same principle. Different package with two piston-style isolation valves, test valve and integral stainless steel strainer with blowdown valve. Now the energy-saving performance and reliability of the inverted bucket steam trap are available in a versatile new package. You'll still enjoy all the familiar benefits. And the same efficient condensate drainage from virtually every kind of steam-using equipment. What you'll find new are all the benefits of a piston valve integrated into the same space-saving package.

Materials—TVS 4000F Connector

Connector	ASTM A351 Gr. CF8M
Strainer screen	Stainless steel
Screen retainer	Stainless steel
Gasket	Stainless steel
Retainer unit	Stainless steel
Test valve	Stainless steel
Blowdown valve	Stainless steel

Isolation Valve Components

Handwheel	.Ductile iron
Nut	.Stainless steel
Stem, washers	.Stainless steel
Bonnet	.ASTM A351 Gr. CF8M
Bonnet, bolts	.DIN 933, Gr. 8.8 per DIN 267
Valve plug	.Stainless steel
Disc springs	.Stainless steel
Valve sealing rings	.Graphite and stainless steel
Lantern bushing	.Stainless steel
Valve washers	.Stainless steel

Materials—Series 2000 Traps

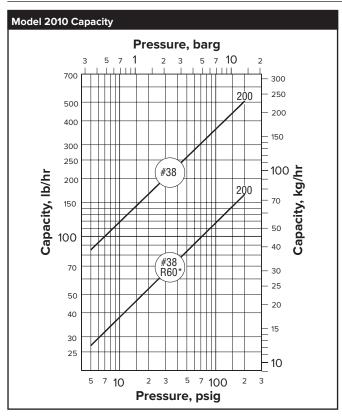
Body	ASTM A240 Gr. 304L
Internals	All stainless steel—304
Valvo and soat	Stainloss stool_17_1DH

Model No.	20	2010		2011		2022	
Dia a Commontinuo	in	mm	in	mm	in	mm	
Pipe Connections	3/4, 1	20, 25	3/4, 1	20, 25	3/4, 1	20, 25	
"A" Trap Diameter	2-11/16	68	2-11/16	68	3-7/8	98	
"B" Height (Valve Open)	8	203	10-1/2	268	12-1/2	318	
"C" Face to Face	12	305	12	305	12	305	
"D" Connection Q to Bottom	4-3/4	120	6	154	8	203	
"E" Connection Q to Outside of Trap	4-1/2	114	4-13/16	122	5-7/8	149	
"F" Connection Q to Front of Handwheel (Valve Open)	3-1/2	89	3-7/8	98	3-7/8	98	
"G" Connection & to Top of Handwheel (Valve Open)	3-1/4	83	4-1/2	114	4-1/2	114	
"H" Connection & to Bottom of Connector	1-7/8	47	3-1/4	83	3-1/4	83	
"J" Width Across Handwheels (Valve Open)	9-1/4	235	8-3/4	222	8-3/4	222	
Test Port Connection	1/4 NPT	6	1/4 NPT	6	1/4 NPT	6	
Weight lb (kg)	16	7.3	16.5	7.5	19	8.6	
Maximum Operating Pressure (Trap)	200 psig (14 barg) 400 psig (28 barg) 650 psig		(45 barg)				
Maximum Operating Conditions (Connector)		830 psig (57.2 barg) @ 800°F (427°C) 1400 psig (96.5 barg) @ 100°F (38°C)					
Maximum Allowable Pressure (Trap)	400	400 psig (28 barg) @ 800°F (427°C) 650 psig @ 600 (45 barg @ 315°			_		

TVS 4000F Series Stainless Steel Trap Valve Station







*NOTE: Because the orifice is located at the top, inverted bucket steam traps handle dirt and scale better than other types of traps. However, in applications where extremely dirty conditions exist, care should be exercised in the use of all types of restricted-orifice, reduced-capacity traps.

Options

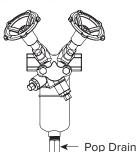
Now you can insulate the in-line traps in your plant without complicating regular trap maintenance. Insu-Pak, a simple reusable insulation package, cuts the time and cost of in-field installation because it goes on in a snap. And it comes off just as easily. The Insu-Pak can prevent trap freeze-up when used with a properly designed condensate manifold. Designed for use with Model 2010 and Model 2011 traps.

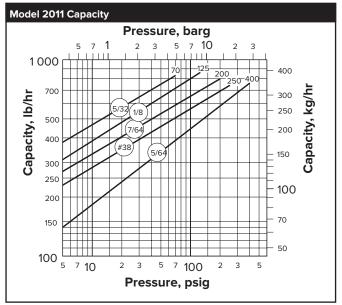
Pop Drain

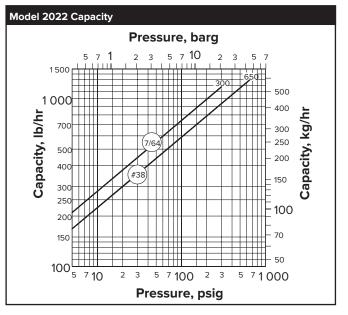
Simple but effective against freeze-up. Properly installed and maintained at low points in your system, the simple, pressure-actuated pop drain opens for condensate drainage at 5 psig (0.35 barg) for Models 2011 and 2022.

Probe Connections are available for trap monitoring on Models 2011 and 2022.









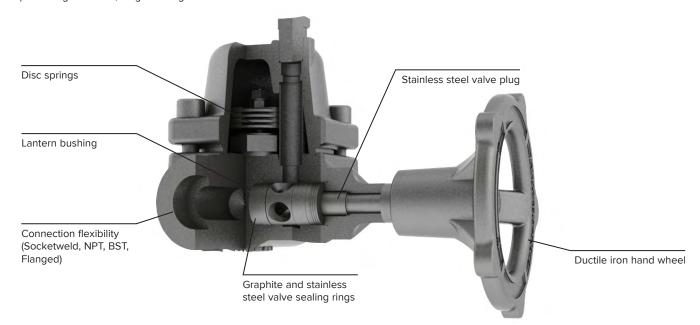
U.S. Patent 6,467,503



TVS 1100 Series Carbon Steel Trap Valve Station

For pressure to 319 psig/22 barg, and cold water capacities to 4 630 lb/hr/2 100 kg/hr

The Armstrong TVS 1100 Series bimetallic steam trap with integral isolation valve incorporates advanced piston sealing technology and a compact design for safer, longer lasting steam isolation service.



- Single valve operation. Eliminates the need for ancillary isolation valve, reducing the number of potential leak points, and providing a compact, space-saving design.
- Dual sealing action. The piston valve is a seatless valve that includes two graphite and stainless steel valve sealing rings that seal the stem and function as a seat. This combination provides long-term protection against leaks to the atmosphere and downstream piping.
- Integral strainer. Eliminates dirt and particulate from steam during operation.
- Bimetallic air vent capsule. Easily removes air and condensate during start-up.
- Sealing Integrity. Flexible disc springs automatically provide leak tightness by exerting pressure, which keeps the upper and lower valve sealing rings compressed at all times. Sealing tightness is ensured by the compression of the sealing rings against the piston and valve body.
- In-line repairability. All sealing valve components may be easily replaced in-line.
- Long-term operation. Piston valve design ensures actuation even after many years without operation.



TVS 1100 Features versus Conventional Designs				
	Armstrong TVS 1100 Series	Conventional Designs		
Design	Compact	Bulky, Multiple Leak Points		
Module Length 6.2" (160 mm)		15.7" (400 mm)		
Module Height	4.01" (102 mm)	6.3" (160 mm)		
No. of Leakage Points	2	4		
Isolation Valve Zero Leakage Piston Valve		Normal Globe/Ball Valve		
Strainer	Standard Feature	Not available - which leads to element failure due to dirt		
Mechanism	Bimetallic/Thermostatic/Thermodynamic	Thermostatic		
Repairable	Yes	No		

TVS 1100 Series Carbon Steel Trap Valve Station

For pressure to 319 psig/22 barg, and cold water capacities to 4 630 lb/hr/2 100 kg/hr



Description

The Armstrong TVS 1100 features an integral piston-style isolation valve, stainless steel strainer and bimetallic steam trap. The space-saving design of the TVS 1100 greatly reduces the number of potential leak points, cuts installation time and expense, and provides years of dependable steam isolation service.

Maximum Operating Conditions

Maximum allowable pressure (Vessel design)
580 psig @ 662°F/40 barg @ 350°C

Maximum operating pressure 319 psig/22 barg

Maximum back pressure 99% of inlet pressure

Materials

Body and cap: ASTM A105

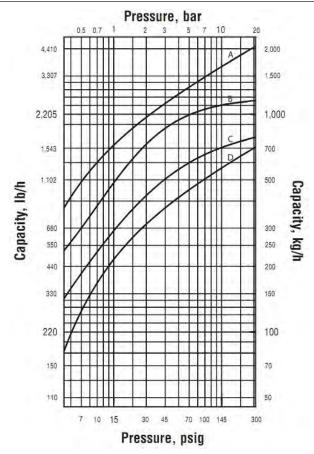
Valve: Stainless steel—17-4PH
Seat: Stainless steel-304
Bimetallic elements: Nickel-plated

Isolation Valve Components

Handwheel Ductile Iron
Nut Stainless steel
Stem, washers; Stainless steel
Bonnet: ASTM A350 Gr LF2
Bonnet, bolts: Carbon steel
Valve plug: Stainless steel
Disc spring: Stainless steel

Valve sealing rings: Graphite and stainless steel

Lantern bushing: Stainless steel
Valve washers: Stainless steel

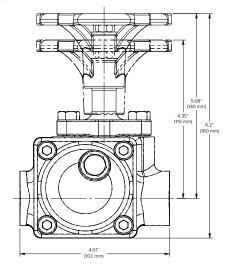


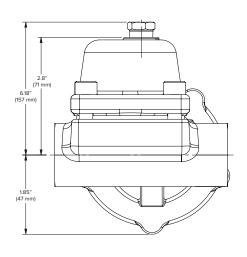
How to Order:

Model	Connection	Type of Connection Inlet/Outlet
TVS 1100	1/2"	NPT
	3/4"	SW
		BSPT
		Flanged*

^{*}Consult factory.

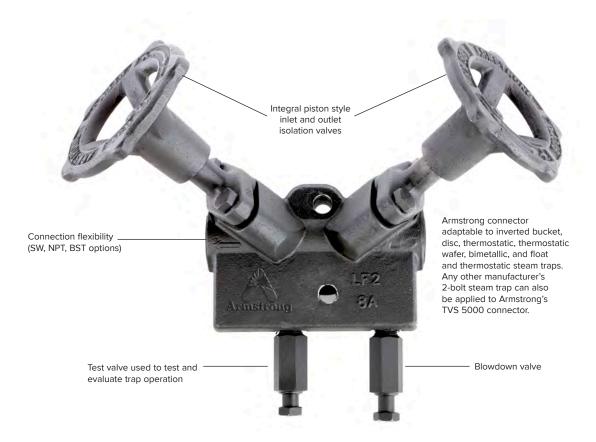
Dimensions:







Armstrong TVS 5000 Trap Valve Station



Description

Armstrong's TVS 5000 is designed as a one piece body equipped with a piston valve(s) combined with a removable steam trap mounted with a connecting flange.

Maximum Operating Conditions

Maximum allowable pressure: 650 psig @ 600°F (45 barg @ 315°C)

Materials—TVS 5000 Connector

Connector: ASTM A350 LF2 Test valve: ASTM A582 T303

Blowdown valve: ASTM A582 T303

Isolation Valve Components

Valve sealing rings: Graphite and stainless steel Bonnet: ASTM A350 LF2

Bolts: DIN 933

Valve plug: ASTM A564

Lantern bushings: ASTM A582 T304
Valve washer: ASTM A582 T304
Disc springs: AISI T301
Nut: AISI T304

Handwheel: Ductile iron A536

Weight

11.71 lb (5.3 kg)

Features

- Reduced costs. TVS saves on these fronts: reduced leak points, installation and maintenance time.
- Reduced design time. Permits combining products with exact face-to-face dimensions.
- Easy, in-line repairability with maximum safety. TVS allows isolation at point of service with upstream/downstream depressurization.
- Simplified trap testing. TVS enhances your capability to check trap
 operation and offers a built-in method to block and bleed traps.

How to Order

Model	Connection	Type of Connection Inlet/Outlet	Flow Direction	Trap Type
TVS 5000	1/2"	NPT	R = Right to Left	Inverted Bucket
	3/4"	SW	L = Left to Right	Disc
		BSPT		Thermostatic wafer
		Flanged*		Bimetallic
				Float and Thermostatic

^{*}Consult factory.

Notes	Armstrong



Armstrong[®] Universal Stainless Steel Connector

IS-2 Stainless Steel Connector with Integral Strainer Provides:

- A full line stainless steel strainer in the connector eliminates leak points and reduces installation time
- · A strainer that is not discarded when the trap is replaced
- · Easy strainer screen replacement
- Optional blowdown valve
- Accommodates Armstrong's inverted bucket, disc, thermostatic, thermostatic wafer, bimetallic, and float and thermostatic traps. Any manufacturer's 2-bolt steam trap can also be applied to Armstrong's IS-2 connector.

Maximum Operating Conditions

Maximum allowable pressure: 830 psig (57.2 barg) @ 800°F (427°C) 1400 psig (96.5 barg) @ 100°F (38°C) Refer to Trap Specifications for further operating conditions.

Connector Styles

- · IS-2 connector with integral strainer
- · IS-2 connector with integral strainer with blowdown valve

Connection Sizes

1/2", 3/4", 1"

Connection Types

Screwed NPT and BSPT Socketweld Flanged (consult factory)

Materials

Connector Body: Strainer:

All stainless steel—304 20 x 20 Mesh 304 stainless steel

Weight

2 lbs (0.91 kg)

How to Order IS-2 Connector with Integral Strainer

Specify:

- · Connection style
- · Connection size
- · Connection type
- · Inlet flow direction
- · Left to Right
- Right to Left



Standard 360° Stainless Steel Connector Provides:

- A compact, lightweight assembly
- Standardization, reducing inventory
 A compact design simplifying piping
- A compact design, simplifying piping
- Accommodates Armstrong's inverted bucket, disc, thermostatic, thermostatic wafer and bimetallic steam traps. Any manufacturer's 2-bolt steam trap can also be applied to Armstrong's standard connector.

Maximum Operating Conditions

Maximum allowable pressure: 830 psig (57.2 barg) @ 800°F (427°C) 1400 psig (96.5 barg) @ 100°F (38°C) Refer to Trap Specifications for further operating conditions.

Connector Styles

• Standard 360°

Connection Sizes

• 3/8", 1/2", 3/4"

Connection Types

Screwed NPT and BSPT Socketweld Flanged (consult factory)

Weight

1-1/2 lbs (0.70 kg)

How to Order Standard 360° Stainless Steel Connector

Specify:

- Connection size
- · Connection type



Universal Stainless Steel Connector - IS-4



Description

With the IS-4 universal connector, you can install a 4-bolt compatible steam trap to fit most piping configurations and applications. The IS-4 combines the integrity of an all welded installation with the versatility of a quick change steam trap replacement.

The IS-4 works with Armstrong Intelligent Monitoring (AlM $^{\text{\tiny M}}$) to bring intelligence to wireless technology by applying smart devices to monitor critical plant applications in real time.

- Class 900 design
- · All stainless steel construction
- · Integral strainer
- · Exceptional corrosion resistance
- Recessed gasket surface
- Three-year guarantee against defects in materials and workmanship (connector only)

Maximum Operating Conditions

Materials and Weights

Body ASTM A351 Gr. CF8M
Screen Stainless steel
Screen retainer ASTM A351 Gr. CF8M
Retainer bolts ASTM A193 Gr. B16

Weights:

IS-4 4.75 lbs (2.15 kg) IS-4BD 9.9 lbs (4.5 kg)

4-Bolt Connector Steam Traps Available

- SH4000 Series
- IB4022
- IB4011

Specification

All stainless steel in-line universal connector with integral strainer able to accept steam traps compatible with the 4-bolt technology. Up to Class 900 service.



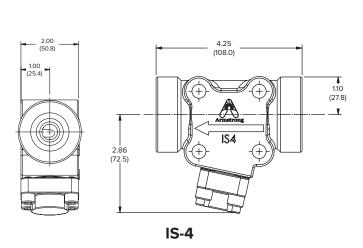
IS-4

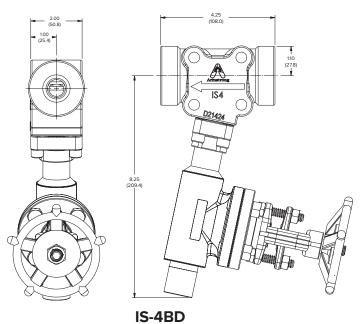
How to order

IS-4	3FL	900	DBB	DBB
Model	Connection Size/Type	Flanges	Inlet Configuration	Outlet Configuration
IS-4 or IS-4BD	3NPT=3/4(20)NPTF 3SW=3/4(20)Socketweld 3FL=3/4(20)Flanged 4NPT=1(25)NPTF 4SW=1(25)Socketweld 4FL=1(25)Flanged	Class 600 Class 900	None SB=Single Block DBB=Double Block & Bleed	None SB=Single Block DBB=Double Block & Bleed

Notes:

- 1. Right to left flow only available.
- 2. IS-4BD includes Class 800 forged steel gate valve for blowdown service.
- Connection Size/Type based on the system condensate supply and return requirements.
- 4. All connections for SB or DBB will be socketweld.
- 5. Flanges available in Class 600 and 900.
- 6. For Block & Bleed dimensions: Consult Factory

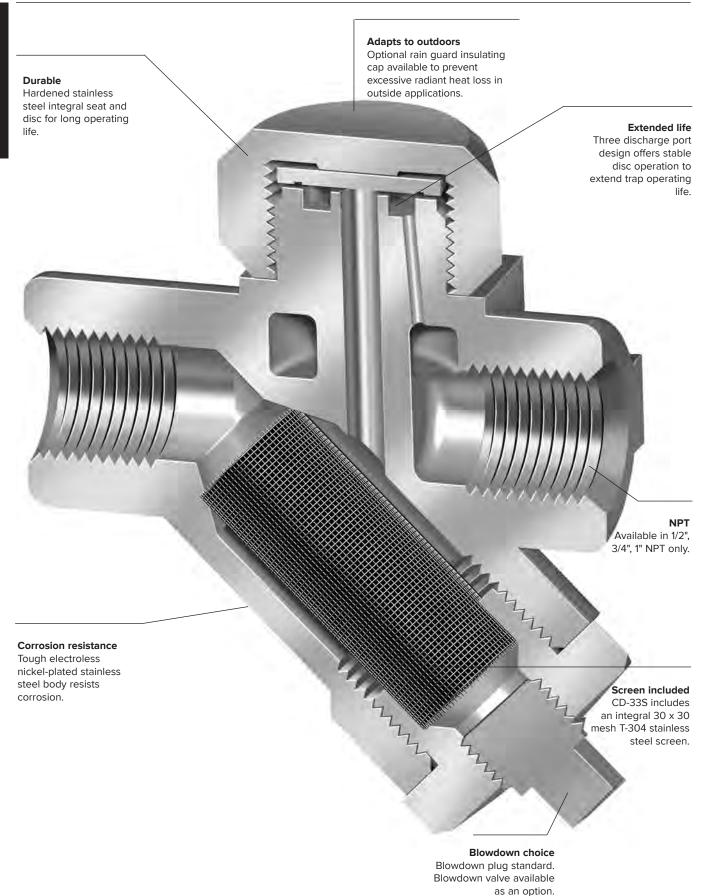




Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Armstrong[®] CD-33/CD-33S Disc Trap



CD-33/CD-33S Disc Trap



The Armstrong CD-33 is a disc style trap designed to control the trap's cycle rate. By reducing the cycle rate, the Armstrong CD-33 will have a longer service life than typical disc traps. This enhanced performance will ensure that maintenance time is minimized and steam costs are greatly reduced.

The CD-33 is designed with three discharge ports, which offer stable disc operation to extend trap operating life. The capacities of the Armstrong CD-33 have been engineered specifically for the following applications: large steam main drips, process equipment, and HVAC heating equipment on constant pressure. The CD-33L (low capacity) trap is designed for the low capacity applications of steam main drips and steam tracing lines. By ensuring that the capacities are designed to suit the application, and are not oversized, the CD-33 Series will last longer than other disc traps with excessive capacity ratings.

Advantages

- Three discharge port design
- · Minimal wear with controlled cycling
- Freeze-resistant
- · Hardened seat and disc

Specification

Steam trap shall be stainless steel thermodynamic type, integral seat design with hardened disc and seating surfaces, and electroless nickel plated finish. When required, trap shall be supplied with an integral Y strainer, integral blowdown valve or rain guard insulating cap. Maximum allowable pressure (vessel design) shall be 915 psig @ 752°F (63 barg @ 400°C). Maximum operating pressure shall be 600 psig @ 752°F (42 barg @ 400°C).

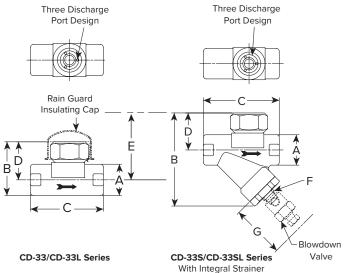






CD-33 Series Disc Trap

For Steam Service up to 600 psig (42 barg)...Capacities to 2 500 lb/hr (1 134 kg/hr)



The Armstrong CD-33 is a disc style trap designed to control the trap's cycle rate. By reducing the cycle rate, the Armstrong CD-33 will have a longer service life than typical disc traps. This enhanced performance will ensure that maintenance time is minimized and steam costs are greatly reduced.

The CD-33 is designed with three discharge ports, which offer stable disc operation to extend trap operating life. The capacities of the Armstrong CD-33 have been engineered specifically for the following applications: large steam main drips, process equipment, and HVAC heating equipment on constant pressure. The CD-33L trap is designed for the low capacity applications of steam main drips and steam tracing lines. By ensuring that the capacities are designed to suit the application, and are not oversized, the CD-33 Series will last longer than other disc traps with excessive capacity ratings.

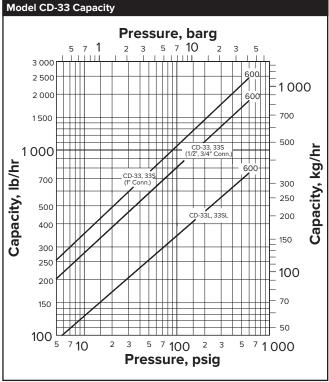
Advantages

- Three discharge port design
- Minimal wear with controlled cycling
- · Freeze-resistant
- Hardened seat and disc

Specification

Steam trap shall be stainless steel thermodynamic type, integral seat design with hardened disc and seating surfaces, and electroless nickel plated finish. When required, trap shall be supplied with an integral Y strainer, integral blowdown valve or rain guard insulating cap. Maximum allowable pressure (vessel design) shall be 915 psig @ 752°F (63 barg @ 400°C). Maximum operating pressure shall be 600 psig @ 752°F (41 barg @ 400°C).

	,
List of Materials	
Name of Part	Material
Body	ASTM A743 Gr. CA40
Cap	ASTM A743 Gr. CA40
Disc	ASTM A276 Gr. 420
Strainer Screen	30 x 30 Mesh T-304 Stainless Steel
Screen Retainer	ASTM A743 Gr. CA40
Blowdown Plug (CD-33S only)	Carbon Steel
Options	
Blowdown Valve	Stainless Steel
Rain Guard Insulating Cap (1/2", 3/4" Sizes Only)	Stainless Steel



CD-33 Series Disc Trap												
Model No.		CD-33			CD-33S (w/strainer)			CD-33L (low capacity)		CD-33SL (w/strainer) (low capacity)		
Pipe Connection Size	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Confidention Size	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20	1	25	3/8, 1/2, 3/4	10, 15, 20	1/2, 3/4	15, 20
"A"	1-7/16	37	1-3/4	44	1-7/16	37	1-3/4	44	1-7/16	36	1-7/16	36
"B" Height	2-1/2	63	3-1/8	79	4-1/4	108	4-3/4	121	2-1/2	63	4-1/4	108
"C" Length	3-5/16	84	3-15/16	100	3-1/2	89	4-1/8	105	3-5/16	84	3-1/2	89
"D" CL to Top of Cap	1-3/4	44	2-1/4	57	1-3/4	44	2-1/4	57	1-3/4	44	1-3/4	44
"E" Withdrawal Distance Rain Guard Insulating Cap	-	-	-	-	3	76	3	76	-	-	3	76
"F" Blowdown Connection Size	_	_	-	_	1/4 NPT	6	1/4 NPT	6	-	-	1/4 NPT	6
"G" Withdrawal Distance Blowdown Valve	_	_	_	_	3-1/2	89	3-1/2	89	_	-	3-1/2	89
Weight, lb (kg)	1.4 (0).64)	2.5 (1	.1)	2.2 (1.0)	3.25 (*	1.5)	1.41 (C	.64)	2.2 ((1.0)
Maximum Allowable Pressure (Vessel Design)	915 psig @ 752°F (63 barg @ 400°C)											
Minimum Operating Pressure, psig (barg)	3.5 psig (0.24 barg)											
Maximum Operating Pressure, psig (barg)					600	psig @ 4	486°F (41	barg (@ 252°C)			

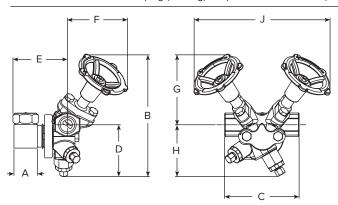
Maximum Back Pressure as Percent of Inlet Pressure, 80%

CD-3300 Series Disc Steam Traps

All Stainless With 360° Connector/IS-2/TVS-4000

For Steam Pressures to 450 psig (31 barg)...Capacities to 800 lb/hr (363 kg/hr)





CD-3300 With TVS-4000 Trap Valve Station

The Armstrong CD-3300 is a three discharge port design, which provides stable disc operation to extend operating life.

The CD-3300 is piped in-line by a 360° universal connector, which allows you to install the trap in virtually any piping configuration. Armstrong's unique standard connector or its IS-2 connector with integral strainer makes the CD-3300 easy to install, easy to renew. You save on labor time and cost because the connector simplifies piping and remains in-line.

Materials

 Trap cap:
 ASTM A743 CA40

 Trap disc:
 ASTM A276 Gr. 420

 Trap body:
 ASTM A276 Gr. 420

 Flange
 ASTM A105 Zinc plated

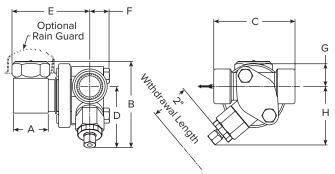
 Stainless steel—304

IS-2 connector with integral strainer:

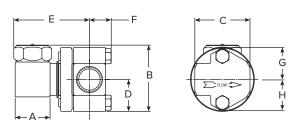
ASTM A351 Gr. CF8 20 x 20 mesh 304 SS Screen

Options

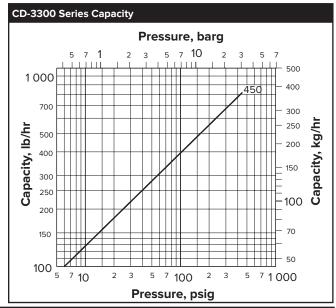
Rain guard insulating cap Blowdown valve—IS-2 connector only



CD-3300 With IS-2 Connector With Integral Strainer and Blowdown Valve



CD-3300 With Standard Connector



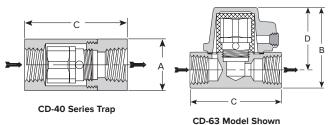
CD-3300 Series Disc Traps										
	CD-3300									
Model	Standard (Connector	IS-2 (Connector Wi	TVS 4000 Connector					
	in	mm	in	mm	in	mm	in	mm		
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20		
"A" Trap Diameter	1-1/2	38	1-1/2	38	1-1/2	38	1-1/2	38		
"B" Total Height	2-7/8	73	3-3/4	94	3-3/4	94	7-13/16	198		
"C" Face-to-Face	2-3/8	60	3-1/2	89	4	101	4-3/4	120		
"D" Connection Q to Bottom	1-3/8	35	2-5/8	67	2-5/8	67	3-1/4	83		
"E" Connection Q to Outside of Trap	3-3/8	86	3-3/8	86	3-9/16	90	3-9/16	90		
"F" Connection Q to Front of Connector	13/16	20	7/8	22	7/8	22	3-7/8	98		
"G" Connection & to Top	1-3/8	46	1	25	1	25	4-1/2	114		
"H" Connection Ç to Bottom of Connector	1-3/8	46	2-1/2	64	2-1/2	64	3-1/4	83		
"J" Width Across Handwheels (Valve Open)	_	_	_	_	_	_	8-11/16	221		
Test Port Connection	_	_	_	_	_	_	1/4 NPT	6		
Trap Only Weight, lb (kg)				2	(0.91)					
Trap and Connector Weight, lb (kg)	3.6	1.6	3.9	1.8	4.2	2	8-1/2	3.8		
Maximum Operating Pressure			450) psig @ 456°	°F (31 barg @ :	236°C)				
Maximum Allowable Pressure (Vessel Design)	720 psig @ 750°F (50 barg @ 400°C)									



CD-40 and CD-60 Series Controlled Disc Steam Trap

Carbon Steel

For Pressures to 600 psig (41 barg)...Capacities to 2 850 lb/hr (1 295 kg/hr)



Description

Armstrong CD-40 and CD-60 Series controlled disc traps contain a replaceable capsule, making it possible to renew a worn trap by simply replacing the capsule. A heating chamber in the shell ensures consistent operation. This steam jacket provides a relatively constant temperature in the control chamber regardless of ambient conditions. Cycling rate is controlled and does not increase when the trap is exposed to cold winds, rain or snow. CD-40 Series traps are also available with optional integral .045 perforated stainless steel strainer screens. CD-60 Series traps contain integral strainers with ratios of open area to inside area of pipe that equal or exceed those of most separate "Y" type strainers.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model CD-40 600 psig @ 500°F (41 barg @ 260°C) 600 psig @ 750°F (41 barg @ 399°C) Model CD-60

Maximum operating pressure: 600 psig (41 barg) at saturated steam temperature

Minimum operating pressure: 10 psig (0.7 barg)

Connections

Model CD-40 and CD-60 Screwed NPT and BSPT Model CD-60 Socketweld

Materials Model CD-40

Carbon steel—C-1215 Body: Control chamber: Hardened 440 stainless steel Hardened 440 stainless steel Disc: Hardened 440 stainless steel Capsule body:

Strainer screen (option): Stainless steel

Materials Model CD-60

ASTM A216 WCB ASTM A216 WCB Cap:

Control chamber: Hardened 440 stainless steel Disc: Hardened 440 stainless steel Capsule body: Hardened 440 stainless steel 20 x 20 mesh stainless steel Strainer screen:

Option

CD-40 Series integral strainer screen (.045 perforated stainless steel)

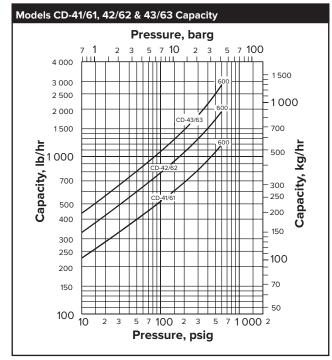
Controlled disc steam trap, type ... in carbon steel. CD-60 includes integral strainer. Maximum allowable pressure 600 psig.

How to Order

- · Specify model number
- · Specify size and type of pipe connection
- · Specify any options required

For a fully detailed certified drawing, refer to CD #1020.





Capacities given are continuous discharge capacities in pounds and kilograms of hot condensate per hour at pressure differential indicated with condensate temperatures approximately 25°F (14°C) below steam temperatures.

NOTE: CD traps can operate with minimum of 2 psig (.15 barg) inlet pressure and a maximum of 80% back pressure. However, for best results, inlet pressure should not drop below 10 psig (.70 barg) and back pressure should not exceed 50% of inlet pressure.

CD-40 and CD-60 Serie	CD-40 and CD-60 Series Controlled Disc Traps															
Model No.		CD)-41*		CD-	-42*	CD	-43*		CD	-61		CD.	-62	CD	-63
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	3/8	10	1/2	15	3/4	20	1	25	3/8	10	1/2	15	3/4	20	1	25
"A" (Diameter)	1-1/4	31.7	1-1/4	31.7	1-5/8	41.3	2-3/8	60.3	-	_	_	_	_	_	_	-
"B" (Height)	_	_	-	_	_	_	-	_	2-3/4	66.7	2-3/4	66.7	3-1/2	87.3	4-1/4	108
"C" (Length)	3	76.2	3-13/32	86.5	3-15/16	100.0	4-5/8	117.5	3-1/2	88.9	3-1/2	88.9	4-5/8	117	4-3/4	122
"D" (Ç to Top of Cap)	_	_	-	_	_	_	_	_	2-1/8	50.8	2-1/8	50.8	2-3/4	68.3	3-5/16	84.1
Weight Ib (kg)	3/4	(0.3)	3/4 (0.3)	1-3/4	(0.8)	4-1/4	l (1.9)	2-3/4	1 (1.2)	2-1/2	2 (1.1)	4-3/4	(2.2)	6-3/4	4 (3.1)

^{*}Optional integral strainer available.

CD72SR Series Disc Traps

For Steam Service up to 1010 psig (69.6 barg) and Capacities from 935 lb/hr (435 Kg/hr)



Armstrong CD72SR is a disc styled trap designed to control the trap's cycle rate. The reduced cycle rate provides Armstrong CD72SR trap with a longer service life than typical disc traps. This enhanced performance ensures minimum maintenance time and reduced steam costs.

The capacity of Armstrong CD72SR has been engineered specifically for the following applications: large steam main drips, process equipments and HVAC heating equipments at constant pressure.

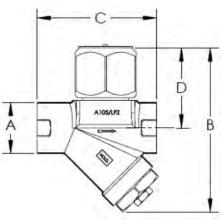
Advantages of CD72SR

- Minimum wear with controlled cyclingFreeze-resistant
- · Hardened Seat and disc
- Weldable
- In-line repairable



Screwed BSPT and NPT Socketweld Flanged DIN or ANSI (Welded). Consult factory for dimensions and weight





List of Materials								
Name of Part	Material							
Name of Part	CD72SR							
Body	Dual certified Forged Corten Steel							
Cap	ASTM A 105N / A350 LF2 Cl. 1							
Disc & Seat	ASTM A 564 TYP630, H900							
Strainer Screen	Stainless steel TYP304, 30 x 30 Mesh							
Screen	Dual certified Forged Corten Steel							
Retainer	ASTM A 105N / A350 LF2 Cl. 1							
Blowdown Plug	ASTM A350 Gr. LF2 CL.1							

Dimensions and Weights									
	CD72SR								
Model No.		nd 3/4" 5 DN20)		1" N25)					
	in	mm	in	mm					
"A"	1.53	38.8	1.89	48.0					
"B" Height	4.89	124.1	5.12	130.0					
"C" Length	3.56	90.5	4.41	112.0					
"D" & to top of cap	2.38	60.5	2.58	65.6					
Weight, lb (Kg)	3.31	(1.5)	4.59	(2.0)					
Max. allowable pressure (Vessel Design)	1010 psig @ 750°F (69.6 barg @ 399°C)								
MIn. operating pressure	3.5 psig (0.24 barg)								
Max. operating pressure	600 ps	sig @ 486°F (4	11.4 barg @ :	252°C)					

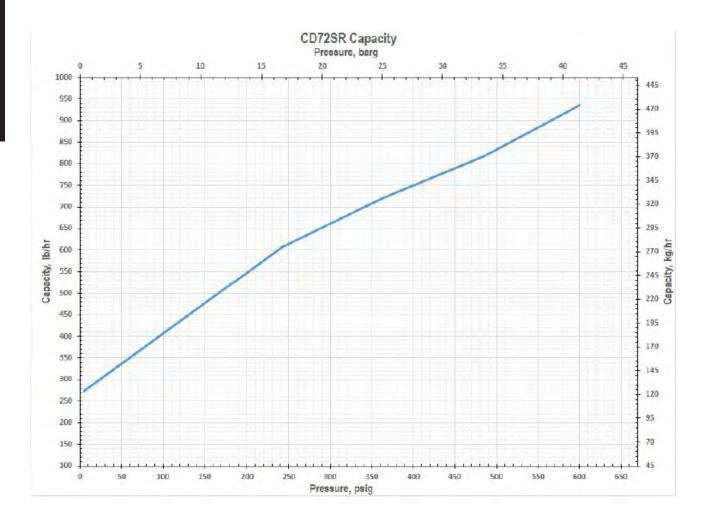


CD72SR Series Disc Traps

For Steam Service up to 1010 psig (69.6 barg) and Capacities from 935 lb/hr (435 Kg/hr)

CD72SR CAPACITY CHART

Capacities given are in continuous discharge capacities in pounds and kilograms of hot condensate per hour at pressure differential indicated with condensate temperatures approximately 25° F (14°C) below steam temperature.



OTHER FACE TO FACE DIMENSIONS ARE AVAILABLE ON REQUEST

	1/2"(DN15)			3/4"(DN20)				1"(DN25)				
CD72SR			INDI	A - IBR			INDIA	- IBR			INDIA	A - IBR
	inch	mm	inch	mm	inch	mm	inch	mm	inch	mm	inch	mm
ANSI 150#	6.7	169	8.3	210	6.9	174	7.9	200	7.9	200	8.7	220
ANSI 300#	7.0	179	8.8	224	7.2	183	8.7	220	8.4	213	9.4	240
ANSI 600#	7.6	192	9.3	235	7.7	195	9.1	230	8.9	226	10	253
PN40	5.9	150	-	-	5.9	150	-	-	6.3	160	-	-

Armstrong®

CD-80S Series Disc Trap

For steam service up to 1 000 psig (68.9 barg)...Capacities to 800 lb/hr (362 kg/hr)



Description

The Armstrong CD-80S series are durable disc style steam traps designed for medium to high-pressure use. Perfectly suited for drip trap applications, the CD-80S series was engineered to meet the demanding conditions found in Power and Petrochemical applications.

With an integral strainer and rugged construction, the CD-80S series offers a compact, reliable solution for high pressure applications with low condensate loads.

Advantages

- Compact
- Integral Strainer
- Freeze-resistant
- · Replaceable seat and disc
- Weldable

Connections

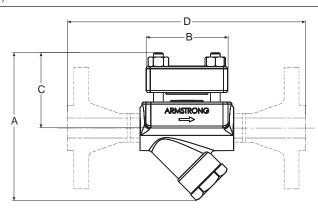
- Screwed NPT and BSPT
- · Socketweld and Buttweld
- Flanged Connections available

Series CD-80S List of Materials								
Material								
CD-80S	CD-82S							
ASTM A182 F11 Class 2	ASTM A182 F22 Class 3							
ACTM AG	01 TVD D2							
ASTIVI AD	01117 DZ							
ASTM A193 Gr. B16 / ASTM A194 Gr. 7								
30 x 30 Mesh T-304 Stainless Steel								
	ASTM A182 F11 Class 2 ASTM A66 ASTM A193 Gr. B16							

Dimensions and Weights - NPT, BSPT and SW Connection							
	in	mm					
	1/2, 3/4	15, 20					
"A" Height	5-11/16	144					
"B" Length*	3-5/8	92					
"C" CL to top of cap	2-31/32	75					
Weight, lb (kg)*	7.75	(3.5)					
Minimum Operating Pressure	100 psig	(6.9 barg)					
Maximum Operating Pressure	1 000 psig @ 546°F (68.9 barg @ 285°C)						
Maximum Allowable Pressure	1 500 psig @ 650°F (103.4 barg @ 343°C)						

Dimensions and Weights - ASME B 16.5 Class 150# Flanged Connection								
	in	mm	in	mm				
	1/2	15	3/4	20				
"A" Height	5-11/16	144	5-11/16	144				
"D" Face-to-Face	8-3/4	222	9-3/32	231				
"C" CL to top of cap	2-31/32	75	2-31/32	75				
Weight, lb (kg)*		11.75	(5.3)					
Minimum Operating Pressure		100 psig	(6.9 barg)					
Maximum Operating Pressure	200 psig @ 400°F (13.7 barg @ 204°C)							
Maximum Allowable Pressure	200 psi	g @ 400°F	(13.7 barg @	204°C)				

Dimensions and Weights Connection	- ASME B 1	6.5 Class	600# Flang	ged	
	in	mm	in	mm	
	1/2	15	3/4	20	
"A" Height	5-11/16	144	5-11/16	144	
"D" Face-to-Face	9-19/32	244	10-1/32	254	
"C" CL to top of cap	2-31/32	75	2-31/32	75	
Weight, lb (kg)*	13.75 (6.2) 15.75 (7.1)				
Minimum Operating Pressure	100 psig (6.9 barg)				
Maximum Operating Pressure	1000 psig @ 546°F (68.9 barg @ 285°C)				
Maximum Allowable Pressure	1 210 psig @ 600°F (83.7 barg @ 316°C)				



Dimensions and Weights - BW Connection					
	in	mm			
	1/2, 3/4	15, 20			
"A" Height	5-11/16	144			
"B" Length*	4-23/32	120			
"C" CL to top of cap	2-31/32	75			
Weight, lb (kg)*	8.0	(3.6)			
Minimum Operating Pressure	100 psig (6.9 barg)				
Maximum Operating Pressure	1000 psig @ 546°F (68.9 barg @ 285°C)				
Maximum Allowable Pressure	1 500 psig @ 650°F (103.4 barg @ 343°C)				

Dimensions and Weights - ASME B 16.5 Class 300# Flanged Connection					
	in	mm	in	mm	
	1/2	15	3/4	20	
"A" Height	5-11/16	144	5-11/16	144	
"D" Face-to-Face	9-3/32	231	9-1/2	241	
"C" CL to top of cap	2-31/32	75	2-31/32	75	
Weight, lb (kg)*	11.75 (5.3) 13.75 (6.2)				
Minimum Operating Pressure	100 psig (6.9 barg)				
Maximum Operating Pressure	665 psig @ 500°F (45.6 barg @ 260°C)				
Maximum Allowable Pressure	665 psig @ 500°F (45.6 barg @ 260°C)				
B	A 60 4E D 4	S = 01		•	

Dimensions and Weights Connection	- ASME B 1	16.5 Class !	900# Flang	ged	
	in	mm	in	mm	
	1/2	15	3/4	20	
"A" Height	5-11/16	144	5-11/16	144	
"D" Face-to-Face	10-1/4	260	10-31/32	279	
"C" CL to top of cap	2-31/32 75 2-31/32 75				
Weight, lb (kg)*	21.75 (9.9)				
Minimum Operating Pressure	100 psig (6.9 barg)				
Maximum Operating Pressure	1000 psig @ 546°F (68.9 barg @ 285°C)				
Maximum Allowable Pressure	1 500 psig @ 650°F (103.4 barg @ 343°C)				

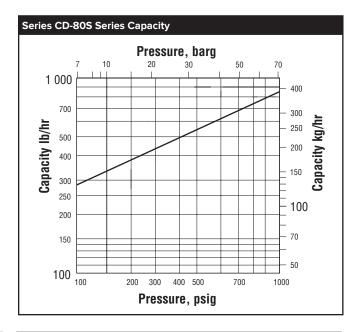


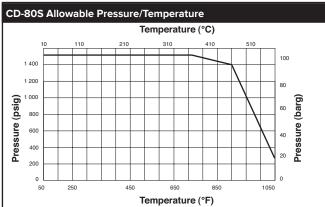
CD-80S Series Disc Trap

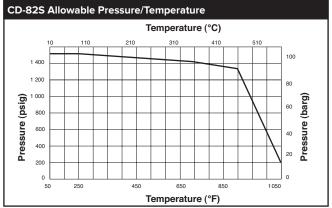
For steam service up to 1 000 psig (68.9 barg)...Capacities to 800 lb/hr (362 kg/hr)

Specification

Steam trap shall be forged steel (ASTM A182 F11 or ASTM A182 F22) thermodynamic type. Trap shall be supplied with bolted cover and replaceable disc and seating surfaces. Trap shall be supplied with an integral Y strainer with stainless steel mesh. Maximum allowable pressure (vessel design) shall be 1 500 psig @ 650°F (103.4 barg @ 343°C). Maximum operating pressure shall be 1 000 psig @ 546°F (68.9 barg @ 285°C).





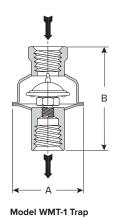


Thermostatic Wafer Steam Trap

Stainless Steel

For Pressures to 250 psig (17 barg)...Cold Water Start-Up Capacities to 1 000 lb/hr (453 kg/hr)





Description

The WMT thermostatic wafer traps are designed to last longer than other oversized, all-purpose thermostatic and thermodynamic steam traps.

A water seal prevents loss of steam through the orifice of the WMT Series.

Adjusts automatically to flow rates, including large start-up loads, at all pressures within its range.

Specification

Thermostatic wafer steam trap, type WMT stainless steel.

How to Order

- Specify model number
- Specify size and type of pipe connection. When flanges are required, specify type of flange in detail

For a fully detailed certified drawing, refer to CD #1017 (WMT-1).

Model	Model WMT-Series Thermostatic Wafer Trap Capacity								
1	ential sure*	Star	Water t-Up (21°C)	Hot Water Start-Up 212°F (100°C)		Start-Up		Oper Conde 50°F Below Sa	ensate (0°C)
psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	**lb/hr	**kg/hr		
5	0.35	120	54	100	45	10	4.5		
10	0.70	150	68	170	77	13	5.9		
20	1.4	320	145	250	113	18	8.2		
30	2	390	177	300	136	20	9.1		
40	3	420	191	350	159	24	10.9		
50	3.5	490	222	400	181	26	11.8		
75	5	570	259	480	218	30	13.6		
100	7	650	295	580	263	35	15.9		
150	10.5	700	318	700	318	40	18.1		
200	14	900	408	800	363	46	20.9		
250	17	1000	454	950	431	50	22.7		

^{*}Capacities based on differential pressure with no back pressure.

WMT Thermostatic Wafer Steam Trap						
Model No.	WMT-1					
Dina Cannastiana	in	mm	in	mm		
Pipe Connections	1/4, 3/8	6, 10	1/2	15		
"A" (Diameter)	2-1/4	57	2-1/4	57		
"B" (Height)	3-5/16	84	3-5/16	84		
Weight lb (kg)	1-1/4 (0.6) 1-1/4 (0.6)					

Model	WMT-1
Connections	Screwed NPT and BSPT
Material	
Cap and body	ASTM A240 Grade 304L
Capsule	All stainless steel—304
Maximum Operating Condition	s
Maximum allowable pressure (vessel design)	250 psig @ 400°F (17 barg @ 204°C)
Maximum operating pressure	250 psig (17 barg)

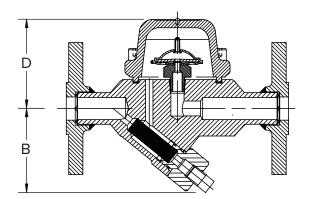
^{**}Capacities will vary with the degree of subcooling. When greater capacities are required, the trap will automatically adjust to the load, up to the maximum (cold water) capacity shown, by increasing the amount of subcooling.

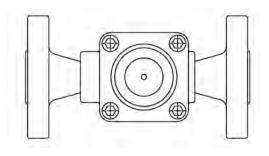


TC-300 Series Thermostatic Wafer Steam Trap

Carbon Steel

For Pressures to 250 psig (17 barg)...Cold Water Start-Up Capacities to 1 000 lb/hr (453 kg/hr)





Description

The TC-300 is sized precisely to handle the extremely low condensate load found in most instrument steam tracer lines. The TC-300 traps are designed to last longer than other oversized, all-purpose thermostatic and thermodynamic steam traps.

This steam trap adjusts automatically to flow rates, including large startup loads, at all pressures within its range.

How to Order

Specify: Model Number, Size and type of pipe connection. When flanges are required, specify type of flange in detail.

TC-30	TC-300 Series Thermostatic Wafer Steam Trap Capacity						
	ential sure*	Cold Water Start-Up 70°F (21°C)		Hot Water Start-Up 212°F (100°C)		Oper Conde 50°F Below Sa	ensate (10°C)
psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	**lb/hr	**kg/hr
5	0.35	120	54	100	45	10	4.5
10	0.70	150	68	170	77	13	5.9
20	1.4	320	145	250	113	18	8.2
30	2	390	177	300	136	20	9.1
40	3	420	191	350	159	24	10.9
50	3.5	490	222	400	181	26	11.8
75	5	570	259	480	218	30	13.6
100	7	650	295	580	263	35	15.9
150	10.5	700	318	700	318	40	18.1
200	14	900	408	800	363	46	20.9
250	17	1000	454	950	431	50	22.7

^{*} Capacities based on differential pressure with no back pressure.
** Capacities will vary with the degree of subcooling. When greater capacities are required, the trap will automatically adjust to the load, up to the maximum (cold water) capacity shown, by increasing the amount of subcooling.

TC-300 Trap		
Dina Connections	in	mm
Pipe Connections	1/2, 3/4,1	15 – 20 – 25
"B" Height (Screwed & SW)	4-19/32	117
"A" Height (flanged PN40*)	4-19/32	117
"C" Face-to-Face (Screwed & SW)	3-1/2 - 3-1/2 - N/A	90 – 90 – N/A
"CC" Face-to-Face	5-29/32 - 5-29/32 -	150 – 150 –
(Flanged PN40*)	6-19/64	160
"D" CL to Top	2-3/8	60
Weight in kg (Screwed & SW)	4-1/4	1,9
Weight in kg (Flanged PN40)	9-1/2 – 9-1/2 – 10	4,3 – 4,5 – 4,7

	,
TC-300 Traps	
Model	TC-300
	Screwed BSPT and
Connections	NPT
	Socketwelded
	Flanged DIN and ANSI
Material	
Cap and Body	ASTM-A-105
Capsule	All Stainless Steel –
Capsule	304
Maximum Operating Conditions	
Maximum allowable pressure (vessel	465 psig @ 662°F
design) [†]	(32 barg @ 350 °C)
Maximum operating pressure	250 psig @ 400°F
Maximum operating pressure	(17 barg @ 207 °C)

[†] May be derated depending on flange rating and type.

WT Series Thermostatic Wafer Steam Trap

Stainless Steel or Carbon Steel

For Pressures to 600 psig (41 barg)...Cold Water Start-Up Capacities to 1 600 lb/hr (726 kg/hr)



Description

Armstrong offers three thermostatic wafer steam traps. The WT-1 is ideal for low-capacity steam tracers and features an exclusive non-welded wafer design and internal strainer screen two to three times larger than that of other thermostatic traps in a sealed stainless steel body. Choice of NPT or BSPT screwed connections.

The WT-2000 does not have an internal strainer, but is equipped with a special 360° connector to expand piping options and simplify installation. Choice of NPT or BSPT screwed connections, or socketweld connections. Also available with optional IS-2 stainless steel connector with integral strainer.

Armstrong's WT-3 is a carbon steel thermostatic wafer trap for superheated drip service. It features an exclusive non-welded wafer design, which eliminates problems associated with weld stress. The WT-3 has no thin-walled enclosures such as bellows or welded diaphragms. It is also resistant to water hammer. Choice of NPT or BSPT screwed connections, or socketweld connections.

NOTE: Since the normal operation of all suppressed temperature-discharge (subcooling) steam traps is to back up condensate, they should not be used on drip legs for saturated steam service, heating or process equipment. Exercise care in the maintenance of any thermostatic wafer trap with a small discharge area susceptible to clogging.

Specification

Thermostatic wafer steam trap, type ... in stainless steel or carbon steel.

How to Order

Specify:

- · Model number
- · Size and type of pipe connection, or connector style
- Any options required

For a fully detailed certified drawing, refer to CD #1017.

Mode	Model WT Series Wafer Trap Capacity						
	rential sure*	Star	Water t-Up (21°C)	Hot V Star 212°F (t-Up	Oper Conde 50°F Below Sa	ensate (10°C)
psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	**lb/hr	**kg/hr
5	0.35	120	54	100	45	10	4.5
10	0.70	150	68	170	77	13	5.9
20	1.4	320	145	250	113	18	8.2
30	2	390	177	300	136	20	9.1
40	3	420	191	350	159	24	10.9
50	3.5	490	222	400	181	26	11.8
75	5	570	259	480	218	30	13.6
100	7	650	295	580	263	35	15.9
150	10.5	700	318	700	318	40	18.1
200	14	900	408	800	363	46	20.9
250	17	1000	454	950	431	50	22.7
300	21	1050	476	1025	465	56	25.4
350	24	1 150	522	1200	544	63	28.6
400	28	1300	590	1 250	567	70	31.8

^{*}Capacities based on differential pressure with no back pressure.

^{**}Capacities will vary with the degree of subcooling. When greater capacities are required, the trap will automatically adjust to the load, up to the maximum (cold water) capacity shown, by increasing the amount of subcooling.

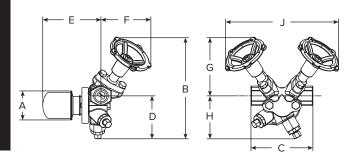
Model	WT-1 All Stainless Steel	WT-2000 Stainless Steel w/360° Connector	WT-3 Carbon Steel			
Design		Welded				
Connections	Screwed (NPT and BSPT) Socketweld	Screwed (NPT and BSPT), Socketweld and Flanged	Screwed (NPT and BSPT) Socketweld			
Material						
Body		ASTM A240—304L	Carbon steel C-1018			
Cap		A31M A240 304E	Carbon steer c 1010			
Capsule wafer		Hastelloy				
Capsule body		Stainless steel—303				
Capsule cap		Stalliless steel—303				
Flange	_	ASTM A105 Zinc plated	_			
Connector						
Standard	_	Stainless steel—304	_			
IS-2 w/integral strainer	_	Stainless steel—304 w/20x20 mesh 304 SS screen	_			
TVS 4000	_	ASTM A351 Gr. CF8M with screen, test valve and blowdown valve—stainless steel	_			
Maximum Operating Conditions						
Maximum allowable pressure (vessel design)	400 ps	400 psig @ 650°F (28 barg @ 343°C)				
Maximum operating pressure	400 psig (28 barg) 600 psig (41 barg)					
Option WT-2000						
Blowdown Valve IS-2 Connector a	nd TVS-4000 Only		<u> </u>			



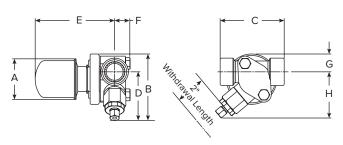
WT Series Thermostatic Wafer Steam Trap

Stainless Steel or Carbon Steel

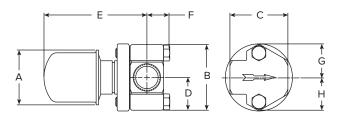
For Pressures to 600 psig (41 barg)...Cold Water Start-Up Capacities to 1 600 lb/hr (726 kg/hr)/hr (726 kg/hr)



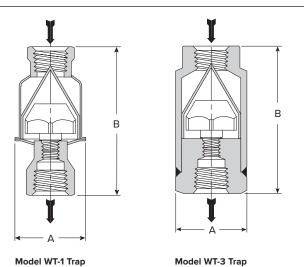
Series WT-2000 With TVS 4000 Trap Valve Station



Series WT-2000 With Integral Strainer and Blowdown Valve



Series WT-2000 With Standard Connector



Connectors

The WT-2000 can be connected to the standard connector, the IS-2 with integral strainer, or TVS 4000. WT-2000 can be used on thermostatic, thermostatic wafer and disc traps.



WT-1 Series Traps												
Model No.		WT-1										
Pipe Connections	in	mm	in	mm								
Pipe Connections	1/2	15	3/4	20								
"A" (Diameter)	2-1/4	57	2-1/4	57								
"B" (Height)	4-1/2	114	4-11/16 119									
Weight, lb (kg)	1 (C).5)	1-1/4	1 (0.6)								

WT-3 Series Traps							
Model No.	WT-3						
Pipe Connections	in	mm					
Pipe Connections	1/2, 3/4	15, 20					
"A" (Diameter)	2-1/4	57					
"B" (Height)	4-5/8	118					
Weight, lb (kg)	3 (1.4)					

WT-2000 Series Traps											
Model No	WT-2000										
Model No.	Standard C	Connector	IS-2 C	onnector Wi	th Integral S	trainer	TVS 4000	Connector			
Dina Cannastians	in	mm	in	mm	in	mm	in	mm			
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20	1/2, 3/4	15, 20	1	25	1/2, 3/4	15, 20			
"A" Trap Diameter	2-1/4	57	2-1/4	57	2-1/4	57	2-1/4	57			
"B" Total Height	2-11/16	68	3-5/8	92	3-5/8	92	7-13/16	198			
"C" Face-to-Face	2-3/8	60	3-1/2	89	4	101	4-3/4	120			
"D" Connection & to Bottom	1-3/8	46	2-5/8	67	2-5/8	67	3-1/4	83			
"E" Connection & to Outside of Trap	4-1/4	107	4-3/4	120	4-15/16	125	4-1/2	115			
"F" Connection டி to Front of Connector	13/16	20	7/8	22	7/8	22	3-7/8	98			
"G" Connection & to Top	1-3/8	46	1	25	1	25	4-1/2	114			
"H" Connection & to Bottom of Connector	1-3/8	46	2-1/2	64	2-1/2	64	3-1/4	83			
"J" Width Across Handwheels (valve open)	_	_	_	_	_	_	8-11/16	221			
Test Port Connection	_	_	_	_	_	_	1/4 NPT	6			
Trap Only Weight, lb (kg)				1-1/2	(0.70)						
Trap and Connector Weight, lb (kg)	3.2	(7)		3.4	(7.5)		8 (3	.6)			

SH Series Superheat Traps

Bimetallic Steam Traps For Superheat Conditions

For Pressures to 1 800 psig (124 barg)...Cold Water Capacities to 6 500 lb/hr (2 950 kg/hr)



Description

Armstrong's SH Series Bimetallic Steam Traps for superheat or low load conditions are the ideal traps for applications where other trap styles are not suitable for long life.

The Armstrong SH Series bimetallic traps also have the ability to handle the large start-up loads associated with superheat applications. The unique bimetallic element allows for shut-off before superheat reaches the trap, thus preventing steam loss. The SH-900/1500 series utilizes titanium valves and seats to ensure extremely long service life in the harsh environment of superheated steam systems.

Maximum Operating Conditions

Maximum allowable pressure (vessel design):

Model SH-300: 580 psig @ 662°F (40 barg @ 350°C) Model SH-900L and H: 900 psig @ 900°F (62 barg @ 482°C) Model SH-1500: 1800 psig @ 1050°F (124 barg @ 565°C)

Maximum operating pressure:

Model SH-300: 319 psig (22 barg) Model SH-900L: 650 psig (45 barg) Model SH-900H: 900 psig (62 barg) Model SH-1500: 1800 psig (124 barg)

Suggested minimum operating pressure:

Model SH-300: Not applicable Model SH-900L and H: 200 psig (14 barg) Model SH-1500: 600 psig (41 barg)

Connections

Model SH-300: Screwed BSPT and NPT, socketweld,

flanged DIN or ANSI (welded)

Model SH-900: Socketweld, flanged, buttweld, screwed,

Model SH-1500 Socketweld, flanged, buttweld

Materials Model SH-300

ASTM A105 Body and cap: ASTM A350-LF2 Valve and seat: Chrome Steel - 440C Elements: Nickel plated Strainer: Stainless steel screen

Model SH-900

Body and cap: ASTM A351 Gr. CF8M

Titanium

Valve and seat: Elements: Ni-Cr and stainless steel Strainer: Stainless steel screen

Model SH-1500

Body and cap: ASTM 217 Gr. C12A

Valve and seat: Titanium

Elements: Ni-Cr and stainless steel Strainer: Stainless steel screen

Specification

Steam trap shall be a bimetallic style. The trap shall be investment cast chrome-moly steel (Model SH-1500) with integral stainless steel strainer, in-line repairable. The mechanism shall consist of a stacked nickel-chrome bimetal operator, with titanium valve and seat. The steam trap shall be capable of operation on low load and superheat applications throughout its pressure/

Bimetallic style steam traps in carbon steel (Model SH-300) or stainless steel (Model SH-900) with integral stainless steel strainer, in-line repairable. The mechanism shall consist of a stacked nickel-chrome bimetal operator (SH-300 nickel plated) with titanium valve and seat (SH-300 chrome steel valve and seat). The steam trap shall be capable of operation on low-load applications throughout its pressure/temperature range.

How to Order

- Specify model number
- · Specify maximum operating pressure
- · Specify size and type of pipe connection. When flanges are required, specify type of flange in detail





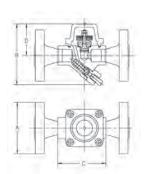


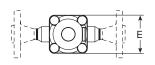


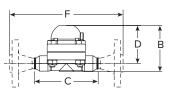
SH Series Superheat Traps

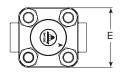
Bimetallic Steam Traps For Superheat Conditions

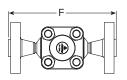
For Pressures to 1 800 psig (124 barg)...Cold Water Capacities to 6 500 lb/hr (2 950 kg/hr)

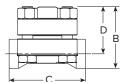


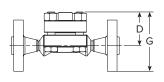












Model SH-300

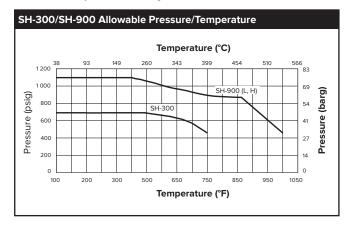
Model SH-900

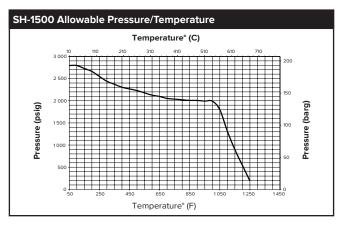
Model SH-1500

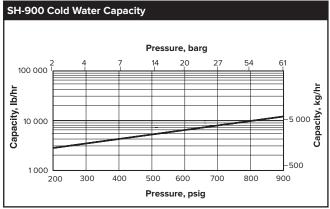
Model	SH-	300	SH-	900	SH-1	500	
Dina Cannastiana	in	mm	in	mm	in	mm	
Pipe Connections	1/2, 3/4, 1***	2, 3/4, 1*** 15, 20, 25 1/2, 3/4, 4-1/2 115 4-1/2 3-1/2 90 6-1/4 2-5/16 59 3-3/4 — — 3-3/4 — — 11 — — —	1/2, 3/4, 1**	15, 20, 25	3/4, 1	20, 25	
"B" Height	4-1/2	115	4-1/2	115	5	127	
"C" Face-to-Face	3-1/2	90	6-1/4	158	6-1/4	158	
"D" & to Top	2-5/16	59	3-3/4	95	3-13/16	97	
"E" Width	_	_	3-3/4	95	4-7/8	124	
*"F"	_	_	11	279	12	305	
*"G"	_	_	_	_	6-3/8	162	
Weight, lb (kg)	4.1	(1.9)	10 (4.4)	15 (6.8)		

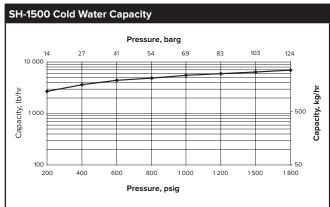
^{*&}quot;F" dimensions for SH-900 are for 3/4" connection, class 600 flanged. "F" and "G" dimensions for SH-1500 are for 3/4" connection, class 1500 flanged. Consult factory for dimensions of models with other connection sizes and/or flanges.

^{***}SH-300 1" only available as flanged connections.









Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

^{**} SH-900 1" buttweld.

SH-2000 Bimetallic Steam Traps

All Stainless Steel

For pressures to 400 psig (28 barg)...Cold Water Capacities to 4 800 lb/hr (2 175 kg/hr)



Description

SH Series Superheat Steam Traps operate by the effect that rising temperature has on the thermostatic bimetallic elements.

The effect of rising temperature on bimetallic elements operates the Armstrong SH-2000 bimetallic steam trap. It adjusts to changing conditions because the curving of the bimetallic elements, caused by increasing temperature, compensates for increasing pressure.

At start-up, the valve is wide open, which allows a large volume of non-condensables and cold condensate to be removed from the system. When the system reaches steam temperature, the elements become sufficiently hot to pull on the trap's valve stem, closing the valve.

The valve remains closed until the bimetallic elements cool, thus allowing the valve to crack open, venting the condensate and non-condensables, and then close again when steam temperature is reached.

The Armstrong SH-2000 has a sealed, stainless steel body that is lightweight, compact and highly resistant to corrosion. It is adaptable to an Armstrong 360° Universal Connector or a Trap Valve Station (TVS). This makes it easy to install and replace, as the trap can be removed while the connector remains in-line. That means savings in labor cost and ultimate flexibility—because inverted bucket, thermostatic, thermostatic wafer, disc, and float and thermostatic steam traps can all be installed on the same connector.



Maximum allowable pressure (vessel design): 400 psig @ 800°F (28 barg @ 427°C)

Maximum operating pressure: 400 psig (28 barg) Suggested minimum operating pressure: 200 psig (14 barg)

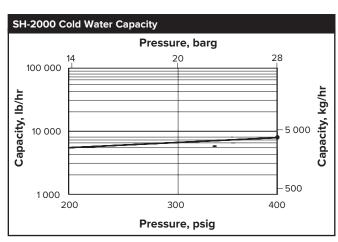
Materials

Body: Stainless Steel

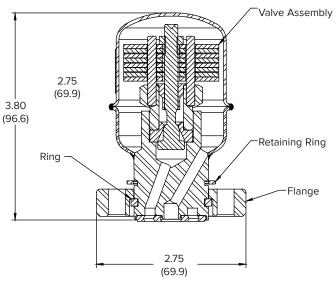
Valve & Seat Elements: Titanium, Ni-Cr and Stainless Steel

Ring: Stainless Steel
Cap Assembly: Stainless Steel
Flange: ASTM A105 Zinc plated

Retainer Ring: Carbon Steel
Spiral Wound Gasket: Stainless Steel
Label: Aluminum







SH-2500 Bimetallic Steam Trap

All Stainless Steel

For Pressures to 650 psig (45 barg)...Capacities to 6 000 lb/hr (2 722 kg/hr)

Description

Armstrong's SH-2500 Bimetallic Steam Trap is the ideal design for applications involving superheated steam.

During start-up, the bimetallic mechanism is fully open and allows large volumes of non-condensable gases and condensate to be removed from the system. As the system reaches saturated steam conditions, the mechanism begins to close preventing any live steam loss. The superheat during normal operating steam conditions keep the valve closed to ensure long service life.

In the event that operating conditions change and condensate forms at the steam trap inlet, the cooling effect allows the bimetallic mechanism to open and discharge any accumulation. The valve quickly closes once normal operating conditions return.

The SH-2500 consists of an investment cast, stainless steel body that is compact and highly resistant to harsh, corrosive environments. The integral mounting flange is compatible with the Armstrong IS-2, TVS-4000, std connector making for labor savings and easy steam trap replacement.



Maximum allowable pressure (vessel design): 650 psig @ 600°F (45 barg @ 316°C)

Maximum operating pressure:

SH-2500 650 psig @ 600°F (45 barg @ 316°C)

Suggested minimum operating pressure: SH-2500 200 psig (14 barg)

Materials and Weight

Body: ASTM A351 Gr. CF8M

Valve & Seat Elements: Titanium
Ni-Cr

NI-Cr

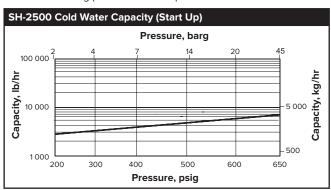
Stainless Steel
Spiral Wound Gasket: Stainless Steel
Bolts: ASTM A193 B7
Weight: 2.8 lbs (1.3 kg)

Specification

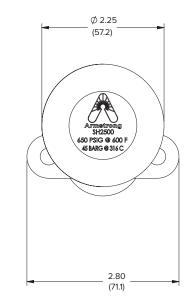
Steam traps shall be a bimetallic style designed for superheated steam applications. The steam trap body shall be tamperproof, investment cast stainless steel A351 Gr. CF8M. The mechanism shall consist of a stacked nickel-chrome bimetal operator with titanium valve and seat. The gaskets shall be captured stainless steel spiral wound. The steam trap shall be compatible with the 2-bolt universal connector technology.

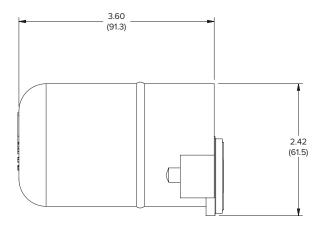
How to Order

Specify model number
Maximum working pressure and temperature









Note: Cold water capacity for start-up loads only. When superheat present, there will be minimal condensate.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

AB-3000 Series Bimetallic Steam Traps

All Stainless Steel

For Pressures to 319 psig (22 barg)...Capacities to 4 630 lb/hr (2 100 kg/hr)



Description

Armstrong's AB-3000 Bimetallic Steam Trap operates by the effect that rising temperature has on bimetallic elements. It adjusts itself to changing conditions, as the increasing pressure on the valve is compensated by the curving of the bimetallic elements caused by the increasing temperature.

Armstrong's AB-3000 has a sealed, stainless steel body that is lightweight, compact and highly resistant to corrosion. The AB-3000 is repairable (body and cap can be unscrewed). It is piped through the Armstrong 360° Universal Connector or Trap Valve Station (TVS). This makes it easy to install and replace, as the trap can be removed while the connector remains in-line. The result is savings in labor cost and increasing in flexibility, as other trap types (Inverted Bucket, Thermostatic and Thermodynamic) can be installed on the same connector.



Maximum allowable pressure

(vessel design): 406 psig @ 650°F (28 barg @ 343°C)

Maximum operating pressure: 319 psig (22 barg)
Maximum back pressure: 99% of inlet pressure



Screwed BSPT and NPT

Socketweld

Materials

Body: ASTM - A240 304L
Standard connector: Stainless steel - 304
Valve: Chrome steel - 440F
Seat: 303 Stainless steel
Elements: Nickel plated
Strainer: 304 Stainless steel

Specification

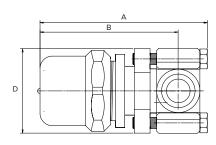
Bimetallic repairable steam trap, type AB-3000 in stainless steel, with integral strainer. Piped through 360° Universal Connector or Trap Valve Station (TVS). Maximum allowable back pressure 99% of inlet pressure.

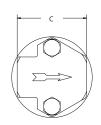
How to order

Specify:

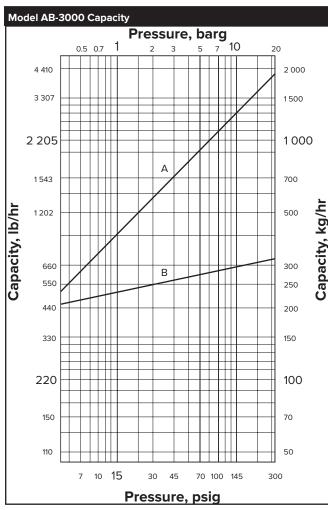
- Size and type of pipe connection.
- Maximum working pressure that will be encountered
- · Maximum condensate load

Model AB-3000 Trap						
	in	mm				
Pipe Connections	3/8, 1/2, 3/4, 1	10, 15, 20, 25				
"A" Length w/ Connector	5-7/16	138				
"B" & to Top of Cap	4-1/2	115				
"C" Face-to-Face (screwed & SW)	2-3/8, 2-3/8, N/A	60, 60, N/A				
"D" Trap Diameter	2-3/16	70				
Weight lb (kg) (screwed & SW)	4 (2)					









A = Cold Water B = Hot Condensate



SH-4000 Series Bimetallic Steam Traps

All Stainless Steel

For Pressures to 1 245 psig (86 barg)...Capacities to 6 000 lb/hr (2 722 kg/hr)

Description

Armstrong's SH-4000 Series Bimetallic Steam Trap is the ideal design for applications involving superheated steam.

During start-up, the bimetallic mechanism is fully open and allows large volumes of non-condensable gases and condensate to be removed from the system. As the system reaches saturated steam conditions, the mechanism begins to close preventing any live steam loss. The superheat during normal operating steam conditions keep the valve closed to ensure long service life.

In the event that operating conditions change and condensate forms at the steam trap inlet, the cooling effect allows the bimetallic mechanism to open and discharge any accumulation. The valve quickly closes once normal operating conditions return.

The SH-4000 consists of an investment cast, stainless steel body that is compact and highly resistant to harsh, corrosive environments. The integral mounting flange is compatible with the Armstrong IS-4, 4-bolt, Class 900, connector making for labor savings and easy steam trap replacement.

Maximum Operating Conditions

Maximum allowable pressure (vessel design): 1 245 psig @ 900°F (86 barg @ 482°C)

Maximum operating pressure:

 SH-4009L
 650 psig @ 900°F (45 barg @ 482°C)

 SH-4009H
 900 psig @ 900°F (62 barg @ 482°C)

 SH-4015
 1 245 psig @ 900°F (86 barg @ 482°C)

Suggested minimum operating pressure: SH-4009L and SH-4009H 200 psig (14 barg) SH-4015 650 psig (45 barg)

Materials and Weight

Body: ASTM A351 Gr. CF8M

Valve & Seat Elements: Titanium

Ni-Cr

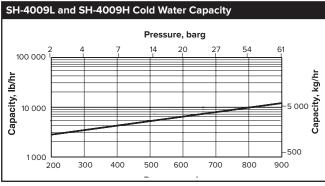
Stainless Steel
Spiral Wound Gasket: Stainless Steel
Bolts: ASTM A193 B7
Weight: 3.75 lbs (1.7 kg)

Specification

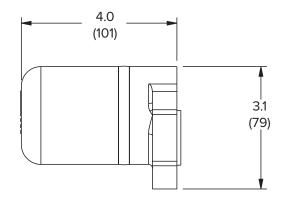
Steam traps shall be a bimetallic style designed for superheated steam applications. The steam trap body shall be tamperproof, investment cast stainless steel A351 Gr. CF8M. The mechanism shall consist of a stacked nickel-chrome bimetal operator with titanium valve and seat. The gaskets shall be captured stainless steel spiral wound. The steam trap shall be compatible with the 4-bolt universal connector technology.

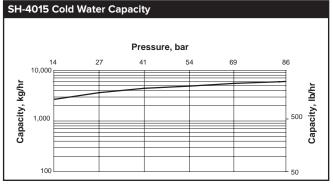
How to Order

Specify model number
Maximum working pressure and temperature









Note: Cold water capacity for start-up loads only. When superheat present, there will be minimal condensate.

TT Series Thermostatic Steam Traps

All Stainless Steel

For Pressures to 300 psig (20 barg)...Capacities to 3 450 lb/hr (1 568 kg/hr)





Description

The balanced pressure bellows thermostatic steam trap has a sealed, stainless-steel body that is lightweight, compact and highly resistant to corrosion. The cage, bellows, valve and seat are all assembled into a precisely calibrated operating unit that ensures positive opening and closing action at slightly below steam temperature. The unique, stainless-steel construction is smaller and much lighter than comparable cast iron, brass or steel traps. TTF-1 is available with straight-thru or right angle connections. TT-2000 with the 360° universal stainless steel connector comes with either a standard connector or the IS-2 connector with integral strainer.

NOTE: Also can be used as a thermostatic air vent (Reference TTF Series Thermostatic Air Vents page 464).

Specification

Thermostatic steam trap, type ... in stainless steel.

How to Order

Specify:

- Model number
- · Size and type of pipe connection
- · Connector type (TT-2000)

Connections

3/8", 1/2", 3/4" (10 mm, 15 mm, 20 mm) 1" (25 mm) IS-2 connector only Socketweld

Materials

Body: 304L stainless steel

Bellows: Stainless steel and bronze with phosphor-

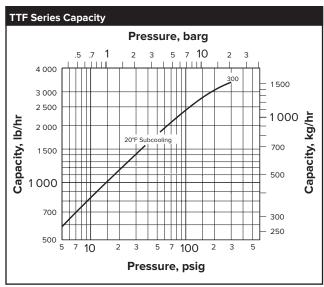
bronze bellows, caged in stainless steel

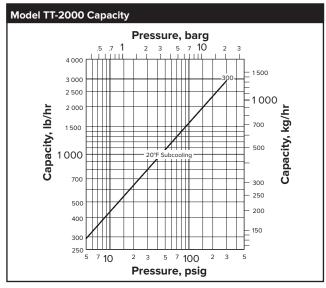
Flange ASTM A105 Zinc plated

Connector: 304 stainless steel (TT-2000)

For a fully detailed certified drawing, refer to:

Standard Connector CD #1018 IS-2 Connector CD #1117





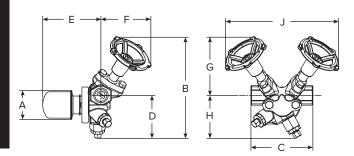
Model	TTF-1	TTF-1R	TT-2000						
Design		We	elded						
Connections		wed d BSPT)	Screwed (NPT and BSPT), Socketweld and Flanged						
Material									
Body		ASTM A	240 - 304L						
Valve		Br	onze						
Seat		Stainle	ess steel						
Thermostatic air vent	Standard stainless s	Standard stainless steel & bronze w/phosphor bronze bellows caged in stainless steel							
Optional: All stainless steel thermostatic air vent									
Connector									
Standard	_	_	Stainless steel - 304						
IS-2 w/integral strainer	_	_	Stainless steel - 304 w/20x20 mesh 304 SS screen						
TVS 4000	with sc		51 Gr. CF8M olowdown valve—stainless steel						
Maximum Operating Conditions									
Maximum allowable pressure (vessel design)		300 psig @ 450°F	= (20 barg @ 232°C)						
Maximum operating pressure		300 psi	g (20 barg)						
Maximum operating temperature bellows		422°F	(217°C)						

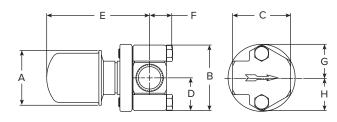


TT Series Thermostatic Steam Traps

All Stainless Steel

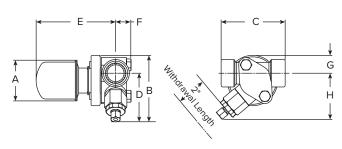
For Pressures to 300 psig (20 barg)...Capacities to 3 450 lb/hr (1 568 kg/hr)



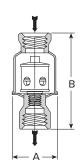


Series TT-2000 With TVS 4000 Trap Valve Station

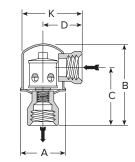
Series TT-2000 With Standard Connector



Series TT-2000 With Integral Strainer and Blowdown Valve



Series TTF-1 Trap



Series TTF-1R Trap

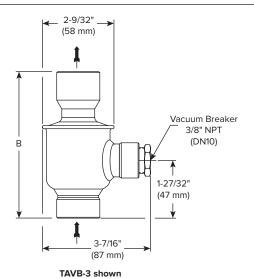
TT-2000 Series Steam Trap												
Model No.	TT-2000											
Model No.	Standard (Connector	IS-2 C	Connector W	ith Integral S	trainer	TVS 4000 Connector					
Dina Cannactions	in	mm	in	mm	in	mm	in	mm				
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20	1/2, 3/4	15, 20	1	25	1/2, 3/4 1	5, 20				
"A" Trap Diameter	2-1/4	57	2-1/4	57	2-1/4	57	2-1/4	57				
"B" Total Height	2-11/16	68	3-5/8	92	3-5/8	92	7-13/16	198				
"C" Face-to-Face	2-3/8	60	3-1/2	89	4	101	4-3/4	120				
"D" Connection & to Bottom	1-3/8	46	2-5/8	67	2-5/8	67	3-1/4	83				
"E" Connection ℚ to Outside of Trap	4-1/4	107	4-3/4	120	4-15/16	125	4-1/2	115				
"F" Connection & to Front of Connector	13/16	20	7/8	22	7/8	22	3-7/8	98				
"G" Connection & to Top	1-3/8	46	1	25	1	25	4-1/2	114				
"H" Connection & to Bottom of Connector	1-3/8	46	2-1/2	64	2-1/2	64	3-1/4	83				
"J" Width Across Handwheels (valve open)	_	_	_	_	_	_	8-11/16	221				
Test Port Connection	_	_	_	_	_	_	1/4 NPT	6				
Trap Only Weight, lb (kg)				1-1/2	(0.70)							
Trap and Connector Weight, lb (kg)	3.2	(7)		3.4	(7.5)		8 (3	3.6)				

TTF-1 Series Steam Trap									
Model No.			F-1 u Connectio	nn.	TTF-1R Right-Angle Connection				
Model No.	in	mm	in	mm	in	mm	in	mm	
Pipe Connections	1/2	15	3/4	20	1/2	15	3/4	20	
"A" Trap Diameter	2-1/4	57	2-1/4	57	2-1/4	57	2-1/4	57	
"B" Total Height	4-1/2	114	4-11/16	119	3-3/4	97	3-15/16	100	
"C" Face-to-Face		_	_	_	2-5/8	67	2-13/16	71	
"D" Connection Q to Bottom	_	_	_	_	1-15/16	49	1-7/8	48	
"K" Inlet to Outside of Trap		_	_	_	3-1/16	78	3	76	
Trap Only Weight, lb (kg)	3/4	3/4 (0.4)		1 (0.5)		(0.4)	1 (0.5)		

Stainless Steel Thermostatic Air Vent/Vacuum Breaker

For Pressures to 150 psig (10 barg)...Capacities to 55 scfm







The Armstrong TAVB is a combination thermostatic air vent/vacuum breaker that is ideally suited for steam-filled vessels with modulating controls. The TAVB will vent air and other non-condensables from vessels such as shell and tube heat exchangers, jacketed kettles and steam coils during their operation. It will also break the vacuum that forms during steam control modulation.

This balanced pressure air vent responds to the pressure-temperature curve of steam, and the soft-seated vacuum breaker responds to $2^{\rm H}\,{}_2{\rm O}$ of vacuum.

Maximum allowable pressure:
 Maximum allowable temperature:
 Maximum working pressure:
 Mosig (20 barg)
 150 psig (10 barg)

All stainless steel welded construction

NPT connections

Armstrong thermostatic air vents should be installed at the highest point on a steam chamber, with the air vent located above the chamber. This will minimize the possibility of any liquid carryover, and air can be vented to atmosphere without a drain line.

For a fully detailed certified drawing, refer to CD #1260.

Features

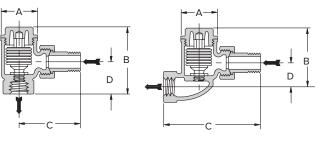
Physical Data									
Mo	del No.	TAV	/B-2	TAV	/B-3				
IVIC	del No.	in	mm	in	mm				
Dina Connections	Thermostatic Air Vent	1/2	15	3/4	20				
Pipe Connections	Vacuum Breaker	3/8	9.5	3/8	9.5				
"A" (Diameter)		2-1/4	57	2-1/4 57					
"B" (Height)		4-5/8 117		4-11/16	119				
"C" (& Inlet to Face of Va	cuum Breaker)	2-1/8	54	2-1/8 54					
Weight lb (kg)		1 (0	.45)	1-1/4	(0.57)				
Maximum Allowable Pres	sure (Vessel Design)		300 psig @ 365°F	(20 barg @ 185°C)					
Maximum Operating Pres	sure	150 psig (10 barg)							
Discharge Orifice Size		3/16"							

List of Materials	
Name of Part	Material
Body	304-L Stainless steel
Connections	304 Stainless steel
Balanced Pressure Thermostatic Air Vent	Stainless steel and bronze with phosphor-bronze bellows, entire unit caged in stainless steel
Gasket	Copper clad non-asbestos
Vacuum Breaker Body	303 Stainless steel
Valve	Stainless steel
Spring	302 Stainless steel
"O" Ring	EPDM
Screen	Stainless steel



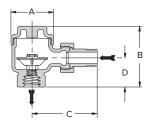
TS-2/TS-3 Radiator Traps

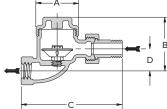
For Pressures to 65 psig (4.5 barg)...Capacities to 1 600 lb/hr (726 kg)



TS-2 Trap Angle Type

TS-2 Trap Straight Type





TS-3 Trap Angle Type

TS-3 Trap Straight Type

Armstrong Series TS radiator traps are offered in both angle and straight patterns. The TS-2 has a balanced pressure thermostatic element with a high quality multiple-convolution bellows. It's ideal for draining equipment such as steam radiators and convectors, small heat exchangers, unit heaters and steam air vents. The TS-2 comes with a strong, cast bronze body and a stainless seat. The valve and seat are renewable in-line.

The TS-3 is a heavy duty, wafer type trap for the drainage of all types of steam radiators and convectors. Its wafer design is well suited to systems prone to water hammer, which may damage conventional bellows type units. The TS-3 is repairable in-line and has an all-stainless steel wafer element.

Materials

Bronze, ASTM B62 Cap: Body: Bronze, ASTM B62 Brass, ASTM B584 Union nipple:

Valve:

Model TS-2 Brass

Model TS-3: Stainless steel Valve seat: Stainless steel

Element:

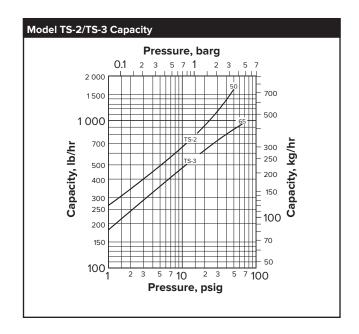
Model TS-2: Phosphor-bronze bellows Model TS-3:

T-316 SS Wafer w/T-304 SS Housing

For a fully detailed certified drawing, refer to:

TS-2 CDY #1045 TS-3 CDY #1046





TS Series Radiator Tra	ps Phy	sical l	Data																	
Model	TS-2					TS-3														
Pattern	Angle Straight					An	gle					Strai	ght							
Dina Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1/2	15	3/4	20	1/2	15	3/4	20	1	25	1/2	15	3/4	20	1	25
"A" Diameter	1-5/8	41	1-5/8	41	1-5/8	41	1-5/8	41	2	50	2	50	2-3/8	86	2	50	2	50	2-3/8	86
"B" Height	2-15/16	75	3	76	2-11/16	68	2-7/8	73	2-7/8	73	3-5/8	92	3-7/8	98	2-5/8	61	3-3/8	86	3-1/2	89
"C"	2-9/16	65	2-7/8	73	4	102	4-1/2	114	3-1/8	79	3-1/2	89	4-1/8	105	4-7/8	124	5-1/4	133	6-1/2	165
"D"	1-3/8	35	1-5/8	41	1-1/8	28	1-5/16	33	1-3/8	35	1-5/8	41	2	50	1-1/8	28	1-3/8	35	1-5/8	41
Weight, Ib (kg)	1-1/2 (0	0.68)	1-3/4	(0.79)	1-1/2 (0).68)	2 (0	.91)	1-1/2	(0.68)	2 (0).91)	2-1/2	2 (1.1)	1-1/2 (0.68) 2-1/4 (1) 3 (1.4)				.4)	
Maximum Allowable Pressure (Vessel Design)		50 psig @ 300°F (3.4 barg @ 149°C)					65 psig @ 315°F (4.5 barg @ 157°C)													
Pressure, psig (barg)				50	(3.4)				65 (4.5)											
Vacuum Ratings				25" N	lercury								1	l0" Me	rcury					

TC Series Clean Steam Thermostatic Traps

For Clean Steam Systems

For Pressures to 120 psig (8 barg)...Capacities to 3 775 lb/hr (1 712 kg/hr)



1-3/16"

(31 mm)

Armstrong offers a complete range of T-316L stainless steel clean steam thermostatic traps to handle the special requirements of clean steam systems. Different body configurations allow for choice of piping and ease of cleaning.

The thermostatic design is free-draining and can operate close to steam temperature at any given pressure.

Features

- Constructed of 316L stainless steel for corrosion resistance
- · Highly polished for cleanability
- Self-draining to minimize contamination
- · Compact and lightweight
- Easy to install
- · Provide easy disassembly for cleaning

Typical Applications

- · Fermentors
- · Sterilizers/autoclaves
- Process piping Block and bleed
- · Bioreactors
- · CIP/SIP systems
- · Equipment sterilization
- Sterile barriers

How to Order:

Specify:

- Model number
- · Pipe connection size
- End connection type

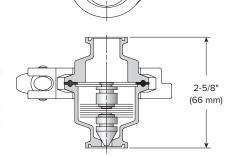
Example:

TC-C, 1/2" sanitary end connections.



For a fully detailed certified drawing, refer to:

TC-C CD #1161 TC-R CD #1162 TC-S CD #1163



2-7/8"

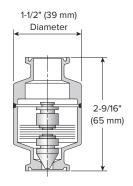
(74 mm)

2"

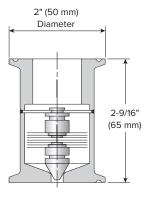
(50 mm)

Model TC-C Clamp With Sanitary Body Clamp

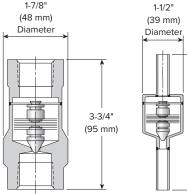
1/2" (15 mm), 3/4" (20 mm), 1" (25 mm) Sanitary End Connections



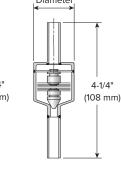
Model TC-S Sealed 1/2" (15 mm), 3/4" (20 mm) Sanitary End Connections



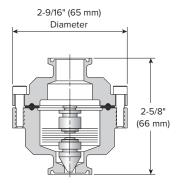
Model TC-S Sealed 1" (25 mm) 1-1/2" (40 mm) Sanitary End Connections



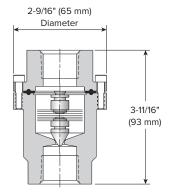
Model TC-S Sealed 1/2" (15 mm), 3/4" (20 mm) Threaded End Connections



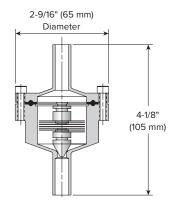
Model TC-S Sealed 1/2" (15 mm), 3/4" (20 mm) **Tube End Connections**



Model TC-R Repairable With Bolted Body and Cap 1/2" (15 mm), 3/4" (20 mm), 1" (25 mm), 1-1/2" (40 mm) Sanitary End Connections



Model TC-R Repairable With Bolted Body and Cap 1/2" (15 mm), 3/4" (20 mm) Threaded End Connections



Model TC-R Repairable With Bolted Body and Cap 1/2" (15 mm), 3/4" (20 mm) **Tube End Connections**



TC Series Clean Steam Thermostatic Traps

For Clean Steam Systems

For Pressures to 120 psig (8 barg)...Capacities to 3 775 lb/hr (1 712 kg/hr)

Materials

Model	TC-C Clamp	TC-R Repairable	TC-S Sealed				
Cap and body		ASTM A479 316L					
Bellows		316L Stainless S	teel				
Body gasket	Vite	on®	_				
Retainer	Stainless Steel						
Clamp	Stainless Steel	_	_				
Screws	_	Stainless Steel	_				
Finish	20 μir below and 15 electro to 30 μ	sh to 1 Ra or inside, 50 grit	Mechanical finish to 63 μin Ra interior and 32 μin Ra exterior				

NOTE: µin = microinches

Physical Data

Model	TC-C Clamp	TC-R Repairable	TC-S Sealed
Maximum Allowable Pressure (Vessel Design)		O psig B barg)	150 psig (10 barg)
Maximum Allowable Temperature	350°	F (177°C)	366°F (186°C)
Maximum Operating Pressure		D psig barg)	120 psig (8.3 barg)
Weight lb (kg)	1-1/4 (0.57)	1-1/2 (0.68)	3/4 (0.34)

TC Se	ries Cle	an Steam Tra	o Capacities		
noia	bora	10°F (5.6°C)	Subcool	20°F (11.2	°C) Subcool
psig	barg	lb/hr	kg/hr	lb/hr	kg/hr
5	0.35	180	82	320	145
10	0.70	360	163	645	293
20	1.4	676	307	1 108	503
30	2.1	1 009	458	1563	709
40	2.8	1 236	561	1830	830
50	3.5	1542	699	2 016	915
60	4.1	1845	837	2 505	1 136
70	4.8	2 037	924	2 668	1 210
80	5.5	2 360	1 071	2 990	1356
90	6.2	2 460	1 116	3 237	1 468
100	6.9	2 547	1 155	3 450	1 565
110	7.6	2 610	1 184	3 640	1 651
120	8.3	2 660	1206	3 775	1 712

Armstrong Simplifies Your Tracing Line Systems



Designed to simplify and supply all the components (steam traps, manifolds, valves, etc.) necessary for your drip and tracer line applications, Armstrong's new Steam Distribution and Condensate Collection Manifolds bring all components together to reduce installation costs and provide a compact, easily accessible, centrally located assembly.

Armstrong's manifold series includes four different configurations, a Steam Distribution (MSD/SMSD), and a Condensate Collection Assembly (CCA/CCAF). As an option, the condensate manifolds can offer freeze protection.

In either case, you will save the expensive headaches of trying to fabricate in-house. What's more, your manifold will be backed by the famous Armstrong quality—and a standard three-year limited warranty.

routine maintenance is faster.

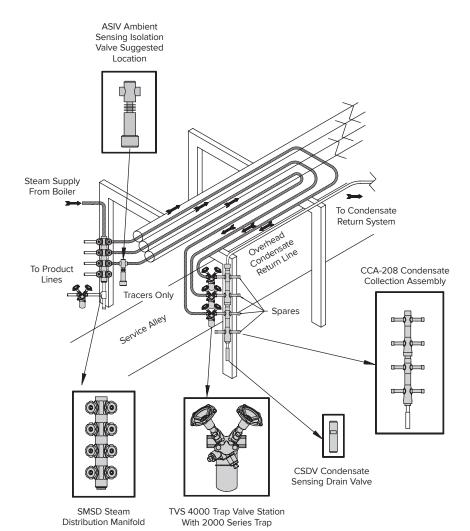
Condensate Collection Manifolds

To make industry's trapping and valving more efficient, Armstrong combines its stainless steel steam trap valve stations with manifolds into a package called the Condensate Collection Assembly (CCA). This prepackaged assembly offers many great benefits—cost savings in installation, design flexibility, and reduced purchasing time. CCAF would also include syphon tube freeze protection.

Whatever your condensate collection or steam distribution needs, Armstrong has the manifold for savings over the long term.

Steam Distribution Manifolds

As a Steam Distribution Assembly (MSD/SMSD), the manifold places all steam supply valves in one location. Standardizing components and centralizing their location simplifies installation, cutting costs from the beginning. You also save because



Shown are typical locations for Armstrong manifolds. The many manifolds in chemical/petrochemical plants consume valuable floor space and often block movement among the units. Operating costs are high, and installation requires expensive custom fabrication on site. Clearly, a prefabricated manifold permitting standardization of components offers substantial savings over conventional units. Shaded products are available from Armstrong. Call or consult your Armstrong Representative if additional product details are required.



Armstrong The Proof Is in the Piston

Many of Armstrong's manifolds utilize the piston valve because of its years of excellent performance in steam systems all over the world. The proof of Armstrong's long service life for manifolds...is in the piston.

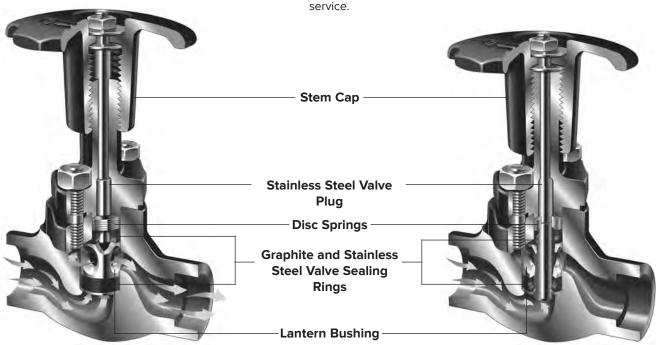
All types of valves—plug valves, gate valves, piston valves and even ball valves—have been summoned for duty in steam service. Due to its excellent sealing characteristics in steam service, and because it has no gland packing, the piston valve is frequently selected for steam systems.

People who have used it over the past 90 years can testify that leakage to atmosphere is extremely rare, even without any maintenance. The elastic contact between piston and valve sealing rings provides a perfect tightness, both in-line and to atmosphere.

Steam system valves, whatever their design, are used to isolate steam and condensate lines or when a faulty steam trap needs to be removed from the line. This means the valves stay in the open position for long periods and are nearly always in contact with the atmosphere. It is not surprising, therefore, that when the valves need to be closed, they refer that when the valves need to be closed, they refer the Piston Valve

can often prove difficult to operate. Our experience and the demands from end users for energy efficiency have led us to a sealing system designed especially for steam service.

Armstrong Steam Distribution Manifolds (MSD/SMSD) and TVS 4000 Trap Valve Stations incorporate advanced piston sealing technology for safer, longer lasting steam isolation



Open Position

- Dual sealing action. The piston valve is a seatless valve that includes two graphite and stainless steel valve sealing rings that seal the stem and function as a seat. This combination provides long-term protection against leaks to the atmosphere and downstream piping.
- Self-cleaning action. Stainless steel piston slides without rotating between the two valve sealing rings, preventing dirt from damaging the surfaces
- Sealing integrity. Flexible disc springs automatically provide leak tightness by exerting pressure, which keeps the upper and lower valve sealing rings compressed at all times. Sealing tightness is ensured by the compression of the sealing rings against the

Closed Position

piston and valve body. This combination of disc springs and dual valve seal rings protects against expansion and contraction due to heating and cooling. This ensures dependable operation, even after years of service.

- Protected valve stem. The valve stem and sealing surfaces are completely protected from dirt and corrosion by the stem cap, whether in an open or closed position.
- In-line repairability. All sealing valve components may be easily replaced in-line.
- Long-term operation. Piston valve design ensures actuation even after many years without operation.

Steam Distribution Manifold (MSD/SMSD)

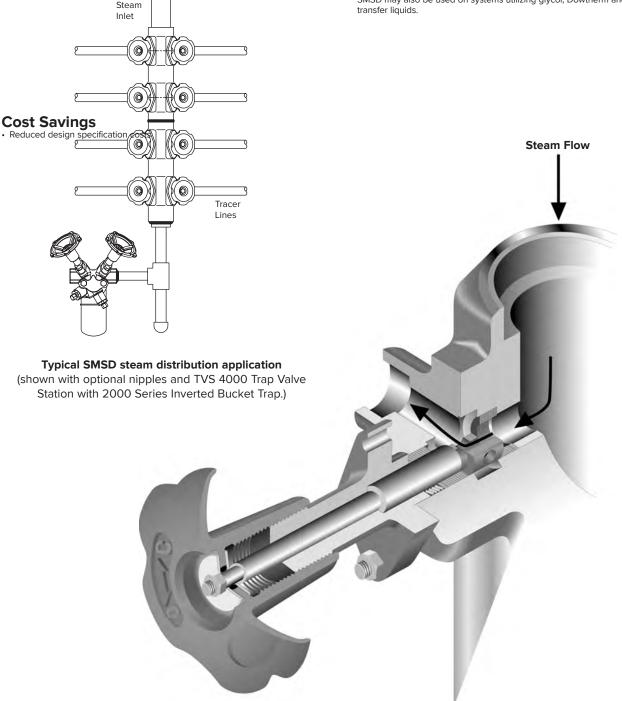


As Steam Distribution Assemblies (MSD/SMSD), the manifolds place all steam supply valves in one location. Standardizing components and centralizing their location simplifies installation while providing cost savings. You also save because routine maintenance is faster. Insulation can also be provided...and can be a major savings in most installations.

- Prefabrication vs. field assembly for easy installation
- · Reduced shipping and field handling costs
- Lower long-term maintenance and operating costs
- 3-year guarantee

Design Flexibility

- · Dimensional consistency
- Space savings
- Insulation package available SMSD may also be used on systems utilizing glycol, Dowtherm and other heat transfer liquids.



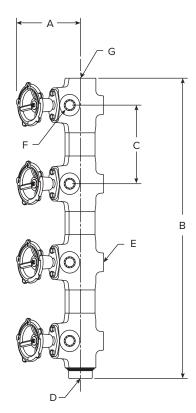


Armstrong[®] Steam Distribution Manifold (MSD/SMSD)

Physical Data												
			MSD Se	eries					SMSD S	eries		
Model	MSD-0	04	MSD-0	38	MSD-	12	SMSD-	04	SMSD	-08	SMSD-	-12
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
"A" (Open Position)	8	203	8	203	8	203	8	203	8	203	8	203
"B" Height	11-1/2	292	24-1/4	615	37-1/8	943	10-1/4	260	19-3/4	501	29-1/4	743
"С" Ҿ to Ҿ	6-3/8	162	6-3/8	162	6-3/8	162	4-3/4	120	4-3/4	120	4-3/4	120
"D" Blowdown Connection	3/4 SW	20	3/4 SW	20	3/4 SW	20	3/4 SW	20	3/4 SW	20	3/4 SW	20
"E" Number of Holes for Mounting (M14)	2	2	4	4	6	6	2	2	4	4	6	6
"G" Inlet	1-1/2 SW	40	1-1/2 SW	40	1-1/2 SW	40	1-1/2 SW	40	1-1/2 SW	40	1-1/2 SW	40
"F" Outlet*	1/2	15	1/2	15	1/2	15	1/2	15	1/2	15	1/2	15
Weight, lb (kg)	21 (10	21 (10) 46 (21) 67 (30)			D)	20 (9) 40 (18)			59 (2	7)		
Maximum Operating Pressure					164 psig (32	barg) @	752°F (40	0°C)				

^{*3/4&}quot; (20 mm) available - contact factory.

List of Materials	
Name	Material
Manifold Body	ASTM A105N/A-350 LF2 Forged Steel
Handwheel	Ductile iron
Bonnet	ASTM A351 Gr. CF8M
Spring Washer	Stainless steel
Bonnet, Bolts	DIN 933, Gr. 8.8 per DIN 267
Piston & Stem	Stainless steel—17-4PH
Valve Sealing Rings	Expanded graphite & stainless steel



Steam Distribution Manifold



Steam Distribution Manifold
With TVS 4000, Inverted Bucket Drip Trap and Optional
Stand





Armstrong combines its Trap Valve Stations (TVS) with manifolds into a package called the Condensate Collection Assembly (CCA). This prepackaged assembly offers many great benefits—cost savings in assembly, design flexibility and reduced purchasing and design time. The CCA with TVS 4000 Trap Valve Station and 2000 Series Inverted Bucket Traps is guaranteed for 3 years.

Cost Savings

This preassembled concept offers tremendous savings by reducing multiple component purchases that cause additional purchase order monitoring and shipping costs. Other savings include far less labor time required for field assembly.

This modular forged steel body design provides quick assembly/delivery, reducing overall project costs.

- Minimal welding vs complete manifold fabrication
- · Eliminates multiple component purchases
- Reduced design specification costs
- · Prefabrication vs. field assembly for easy installation
- · Reduced shipping and field handling costs
- · Lower long-term maintenance and operating costs
- · 3-year guarantee

Design Flexibility

Armstrong can meet virtually any design parameter, including dimensional consistency, with your choice of socketweld or threaded connections. Armstrong inverted bucket, thermostatic, thermostatic wafer, bimetallic or disc steam traps can be provided or any other manufacturer's two-bolt steam trap can be used. If you require a specific piping arrangement, Armstrong can offer the flexibility to meet your specifications.

Materials

Manifold body:

ASTM A105N/A-350 LF2 Forged Steel

Removable Insulation Package

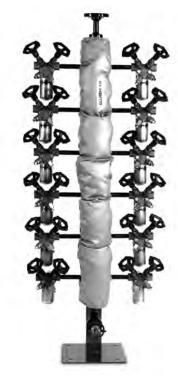
A removable insulation package is available for all steam and condensate manifolds.

- Inexpensive
- Quick to install
- Removable for maintenance
- · Reusable after maintenance
- · Weatherproof
- Formed to cover all manifold elements
- Strong, durable cover
- Available to fit all manifold sizes

Freeze Protection Package (CCAF)-Optional

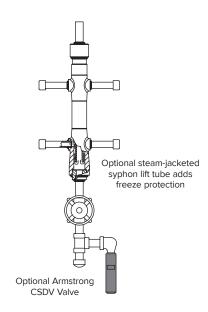
A manifold assembly for more efficient condensate return has another benefit—freeze protection. Armstrong's innovative manifold design actually serves as a heat station, heating one or more traps if the steam supply is interrupted or shut off to the traps. The protection is accomplished as long as one trap continues to discharge into the manifold. The manifold's internal syphon tube creates a water seal, which contains the flash steam from the discharge of the live trap. This allows radiant heat to protect shut-off traps from freezing.

An optional freeze protection valve package senses condensate temperature. When this device opens, it drains condensate from the manifold assembly, thus providing further freeze protection.



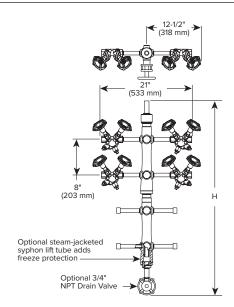
CCAF 212 Condensate Collection Assembly

(Shown with TVS 4000 Trap Valve Station with 2000 Series Inverted Bucket all stainless steel steam traps with optional removable insulation package including nipples, drain valve and stand.)



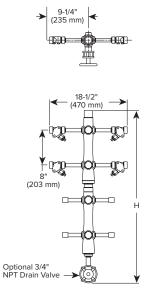


Armstrong® Pre-Assembled...Condensate Collection Assembly (CCA)



CCAF Condensate Collection Assembly with TVS 4000 Trap Valve Station, Optional Freeze Protection and Drain Valve.

Available with Armstrong's inverted bucket, disc, thermostatic, thermostatic wafer or bimetallic steam traps. Any manufacturer's 2-bolt steam trap can also be applied to Armstrong's trap connectors.



CCA Condensate Collection Assembly With IS-2 Connectors with Strainer, Blowdown Valve and Optional Drain Valve

Available with Armstrong's inverted bucket, disc, thermostatic, thermostatic wafer or bimetallic steam traps. Any manufacturer's 2-bolt steam trap can also be applied to Armstrong's trap connectors.

Physical Data										
Model	CCA	-204	CCA	-206	CCA	-208	CCA	-210	CCA	-212
" <u></u> "	in	mm	in	mm	in	mm	in	mm	in	mm
	23-1/8	587	31-1/8	790	39-1/8	994	47-1/8	1 197	55-1/8	1 400
Maximum Allowable Pressure		604 psig @ 800°F (42 barg @ 427°C)								

Physical Data										
Model	CCAF	-204	CCAF	-206	CCAF	-208	CCA	-210	CCAI	F-212
" 山 "	in	mm	in	mm	in	mm	in	mm	in	mm
"	27-5/16	694	35-5/16	897	43-5/16	1100	51-5/16	1303	59-5/16	1506
Maximum Allowable Pressure				604 ps	ig @ 800°F	(42 barg @	427°C)			

How to Order Manifold Packages

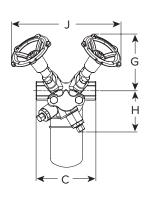
CCA	208	2NPT	6PE	3DVN	TVS 4000 SCH80
Manifold Model	Number of Take-offs Per Manifold	Connection Size Take-offs, NPS in (mm)	Connection Size Top, NPS in (mm)	Connection Bottom, NPS in (mm)	Trap Valve Station
MSD Steam Distribution Manifold	04 08		6SW = 1-1/2 (40) SW ¹ 6FW150 = 1-1/2 (40) 150# RF Flange 6FW300 = 1-1/2 (40) 300# RF	3SW = 3/4 (20) SW ¹ 3NPT = 3/4 (20) NPTF	
SMSD Small Steam Distribution Manifold	12	2NPT = 1/2 (15) NPTF ¹ 2SW = 1/2 (15) SW ¹	Flange 8FW150 = 2 (50) 150# RF Flange 8FW300 = 2 (50) 300# RF Flange	3WD = 3/4 (20) Welded Dripleg ² 3TD = 3/4 (20) Threaded Dripleg ²	TVS 4000 IS2
CCA Condensate Collection Assembly	204 206	3NPT = 3/4 (20) NPTF 3SW = 3/4 (20) Socketweld	6PE = 1-1/2 (40) Plain End ¹ 6FW150 = 1-1/2 (40) 150# RF Flange	3NPT = 3/4 (20) NPTM ¹ 3DVN = 3/4 (20) Drain Valve NPTM/	with BD IS2 Standard None
CCAF Condensate Collection Assembly Freeze Protection	208 210 212		3PE = 3/4 (20) Plain end ¹ 3NPT = 3/4 (20) NPTM 3FW150 = 3/4 (20) 150# Flange	NPTM 3DVS = 3/4 (20) Drain Valve SW/ NPTM	

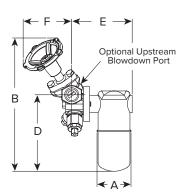
- 1. Armstrong stocks manifold cores (less nipples, drain valves and trap stations) in these connections.
- 2. Must pick this bottom connection to use trap station (TVS 4000 only choice) and trap on MSD and SMSD.
- 3. Nipples connecting manifold to trap station can be Schedule 80 (standard) or schedule 160 (optional).

TVS 4000 Series Stainless Steel Trap Valve Station

For Pressures to 650 psig (45 barg)...Capacities to 1 300 lb/hr (590 kg/hr) (Using 2000 Series Inverted Bucket Steam Traps)

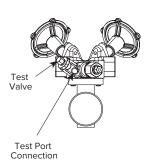




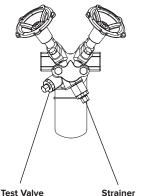


Model TVS 4000 With 2000 Series SS Trap Front View

Model TVS 4000 With 2000 Series SS Trap Side View



Model TVS 4000 With 2000 Series SS Trap Bottom View



Test Valve
Used to test and
evaluate trap
operation

Strainer Blowdown Valve

Same principle. Different package with two piston-style isolation valves, test valve and integral stainless steel strainer with blowdown valve. Now the energy-saving performance and reliability of the inverted bucket steam trap are available in a versatile new package. You'll still enjoy all the familiar benefits. And the same efficient condensate drainage from virtually every kind of steam-using equipment. What you'll find new are all the benefits of a piston valve integrated into the same space-saving package.

Materials—TVS 4000 Connector

Connector: ASTM A351 Gr. CF8M
Strainer screen: Stainless steel
Screen retainer: Stainless steel
Gasket: Stainless steel
Retainer unit: Stainless steel
Test valve: Stainless steel
Blowdown valve: Stainless steel

Isolation Valve Components

 Handwheel:
 Ductile iron

 Nut:
 Stainless steel

 Stem, washers:
 Stainless steel

 Bonnet:
 ASTM A351 Gr. CF8M

 Bonnet, bolts:
 DIN933, Gr. 8.8 per DIN267

Valve plug: Stainless steel Disc springs: Stainless steel

Valve sealing rings: Graphite and stainless steel

Lantern bushing: Stainless steel Valve washers: Stainless steel

Materials—Series 2000 Traps

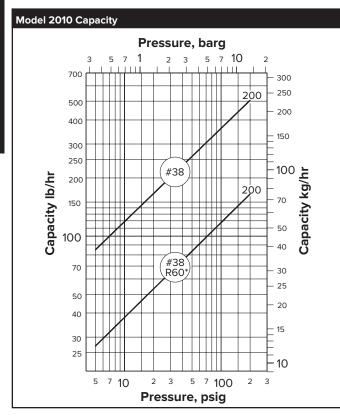
Body: ASTM A240 Gr. 304L
Internals: All stainless steel—304
Valve and seat: Stainless steel—17-4PH

Model No.	20	10	20)11	20	22
Dina Connections	in	mm	in	mm	in	mm
Pipe Connections	3/8, 1/2, 3/4	10, 15, 20	3/8, 1/2, 3/4	10, 15, 20	3/8, 1/2, 3/4	10, 15, 20
"A" Trap Diameter	2-11/16	68	2-11/16	68	3-7/8	98
"B" Height (Valve Open)	8	203	10-1/2	268	12-1/2	318
"C" Face to Face	4-3/4	120	4-3/4	120	4-3/4	120
"D" Connection Q to Bottom	4-3/4	120	6	154	8	203
"E" Connection & to Outside of Trap	4-1/2	114	4-13/16	122	5-7/8	149
"F" Connection & to Front of Handwheel (Valve Open)	3-1/2	89	3-7/8	98	3-7/8	98
"G" Connection & to Top of Handwheel (Valve Open)	3-1/4	83	4-1/2	114	4-1/2	114
"H" Connection & to Bottom of Connector	1-7/8	47	3-1/4	83	3-1/4	83
"J" Width Across Handwheels (Valve Open)	9-1/4	235	8-3/4	222	8-3/4	222
Test Port Connection	1/4 NPT	6	1/4 NPT	6	1/4 NPT	6
Weight, lb (kg)	9	(4)	9-1/2	(4.3)	12 (5.4)
Maximum Operating Pressure (Trap)	200 psig	(14 barg)	400 psig	(28 barg)	650 psig	(45 barg)
Maximum Allowable Pressure (Trap)	400 psig (28 barg) @ 750°E (399°C) 650 psig			@ 600°F @ 315°C)		



TVS 4000 Series Stainless Steel Trap Valve Station

For Pressures to 650 psig (45 barg)...Capacities to 1 300 lb/hr (590 kg/hr) (Using 2000 Series Inverted Bucket Steam Traps)



*NOTE: Because the orifice is located at the top, inverted bucket steam traps handle dirt and scale better than other types of traps. However, in applications where extremely dirty conditions exist, care should be exercised in the use of all types of restricted-orifice, reduced-capacity traps.

Options

Insu-Pak™

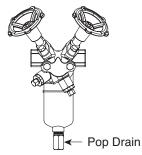
Now you can insulate the in-line traps in your plant without complicating regular trap maintenance. Insu-Pak, a simple reusable insulation package, cuts the time and cost of in-field installation because it goes on in a snap. And it comes off just as easily. The Insu-Pak can prevent trap freeze-up when used with a properly designed condensate manifold. Designed for use with Model 2010 and Model 2011 traps.

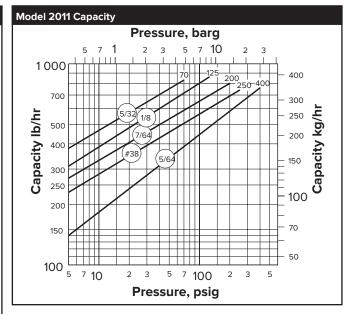


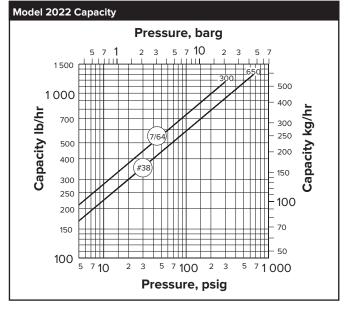
Simple but effective against freeze-up. Properly installed and maintained at low points in your system, the simple, pressure-actuated pop drain opens for condensate drainage at 5 psig (0.35 barg) for Models 2011 and 2022.

Probe Connections are available for trap monitoring on Models 2011 and 2022.









How to Order

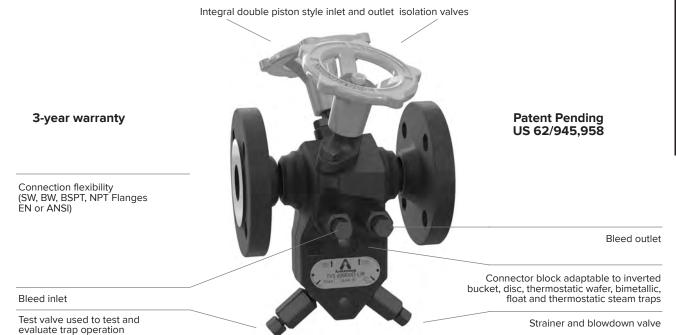
Model	Connection	Type of Connection Inlet/Outlet	Flow Direction	Trap Type
TVS 4000	1/2" 3/4"	NPT SW BSPT Flanged*	R = Right to Left L = Left to Right	Inverted Bucket Disc Thermostatic wafer Bimetallic Float and Thermostatic

^{*}Consult factory.

TVS 6000UD Forged Steel Trap Valve Station

Compact double isolation and bleed concept (Up and Downstream) with 360° Connector For pressures up to 650 psig (45 barg)...Capacities to 1300 lb/hr (590 kg/h) Using 2000 Series IB Steam Traps





Description

This original concept has been developed to meet new demanding requirements regarding safety when operating steam equipments such as steam traps, in various industrial environments. TVS 6000UD is a compact double isolation and bleed concept (up and downstream) with a 360° connector.

TVS 6000UD provides double isolation inlet and outlet piston valves, bleed of inlet/outlet valves, a test valve, a strainer and a blowdown valve at trap inlet all merged together in a single compact 2-bolts universal connector. The TVS 6000UD's design ensures increased safety while saving space, time and cost.

This TVS 6000UD is covered by a three-year-warranty. The TVS 6000UD can be fitted with steam traps of different technologies (thermodynamic, thermostatic, float and thermostatic or free float. Please refer to specific steam trap capacity charts).

Connections

Screwed BSPT and NPT Socketweld and Buttweld Flanged EN1092-1 PN40 or ASME B16.5

Table ST-189-1. TVS 6000U	D Com	pact do	ouble is	olation	and ble	eed
	in	mm	in	mm	in	mm
Connection Size	1/2	15	3/4	20	1	25
"A" valve closed	9	230	9	230	9	230
"A" valve open	9 13/16	250	9 13/16	250	9 13/16	250
"B"	2 13/16	72	2 13/16	72	2 13/16	72
"C" Face-to-Face (screwed, SW & BW)	3 15/16	100	3 15/16	100	3 15/16	100
"CC" Face-to-Face (flanged EN1092-1 PN40)	5 7/8	150	5 7/8	150	6 1/4	160
"CC" Face-to-Face (flanged ASME B16.5 #150)	6 11/16	170	6 3/4	172	7	179
"CC" Face-to-Face (flanged ASME B16.5 #300)	7	179	7 1/8	182	7 1/2	192
Weight in lb (kg) (screwed, SW & BW)	11.4	(5.2)	11.4	(5.2)	11.4	(5.2)
Weight in lb (kg) (flanged EN1092-1 PN40)	15.2	(6.9)	16.5	(7.5)	17.4	(7.9)
Maximum Allowable Pressure +	45 barg @ 315 °C 653 psig @ 599 °F				99 °F	
Maximum Hydrotest Temperature	599 °F / 315 °C					
Maximum Hydrotest Pressure		98	86 psig	/ 68 ba	ırg	

Materials - TVS 6000UD Connector

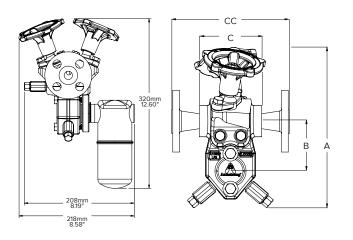
Connector: ASTM A350 LF2
Test valve: ASTM A582 T303 – Nitronic 60
Blowdown valve: ASTM A582 T303 – Nitronic 60
Depressurising valve: ASTM A582 T303 – Nitronic 60
Flanges: P250GJ (other material on request)

Isolation Valve Components

Valve Sealing Rings: Graphite and Stainless Steel
Bonnet ASTM A350 LF2
Bonnet Bolting DIN933 8.8

Flow Direction

Left to Right (L/R) Right to Left (R/L)

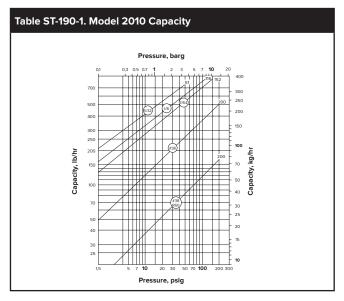


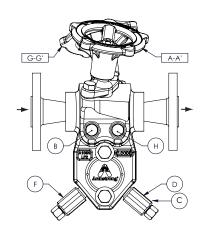
⁺ May be derated depending on flange rating and type.

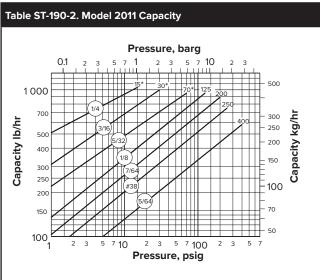


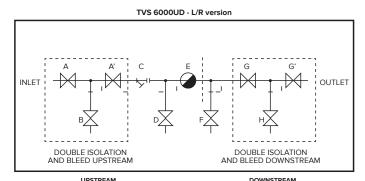
TVS 6000UD Forged Steel Trap Valve Station Compact double isolation and bleed concept (Up and Downstream) with 360° Connector

For pressures up to 650 psig (45 barg)...Capacities to 1300 lb/hr (590 kg/h) Using 2000 Series IB Steam Traps









- A : INLET FIRST ISOLATION VALVE A' : INLET SECOND ISOLATION VALVE B: BLEED INLET
- C : STRAINER
 D : DEPRESSURIZING VALVE
 E : STEAM TRAP CONNECTION
- F: TEST VALVE
 G: OUTLET FIRST ISOLATION VALVE
 G': OUTLET SECOND ISOLATION VALVE

Table ST-190-3. Model 2022 Ca	•
Pres	sure, barg
500 400 300 250 200 150 100 1 2 3 5 7 10	2 3 5 7 10 2 3 5 1 000 40 80 125 250 650 700 500 250 250 150 9 100 100 100 100 100 100 100 10
Pres	sure, psig

Table ST-190-4. How to Order										
Model	Connection	Type of Connection	Flow Direction							
	DN15 DN20 DN25	Flanges EN1092-1 & PN Class	L/R = Left to Right							
TVS 6000UD	1/2" 3/4" 1"	BSPT, NPT, SW, BW, Flanges ASME B16.5 & Class RF	R/L = Right to Left							

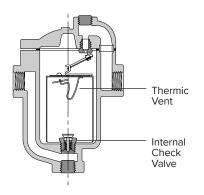
Capacities to be reduced by 5% for pressure below 5 bar (tested with Armstrong steam traps).

Steam Trap Options



Thermic Vent Buckets

Whenever steam is turned on and off, air will accumulate in the piping and steam equipment. A trap equipped with a thermic bucket will discharge this air 50 to 100 times faster than a standard bucket, reducing warm-up time. Thermic vent buckets are suitable for pressures up to 130 psig (9 barg). A large vent hole in the bucket can also solve air venting problems upon start-up.

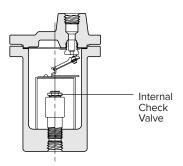


Internal Check Valves—1/2" (15 mm) Thru 2" (50 mm) NPT

Almost all Armstrong inverted bucket steam traps can be equipped with internal check valves. A check valve is needed between the trap and the equipment being drained in the following cases:

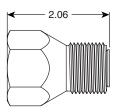
- When the trap is installed above the unit drained
- When sudden pressure drops may occur in the steam supply to the unit
- · Whenever a back pressure exists in the condensate return line

Armstrong spring-loaded, stainless-steel internal check valves can be screwed directly into the trap inlet or into an extended inlet tube having a pipe coupling at the top.



"In-Line" Check Valve—1/2" (15 mm) and 3/4" (20 mm) NPT

On 1800 and 2000 Series stainless-steel traps, an internal check valve cannot be installed. Armstrong's CVI "in-line" check valve will solve the problem.

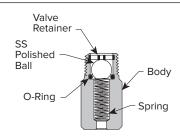


Pop Drain for Freeze Protection—1/2" (15 mm) NPT

In general, a properly selected and installed Armstrong trap will not freeze as long as steam is coming to the trap. If the steam supply is shut off, a pop drain should be used to automatically drain the trap.

Maximum Operating Conditions

Pressure: 600 psig (41 barg) Temperature: 350°F (177°C)





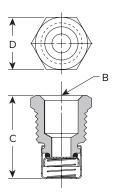
Armstrong Steam Trap Options

Vacuum Breaker—3/8" (10 mm) and 1/2" (15 mm) NPT

Many times, condensate will be retained ahead of steam traps because of the presence of a vacuum. To break a vacuum, air must be introduced into the system by means of a vacuum breaker.

For maximum protection against freezing and water hammer in heating coils under modulated control, for example, vacuum breakers are recommended in conjunction with freeze protection devices.

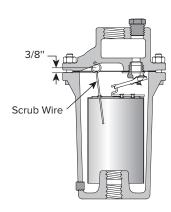
Vacuum Breaker										
Size	in	mm	in	mm						
Size	1/2 NPT	15	3/8 NPT	10						
"B" Pipe Connections	3/8 NPT	10	1/4 NPT	6						
"C" Height	1-1/4	32	1-3/32	28						
"D" Width	7/8 Hex	22 Hex	11/16 Hex	17 Hex						



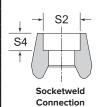
Dirt Problems

Whenever dirt plugs the bucket vent, Armstrong recommends the use of a scrubbing wire which, on each cycle, keeps the bucket vent hole open.

In normal conditions, the inverted bucket trap is not sensitive to dirt problems (because of its orifice at the top of the trap), unlike most other traps, which should be installed normally with a strainer (see Armstrong "Y" Type Strainers page 445).



Socketweld Dimensions									
Pipe	Size	S-	-2	S-4 Min.					
in	mm	in	mm	in	mm				
1/2	15	0.855	22	3/8	10				
3/4	20	1.065	27	1/2	13				
1	25	1.330	34	1/2	13				
1-1/4	32	1.675	43	1/2	13				
1-1/2	40	1.915	49	1/2	13				
2	50	2.406	61	5/8	16				
2-1/2	65	2.906	74	5/8	16				
3	80	3.535	90	5/8	16				

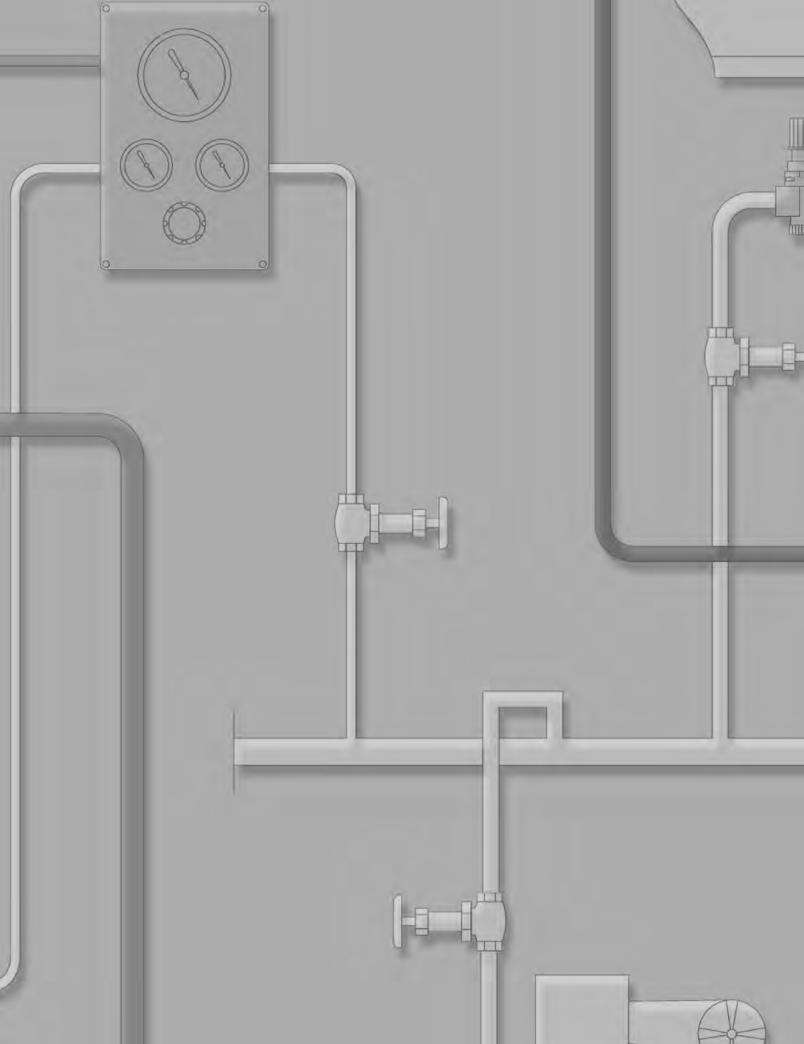


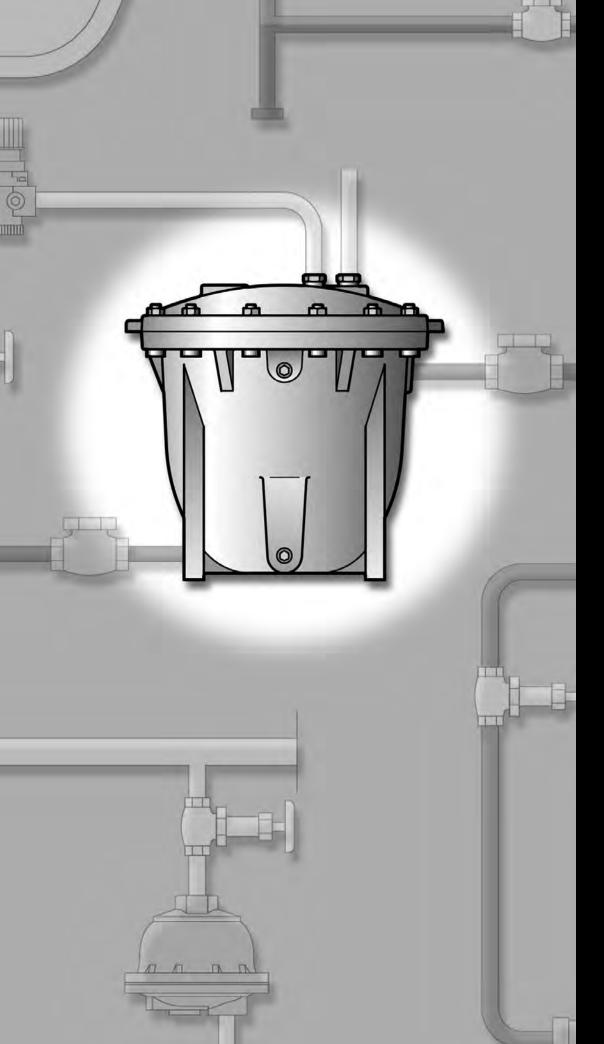
Flanged Connections

Flanged traps are furnished with the following ANSI B16.5 flanges as standard. Flange facings comply with ANSI B16.5.

Pressure Class Rating	Inlet Connection	Outlet Connection
150 and 300	1/16" Raised Face	1/16" Raised Face
600 and Higher	1/4" Raised Face	1/4" Raised Face

Other types of flanged connections (such as large male and female ring joint, large or small tongue and groove, etc.) can be furnished. Flange requirements for both inlet and outlet must be specified.





Condensate Recovery Equipment

Armstrond



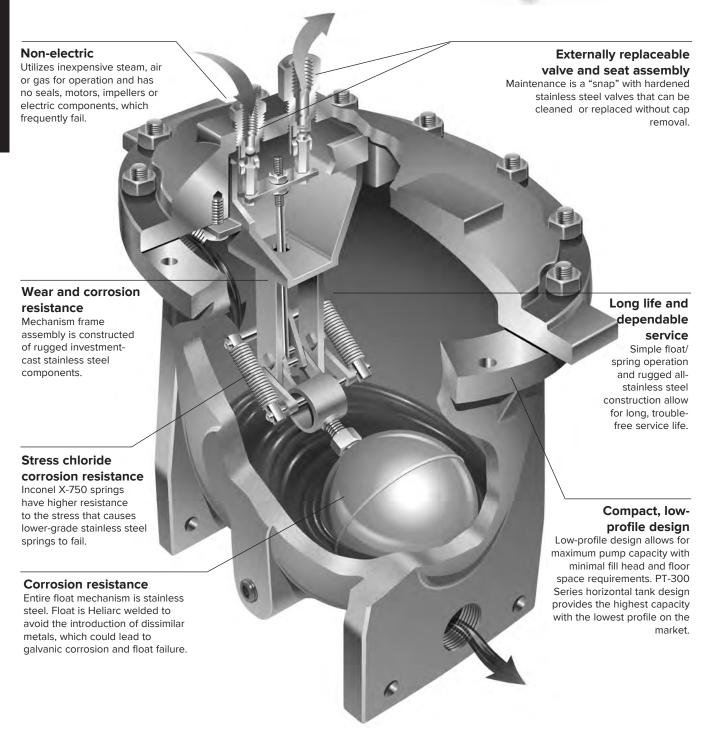


Pumping Traps

Inside Advantages

Mechanical condensate pumps operate with a spring-assisted float mechanism, which means the springs themselves are a major wear point. Armstrong pumping traps have largediameter Inconel X-750 springs, which provide superior corrosion resistance and longer service life than those in competitive models. For other inside advantages, see below.





Effective Condensate Management = Energy Savings



The most basic part of energy management is utilizing all valuable Btu within the steam system. Depending on the pressure, condensate exiting a trap contains approximately 20% of the heat energy transferred at the boiler in the form of sensible heat. Effective recovery of condensate reduces three tangible costs of producing steam:

These savings can be calculated using the attached savings form. Returning condensate saves money, energy and the environment. Pour money and energy savings back into your plant—not down the drain.

- Fuel/energy costs associated with producing steam
- · Boiler water make-up and sewage treatment
- · Boiler water chemical treatment

Condensate Recovei	y Savings Analysis	Location _
--------------------	--------------------	------------

Bldc

Energy costs will vary from plant to plant and regions of the world. Values shown are conservative. Complete this form using your facilities' numbers to determine annual savings in your plant by returning condensate. If some costs are not known, use the figures below for conservative estimates.

- A) Condensate Load = 8 000 lb/hr
- B) Annual Hours of Operation..... = 7 200 hrs per year
- C) Total Water and Sewage Cost.....= \$.005 per gal c1) Untreated water and sewage= \$.002 per gal c2) Water treatment chemicals= \$.003 per gal
- D) Make-Up Water Preheating Requirements = **140 Btu/lb** d1)Condensate Return Temperature...= **200°F** d2) Make-Up Water Temperature.....= **60°F**
- E) Steam Cost.....= \$ 5.00/1 000 lb

- F) Annual Water Savings.....= **\$ 34 532.00**(A)8000 x (B)7200 x (C).005
 8.34 lb/qal
- H) Cost of Steam to Operate¹
 Armstrong Pump Trap.....= **\$ 864.00**3 x (A)8000 x (B)7200 x (E)5.00
- I) Total Dollars Saved Annually (F + G H). = \$ 73 988.00

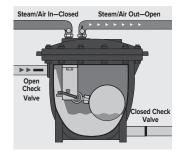
1000 x 1000

- J) Payback Period in Years.....= .27 Years

 **(cost of equipment/installation) \$20 000

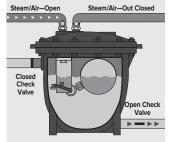
 (I) 73 988
- * Btu/lb from direct steam injection
- ** Estimated equipment and installation cost
- * Cost to operate in example assumes an "open" vented system. If pump trap is used in "closed loop" application, steam operation cost is negligible.

Pumping Trap Operation



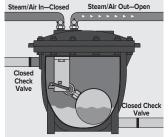
Filling

1. During filling, the steam, air or inert gas inlet and check valve on pumping trap outlet are closed. The vent and check valve on the inlet are open.



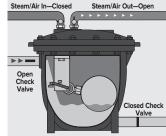
Begin Pumping

2. Float rises with level of condensate until it passes trip point, and then snap action reverses the internal valve positions shown in step one.



End Pumping

3. Float is lowered as level of condensate falls until snap action again reverses the internal valve positions.



Repeat Filling

4. Steam, air or inert gas inlet and trap outlet are again closed while vent and condensate inlet are open. Cycle begins anew.



Armstrong Pumping Trap ID Charts

Illustration	T	Connection	Max. Allow.	тма	Body	Mechanism	Model	Max. Oper.	Capacity Range	Connection Size			Located	
illustration	Туре	Туре	Press. psig	. °F	Material	Material	Wodei	Press. psig	lb/hr	1"	1-1/2"	2"	3" x 2"	on Page
	Series PT-100	Screwed	150	450	ASTM A48 Class 30 Cast Iron	Stainless Steel with Inconel X-750 Spring	PT-104	100	1800	•				199
	Series PT-200	Screwed	150	450	ASTM A48 Class 30 Cast Iron	Stainless Steel with Inconel X-750 Spring	PT-204 PT-206	125	2 400 3 700	•	•			201
· ·	Series PT-400	**Screwed	150	**Fabricated Steel 150 psig ASME	Stainless Steel with	PT-404 PT-406	125	3 600 5 500	•	•			203	
	Series PT-400LL	**150# ANSI Flanged	150	*650	Sec. VIII Design "U" Stamped	Sec. VIII X-750 Design "U" Spring	PT-408 PT-412	125	7 400 12 200			•	•	214
	Series PT-3500	Screwed	150	450	ASTM A48 Class 30 Cast Iron	Stainless Steel with Inconel X-750 Spring	PT-3508	125	9 900			•	•	205
	Series PT-300	Screwed		*650	**Fabricated	Stainless	PT-308		11 600			•		207
	Series PT-300LL	**150# ANSI Flanged **300# ANSI Flanged	150	550	Steel 150 psig ASME Sec. VIII Design "U" Stamped	Steel with Inconel X-750 Spring	PT-312	125	16 600				•	214
	Series PT-500	**150# ANSI Flanged	150	500	**Fabricated Steel 150 psig ASME Sec. VIII Design "U" Stamped	Stainless Steel with Inconel X-750 Spring	PT-516	150	80 000		4":	x 4"		211
	Double Duty 4	Screwed	72	320	Ductile Iron	Stainless Steel	Simplex	72	up to 350		1" :	x 1"		215
	Double Duty 6	**150# ANSI				Stainless Steel with	Simplex Duplex		up to 4 800		1-1/2	!" × 1"		217
	Double Duty 12	Flanged	200	400	Carbon Steel	on Steel Inconel X-750	Triplex Quadplex	200	up to 19 900		3":	x 3"		230
	Series 100, 200, 300, 3500 Low Boy [™] Packages	Fo	or detaile	d infor	mation, regard or visit	ing Armstrong our website a				ease	contact	the 1	factory	

^{**}Other connection type, receiver pressure vessel ratings and material type available upon request—consult factory.

^{*}Standard mechanism: Maximim motive 125 psig; maximum allowable pressure 150 psig (vessel rating); maximum temperature 480°F (vessel rating).

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Pumping Trap ID Charts



		ID Char		,								
Electric Centrifugal C	Type	Sq. Ft. EDR	Pump Capacity GPM	Pump Disch. Press.	Motor HP	RPM	Disch. Size Inches	Inlet Size Inches	Receiver Cap. Gallons	Locate Page for Sizing		
	FHS Series FHC Series	8 000 thru	12 thru 30	Max. 20	Simplex 1/3, 1/2, 3/4	3 500 RPM Only	3/4"	2" thru	FHS Series 8 - 30 (Steel)	240		
	Simplex or Duplex	20 000	12 1111 30	psig	Duplex 1/2 or 3/4	Single Phase Only	3/4	3"	FHC Series 15 - 36 (Cast Iron)	240		
	AFH-4100 4200 4300 3500 Simplex or Duplex	2 000 thru 50 000	*3 thru 75	*20 thru 50	*1/3 thru 5	1750 and 3 500 Single or Three Phase	3/4" thru 1-1/2"	2" thru 4"	AFH-4100/4300 8 - 120 (Steel/SS) AFH-4200 6 - 120 (Cast Iron)	243 thru 252		
000	AFH-4400 Simplex or Duplex	4 000 thru 60 000	6 thru 90	*10 thru 50	1/3 thru 1-1/2"	3500 RPM	3/4" thru 1-1/2"	2" thru 2-1/2"	12 - 100	253		
Boiler Feed Condensa	te Pump ID Ch	Boiler HP BHP	Pump Capacity GPM	Pump Disch. Press.	Motor HP	RPM	Disch. Size Inches	Inlet Size Inches	Receiver Cap. Gallons	Locate Page for Sizing		
	AFH-4100 4200 4300 **3500 5000	15 to 700	*3 to 140	*20 to 50	1/3 to 7-1/2	1750 and 3 500 Single or Three Phase	Consult	Factory 30 to 714		243		
Rescue Cap® Non-Elec	tric Steam/Air I	Powered Pun				and Listed Dale				Dana		
	ipirax Sarco Models PPC & PPF PTC & PTF	/atson McDar Models PMPC & PMF	spen Nicho	ce & olson nsate	Mechanical Pur KADANT- Johnson Corporation	ITT Hoffmar PCS			lark Reliance	Page 227		
Flash Tank ID Chart Illustration	Туре	Conn	ections	Size	Pressure	Rating	Sparge	Pipe	Body Material	Page		
	VAFT Vertical Flash Tanks		NPT nged	6" 8" 12" 16"	*****	noig					Carbon Steel	259
	HAFT Horizontal Flash Tanks		NPT nged	4" thru 30"	- ***150	psig	N/A		N/A Carbon Steel		Carbon Steel	250

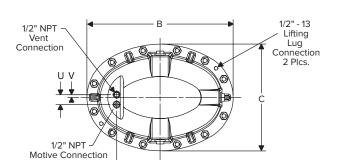
^{*}Other capacities, discharge pressures and HP available - consult factory.

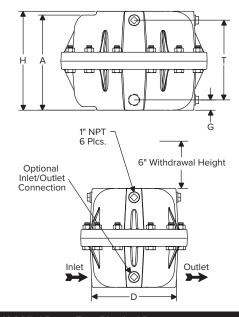
^{**3500} Series has elevated tank as standard.

^{***}Other pressure ratings available upon request.



PT-104 Series Mini Pump Trap





PT-104 Mini Pump Trap Physical Data								
Symbol	in	mm						
"A"	12	305						
"B"	18-1/2	470						
"C"	13-1/2	343						
"D"	10-3/4	272						
"F"	5-1/2	140						
"G"	1-5/16	33						
"H"	12-1/2	317						
"U"	1-1/4	32						
"V"	3/8	9						
"T"	10-1/16	256						
Weight lb (kg)	140 ((64)						
Bronze Check Valves lb (kg)	A (2)						
Stainless Steel Check Valve lb (kg)	4 (2)							
Maximum Operating Pressure	100 psig (7 barg)							
Maximum Allowable Pressure (vessel design)	150 psig @ 450 232							

PT-104 Mini Pump Trap Connection Sizes								
Connection	Туре	in	mm					
Inlet		1	25					
Outlet		1	25					
Vent		1/2	15					
Motive Pressure	NPT	1/2	15					
Optional Gauge Glass		1	25					
Optional Cycle Counter/Pressure Gauge		1	25					



The patented Armstrong PT-104 Mini Pump Trap is the smallest non-electric solution that can move condensate or other liquids from lower to higher points and from lower to higher pressures. Condensate can be returned at temperatures well above the 200°F (93°C) limit of conventional electric centrifugal pumps without the headaches of leaking seals or cavitation problems. The PT-104 Mini Pump Trap is the small solution for a big problem.

Features

- Economical non-electric operation. Uses inexpensive steam, air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- Lower installation costs. Single trade required for installation and maintenance.
- · Peace of mind. Standard unit is intrinsically safe.
- Cast iron durability. Rugged construction material means long service life.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.

For a fully detailed certified drawing, refer to CDF #1028.

PT-104 Mini Pump Trap Materials								
Name of Part	Material							
Body and Cap	Cast iron ASTM A48 Cl.30							
Vent/Inlet Valves	Stainless steel							
Mechanism Assembly	Stainless steel							
Spring	Inconel X-750							
Gasket	Graphoil							
Bolts	SA 449							
Nuts	ASTM A194 Gr.2H							
Plug	Cast iron							

PT-104 Series Mini Pump Trap



Options

Use of external check valves required for operation of pumping trap.

 Inlet Swing Check Valve NPT Bronze ASTM B 62 Teflon* Disc Class 150 (Minimum)

Outlet

Stainless Steel Check Valve Class 150 (Minimum)

- In-line Check Valves Stainless Steel Non-Slam Check Valves
- Bronze Gauge Glass Assembly
- · Steel Gauge Glass Assembly
- Removable Insulation Jacket
- Digital Cycle Counter

Capacity Conversion Factors for Other Filling Heads									
Filling Head									
in	0	6	12	* 24 or greater					
mm	0	150	305	* 620 or greater					
PT-104 Mini Pump Trap	0.7	1.0	1.2	* Consult factory					

NOTE: Fill head measured from drain to top of cap. See figures on page 234.

PT-104	PT-104 Mini Pump Trap Capacities										
	tive ssure	Total I		Filling Head 6" (152 mm) Liquid Specific Gravity 0.9 - 1.0							
Pres	sure	Dack Pi	essure	Ste	am	Α	r				
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr				
15	1.0			1 125	510	2 100	952				
25	1.7			1300	590	2 200	998				
50	3.5	5	0.34	1550	703	2 275	1 032				
75	5.0			1650	748	2 300	1 043				
100	7.0			1400	635	2 350	1 066				
25	1.7		1.0	650	295	1900	862				
50	3.5	45		1.0	700	317	2 050	930			
75	5.0	15			750	340	2 100	952			
100	7.0			800	363	2 150	975				
35	2.5			400	181	1800	816				
50	3.5	25	4.5	450	204	1 935	878				
75	5.0	25	1.5	500	227	2 050	930				
100	7.0			550	249	2 075	941				
50	3.5			250	113	1620	735				
75	5.0	40	2.75	300	136	1850	823				
100	7.0			350	159	1950	884				

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump case. See figures on page 234.



PT-200 Series Low Profile Cast Iron Pump Trap



The Armstrong PT-200 Series Low Profile Pump Trap is a low maintenance, non-electric solution to move condensate or other liquids from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. Condensate can be returned well above the 200°F (93°C) limit of conventional electric condensate pumps without the headaches of leaking seals or cavitation problems.

Features

- Economical non-electric operation. Uses inexpensive steam, air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- Lower installation costs. Single trade required for installation and maintenance.
- · Peace of mind. Standard unit is intrinsically safe.
- Cast iron durability. Rugged construction material means long service life.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.

Options

Use of external check valves required for operation of pumping trap.

- Inlet Swing Check Valve NPT Bronze ASTM B 62 Teflon* Disc Class 150 (Minimum)
- Outle
 - Stainless Steel Check Valve Class 150 (Minimum)
- In-line Check Valves
 Stainless Steel Non-Slam Check Valves
- Bronze Gauge Glass Assembly
- Steel Gauge Glass Assembly
- Removable Insulation Jacket
- · Digital Cycle Counter

For a fully detailed certified drawing, refer to CDF #1000.



PT-200 Pumping Trap Mate	rials
Name of Part	Series PT-200
Body and Cap	Cast iron ASTM A48 CI. 30
Cap Gasket	Graphoil
Bolts	SA-449 Steel
Nuts	Alloy steel ASTM A194 Gr. 2H
Inlet Valve Assembly	Stainless steel
Vent Valve Assembly	Stainless steel
Valve Assembly Washers	Zinc plated steel
Plug	Steel
Mechanism Assembly	Stainless steel
Springs	Inconel X-750

Cast Iron											
Model	PT-	204	PT-206								
	in	mm	in	mm							
Inlet Connection	1	25	1-1/2	40							
Outlet Connection	1	25	1-1/2	40							
Optional Low Inlet or Same Side Outlet Connection	1	25	1-1/2	40							
Motive Pressure Connection	1/2	15	1/2	15							
Vent Connection	1/2	15	1/2	15							
Gauge Glass Connection	1/2	15	1/2	15							

PT-200 Series Low Profile Cast Iron Pump Trap



mm

519

342

328

482

293

18

51

111

305

57

104

28

1-1/2 (40)

9 (4)

PT-204

PT-206

in

20-7/16

13-1/2

12-15/16

19

11-35/64

23/32

2-1/32

4-3/8

12

2-1/4

4-1/8

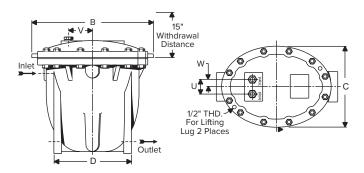
1-1/8

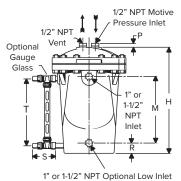
210 (96)

12

1 (25)

4 (2)





or Same Side Outlet

| Statiness Steel Check Valves | 4 (2) | 9 (4) | | (1b (kg) | | (2) | (2) | (3) | (4) | (2) | (4) | (2) | (4) | (2) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4) | (4

PT-200 Pumping Trap Physical Data

"C"

"D"

"H"

"M'

"P"

"R"

"S'

"V"

"W"

Weight lb (kg)

Number of Body/Cap Bolts

Check Valve Conn. in (mm)

Bronze Check Valves lb (kg)

Stainless Steel Check Valves

Maximum Operating Pressure 125 psig (9 barg)

PT-20	PT-200 Capacity Conversion Factors for Other Fill Heads											
-:	Head	in	mm	in	mm	in	mm	in	mm	in	mm	
""	неаа	0	0	6	152	12	305	24	610	36	914	
PT-204		0.7		1		1.1		1.3		1.	4	
Model	PT-206	0	0.7		1		1.1		.3	1.	4	

NOTE: Fill head is measured from drain point to top of cap. See figures on page 234.

Motive I	Pressure		t or Back		PT-204 (6" Fi	II Head) 1" x 1"	PT-206 (6" Fill Head) 1-1/2" x 1-1/2"					
				Steam	Motive	Air N	lotive	Steam Motive		Air Motive		
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	
15	1.0			1800	816	2 100	953	2 700	1 2 2 5	3 000	1 361	
25	1.7			2 025	919	2 300	1 043	3 200	1 451	3 500	1588	
50	3.5	_	004	2 100	953	2 500	1 134	3 400	1 542	3 600	1633	
75	5	5	0.34	2 200	998	2 700	1 2 2 5	3 500	1588	3 700	1678	
100	7			2 300	1 043	*	*	3 600	1633	*	*	
125	8.5			2 400	1 089	*	*	3 700	1 678	*	*	
25	1.7			1500	680	2 000	907	2 400	1 088	2 700	1 2 2 5	
50	3.5			2 000	907	2 250	1 021	3 200	1 451	3 400	1542	
75	5	15	1	2 100	953	2 500	1 134	3 300	1 497	3 500	1 588	
100	7			2 110	957	*	*	3 350	1520	*	*	
125	8.5			2 125	964	*	*	3 400	1 542	*	*	
35	2.5			1500	680	1700	771	2 100	953	2 300	1 043	
50	3.5			1 700	771	2 000	907	2 400	1 089	2 600	1 179	
75	5	25	1.5	1900	862	2 300	1 043	2 700	1 2 2 5	2 900	1 315	
100	7			2 000	907	*	*	2 800	1 270	*	*	
125	8.5			2 100	953	*	*	2 900	1 315	*	*	
50	3.5			1 400	635	1700	771	1500	680	2 000	907	
60	4			1500	680	2 000	907	2 000	907	2 300	1 043	
75	5	40	2.75	1700	771	2 200	998	2 300	1 043	2 500	1 134	
100	7			1800	816	*	*	2 400	1 089	*	*	
125	8.5			1920	871	*	*	2 500	1134	*	*	
70	4.5			1100	499	2 000	907	1150	522	2 000	907	
75	5	60	4	1300	590	2 300	1 043	1325	601	2 300	1 043	
100	7	00	4	1600	726	*	*	1900	862	*	*	
125	8.5			1720	780	*	*	2 000	907	*	*	

NOTES: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump cap. See figures on page 234. Although motive pressures are shown at high pressure differentials (difference between motive inlet pressure and total lift or back pressure), it is preferable to use a motive pressure of 10 - 15 psig (0.65 - 1.0 barg) above discharge (outlet) pressure. This ensures longevity of economical (bronze) check valves and reduces both venting time and temperature differential (on steam). If a higher differential is used, stainless steel check valves are recommended.



PT-400 Series Vertical Steel Pump Trap

3-Year No Fail Ann Trap Meditine

The Armstrong PT-400 Series Vertical Pump Trap is the low maintenance, non-electric solution to move condensate or other liquids from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. Condensate can be returned at temperatures well above the 200°F (93°C) limit of conventional electric condensate pumps without the headaches of leaking seals or cavitation problems.

Features

- Economical non-electric operation. Uses inexpensive steam, air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Lower installation costs. Single trade required for installation and maintenance.
- · Peace of mind. Standard unit is intrinsically safe.
- Durable construction. ASME code-stamped carbon steel body vessel.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.

Options

Use of external check valves required for operation of pumping trap.

• Inlet Swing Check Valve

NPT Bronze ASTM B 62

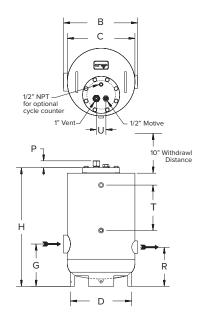
Teflon® Disc

Class 150 (Minimum)

- Outlet
 - Stainless Steel Check Valve Class 150 (Minimum)
- In-line Check Valves
 Stainless Steel Non-Slam Check Valves
- Bronze Gauge Glass Assembly
- Steel Gauge Glass Assembly
- Removable Insulation Jacket
- · Digital Cycle Counter

For a fully detailed certified drawing, refer to CDF #1004.





PT-400 Pumping Trap P	PT-400 Pumping Trap Physical Data											
Model Number	PT-404, PT-406, PT-408 and PT-412											
Model Number		in	m	ım								
"B"	17	'-1 /2	4	45								
"C"		16	4	06								
"D"	14-1/2 368											
"G"		10	2	54								
"H"	:	28	7	'11								
"P"	1-	5/8	41									
"R"	9	-1/4	2	35								
"T"	12 305											
"U"	2	-1/4	5	57								
Weight, lb (kg)		1	66 (75)									
Number of Body/Cap Bolts			8									
Model Number	PT-404	PT-406	PT-408	PT-412								
Check Valve Conn., in (mm)	1 (25)	1-1/2 (40)	2 (50)	3 (75)								
Bronze Check Valves, lb (kg)	4 (2)	9 (4)	16 (7)	29 (13)								
Stainless Steel Check Valves, lb (kg)	4 (2)	9 (4)	15 (7)	38 (17)								

PT-400 Series Vertical Steel Pump Trap



PT-400 Pumping Trap Connection Sizes												
	Vertical Steel											
Model	PT-	404	PT-	406	PT-	408	PT-412					
	in	mm	in	mm	in	mm	in	mm				
Inlet Connection	1	25	1-1/2	40	2	50	3	80				
Outlet Connection	1	25	1-1/2	40	2	50	2	50				
Motive Pressure Connection	1/2	15	1/2	15	1/2	15	1/2	15				
Vent Connection	1	25	1	25	1	25	1	25				
Gauge Glass Connection	1/2	15	1/2	15	1/2	15	1/2	15				

NOTES: Optional flanged connections available. Consult factory. Inlet/outlet socketweld connections available. Consult factory.

PT-40	PT-400 Pumping Trap Capacities																			
Mo Pres	tive	Tota or B		PT-40	4 (12" Fi	II Head)	1" x 1"	PT	•	" Fill Hea x 1-1/2"	ıd)	PT-40	PT-408 (12" Fill Head) 2" x 2"			PT-412	PT-412 (12" Fill Head) 3" x 2"			
Pres	sure	Pres	sure	Steam	Motive	Air M	lotive	Steam	Motive	Air M	otive	Steam	Motive Air Mo		lotive	Steam I	Motive	Air M	lotive	
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	
15	1.0			1900	862	2 250	1 021	3 100	1406	3 350	1520	4 500	2 041	4 850	2 200	7 500	3 402	8 100	3 674	
25	1.7			2 500	1 134	2 650	1202	4 600	2 086	4 875	2 211	6 600	2 994	7 000	3 175	11 000	4 990	11 650	5 284	
50	3.5	5	0.34	3 100	1 406	3 225	1463	4 900	2 222	5 100	2 313	7 100	3 220	7 375	3 345	11 700	5 307	12 150	5 511	
75	5	5	0.54	3 400	1542	3 500	1588	5 200	2 359	5 300	2 404	7 200	3 266	7 400	3 357	12 000	5 443	12 350	5 602	
100	7			3 500	1 588	*	*	5 400	2 449	*	*	7 300	3 311	*	*	12 100	5 488	*	*	
125	8.5			3 600	1 633	*	*	5 500	2 495	*	*	7 400	3 357	*	*	12 200	5 534	*	*	
25	1.7			2 200	999	2 525	1 145	3 500	1588	4 025	1826	5 400	2 449	6 200	2 812	7 200	3 266	8 275	3 753	
50	3.5			2 600	1 179	2 800	1270	4 100	1860	4 425	2 007	6 300	2 857	6 800	3 084	10 400	4 717	11 250	5 103	
75	5	15	1	2 800	1 270	2 950	1 338	4 400	1 996	4 750	2 155	6 500	2 948	6 900	3 130	10 800	4 899	11 450	5 194	
100	7			3 100	1 406	*	*	4 800	2 177	*	*	6 700	3 039	*	*	11 000	4 990	*	*	
125	8.5			3 200	1 451	*	*	4 900	2 222	*	*	6 800	3 084	*	*	11 200	5 080	*	*	
35	2.5			2 000	907	2 350	1 066	2 900	1 315	3 425	1554	4 200	1905	4 950	2 245	6 900	3 130	8 150	3 697	
50	3.5			2 400	1 088	2 675	1 213	4 000	1 814	4 500	2 041	5 800	2 631	6 400	2 903	9 700	4 400	10 850	4 921	
75	5	25	1.5	2 600	1 179	2 800	1270	4 300	1950	4 550	2 064	6 000	2 721	6 500	2 948	10 000	4 536	10 900	4 944	
100	7			2 800	1 270	*	*	4 700	2 132	*	*	6 100	2 767	*	*	10 200	4 626	*	*	
125	8.5			2 900	1 315	*	*	4 800	2 711	*	*	6 400	2 903	*	*	10 400	4 717	*	*	
50	3.5			1900	862	2 350	1 066	3 300	1 451	4 050	1 837	4 350	1 973	5 350	2 427	5 800	2 631	7 125	3 232	
60	4			2 200	999	2 600	1 179	3 600	1 633	4 250	1 927	5 100	2 313	6 000	2 722	6 900	3 130	8 150	3 697	
75	5	40	2.75	2 400	1 088	2 675	1 213	4 000	1 814	4 475	2 030	5 700	2 585	6 375	2 892	7 600	3 447	8 500	3 856	
100	7			2 500	1 135	*	*	4 200	1905	*	*	6 000	2 721	*	*	8 100	3 674	*	*	
125	8.5			2 700	1225	*	*	4 500	2 041	*	*	6 200	2 612	*	*	8 500	3 856	*	*	
70	4.5			1800	816	2 400	1088	3 200	1 451	4 300	1950	3 800	1724	5 050	2 291	5 000	2 268	6 650	3 016	
75	5	60	4	2 000	907	2 450	1 111	3 500	1588	4 650	2 109	4 100	1859	5 175	2 347	5 400	2 450	6 900	3 130	
100	7		·	2 300	1 233	*	*	3 700	1678	*	*	4 500	2 041	*	*	6 000	2 722	*	*	
125	8.5			2 400	1088	*	*	3 800	1724	*	*	4 800	2 177	*	*	6 400	2 903	*	*	

NOTES: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump cap. See figures on page 234. Although motive pressures are shown at high pressure differentials (difference between motive inlet pressure and total lift or back pressure), it is preferable to use a motive pressure of 10 - 15 psig (0.65 - 1 barg) above discharge (outlet) pressure. This ensures longevity of economical (bronze) check valves and reduces both venting time and temperature differential (on steam). If a higher differential is used, stainless steel check valves are recommended.

*Consult factory.

PT-400 Series Pumping Trap N	Materials
Name of Part	Series PT-400*
Body and Cap	Fabricated steel 150 psig ASME Sec. VIII design "U" stamped
Cap Gasket	Graphoil
Bolts	SA-449 steel
Nuts	None
Inlet Valve Assembly	Stainless steel
Vent Valve Assembly	Stainless steel
Valve Assembly Washers	Zinc-plated steel
Plug	Steel
Mechanism Assembly	Stainless steel
Springs	Inconel X-750

*Series PT-400 is available in all stainless steel. Consult factory

PT-400	PT-400 Capacity Conversion Factors for Other Fill Heads												
E:11	in	mm	in	mm	in	mm	in	mm	in	mm			
FIII	Head	0	0	6	152	12	305	24	610	36	914		
	PT-404	0.7		0.85		1.0		1.3		1.4			
Model	PT-406	0.7		0.85		1.	.0	1.2		1.3	35		
Model	PT-408	0	.7	0.8	85	1.0		1.	.2	1.3	35		
	PT-412	0	.7	0.8	85	1.0		1.08		1.	2		

NOTES: Fill head is measured from drain point to top of cap. See figures on page 234.



PT-3500 Series Low Profile Pump Trap





The Armstrong PT-3500 Series Low Profile Pump Trap is the low maintenance, non-electric solution to move condensate or other liquids from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. Condensate can be returned at temperatures well above the 200°F (93°C) limit of conventional electric pumps without the headaches of leaking seals or cavitation problems.

Features

- Economical non-electric operation. Uses inexpensive steam, air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- Lower installation costs. Single trade required for installation and maintenance.
- · Peace of mind. Standard unit is intrinsically safe.
- Cast iron durability. Rugged construction material means long service life.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.

Ontions

Use of external check valves required for operation of pumping trap.

· Inlet Swing Check Valve

NPT Bronze ASTM B 62

Teflon® Disc

Class 150 (Minimum)

Outlet

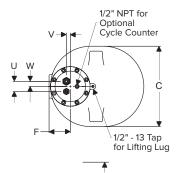
Stainless Steel Check Valve Class 150 (Minimum)

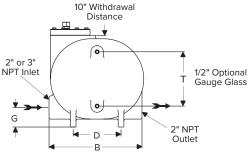
In-line Check Valves

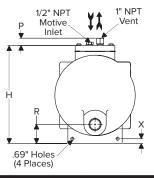
Stainless Steel Non-Slam Check Valves

- Bronze Gauge Glass Assembly
- Steel Gauge Glass Assembly
- Removable Insulation Jacket
- Digital Cycle Counter

For a fully detailed certified drawing, refer to CDF #1041.







PT-3500 Series Pump Trap Physical Data										
		PT-3508 a	nd PT-3512							
		in	mm							
"B"		20-1/4	514							
"C"		17-3/4	451							
"D"		10-9/16	268							
"F"		4-3/4	120							
"G"		4-5/16	110							
"H"		21-11/16	550							
"P"		1-5/8	41							
"R"		4-5/16	110							
"T"		12	305							
"U"		2-1/4	27							
"V"		7/8	22							
"W"		1-1/4	32							
"X"		1-1/16	27							
Weight		PT-3508	PT-3512							
Pump Trap Weight		244 (111)	243 (110)							
Bronze Check Valve	lb (kg)	16 (7)	29 (13)							
Stainless Check Valve		15 (7)	38 (17)							

Maximum Operating Pressure: 125 psig (9 barg)

Maximum Allowable Pressure: Cast iron 150 psig @ 450°F (10 barg @ 232°C)

PT-3500 Series Low Profile Pump Trap



PT-3500 S	eries Low P	rofile Pump	Trap Capac	ities								
							-	12" (305 mn	•			
Operat	ing Inlet	Total	Lift or				iid Specific	Gravity 0.9				
•	sure	Back P	ressure			3508 x 2"		PT-3512 3" x 2"				
				Ste	am		ir	Ste		Air		
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	
15	1.0			6 100	2 767	8 100	3 674	8 300	3 765	10 300	4 627	
25	1.7			8 700	3 946	9 300	4 818	12 100	5 489	12 950	5 874	
50	3.5	_	0.24	8 900	4 037	9 675	4 389	13 400	6 078	14 000	6 350	
75	5	5	0.34	9 200	4 173	9 800	4 452	13 700	6 214	14 300	6 486	
100	7			9 400	4 264	*	*	14 000	6 350	*	*	
125	8.5			9 900	4 491	*	*	14 400	6 532	*	*	
25	1.7			6 300	2 858	8 200	3 719	8 100	3 674	9 800	4 445	
50	3.5		1	8 200	3 719	10 400	4 717	11 600	5 262	12 600	5 715	
75	5	15		9 200	4 173	11 100	5 035	12 500	5 670	13 300	6 033	
100	7			9 600	4 354	*	*	12 600	5 715	*	*	
125	8.5			9 800	4 445	*	*	13 400	6 078	*	*	
35	2.5			6 100	2 767	7 900	3 583	7 600	3 447	9 900	4 491	
50	3.5			7 100	3 221	9 600	4 355	10 000	4 536	10 650	4 831	
75	5	25	1.5	8 600	3 901	10 800	4 899	11 200	5 080	12 200	5 534	
100	7			8 700	3 946	*	*	11 450	5 194	*	*	
125	8.5			9 100	4 128	*	*	11 600	5 262	*	*	
50	3.5			5 000	2 268	6 500	2 948	6 200	2 812	8 500	3 856	
60	4			5 900	2 676	7 400	3 357	7 700	3 493	9 400	4 264	
75	5	40	2.75	6 650	3 016	8 300	3 765	8 700	3 946	10 600	4 800	
100	7			7 200	3 266	*	*	9 100	4 128	*	*	
125	8.5			7 800	3 538	*	*	9 400	4 264	*	*	
75	5			4 500	2 042	6 300	2 858	5 900	2 676	8 700	3 946	
100	7	60	4	5 500	2 495	*	*	6 500	2 948	*	*	
125	8.5			5 700	2 586	*	*	6 900	3 130	*	*	

NOTES: Published capacities based on use of external check valves supplied by Armstrong. Although motive pressures are shown at high pressure differential (difference between motive inlet pressure and total lift or back pressure), it is preferable to use a motive pressure of 10 - 15 psig (0.65 - 1.0 barg) above discharge (outlet) pressure. This ensures longevity of economical (brass) check valves and reduces both venting time and temperature differential (on steam). Shading indicates sizing example shown on page 220.

^{*}Consult factory.

PT-3500 Cap	acity Conver	sion Facto	ors for Ot	her Fill He	eads								
F:U.1	laad	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Fill H	ieau	0	0	6	152	12	305	18	457	24	610	36	914
Madal	PT-3508	0	.7	0.	85	1.	.0	1	.1	1.	2	1.3	35
Model	PT-3512	0	.7	0.	85	1.	.0	1.0)4	1.0)8	1.	.2

NOTE: Fill head measured from drain point to top of cap. See figures on page 234.

PT-3500 Series Low Profile Pun	np Trap Materials
Name of Part	Material
Body	Cast iron - ASTM A48 class 30
Cap	Carbon steel SA-516-70
Cap Gasket	Graphoil
Inlet Valve Assembly	Stainless steel
Vent Valve Assembly	Stainless steel
Valve Assembly Washers	Zinc-plated steel
Plug	Steel
Mechanism Assembly and Float	Stainless steel
Springs	Inconel X-750

PT-3500 Series Low Profile Pump Trap Connection Sizes							
Model Number	PT-3	508	PT-3512				
Model Number	in	mm	in	mm			
Inlet Connection	2	50	3	75			
Outlet Connection	2	50	2	50			
Motive Pressure Connection	1/2	15	1/2	15			
Vent Connection	1	25	1	25			
Gauge Glass Connection	1/2	15	1/2	15			



PT-300 Series Horizontal Steel, Low Profile Pump Trap



The Armstrong PT-300 Series Horizontal, Low Profile Pump Trap is the low maintenance non-electric solution to move condensate or other liquids from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. Condensate can be returned at temperatures well above the 200°F (93°C) limit of conventional electric condensate pumps without the headaches of leaking seals or cavitation problems.

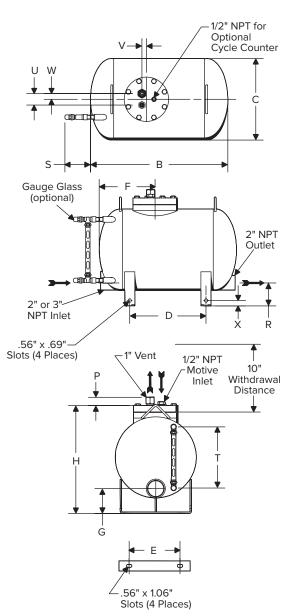
Features

- Economical non-electric operation. Uses inexpensive steam, air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- Lower installation costs. Single trade required for installation and maintenance.
- · Peace of mind. Standard unit is intrinsically safe.
- Durable construction. ASME code-stamped carbon steel body vessel.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.

PT-300 Pumping Trap Physical Data		
Model Number		308 312
	in	mm
"B"	27	686
"C"	16	406
"D"	13	381
"E"	10	254
"F"	11	279
"G"	5-7/16	138
"H"	21-3/16	538
"P"	1-5/8	41
"R"	4-13/16	122
"S"	5-1/32	128
"T"	12	305
"U"	2-1/4	57
"V"	7/8	22
"W"	1-1/4	32
"X"	1-1/16	27
Face to Face	27-1/2*	698
Weight Ib (kg)	154	(70)
Number of Body/Cap Bolts	8	3
Check Valve Conn. in (mm)	2 (50)	3 (75)
Bronze Check Valves lb (kg)	16 (7)	29 (13)
Stainless Steel Check Valves Ib (kg)	15 (7)	38 (17)

Maximum Allowable Pressure (Vessel Design): 150 psig @ 650°F (10 barg @ 343°C) Maximum Operating Pressure: 125 psig (9 barg)





For a fully detailed certified drawing, refer to CDF #1001.

^{*}Tolerance +/- 1/2"

PT-300 Series Horizontal Steel, Low Profile Pump Trap



PT-300 Pumping Trap Mater	ials
Name of Part	Series PT-300*
Body and Cap	Fabricated steel 150 psig ASME Sec. VIII design "U" stamped
Cap Gasket	Graphoil
Bolts	SA-449 steel
Nuts	None
Inlet Valve Assembly	Stainless steel
Vent Valve Assembly	Stainless steel
Valve Assembly Washers	Zinc plated steel
Plug	Steel
Mechanism Assembly	Stainless steel
Springs	Inconel X-750

		Horizon	tal Stee	el
Model	PT-	308	PT-	312
	in	mm	in	mm
Inlet Connection	2	50	3	80
Outlet Connection	2	50	2	50
Motive Pressure Connection	1/2	15	1/2	15
Vent Connection	1	25	1	25
Optional Gauge Glass Connection	1/2	15	1/2	15

NOTES: Optional flanged or socketweld connections available. Consult factory. *Series PT-300 is available in all stainless steel. Consult factory.

Motive I	Pressure	Total Lift or Back			PT-308 (12" Fi	ll Head) 2" x 2"		PT-312 (12" Fill Head) 3" x 2"				
mouve r ressure		Pressure		Steam	Motive	Air M	lotive	Steam	Motive	Air Motive		
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	
15	1.0			6 900	3 130	9 200	4 173	9 000	4 082	12 300	5 579	
25	1.7			10 200	4 622	10 900	4 944	13 200	5 987	14 200	6 441	
50	3.5	5	0.34	10 600	4 808	11 100	5 035	15 100	6 849	15 800	7 167	
75	5	5	0.34	10 800	4 898	11 300	5 126	15 300	6 940	16 100	7 303	
100	7			11 200	5 080	*	*	15 500	7 031	*	*	
125	8.5			11 600	5 261	*	*	16 600	7 530	*	*	
25	1.7			7 000	3 175	10 100	4 581	9 000	4 082	11 200	5 080	
50	3.5			9 600	4 354	10 900	4 944	12 800	5 806	13 800	6 260	
75	5	15	1	10 750	4 876	11 100	5 035	14 200	6 441	15 000	6 804	
100	7			10 900	4 944	*	*	14 300	6 486	*	*	
125	8.5			11 300	5 125	*	*	15 100	6 849	*	*	
35	2.5			7 100	3 221	9 200	4 173	8 100	3 674	11 500	5 216	
50	3.5			8 300	3 765	10 200	4 627	10 200	4 627	12 750	5 783	
75	5	25	1.5	10 100	4 581	11 000	4 989	12 500	5 670	13 500	6 123	
100	7			10 200	4 627	*	*	12 700	5 761	*	*	
125	8.5			10 300	4 672	*	*	13 000	5 897	*	*	
50	3.5			5 700	2 585	7 600	3 447	6 600	2 994	9 800	4 445	
60	4			6 600	2 994	8 800	3 992	8 400	3 810	10 500	4 763	
75	5	40	2.75	7 600	3 447	10 100	4 581	9 800	4 445	12 700	5 761	
100	7			8 400	3 810	*	*	10 100	4 581	*	*	
125	8.5			9 400	4 264	*	*	10 300	4 672	*	*	
70	4.5			4 500	2 041	7 000	3 175	6 000	2 722	10 200	4 627	
75	5		,	4 700	2 132	7 100	3 221	6 400	2 903	10 400	4 717	
100	7	60	4	6 400	2 903	*	*	7 100	3 221	*	*	
125	8.5		1 1	6 600	2 994	*	*	7 400	3 357	*	*	

NOTES: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump cap. See figures on page 234. Although motive pressures are shown at high pressure differentials (difference between motive inlet pressure and total lift or back pressure), it is preferable to use a motive pressure of 10 - 15 psig (0.65 - 1 barg) above discharge (outlet) pressure. This ensures longevity of economical (brass) check valves and reduces both venting time and temperature differential (on steam). If a higher differential is used, stainless steel check valves are recommended.

*Consult factory.

PT-300	PT-300 Capacity Conversion Factors for Other Fill Heads										
F:11 1	llaad	in	mm	in	mm	in	mm	in	mm	in	mm
"	Head	0	0	6	152	12	305	24	610	36	914
Model	PT-308	0	.7	0.	85	1.	.0	1.	2	1.	.3
iviouei	PT-312	0	.7	0.	85	1.	.0	1.0	08	1.	2

NOTES: Fill head is measured from drain point to top of cap. See figures on page 234.

Options

Use of external check valves required for operation of pumping trap.

- Inlet Swing Check Valve
- NPT Bronze ASTM B 62
 - Teflon® Disc
 - Class 150 (Minimum)
- Outlet
 - Stainless Steel Check Valve Class 150 (Minimum)
- In-line Check Valves
 Stainless Steel Non-Slam C
 - Stainless Steel Non-Slam Check Valves
- Bronze Gauge Glass Assembly
- · Steel Gauge Glass Assembly
- Removable Insulation Jacket
- Digital Cycle Counter



Sizing and Selection— PT-100/200/300/3500/400/DD-4/DD-6/PT-6F Series

The Armstrong non-electric pump trap is sized based on actual condensate load (lb/hr or kg/hr) being pumped. The following steps are used to size the pump.

- Determine the total condensate load to be pumped in lb/hr or kg/hr. See table on page 217 for conversion factors.
- Determine the total back pressure the pump will operate against. Total back pressure is the sum of the following:
- Vertical lift expressed in psig. See conversion formula below to convert lift to psig
- Existing pressure in condensate return line or D.A. tank
- Frictional loss from pipe, valves and fittings
- Determine type of motive gas to be used (steam, air or other inert gas) and pressure available.

Example:

- Condensate load = 7 100 lb/hr (3 221 kg/hr).
- Total back pressure = 25 psig (1.5 barg)
 (25 foot vertical lift = 10.8 psig, 14 psig in condensate return line).
- · Motive pressure is steam at 50 psig (3.5 barg).

Solution: Model PT-3508

Find 25 psig total lift or back pressure in column two of Low Profile Pump Trap Capacities table on page 217. Then find 50 psig motive pressure in column one. Move across the capacity table until you reach a model number with the correct capacity. A PT-3508 has been highlighted on page 217 for this example.

Either a closed reservoir pipe or a vented receiver is required for proper condensate storage during the pump-down cycle of the pumping trap.

For vented/open system receiver sizing:

- Determine the pressure from where the condensate is being discharged.
- · Determine condensate load.

Reference Percentage of Flash Steam chart on page 221 to find the pressure that corresponds with the discharge condensate pressure. For this example, use 15 psig.

Follow 15 psig on the horizontal axis where it intersects the curve. Move left from the intersecting lines to the vertical axis for the percentage of flash steam that is created. For this example it will be 3% (see shaded area on Percentage of Flash Steam chart).

Multiply 3% by the condensate load. Using example above 7 100 lb/hr. $7 100 \times .03 = 213$ lb/hr flash steam.

Using the Vented Receiver Sizing table on page 221, find the amount of flash steam in column one. Follow the table across to determine the size of the vented receiver. (See shaded area on Inlet Reservoir Pipe Sizing table—page 221 for this example.)

For closed reservoir piping:

1. Determine condensate load (using example above 7 100 lb/hr).

Reference the inlet reservoir pipe sizing for closed systems on page 221. Find 7 100 lb/hr in column one. Move horizontally across to find proper pipe size. (Note length or diameter may be slightly enlarged when capacity falls between given condensate loads in column one.) Selection is shaded.

Metric Conversion Formulas

Convert lb/hr to kg/hr—By dividing by 2.2046 Example: 1800 lb/hr ÷ 2 2046 = 816 kg/hr

Convert psig to barg—By dividing by 14.5 Example: 15 psig ÷ 14.5 = 1.03 barg

Convert psig to kg/cm²—By dividing by 14.22 Example: 15 psig ÷ 14.22 = 1.05 kg/cm²

Sizing and Selection— PT-100/200/300/3500/400/DD-4/DD-6/PT-6F Series Armstrong®

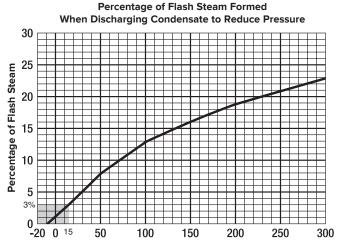


Condens	sate Load					Re	servoir Pi	pe Diame	eter				
		in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
lb/hr	kg/hr	2	50	3	75	4	100	6	150	8	200	10	250
up to							Length	of Pipe					
		ft	m	ft	m	ft	m	ft	m	ft	m	ft	m
500	227	4	1.2	2-1/2	0.7	1-1/2	0.4						
1000	453	4-1/2	1.4	2	0.6	1-1/2	0.4						
1500	680	7	2.1	3	0.9	2	0.6						
2 000	907	9	2.7	4	1.2	2-1/2	0.7						
2 500	1 134	11	3.4	5	1.5	3	0.9	1-3/4	0.5				
3 000	1 360	13-1/2	4.1	6	1.8	3-1/2	1.1	2	0.6				
4 000	1 814	18	5.5	8-1/2	2.6	5	1.5	2-1/2	0.7				
5 000	2 268			10	3.0	6	1.8	3	0.9	1-1/2	0.4		
6 000	2 722			12	3.7	7	2.1	3-1/2	1.1	2	0.6		
7 000	3 175			14-1/2	4.4	8-1/2	2.6	4	1.2	2	0.6		
8 000	3 629			16-1/2	5.0	9-1/2	2.9	4-1/2	1.4	2-1/2	0.7	1-1/2	0.4
9 000	4 082					11	3.4	5	1.5	3	0.9	2	0.
10 000	4 536					12	3.7	5-1/2	1.7	3	0.9	2	0.
11 000	4 990					13	4.0	6	1.8	3-1/2	1.1	2	0.
12 000	5 443					14	4.3	6-1/2	2.0	4	1.2	2-1/2	0.

NOTE: When draining condensate from a single piece of equipment in a closed system, to achieve maximum energy efficiency a reservoir should be installed horizontally above and ahead of the pump trap. Sufficient reservoir volume is required above the filling head level to hold condensate during the pump trap discharge cycle. The chart above shows the minimum reservoir sizing, based on the condensate load, to prevent equipment flooding during the pump trap discharge cycle.

Vented R	eceiver S	Sizing fo	r Open S	ystems	;			
Fla Stea			eiver neter		eiver ngth	Vent Line Diameter		
lb/hr	kg/hr	in	mm	in	mm	in	mm	
up to								
75	34	4	102			1-1/2	40	
150	68	6	152			2	50	
300	136	9	229	36	914	2-1/2	65	
500	227	10	254	30	914	3	75	
900	408	12	300			4	100	
1200	544	16	405			6	150	
2 000	907	20	508			8	200	

NOTE: When draining from single or multiple pieces of equipment in an open system, a vented receiver should be installed horizontally above and ahead of the pump trap. In addition to sufficient holding volume of the condensate above the fill head of the pump trap to hold the condensate during the pump trap cycle, the receiver must also be sized to allow enough area for flash steam and condensate separation. An overflow could also be added when required. The minimum recommended water seal is 12" (300 mm). This table shows proper receiver tank sizing based on flash steam present. See the chart at right to calculate the percentage of flash steam at a given pressure drop.



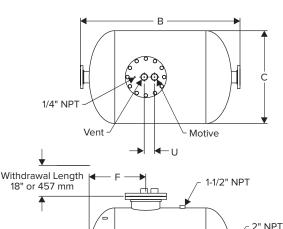
PSIG from which condensate is discharged NOTE: Back pressure = 0 psig



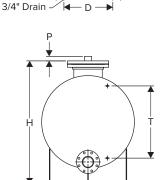
PT-516 High Capacity Pump Trap

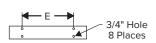
Outlet





Inlet





PT-516 Capa	city (Conve	rsion	Facto	ors fo	r Othe	er Fill	Head	s			
Fill Head	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Fili Head	0	0	6	152	12	305	16	406	24	610	36	914
PT-516	0	.7	0.	75	0	.8	0.	85	1.	0	1.0	08

Effective recovery and return of hot condensate are essential to overall plant efficiency while conserving energy. Large amounts of condensate provide the best opportunities to save energy.

The Armstrong PT-516 High Capacity Pump Trap is the low maintenance, non-electric solution to moving large amounts of condensate and other liquids from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. Condensate can be returned at temperatures well above the 200°F (93°C) limit of conventional electric pumps without the headaches of leaking seals or cavitation.

Features

- Economical non-electric operation. Uses inexpensive steam air or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Lower installation costs. Single trade required for installation and maintenance
- Peace of mind. Standard unit is intrinsically safe—explosion-proof.
- Durable construction. ASME code-stamped carbon steel body vessel.
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.

For a fully detailed certified drawing, refer to FH1367.

	in	mm
Inlet Connection	4 150# ANSI Flg.	100 150# ANSI Flg.
Outlet Connection	4 150# ANSI Flg.	100 150# ANSI Flg.
Motive Connection	2 NPT	50 NPT
Vent Connection	2 NPT	50 NPT
Gauge Glass Conn.	1/2 NPT	15 NPT
"B"	62	1 574
"C"	36	914
"D"	19-1/16	484
"E"	20	508
"F"	22	559
"H"	48	1 219
"P"	1-3/4	44
"R"	8-3/4	222
"T"	28	711
"U"	4	100
Weight	807	366
Number of Bolts	12	12

Maximum Operating Pressure on standard unit: 150 psig (10 barg). For higher pressure, consult factory.

Maximum Allowable Pressure (standard vessel deisgn): 150 psig @ 500°F (10 barg @ 277°C).

300 psig (21 barg) vessel available upon request.

PT-516 High Capacity Pump Trap



4" x 4" Connections 24" Fill Head

Typical Applications

- · Low pressure heating systems
- · Process heat exchanger or coils with modulating steam control
- · Remote installations (tracing, tank farms or remote coils)
- Systems under vacuum
- · Hazardous (explosion proof) areas
- Caustic environments
- · Sumps or submersed areas

PT-516 High-Capacity Pump Trap Materials					
Name of Part	Description				
Cap, Body, Bolting	Fabricated steel 150 psig ASME Sec. VIII design "U" stamp coded				
Cap Gasket	Stainless steel spiral wound				
Inlet Valve Assembly	Stainless steel				
Vent Valve Assembly	Stainless steel				
Mechanism Assembly: Frame, Float and Spring	Stainless steel				

NOTES: 300 psig ASME vessel available upon request. PT-516 available in all stainless steel. Consult factory.

Total Lift or Back

Motive Pressure

Armstrong PT-516 Pump Trap Sizing and Selection

PT-516 Pump Trap Capacities							
Motive Pressure		Total Lift or Back		4" x 4" Connections 24" Fill Head			
Wollve F	ressure	Pressure		Steam Motive		Air Motive	
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr
15	1.0		0.34	28 962	13 137	57 619	26 136
25	1.7			37 162	16 857	61 911	28 083
35	2.5			42 563	19 307	64 738	29 365
50	3.5			48 288	21 903	67 735	30 725
60	4	5		51 214	23 231	69 267	31 420
70	4.5	5		53 688	24 138	70 562	32 007
75	5			54 796	24 855	71 142	32 270
100	7			59 414	26 950	73 559	33 366
125	8.5			62 995	28 575	*	*
150	10.34			65 922	29 902	*	*
25	1.7		1	36 720	16 656	50 783	23 035
35	2.5			40 611	18 421	54 293	24 627
50	3.5			45 196	20 501	58 013	26 315
60	4			47 740	21 655	59 915	27 177
70	4.5	15		50 005	22 682	61 523	27 907
75	5			51 054	23 159	62 243	28 233
100	7			55 675	25 254	65 243	29 594
125	8.5			59 552	27 013	*	*
150	10.34			62 923	28 542	*	*

			Pressure		Steam Motive		Air Motive		
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr		
35	2.5			29 212	13 251	46 238	20 973		
50	3.5				33 413	15 156	50 962	23 116	
60	4			35 672	16 181	53 376	24 211		
70	4.5	25	25 1.5	37 646	17 076	55 418	25 138		
75	5	25		38 548	17 485	56 313	25 544		
100	7			42 454	19 257	60 141	27 280		
125	8.5			45 649	20 706	*	*		
150	10.34			*	*	*	*		
50	3.5			26 210	11 889	41 244	18 708		
60	4			27 353	12 407	44 028	19 971		
70	4.5			28 319	12 846	46 382	21 039		
75	5	40	2.75	28 752	13 042	47 435	21 517		
100	7		1	1		30 555	13 860	51 828	24 022
125	8.5			31 954	14 494	*	*		
150	10.34			33 097	15 013	*	*		
70	4.5			25 973	11 781	32 026	14 527		
75	5			26 373	11 963	33 514	15 202		
100	7	60	4	28 042	12 720	40 951	18 575		
125	8.5			29 336	13 307	*	*		
150	10.34			30 394	13 787	*	*		
100	7			23 892	10 837	34 893	15 827		
125	8.5	80	5.5	24 231	10 991	*	*		
150	10.34			24 570	11 145	*	*		

NOTES: Published capacities above are based on actual steam testing using a minimum 200°F condensate. Published capacities are based on the use of external check valves supplied by Armstrong. *Consult factory.

Options

External check valves required for use of pumping trap.

- Inlet/Outlet Check Valve
 CS/SS Wafer Style or All Stainless Steel Wafer Style
- Bronze Gauge Glass Assembly
- Removable Insulation Jacket
- · Digital Cycle Counter



Reservoir Sizing — DD-12/PT-12F/PT-516 Series High Capacity

Either a closed reservoir pipe or a vented receiver is required for proper condensate storage during the pump-down cycle of the pumping trap. Refer to the tables for sizing.

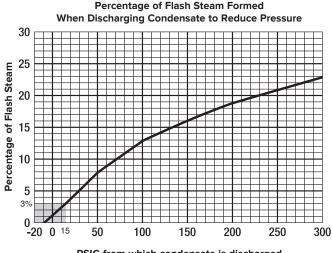
For Closed Reservoir Piping

- Determine condensate load. Example 30 000 lb/hr:
- Reference the Inlet Reservoir Pipe table top right. Find the 30 000 lb/hr condensate load in column one. Move across the columns to find the proper pipe sizing.

For Vented Receiver Sizing

- Determine the pressure from where the condensate is being discharged.
- 2. Determine condensate load.
 - Reference the chart below to find the pressure that corresponds with the discharge condensate pressure. For this example, use 15 psig.
 - Follow 15 psig to where it intersects the "0" psig curve. Move to the left from intersecting lines for the percentage of flash that will be created. For this example, it will be 3%.
 - Multiply the 3% by the condensate load. For this example, it is 30 000 lb/hr. Thus, 30 000 \times .03 = 900 lb/hr of flash steam.

Using the Vented Receiver table bottom right, find the amount of flash steam in column one. Follow the table across to determine the sizing of the vented receiver.



PSIG from which condensate is discharged NOTE: Back pressure = 0 psig

Inlet Reservoir Pipe Sizing for Closed Systems						
Condensate	Reservoir Pipe Diameter (in)					
Load lb/hr	8	10	12	16	20	24
up to	Length of Pipe (feet)					
10 000	6-1/2	6	5	3	2	
20 000	12	11-1/2	10	7	4	
30 000		12	10-1/2	9	6	4
40 000		17	14	12	8	6
50 000			16	13	9	6
60 000				15	11	8
70 000					15	10

NOTE: When BP/MP is less than 50%, the reservoir diameters above can be reduced by 1/2" (15 mm). When draining condensate from a single piece of equipment in a **closed system**, to achieve maximum energy efficiency (see Closed System figure on page 234) a reservoir should be installed horizontally above and ahead of the pump trap. Sufficient reservoir volume is required above the filling head level to hold condensate during the pump trap discharge cycle. The table above shows the minimum reservoir sizing, based on the condensate load, to prevent equipment flooding during the pump trap discharge cycle.

Vented Receiver for an Open System							
Flash Steam lb/hr	Receiver Diameter (in)						
up to							
1 000	16	60	6				
2 000	20	60	8				
3 000	24	60	8				
4 000	26	60	10				
5 000	28	60	10				
6 000	30	72	12				
7 000	32	72	12				
8 000	36	72	14				

NOTE: When draining from single or multiple pieces of equipment in an open system, a vented receiver should be installed horizontally above and ahead of the pump trap (see Open System figure on page 234). In addition to sufficient holding volume of the condensate above the fill head of the pump trap to hold the condensate during the pump trap cycle, the receiver must also be sized to allow enough area for flash steam and condensate separation. An overflow could also be added when required. The minimum recommended water seal is 12" (305 mm). The table above shows proper receiver tank sizing based on flash steam present. See chart left to calculate the percentage (%) of flash steam at a given pressure drop.

PT-300LL/PT-400LL Light Liquid Pump Traps



Features

- Economical non-electric operation. Uses inexpensive steam or inert gas.
- Low-maintenance operation. No leaking seals, impeller or motor problems means lower maintenance. No NPSH issues.
- Lower installation costs. Single trade required for installation and maintenance.
- Peace of mind. Standard unit is intrinsically safe.
- Durable construction. ASME code-stamped carbon steel body
 vessel
- Corrosion resistance. Internals are all stainless steel for corrosion resistance and long life.
- Heavy-duty springs. Springs are made from long-lasting Inconel X-750.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The pump can be used in flooded pits without fear of electrocution or circuit breaker defaults.
- Externally removable/replaceable seats. Seats can be replaced or cleaned without removing the mechanism assembly.
- Specific gravity range. Pumps can accommodate specific gravity down to 0.65.

Typical Applications

- Hydrocarbon knockout drum/separator
- Flare header drain
- Applications where the specific gravity of the liquid could be as low as 0.65
- · Applications where hydrocarbons may be present

Technical Data

Back Pressure

Maximum back pressure for the PT-300LL or PT-400LL is 60 psig (4.1 barg)

Motive Pressure

 Maximum motive pressure (Nitrogen or Inert Gas) is 100 psig (6.9 barg)

NOTE: To determine the lb/hr of liquid being pumped, use the following formula:

lb/hr of liquid = capacities x specific gravity of liquid

To size the Light Liquid Pumps, use the sizing charts on pages 215 and 219.

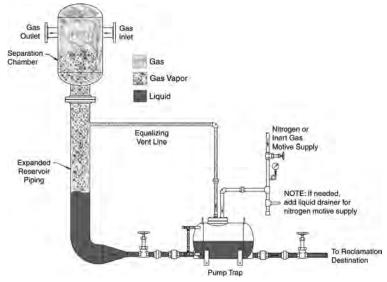
Consult Armstrong for engineered pre-piped receiver packages.



PT-300LL Light Liquid Pump Trap



PT-400LL Light Liquid Pump Trap



Hydrocarbon Knockout Drum Separator



Steam Trap/Pump Combination

Description

Armstrong's Double Duty' Series steam trap/pump combination offers a low profile solution to draining heat exchangers in various applications.

The Double Duty* 4 is a low profile pump that offers you the versatility of combining a pump within a steam trap to aide in condensate drainage from a heat exchanger under all operating conditions.

Features

- Economical. non-electric operation
- Low-maintenance operation. No leaking seals, impeller or motor problems. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- · Lower installation costs. Single trade installation.
- Peace of mind. Intrinsically safe.
- Ductile iron durability. Rugged construction material means long service life.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The trap/pump can be used in pits or sumps without fear of electrocution or circuit breaker defaults.

Maximum Operating Conditions

Maximum allowable pressure

DD-4 72 psig @ 320°F (5 barg @ 160°C)

Maximum operating pressure:

DD-4 72 psig @ 320°F (5 barg @ 160°C)

Materials

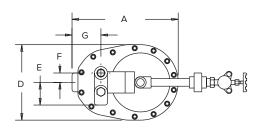
Body: Ductile iron
Mechanism: All stainless steel
Springs: 304 Stainless steel
Float: All stainless steel

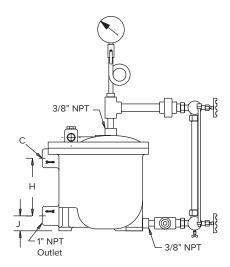
For a fully detailed certified drawing, refer to CD-2030.

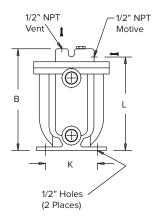
Double Duty® 4 Physical Data				
	in	mm		
"A"	11-3/16	284		
"B"	10-13/16	274		
"C"	1	25		
"D"	8	203		
"E"	2-7/16	61		
"F"	1	25		
"G"	3	76		
"H"	6-1/8	155		
"J"	1-5/8	41		
"K"	5-1/2	140		
"L"	9-15/16	251		
Weight lb (kg)	37 (17)			



Double Duty® 4







Steam Trap/Pump Combination



Double Duty 4 Pump Capacities							
Мо	tive	Back P	ressure	Ca	pacity		
psig	barg	psig	barg	lb/hr	kg/hr		
15	1			220	100		
25	1.7	5	0.34	300	136		
50	3.5	5	0.54	348	158		
70	4.5			350	159		
25	1.7			220	100		
50	3.5	15	1	345	156		
70	4.5			348	158		
35	2.5			220	100		
50	3.5	25	1.5	325	147		
70	4.5			348	158		
50	3.5			220	100		
60	4	40	2.75	300	136		
70	4.5			335	152		
70	4.5	60	4	220	100		

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump case

Capacity Conversion Factors for Other Filling Heads						
Filling Head						
in 0 2 6						
mm	0	50	152			
Double Duty DD-4	.65	1.0	1.10			

NOTE: Fill head measured from drain to top of cap.

Double Duty 4	Trap Capacities		
Differentia	I Pressure	Сар	acity
psig	barg	lb/hr	kg/hr
5	0.34	1342	610
10	0.7	1980	900
20	1.4	2 860	1300
30	2.1	3 410	1550
40	3	3 795	1725
50	3.4	4 070	1850
60	4.1	4 235	1 925
70	4.8	4 400	2 000



Steam Trap/Pump Combination

Description

Armstrong's Double Duty' Series steam trap/pump combination offers a low profile solution to draining heat exchangers in various applications.

The Double Duty* 6 is an ASME code stamped carbon steel vessel. The Double Duty* 6 offers you the versatility of combining a pump within a steam trap to aide in condensate drainage under all operating conditions.

Features

- Economical. non-electric operation
- Low-maintenance operation. No leaking seals, impeller or motor problems. No NPSH issues.
- Space-saving size. Low-profile body fits in tight spaces while allowing minimal fill head.
- Lower installation costs. Single trade installation.
- Peace of mind. Intrinsically safe.
- ASME Carbon Steel durability. Rugged construction material means long service life.
- Efficiency. A closed loop means no motive or flash steam is lost. All valuable Btu's are captured and returned to the system.
- Safety. The trap/pump can be used in pits or sumps without fear of electrocution or circuit breaker defaults.

Maximum Operating Conditions

Maximum allowable pressure

DD-6 200 psig @ 400°F (14 barg @ 204°C)

Maximum operating pressure:

DD-6 200 psig @ 400°F (14 barg @ 204°C)

Materials

Body: ASME Code Stamped Carbon Steel

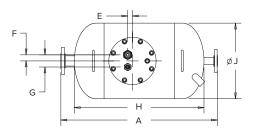
Springs: Inconel X-750
Internals: All stainless steel

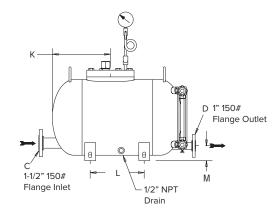
For a fully detailed certified drawing, refer to CD2035.

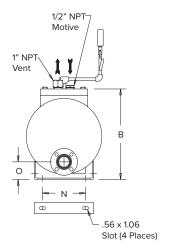
Double Duty® 6 Physical Data				
	in	mm		
"A"	29	737		
"B"	16-11/16	424		
"C"	1-1/2	38		
"D"	1	25		
"E"	7/8	22		
"F"	1-1/8	28		
"G"	2-1/4	57		
"H"	24	610		
"J"	14	356		
"K"	10-13/16	275		
"L"	10	254		
"M"	2-13/16	71		
"N"	8	203		
"O"	3-3/16	81		
Weight lb (kg)	140 (64)			



Double Duty® 6







Steam Trap/Pump Combination



Daubla Du	ity° 6 Pump C	`anacitica			
	otive		ressure	Ca	pacity
				lb/hr	pacity
psig 15	barg 1	psig	barg	2 400	kg/hr 1 089
25	1.7			3 000	1361
50	3.5			4 000	1 814
75	5.5			4 500	2 041
100	7	5	0.34	4 600	2 041
125	8.5	5	0.54	4 700	2 132
150	10.34			4 800	2 132
175	12			4 800	2 177
200	14			4 600	2 087
25	1.7			2 000	907
50	3.5			2 800	1270
75	5.5			3 400	1542
100	7			3 600	1633
125	8.5	15	1	3 700	1678
150	10.34			3 800	1724
175	12			3 600	1633
200	14			3 500	1588
35	2.5			1800	816
50	3.5			2 300	1 043
75	5			2 900	1 315
100	7			3 000	1361
125	8.5	25	1.5	3 000	1361
150	10.34			2 900	1 315
175	12			2 500	1 134
200	14			2 300	1 043
50	3.5			1400	635
75	5			2 000	907
100	7			2 400	1 089
125	8.5	40	2.75	2 500	1134
150	10.34			2 500	1 134
175	12			1800	816
200	14			1700	771
75	5			1500	680
100	7			1800	816
125	8.5	60	_	2 000	907
150	10.34	60	4	1700	771
175	12			1500	680
200	14			1 400	635

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump case.

Double Duty® 6 Trap Capacities						
Differential	Pressure	Capa	city			
psig	barg	lb/hr	kg/hr			
2	0.14	9 500	4 309			
5	0.34	12 400	5 625			
10	0.7	15 000	6 804			
25	1.5	20 400	9 253			
50	3.5	22 500	10 206			
75	5.2	22 500	10 206			
100	6.9	22 500	10 206			
150	10.3	22 500	10 206			
200	13.8	22 500	10 206			

Capacity Conversion Factors for Other Filling Heads						
	Filling Head					
in	in 0 6 12 * 24 or greater					
mm	0	150	305	* 620 or greater		
Double Duty DD-6	0.7	1.0	1.08	* Consult factory		

NOTE: Fill head measured from drain to top of cap.

Steam Trap/Pump Combination

Description

Armstrong's Double Duty-12 steam trap/pump combination offers a unique solution for draining condensate from heat exchangers and coils in various applications.

The Double Duty-12 is an ASME code stamped carbon steel vessel which offers you the versatility of combining a pump mechanism within a steam trap to assist in condensate drainage under all operating conditions.

Features

- ASME Section VIII "U" stamped vessel
- Inconel X-750 springs for long service life
- All stainless steel internals
- Easy access to the steam trap mechanism without removing cap assembly
- Externally removable vent and motive seats
- Separate pump and trap mechanisms

Maximum Operating Conditions

Maximum allowable pressure: 200 psig @ 400°F (14 barg @ 204°C) Maximum operating pressure: 200 psig @ 400°F (14 barg @ 204°C)

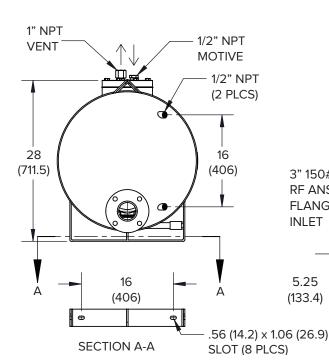
(Consult factory for different pressure/temperature ratings)

Materials

Body: ASME code carbon steel

Springs: Inconel X-750 Internals: Stainless steel

For a fully detailed certified drawing, refer to CD-2472.



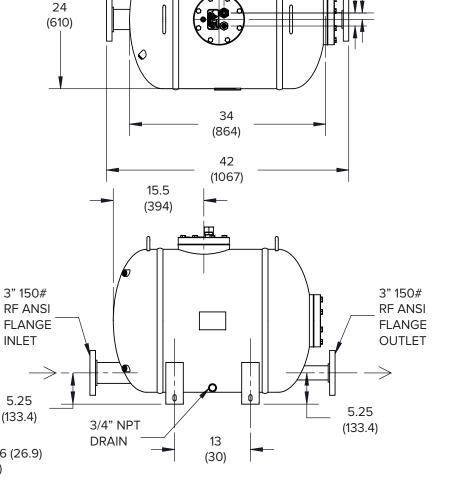


(22.1)

2.25

(57.2)

1.125 (28.58)



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Steam Trap/Pump Combination



Double Dut	y [®] 12 Pump C	apacities	_		
Мо	otive	Back Pressure C		Сар	acity
psig	barg	psig	barg	lb/hr	kg/hr
15 25 50 75 100 125 150 175 200	1 1.7 3.5 5 7 8.5 10.34 12 14	5	0.34	9 800 12 900 16 500 18 200 18 900 19 300 19 800 19 900	4 445 5 581 7 484 8 255 8 573 8 754 8 981 9 026 9 026
25 50 75 100 125 150 175 200	1.7 3.5 5 7 8.5 10.34 12 14	15	1	8 500 12 900 14 800 16 000 16 400 17 200 17 300 17 300	3 856 5 851 6 713 7 257 7 439 7 802 7 847 7 847
35 50 75 100 125 150 175 200	2.5 3.5 5 7 8.5 10.34 12 14	25	1.5	7 200 10 300 12 300 13 700 13 700 14 700 14 800 15 000	3 266 4 672 5 579 6 214 6 214 6 668 6 713 6 804
50 75 100 125 150 175 200	3.5 5 7 8.5 10.34 12 14	40	2.75	6 700 9 500 10 600 10 900 11 300 11 300 11 400	3 039 4 309 4 808 4 944 5 126 5 126 5 171
75 100 125 150 175 200	5 7 8.5 10.34 12 14	60	4	6 900 8 300 8 300 8 400 8 400 8 600	3 130 3 765 3 765 3 810 3 810 3 901
100 125 150 175 200	7 8.5 10.34 12 14	80	5.5	6 400 6 400 7 200 7 200 7 300	2 903 2 903 3 266 3 266 3 311

Capacity Conversion Factors for Other Filling Heads						
	Filling Head					
in	0	6	12	24	* 24 or greater	
mm	0	150	305	610	* 620 or greater	
Double Duty DD-12	.7	.85	1	1.08	* Consult Factory	

Double Duty [®] 12 T	rap Capacities			
Differentia	al Pressure	Capactiy		
psig	barg	lb/hr	kg/hr	
2	.14	21 500	9 752	
5	.34	28 700	13 018	
10	.7	35 900	16 284	
25	1.5	52 100	23 632	
50	3.5	59 600	27 034	
75	5.2	72 000	32 659	
100	6.9	81 000	36 741	
150	10.3	93 000	42 184	

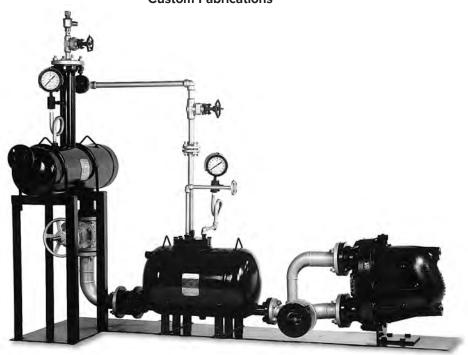
NOTE: Fill head measured from drain to top of cap. Weight in lb/kg: 348 (158)

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong.



Armstrong Packaged Solutions

Custom Fabrications



Armstrong can design and fabricate custom packages to fit your application needs.

ASME Packages



Armstrong can design and fabricate all ASME packages to meet your plant piping requirements.

Standard

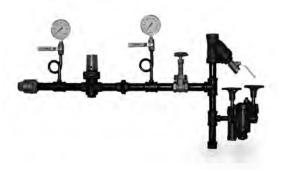


Armstrong's standard simplex (shown), duplex, triplex or quadraplex packages are unparalleled in quality and craftsmanship.



Horizontal ASME Reservoirs/Horizontal Flash Tanks

ASME stamped vessels designed for condensate collection or use as horizontal flash tanks. (Horizontal flash tanks with sparge tubes and drop legs are also available - consult factory)



Pre-Piped PRV Station

PRV/Drip trap stations, pre-piped to single pumps or packages.

Exhaust Heads

Eliminate water carryover in atmospheric vent pipe.



Insulation Blankets

- Pumps
- Receivers (consult factory for models)



- Open- or closed-loop designs
- Optional external dry contacts
- Intrinsically safe models available (consult factory)

Options

Use of external check valves required for operation of pumping trap.

- Inlet Swing Check Valve NPT Bronze ASTM B 62 Teflon® Disc Class 150 (Minimum)
- Outlet Stainless Steel Check Valve Class 150 (Minimum)
- In-line Check Valves
 Stainless Steel Non-Slam
 Check Valves
- Bronze Gauge Glass Assembly
- Steel Gauge Glass Assembly
- Removable Insulation JacketDigital Cycle Counter



Check Valves

- Stainless steel in-line non-slam check valves
- · Bronze/stainless steel (standard)
- Cast steel/stainless steel waferstyle (flanged pumps)
- Stainless steel/stainless steel wafer-style (flanged pumps)
- Bronze (standard)

Level Gauges

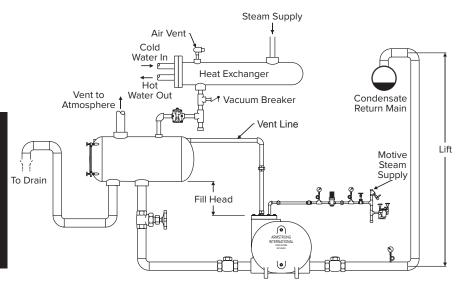
- Bronze glass gauge (standard)
- Carbon steel glass gauge
- Reflex gauge (HPI Service) consult factory

Pump/Package Accessories

Low Boy™ packages enable you to utilize mechanical pump technology in limited height applications.



General Applications

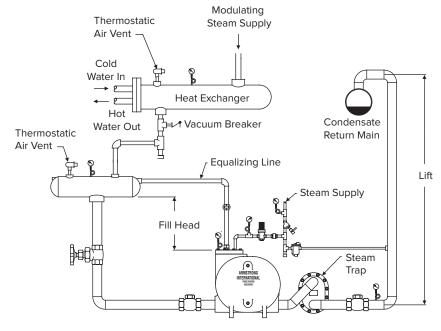


Multiple or single traps discharging to vented receiver.

OPEN SYSTEMS

For the majority of applications, a steam trap is recommended on each piece of heat exchange equipment. The steam trap, or traps, discharge to a vented receiver where flash steam will be vented to the atmosphere. The pump trap is located downstream and below the vented receiver, allowing for proper fill head height. See tables on page 221 and 224 for vented receiver and vent sizing for an open system.

Note 1: Drip trap may be discharged into the receiver, the return line or to the drain.



Draining steam coil or heat exchanger when steam pressure may exceed the return line pressure, a steam trap is required on the discharge side of the pump trap. Request installation and operation manual IB-100.

CLOSED SYSTEMS

Applications exist where it is desirable to tie the vent line back into the heat exchange space, equalizing the pressure in the heat exchanger, reservoir/piping and the pump trap. This allows water to flow by gravity down to the pump where it can be returned. Valuable Btu's remain within the system due to no flash steam loss to the atmosphere through the vent. Closed system applications can also be used to drain liquid from the equipment under a vacuum. See installation and operation manual IB-100. See tables on pages 221 and 224 for reservoir pipe sizing.

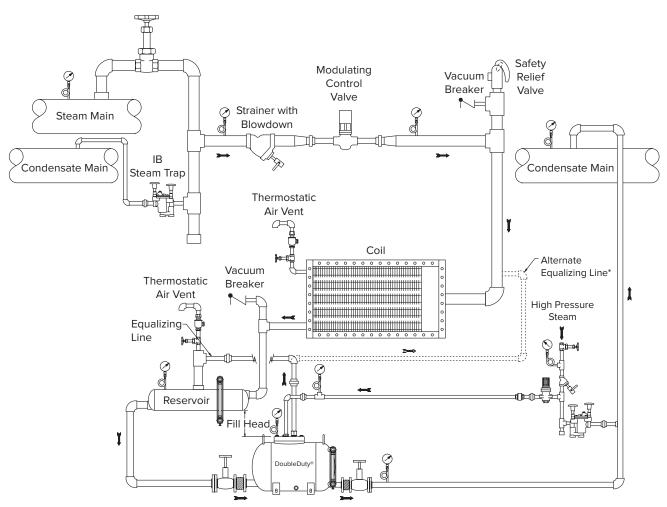
Note 1: If steam motive is used, the drip trap may be discharged into the return line or to the drain.

Note 2: Vent piping from the pump trap can be connected to the inlet side of the equipment being drained if the pressure drop across the equipment is less than .5 psig (0.03 barg) and there is a minimum of 24" (609 mm) of fill head present.

Note 3: A vacuum breaker must be installed if the vent piping from the pump trap is connected to the receiver. If the equipment modulated down to a sub-atmospheric condition, the vacuum breaker will open to equalize the system and provide adequate drainage.

Double Duty® Typical Application





*Used only if pressure drop across coils is less than 1/2 psi.

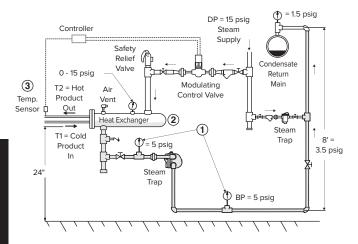
Common Applications for Condensate Armstrong Pump Traps

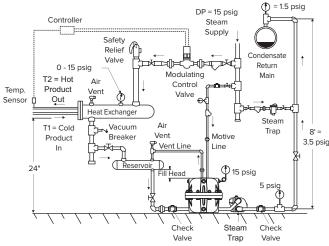
- Air Heating Coils
- Plate and Frame Heaters
- Jacketed Kettles
- Vacuum Space
- Flash Tanks
- · Shell and Tube Heat Exchangers
- Absorption Chillers
- Low Pressure Applications

Any application using modulated control.



Condensate Drainage From Modulated Steam/Temperature Controlled Equipment





Problem: "Stall" Condition on Modulated Steam Control

Modulated steam controls are required to change steam pressure in the heat exchanger to control accurate product output temperature. Due to these varying steam pressure changes, a stall condition exists in all heat exchangers where condensate cannot flow through the steam trap due to insufficient pressure differential. Under the stall condition, partial or complete flooding will occur. Reference figure above noting the stall conditions and problems that can occur.

Problems

- Stall condition—no condensate drainage due to insufficient pressure to move condensate through the steam trap
- Heat exchange equipment floods causing equipment damage from:
- Water hammer due to steam and condensate occupying the same space
- Corrosion due to carbonic acid forming from sub-cooled condensate reabsorbing trapped carbon dioxide and noncondensable gases
- 3. Inaccurate temperature control

Stall Chart

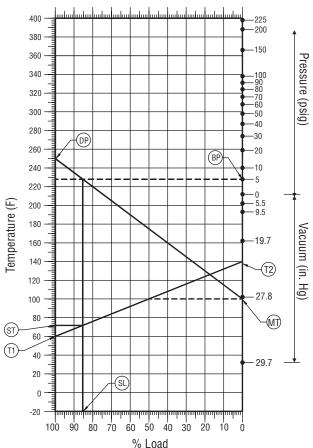
Use of the stall chart on right will determine the point where flooding will occur.

Application information required:	Example
DP = design pressure to heat exchanger 15 psig	
BP = back pressure	5 psig
T1 = incoming temperature	60°F
T2 = exit temperature	140°F
MT = mean temperature	100°F
Stall Information:	
SL = stall load %	85%
ST = stall load temperature	72°F

Armstrong Solution

The Armstrong pump trap and steam trap combination is the total solution to the stall condition by removing condensate under all system conditions. When the steam system pressure is sufficient to overcome the back pressure, the steam trap operates normally. When the system pressure falls to the stall condition, the pump trap operates and pumps condensate through the steam trap. Temperature control and condensate drainage are assured under all system conditions.

NOTE: The pump trap is sized for the stall conditions. **NOTE:** Closed-loop solution shown. See page 234 for vented system arrangement.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Notes	Armstrong



Rescue Cap[®] Non-Electric Steam/Air Powered Pump Retrofit Assembly

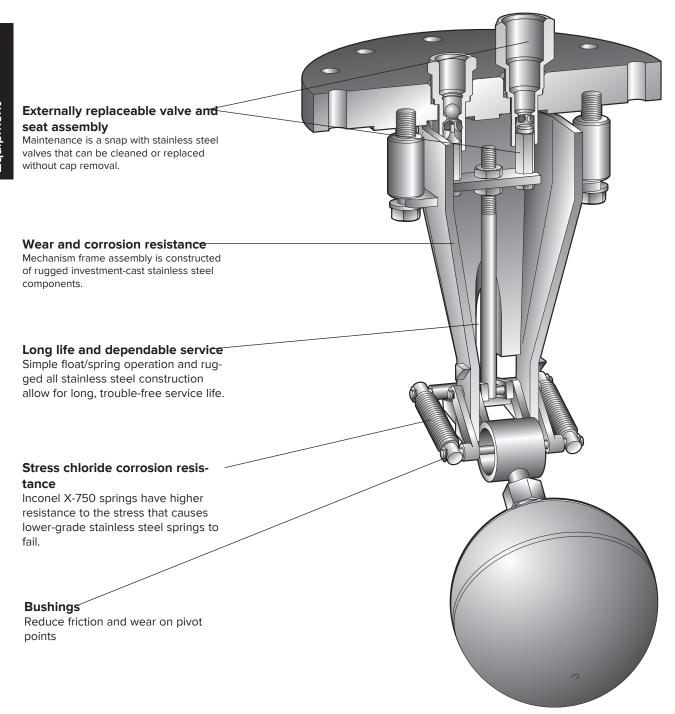
Do you experience spring failures?

3-Year No Fail

Do you experience maintenance problems with nonelectric steam/air powered pumps?

Are you dumping valuable condensate because of frequent maintenance?

Do you have to remove the complete cap assembly to view, clean or replace the motive or vent valve?



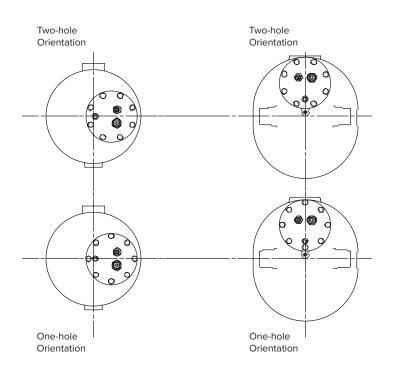
Rescue Cap[®] Non-Electric Steam/Air Powered Pump Retrofit Assembly



Armstrong's non-electric steam/air powered pump retrofit cap and mechanism assembly fits most competitive models. To ensure proper fit, please provide the following information:

- Number of bolt holes in cap:
- Inside diameter of vessel opening "A":_______
- Bolt hole orientation (one hole or two holes):_______





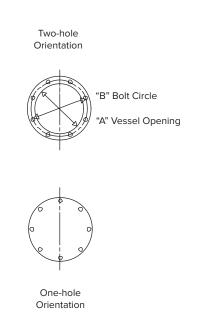


Illustration		Fits Competitors' Mechanical Pumps Listed Below											
	Spirax Sarco Models PTC & PTF PPC & PPF	Watson McDaniel Models PMPC & PMP	Spence & Nicholson Condensate Commanders	KADANT Johnson Corporation	ITT Hoffman PCS	Yarway Series 65 Steel	Clark Reliance						

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



FHC / FHS Series Electric Condensate Pumps

Armstrong FHC (cast iron) and FHS (steel) electric condensate pumps are offered as packaged units, pre-assembled, wired and factory tested.

Features

- Heavy duty, ballbearing, close-coupled pump motors with stainless steel shaft. 3450 RPM for greater efficiency and more economical operation.
- Level controls with two-pole, drip proof case, stainless steel float and float rod, doublebreak silver-to-silver contacts. Float travel adjustment is easy, visible and accessible.
- Pump mounting design provides efficient operation and extended life by venting air and flushing seal area.
- Offers a wide range of pressures and GPM. Unique design for easy maintenance.
- Pumps made of durable cast iron for extended life; efficient design provides maximum capacity with minimum motor load.
- The ultimate in ceramic technology for extended life. The seal runs on the brass impeller hub with the motor shaft actually outside the pump body. Therefore, the shaft is not exposed to corrosion by condensate. Recommended for temperatures up to 250°F (120°C).

For control panel information and optional items, please refer to page 258.



Please visit our web site, **armstrong**internationl.com, for detail information regarding dimensions and weights.

For a fully detailed certified drawing, refer to:

FHC-112	CDF1092	FHS-4028G	CD2243
FHC-122	CDF1093	FHS-112	CDF1089
FHC-212	CD2244	FHS-122	CD2241
FHC-222	CDF1095	FHS-212	CD2242
		FHS-222	CDF1091
		FHS-230	CDF1091

Specification	s - FHC Cast Ir	on Receive	r Condensate Pump	s				
Mode	el No.	Pump	Standard	Maximum Pump	Pump Discharge	Pump	Receiver Size	sq ft
Simplex	Duplex	GPM	Motor Voltage*	Discharge, psig	Nozzle Size	HP	Gallons	EDR
FHC-112	FHC-212	12	115V/1Ph	20	2/4"	1/3	15	8 000
FHC-122	FHC-222	22	3500 RPM	20	3/4"	1/2	24	15 000

Specification	Specifications - FHS Carbon Steel Receiver Condensate Pumps												
Mode	el No.	Pump	Standard	Maximum Pump	Pump Discharge	Pump	Receiver Size	sq ft					
Simplex	Duplex	GPM	Motor Voltage*	Discharge, psig	Nozzle Size	HP	Gallons	EDR					
FHS-4028G	_	12				1/3	8	0.000					
FHS-112	FHS-212	12	115V/1Ph	20	2/4"	1/3	15	8 000					
FHS-122	FHS-222	22	3500 RPM	20	3/4"	1/2	20	15 000					
_	FHS-230	30				3/4	30	20 000					

^{*}Can be field wired to 230V/1Ph/60Hz

Additional units for larger capacities and higher pressures available upon request. Pumps have cast iron bodies.

FHC / FHS Series Electric Condensate Pumps



Sizing Condensate Pumps

Step 1—Determine the condensing rate of the system:

Where: C = Condensing Rate in lb/hr F_1 = Conversion to GPM = 500 F_2 = Conversion to EDR = .0005

Formula: $C \div F_1 = GPM$

 $GPM \div F_2 = sq. ft. EDR$

Example: $2000 \text{ lb/hr} \div 500 = 4 \text{ GPM}$

4 GPM ÷ 0.0005 = 8 000 sq. ft. EDR

Step 2—Apply a 3:1 safety factor by multiplying by 3

Example: 4 GPM x safety factor of 3 = 12 GPM

Select a pump with a 12 GPM rating with

a sq. ft. EDR of 8 000

Step 3—Determine system back pressure

The total back pressure is determined by vertical lift, system pressure on the discharge side of the pump, plus frictional loss through pipe, valves and fittings.

Vertical lift, 2.31 ft. = 1 psig + system pressure (psig) + frictional loss (psig) = total system back pressure.

Select a pump that has a maximum discharge pressure greater than the total system back pressure calculated for the system.

Special Notes:

- Floor mounted condensate receivers have a maximum operating temperature rating of 200°F. Higher temperature applications will require that the receiver be elevated to achieve proper net positive suction head (NPSH).
- Duplex units are typically sized for system redundancy, using a mechanical alternator for less wear on each pump.
- For systems that require vacuum pumps, control panels, high performance motors and special condensate receivers, consult the factory for engineering and pricing assistance.
- Condensate receivers are typically sized for one to three minutes of storage capacity.
- The condensate receiver that is mounted to the pump must always remain vented to the atmosphere.

NPSH is critical to the proper operation of an electric condensate pump. NPSH is the measure of how close the suction passage of the pump is to boiling. NPSH can be calculated by the following formula: NPSH = $\rm H_S + \rm H_D - \rm H_V - \rm H_f$

Where:

 H_s = static head of the liquid at the pump suction H_V = vapor pressure of the liquid at the pump suction

 ${\rm H}_{\rm p}$ = absolute pressure above the static head of the liquid ${\rm H}_{\rm f}$ = friction loss in the suction piping



Sizing for Electric Condensate Package

		Representa	tive:
person:		Application	·
omer:		Customer L	ocation:
Pump GPM required	* (with 3:1 safety f	actor)	
Determine pump dis	charge:		
Friction loss of	pipe		
Vertical lift			
If pumping into	a pressurized lin	e (add pressure o	f line)
Add 5 psig safe	ety factor		
Total psig			
Standard packages I	ated to pump up	to 200°F condens	sate
Temperature o	f condensate		
Motor voltage and p	nase		
Material of receiver:	☐ Steel	☐ Cast Iron	☐ Stainless Steel
Motor enclosure:	□ ODP	☐ TEFC*	☐ Explosion Proof*
Is a control panel ne	eded: 🛘 Yes	□ No	
NEMA rating:	☐ NEMA 12	□ NEMA 4*	
Type of alternator or	a duplex: 🗖 Me	chanical 🔲 Ele	ectric
densate Return S	chedule		
Model Number			
Capacity			
		RPM	
Receiver	_ gallons		
Current	_ phase, 60 cyc	les,vo	lts
Options included on	nackade.		

*It is acceptable to use a 2:1 safety factor if the actual loads are known. If actual load is unknown, use standard 3:1 safety factor.

4100/4200/4300/5000/3500 Series

Condensate Boiler Feed Pumps





Series 4100 Condensate and Boiler Feed

- Heavy gauge 3/16" steel receivers for long service life
- 3450 rpm motors for maximum efficiency with minimum horsepower
- Simplex/duplex
- Wide range of options available
- Standard Units: 3 gpm 75 gpm
- Consult factory for additional sizes



Series 4300 Condensate and Boiler Feed

- Heavy gauge 3/16" stainless steel receivers for long service life
- 3450 rpm motors for maximum efficiency with minimum horsepower
- Simplex/duplex
- Wide range of options available
- Standard Units: 3 gpm 75 gpm
- Consult factory for additional sizes





Series 4200 Condensate and Boiler Feed

- Heavy duty cast iron receivers for long service life
- 3450 rpm motors for maximum efficiency with minimum horsepower
- Simplex/duplex
- Wide range of options available
- Standard Units: 3 gpm 75 gpm
- Consult factory for additional sizes



Series 5000 Boiler Feed

- Heavy gauge 3/16" carbon steel cylindrical receivers (stainless steel available)
- 3450 rpm motors for maximum efficiency with minimum horsepower
- Simplex/duplex (other)
- Wide range of options available
- Standard Units: 25 gpm 100 gpm
- Consult factory for additional sizes

Series 3500 Condensate and Boiler Feed

- Heavy gauge 3/16" carbon steel cylindrical receivers (stainless steel available)
- 3450 rpm motors for maximum efficiency with minimum horsepower
- Simplex/duplex
- Wide range of options available
- Standard Units: 3 gpm 140 gpm
- Consult factory for additional sizes

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Armstrong Carbon Steel Receiver Electric Pump Packages

AFH-4100) Series										
Cap Sq. Ft. EDR	Discharge Pressure PSIG	Pump Cap. G.P.M.	HP 3500 R.P.M.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In.	
8 000	20	12		8	AFH-4028-G	_	90	_			
2 000		3			AFH-4122-G	AFH-4122-GDA					
4 000		6	1/3	15	AFH-4124-G	AFH-4124-GDA	125	185		2"	
6 000		9			AFH-4126-G	AFH-4126-GDA		185	3/4"		
8 000		12			AFH-4128-G	AFH-4128-GDA			3/4		
10 000		15	1/2		AFH-41210-G	AFH-41210-GDA	190	240			
15 000	20	22.5	1/2	30	AFH-41215-G	AFH-41215-GDA	190	240		2-1/2"	
20 000		30	3/4		AFH-41220-G	AFH-41220-GDA	200	250			
25 000		37.5	3/4	45	AFH-41225-J	AFH-41225-JDA	205	350			
30 000		45	1	45	AFH-41230-J	AFH-41230-JDA	- 285	350		2.4/2"	
40 000		60	1-1/2	60	AFH-41240-J	AFH-41240-JDA	335	405		2-1/2"	
50 000		75	2	95	AFH-41250-J	AFH-41250-JDA	385	460			
2 000		3			AFH-4132-J	AFH-4132-JDA					
4 000		6			AFH-4134-J	AFH-4134-JDA	1				
6 000		9	1/2	15	AFH-4136-J	AFH-4136-JDA	180	250		2"	
8 000		12			AFH-4138-J	AFH-4138-JDA	1				
10 000		15	3/4	1 1	AFH-41310-J	AFH-41310-JDA	185	255	1		
15 000	30	22.5			AFH-41315-J	AFH-41315-JDA					
20 000		30	1	30	AFH-41320-J	AFH-41320-JDA	230	300			
25 000		37.5			AFH-41325-J	AFH-41325-JDA	285	350			
30 000		45	1-1/2	45	AFH-41330-J	AFH-41330-JDA	290	355	2-1/2	2-1/2"	
40 000		60	2	60	AFH-41340-J	AFH-41340-JDA	340	410			
50 000		75	3	95	AFH-41350-J	AFH-41350-JDA	395	470	1		
2 000		3			AFH-4142-J	AFH-4142-JDA					
4 000		6			AFH-4144-J	AFH-4144-JDA	-				
6 000		9	1	15	AFH-4146-J	AFH-4146-JDA	190	270	270		2"
8 000		12			AFH-4148-J	AFH-4148-JDA	-		1-1/2"		
10 000		15			AFH-41410-J	AFH-41410-JDA					
15 000	40	22.5			AFH41415-J	AFH-41415-JDA					
20 000		30	1-1/2	30	AFH-41420-J	AFH-41420-JDA	240	310			
25 000		37.5			AFH-41425-J	AFH-41425-JDA	290	355			
30 000		45		45	AFH-41430-J	AFH-41430-JDA	295	360		2-1/2"	
40 000		60	2	60	AFH-41440-J	AFH-41440-JDA	340	410			
50 000		75	3	95	AFH-41450-J	AFH-41450-JDA	395	470			
2 000		3			AFH-4152-J	AFH-4152-JDA		.,,			
4 000		6			AFH-4154-J	AFH-4154-JDA	†				
6 000		9		15	AFH-4156-J	4156-JDA	195	275		2"	
8 000		12	2	.5	AFH-4158-J	4158-JDA	1 .55				
10 000		15			AFH-41510-J	41510-JDA	-				
15 000	50	22.5			AFH-41515-J	41515-JDA	245	320			
20 000		30		30	AFH-41520-J	41520-JDA	255	330	-		
25 000		37.5	3		AFH-41525-J	41525-JDA	233	330			
30 000		45	3	45	AFH-41525-J AFH-41530-J	41525-JDA 41530-JDA	305	385		2-1/2"	
40 000		60		60	AFH-41540-J	41530-JDA 41540-JDA	370	500			
			5								
50 000		75		95	AFH-41550-J	41550-JDA	430	560			

Note: When ordering units, specify sq. ft. capacity, discharge pressure, G.P.M. model number and motor voltage. Higher G.P.M. and discharge pressure available upon request.

² ft NPSH units available for 200°F - 212°F condensate.

Models with higher capacities or discharge pressures available upon request.

Contact Armstrong or your local Armstrong representative for submittal drawings and specifications.

Pumps have cast iron bodies.



Cast Iron Receiver Electric Pump Packages

AFH-420	00 Series									
Cap Sq. Ft. EDR	Discharge Pressure PSIG	Pump Cap. G.P.M.	HP 3500 R.P.M.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size Inches	Inlet Size Inches
2 000		3			AFH-4222-G	_	450	_		
4 000		6	4/2	6	AFH-4224-G	_	150	_		
6 000		9	1/3		AFH-4226-G	AFH-4226-GDA				2"
8 000		12		15	AFH-4228-G	AFH-4228-GDA	260	295	3/4"	2"
10 000		15	4/0		AFH-42210-G	AFH-42210-GDA				
15 000	20	22.5	1/2	24	AFH-42215-G	AFH-42215-GDA	300	335		
20 000		30	2/4		AFH-42220-G	AFH-42220-GDA	410	445		
25 000		37.5	3/4	36	AFH-42225-J	AFH-42225-JDA	350	420		
30 000		45	1		AFH-42230-J	AFH-42230-JDA	355	430		3"
40 000		60	1-1/2	F0	AFH-42240-J	AFH-42240-JDA	420	500		
50 000		75	2	50	AFH-42250-J	AFH-42250-JDA	425	510		
2 000		3			AFH-4232-J	_	465			
4 000		6	4/2	6	AFH-4234-J	_	165	_		
6 000		9	1/2		AFH-4236-J	AFH-4236-JDA	205	260		2"
8 000	1	12		15	AFH-4238-J	AFH-4238-JDA	295	360		2"
10 000	1	15	3/4	1	AFH-42310-J	AFH-42310-JDA	300	365		
15 000	30	22.5		24	AFH-42315-J	AFH-42315-JDA	305	380		
20 000	1	30	1		AFH-42320-J	AFH-42320-JDA	255	420		
25 000	1	37.5		36	AFH-42325-J	AFH-42325-JDA	355	430		
30 000	1	45	1-1/2	1	AFH-42330-J	AFH-42330-JDA	360	440		3"
40 000	1	60	2	F0	AFH-42340-J	AFH-42340-JDA	425	510		
50 000	1	75	3	50	AFH-42350-J	AFH-42350-JDA	435	525		
2 000		3			AFH-4242-J	_	470			
4 000]	6		6	AFH-4244-J	_	170	_		
6 000]	9	1		AFH-4246-J	AFH-4246-JDA				2"
8 000		12		15	AFH-4248-J	AFH-4248-JDA	295	360	1-1/2"	2"
10 000		15			AFH-42410-J	AFH-42410-JDA				
15 000	40	22.5		24	AFH-42415-J	AFH-42415-JDA	310	390		
20 000		30	1-1/2		AFH-42420-J	AFH-42420-JDA	200	440		
25 000		37.5		36	AFH-42425-J	AFH-42425-JDA	360	440		
30 000		45	2		AFH-42430-J	AFH-42430-JDA	365	450		3"
40 000		60	2	F0	AFH-42440-J	AFH-42440-JDA	425	510		
50 000		75	3	50	AFH-42450-J	AFH-42450-JDA	435	525		
2 000		3			AFH-4252-J	_	475			
4 000		6		6	AFH-4254-J	_	175	_		
6 000		9	_		AFH-4256-J	AFH-4256-JDA				2"
8 000		12	2	15	AFH-4258-J	AFH-4258-JDA	315	395		2"
10 000		15			AFH-42510-J	AFH-42510-JDA				
15 000	50	22.5		24	AFH-42515-J	AFH-42515-JDA	330	415		
20 000		30			AFH-42520-J	AFH-42520-JDA				
25 000		37.5	3	36	AFH-42525-J	AFH-42525-JDA	370	460		
30 000		45			AFH-42530-J	AFH-42530-JDA				3"
40 000		60		E0	AFH-42540-J	AFH-42540-JDA	445	EDE		
50 000		75	5	50	AFH-42550-J	AFH-42550-JDA	445	535		

Note: When ordering units, specify sq. ft. capacity, discharge pressure, G.P.M. model number and motor voltage. Higher G.P.M. and discharge pressure available upon request.

² ft NPSH units available for 200°F - 212°F condensate.

Models with higher capacities or discharge pressures available upon request.

Contact Armstrong or your local Armstrong representative for submittal drawings and specifications.

Pumps have cast iron bodies.



Armstrong Stainless Steel Receiver Electric Pump Packages

AFH-430	0 Series Stainl	ess Steel E	lectric C	ondensate	Pump Package	s				
Cap Sq. Ft. EDR	Discharge Pressure PSIG	Pump Cap. G.P.M.	HP 3500 R.P.M.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size Inches	Inlet Size Inches
8 000		12		8	AFH-4028-GS	_	90	_		
2 000		3			AFH-4322-G	AFH-4322-GDA				
4 000		6	1/3	45	AFH-4324-G	AFH-4324-GDA	425	405		2"
6 000		9		15	AFH-4326-G	AFH-4326-GDA	125	185	2/4"	
8 000		12			AFH-4328-G	AFH-4328-GDA			3/4"	
10 000	20	15	1/2		AFH-43210-G	AFH-43210-GDA	190	240		
15 000	20	22.5	1/2	30	AFH-43215-G	AFH-43215-GDA	190	240		
20 000		30	3/4		AFH-43220-G	AFH-43220-GDA	200	250		
25 000		37.5	3/4	45	AFH-43225-J	AFH-43225-JDA	205	350		2-1/2"
30 000		45	1	45	AFH-43230-J	AFH-43230-JDA	285	350		
40 000		60	1-1/2	60	AFH-43240-J	AFH-43240-JDA	335	405		
50 000		75	2	95	AFH-43250-J	AFH-43250-JDA	385	460		
2 000		3			AFH-4332-J	AFH-4332-JDA				
4 000		6	1/2		AFH-4334-J	AFH-4334-JDA	190	250		
6 000		9	1/2	15	AFH-4336-J	AFH-4336-JDA	180	250		2"
8 000		12			AFH-4338-J	AFH-4338-JDA				
10 000		15	3/4		AFH-43310-J	AFH-43310-JDA	185	255		
15 000	30	22.5		20	AFH-43315-J	AFH-43315-JDA	220	200		
20 000		30	1	30	AFH-43320-J	AFH-43320-JDA	230	300		
25 000		37.5		45	AFH-43325-J	AFH-43325-JDA	285	350		2.4/2#
30 000		45	1-1/2	45	AFH-43330-J	AFH-43330-JDA	290	355		2-1/2"
40 000		60	2	60	AFH-43340-J	AFH-43340-JDA	340	410		
50 000		75	3	95	AFH-43350-J	AFH-43350-JDA	395	470		
2 000		3			AFH-4342-J	AFH-4342-JDA				
4 000		6			AFH-4344-J	AFH-4344-JDA				
6 000		9	1	15	AFH-4346-J	AFH-4346-JDA	190	270		2"
8 000		12			AFH-4348-J	AFH-4348-JDA			1-1/2"	
10 000		15			AFH-43410-J	AFH-43410-JDA				
15 000	40	22.5		30	AFH43415-J	AFH-43415-JDA	240	310		
20 000		30	1-1/2	30	AFH-43420-J	AFH-43420-JDA	240	310		
25 000		37.5		45	AFH-43425-J	AFH-43425-JDA	290	355		2.4/2#
30 000		45	2	45	AFH-43430-J	AFH-43430-JDA	295	360		2-1/2"
40 000		60		60	AFH-43440-J	AFH-43440-JDA	340	410		
50 000		75	3	95	AFH-43450-J	AFH-43450-JDA	395	470		
2 000		3			AFH-4352-J	AFH-4352-JDA				
4 000		6			AFH-4354-J	AFH-4354-JDA				
6 000		9	2	15	AFH-4356-J	4356-JDA	195	275		2"
8 000		12			AFH-4358-J	4358-JDA				
10 000		15			AFH-43510-J	43510-JDA				
15 000	50	22.5		30	AFH-43515-J	43515-JDA	245	320		
20 000		30		30	AFH-43520-J	43520-JDA	255	330		
25 000		37.5	3	45	AFH-43525-J	43525-JDA	305	385		2-1/2"
30 000		45		45	AFH-43530-J	43530-JDA	305	383		2-1/2"
40 000		60	5	60	AFH-43540-J	43540-JDA	370	500		
50 000		75	, s	95	AFH-43550-J	43550-JDA	430	560		

Note: When ordering units, specify sq. ft. capacity, discharge pressure, G.P.M. model number and motor voltage. Higher G.P.M. and discharge pressure available upon request.

² ft NPSH units available for 200°F - 212°F condensate.

 $[\]label{thm:models} \mbox{Models with higher capacities or discharge pressures available upon request.}$

Contact Armstrong or your local Armstrong representative for submittal drawings and specifications.

Pumps have cast iron bodies.

ondensate Reovery guipment

Sizing for Boiler Feed Package



This sheet MUST be sent in with every order

Pate:	Representative:	
alesperson:	Application:	
customer:	Customer Location:	
Number of boilers the pump is feeding _	(need a minimum of one dedicated pump per b	oiler
Capacity of each boiler (BHP):		
BTU/HR / 33 475 = BHP		
GPM / 0.069 = BHP		
LBS/HR / 34.5 = BHP		
Determine pump discharge:		
Operating pressure of boiler		
Friction loss of pipe between pump	and boiler (psig)	
Lift from pump to boiler (psig)	(2.31' lift = 1 psig)	
Add 5 psig safety factor		
Total (psig)		
Standard packages rated to pump up to	200°F condensate	
Temperature of condensate		
Motor voltage and phase		
Material of receiver: ☐Steel	□Cast Iron □Stainless Steel	
Motor enclosure: □ODP	□TEFC*	
Is a control panel needed: □Yes	□No	
NEMA rating: ☐NEMA 12	□NEMA 4*	
Is there a need for pre-heat tube to heat	the feed water in the tank?)
If so, up to what temperature?		
What is the maximum inlet pressure of th	ne make-up water to the tank?	
Need to use a solenoid maek-up w	rater valve if over 45 psig.	
Boiler Feed Schedule		
Model Number		
Capacity GPM at		
HP	RPM	
Receiver gallons		
Current phase, 60 cycles	,volts	

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Armstrong[®] Carbon Steel Receiver Boiler Feed Packages

AFH-4100	Series Steel Bo	iler Feed Pac	kages							
Boiler H.P.	Discharge Pressure PSIG	Pump Cap. G.P.M.	Motor H.P.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In.
	20		1/3		AFH-4122-GF	AFH-4122-GDF	200	240		3/4"
15	30	3	1/2		AFH-4132-JF	AFH-4132-JDF	260	300		
15	40	3	1		AFH-4142-JF	AFH-4142-JDF	265	310		1-1/2"
	50		2	30	AFH-4152-JF	AFH-4152-JDF	275	330		
	20		6 1/3	AFH-4124-GF	AFH-4124-GDF	200	240		3/4"	
30	30				AFH-4134-JF	AFH-4134-JDF	260	300		
30	40	б	1		AFH-4144-JF	AFH-4144-JDF	265	310		1-1/2"
	50		2		AFH-4154-JF	AFH-4154-JDF	275	330]	
	20		1/3		AFH-4126-GF	AFH-4126-GDF	240	280]	3/4"
45	30		9 1/2	45	AFH-4136-JF	AFH-4136-JDF	300	340]	
45	40	9	1	45	AFH-4146-JF	AFH-4146-JDF	305	350		1-1/2"
	50		2		AFH-4156-JF	AFH-4156-JDF	315	370]	
	20		1/3	3	AFH-4128-GF	AFH-4128-GDF	275	335]	3/4"
60	30	12	1/2 60	AFH-4138-JF	AFH-4138-JDF	335	395	2-1/2"		
60	40	12		AFH-4148-JF	AFH-4148-JDF	340	405	2-1/2	1-1/2"	
	50		2		AFH-4158-JF	AFH-4158-JDF	350	425]	ıİ
	20		1/2		AFH-41210-GF	AFH-41210-GDF	360	420		3/4"
75	30	45	3/4]	AFH-41310-JF	AFH-41310-JDF	420	480	1	
75	40	15	1		AFH-41410-JF	AFH-41410-JDF	425	490		1-1/2"
	50		2	95	AFH-41510-JF	AFH-41510-JDF	435	510		
	20		1/2	95	AFH-41215-GF	AFH-41215-GDF	360	420	1	3/4"
400	30	20	1		AFH-41315-JF	AFH-41315-JDF	420	480		
100	40	20	1-1/2		AFH-41415-JF	AFH-41415-JDF	425	490		1-1/2"
	50		2		AFH-41515-JF	AFH-41515-JDF	435	510		
	20		3/4		AFH-41220-GF	AFH-41220-GDF	415	475		3/4"
150	30	20	1	120	AFH-41320-JF	AFH-41320-JDF	475	535		
150	40	30	1-1/2	120	AFH-41420-JF	AFH-41420-JDF	480	545		1-1/2"
	50		3		AFH-41520-JF	AFH-41520-JDF	490	565		

Note: All boiler feed units supplied with Armstrong make-up water valve (rated to 45 psig maximum inlet pressure) and gauge glass; solenoid make-up valve available.

Models with higher capacities or discharge pressures available upon request. Pumps have cast iron bodies.



Cast Iron Receiver Boiler Feed Packages

Boiler H.P.	Discharge Pressure PSIG	Pump Cap. G.P.M.	Motor H.P.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In.
	20		1/3		AFH-4222-GF	AFH-4222-GDF	465	500		3/4"
45	30		1/2		AFH-4232-JF	AFH-4232-JDF	505	580		
15	40	3	1		AFH-4242-JF	AFH-4242-JDF	510	590		1-1/2"
	50		2	20	AFH-4252-JF	AFH-4252-JDF	520	600		
	20		1/3	36	AFH-4224-GF	AFH-4224-GDF	465	500		3/4"
20	30		1/2	1	AFH-4234-JF	AFH-4234-JDF	505	580	2,1	
30	40	6	1	1	AFH-4244-JF	AFH-4244-JDF	510	590		1-1/2"
	50		2	1	AFH-4254-JF	AFH-4254-JDF	520	600		
	20		1/3		AFH-4226-GF	AFH-4226-GDF	575	610	3"	3/4"
45	30		1/2	1	AFH-4236-JF	AFH-4236-JDF	615	690		
45	40	9	1	1	AFH-4246-JF	AFH-4246-JDF	620	700		1-1/2"
	50		2	1	AFH-4256-JF	AFH-4256-JDF	625	710		
	20		1/3	50	AFH-4228-GF	AFH-4228-GDF	575	610		3/4"
	30		1/2	1	AFH-4238-JF	AFH-4238-JDF	615	690		
60	40	12	1		AFH-4248-JF	AFH-4248-JDF	620	700		1-1/2"
	50		2		AFH-4258-JF	AFH-4258-JDF	625	710		
	20		1/2		AFH-42210- GF	AFH-42210-GDF	785	820		3/4"
75	30	15	3/4	75	AFH-42310-JF	AFH-42310-JDF	825	900		
	40		1	1	AFH-42410-JF	AFH-42410-JDF	830	910		1-1/2"
	50		2	1	AFH-42510-JF	AFH-42510-JDF	835	920		
	20		1/2		AFH-42215- GF	AFH-42215-GDF	1 043	1 078		3/4"
100	30	20	1	1	AFH-42315-JF	AFH-42315-JDF	1 085	1 160		
	40		1-1/2	1	AFH-42415-JF	AFH-42415-JDF	1 095	1 180	4"	1-1/2"
	50		2	1	AFH-42515-JF	AFH-42515-JDF	1 100	1200	4	
	20		3/4	120	AFH-42220- GF	AFH-42220-GDF	1 043	1 078		3/4"
150	30	20	1		AFH-42320- JF	AFH-42320-JDF	1 085	1 160		
150	40	30	1-1/2		AFH-42420- JF	AFH-42420-JDF	1 095	1 180		1-1/2"
	50		3	1	AFH-42520- JF	AFH-42520-JDF	1 110	1220		

Note: All boiler feed units supplied with Armstrong make-up water valve (rated to 45 psig maximum inlet pressure) and gauge glass; solenoid make-up valve available.

Models with higher capacities or discharge pressures available upon request.



Armstrong[®] Stainless Steel Receiver Boiler Feed Packages

AFH-430	00 Series Stainle	ss Steel Rece	eiver Boile	r Feed Pack	ages					
Boiler H.P.	Discharge Pressure PSIG	Pump Cap. G.P.M.	Motor H.P.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In.
	20		1/3		AFH-4322-GF	AFH-4322-GDF	200	240		3/4"
15	30	3	1/2		AFH-4332-JF	AFH-4332-JDF	260	300		
15	40	3	1		AFH-4342-JF	AFH-4342-JDF	265	310		1-1/2"
	50		2	30	AFH-4352-JF	AFH-4352-JDF	275	330		
	20		1/3	30	AFH-4224-GF	AFH-4224-GDF	200	240		3/4"
30	30		1/2		AFH-4334-JF	AFH-4334-JDF	260	300		
30	40	6	1		AFH-4344-JF	AFH-4344-JDF	265	310		1-1/2"
	50		2		AFH-4354-JF	AFH-4354-JDF	275	330		
	20		1/3		AFH-4326-GF	AFH-4326-GDF	240	280		3/4"
45	30		1/2	1 4-	AFH-4336-JF	AFH-4336-JDF	300	340		
45	40	9	1	45	AFH-4346-JF	AFH-4346-JDF	305	350		1-1/2"
	50		2		AFH-4356-JF	AFH-4356-JDF	315	15 370		
	20		1/3		AFH-4328-GF	AFH-4328-GDF	275	335		3/4"
60	30	40	1/2		AFH-4338-JF	AFH-4338-JDF	335	395	,	
60	40	12	1 60	AFH-4348-JF	AFH-4348-JDF	340	405	2-1/2"	1-1/2"	
	50		2		AFH-4358-JF	AFH-4358-JDF	350	425]	
	20		1/2		AFH-43210-GF	AFH-43210-GDF	360	420	1	3/4"
75	30	15	3/4		AFH-43310-JF	AFH-43310-JDF	420	480		
/5	40	15	1		AFH-43410-JF	AFH-43410-JDF	425	490		1-1/2"
	50		2	95	AFH-43510-JF	AFH-43510-JDF	435	510		
	20		1/2	95	AFH-43215-GF	AFH-43215-GDF	360	420		3/4"
400	30	[1		AFH-43315-JF	AFH-43315-JDF	420	480		
100	40	20	1-1/2		AFH-43415-JF	AFH-43415-JDF	425	490		1-1/2"
	50		2		AFH-43515-JF	AFH-43515-JDF	435	510		
	20		3/4		AFH-43220- GF	AFH-43220-GDF	415	475		3/4"
150	30	30	1	120	AFH-43320-JF	AFH-43320-JDF	475	535		
	40		1-1/2		AFH-43420-JF	AFH-43420-JDF	480	545		1-1/2"
	50		3		AFH-43520-JF	AFH-43520-JDF	490	565		

Note: All boiler feed units supplied with Armstrong make-up water valve (rated to 45 psig maximum inlet pressure) and gauge glass; solenoid make-up valve available.

 $\label{thm:models} \mbox{Models with higher capacities or discharge pressures available upon request.}$

Cylindrical Carbon Steel Receiver Boiler Feed Packages



Boiler H.P.	Discharge Pressure PSIG	Pump Cap. G.P.M.	Motor H.P.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In.
	20		3/4		AFH-502150-JF	AFH-502150-JDF	570	665		
450	30	25	1	125	AFH-503150-JF	AFH-503150-JDF	590	685		
150	40	25	1-1/2	125	AFH-504150-JF	AFH-504150-JDF	600	695		
	50		2		AFH-505150-JF	AFH-505150-JDF	615	710		
	20		3/4		AFH-502200-JF	AFH-502200-JDF	635	690		
200	30	20	1	446	AFH-503200-JF	AFH-503200-JDF	640	730		
200	40	30	1-1/2	146	AFH-504200-JF	AFH-504200-JDF	650	750		
	50		2		AFH-505200-JF	AFH-505200-JDF	670	770		
	20		3/4		AFH-502250-JF	AFH-502250-JDF	800	870		
250	30	25	1	175	AFH-503250-JF	AFH-503250-JDF	805	875	2"	
250	0 40 35	35	1-1/2] 1/5	AFH-504250-JF	AFH-504250-JDF	815	885	3"	
	50		2]	AFH-505250-JF	AFH-505250-JDF	840	910		
	20		1		AFH-502300-JF	AFH-502300-JDF	830	920		
200	30	45	1.1/2	240	AFH-503300-JF	AFH-503300-JDF	835	930		
300	40	45	1-1/2	210	AFH-504300-JF	AFH-504300-JDF	840	940		
	50		2		AFH-505300-JF	AFH-505300-JDF	860	980		4.4/0."
	20		1.1/2		AFH-502400-JF	AFH-502400-JDF	900	995		1-1/2"
400	30	55	1-1/2	250	AFH-503400-JF	AFH-503400-JDF	905	1005		
400	40	55	2	250	AFH-504400-JF	AFH-504400-JDF	920	1020		
	50		5		AFH-505400-JF	AFH-505400-JDF	930	1 030		
	20				AFH-502500-JF	AFH-502500-JDF	975	1 070		
F00	30	70	2	220	AFH-503500-JF	AFH-503500-JDF	980	1 075		
500	40	70	3	326	AFH-504500-JF	AFH-504500-JDF	990	1 085		
	50		5		AFH-505500-JF	AFH-505500-JDF	1 045	1 140		
	20		2		AFH-502600-JF	AFH-502600-JDF	1 070	1 170		
600	30	0.5	3	205	AFH-503600-JF	AFH-503600-JDF	1 070	1 170	4"	
600	40	85	_	395	AFH-504600-JF	AFH-504600-JDF	1090	1 190	4"	
	50		5		AFH-505600-JF	AFH-505600-JDF	1090	1 190		
	20		2		AFH-502700-JF	AFH-502700-JDF	1 235	1335		
700	30	100		470	AFH-503700-JF	AFH-503700-JDF	1 245	1345		
700	40	100	5	1 470 ⊢	AFH-504700-JF	AFH-504700-JDF	1 245	1345		
	50				AFH-505700-JF	AFH-505700-JDF	1 295	1395		

Note: All boiler feed units supplied with Armstrong make-up water valve (rated to 45 psig maximum inlet pressure) and gauge glass; solenoid make-up valve available.

Models with higher capacities or discharge pressures available upon request.



Cylindrical Elevated Carbon Steel Receiver Boiler Feed Packages

		uncai Elevat	ed Carbo	JII Steer Re	ceiver Boiler Fee	-u Fackages							
Boiler H.P.	Discharge Pressure PSIG	Pump Cap. G.P.M.	Motor H.P.	Rec. Cap Gal.	Unit Model No. Simplex	Unit Model No. Duplex	Weight (lb) Simplex	Weight (lb) Duplex	Disch. Size In.	Inlet Size In			
	20		1/2		AFH-35215-GF	AFH-35215-GDF	265	325	3/4				
15	30	3	1/2		AFH-35315-JF	AFH-35315-JDF	285	365					
15	40] 3	1		AFH-35415-JF	AFH-35415-JDF	290	375	1-1/2				
	50		2	33	AFH-35515-JF	AFH-35515-JDF	310	415		4			
	20		1/2	33	AFH-35230-GF	AFH-35230-GDF	265	325	3/4	4			
30	30	6	1/2		AFH-35330-JF	AFH-35330-JDF	285	365					
30	40		1		AFH-35430-JF	AFH-35430-JDF	290	375	1-1/2				
	50		2		AFH-35530-JF	AFH-35530-JDF	310	415					
	20		1/2		AFH-35245-GF	AFH-35245-GDF	350	410	3/4				
45	30	9	1/2	49	AFH-35345-JF	AFH-35345-JDF	370	450					
45	40] 9	1	49	AFH-35445-JF	AFH-35445-JDF	375	460	1-1/2				
	50		2		AFH-35545-JF	AFH-35545-JDF	395	500		_			
	20		1/2		AFH-35260-GF	AFH-35260-GDF	390	450	3/4	5			
60	30	42	1/2		AFH-35360-JF	AFH-35360-JDF	410	490]			
60	40	12	1	65	AFH-35460-JF	AFH-35460-JDF	415	500	1-1/2				
	50]	2	1	AFH-35560-JF	AFH-35560-JDF	435	540					
	20		1/2		AFH-35275-GF	AFH-35275-GDF	440	500	3/4				
I	30	1	3/4	1	AFH-35375-JF	AFH-35375-JDF	460	540		1			
75	40	15	1		AFH-35475-JF	AFH-35475-JDF	465	550	1-1/2				
	50	1	2	1	AFH-35575-JF	AFH-35575-JDF	485	590					
	20		1/2	95	AFH-352100-GF	AFH-352100-GDF	615	675	3/4	1			
	30		3/4	1	AFH-353100-JF	AFH-353100-JDF	635	715	3/4	1			
100	40	20	20	20	20	1-1/2		AFH-354100-JF	AFH-354100-JDF	645	735	1-1/2	
	50	_	2		AFH-355100-JF	AFH-355100-JDF	660	765		ĺ			
	20		3/4		AFH-352150-GF	AFH-352150-GDF	720	790	3/4	1			
	30	-	1		AFH-353150-JF	AFH-353150-JDF	740	830		1			
150	40	30	1-1/2	146	AFH-354150-JF	AFH-354150-JDF	750	850	-				
	50	-	3		AFH-355150-JF	AFH-355150-JDF	770	890					
	20		1		AFH-352200-JF	AFH-352200-JDF	930	1020					
	30	-	1-1/2		AFH-353200-JF	AFH-353200-JDF	935	1030					
200	40	40	2	210	AFH-354200-JF	AFH-354200-JDF	940	1040		6			
	50	1	3		AFH-355200-JF	AFH-355200-JDF	960	1 080					
	20		2		AFH-352500-JF	AFH-352500-JDF	1335	1450					
	30	1		1	AFH-353500-JF	AFH-353500-JDF	1340	1460					
500	40	100	3	470	AFH-354500-JF	AFH-354500-JDF	1340	1460	1-1/2				
	50	1	5	†	AFH-355500-JF	AFH-355500-JDF	1390	1560					
	20		2		AFH-352600-JF	AFH-352600-JDF	1 440	1 555					
	30	1	3	1	AFH-353600-JF	AFH-353600-JDF	1 445	1 565					
600	40	120		595	AFH-354600-JF	AFH-354600-JDF	1495	1 665					
	50	1	5		AFH-355600-JF	AFH-355600-JDF	1495	1 665					
	20		3		AFH-352700-JF	AFH-352700-JDF							
	30	-		1	AFH-352700-JF	AFH-352700-JDF	1605	1775					
	30	140	5	714		AFH-353700-JDF	1605	1775					
700	40				AFH-354700-JF								

Note: All boiler feed units supplied with Armstrong make-up water valve (rated to 45 psig maximum inlet pressure) and gauge glass; solenoid make-up valve available.

Models with higher capacities or discharge pressures available upon request..

AFH 4400 Series Stainless Steel Condensate Return Units



High Quality Stainless Steel Exceptional Value, Extraordinary Quality

Armstrong Stainless Steel Condensate Return Units offer the best materials available for long life. Tanks have a 20-year warranty against failure due to corrosion and are made from 304 SS with internal ribbing where needed for excellent strength. Available in six standard sizes; 12, 25, 45, 70, and 100 gallon capacities (with custom sizes available) in simplex or duplex pump configuration. Compact dimensions and light weight make it a simple task to replace your old cast iron unit. System accessories are of the highest quality.

These pumps are made of investment cast 316 stainless steel. The single stage impeller is of semi-open design allowing for occasional pumping of small solids without clogging. Pump is permanently aligned to the electric motor, never requiring alignment at the job site. Pumps are furnished with 250°F mechanical seals, and are equipped with a seal cavity bleed line to keep the seal lubricated and minimize the probability of premature seal failure. Pump discharge openings are NPT.

Standard motors are: three phase- 208/230/460 V TEFC, Single phase -115/208/230 V ODP. Other voltages are available on request. Other motors available are explosion proof, wash down duty, premium efficiency, and any other motor available with a 56C frame.

Motor/pump controls available for simplex, duplex, triplex, and quadplex, in single phase or three phase with a limitless array of available options for any requirement. NEMA 1 is standard enclosure. All other enclosures are available.





AFH 4400 Series Armstrong Stainless Steel Condensate Return Units

EDR (SQ. FT.)	PSIG	GРM	MOTOR HP	TANK SIZE	SIMPLEX MODEL NUMBER THREE PHASE	SIMPLEX MODEL NUMBER SINGLE PHASE	DUPLEX MODEL NUMBER THREE PHASE	DUPLEX MODEL NUMBER SINGLE PHASE
	10		1/3		AFH-44S3106	AFH-44S1106	AFH-44D3106	AFH-44D1106
	20		1/3		AFH-44S3206	AFH-44S1206	AFH-44D3206	AFH-44D1206
	25		1/2		AFH-44S3256	AFH-44S1256	AFH-44D3256	AFH-44D1256
4000	30	6	3/4		AFH-44S3306	AFH-44S1306	AFH-44D3306	AFH-44D1306
	40		1		AFH-44S3406	AFH-44S1406	AFH-44D3406	AFH-44D1406
	50		1-1/2	40	AFH-44S3506	AFH-44S1506	AFH-44D3506	AFH-44D1506
	10		1/3	12	AFH-44S3109	AFH-44S1109	AFH-44D3109	AFH-44D1109
	20		1/3		AFH-44S3209	AFH-44S1209	AFH-44D3209	AFH-44D1209
6000	25	9	1/2		AFH-44S3259	AFH-44S1259	AFH-44D3259	AFH-44D1259
0000	30	9	1		AFH-44S3309	AFH-44S1309	AFH-44D3309	AFH-44D1309
	40		1-1/2		AFH-44S3409	AFH-44S1409	AFH-44D3409	AFH-44D1409
	50		1-1/2		AFH-44S3509	AFH-44S1509	AFH-44D3509	AFH-44D1509
	10		1/3		AFH-44S31015	AFH-44S11015	AFH-44D31015	AFH-44D11015
	20		1/2		AFH-44S32015	AFH-44S12015	AFH-44D32015	AFH-44D12015
10000	25	15	1/2		AFH-44S32515	AFH-44S12515	AFH-44D32515	AFH-44D12515
	30		1		AFH-44S33015	AFH-44S13015	AFH-44D33015	AFH-44D13015
	40		1-1/2		AFH-44S34015	AFH-44S14015	AFH-44D34015	AFH-44D14015
	50		2	25	AFH-44S35015	AFH-44S15015	AFH-44D35015	AFH-44D15015
	10		1/3		AFH-44S31022	AFH-44S11022	AFH-44D31022	AFH-44D11022
	20		1/2		AFH-44S32022	AFH-44S12022	AFH-44D32022	AFH-44D12022
15000	25	22.5	1		AFH-44S32522	AFH-44S12522	AFH-44D32522	AFH-44D12522
	30		1-1/2		AFH-44S33022	AFH-44S13022	AFH-44D33022	AFH-44D13022
	40 50		3		AFH-44S34022 AFH-44S35022	AFH-44S14022	AFH-44D34022 AFH-44D35022	AFH-44D14022
	10		1/3		AFH-44S31030	AFH-44S11030	AFH-44D33022 AFH-44D31030	AFH-44D11030
20000	20 25	20	3/4		AFH-44S32030 AFH-44S32530	AFH-44S12030 AFH-44S12530	AFH-44D32030 AFH-44D32530	AFH-44D12030 AFH-44D12530
20000	30	30						
			1-1/2		AFH-44S33030	AFH-44S13030	AFH-44D33030	AFH-44D13030
	40		2		AFH-44S34030	AFH-44S14030	AFH-44D34030	AFH-44D14030
	10		1/2		AFH-44S31037	AFH-44S11037	AFH-44D31037	AFH-44D11037
	20		3/4		AFH-44S32037	AFH-44S12037	AFH-44D32037	AFH-44D12037
25000	25	37.5	1-1/2	45	AFH-44S32537	AFH-44S12537	AFH-44D32537	AFH-44D12537
	30		1-1/2		AFH-44S33037	AFH-44S13037	AFH-44D33037	AFH-44D13037
	40		3		AFH-44S34037		AFH-44D34037	
	10		1/2		AFH-44S31045	AFH-44S11045	AFH-44D31045	AFH-44D11045
	20		3/4		AFH-44S32045	AFH-44S12045	AFH-44D32045	AFH-44D12045
30000	25	45	1-1/2		AFH-44S32545	AFH-44S12545	AFH-44D32545	AFH-44D12545
	30		2		AFH-44S33045	AFH-44S13045	AFH-44D33045	AFH-44D113045
	40		3		AFH-44S34045		AFH-44D34045	
	10		3/4		AFH-44S31060	AFH-44S11060	AFH-44D31060	AFH-44D11060
	20		1		AFH-44S32060	AFH-44S12060	AFH-44D32060	AFH-44D12060
40000		60						
	25		2	_	AFH-44S32560	AFH-44S12560	AFH-44D32560	AFH-44D12560
	30		2	70	AFH-44S33060	AFH-44S13060	AFH-44D33060	AFH-44D13060
	10		3/4		AFH-44S31070	AFH-44S11070	AFH-44D31070	AFH-44D11070
50000	20	70	1		AFH-44S32070	AFH-44S12070	AFH-44D32070	AFH-44D12070
	25		2		AFH-44S32570	AFH-44S12570	AFH-44D32570	AFH-44D12570
60000	15	90	1	100	AFH-44S31590	AFH-44S11590	AFH-44D31590	AFH-44D11590

Standard unit includes:

Stainless steel tank complete with flange mounted stainless steel pump close coupled to motor of HP shown 115/208-230V/1/60 ODP or 208/230/460v/3/60 3450 RPM TEFC. Simplex unit has NEMA 1 float switch and duplex has NEMA 1 mechanical alternator. Sight Glass is standard.

Additional motor options are: Washdown duty and explosion proof.

Additional Accessories: Thermometer, Electrical enclosures, Isolation valves.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

AFH 4400 Series Stainless Steel Condensate Return Unit Accessories (210°F)



All Stainless Steel Electric Condensate Pumps (Simplex) 210°F Capable

AFH-4400 Se	ries All Stainle	ss Steel Electr	ic Pump Pack	ages good to 2	210° max water temp	
EDR (Sq. Ft.)	PSIG	GPM	Motor HP	Tank Size	Simplex Model Number Three Phase	Simplex Model Number Single Phase
	20		1/2		AFH-44S32FT206	AFH-44S12FT206
4 000	25	6	1/2	12	AFH-44S32FT256	AFH-44S12FT256
	30		3/4		AFH-44S32FT306	AFH-44S12FT306
	20		1/2		AFH-44S32FT209	AFH-44S12FT209
6 000	25	9	3/4	12	AFH-44S32FT259	AFH-44S12FT259
	30		3/4		AFH-44S32FT309	AFH-44S12FT309
	20		3/4		AFH-44S32FT2015	AFH-44S12FT2015
10 000	25	15	1/2	25	AFH-44S32FT2515	AFH-44S12FT2515
	30					
	20		1/2		AFH-44S32FT2022	AFH-44S12FT2022
15 000	25	22.5	1/2	25	AFH-44S32FT2522	AFH-44S12FT2522
	30					

^{*}Use standard Simplex/Duplex drawings.

All Stainless Steel Electric Condensate Pumps (Duplex) 210°F Capable

AFH-4400 Se	ries All Stainles	s Steel Electric	Pump Packag	es good to 210	0° max water temp	
EDR (Sq. Ft.)	PSIG	GPM	Motor HP	Tank Size	Duplex Model Number Three Phase	Duplex Model Number Single Phase
	20		1/2		AFH-44D32FT206	AFH-44D12FT206
4 000	25	6	1/2	12	AFH-44D32FT256	AFH-44D12FT256
	30		3/4		AFH-44D32FT306	AFH-44D12FT306
	20		1/2		AFH-44D32FT209	AFH-44D12FT209
6 000	25	9	3/4	12	AFH-44D32FT259	AFH-44D12FT259
	30		3/4		AFH-44D32FT309	AFH-44D12FT309
	20		3/4		AFH-44D32FT2015	AFH-44D12FT2015
10 000	25	15	1/2	25	AFH-44D32FT2515	AFH-44D12FT2515
	30					
	20		1/2		AFH-44D32FT2022	AFH-44D12FT2022
15 000	25	22.5	1/2	25	AFH-44D32FT2522	AFH-44D12FT2522
	30					

^{*}Use standard Simplex/Duplex drawings.



AFH 4400 Series Stainless Steel Condensate Return Unit Accessories (212°F)

All Stainless Steel Electric Condensate Pumps (Simplex) 212°F Capable

AFH-4400 Se	ries All Stainle	ss Steel Electr	ic Pump Pack	ages good to 2	212° max water temp	
EDR (Sq. Ft.)	PSIG	GPM	Motor HP	Tank Size	Simplex Model Number Three Phase	Simplex Model Number Single Phase
	20		1/2		AFH-44S32FTE206	AFH-44S12FTE206
4 000	25	6	1/2	12	AFH-44S32FTE256	AFH-44S12FTE256
	30		3/4		AFH-44S32FTE306	AFH-44S12FTE306
	20		1/2		AFH-44S32FTE209	AFH-44S12FTE209
6 000	25	9	3/4	12	AFH-44S32FTE259	AFH-44S12FTE259
	30		3/4		AFH-44S32FTE309	AFH-44S12FTE309
	20		3/4		AFH-44S32FTE2015	AFH-44S12FTE2015
10 000	25	15	1/2	25	AFH-44S32FTE2515	AFH-44S12FTE2515
	30					
	20		1/2		AFH-44S32FTE2022	AFH-44S12FTE2022
15 000	25	22.5	1/2	25	AFH-44S32FTE2522	AFH-44S12FTE2522
	30					

^{*}Use standard Simplex/Duplex drawings.

All Stainless Steel Electric Condensate Pumps (Duplex) 212°F Capable

AFH-4400 Sei	ries All Stainles	s Steel Electric	: Pump Packag	ges good to 212	2° max water temp	
EDR (Sq. Ft.)	PSIG	GPM	Motor HP	Tank Size	Duplex Model Number Three Phase	Duplex Model Number Single Phase
	20		1/2		AFH-44D32FTE206	AFH-44D12FTE206
4 000	25	6	1/2	12	AFH-44D32FTE256	AFH-44D12FTE256
	30		3/4		AFH-44D32FTE306	AFH-44D12FTE306
	20		1/2		AFH-44D32FTE209	AFH-44D12FTE209
6 000	25	9	3/4	12	AFH-44D32FTE259	AFH-44D12FTE259
	30		3/4		AFH-44D32FTE309	AFH-44D12FTE309
	20		3/4		AFH-44D32FTE2015	AFH-44D12FTE2015
10 000	25	15	1/2	25	AFH-44D32FTE2515	AFH-44D12FTE2515
	30					
	20		1/2		AFH-44D32FTE2022	AFH-44D12FTE2022
15 000	25	22.5	1/2	25	AFH-44D32FTE2522	AFH-44D12FTE2522
	30					

^{*}Use 212°F Elevated Receiver drawing.

AFH 4400 Series

Stainless Steel Condensate Return Unit Accessories





Sight Gauge Assembly

SS bottom fixture with shut-off valve, SS top fixture, 2- heavy duty SS glass guards, and tempered glass tube.

Stainless Steel Butterfly Isolation Valves (Optional)

Butterfly Isolation Valves between pump and receiver are available. These valves are of great value when removing one pump of a duplex system without having to shut the system down.

Float Switches

Float Switches are heavy duty 2 pole with stainless steel rod and float. Duplex alternating float switch includes high level lag pump on feature.

Nema 1 standard, Nema 4 and Nema 7/9 are available.

Pressure Gauges (Optional) Not Shown

2 1/2" Liquid Filled SS Casing

Thermometer (Optional)

2 1/2" Diameter face, Bi-metal, 4" stem, Range 32 - 250°F.







4100/4200/4300/3500/5000 Series

Electric and Boiler Feed Control Panel and Accessories

Features

- Motor circuit protector (MCP)
- HOA selector switch
- External reset
- · Control circuit transformer
- Pilot light (pump running)
- Removable mounting plate and thermal strip in a single NEMA 12 enclosure
- Mounted and wired with single-point power connection
- CE
- · CSA
- · UL listed component

Options

- UL certification
- · CUL certification
- Pilot light
- Test push button
- Electric alternator
- · Low water cutoff
- Manual transfer switch (boiler feed only)
- High-level alarm horn and light with silencing switch
- · Low-level alarm horn and light with silencing switch
- Remote mounting deduction
- Simplex, triplex, quadruplex pumps
- · Explosion proof
- NEMA 4, 4X

Special Options

- · Mechanical and electrical alternators
- Thermometer
- Isolation valves
- · Special motor construction
 - TEFC
 - Explosion proof
- 1750 RPM motors
- · Larger pumping capacities
- Higher discharge pressures
- · 2' NPSH Rating
- Water level gauge
- · Discharge pressure gauges
- Inlet strainer



Control Panel



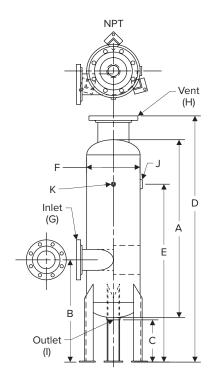
Water Level Gauge (optional on most models)



Isolation Valve (optional on most models)

Vertical Flash Tanks (VAFT)







Features

- ASME coded and stamped vessels
- Standard pressure rating 150 psig (other pressure ratings available upon request)
- Standard models are designed and sized to cover a wide range of applications and loads
- Flash vessels are designed to provide low velocity flash steam with no water carryover
- Quick payback for flash recovery investment
- Special tanks available upon request

For a fully detailed certified drawing, refer to CDF #1023.

Flash Steam Savings Analysis

Part I: Determining the amount of flash steam produced

•	art i. Determining the amount of hash st	cum produce	·u
Α	. Condensate Load	A =	_ lb/hr.
В	. Annual hours of operation	B =	_ hrs/yr.
C	. Steam Cost	C =	_ \$/1 000 lbs.
D	. Flash steam percentage from chart (on page 264)	D =	_ %
F	Flash steam produced:		

Part II: Determining dollar value of the flash steam

 $D \times A = flash steam produced$

F. Annual flash steam savings:

Physica	Physical Data—Standard Design Model VAFT												
Model	AF	T-6	AF	T-8	AFT-12		AFT-16						
No.	in	mm	in	mm	in	mm	in	mm					
Α	36	914	36	914	40	1 016	48	1 219					
В	21	533	21	533	23	584	26	660					
С	9-1/2	241	9-1/2	241	9-1/2	241	9-1/2	241					
D	51	1295	52	1321	55- 3/8	1407	63-1/2	1 613					
Е	36	914	36	914	40	1 016	48	1 219					
F	6	150	8	203	12	305	16	406					
G	2	50	3	80	4	102	6	150					
Н	2-1/2	65	4	102	6	150	6	150					
Ī	1-1/2	40	1-1/2	40	2	50	2	50					
J	3/4	20	1	25	1-1/2	40	2	50					
K	1/2	15	1/2	15	1/2	15	1/2	15					

NOTE: Connections "G" and "H" are 150 lb. flanges. All others are NPT. All flash tanks are ASME coded for 150 psig (10 barg). Special sizes available upon request.

Capacitie	Capacities—Standard Design Model VAFT											
Model	Maximum Cor	ndensate Load	Maximum Flash Load									
No.	lb/hr	kg/hr	lb/hr	kg/hr								
AFT-6	2 000	907	325	147								
AFT-8	5 000	2 268	900	408								
AFT-12	10 000	4 536	2 000	907								
AFT-16	20 000	9 072	2 000	907								

lb/hr.



Series VAFT-BDV Boiler Blowdown Vessels

All Stainless Steel

For pressures to 150 psig (10 barg) / Capacities to 20 000 lb/hr (9 072 kg/hr)

Description

The Armstrong VAFT-BDV blowdown vessel is designed to efficiently separate surface blowdown water and flash steam. Built according to ASME Section VIII standards, the design is compact, requiring a small footprint in which to operate. For blowdown loads up to 20 000 lb/hr (9 072 kb/hr), Armstrong has a model to fit your needs.

- ASME-coded and stamped vessels
- 3/8" Carbon steel construction
- Stainless Steel Strike Plate
- Standard pressure rating 150 psig (10 barg) (Other pressure
- ratings available.)
- Vessels are designed to provide low velocity flash steam with no water carryover.

Standard Models:

VAFT-1238BDV (12") VAFT-1638BDV (16")

Optional Equipment:

- 3/4" Commercial or Industrial Aftercooler Assembly
- 1" Commercial or Industrial Aftercooler Assembly
- Pressure Guage
- Safety Relief Valve



Blowdown Vesse	Blowdown Vessel										
Model	Condensate Load/ Flash Load lb/hr	Diameter(in)	Inlet Size (in)	Discharge Size (in)	Material	Weight (lb)					
VAFT1238BDV	max 10 000/max 2 000	12	4	3	CS 150F 3/8" Nominal Thickness						
VAFT1638BDV	max 20 000/max 3 000	16	6	3	CS 150F 3/8" Nominal Thickness	Consult Factory					

Horizontal Flash Tanks (HAFT)



Features

- · ASME coded and stamped vessels
- Standard pressure rating 150 psig (other pressure ratings available upon request)
- Standard models are designed and sized to cover a wide range of applications and loads
- Flash vessels are designed to provide low velocity flash steam with no water carryover
- · Quick payback for flash recovery investment
- · Special tanks available upon request
- HAFT-Series horizontal flash tanks for low flash load applications.

For a fully detailed certified drawing, refer to CDF #1038.

Flash Steam Savings Analysis

Part I: Determining the amount of flash steam produced

A. Condensate Load	A = lb/hr.
B. Annual hours of operation	B = hrs/yr.
C. Steam Cost	C = \$/1 000 lbs
D. Flash steam percentage from chart (on page 264)	D = %

E. Flash steam produced:

D x A = flash steam produced E =_____ lb/hr.

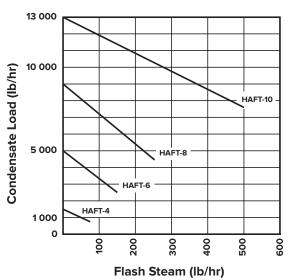
Part II: Determining dollar value of the flash steam

F. Annual flash steam savings:

NOTES

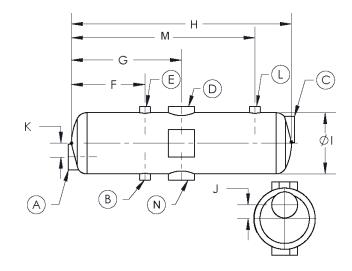
- 1. Models are ASME SEC. VIII "U" stamped for 150 psig
- 2. All connections are FNPT.





Physical Data — Standard Design Model (HAFT)								
Model	HAFT-10		HAFT-8		HAFT-6		HAFT-4	
No.	in	mm	in	mm	in	mm	in	mm
Α	3	76	2	50	1-1/2	38	1-1/2	38
В	1	25	1	25	1	25	1	25
С	3	76	2	50	1-1/2	38	1-1/2	38
D	3	76	2-1/2	64	2	50	1-1/2	38
Е	1	25	1	25	1	25	1	25
F	12	305	12	305	12	305	8	203
G	18	457	18	457	18	457	12	305
Н	36	914	36	914	36	914	24	610
I	10	254	8	203	6	152	4	102
J	2-1/4	57	1-3/4	44	1-1/4	32	1	25
K	2-1/4	57	1-3/4	44	1-1/4	32	1	25
L	1	25	1	25	1	25	1	25
М	30	762	30	762	30	762	18	457
N	3	76	2	50	2	50	1-1/2	38

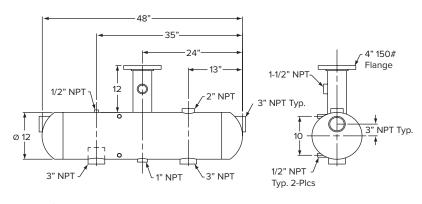
Note: All flash tanks are ASME coded for 150 psig (10 barg). Special sizes and connections available upon request.

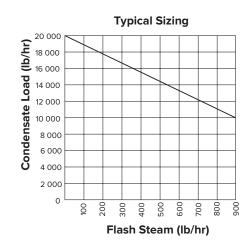


Capacities — Standard Design Model (HAFT)						
Model No.	Maximum Condensate Load					
	lb/hr	kg/hr				
HAFT-10	13 000	5 897				
HAFT-8	9 000	4 082				
HAFT-6	5 000	2 268				
HAFT-4	1500	680				



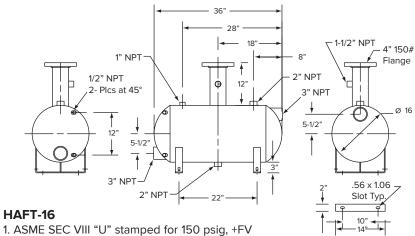
Horizontal Flash Tanks (HAFT)

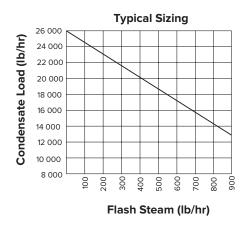




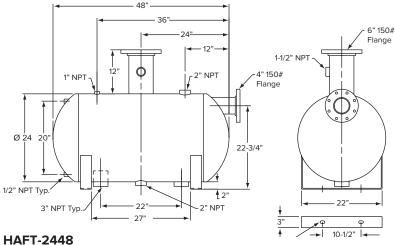
HAFT-12

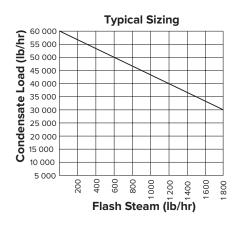
- 1. ASME SEC VIII "U" stamped for 150 psig, +FV
- 2. Temperature rating -20° to 550°F
- 3. Approximate volume: 22 gallons
- 4. Maximum flash load 900 lb/hr





- 2. Temperature rating -20° to 550°F
- 3. Approximate volume: 30 gallons
- 4. Maximum flash load 900 lb/hr

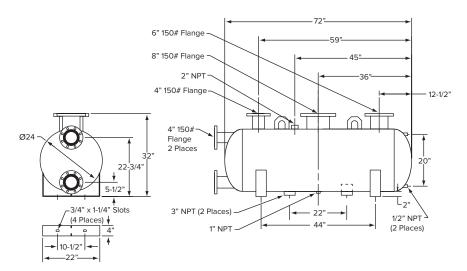


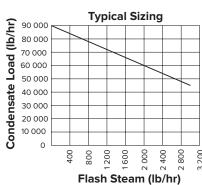


- 1. ASME SEC VIII "U" stamped for 150 psig, +FV
- 2. Temperature rating -20° to 550°F
- 3. Approximate volume: 85 gallons
- 4. Maximum flash load 1800 lb/hr

Horizontal Flash Tanks (HAFT)

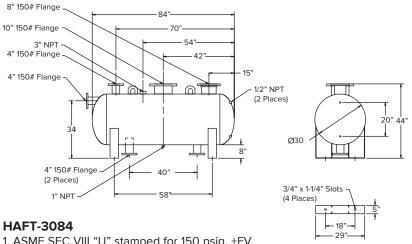


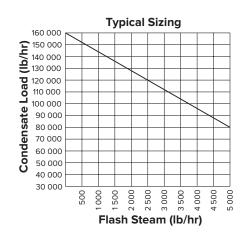




HAFT-2472

- 1. ASME SEC VIII "U" stamped for 150 psig, +FV
- 2. Temperature rating -20° to 550°F
- 3. Approximate volume: 130 gallons
- 4. Maximum flash load 3 000 lb/hr





- 1. ASME SEC VIII "U" stamped for 150 psig, +FV
- 2. Temperature rating -20° to 550°F
- 3. Approximate volume: 240 gallons
- 4. Maximum flash load 5 000 lb/hr



Armstrong® Flash Recovery Vessels

How much flash steam is available?

- 1. Follow horizontal axis right to primary discharge pressure.
- 2. Follow vertically up to secondary pressure curve.
- 3. Move left to "Percentage of flash steam."

Example:

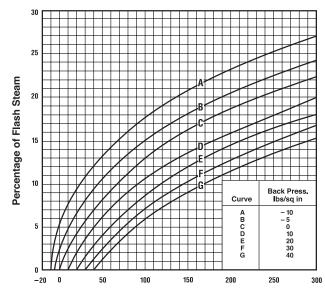
Condensate load = 10 000 lb/hr Primary pressure = 100 psig Secondary pressure = 10 psig

Percentage of flash = 10.6% Secondary steam load = 1 060 lb/hr (10 000 lb/hr x .1060 = 1 060 lb/hr)

Selection:

Model AFT-12

Percentage of Flash Steam Formed When Discharging Condensate to Reduced Pressure



PSI From Which Condensate Is Discharged

Application Information

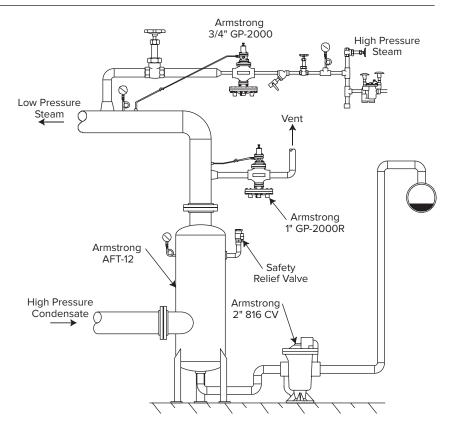
- A. Condensate Load to Flash Tank 6 000 lb/hr
- B. Pressure of Incoming Condensate 100 psig
- C. Flash Tank Pressure 20 psig
- D. Flash Percentage 9.5%
- E. Flash Amount = $A \times (D/100) = 570 \text{ lb/hr}$
- F. Low Pressure Steam Required 2 500 lb/hr
- G. High Pressure Steam 200 psig
- H. Back Pressure 5 psig

Flash tank will accommodate (A) **6 000** lb/hr of condensate at (B) **100** psig, resulting in (E) **570** lb/hr of flash steam at (C) **20** psig. The flash tank shall be Armstrong Model AFT-12.

The back pressure regulator shall pass (E) **570** lb/hr of steam from (C) 20 psig to atmosphere. The back pressure regulator shall be Armstrong Model **1" GP-2000R.**

The pressure reducing valve shall pass (F) 2 500 lb/hr of steam from (G) 200 psig to (C) 20 psig. Pressure reducing valve shall be 3/4" GP-2000.

The steam trap shall be an inverted bucket type with large vent and internal check valve. The steam trap will be sized using a 3:1 safety factor. The steam trap shall pass $3 \times (A - E)$ 16 290 lb/hr at a (C - H) 15 psig differential. The steam trap shall be an Armstrong Model 2" 816 CV.



Notes	Armstrong



PT-12F

High Capacity Pump Trap

Description

Armstrong's PT-12F pump trap offers a non-electric solution to move condensate from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. The PT-12F is an ASME code-stamped carbon steel vessel, capable of returning condensate at temperatures well above the 200°F (93°C) limit of conventional electric pumps.

Features

- Low-maintenance, non-electric operation. No leaking seals, impeller or motor problems. No NPSH issues.
- Externally removable vent and motive seats
- ASME Section VIII "U" stamped vessel
- Lower installation costs. Single trade installation.
- ASME Carbon Steel durability, Inconel X-750 springs and all
- · stainless steel internals for long service life
- Safety. The pump can be used in pits or sumps without fear of electrocution or circuit breaker defaults.

Maximum Operating Conditions

Maximum allowable pressure: 200 psig @ 400°F (14 bar @ 204°C)

Maximum operating pressure: 200 psig @ 400°F (14 bar @ 204°C) (Consult factory for different pressure/temperature ratings and materials)

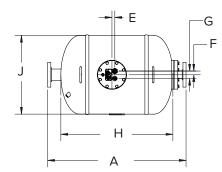
Materials

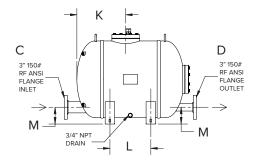
Body: Carbon Steel
Springs: Inconel X-750
Internals: Stainless Steel

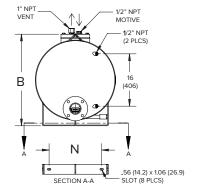
For a fully detailed certified drawing, refer to CD2914.

PT-12F Physical Data		
	in	mm
"A"	42	1067
"B"	28	711.5
"C"	3	80
"D"	3	80
"E"	7/8	22
"F"	1-1/8	28
"G"	2-1/4	57
"H"	34	864
"J"	24	610
"K"	15-1/2	394
"L"	13	330
"M"	5-1/4	133
"N"	16	406
Weight lb (kg)	348	3 (158)











PT-12F Pum	p Capacities						
Мо	tive	Back P	ressure	Steam	Motive	Air M	lotive
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr
15 25 50 75 100 125 150 175 200	1 1.7 3.5 5 7 8.5 10.34 12 14	5	0.34	9 800 12 900 16 500 18 200 18 900 19 300 19 800 19 900	4 445 5 581 7 484 8 255 8 573 8 754 8 981 9 026 9 026	15 800 17 800 18 800 19 500 - - - - -	7 166 8 073 8 526 8 844 - - - - -
25 50 75 100 125 150 175 200	1.7 3.5 5 7 8.5 10.34 12 14	15	1	8 500 12 900 14 800 16 000 16 400 17 200 17 300 17 300	3 856 5 851 6 713 7 257 7 439 7 802 7 847 7 847	14 000 17 500 18 300 - - - - -	6 349 7 937 8 299 - - - - -
35 50 75 100 125 150 175 200	2.5 3.5 5 7 8.5 10.34 12 14	25	1.5	7 200 10 300 12 300 13 700 13 700 14 700 14 800 15 000	3 266 4 672 5 579 6 214 6 214 6 668 6 713 6 804	12 700 15 600 16 800 - - - - -	5 760 7 075 7 619 - - - - -
50 75 100 125 150 175 200	3.5 5 7 8.5 10.34 12 14	40	2.75	6 700 9 500 10 600 10 900 11 300 11 300 11 400	3 039 4 309 4 808 4 944 5 126 5 126 5 171	12 100 14 700 - - - - -	5 488 6 667 - - - - -
75 100 125 150 175 200	5 7 8.5 10.34 12 14	60	4	6 900 8 300 8 300 8 400 8 400 8 600	3 130 3 765 3 765 3 810 3 810 3 901	10 900 - - - - -	4 943 - - - - -
100 125 150 175 200	7 8.5 10.34 12 14	80	5.5	6 400 6 400 7 200 7 200 7 300	2 903 2 903 3 266 3 266 3 311	9 600 - - - -	4 354 - - - -

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump case.

Capacity Conversion Factors for Other Filling Heads													
Filling Head													
in	0	6	12	24	* 24 or greater								
mm													
Capacity Multiplier	0.7	85	10	108	* Consult factory								

NOTE: Fill head measured from drain to top of cap.



PT-6F

Low Profile Pump Trap

Description

Armstrong's PT-6F pump trap offers a low profile non-electric solution to move condensate from low points, low pressures or vacuum spaces to an area of higher elevation or pressure. The PT-6F is an ASME code-stamped carbon steel vessel, and will return condensate at temperatures well above the 200°F (93°C) limit of conventional electric pumps.

Features

- Low-maintenance, non-electric operation. No leaking seals, impeller or motor problems. No NPSH issues.
- Externally removable vent and motive seats
- · ASME Section VIII "U" stamped vessel
- Space-saving size, low-profile body fits in tight spaces
- ASME Carbon Steel durability, Inconel X-750 springs and all stainless steel internals for long service life
- · Lower installation costs. Single trade installation F
- Safety. The pump can be used in pits or sumps without fear of electrocution or circuit breaker defaults.

Maximum Operating Conditions

Maximum allowable pressure: 200 psig @ 400°F (14 bar @ 204°C)

Maximum operating pressure: 200 psig @ 400°F (14 bar @ 204°C)

Materials

Body: Carbon Steel
Springs: Inconel X-750
Internals: Stainless Steel

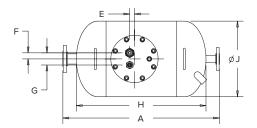
(Consult factory for different pressure/temperature ratings and materials)

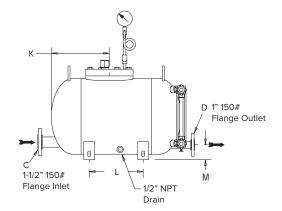
For a fully detailed certified drawing, refer to CD2913.

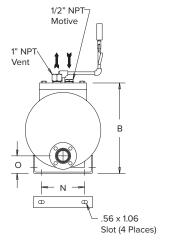
PT-6F Physical Data		
	in	mm
"A"	29	737
"B"	16-11/16	424
"C"	1-1/2	38
"D"	1	25
"E"	7/8	22
"F"	1-1/8	28
"G"	2-1/4	57
"H"	24	610
"J"	14	356
"K"	10-13/16	275
"L"	10	254
"M"	2-13/16	71
"N"	8	203
"O"	3-3/16	81
Weight lb (kg)	140) (64)



PT-6F







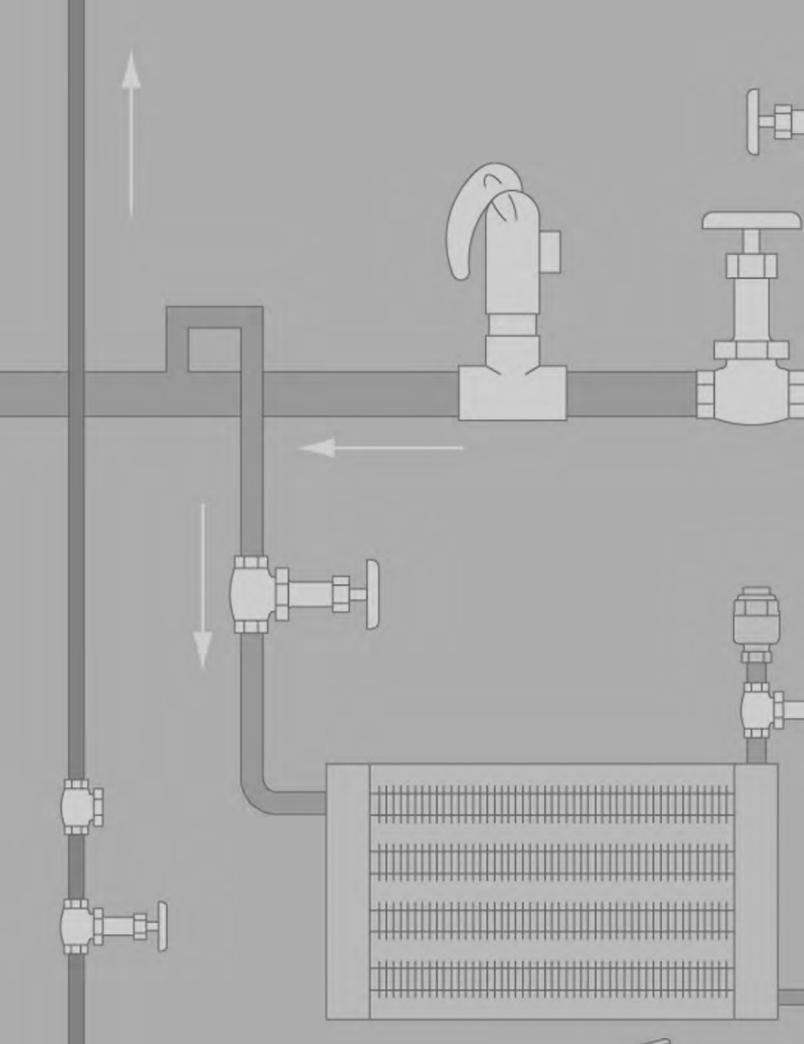


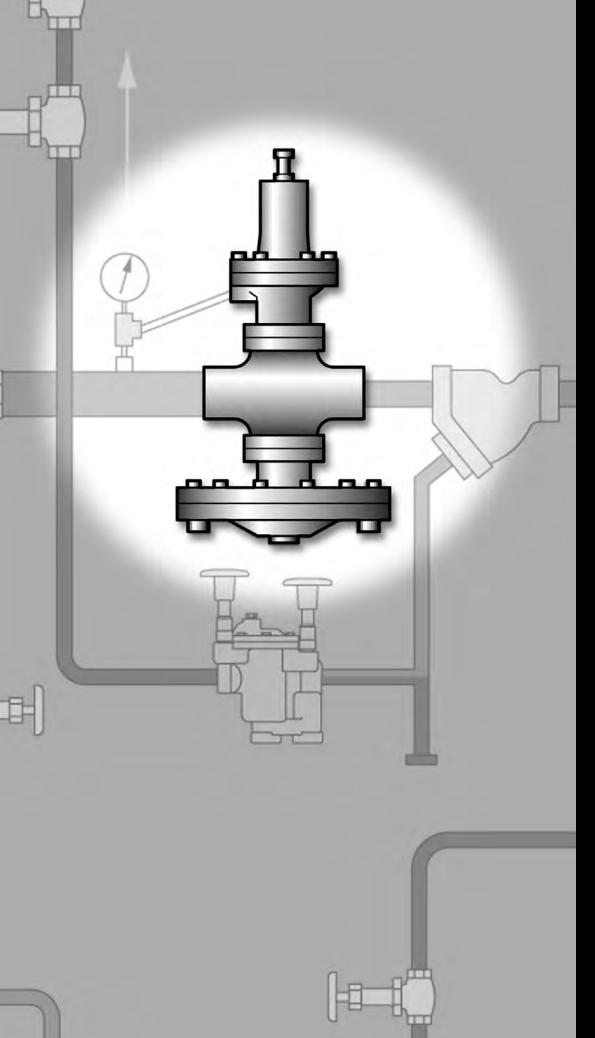
M	otive	Back P	ressure	Stear	n Motive	Air M	otive
psig	barg	psig	barg	lb/hr	kg/hr	lb/hr	kg/hr
15	1			2 400	1 089	3 600	1 632
25	1.7			3 000	1 361	4 500	2 040
50	3.5			4 000	1 814	5 500	2 494
75	5			4 500	2 041	6 000	2 721
100	7	5	0.34	4 600	2 087	-	-
125	8.5			4 700	2 132	-	-
150	10.34			4 800	2 177	-	-
175	12			4 800	2 177	-	-
200	14			4 600	2 087	-	-
25	1.7			2 000	907	4 000	1 814
50	3.5			2 800	1 270	4 500	2 045
75	5			3 400	1542	5 000	2 267
100	7	45		3 600	1 633	-	-
125	8.5	15	1	3 700	1 678	-	-
150	10.34			3 800	1724	-	-
175	12			3 600	1 633	-	-
200	14			3 500	1 588	-	-
35	2.5			1800	816	3 500	1 587
50	3.5			2 300	1 043	4 500	2 040
75	5			2 900	1 315	4 800	2 176
100	7	25	4.5	3 000	1 361	-	-
125	8.5	25	1.5	3 000	1 361	-	-
150	10.34			2 900	1 315	-	-
175	12			2 500	1 134	-	-
200	14			2 300	1 043	-	-
50	3.5			1400	635	3 500	1 587
75	5			2 000	907	4 400	1 995
100	7			2 400	1 089	-	-
125	8.5	40	2.75	2 500	1 134	-	-
150	10.34			2 500	1 134	-	-
175	12			1800	816	-	-
200	14			1700	771	-	-
75	5			1500	680	3 300	1496
100	7			1800	816	-	_
125	8.5			2 000	907	-	-
150	10.34	60	4	1700	771	-	_
175	12			1500	680	-	_
200	14			1400	635	_	_

NOTE: Published capacities are based on the use of external check valves supplied by Armstrong. Fill head measured from drain point to top of pump case.

Capacity Conversion Factor	Capacity Conversion Factors for Other Filling Heads											
Filling Head												
in	0	6	12	24	* 24 or greater							
mm	0	150	305	610	* 620 or greater							
Capacity Multiplier	and the second s											

NOTE: Fill head measured from drain to top of cap.





Pressure and Temperature Controls

Armstrond





Pressure Reducing Valves

Armstrong pressure reducing valves (PRVs) and temperature regulators help you manage steam, air and liquid systems safely and efficiently. And assure uninterrupted productivity—by maintaining constant pressure or temperature for process control. In short, Armstrong products make using resources safe and productive...as well as environmentally sound.

For decades, Armstrong has devoted itself to learning—and sharing—all it can about energy conservation as it relates to steam equipment. As part of our product/service network, PRVs and temperature regulators represent expanded options for a reliable Armstrong solution.

PRV Types

Steam, liquids and gases usually flow at high pressures to the points of final use. At these points, a pressure reducing valve lowers the pressure for safety and efficiency and to match the requirements of the application. There are three types of pressure reducing valves.

Direct Acting. The simplest of PRVs, the direct acting type operates with either a flat diaphragm or convoluted bellows. Since it is self-contained, it does not need an external sensing line downstream to operate. It is the smallest and most economical of the three types and designed for low to moderate flows. Accuracy of direct acting PRVs is typically +/-10% of the downstream set point.

Internally Piloted Piston-Operated. This type of PRV incorporates two valves—a pilot and main valve—in one unit. The pilot valve has a design similar to the direct acting valve. The discharge from the pilot valve acts on top of a piston, which opens the main valve. This design makes use of inlet pressure in opening a larger main valve than could otherwise be opened directly. As a result, there is a greater capacity per line size and greater accuracy (+/-5%) than with the direct acting valve. As with direct acting valves the pressure is sensed internally, eliminating the need for an external sensing line.

Externally Piloted. In this type, double diaphragms replace the piston operator of the internally piloted design. This increased diaphragm area can open a larger main valve, allowing a greater capacity per line size than the internally piloted valve. In addition, the diaphragms are more sensitive to pressure changes, and that means accuracy of +/-1%. This greater accuracy is due to the location, external of the valve, of the sensing line where there is less turbulence. This valve also offers the flexibility to use different types of pilot valves (i.e., pressure, temperature, air loaded, solenoid or combinations).



Selector Guide



Pressure Reduc	ing Valve S	election						
If Fluid Is	If Inlet Pr	essure Is	If Outlet F	Pressure Is	If Maximum Cap	acity Is Less Than	Look for Model	Find on Done
II Fluid IS	psig	barg	psig	barg	lb/hr	kg/hr	LOOK for Model	Find on Page
	15 to 150	1 to 10	3 to 60	.21 to 4	425	193	GD-6N	282
	5 to 15	.3 to 1	2 to 12	.14 to .8	5 643	2 565	GP-2000L	291
	15 to 250	1 to 17	7 to 200	.48 to 13.8	18 024	8 175	GP-1000	291
Charan	15 to 300	1 to 20	1.5 to 200	.10 to 14	134 534	61 024	GP-2000 Series	296
Steam	15 to 300	1 to 20	3 to 140	.21 to 9.6	1 038	471	GD-30S/GD-45	278/280
	15 to 250	1 to 17	3 to 140	.21 to 9.6	3 471	1 575	GD-30	278
	15 to 425	1 to 30	1.5 to 248	.10 to 17	25 706	11 660	GP-2000CS	296
	15 to 150	1 to 10	5 to 125	.34 to 8.6	4 505	2 048	GP-1000 SS/AS	291
If Fluid Is	If Inlet Pr	essure Is	If Outlet F	Pressure Is	If Maximum Cap	acity Is Less Than	Look for Model	Find on Page
II Fluid IS	psig	barg psig barg gpm		l/min	LOOK for Model	Find on Page		
	20 to 230	1.4 to 16	7 to 80	.48 to 5.5	141	534	GD-24	285
Water and Non-corrosive	15 to 150	1 to 10	3 to 60	.21 to 4.1	18	68	GD-6	282
Liquids	15 to 150	1 to 10	7 to 100	.48 to 6.9	1323	5 007	GD-200	286
·	15 to 300	1 to 20	7 to 130	.48 to 9.0	1323	5 007	GD-200H	286
If Fluid Is	If Inlet Pr	essure Is	If Outlet F	Pressure Is	If Maximum Cap	acity Is Less Than	Look for Model	Find on Page
II Fluid IS	psig	barg	psig	barg	scfm	m3/min	LOOK for Model	Find on Page
	15 to 150	1 to 10	5 to 125	.34 to 8.6	413	702	GD-10F	283
	15 to 300	1 to 20	5 to 125	.34 to 8.6	8 329	14 153	GD-10	283
	15 to 150	1 to 10	3 to 60	.21 to 4.1	153	260	GD-6	282
Air and Non- Corrosive	15 to 150	1 to 10	7 to 125	.48 to 8.6	6 488	11 024	GP-1000A	291
Gases	15 to 150	1 to 10	7 to 100	.48 to 6.9	20 614	35 028	GD-200	286
	15 to 300	1 to 20	7 to 130	.48 to 9.0	20 614	35 028	GD-200H	286
	15 to 300	1 to 20	3 to 140	.21 to 9.6	374	764	GD-45	274
	15 to 250	1 to 17	3 to 150	.21 to 9.6	1 249	2 122	GD-30	272

NOTE: GD models are direct acting; GP models are pilot controlled.

Pressure and Temperature Control ID Charts

Illustration	Туре	Fluid	Conn. Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size	Located on Page
	GD-30 Direct Acting Valves	Steam, Air,	NDT	250	410	Cast Bronze ASTM B584	GD-30	250	1/2", 3/4", 1", 1-1/2", 2"	270
	valves	Non-Corrosive Gases	NPT	300	430	Stainless Steel AISI 316	GD-30S	300	1/2", 3/4", 1"	278
	GD-45 Direct Acting Valves	Steam, Air, Non-Corrosive Gases	NPT	300	450	Ductile Iron ASTM A536	GD-45	300	1/2", 3/4", 1"	280
	GD-6 Direct Acting Valves	Steam	NPT	150	450	Cast Iron ASTM	GD-6N	150	3/8", 1/2", 3/4", 1"	282
	Valves	Liquid, Gas	INPI	150	175	A278	GD-6	150	3/8 , 1/2 , 3/4 , 1	202
	GD-10 Direct Acting	Air, Non-		300			GD-10	300	1/4", 3/8", 1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Valves	Corrosive Gases	NPT	250	175	Zinc and Aluminum	GD-10F	250	1/4", 3/8", 1/2", 3/4"	283
							AF-10		1/4", 3/8", 1/2", 3/4", 1"	



Armstrong Pressure and Temperature Control ID Charts

Illustration	Туре	Fluid	Conn. Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size	Located on Page
	GD-24 Direct Acting Valves	Water	NPT	230	175 210 (Viton)	Cast Bronze ASTM B584	GD-24	230	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	285
	GD-200 Direct Acting	Air, Water, Non-	Flanged ANSI 150#	150	175	Ductile Iron	GD-200	150		
	Valves	Corrosive and Non-Viscous Liquids	Flanged ANSI 300#	anged 210 ASTM A536		GD-200H	300	2", 2-1/2", 3", 4", 5", 6"	286	
	GD-20R Direct Acting Valves	Water, Non- Corrosive Gases	Flanged ANSI 150#	150	175	Ductile Iron ASTM A536	GD-20R	150	1/2", 3/4", 1", 1-1/4", 1-1/2", 2", 2-1/2", 3", 4", 5", 6"	288
Ā	GP-1000 Internal		NPT	250				250	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Pilot Piston Operated	Steam	Flanged ANSI 150#	150	450	Ductile Iron ASTM A536	GP-1000	150	2", 2-1/2", 3", 4"	291
	GP-1000 A Internal Pilot Piston	Air, Non- Corrosive	NPT	450	475	Ductile Iron	CD 4000A	150	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	204
	Operated	Gases	Flanged ANSI 150#	150	175	ASTM A536	GP-1000A	150	2", 2-1/2", 3", 4"	291
	GP-1000 SS Internal Pilot Piston Operated	Steam	NPT	150	450	Stainless Steel AISI 304	GP-1000SS	150	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	291
	GP-1000 AS Internal Pilot Piston Operated	Steam	NPT	150	450	Stainless Steel AISI 304	GP-1000AS	150	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	291
	GP-2000 External Pilot Diaphragm		NPT	300			GP-2000	300	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Operated	Steam	Flanged ANSI 150#	185	450	Ductile Iron ASTM A536	Integral or Remote	185		296
			Flanged ANSI 300#	300			Pilot	300	2", 2-1/2", 3", 4", 6"	
	GP-2000 L External Pilot		NPT						1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Diaphragm Operated (low pressure)	Steam	Flanged ANSI 150#	150	450	Ductile Iron ASTM A536	GP-2000 L	15	2", 2-1/2", 3", 4", 6"	297
	GP-2000CS External Pilot		NPT	450				450		
	Diaphragm Operated	Steam	Flanged ANSI 150#		600	Carbon Steel Grade WCB	GP-2000CS	140	1/2", 3/4", 1", 1-1/4", 1-1/2", 2" 2", 2-1/2", 3", 4"	298
			Flanged ANSI 300#	450				450		
	GP-2000K-1, GP-2000K-3,		NPT	300			GP-2000K-1	300	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	GP-2000K-6 External Pilot	Steam	Flanged ANSI 150#	185	450	Ductile Iron ASTM A536	GP- 2000K-3	185		299
	Diaphragm Operated		ANSI 150# NPT	300		ASIM ASS6	GP- 2000K-6	300	2", 2-1/2", 3", 4", 6"	



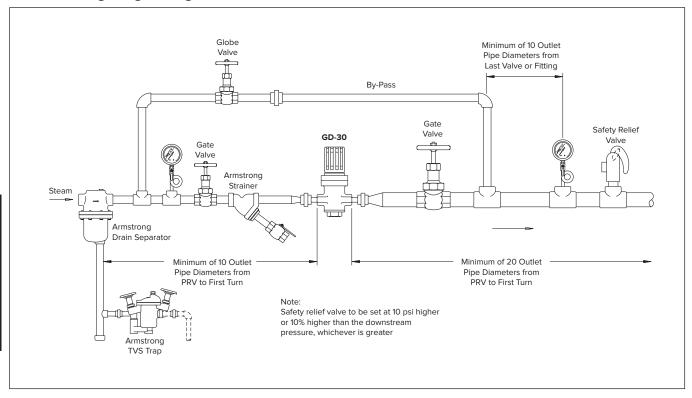
Pressure and Temperature Control ID Charts

Illustration	Туре	Fluid	Conn. Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size	Located on Page
	GD-2000K Direct Acting		NPT	300				300	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Diaphragm Operated	Steam	Flanged ANSI 150#	185	450	Ductile Iron ASTM A536	GD-2000K	185	2", 2-1/2", 3", 4"	300
			Flanged ANSI 300#	300				300	2,2-1/2,3,4	
	OBK-2000 Pneumatic Temperature Pilot	Air	NPT	250 (Process) 25 (Air)	400	Brass	OBK-2000	250 (Process) 25 (Air)	1/2" Process 1/8" Air	303
	GP-2000R External Pilot		NPT	200				200	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Diaphragm Operated	Steam	Flanged ANSI 150#	185	450	Ductile Iron ASTM A536	GP-2000R	185	21. 2.4/21. 21. 41. 61.	304
			Flanged ANSI 300#	200				200	2", 2-1/2", 3", 4", 6"	
	GP-2000 On/Off		NPT						1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	External Pilot Solenoid Operated Valve	Steam	Flanged ANSI 150# Flanged ANSI 300#	150	366	Ductile Iron ASTM A536	GP-2000	150	2", 2-1/2", 3", 4", 6"	307
	OB-30/31 Direct Acting	Water, Steam					OB-30 (Heating)	150		
	Temperature Regulators	and Non- Corrosive Liquids	NPT	250	366	Bronze ASTM B584	OB-31 (Cooling)	250	1/2", 3/4", 1"	310
	OB-2000 Piloted		NPT	300		Pilot		300	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Diaphragm Operated Temperature	Steam	Flanged ANSI 150#	185	450	Bronze ASTM B584	OB-2000	185		312
	Regulator		Flanged ANSI 300#	300		Valve Ductile Iron A536		300	2", 2-1/2", 3", 4", 6"	
	OB-2000 L Piloted		NPT			Pilot			1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Diaphragm Operated Temperature Regulator (low pressure)	Steam	Flanged ANSI 150#	150	450	Bronze ASTM B584 Valve Ductile Iron A536	OB-2000 L	15	2", 2-1/2", 3", 4"	314
i Ai	OB-2000PT Pressure/ Temperature		NPT	300		Temp. Pilot Bronze		300	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	
	Piloted Diaphragm Operated	Steam	Flanged ANSI 150#	185	450	ASTM B584 Valve and	OB-2000PT	185		316
	Temperature Regulator		Flanged ANSI 300#	300	Pressure Pilot Ductile Iron A536			300	2", 2-1/2", 3", 4", 6"	
•	Control Valve Pnuematic		NPT	300			CV1500 (1/2" - 4"	300		
	Actuated Control Valve	Steam, Liquid	Flanged ANSI 150#	185	450	Carbon Steel	Sizes)	185	1/2", 3/4", 1", 1-1/2",	320
		, , , ,	Flanged ANSI 300#	300		A216 Gr. WCB	CV1100 (6" & 8" Sizes)	300	2", 2-1/2", 3, 4, 6, 8	



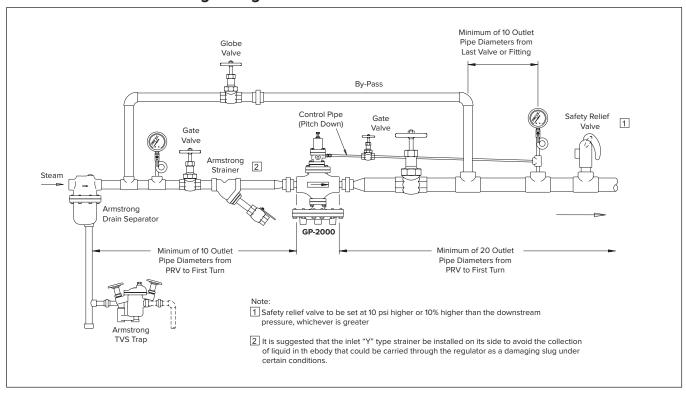
Application Data—Pressure Reducing Valves

Direct Acting Single Stage Reduction



Typical Direct Acting PRV Installation

External Pressure Pilot Single Stage Reduction



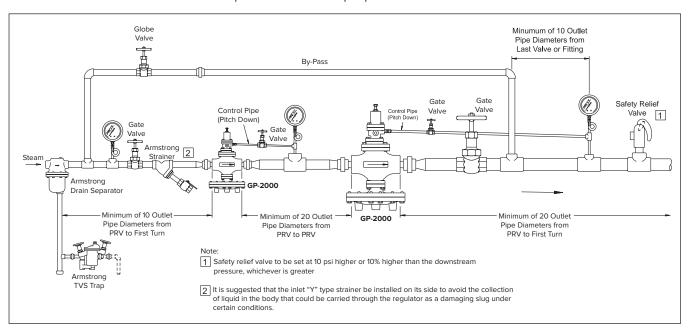
Typical External Pressure Pilot PRV Installation

Application Data—Pressure Reducing Valves



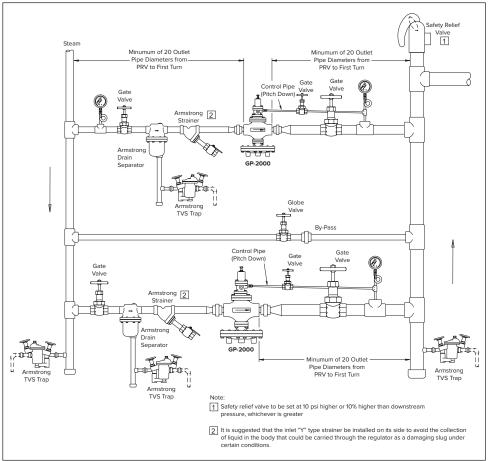
External Pressure Pilot Two Stage Reduction

This piping application is used when the pressure turndown ratio is greater than that of a single valve. Pressure reduction is accomplished by using two valves in series to reduce the pressure in stages. Depending on the volume of fluid required and pressure reduction, the second stage valve typically will be larger in size than the first stage valve. Unless a specific intermediate pressure of the fluid is required, this intermediate pressure is typically selected so as to keep the pressure turndown ratios of both valves as similar as possible. This will help equalize and maximize the service life of both valves.



External Pressure Pilot One-Third to Two-Thirds Reduction Station◆◆

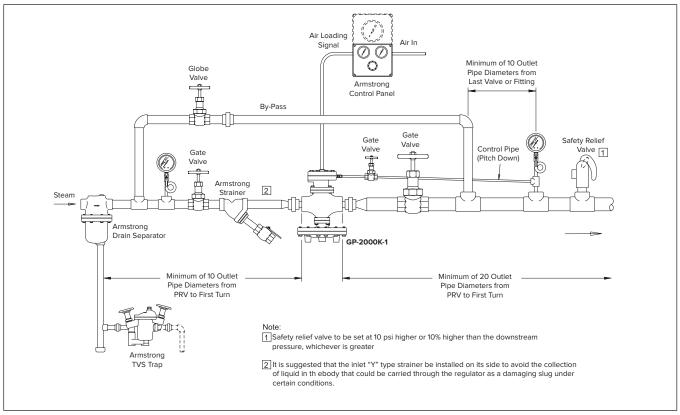
This piping application is used when the flow rangeability is greater than that of a single valve. Better control is achieved by piping two valves in parallel and sizing one to handle 1/3 the maximum load and the other 2/3 the maximum load. These two valves are staged by offsetting their pressure set points by 2-3 psig. The smaller valve is usually the lead valve and would have a pressure set point at the desired pressure. The larger valve is usually the lag valve and would have a pressure set point of 2-3 psig below the lead valve. This offset of set points will stage the valves so that the lag valve will remain closed until the lead valve can no longer pass the required flow and is wide open. This lack of flow will cause the set pressure to drop slightly until the lag valve opens and regulates at the higher demands of flow.





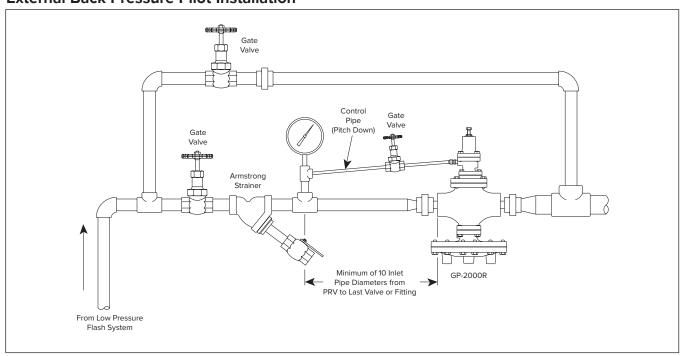
Application Data—Pressure Reducing Valves

Air Loaded External Pilot Single Stage Reduction



Typical Air Loaded External Pilot Reduction Station. Complete with remote located air loading control panel.

External Back Pressure Pilot Installation



Typical External Pilot Back Pressure Installation. Used to maintain a constant upstream pressure in the piping system.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Sizing Data



Selection Formulas

C_V Value and Calculations

1. For Steam:

When
$$P_2 > \frac{P_1}{2} C_v = \frac{W}{2.1\sqrt{\Delta P (P_1 + P_2)}}$$

*When
$$P_2 \le \frac{P_1}{2} C_v = \frac{W}{1.71 (P_1)}$$

2. For Gas:

When
$$P_2 > \frac{P_1}{2} C_v = \frac{Q \sqrt{G (T+460)}}{963 \sqrt{\Delta P (P_1 + P_2)}}$$

When
$$P_2 \le \frac{P_1}{2} C_v = \frac{Q}{36.39 (P_1)}$$

3. For Liquid:

$$C_v = \frac{(GPM)\sqrt{G}}{\sqrt{\Delta P}}$$

Formula Key

W = Maximum flow capacity of steam, lbs/hr

 P_1 = Inlet pressure, psia (psig + 14.7)

 P_2 = Outlet pressure, psia (psig + 14.7)

 ΔP = Pressure drop ($P_1 - P_2$) psig

Q = Maximum flow capacity of gas SCFH

G = Specific gravity

T = Fluid temperature °F

GPM = Maximum flow capacity of liquid GPM

 C_v = Valve flow coefficient

Ordering Information

C _v Values for Each Product																														
												Co	nnectio	n Size	•															
Model	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm				
		8	3/8	10	1/2	15	3/4	20	1	25	1-1/4	32	1-1/2	40	2	50	2-1/2	65	3	80	4	100	5	125	6	150				
GD-10	1.4 1.4		1	.4	2	.6	Ę	5.8	5.	8	5.	.8	43		-			_				_								
GD-10F	1	.4	1	.4	1	.4	2	.6	Ę	5.8	_	-	_				_			_				_		_				
GD-6/6N		_	.3	35		.5	1.	.0	1	1.5				_	_			_		_		T -		_						
GD-200/200H		_	-	_	-	_	-	_ _		_	_		_		16		28		36		36		68		75		108			
GD-20R		_	-		1	.5	2.7		4		8	1	1	1	1	14	2	3	3	32	48		8 75		108					
GD-24		_	-	_	1	.5	1.9		3		4		7		10						_			_						
GD-30/GD-45		_	-	_	1	.3	1.	.5	2	2.5	_	_		5.6*		3.5*		_		- -			_		_					
GP-2000 Series		_	-	_		5 7.		7.2		7.2		10.9		14.3		18.8		32	60		78		78		1.	20		_	2	250
GP-1000	-	_	-			1	2.3		4		6.	5	9		16		25		3	36		64				_				
OB-30/OB-31	-	_	-		3	3.7	4.6		5.8		_		_		_				-	_			-	_		_				
OB-2000/OB-2000PT	-	_	-	_		5	7	.2	10	0.9	14.	.3	18.8		32 60		7	78	120		T -			_						

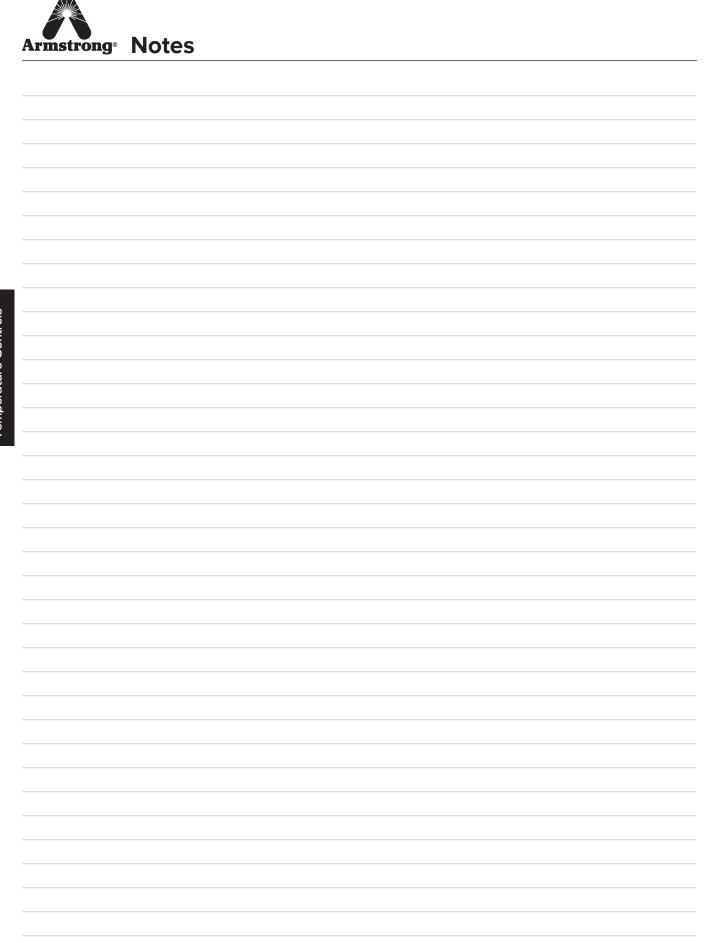
NOTE: 50% reduced ports are available for all 2000 Series valves. Capacities and Cv are reduced by 1/2. GD-6/6N and GD-30/45 capacities cannot be determined with a formula—consult capacity tables. Reference note under formula key above.

*GD-30 only.

When ordering please specify:

- 1. Model number
- 2. Connection size and type
- 3. Quantity
- 4. Service fluid
- 5. Specific gravity (if other than steam, air, water)
- 6. Fluid temperature
- 7. Maximum inlet pressure
- 8. Desired delivered pressure (reduced pressure)
- 9. Flow rate
- 10. Special conditions (if any)

^{*} Formula applies only to piloted valves. With direct acting valves, at critical flow or sonic flow, capacities diminish with greater differential pressure.



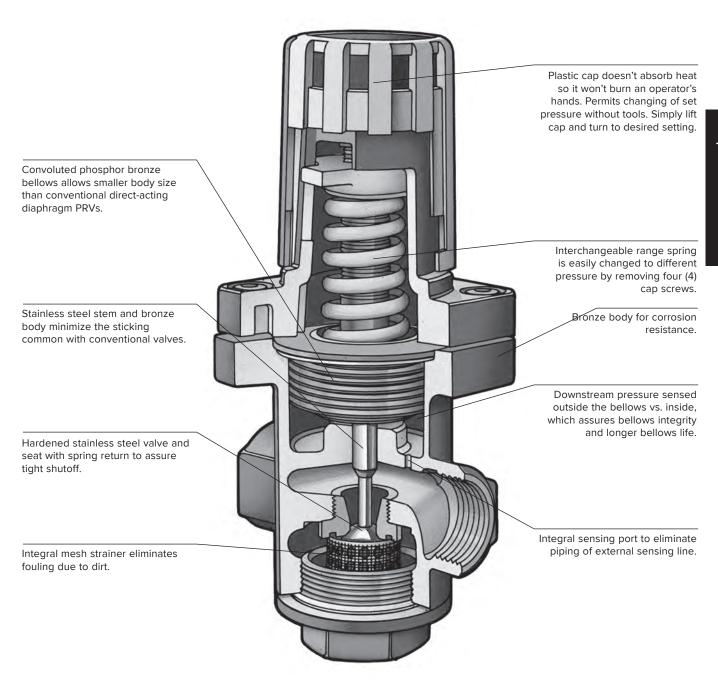
Direct Acting



For Steam, Air and Non-Corrosive Gas Service

The simplest of pressure reducing valves, the direct acting type operates with either a flat diaphragm or convoluted bellows. Since it is self-contained, it does not need an external sensing line downstream to operate. It is the

smallest and most economical of the three types and is designed for low to moderate flows. Accuracy of direct acting PRVs is typically +/-10%.





GD-30/30S

For Steam, Air and Non-Corrosive Gases

The GD-30 is a compact, high performance direct acting valve. Economical to buy and use, it's ideal for those low to moderate flow applications where accuracy of +/-10% is acceptable. The GD-30 is well suited for laundry and dry cleaning equipment, hospital equipment, tire molds, humidifiers, small heaters and applications in food processing. It provides tight shutoff for dead-end service on steam. Turndown ratio is 10:1 and ANSI Class IV Shutoff.

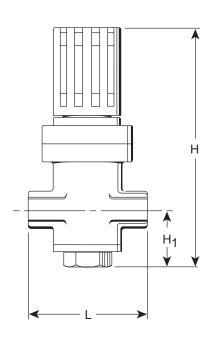
For a fully detailed certified drawing, refer to: GD-30 (bronze only) CDY #1038 GD-30S (stainless steel) CDY #1089

GD-30/3	GD-30/30S Specifications													
	Inlet			Minimum		Maximum		Materials						
Model Number	psig (barg)	psig psig (barg) Color psig (barg)		Differential psig (barg)	Application	Temp. °F (°C)	Body	Valve/Seat	Bellows					
GD-30	15 - 250 (1 - 17)	3 - 15 (.21 - 1.0)	Yellow		Steam, Air, Non- Corrosive Gases	410 (210)	Cast Bronze ASTM B584	Stainland Stanl	Phosphor Bronze ASTM B103*					
GD-30S	15 - 300 (1 - 20)	7 - 60 (0.5 - 4.0) 50 - 140 (3.4 - 9.6)	Blue Green	7 (.48)	Steam, Air, Non- Corrosive Gases	430 (220)	Stainless Steel AISI 316	Stainless Steel AISI 440/304	Stainless Steel AISI 316L					

^{*}Stainless steel optional

GD-30/30S Dime	nsions and V	Veights								
					Connect	ion Size				
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2	15	3/4	20	1	25	1-1/2*	40	2*	50
L	3-1/8	80	3-3/8	85	3-3/4	95	5-1/2	140	5-7/8	150
H ₁	2	47	2	47	2	47	3	77	3	77
Н	7-1/2	191	7-1/2	191	7-1/2	191	12-1/8	3071	2-1/8	307
Weight lb (kg)	4-1/4	(1.9)	4-1/4	l (1.9)	4-1/2	(2.0)	21-3/8	3 (9.7)	22 ((10)
C _v	1.	3	1.	.5	2	.5	5.	.6	8.	5

NOTE: GD-30 capacities cannot be determined with a formula—consult capacity tables. Reference note under formula key on page 275. *GD-30S available in 1/2", 3/4", and 1" only.





GD-30/30S



			lb/hr								kg/hr			ĺ
-1-4	Outlet		Col	nnection S	Size		lala					nnection	Size	
nlet	Outlet			in			Inle	Ou	ıtlet			mm		
ps	sig	1/2	3/4	1	1-1/2	2		barg		15	20	25	40	4
C _v F	actor	1.3	1.5	2.5	5.6	8.5	С	Facto	r	1.3	1.5	2.5	5.6	
15	7	49	56	92	198	297	1.0		.5	22	25	42	90	
20	13	53	61	105	216	331	1.4		.9	24	28	48	98	
20	7	42	55	63	180	264	1.4		.5	19	25	35	82	
	23	62	71	112	242	408		1	.6	28	32	51	110	
30	15	53	60	101	209	309	2.0	1	.0	24	27	46	95	
	3	33	40	60	139	216			.2	15	18	27	63	
	32	99	121	187	407	617		2	2.2	45	55	85	185	
40	20	79	97	159	330	517	2.8	1	.4	36	44	72	150	
	4	40	55	77	159	264			.3	18	25	35	72	
	40	130	143	242	539	837		2	2.8	59	65	110	245	
50	20	99	115	187	407	628	3.4		.4	45	52	85	185	
-	5	48	62	88	193	297			.3	22	28	40	88	
	48	137	154	265	584	899		_	3.3	62	70	120	265	+
	40	150	165	289	617	969			2.8	68	75	131	280	
60	18	90	104	170	374	584	4.0		.2	41	47	77	170	
	6	55	73	99	220	331		1	.4	25	33	45	100	
	64	176	205	342	738	1168		_	1.4	80	93	155	335	-
	54	187	205	353	782	1 201			3.7	85	102	160	355	
80	23	121	137	220	489	749	5.5		.6	55	62	100	222	
	8	60	77	108	231	363			.5	27	35	49	105	
	80	203	242	397	863	1355	-		5.5	92	110	180	392	-
	66	203	242 262	437	958	1 465			i.5	102	119	198	435	
00	40	198	262	375	837	1 278	6.9		2.8	90	105	170	380	
	10	68	79	132	297	473			.7	31	36	60	135	
	96		276		991				5.6					-
	70	231		452	l	1520				105	125	205 235	450	
20		276	311	518	1 168	1 818	8.3		1.8	125	141	1	530	
	45	240	267	450	980	1509			3.1	109	121	204	445	
	12	110	121	198	462	705		_	.8	50	55	90	210	_
	120	287	333	551	1 212	1862		- 1	3.3	130	151	250	550	
50	85	364	421	705	1 531	2 369	10.3		5.9	165	191	320	695	
	55	298	353	595	1278	2 005			8.8	135	160	270	580	
	15	132	165	254	562	848			.0	60	75	115	255	_
	140	408	485	794	1 719	2 677			9.7	185	220	360	780	
80	115	430	507	860	1829	2 832	12.4	.	3.0	195	230	390	830	
	70	386	430	739	1 619	2 501	12.	4	1.8	175	195	335	735	
	18	165	187	309	683	1 0 3 5			.2	75	85	140	310	_
	140	461	518	871	1 983	3 063		- 1	9.7	209	235	395	900	
00	115	474	540	904	2 005	3 085	13.8		3.0	215	245	410	910	
	80	430	496	827	1 818	2 810	.5.0	5	5.5	195	225	375	825	
	20	209	242	386	848	1300			.4	95	110	175	385	
	140	485	573	948	2 060	3 195		- 1	9.7	220	260	430	935	
25	115	496	584	961	2 071	3 207	15.5	. 1	3.0	225	265	436	940	
-25	85	463	540	904	1 983	3 063	13.5	5	5.9	210	245	410	900	
	23	254	298	496	1 079	1 675			.6	115	135	225	490	
	140	525	606	1 014	2 226	3 438			9.7	238	275	460	1 010	
50	120	551	584	1 038	2 248	3 471	170	8	3.3	250	265	471	1020	J
50	70	463	529	893	1 939	2 997	17.2	4	1.8	210	240	405	880	
	25	276	320	529	1 146	1796	L	- 1	.7	125	145	240	520	ا
	140	529	613	1 023	_	_		g	9.7	240	278	464	_	1
\ 7 E	120	529	613	1 023	_	_	40.0	8	3.3	240	278	464	_	
275	70	470	542	902	_	_	18.9		1.8	213	246	409	_	
	28	295	344	562	_	_		- 1	.9	134	156	255	_	
	140	529	613	1 023	_	_			9.7	240	278	464	_	1
	100	529	613	1 023	_	_		6	5.9	240	278	464	_	
00	70	478	551	926	_	_	20.0)	1.8	217	250	420	_	
	30	309	359	595	1		1	"		-17	200	1 720	1	- 1

NOTE: For air capacities scfm, multiply steam capacities (lb/hr) by 0.36. For air capacities m3/hr, multiply steam capacities (kg/hr) by 1.35. Maximum pressure reduction ratio 10:1.



For Steam, Air and Non-Corrosive Gas Service

The GD-45 is a compact, high-performance, direct-acting valve. Inexpensive to buy and use, it is ideal for those moderate flow applications that do not justify the higher cost of pilot-controlled valves.

The GD-45 is well-suited for laundry and dry-cleaning equipment, hospital equipment, tire molds, humidifiers, small heaters, and applications in food processing. It provides tight, quick, easy installation.

Quick, easy installation

- Lightweight and compact
- Piping supports the valve of ductile iron for greater durability and higher inlet pressure
- Screwed connections
- No external sensing lines or parts needed
- Maximum turndown ratio 10:1
- · ANSI Class IV shutoff

Simple selection

- •1/2", 3/4" and 1"
- Match pipe size normally
- Three pressure range springs (for best control when ranges overlap, use smaller range spring)

Long life/easy maintenance

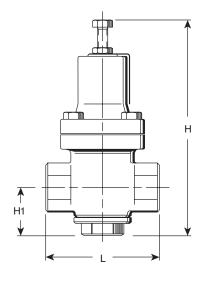
- Highly resilient phosphor-bronze bellows
- Hardened stainless-steel working parts
- Integral strainer (removable for cleaning) for protection from wear or dirt
- Teflon gaskets used at all joints for improved leakage prevention

For a fully detailed certified drawing, refer to CDY #1090.

	GD-45 Specifica	ations						
	Service	Inlet Pressure	Reduced Pressure psig	Minimum Differential	Maximum Temperature		Materials	
		psig (barg)	(barg)	psig (barg)	°F (°C)	Body	Valve/Seat	Bellows
ſ	Steam, Air		3 - 15 (.21 - 1.0) Yellow				Hardened	
	Non-Corrosive	15 - 300 (1 - 20)	7 - 60 (0.5 - 4.0) Blue	7 (.48)	450 (232)	ASTM A536 Ductile Iron	Stainless Steel	Phosphor Bronze ASTM B103
	Gases	(1 - 20)	50 - 140 (3.4 - 9.6) Green			Ductile Iron	AISI 420	ASTIVI DIUS

GD-45 Dimensions and W	/eights					
			Connect	ion Size		
Symbol	in	mm	in	mm	in	mm
	1/2	15	3/4	20	1	25
L	4-3/8	111	4-3/8	111	4-3/8	111
H ₁	1-7/8	47	1-7/8	47	1-7/8	47
Н	8-1/2	216	8-1/2	216	8-1/2	216
Wt, lb (kg)			7 (3	3.2)		
Cv	1	.3	1.	5	2	.5

NOTE: GD-45 capacities cannot be determined with a formula—consult capacity tables. Reference note under formula key on page 275.







	acities—Stean	lb/hr					kg/hr		
	T		onnection Si	70		I		Connection Size	70
Inlet	Outlet		in	26	Inlet	Outlet		mm	26
р	sig	1/2	3/4	1	bi	arg	15	20	25
	actor	1.3	1.5	2.5		actor	1.3	1.5	2.5
15	7	49	56	92	1.0	.5	22	25	42
	13	53	61	105		.9	24	28	48
20	7	42	55	63	1.4	.5	19	25	35
	23	62	71	112		1.6	28	32	51
30	15	53	60	101	2.0	1.0	24	27	46
	3	33	40	60		.2	15	18	27
	32	99	121	187		2.2	45	55	85
40	20	79	97	159	2.8	1.4	36	44	72
	4	40	55	77		.3	18	25	35
	40	130	143	242		2.8	59	65	110
50	20	99	115	187	3.4	1.4	45	52	85
	5	48	62	88		.3	22	28	40
	48 40	137 150	154 165	265 289		3.3 2.8	62 68	70 75	120
60	18	90	104	170	4.0	1.2	41	47	77
	6	55	73	99		.4	25	33	45
	64	176	205	342		4.4	80	93	155
	54	187	225	353		3.7	85	102	160
80	23	121	137	220	5.5	1.6	55	62	100
	8	60	77	108		.5	27	35	49
	80	203	242	397		5.5	92	110	180
100	66	225	262	437	6.9	4.5	102	119	198
100	40	198	231	375	6.9	2.8	90	105	170
	10	68	79	132		.7	31	36	60
	96	231	276	452		6.6	105	125	205
120	70	276	311	518	8.3	4.8	125	141	235
	45	240	267	450		3.1	109	121	204
	12	110	121	198		.8	50	55	90
	120	287	333	551		8.3	130	151	250
150	85	364	421	705	10.3	5.9	165	191	320
	55 15	298 132	353 165	595 254		3.8 1.0	135 60	160 75	270 115
	140	408	485	794		9.7	185	220	360
	115	430	507	860		8.0	195	230	390
180	70	386	430	739	12.4	4.8	175	195	335
	18	165	187	309		1.2	75	85	140
	140	461	518	871		9.7	209	235	395
200	115	474	540	904	12.0	8.0	215	245	410
200	80	430	496	827	13.8	5.5	195	225	375
	20	209	242	386		1.4	95	110	175
	140	485	573	948		9.7	220	260	430
225	115	496	584	961	15.5	8.0	225	265	436
	85	463	540	904		5.9	210	245	410
	23	254	298	496		1.6	115	135	225
	140	525	606	1 014		9.7	238	275	460
250	120	551	584	1038	17.2	8.3	250	265	471
	70	463	529	893		4.8	210	240	405
	25 140	276	320	529		1.7 9.7	125	145	240
	120	528 551	616 627	1 023 1 038		8.3	240 250	280 285	465
300	70	484	550	913	20	4.8	220	250	415
	30	319	352	583		2.0	145	160	265

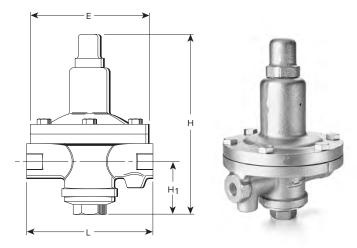
NOTE: For air capacities scfm, multiply steam capacities (lb/hr) by 0.36. For air capacities m3/hr, multiply steam capacities (kg/hr) by 1.35. Maximum pressure reduction ratio 10:1.



GD-6N (Steam), GD-6 (Liquid, Gas)

For Steam, Air and Water

The GD-6N and GD-6 are compact, direct acting diaphragm valves ideal for low-flow applications, including laundry/dry cleaning equipment, hospital equipment, tire/plastic molds and food processing. Lightweight and compact, the valves require no external sensing lines or additional parts. External adjusting screw with locking nut and cover make for quick, easy setting and adjustment. Tight shutoff for dead-end service. Removable stainless steel diaphragm, hardened stainless steel working parts (6N), integral removable strainer (6N) and in-line renewable valve and seat. Available in 3/8", 1/2", 3/4" and 1" sizes with a choice of two set pressure spring ranges.



For a fully detailed certified drawing, refer to CDY #1040.

GD-6N/	GD-6 Specific	ations											
		Inlet	Reduced	Spring	Minimum Maximum			Materials					
Model			Pressure psig (barg) Color		Differential psig (barg)	Temperature °F (°C)	Body	Main Valve	Valve Seat	Diaphragm			
GD-6N	Steam	15 - 150 (1	3 - 15 (.21 - 1.0)	Yellow Stripe		450 (232)	Cast Iron	Stainless Steel AISI 304	Stainless Steel AISI 420	Stainless Steel			
GD-6	Liquid Gas	- 10)	and 15 - 60 (1 - 4)	Yellow/Blue Stripe	7 (.48)	175 (79)	ASTM A278	Brass (w/Disc) ASTM B16	Bronze ASTM B584	AISI 304			

GD-6	6N Capa	acitie	s—S	team							
		lb/ł	ır					kg.	/hr		
Inlak	Outlet	Со	nnec	tion S	Size	Inlat	Outlet	C	onne	tion S	ize
Inlet	Outlet		i	in		iniet	Outlet		n	nm	
p	sig	3/8	1/2	3/4	1	b	arg	10	15	20	25
15	3 - 8	18	25	51	76	1.0	.26	8.2	11.3	23.1	34.5
20	13	12	17	34	51	1.4	.9	5.4	7.7	15.4	23.1
20	3 - 10	21	30	59	89	1.4	.27	9.5	13.6	26.8	40.4
	18	14	20	41	61		1.2	6.4	9.1	18.6	27.7
25	15	19	28	55	83	1.7	1.0	8.6	12.7	24.9	37.6
	3 - 12	24	34	68	102		.28	10.9	15.4	30.8	46.3
	23	16	23	47	71		1.6	7.3	10.4	21.3	32.2
30	20	21	30	59	89	2.1	1.4	9.5	13.6	26.8	40.4
	3 - 15	27	38	76	115		.2 - 1	12.2	17.2	34.5	52.2
	32	21	30	60	90		2.2	9.5	13.6	27.2	40.8
40	25	28	40	79	119	2.8	1.7	12.7	18.1	35.8	54.0
	4 - 20	33	47	94	140		.3 - 1.4	15.0	21.3	42.6	63.5
	40	25	36	73	109		2.8	11.3	16.3	33.1	49.4
50	32	33	47	94	141	3.4	2.2	15.0	21.3	42.6	64.0
	5 - 25	39	55	111	166		.3 - 1.7	17.7	24.9	50.3	75.3
	48	30	43	55	128		3.3	13.6	19.5	24.9	58.1
60	40	37	53	107	160	4.1	2.8	16.8	24.0	48.5	72.6
	6 - 30	45	64	128	192		.4 - 2.1	20.4	29.0	58.1	87.1
	60	37	52	104	156		4.1	16.8	23.6	47.2	70.8
75	48	47	67	135	202	5.2	3.3	21.3	30.4	61.2	91.6
	7 - 37	54	77	153	230		.5 - 2.6	24.5	34.9	69.4	104.3
100	65	61	87	173	260	6.9	4.5	27.7	39.5	78.5	117.9
100	10 - 50	69	98	196	294	0.9	.7 - 3.4	31.3	44.5	88.9	133.4
125	13 - 60	84	119	239	358	8.6	.9 - 4.1	38.1	54.0	108.4	162.4
150	15 - 60	99	142	283	425	10.3	1 - 4.1	44.9	64.4	128.4	192.8

GD-6N/GD-6 Dimensions and Weights															
				onne	ction Size	е									
Symbol	in	mm	in	mm	in	mm	in	mm							
	3/8														
L	6-1/2	6-1/2 165 6-1/2 165 7-1/4 185 7-1/4 185													
Н	9-1/2	9-1/2 237 9-1/2 237 10-1/4 261 10-1/4 26 ²													
H ₁	2-1/4	57	2-1/4	57	3	76	3	76							
E	6-1/8	155	6-1/8	155	7	175	7	175							
Wt Ib (kg)	12 (5	5.5)	12 (5	.5)	18 (8.	2)	18 (8.	2)							
C _v	.3!	.35 .5 1.0 1.5													

GD-6 C	apaciti	es—W	/ater							
		gpm						l/min		
ΛP	Co	nnec	tion Si	ze		ΔΡ	С	onnect	tion Siz	:e
		i	n			ΔΡ		m	m	
psig	3/8	1/2	3/4	1		barg	10	15	20	25
5	.8	1.1	2.2	3.4		.35	3.0	4.2	8.3	12.9
10	1.1	1.6	3.2	4.7		.7	4.2	6.0	12.1	17.8
15	1.4	1.9	3.9	5.8		1.0	5.3	7.2	14.8	22.0
25	1.8	2.5	5.0	7.5		1.7	6.8	9.5	18.9	28.4
50	2.5	3.5	7.1	10.6		3.5	9.5	13.2	26.9	40.1
75	3.0	4.3	8.7	13.0		5.2	11.4	16.3	32.9	49.2
100	100 3.5 5.0 10.0 15.0					6.9	13.2	18.9	37.9	56.8
125	3.9	5.6	11.2	16.8		8.6	14.8	21.2	42.4	63.6
147	4.2	6.1	12.1	18.2		10.0	15.9	23.1	45.8	68.9

NOTE: For air capacities scfm, multiply steam capacities (lb/hr) by 0.36. For air capacities m3/hr, multiply steam capacities (kg/hr) by 1.35.

Maximum pressure reduction ratio 10:1.

ANSI Class IV Shutoff.

GD-10, GD-10F, AF-10



For Air and Non-Corrosive Gases

The GD-10/10F is a lightweight direct acting diaphragm valve used primarily for pneumatic tool air supply and non-hazardous gas regulation. Screwed connections make it easy to support in position without external sensing lines or other parts. Zinc or aluminum bodies eliminate rust and scale. Plug, seat and diaphragm are renewable in-line, and you can make quick adjustments externally with locking handle. Quarter-inch pressure gauge connection is standard, and all units are capable of tight shutoff for dead-end service.

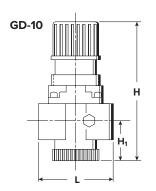
GD-10 available in sizes 1/4" - 2." Highly efficient Model AF-10 air filters with zinc or aluminum bodies are used to remove liquids and solid particles from compressed air. The AF-10 is available in sizes 1/4" - 1."

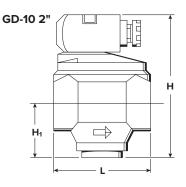
For a fully detailed certified drawing, refer to list below.

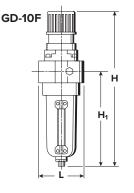
GD-10 CDY #1003 GD-10F CDY #1002 AF-10 CDY #1004

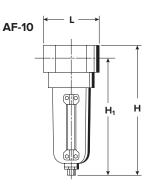
	GD-10F/AF-10	Inlet Pres.	Reduced Pressure	Min. Differ.	Max.		Materials							
Model	Application	psig (barg)	psig (barg)	psig (barg)	Temp. °F (°C)	Body in (mm)	Bowl	Main Valve in (mm)	Valve Plug in (mm)	Diaphragm				
GD-10	Air and	15 - 300 (1 - 20)	5 - 125 (.34 - 8.6)	7 (.48)		Zinc 1/4, 3/8, 1/2, 3/4 (6, 9, 15, 20) Aluminum 1 - 2 (25 - 50)	_	Zinc 1/4, 3/8, 1/2, 3/4 (6, 9, 15, 20) Aluminum 1 - 2 (25 - 50)	Brass 1/4, 3/8, 1/2, 3/4 (6, 9, 15, 20) Nylon 1 - 2 (25 - 50)	Nitrile				
GD-10F	Other Non- Corrosive	15 - 250 (1 - 17)	5 - 125 (.34 - 8.6)	7 (.48)	175 (79)		Zinc		Brass	Nitrile				
AF-10	Gases	0 - 250 (0 - 17)	_	_		Zinc 1/4, 3/8, 1/2, 3/- (6, 9, 15, 20) Aluminum 1 (25)	4	_	_	_				

GD-10 Dimens	-10 Dimensions and Weights															
		Connection Size														
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm				
	1/4	8	3/8	10	1/2	15	3/4	20	1, 1-1/4, 1-1/2	25, 32, 40	2	50				
L	2-5/8	67	2-5/8	67	2-5/8	67	3-1/2	98	4-1/4	108	6	152				
Н	5-3/8	136	5-3/8	136	5-3/8	136	5-7/8	149	7-1/8	181	9-3/4	248				
H ₁	1-1/2	38	1-1/2	38	1-1/2	38	1-1/2	38	2-3/8	60	3-9/16	90				
Wt, Ib (kg)	1-1/2	(.7)	1-1/2	(.7)	1-1/2	(.7)	2 (.9))	3 (1.4	!)	10 ((4.5)				
C _v	·		1.4	·			2.6		5.8		4	13				











Armstrong[®] GD-10, GD-10F, AF-10

GD-10/GI	D-10F Capa	cities—Air										
		sc	fm						m ³	³ /hr		
			Conne	ection Size						Connec	tion Size	
Inlet	Outlet			in			Inlet	Outlet		n	ım	
р	sig	1/4, 3/8, 1/2	3/4	1*, 1-1/4, 1-1/2	2**		ba	arg	8, 10, 15	20	25*, 32, 40	50**
15	8	19	35	78	580]	1.0	0.6	32	60	133	985
	23	24	44	98	727			1.6	40	75	167	1 235
30	15	33	61	136	1 011		2.0	1.0	56	104	232	1 718
	5 - 7	38	70	157	1 166			.34 - 48	64	120	267	1 981
	33	26	49	109	810			2.3	45	83	186	1 377
40	20	42	77	173	1280		2.8	1.4	71	131	293	2 174
	5 - 12	46	86	192	1 427			.3483	79	147	327	2 424
	40	34	63	141	1 046			2.8	58	107	240	1 777
50	30	46	86	191	1 416		3.4	2.1	78	145	324	2 405
	5 - 17	55	102	228	1 687	-		.34 - 1.17	93	173	387	2 867
	60	49	91	203	1503			4.1	83	154	344	2 553
75	45	66	123	273	2 026		5.2	3.1	112	208	464	3 442
	7 - 30	76	141	316	2 339			.48 - 2.1	129	240	536	3 975
	80	64	118	264	1 958			5.5	108	201	449	3 327
100	60	86	159	355	2 634		6.9	4.1	146	271	604	4 475
	10 - 42	97	181	403	2 991]		.69 - 2.9	165	307	686	5 082
	100	79	146	326	2 413			6.9	134	248	553	4 101
125	75	106	196	437	3 241		8.6	5.2	179	333	743	5 507
	13 - 55	119	220	491	3 643]		.89 - 3.8	202	374	835	6 190
	120	93	173	387	2 868			8.3	159	295	657	4 873
150	85	129	240	535	3 967		10.3	5.9	219	408	909	6 741
	15 - 67	140	260	579	4 295]		1.03 - 4.6	238	441	984	7 298
	125	126	235	524	3 884			8.6	215	399	890	6 599
175	100	149	276	617	4 573		12.1	6.9	253	470	1 048	7 769
	18 - 80	161	299	667	4 947			1.24 - 5.5	274	508	1134	8 405
200	125	161	298	666	4 934		13.8	8.6	273	507	1 131	8 383
200	20 - 92	182	339	755	5 599		13.0	1.38 - 6.3	310	575	1283	9 513
250†	25 - 125	225	417	931	6 903		17.2 ⁺	1.7 - 8.6	382	709	1582	11 729
300	30 - 125	267	496	1 107	8 207		20.0	2.1 - 8.6	454	843	1 881	13 944
350**	35 - 125	_	_	_	9 511		24.1**	2.4 - 8.6	_	_	_	16 159
425**	43 - 125	_	_	_	11 467		29.3**	3.0 - 8.6	_	_	_	19 482

^{*} GD-10F not available above 3/4" (20 mm).

[†] GD-10F has a maximum inlet pressure of 250 psig (17 barg).

GD-10F Dimer	sions an	d Weig	hts					
			(Conne	ction Si	ze		
Symbol	in	mm	in	mm	in	mm	in	mm
	1/4	8	3/8	10	1/2	15	3/4	20
L	2-3/4	70	2-3/4	70	2-3/4	70	3-7/8	98
Н	9-3/8	238	9-3/8	238	9-3/8	238	10-7/8	276
H ₁	5-3/4	146	5-3/4	146	5-3/4	146	6-3/8	162
Wt, lb (kg)	2-1/2	(1.2)	2-1/2	(1.2)	4-1/2	(2.0)	4-1/2	(2.0)
C _v			1.4				2.	6

AF-10 Dime	nsions	and V	Veights	5										
				C	onnect	ion S	ze							
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm				
	1/4	8	3/8	10	1/2	15	3/4	20	1	25				
L	2-3/4	70	2-3/4	70	2-3/4	70	3-7/8	98	4-3/4	121				
Н	6-3/8	162	6-3/8	162	6-3/8	162	7	178	11-3/8	289				
H ₁	5-3/4													
Wt, lb (kg)				2 (.	.9)				3 (1.	4)				



^{** 2&}quot; (50 mm) GD-10 valve maximum inlet pressure is 425 psig (30 barg).

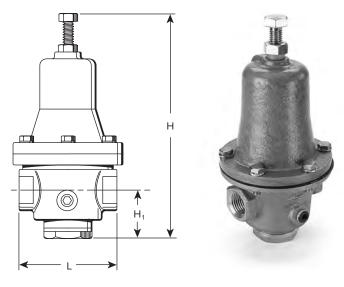


For Non-Potable Water Service Only

An industrial-grade valve for non-potable water systems, the GD-24 is lightweight, compact and economical. Comes with screwed connections and will mount in any position. Requires no external sensing lines. Bronze body and high temperature diaphragm suitable for hot or cold process water service. Valve, seat and diaphragm are renewable in line. External adjusting screw with lock. Six sizes, 1/2" through 2". ANSI Class IV shutoff.

Illegal for potable water service per SDWA section 1417 (As Amended).

For a fully detailed certified drawing, refer to CDY #1023.



GD-24 Speci	ifications							
Application	Maximum Pressure	Reduced Pressure Range	Minimum Differential	Maximum Temperature			Materials	
Application	psig (barg)		psig (barg)	°F (°C)	Body	Main Valve	Valve Seat	Diaphragm
Hot or Cold Water	20 - 230 (1.3 - 16)	7 - 80 (.48 - 5.5)	7 (.48)	175* (79)	Cast Bronz	ze ASTM 584	Stainless Steel AISI 304	NBR**

^{*}With Viton® diaphragm maximum temperature is 210°F (99°C).

^{**}Viton optional.

GD-24 Cap	acities—\	Water											
			gpm							l/min			
$\Delta \mathbf{P}$			Connect	tion Size			ΔΡ			Connec	tion Size		
ΔΡ			i	n			ΔΓ			m	ım		
DP (psig)	1/2	3/4	1	1-1/4	1-1/2	2	DP (barg)	15	20	25	32	40	50
7	4	5	8	11	19	26	0.5	15	20	30	40	70	100
10	5	6	9	13	22	32	0.7	18	24	36	48	84	120
15	6	8	12	15	27	39	1.0	22	29	44	59	103	147
25	8*	10	15	20	35	50	1.7	30*	38	57	76	132	189
50	11	14*	21	28	49	71	3.4	40	53*	80	107	187	268
75	13	17	26*	35	61*	87	5.2	49	66	98*	131	231*	328
100	15	20	30	40*	70	100*	6.9	57	76	114	151*	265	378*
125	17	22	34	45	78	112	8.6	63	85	127	169	296	423
150	18	24	37	49	86	122	10.3	70	93	139	185	325	464
175	20	26	40	53	93	132	12.0	75	100	150	200	351	501
200	21	28	42	57	99	141	13.8	80	107	161	214	375	535

*At flows greater than this, velocities will exceed 10 ft/sec and pipe erosion could occur. NOTE: Maximum pressure reduction ratio 10:1.

						Connec	tion Size					
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2	15	3/4	20	1	25	1-1/4	32	1-1/2	40	2	50
L	3-1/4	83	3-1/2	89	4	102	4-3/4	121	6	152	7-1/4	184
H ₁	1-3/4	45	2	51	2-1/2	64	3-1/4	83	3-1/2	89	4-1/2	115
Н	7-3/4	197	8-1/2	216	9-5/8	245	11-1/4	286	13-1/2	343	16	407
Wt, lb (kg)	4	(1.8)	5-1/4	(2.4)	7-1/4	(3.3)	10-3/8	(4.7)	18	(8.2)	31-1/2	(14.3)
C _v	1.	5	- :	2		3	4	1	-	7	1	0



GD-200/200H

For Air, Water, Non-Corrosive and Non-Viscous Liquids

The GD-200/200H offers high capacity and highly accurate control with a large, cupped diaphragm for a long stroke. Compact and rugged, the GD-200's composition valve and stainless steel seat mean high performance over a long service life. Well suited to non-viscous liquid pressure reduction, the valve is widely applied in domestic water

applications, construction equipment, irrigation, tank car loading and industrial or commercial air conditioning. Upstream variations do not affect balanced pressure valve, and composition disc assures tight shutoff. Turndown ratio is 10:1, and sizes range from 2" through 6". ANSI Class IV Shutoff

GD-200/	200H Sp	ecifications										
		Pressure					Min.			Mate	erials	
Model	Inlet	Reduced p	osig (barg)	Spring	Application	Max. Temp.	Diff.					
Number	psig	2" - 3"	4" - 6"	Color	Application	°F (°C)	psig	Body	Main Valve	Valve Seat	Diaphragm	Connection
	(barg)	(50 - 80 mm)	(100 - 150 mm)			, -,	(barg)		vaive	Jear		
GD-200	150 (10)	7 - 36 (.48 - 2.5)	7 - 36 (.48 - 2.5)	Yellow	Liquid	475 (70)**	7 (40)	Ductile Iron	NIDD	Stainless	NDD***	ANSI 150 lb. Flg.
GD-200H	300 (20)	37 - 100 (2.5 - 6.9) *72 - 130 (4.9 - 8.8)	37 - 72 (2.5 - 5.0) *72 - 108 (4.9 - 7.3)	Black	Gas	175 (79)**	7 (.48)	ASTM A536	NBR	Steel AISI 304	NBR***	ANSI 300 lb. Flg.

^{*}This spring range for GD-200H only.

^{***}Viton optional.

GD-200	/200H Ca	pacities-	-Air												
			sc	fm							m3.	/hr			
Inlet	Outlet			Connect	ion Size			Inlet	Outlet			Connect	tion Size		
met	Outlet			i	n			met	Outlet			m	m		
ps	sig	2	2-1/2	3	4	5	6	k	parg	50	65	80	100	125	150
15	8	216	377	485	917	1 011	1 456	1.03	0.55	366	641	824	1 5 5 7	1 718	2 473
20	13	235	412	530	1 000	1 103	1589	1.38	0.90	400	700	900	1699	1874	2 699
20	7	305	534	686	1 296	1429	2 058	1.30	0.48	518	907	1 166	2 202	2 428	3 497
25	18	254	444	570	1 077	1 188	1 711	1.72	1.24	431	754	969	1 831	2 019	2 907
	7	374	655	842	1 591	1755	2 527	1.72	0.48	636	1 113	1 431	2 703	2 981	4 293
30	23	270	473	609	1 149	1 268	1826	2.07	1.59	459	804	1 034	1953	2 154	3 102
	7	440	770	990	1870	2 063	2 970	2.07	0.48	748	1308	1682	3 178	3 505	5 047
	32	321	561	722	1363	1503	2 165		2.21	545	954	1226	2 316	2 554	3 678
40	20	476	833	1 071	2 024	2 232	3 214	2.76	1.38	459	804	1 034	1953	2 154	3 102
	7 - 12	531	929	1 194	2 256	2 488	3 583		.4883	902	1 578	2 029	3 833	4 227	6 087
	40	389	681	875	1654	1824	2 626		2.76	661	1 157	1 487	2 810	3 099	4 462
50	30	527	922	1 185	2 239	2 469	3 555	3.45	2.07	809	1 416	1820	3 438	3 792	5 461
	7 - 17	628	1 099	1 413	2 668	2 943	4 238		.48 - 1.17	1 0 6 7	1867	2 400	4 534	5 000	7 200
	48	457	800	1029	1943	2 143	3 086		3.31	777	1360	1748	3 302	3 642	5 244
60	35	628	1 099	1 413	2 669	2 944	4 239	4.14	2.41	895	1 566	2 014	3 803	4 195	6 041
	7 - 22	725	1269	1 631	3 081	3 398	4 893		.48 - 1.5	1232	2 155	2 771	5 234	5 773	8 313
	60	559	979	1258	2 377	2 621	3 775		4.14	950	1 663	2 138	4 038	4 453	6 413
75	45	754	1 319	1 696	3 204	3 534	5 089	5.17	3.10	1 067	1867	2 401	4 535	5 001	7 202
	7 - 30	870	1523	1959	3 699	4 080	5 876		.48 - 2.1	1 4 7 9	2 588	3 328	6 285	6 932	9 983
	80	729	1 275	1640	_	_	_		5.52	1 238	2 167	2 786	-	_	_
100	60	980	1 715	2 205	4 166	4 594	6 616	6.89	4.14	1 281	2 241	2 882	5 444	6 004	8 646
	10 - 42	1 113	1948	2 504	4 730	5 217	7 513		.69 - 2.9	1 891	3 309	4 255	8 037	8 864	12 765
	100	898	1 572	2 021	_	_	_		6.89	1526	2 670	3 433	-	_	_
125	70	1206	2 111	2 714	5 317	5 864	8 444	8.62	5.17	1665	2 914	3 747	7 077	7 806	11 241
	13 - 55	1356	2 372	3 050	5 762	6 355	9 151		.89 - 3.8	2 303	4 031	5 182	9 789	10 796	15 547
	100	1 331	2 329	2 995	_	_	-		6.89	2 261	3 957	5 088	_	-	_
150	80	1 517	2 655	3 414	_	_	-	10.34	5.52	2 049	3 586	4 610	_	-	_
	15 - 67	1598	2 797	3 596	6 793	7 492	10 788		1.03 - 4.6	2 715	4 752	6 110	11 541	12 729	18 329
l	100	1772	3 100	3 986	_	_	_		6.89	3 010	5 268	6 773	_	_	_
180	90	1848	3 235	4 159	_	_	_	12.41	6.21	2 578	4 512	5 801	_	_	_
	18 - 80	1889	3 306	4 251	8 030	8 856	12 753		1.24 - 5.5	3 210	5 618	7 223	13 643	15 047	21 668
200	100	2 044	3 577	4 598	_	_	_	13.79	6.89	3 472	6 077	7 813	_	_	_
	20 - 92	2 083	3 646	4 688	8 855	9 766	14 063	15.75	1.38 - 6.3	3 540	6 195	7 965	15 044	16 593	23 894
250	25 - 100	2 569	4 495	5 779	10 917	12 041	17 338	17.24	1.72 - 6.9	4 364	7 637	9 819	18 548	20 457	29 458
300	25 - 100	3 054	5 344	6 871	12 979	14 315	20 613	20.00	1.72 - 6.9	5 188	9 080	11 674	22 051	24 321	35 022

NOTE: Maximum pressure reduction ratio 10:1.

NOTES: Available in sizes below 2" upon request. Differential valve (GD-21) available upon request

^{**}With Viton® diaphragm maximum temperature is 210°F (99°C).

GD-200/200H



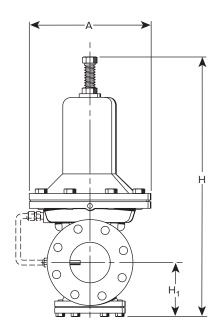
GD-200/2	200H Ca	pacities	Water										
			gpm							l/min			
4.5			Conne	ection Size			4.5			Conne	ction Size		
ΔР				in			ΔР				mm		
DP (psig)	2	2-1/2	3	4	5	6	DP (barg)	50	65	80	100	125	150
7	42	74	95	180	198	286	0.5	160	280	361	681	751	1082
10	51	89	114	215	237	342	0.7	192	335	431	814	898	1293
15	62	108	139	263	290	418	1.0	235	411	528	997	1 100	1583
20	72	125	161	304	335	483	1.4	271	474	609	1 151	1 270	1828
25	80	140*	180	340	375	540	1.7	303	530*	681	1 287	1 420	2 044
35	95*	166	213*	402*	444	639	2.4	360*	627	806*	1520*	1680	2 419
50	113	198	255	481	530*	764	3.4	428	749	964	1820	2 006*	2 891
75	139	242	312	589	650	900*	5.2	525	918	1 180	2 229	2 459	3 407*
100	160	280	360	680	750	1 080	6.9	606	1060	1363	2 574	2 839	4 088
125	179	313	402	760	839	1207	8.6	677	1 185	1524	2 878	3 174	4 571
150	196	343	441	833	919	1323	10.0	742	1298	1 669	3 153	3 477	5 007

*At flows greater than this, velocities will exceed 10 ft/sec and pipe erosion could occur. NOTE: Minimum flow is 1.3 gpm (4.9 l/min).

GD-20	00/2001	H Dimensi	ions and V	Weights										
Si	ze	GD- Face-t		GD-2 Face-t	200H o-Face	,	A	F	4	F	I ₁	c _v	We	ight
in	mm	in	mm	in	mm	in mm 6 152		in	mm	in	mm		lb	kg
2	50	7-5/8	195	7-7/8	200	6	152	16-1/4	415	3-1/8	81	16	43	19.2
2-1/2	65	10-5/8	270	10-7/8	277	7	178	21-1/2	550	4-1/16	105	28	88	40.0
3	80	10-5/8	270	11-1/8	283	7-1/2	191	22-9/16	577	4-9/16	120	36	97	43.7
4	100	12-1/8	308	12-3/4	342	9	229	25-1/6	637	5-1/4	135	68	154	70.0
5	125	15	380	15-7/8	403	10	254	33	839	6-1/2	169	75	317	144.0
6	150	15-3/4	400	16-5/8	422	11	280	35-9/16	908	7-1/2	194	108	381	173.0

For a fully detailed certified drawing, refer to:

GD-200 CD #2106 GD-200H CD #2107



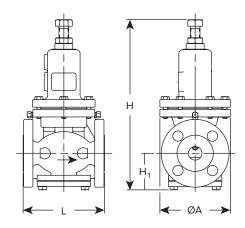




For Water, Non-Corrosive and Non-Viscous Liquids

The GD-20R offers high capacity and highly accurate control with a large, cupped diaphragm for a long stroke. Compact and rugged, the GD-20R's composition valve and stainless steel seat mean high performance over a long service life. It is mainly used in heating and cooling equipment, and automatically regulates the pressure according to load fluctuations. It can be used in by-pass systems to prevent pump shutoff and to maintain a constant fluid pressure in the line. Turndown ratio is 10:1, and sizes range from 1/2" through 6"



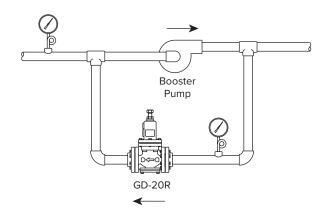


GD-20R	Capad	cities-	-Wateı	r																
				gp	m										l/m	iin				
ΔР				Co	nnectio	n Size					ΔΡ				Co	nnectio	n Size			
DP (psig)	1/2	3/4	1	1-1/4	1-1/2	2	2-1/2	3	4		DP (barg)	15	20	25	32	40	50	65	80	100
7	7 4 7 11 22 29 37 61 86										0.5	15	27	40	85	110	140	230	325	481
10	5 9 13 27 35 44 73 103										0.7	18	32	48	102	132	168	275	389	575
15	5 9 13 27 35 44 73 10 6 10 15 33 43 54 89 12										1.0	22	40	59	125	161	205	337	476	704
25	8*	14*	20	43*	55*	70	115	163	240		1.7	30*	53*	76	162*	208*	265	435	615	908
50	11	19	28*	60	78	99*	163*	230*	339		3.4	40	72	106*	228	294	374*	617*	870*	1 285
75	13	23	35	74	95	121	199	281	416*		5.2	49	89	131	279	361	459	754	1065	1 575*
100	15	27	40	85	110	140	230	325	480		6.9	57	102	151	322	416	530	871	1230	1 817

 $^*\!$ At flows greater than this, velocities will exceed 10 ft/sec and pipe erosion could occur.

GD-20R	Dimens	ions	and W	eigh	ts																	
										(Connecti	on Si	ze									
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2	15 3/4 20 1 25 1-1/4 32 1-1/2 40 2 50 2-1/2 65 3 80 4 100 5 125 6 150 145 5-15/16 150 5-15/16 150 5-15/16 150 7-11/16 195 7-11																				
L	5-11/16	145	5-15/16	150	5-15/16	150	7-11/16	195	7-11/16	195	7-11/16	195	10-5/8	270	10-5/8	270	12-1/8	308	15-1/8	384	15-15/16	404
Н	11-5/8	296	11-5/8	296	12-1/2	317	15-9/16	395	15-9/16	395	16-5/16	415	21-7/8	555	22-15/16	582	25-3/8	645	33-7/16	849	36-1/8	918
H ₁	2-1/4	57	2-1/4	57	2-5/8	67	3	76	3	76	3-3/16	81	4-5/16	110	4-15/16	125	5-5/8	143	7-1/16	179	8-1/16	204
Wt., lb (kg)	18 (8	3)	18 (8)	22 (1											4)	156 (71)	320 (1	45)	386 (1	75)
C_{V}	1.5		2.7	7	4		8		11		14		23		32		48		75		108	

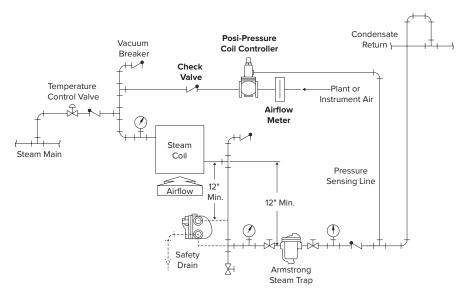
GD-20R Spe	cifications										
Pressure	Sat Dr	essure						Materials			
	Set Fi	Spring		Max.	Min.						
Inlet psig (barg)	1/2" - 3" (15 - 80 mm)	4" - 6" (100 - 150 mm)	Color	Application	Temp. °F (°C)	Diff. psig (barg)	Main Valve	Valve Seat	Diaphragm	Connection	
150 (10)	7 - 36 (.48 - 2.5) 37 - 100 (2.5 - 6.9)	7 - 36 (.48 - 2.5) 37 - 72 (2.5 - 5.0)	Yellow Black	Liquid	175 (79)	7 (.48)	NBR	Stainless Steel AISI 304	NBR	ANSI 150 lb. Flanged	



Armstrong Posi-Pressure Control System

A Revolutionary Way to Provide Positive Condensate Drainage for Heat Exchange Equipment







Posi-Pressure Control System Suggested Installation

Posi-Pressure Control System Kit, consisting of controller, check valve, airflow meter

Forget About Flooded Heat Exchangers

The major cause of flooded heat exchangers is a lack of sufficient pressure differential across the steam trap under modulated steam conditions. With Armstrong's Posi-Pressure Control System, there is always a minimum preset differential pressure between the heat exchanger and the condensate return system. Even if the pressure in the condensate return changes, the Posi-Pressure Controller automatically adjusts to maintain the preset differential.

Forget About Water Hammer

When heat exchangers flood, steam and cold condensate frequently come in contact with each other. When this happens, the steam rapidly condenses, causing water hammer. This water hammer condition can cause damage to heat exchangers, piping and fittings. By eliminating heat exchanger flooding, the Posi-Pressure Control System will solve the problem.

Forget About Frozen Steam Coils

Most steam coils freeze because they are flooded with condensate. Costly—bulky—and high maintenance face and by-pass coil systems were created to solve this problem by maintaining a positive differential steam pressure. Now, with Armstrong's Posi-Pressure Control System, simple and inexpensive modulated control systems can do the same job. However, we must caution that proper steam coil design, steam trapping and venting practices are also required for freeze protection. If assistance is needed, Armstrong's Representatives are trained to analyze your total steam system and offer you solutions to your problems.

How Does the Posi-Pressure Control System Work?

A normal steam system may modulate into a vacuum to control temperature. A vacuum breaker is often installed to prevent this condition. Once the vacuum breaker opens, temperature control is accomplished by mixing the air with the steam. The steam/air mixture results in a lower temperature. However,

even a vacuum breaker will not work if condensate has to be elevated to an overhead return, or if the return system is pressurized.

The Posi-Pressure Control System acts as a vacuum breaker. Instead of introducing air at atmospheric pressure, the controller injects air at an elevated pressure into the heat exchanger. The user presets the level of elevated air pressure at the time of installation. Rather than a specific pressure, the controller maintains a specific differential pressure across the steam trap. Even if a steam trap fails or other causes change the condensate return pressure, the controller will sense this difference and maintain the preset differential.

How Much Air Will Be Used?

The Posi-Pressure Control System uses very little air. The amount depends upon the size of the steam trap selected. Air usage can vary from as little as 10 SCFH to 90 SCFH or more on large systems. To put this in perspective, a 27 SCFH parcel of air amounts to a 3-foot cube in one hour! Once the initial air is introduced, only the leakage through the large vent bucket in the steam trap must be added. This air volume is so low that it is practically undetectable in a deaerator.

Are There Any Other Advantages?

Yes! It is generally recommended that float and thermostatic traps be used on modulated steam systems because they drain better when there is no motive pressure other than the static head of condensate. With a positive pressure always being maintained by the Posi-Pressure Control System, an inverted bucket steam trap with its inherent longer life expectancy can, and must, be used. Since air is injected at a positive pressure, carbon dioxide (the real cause of corrosion) is diluted and swept clear of the heat exchanger.

For a fully detailed certified drawing, refer to CDY #1041.

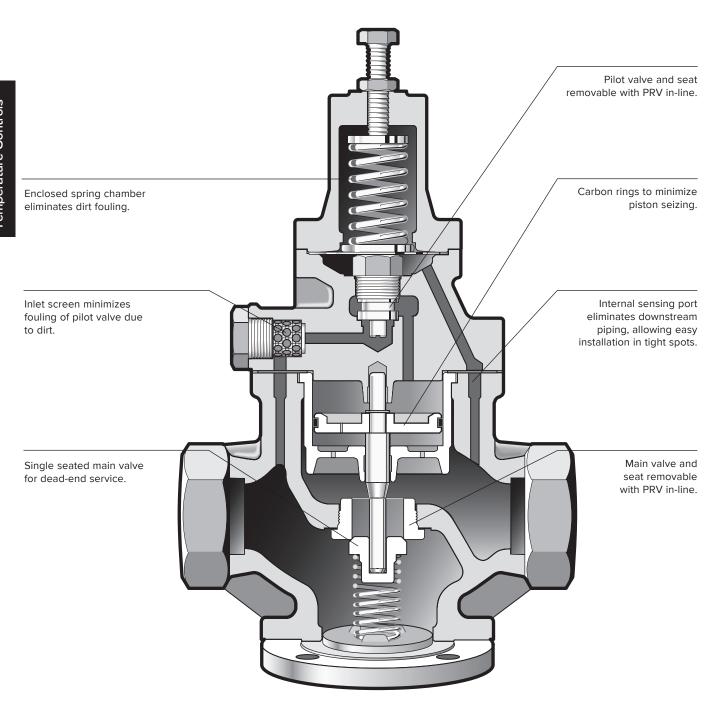


Internally Piloted

For Steam, Air and Non-Corrosive Gas Service

This type of PRV incorporates two valves—a pilot and main valve—in one unit. The pilot valve has a design similar to the direct acting valve. The discharge pressure from the pilot valve is transmitted on top of a piston which opens the main valve. This design makes use of inlet pressure in opening a

larger main valve than could otherwise be opened directly. As a result, there is a greater capacity per line size and greater accuracy ($\pm 5\%$) than with the direct acting valve.





For Steam, Air and Non-Corrosive Gas

The GP-1000 Series valves are pilot-controlled for accurate regulation of pressure under wide-ranging flow. Internal pilot design eliminates external components and piping.

Internally piloted GP Series valves are capable of larger capacity and greater accuracy than direct acting valves.

Completely supported by piping, lightweight GP Series valves install easily with NPT or flanged connections. A stainless steel diaphragm, hardened stainless steel working parts and integral removable strainer team up to provide

high performance over a long, trouble-free service life. Valves are equipped with a single seated main valve, piston valve rings for longer life and an external adjusting screw with locking nut. All working parts are renewable in-line. ANSI Class IV Shutoff.

For a fully detailed certified drawing, refer to list below.

GP-1000 NPT CD #2104 GP-1000 Flanged CD #2105 GP-1000 SS/AS CDY #1081

GP-1000												
	Pressure				Maximum							
Model Number	Inlet psig (barg)	Reduced psig (barg)	Spring Color	Application	Temp. °F (°C)	Minimum Diff. psig (barg)	Body	Main Valve/ Valve Seat	Pilot Valve/ Seat	Piston/Cylinder	Diaphragm	
NPT	15 - 250	7 - 125 (.48 - 8.6)	Black							Stainless Steel		
GP-1000	(1 - 17)	125 - 200 (8.6 - 13.8)	Green	Steam	450 (232)		Ductile Iron ASTM	Stainless Steel AISI 420	Stainless Steel AISI 403/420	AISI 420/Stainless Steel AISI 403		
150 ANSI GP-1000	15 - 150 (1 - 10)	7 - 125 (.48 - 8.6)										
NPT GP-1000A	15 - 150 (1 - 10)	7 - 125 (.48 - 8.6)	Black	Air & Gas	175 (80)	7 (.48)	A536	Stainless Ste	eel AISI 420/ w/NBR	Bronze/Bronze ASTM C36000	Stainless Steel AISI 301	
150 ANSI GP-1000A	15 - 150 (1 - 10)	7 - 125 (.48 - 8.6)	ыаск		(80)			Didss	W/INDR			
GP-1000SS* GP-1000AS*	15 - 150 (1 - 10)	7 - 125 (.48 - 8.6)		Steam	450 (232)		Stainless Steel AISI 304	Stainless Steel AISI 420	Stainless Steel AISI 403/420	Stainless Steel AISI 420/Stainless Steel AISI 403		

NOTES: Sizes 2" (50 mm) and below are NPT connections. Sizes 2" (50 mm) and larger are flanged connections. Turndown ratio for GP-1000 20:1.

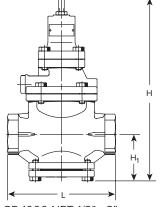
^{*}GP-1000SS/GP-1000AS are available in 1/2" - 2" only and are flanged with NPT companion flanges.

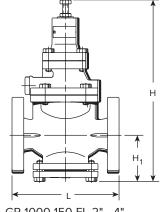
GP-1000, GP-1000	A, GP-1	0005	S, GP-1	0004	S Dime	nsion	s and W	eight	5									
									Conne	ction	Size							
Symbol	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2	15	3/4	20	1	25	1-1/4	32	1-1/2	40	2*	50	2-1/2	65	3	80	4	100
L	5-7/8	150	6-1/8	155	6-5/16	160	7-1/2	190	7-1/2	190	8-11/16	220	9-5/8	245	11-3/8	290	13	330
Н	11-1/4	285	11-1/4	285	11-7/8	300	12-3/4	323	12-3/4	323	13-5/8	347	14	357	15-7/8	404	17-3/4	450
H ₁	2-1/2	64	2-1/2	64	2-5/8	67	3-1/4	82	3-1/4	82	3-11/16	93	4	100	4-13/16	122	5-9/16	144
Wt, lb (kg)	15-1/2	2 (7)	15-1/2	2 (7)	19 (8	3.5)	25-1/2	(12)	27-1/2 (12.5)	40 (1	8)	66 (30)	77 (3	35)	116 (53)
C_V	1		2.3	3	4		6.5	5	9		16		2!	5	36	5	64	4

NOTES: GP-1000 is 1/2"-2" (20-50 mm) NPT, 2"- 4" (50-100 mm) ANSI 150 lb flanged.

^{* &}quot;L" Dimension for 2" 150# flange is 8-11/16" (220 mm).







GP-1000 NPT 1/2" - 2" GP-1000 150 FL 2" - 4"



Capacities for Steam, Air and Non-Corrosive Gas

-1000 <u>C</u>	Capacities—S	team								
					lb/hr					
					С	onnection Size	ze			
Inlet	Outlet					in				
р	sig	1/2	3/4	1	1-1/4	1-1/2	2	2-1/2	3	4
C _V F	actor	1	2.3	4	6.5	9	16	25	36	64
1E	8	40	93	161	261	362	644	1005	1 448	2 574
15	7	43	98	170	277	383	681	1264	1 533	2 725
20	13	44	101	176	285	395	702	1 097	1580	2 809
20	7	60	130	227	369	511	909	1 421	2 047	3 639
30	23	50	116	202	328	454	807	1 261	1 816	3 228
30	7	76	176	306	497	688	1 223	1 911	2 752	4 892
	33	56	129	225	365	506	900	1 406	2 024	3 598
40	25	79	182	316	514	711	1 2 6 4	1 976	2 845	5 057
	5 - 12	94	215	374	608	842	1 497	2 338	3 367	5 986
	42	65	151	262	425	589	1 047	1636	2 356	4 188
50	30	98	226	393	638	884	1 572	2 456	3 536	6 287
	7 - 17	111	254	443	719	996	1 770	2 766	3 983	7 08
	63	94	216	376	612	847	1506	2 353	3 388	6 024
75	45	141	323	562	914	1265	2 249	3 515	5 061	8 998
	7 - 30	153	353	614	997	1380	2 454	3 835	5 522	9 817
	85	119	274	476	774	1 072	1905	2 977	4 287	7 622
100	70	162	374	650	1 0 5 6	1462	2 599	4 061	5 847	10 39
	7 - 42	196	451	785	1 275	1 765	3 138	4 903	7 061	12 55
	106	148	340	591	960	1329	2 363	3 693	5 318	9 454
	100	167	385	670	1 089	1 507	2 680	4 187	6 029	10 71
125	75	225	517	900	1462	2 024	3 598	5 623	8 097	14 39
	7 - 55	239	549	956	1553	2 150	3 822	5 972	8 600	15 28
	125	183	421	733	1 191	1649	2 931	4 580	6 595	11 72
	100	248	571	993	1 613	2 234	3 971	6 205	8 936	15 88
150	80	283	651	1 132	1 839	2 547	4 528	7 074	10 187	18 11 ⁻
	8 - 67	282	648	1 127	1 831	2 535	4 506	7 041	10 139	18 02
	148	205	471	819	1 331	1 844	3 277	_	_	_
	125	270	620	1 078	1752	2 426	4 312	_	_	_
175	100	317	730	1269	2 062	2 856	5 077	_	_	_
	9 - 80	324	746	1298	2 109	2 919	5 190	_	_	_
	170	230	529	919	1494	2 069	3 678	_	_	_
	150	289	665	1 157	1880	2 603	4 628	_	_	_
200	125	342	787	1369	2 225	3 081	5 478	_	_	_
	10 - 92	367	844	1 469	2 386	3 304	5 874	_	_	_
	191	258	594	1 034	1680	2 326	4 135	_	_	_
005	175	308	708	1 231	2 000	2 769	4 923	_	_	_
225	150	366	841	1 463	2 377	3 292	5 852	_	_	_
	12 - 105	410	943	1640	2 664	3 689	6 558	_	_	_
	200	325	748	1 301	2 113	2 926	5 202	_	36 1 448 1 533 1 580 2 047 1 816 2 752 2 024 2 845 3 367 2 356 3 536 3 983 3 388 5 061 5 522 4 287 5 847 7 061 5 318 6 029 8 097 8 600 6 595 8 936 10 187 10 139	_
	175	388	892	1 551	2 520	3 489	6 203	_	_	_
250	150	435	1 001	1 741	2 829	3 916	6 963	_	36 1 448 1 533 1 580 2 047 1 816 2 752 2 024 2 845 3 367 2 356 3 536 3 983 3 388 5 061 5 522 4 287 5 847 7 061 5 318 6 029 8 097 8 600 6 595 8 936 10 187 10 139	_
	13 - 117	453	1 041	1 811	2 942	4 074	7 242	_	_	_

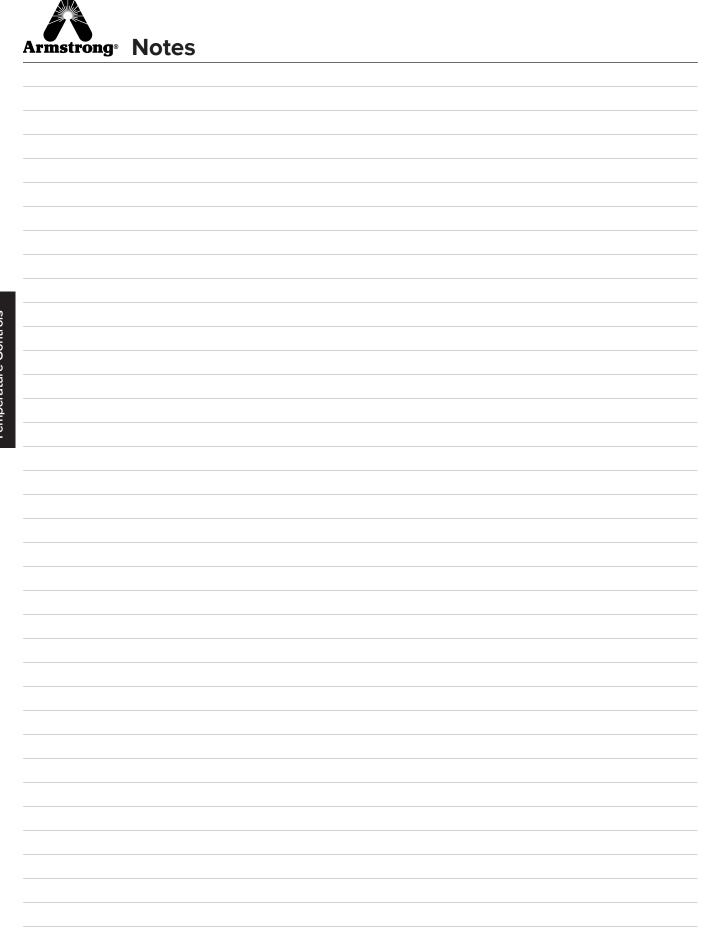
NOTE: For air capacities scfm, multiply steam capacities lb/hr by 0.36.



Capacities for Steam, Air and Non-Corrosive Gas

	Capacities—S				Jan. //								
					kg/hr								
Inlet	Outlet				С	onnection Si	ze						
		mm											
	arg	15	20	25	32	40	50	65	80	100			
C _V I	Factor	1	2.3	4	6.5	9	16	25	36	64			
1.03	0.55	18	42	73	119	164	292	456	657	1 168			
1.03	0.48	20	44	77	126	174	309	483	695	1 23			
1.38	0.90	20	46	80	129	179	319	498	717	1 27			
1.50	0.48	25	59	103	167	232	412	644	928	165			
2.07	1.59	23	53	92	149	206	366	572	824	146			
2.07	.48	35	80	139	225	312	555	867	1 248	2 21			
	2.28	26	59	102	166	230	408	638	918	163			
2.76	1.72	36	82	143	233	323	574	896	1 290	2 29			
	.4883	42	98	170	276	382	679	1 061	1527	2 71			
	2.90	30	68	119	193	267	475	742	1 069	190			
3.45	2.07	45	102	178	290	401	713	1 114	1604	2 85			
	.48 - 1.17	50	115	201	326	452	803	1 255	1807	3 21			
	4.34	43	98	171	278	384	683	1 067	1 537	2 73			
5.17	3.10	64	147	255	415	574	1020	1 594	2 296	4 08			
	.48 - 2.1	70	160	278	452	626	1 113	1739	2 505	4 45			
	5.86	54	124	216	351	486	864	1350	1 945	3 45			
6.89	4.83	74	169	295	479	663	1 179	1842	2 652	4 71			
	.48 - 2.9	89	205	356	578	801	1 423	2 224	3 203	5 69			
	7.31	67	154	268	436	603	1072	1 675	2 412	4 28			
8.62	6.89	76	175	304	494	684	1 215	1899	2 735	4 86			
	5.17	102	235	408	663	918	1 632	2 550	3 673	6 52			
	.48 - 3.7	108	249	433	704	975	1734	2 709	3 901	6 93			
	8.62	83	191	332	540	748	1330	2 077	2 991	5 31			
10.00	6.89	113	259	450	732	1 013	1 801	2 815	4 053	7 20			
	5.52	128	295	513	834	1 155	2 054	3 209	4 621	8 21			
	.55 - 4.6	128	294	511	830	1150	2 044	3 194	4 599	8 17			
	10.20	93	214	372	604	836	1 487	_	_	_			
12.07	8.62	122	281	489	795	1100	1956	_	_	_			
	6.89	144	331	576	936	1 295	2 303	_	_	_			
	.62 - 5.5	147	338	589	956	1324	2 354	_	_	_			
	11.72	104	240	417	678	938	1668	_	_	_			
13.79	10.34	131	302	525	853	1 181	2 099	_	_	_			
	8.62	155	357	621	1009	1398	2 485	_	_	_			
	.68 - 6.3	167	383	666	1082	1499	2 665	_	_	_			
	13.17	117	270	469	762	1055	1876	_	_	_			
15.51	12.07	140 166	321	558	907	1 256	2 233	_	_	_			
	10.34	166	382	664	1 078	1493	2 654	_	_	_			
	.82 - 7.24	186	428	744	1209	1673	2 975	_	_	_			
	13.79	147 176	339	590	959	1327	2 360	_	_	_			
17.24	12.07	176	404	703	1 143	1583	2 814	_	_	_			
	10.34	197	454	790	1 283	1776	3 158	_	_	_			
	.89 - 8.06	205	472	821	1 3 3 5	1848	3 285	_	_	_			

For air capacities m^3/hr , multiply steam capacities kg/hr by 1.35.



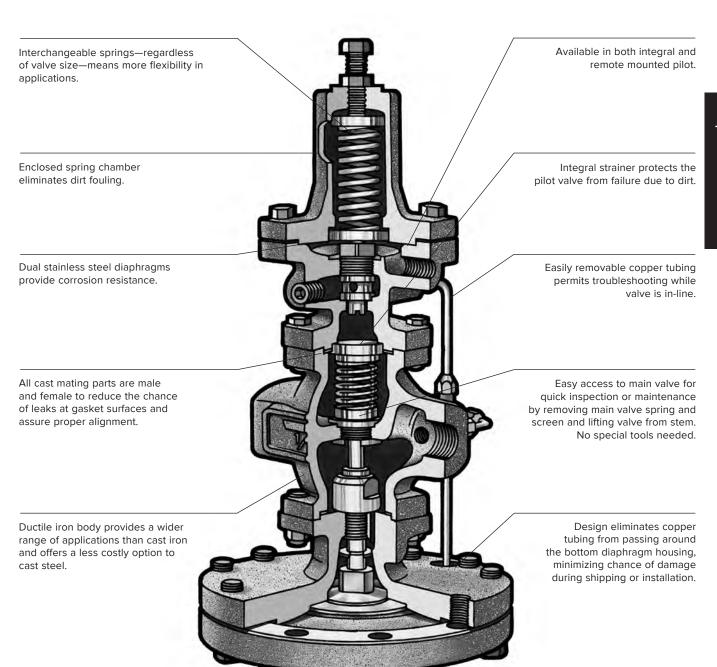
Externally Piloted



For Steam Service

This type is similar to the internally piloted piston-operated valve in that a pilot and main valve are utilized. However, double diaphragms replace the piston. This increased diaphragm area can open a larger main valve, allowing a greater capacity per line size than the internally piloted piston-operated valve. In addition, the diaphragms are more

sensitive to pressure changes, which results in accuracy of ±1%. This greater accuracy is due to the positioning of the sensing line downstream, where there is less turbulence. This valve also offers the flexibility to use different types of pilot valves (i.e., pressure, temperature, air loaded, solenoid or combination).





For Steam Service

The GP-2000 is a high performance, externally piloted reducing valve for large capacity requirements. Typical use is on intermittent service, including applications such as heat exchangers, steam coils, rotating dryers, process equipment and heating systems. With a 20:1 rangeability and high C_v , the GP-2000 is reliable and accurate (+/-1% of pressure set point from 5% to 100% of flow) over a long, trouble-free service life. Hardened stainless steel working parts

are renewable in-line. Single seated for dead-end service. Available with both NPT (1/2" - 2") and flanged connections in 1/2" - 6" sizes. ANSI Class IV Shutoff.

For a fully detailed certified drawing, refer to:

GP-2000 CDY #1008 GP-2000 Flanged CDY #1007

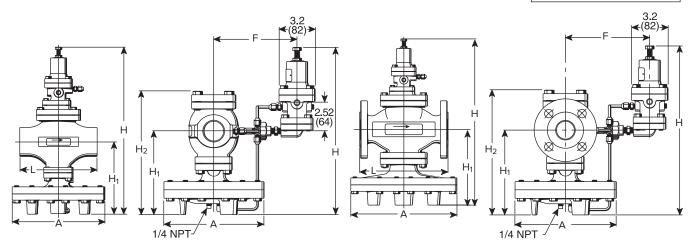
GP-2000 Sp	ecifications									
		Reduced		Maximum	Minimum			Materials		
Application	Inlet Pressure psig (barg)	Pressure psig (barg)	Spring Color	Temperature °F (°C)	Differential psig (barg)	Body	Main Valve/Seat	Pilot Valve/Seat	Diaphragm	Color
Steam	NPT 15 - 300 (1 - 20) 15 - 185 (1 - 13) 150 lb. Flanged 15 - 300 (1 - 20) 300 lb. Flanged	*1.5 - 3 - (.1021) 3 - 21 (.21 - 1.4) - 15 - 200 (1 - 13.8)	Yellow Yellow Green	450 (232)	7 (.48)	Ductile Iron ASTM A536	Stainless St	eel AISI 420	Stainless Steel AISI 301	Dark Gray

*NOTE: When using this spring range, remove one (1) pilot diaphragm. Capacities are reduced by 1/2 of capacity chart when this spring is being used.

GP-2	000	Dimens	ions	and We	ights	;																				
Siz			Fa	ce-to-F	ace "	L"				F		LI Into		H Rem	-4-							We	eight	t		
312	:e	NP1	Г	150	#	300	#	Α		Г		H Inte	grai	пкет	ote	H ₁		H ₂	2	N	РТ	15	0#	30	0#	C_{V}^{*}
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	
1/2	15	5-15/16	150	_	_	_	_	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170	9-5/8	244	34	14	36	15	42	19	5.0
3/4	20	5-15/16	150	_	_	-	-	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170	9-5/8	244	34	14	36	15	42	19	7.2
1	25	6-5/16	160	5-3/4	147	_	_	8-15/16	226	7-1/16	179	15-15/16	404	14-7/16	367	6-15/16	175	10	254	44	19	48	20	54	23	10.9
1-1/4	32	7-1/8	180	6-1/2	166	_	-	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192	11-1/8	283	51	22	53	22	59	25	14.3
1-1/2	40	7-1/8	180	7-7/16	189	_	-	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192	11-1/8	283	51	22	55	23	61	26	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	10-15/16	276	7-11/16	195	19-5/8	498	16	406	8-1/2	216	12-5/8	321	75	33	81	36	84	36	32
2-1/2	65	_	_	10-15/16	278	11-1/2	292	13-13/16	352	8-5/16	211	21-3/4	552	17-5/16	440	9-13/16	251	14-3/4	375	_	-	142	65	150	65	60
3	80	ı	-	11-3/4	298	12-7/16	315	13-13/16	352	8-3/4	222	22-5/8	575	17-15/16	456	10-7/16	264	15-3/4	400	_	_	155	69	166	72	78
4	100	-	_	13-1/2	343	14-1/8	359	15-13/16	401	9-7/16	239	25-15/16	658	20-1/8	511	12-5/8	321	19-1/4	489	_	_	247	112	264	119	120
6	150	_	_	18-1/8	460	19	483	19-3/4	502	_	_	31-3/4	806	_	_	16-1/4	414	26-1/2	673	_	_	507	230	553	252	250

 $^*50\%$ reduced port available for sizes 1/2" - 4". The CV value should be divided by 2 to get reduced port CV.

For capacities see page 305.





For Steam Service

The GP-2000L is a high performance, externally piloted reducing valve for large capacity and low inlet pressure requirements. The GP-2000L is reliable and accurate (+/-1% of pressure set point from 5% to 100% of flow) over a long, trouble-free service life. Hardened stainless steel working

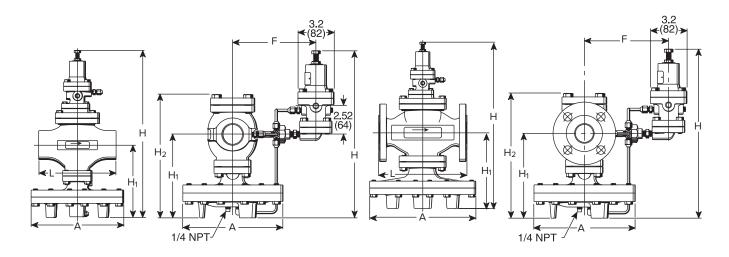
parts are renewable in-line. Single seated for dead-end service. Available with both NPT (1/2" - 2") and flanged connections in 1/2" - 4" sizes. ANSI Class IV Shutoff.

GP-2000L Sp	ecifications									
	Inlet	Reduced		Maximum	Minimum			Materials		
Application	Pressure psig (barg)	Pressure psig (barg)	Spring Color	Temperature °F (C)	Differential psig (barg)	Body	Main Valve/ Seat	Pilot Valve/ Seat	Diaphragm	Color
Steam	5 - 15 (.3 - 1)	2 - 12 (.138)	Yellow	450 (232)	3 (.21)	Ductile Iron ASTM A536	Stainless St	eel AISI 420	Stainless Steel AISI 301	Dark Gray

GP-2	000	L Dimer	sion	s and W	/eigh	ts																				
			Fa	ace-to-F	ace "	L"		^		F		LI Into		LI Dam								We	eight	t		\Box
Siz	ze	NP	Г	150	#	300	#	Α		Г		H Inte	grai	H Rem	ote	H ₁		H ₂	2	N	РТ	15	0#	30	0#	c _v *
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	
1/2	15	5-15/16	150	_	_	-	_	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170	9-5/8	244	34	14	36	15	42	19	5.0
3/4	20	5-15/16	150	_	_	-	-	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170	9-5/8	244	34	14	36	15	42	19	7.2
1	25	6-5/16	160	5-3/4	147	_	_	8-15/16	226	7-1/16	179	15-15/16	404	14-7/16	367	6-15/16	175	10	254	44	19	48	20	54	23	10.9
1-1/4	32	7-1/8	180	6-1/2	166	-	_	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192	11-1/8	283	51	22	53	22	59	25	14.3
1-1/2	40	7-1/8	180	7-7/16	189	_	_	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192	11-1/8	283	51	22	55	23	61	26	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	10-15/16	276	7-11/16	195	19-5/8	498	16	406	8-1/2	216	12-5/8	321	75	33	81	36	84	36	32
2-1/2	65	_	_	10-15/16	278	11-1/2	292	13-13/16	352	8-5/16	211	21-3/4	552	17-5/16	440	9-13/16	251	14-3/4	375	_	-	142	65	150	65	60
3	80	_	_	11-3/4	298	12-7/16	315	13-13/16	352	8-3/4	222	22-5/8	575	17-15/16	456	10-7/16	264	15-3/4	400	_	_	155	69	166	72	78
4	100	_	-	13-1/2	343	14-1/8	359	15-13/16	401	9-7/16	239	25-15/16	658	20-1/8	511	12-5/8	321	19-1/4	489	-	-	247	112	264	119	120

 $^{^*50\%}$ reduced port available for sizes 1/2" - 4". The C_V value should be divided by 2 to get reduced port C_V .

For capacities see page 315.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



GP-2000CS Carbon Steel Body

For Steam Service

The GP-2000CS is a high performance, externally piloted reducing valve for large capacity requirements. Typical use is on intermittent service, including applications such as heat exchangers, steam coils, rotating dryers, process equipment and heating systems. With a 20:1 rangeability and high C_V , the GP-2000CS is reliable and accurate (+/-1% of pressure set point from 5% to 100% of flow) over a long, trouble-free service life. Stellited stainless steel working

parts are renewable in-line. Single seated for dead-end service. Available with both NPT (1/2" - 2") and flanged connections in 2" - 4" sizes.

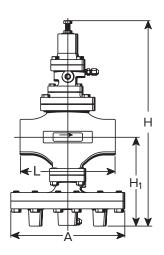
For a fully detailed certified drawing, refer to:

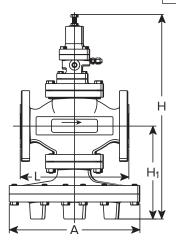
GP-2000 CDY #1008 GP-2000 Flanged CDY #1007

GP-2000GP-	2000CS Specific	cations								
	Inlet Pressure	Reduced	Spring	Maximum	Minimum		ı	Materials		
Application	psig (barg)	Pressure psig (barg)	Color	Temperature °F (°C)	Differential psig (barg)	Body	Main Valve/Seat	Pilot Valve/Seat	Diaphragm	Color
Steam	NPT 15 - 450 (1 - 31) 150 lb Flanged 15 - 140 (1 - 9.6) 300 lb Flanged 15 - 450 (1 - 31)	3 - 21 (.21 - 1.4) 15 - 200 (1 - 13.6) 190 - 300 (13.1 - 20.6)	Yellow Green Brown	600°F (315°C)	7 (.48)	Carbon Steel WCB ASTM216 A216M-08	Stainless Steel 304 Stainless Steel Stellite	420 Stainless Steel	Stainless Steel AISI 301	Silver

GP-2	0000	CS Dime	nsior	ns and W	eight	s																		
Si	70			L				А		_		Н		H₁						We	eight			
٦	26	NP	Γ	150#	<i>‡</i>	300	#	1		<u>'</u>		Integr	al	''1		H ₂	2	NF	РΤ	15	0#	30	0#] c _v
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	oxdot
1/2	15	5-15/16	150	_	-	-	-	7-15/16	200	6-7/8	176	15-3/4	398	6-3/4	170	9-5/8	244	35	16	_	_	_	_	5.0
3/4	20	5-15/16	150	_	_	-	_	7-15/16	200	6-7/8	176	15-3/4	398	6-3/4	170	9-5/8	244	35	16	_	_	_	_	7.2
1	25	6-5/16	160	_	_	-	_	8-15/16	226	7-1/16	179	15-15/16	404	6-15/16	175	10	254	49	22	_	_	_	_	10.9
1-1/4	32	7-1/8	180	_	- 1	_	– 1	8-15/16	226	7-7/16	188	17-1/8	434	7-5/8	192	11-1/8	283	53	24	_	_	_	_	14.3
1-1/2	40	7-1/8	180	_		-	_	8-15/16	226	7-7/16	188	17-1/8	434	7-5/8	192	11-1/8	283	53	24	_	_	_	_	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	10-15/16	276	7-11/16	195	19-5/8	498	8-1/2	216	12-5/8	321	62	37	88	40	92	42	32
2-1/2	65	_	_	10-15/16	278	11-1/2	292	13-13/16	352	8-5/16	211	21-3/4	552	9-13/16	251	14-3/4	375	-	- 1	159	72	168	76	60
3	80	_	_	11-3/4	298	12-7/16	315	13-13/16	352	8-3/4	222	22-5/8	575	10-7/16	264	15-3/4	400		-	174	79	185	84	78
4	100	_		13-1/2	343	14-1/8	359	15-13/16	401	9-7/16	239	25-15/16	658	12-5/8	321	19-1/4	489			276	125	293	133	120

For capacities see page 305.





GP-2000K-1/GP-2000K-3/GP-2000K-6



Air Loaded Valves for Steam

A high performance externally air piloted pressure reducing valve, the GP-2000K-1/GP-2000K-3/GP-2000K-6 is an ideal choice when set point changes are frequent and access to the PRV is difficult. The valve comes totally assembled and requires no field installation except downstream sensing line and air line connection. High Cv, 20:1 turndown ratio and accurate control $\pm 1\%$ of pressure set point from 5% to 100% of flow. A rugged ductile iron body, hardened stainless steel working parts, double stainless steel diaphragms and in-line repairability add up to reliability on the job. Single seated for dead-end service.

For a fully detailed certified drawing, refer to:

GP-2000K CDY #1014 GP-2000K Flanged CDY #1015

GP-20	00K-1, G	SP-2000	K-3, GF	P-2000F	(-6 Weig	ghts		
C:	ze			Weight	, lb (kg)			
31	26	NI	PT	15	0#	30	0#	C _V
in	mm	lb	kg	lb	kg	lb	kg	
1/2	15	34	16	36	15	42	19	5.0
3/4	20	34	16	36	15	42	19	7.2
1	25	44	20	48	20	54	23	10.9
1-1/4	32	51	23	53	22	59	25	14.3
1-1/2	40	51	23	55	23	61	26	18.8
2	50	75	34	81	36	84	36	32
2-1/2	65	_	_	142	65	150	65	60
3	80	_	_	155	69	166	72	78
4	100	_	_	247	112	264	119	120
6	150	_	_	507	230	553	252	250

^{*50%} reduced port available for sizes 1/2" - 4". The CV value should be divided by 2 to get reduced port CV.

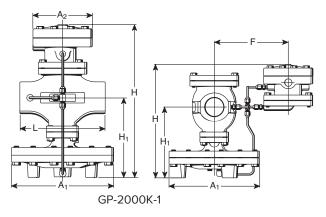
⁺ For GP-2000K-3 and GP-2000K-6 weights, add 7-1/4 lb. (3.3 kg).

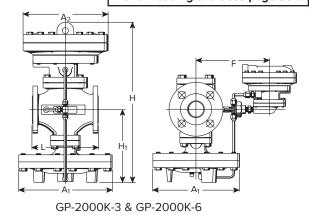
GP-2000K-1,	GP-2000K-3, GP	2-2000K-6 Specification	ıs						
	Inlet Pressure	Reduced Pressure	Max.	Minimum		M	laterials		
Application	psig (barg)	psig (barg)	Temp. °F (°C)	Differential psig (barg)	Body	Main Valve/ Seat	Pilot Valve/ Seat	Diaphragm	Color
Steam	NPT 15 - 300 (1 - 20) 150 lb Flanged 15 - 185 (1 - 13) 300 lb Flanged 15 - 300 (1 - 20)	K-1 7 - 125 (.48 - 8.6) K-3 30 - 200 (2 - 13.8) K-6 45 - 200 (3.1 - 13.8)	450 (232)	7 (.48)	Ductile Iron ASTM A536	Stainles AISI 4		Stainless Steel AISI 301	Dark Gray

GP-20	000K-	1, GP-200	00K-3	, GP-2000)K-6 D	imensior	าร												
				Face-to-F	ace "L	,,				_		Lilinda		LI Dam	-4-			** A	
Siz	ze	NPT	•	150#	#	300	#	A ₁				H Inte	grai	H Rem	ote	H ₁		**▲	12
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
1/2	15	5-15/16	150	_	_	-	-	7-15/16	200	6-7/8	175	13-3/16	335	11-13/16	300	6-3/4	170	3-1/4	82
3/4	20	5-15/16	150	-	_	-	ı	7-15/16	200	6-7/8	175	13-3/16	335	11-13/16	300	6-3/4	170	3-1/4	82
1	25	6-5/16	160	5-3/4	147	_	-	8-15/16	226	7-1/16	179	13-7/16	341	12	305	6-15/16	175	3-1/4	82
1-1/4	32	7-1/8	180	6-1/2	166	ı	ı	8-15/16	226	7-7/16	188	14-5/8	371	12-11/16	322	7-5/8	192	3-1/4	82
1-1/2	40	7-1/8	180	7-7/16	189	_	-	8-15/16	226	7-7/16	188	14-5/8	371	12-11/16	322	7-5/8	192	3-1/4	82
2	50	9-1/8	230	8-9/16	217	9-1/8	232	10-15/16	276	7-11/16	195	17-1/8	435	13-1/4	337	8-1/2	216	3-1/4	82
2-1/2	65	_	_	10-15/16	278	11-1/2	292	13-13/16	352	8-5/16	211	19-1/4	489	15-3/8	391	9-13/16	251	3-1/4	82
3	80	_	-	11-3/4	298	12-7/16	316	13-13/16	352	8-3/4	222	20-1/8	512	16-3/8	416	10-7/16	264	3-1/4	82
4	100	_	_	13-1/2	343	14-1/8	359	15-13/16	401	9-7/16	239	23-7/16	595	19-7/8	505	12-5/8	321	3-1/4	82
6	150		_	18-1/8	460	19	483	19-3/4	502	-	_	29-3/8	746	-	_	27-1/4	692	3-1/4	82

^{*}For GP-2000K-3 and GP-2000K-6 add 1-1/4" (18 mm) to "H" dimension.

For capacities see page 305.
For air loading chart see page 301.





Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

^{**}For GP-2000K-3 and GP-2000K-6, A2 dimension = 6-13/16" (172 mm).



Air Loaded Valves for Steam

The GD-2000K is an ideal choice when set point changes are frequent, access to the valve is difficult and steam quality is poor. The GD-2000K comes with either NPT or flanged connections for quick, easy installation. It also comes with a durable ductile iron body and features double stainless steel diaphragms and hardened stainless working parts,

renewable in-line. High Cv and 10:1 turndown ratio. Single seated for dead-end service.

For a fully detailed certified drawing, refer to:

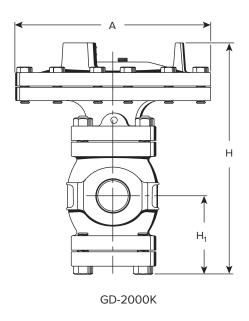
GD-2000K NPT CDY #1020 GD-2000K Flanged CDY #1021

GD-2000K Sp	ecifications							
	Inlet Pressure	Reduced	Maximum	Minimum		Materials		
Application	psig (barg)	Pressure psig (barg)	Temperature °F (°C)	Differential psig (barg)	Body	Main Valve/Seat	Diaphragm	Color
	NPT 15 - 300 (1 - 20)							
Steam	150 lb Flanged 15 - 185 (1 - 13)	7 - 200 (.48 - 13.8)	450 (232)	7 (.48)	Ductile Iron ASTM A536	Stainless Steel AISI 420	Stainless Steel AISI 301	Dark Gray
	300 lb Flanged 15 - 300 (1 - 20)							

C:-				Face-to-	Face			٠		٠.,						We	eight			1
Siz	e e	NPT	•	150#	#	300	#	H.	I	Н		A		NI	PT	15	0#	30	0#	C _v *
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	
1/2	15	5-15/16	150	_	_	_	_	2-7/8	74	9-5/8	244	7-15/16	200	27	13	_	_	_	_	5.0
3/4	20	5-15/16	150	_	_	_	_	2-7/8	74	9-5/8	244	7-15/16	200	27	13	_	_	_	_	7.2
1	25	6-5/16	160	_	_	_	_	3-1/16	76	10	251	8-15/16	226	35	17	_	_	_	_	10.9
1-1/4	32	7-1/8	180	_	_	_	_	3-1/2	90	11-1/8	282	8-15/16	226	43	20	_	_	_	_	14.3
1-1/2	40	7-1/8	180	_	_	_	_	3-1/2	90	11-1/8	282	8-15/16	226	43	20	_	_	_	_	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	4-1/2	114	12-5/8	319	10-15/16	276	66	31	72	34	73	34	32.0
2-1/2	65	_	_	10-15/16	278	11-1/2	292	4-3/4	122	14-3/4	373	13-13/16	352	_	_	135	62	136	62	60.0
3	80	_	_	11-3/4	298	12-7/16	315	5-1/2	140	15-3/4	399	13-13/16	352	_	_	146	67	152	69	78.0
4	100	_	_	13-1/2	343	14-1/8	359	6-1/2	167	19-1/4	488	15-13/16	401	_	_	230	105	240	109	120.0

^{*50%} reduced port available for sizes 1/2" - 4". The Cv value should be divided by 2 to get reduced port Cv.

For capacities see page 305. For air loading chart see page 301.

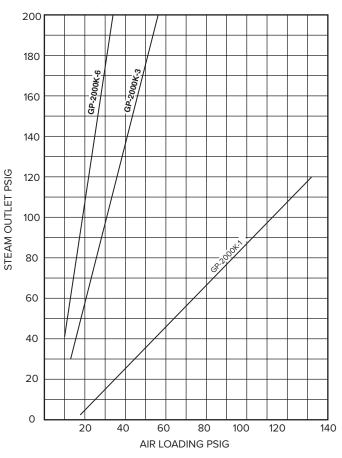




Air Loading Charts



GP-2000K-1,3,6



How to Use the Air Loading Charts (GP-2000K-1,3,6)

- Enter the graph at the steam outlet pressure from the value on the vertical axis.
- Move horizontally to the right until the air loading lines are intersected.
- Then read vertically below the point of intersection for the air loading pressure required.

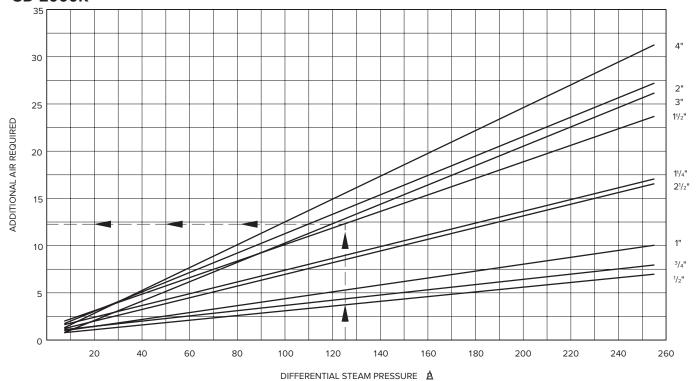
Selection Example (GD-2000K)

Read horizontally across the bottom of the chart to the 125 psig ΔP line.

Read vertically up to the diagonal line that corresponds to a 1-1/2" GD-2000K.

Read horizontally to the left for additional air signal required.

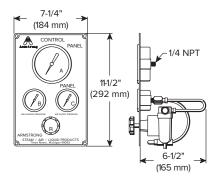
GD-2000K

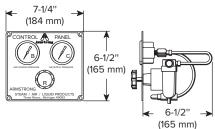


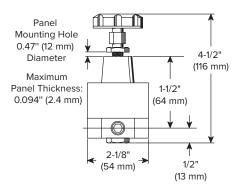


Control Panels & Air Loaders

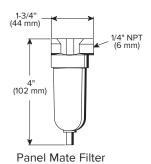
Armstrong Control Panels and Air Loaders are designed to provide the necessary air loading signal to control any air-operated pressure reducing valve. While designed specifically to control Armstrong pressure reducing valves such as the GP-2000K-1, 3 & 6, GD-2000K and GP-1000, these panels can remotely control other air-loaded valves. Panel is of rigid lightweight anodized aluminum for easy handling and installation. Control panel comes fully assembled with gauges suited to applications. Panel mate regulator and panel mate filter are standard on panels and are also available separately.







Panel Mate Regulator





For a fully detailed certified drawing, refer to:

"A" Panel CDY #1028

"Y" Panel CDY #1029

Materials of Constru	ction—Panel Mate—Filte	r
Name of Part	Panel Mate	Filter
Body	Z	inc
Bottom plug	Brass	_
Pilot diaphragm	Nitrile	_
Main diaphragm	Nitrile	_
Pilot valve	Stainless steel	_
Main valve	Polycarbonate	_
Main valve seat	Teflon	_
Bowl	_	Zinc
Element	_	Porous polypropylene
Elastomers	Nitrile, neoprene and polyurethane	Nitrile and neoprene

NOTE: Panel material is anodized aluminum.

Specifications—Control Panel											
Standa	rd Pressure Gauge Ra	nges									
Gauge	"A" Panel	"Y" Panel									
"A" psig (barg)	0 - 100 (0 - 7)	_									
"B" psig (barg)	0 - 100	(0-7)									
"C" psig (barg)	0 - 200	(0-14)									
Optional: Gauge "A" Ranges psig (barg)	0 - 30, 0-200, 0-300 (0-2, 0-14, 0-20)	_									
Optional: Gauge "B" and "C" Ranges psig (barg)	0-30, 0-100, 0-200, 0-300 (0-2, 0-7, 0-14, 0-20)										
Max. Inlet Air Pressure psig (barg)	200 (14)										
Max. Outlet Air Pressure psig (barg)	150 (10)										

Specifications—Panel Mate—Regulator and Filter											
	*Regulator Filter										
	psig	barg	psig	barg							
Inlet pressure maximum	200	14	250	17							
Outlet pressure maximum	150	10	_	_							
Temperature maximum, °F (°C)	160	(71)	175	(79)							

*NOTE: Use a panel mate filter upstream of regulator to prevent fouling.

louing.

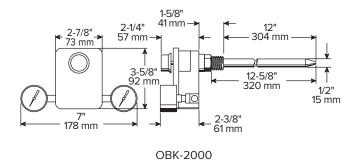


Pneumatic Temperature Pilot

A compact pneumatic temperature pilot with broad temperature ranges, the OBK-2000 can be remotely located away from the regulator valve, an advantage not available with a conventional capillary system.

Typical applications include instantaneous or storage tank water heaters, air make-up units and manufacturing process operations such as parts washing, die casting and plastic molding.

Capable of reverse-acting (heating) or direct-acting (cooling) operation, the OBK-2000 features a simple design with fewer moving parts for trouble-free operation. Other features include supply and control pressure gauges, a rugged cast brass housing, and precise and rapid response to temperature changes. Brass and stainless steel wells are available.



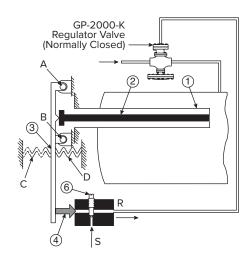
OBK-2000 Materials	
Name of Part	Material
Body	Brass
O-rings	Silicone Rubber/Buna "N"
Valve	Phos. Bronze
Valve Seat	Phos. Bronze

NOTE: Thermal wells available. 304 stainless steel or brass are standard materials. Other materials available upon request.

Reverse-Acting Operation—For Heating

During operation, a temperature change in the medium being controlled creates a change in the length of the sensitivity tube. An increase in temperature lengthens the sensitivity tube (1) and moves the invar rod (2) from the lever (3). The lever pivots at point B and is moved so the exhaust valve (4) is opened by the spring at (D). This lever action decreases the supply air at point (S) in the control line at point (R) and closes the regulator valve. A decrease in temperature shortens the sensitivity tube at point (1) and moves the invar rod against the lever point (3). The lever at this point moves against the spring at point (D) to close the exhaust valve at point (4). This lever action increases the pressure in the control line at point (R) and opens the valve.

The sensitivity adjustment screw at point (6) regulates the rate of flow of the supply air to the controller to a change in temperature. Turning the screw clockwise increases the sensitivity by reducing the flow and increasing the response time. Turning the screw counterclockwise decreases the sensitivity by increasing flow and reducing the response time. Valve closes on air failure, making it fail-safe.



Positions A and C show pivot point A and spring C when controller is direct acting.

OBK-2000 Specifications	
Dial adjustment range—°F (°C)	Standard—50 to 350 (10 to 177)
Maximum supply pressure (air) @ room temperature—psig (barg)	25 (2)
Air consumption (maximum)—SCIM (cm/s)	800 (218 - 3)
Maximum operating pressure—psig (barg)	250 (17)
Maximum operating temperature—°F (°C)	400 (204)
Temperature response—°F (°C)	0.5 (0.3)
Mounting—in (mm)	1/2 (15)
Air connections —in (mm)	1/8 (3)
Shipping weight—lb (kg)	4 (1.8)
Sensitivity (adjustable)—psig (barg)	1/4 to 2-1/4 (0.02 to 0.16)
Maximum pressure on wells	
Stainless steel—psig (barg)	1 125 (79)
Brass—psig (barg)	525 (36)



For Steam Back Pressure Regulation

The GP-2000R is a high performance externally piloted throttling back pressure valve for large capacity applications. Typical applications would include those systems utilizing flash steam for low pressure heating or processes. The GP-2000R valves will function to maintain a constant upstream pressure. This valve is not a safety valve and should not be used for that purpose.

For a fully detailed certified drawing, refer to:
GP-2000R Threaded CDY #1018
GP-2000R Flanged CDY #1019

GP-2000R S	GP-2000R Specifications											
				Maximum	Minimum			Materials				
Application	Inlet Pressure psig (barg)	Relieving Pressure psig (barg)	Spring Color	Temperature °F (°C)	Differential psig (barg)	Body	Main Valve/ Seat	Pilot Valve/ Seat	Diaphragm	Color		
	NPT 3 - 200 (.21 - 13.8)	3 - 21 (.21 - 1.4)	Yellow			Ductile Iron ASTM A536						
Steam	150 lb Flanged 3 - 185 (.21 - 13)	14 - 157 (1.0 - 11.0)	Green	450 (232)	3 (.21)*		Stainless Steel AISI 420		Stainless Steel AISI 301	Dark Gray		
	300 lb Flanged 3 - 200 (.21 - 13.8)	143 - 200 (10 - 13.8)	Brown			7.000			7			

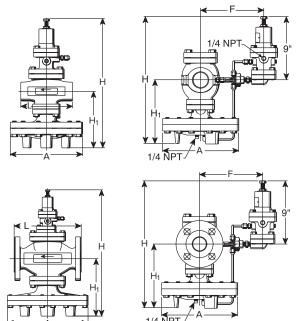
*If used for a 3-15 psig set point, outlet pressure must be 0 psig.

GP-20	oor D	imensions	5														
Siz			Face-to-Face "L"								F		ral	H Remote			
312	•	NP1	Γ	150a	#	300	#	A				H Integral		n kelliote		H ₁	
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
1/2	15	5-15/16	150	_	_	_	_	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170
3/4	20	5-15/16	150	-	-	_	_	7-15/16	200	6-7/8	176	15-3/4	398	14-1/4	362	6-3/4	170
1	25	6-5/16	160	5-3/4	147	-	_	8-15/16	226	7-1/16	179	15-15/16	404	14-7/16	367	6-15/16	175
1-1/4	32	7-1/8	180	6-1/2	166	-	_	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192
1-1/2	40	7-1/8	180	7-7/16	189	-	_	8-15/16	226	7-7/16	188	17-1/8	434	15-1/8	384	7-5/8	192
2	50	9-1/8	230	8-9/16	217	9-1/8	232	10-15/16	276	7-11/16	195	19-5/8	498	16	406	8-1/2	216
2-1/2	65	_	-	10-15/16	278	11-1/2	292	13-13/16	352	8-5/16	211	21-3/4	552	17-5/16	440	9-13/16	251
3	80	_	_	11-3/4	298	12-7/16	316	13-13/16	352	8-3/4	222	22-5/8	575	17-15/16	456	10-7/16	264
4	100	-	_	13-1/2	343	14-1/8	359	15-13/16	401	9-7/16	239	25-15/16	658	20-1/8	511	12-5/8	321
6	150	_	_	18-1/8	460	19	483	19-3/4	502	_	_	31-3/4	806	_	_	26-1/2	673

GP-2000	GP-2000R Weights													
Siz	_			Wei	ight									
Siz	e	N	PT	15	0#	30	C _v *							
in	mm	lb kg		lb	kg	lb	kg							
1/2	15	34	14	36	15	42	19	5						
3/4	20	34	14	36	15	42	19	7.2						
1	25	44	19	48	20	54	23	10.9						
1-1/4	32	51	22	53	22	59	25	14.3						
1-1/2	40	51	22	55	23	61	26	18.8						
2	50	75	33	81	36	84	38	32						
2-1/2	65	_	-	142	65	150	68	60						
3	80	_	_	155	69	166	75	78						
4	100	_	_	247	112	264	120	120						
6	150	_	_	509	231	555	253	250						

*50% reduced port available for sizes 1/2" - 4".

The C_V value should be divided by 2 to get reduced port C_V .



For capacities see page 305.

GP-2000, 2000K-1, 3 & 6, GD-2000K, GP-2000R, GP-2000CS



Capacities for Steam

	1	1			lb/l		6:				
Inlet	Outlet					Connect					
р	sig	1/2	3/4	1	1-1/4	1-1/2	2	2-1/2	3	4	(
C _V F	actor	5	7.2	10.9	14.3	18.8	32	60	78	120	25
15	8	201	290	438	575	756	1 287	2 413	3 137	4 826	10 (
	3 13	250 219	361 316	546 478	716 628	942 825	1 603 1 404	3 005 2 633	3 907 3 423	6 010 5 267	12 !
20	3	313	451	683	896	1 178	2 006	3 761	4 889	7 521	15 6
	18	236	340	515	676	889	1 513	2 837	3 688	5 673	11 8
25	3 - 5	339	489	740	971	1 276	2 172	4 073	5 295	8 146	16 9
	23	252	363	550	721	948	1 614	3 026	3 934	6 052	12 6
30	3 - 7	382	550	833	1 093	1 437	2 446	4 586	5 962	9 172	19 1
	33	281	405	613	804	1 057	1799	3 373	4 385	6 747	14 (
40	25	395	569	861	1 130	1 486	2 529	4 741	6 164	9 483	19 7
	3 - 12	468	673	1 020	1338	1758	2 993	5 612	7 296	11 224	23
	42	327	471	713	936	1 230	2 094	3 927	5 105	7 853	16 3
50	30	491	707	1 071	1405	1847	3 143	5 894	7 662	11 788	24
	3 - 17 51	553 373	797 537	1 206 814	1 582 1 067	2 080 1 403	3 540 2 389	6 638 4 479	8 630 5 823	13 276 8 958	27 (
	45	471	679	1 028	1348	1773	3 017	5 657	7 355	8 958 11 315	18 6
60	35	586	843	1 277	1675	2 202	3 748	7 027	9 135	14 053	29 2
	3 - 22	639	920	1392	1827	2 401	4 088	7 664	9 963	15 328	31 9
	63	471	678	1026	1346	1769	3 012	5 647	7 341	11 295	23 !
75	55	593	854	1 2 9 2	1 696	2 229	3 794	7 114	9 249	14 229	29 (
75	45	703	1 012	1 532	2 010	2 643	4 499	8 435	10 966	16 871	35
	4 - 30	767	1104	1672	2 193	2 884	4 908	9 203	11 964	18 406	38
	85	595	857	1298	1 703	2 239	3 811	7 145	9 289	14 291	29
100	75	751	1 081	1636	2 147	2 822	4 804	9 007	11 709	18 014	37 5
	60 5 - 42	914 981	1 316 1 412	1 992 2 138	2 614 2 805	3 436 3 687	5 849 6 276	10 967 11 768	14 257 15 299	21 934 23 536	45 (49 (
	106	739	1064	1 610	2 112	2 777	4 727	8 863	11 522	17 725	36 9
	100	837	1 206	1825	2 395	3 149	5 359	10 048	13 063	20 097	41 8
125	75	1125	1 619	2 451	3 216	4 228	7 197	13 494	17 543	26 989	56
	7 - 55	1 194	1720	2 604	3 416	4 491	7 644	14 333	18 633	28 666	59
	127	881	1 2 6 9	1922	2 521	3 314	5 641	10 577	13 751	21 155	44 (
150	100	1 241	1 787	2 705	3 549	4 666	7 943	14 893	19 360	29 785	62 (
	8 - 67	1 408	2 028	3 070	4 027	5 295	9 012	16 898	21 968	33 796	70 4
	148	1024	1 475	2 233	2 929	3 851	6 555	12 291	15 978	24 581	51
175	125 100	1 348 1 587	1 940 2 285	2 938 3 459	3 854 4 537	5 067 5 965	8 624 10 154	16 170 19 038	21 021 24 750	32 341 38 076	67 3 79 3
	9 - 80	1622	2 336	3 536	4 639	6 098	10 154	19 463	25 302	38 926	81 (
	170	1149	1655	2 506	3 287	4 322	7 356	13 792	17 930	27 585	57 4
	150	1 446	2 083	3 153	4 136	5 438	9 256	17 354	22 560	34 708	72 3
200	125	1 712	2 465	3 732	4 896	6 437	10 956	20 542	26 705	41 085	85 !
	10 - 92	1836	2 643	4 002	5 250	6 902	11 748	22 028	28 637	44 056	917
	191	1 292	1 861	2 817	3 695	4 858	8 270	15 505	20 157	31 011	64 (
225	175	1539	2 215	3 354	4 400	5 785	9 847	18 462	24 001	36 925	76 9
-	150	1829	2 633	3 986	5 230	6 876	11 703	21 944	28 527	43 887	91
	12 - 105 200	2 049 1 626	2 951 2 341	4 468 3 544	5 861 4 649	7 706 6 112	13 116 10 404	24 593 19 508	31 971 25 360	49 186 39 015	102 81.2
	175	1938	2 791	4 226	5 544	7 288	12 406	23 261	30 239	46 521	96
250	150	2 176	3 133	4 743	6 223	8 181	13 925	26 110	33 943	52 219	108
	13 - 117	2 263	3 259	4 934	6 473	8 510	14 484	27 158	35 306	54 316	113
	200	2 042	2 941	4 452	5 841	7 679	13 070	24 507	31 859	49 014	102
275	175	2 299	3 311	5 012	6 575	8 644	14 714	27 588	35 864	55 176	114 9
	14 - 130	2 477	3 567	5 400	7 084	9 313	15 852	29 723	38 640	59 446	123
000	200	2 416	3 479	5 267	6 910	9 084	15 462	28 991	37 688	57 982	120
300	175	2 637	3 797	5 748	7 540	9 913	16 874	31 638	41 130	63 277	131
	15 - 142	2 691	3 875	5 866	7 695	10 117	17 220	32 288	41 975	64 576	134
	248 225	2 656 2 886	3 825 4 156	5 791 6 292	7 597 8 254	9 987 10 852	17 000 18 471	31 864 34 629	41 423 45 017	63 728 69 258	-
350	200	3 095	4 457	6 748	8 853	11 639	19 811	37 135	48 276	74 270	_
	18 - 160	3 118	4 490	6 798	8 918	11 724	19 956	39 890	51 856	74 270 79 779	_
	248	3 702	5 331	8 071	10 588	13 921	23 695	44 415	57 740	88 830	_
425	225	3 870	5 574	8 438	11 070	14 553	24 771	46 439	60 370	92 877	-
	22 - 195	4 000	5 578	8 719	11 439	15 038	25 595	48 096	62 525	96 192	_

NOTE: Maximum pressure reduction 20:1, except for GD-2000K 10:1. Minimum pressure reduction is 85% of inlet pressure. For 50% reduced port capacities, divide the capacity by 2.

50% reduced port available for sizes 1/2" - 4".



GP-2000, 2000K-1, 3 & 6, GD-2000K, GP-2000R, GP-2000CS

Capacities for Steam continued

						/hr Connect	ion Size				
Inlet	Outlet			,	,		m				
	arg	15	20	25	32	40	50	65	80	100	1!
c _v ı	actor	5	7.2	10.9	14.3	18.8	32	60	78	120	2
1.03	0.55	91	131	199	261	343	584	1095	1 423	2 189	4
	0.21	114 100	164 143	248 217	325 285	427 374	727 637	1 363 1 194	1 772 1 553	2 726 2 389	5 4
1.38	0.90	142	205	310	407	534	910	1706	2 218	3 412	7
	1.24	107	154	234	307	403	686	1287	1673	2 573	5
1.72	.2134	154	222	336	440	579	985	1848	2 402	3 695	7 (
2.07	1.59	114	165	249	327	430	732	1 373	1784	2 745	5
2.07	.2148	173	250	378	496	652	1 109	2 080	2 704	4 161	8
	2.28	128	184	278	365	479	816	1530	1 989	3 060	63
2.76	1.72	114	165	249	327	430	732	1 373	1784	2 745	5
	.2183	173	250	378	496	652	1109	2 080	2 704	4 161	8 6
2.45	2.90	128	184	278	365	479	816	1530	1989	3 060	63
3.45	2.07 .21 - 1.17	179 212	258 305	391 462	513 607	674 798	1 147 1 358	2 151 2 546	2 796 3 309	4 301 5 091	8 10
	3.52	148	214	324	425	558	950	1 781	2 315	3 562	7
	3.52	148	214	324	425	558	950	1 781	2 315	3 562	7
4.14	2.41	223	321	486	637	838	1 426	2 673	3 475	5 347	11
	.21 - 1.5	251	361	547	718	943	1606	3 011	3 914	6 022	12
	4.34	213	307	465	611	803	1 366	2 562	3 330	5 123	10
E 47	3.79	269	387	586	769	1 011	1 721	3 227	4 195	6 454	13
5.17	3.10	319	459	695	912	1 199	2 041	3 826	4 974	7 653	15
	.27 - 2.1	348	501	758	995	1308	2 226	4 175	5 427	8 349	17
	5.86	270	389	589	772	1 016	1729	3 241	4 213	6 482	13
6.89	5.17	340	490	742	974	1280	2 179	4 086	5 311	8 171	17
0.03	4.14	415	597	904	1 186	1 559	2 653	4 975	6 467	9 949	20
	.34 - 2.9	445	641	970	1 272	1 673	2 847	5 338	6 939	10 676	22
	7.31	335	482	730	958	1260	2 144	4 020	5 226	8 040	16
8.62	6.89	380	547	828	1086	1 428	2 431	4 558	5 925	9 116	18
	5.17 .48 - 3.7	510 542	735 780	1 112 1 181	1 459 1 550	1 918 2 037	3 265 3 467	6 121	7 957 8 452	12 242 13 003	25 27
	8.76	400	576	872	1143	1503	2 559	6 502 4 798	6 237	9 596	19
10.34	6.89	563	811	1227	1 610	2 117	3 603	6 755	8 782	13 510	28
	.55 - 4.6	639	920	1392	1827	2 402	4 088	7 665	9 964	15 330	31
	10.20	465	669	1 013	1329	1 747	2 973	5 575	7 247	11 150	23
10.07	8.62	611	880	1332	1 748	2 298	3 912	7 335	9 535	14 670	30
12.07	6.89	720	1 036	1 569	2 058	2 706	4 606	8 636	11 226	17 271	35
	.62 - 5.5	736	1059	1 604	2 104	2 766	4 709	8 828	11 477	17 657	36
	11.72	521	751	1 137	1 491	1 960	3 337	6 256	8 133	12 512	26
13.79	10.34	656	945	1 430	1 876	2 466	4 198	7 872	10 233	15 744	32
-	8.62	776	1 118	1693	2 221	2 920	4 970	9 318	12 113	18 636	38
	.68 - 6.3	833	1 199	1 815	2 381	3 131	5 329	9 992	12 990	19 984	41
	13.17 12.07	586 698	844 1 005	1 278 1 521	1 676 1 996	2 204 2 624	3 751 4 466	7 033 8 374	9 143 10 887	14 066 16 749	29 34
15.51	10.34	829	1 194	1808	2 372	3 119	5 309	9 954	12 940	19 907	34 41
	.82 - 7.24	930	1339	2 027	2 659	3 495	5 950	11 155	14 502	22 311	46
	13.79	737	1062	1607	2 109	2 773	4 719	8 849	11 503	17 697	36
1704	12.07	879	1266	1 917	2 515	3 306	5 627	10 551	13 716	21 102	43
17.24	10.34	987	1 421	2 152	2 823	3 711	6 316	11 843	15 396	23 687	49
	.89 - 8.06	1 027	1 478	2 238	2 936	3 860	6 570	12 319	16 015	24 638	51
	13.79	926	1 334	2 019	2 649	3 483	5 929	11 116	14 451	22 233	46
18.96	12.07	1043	1 502	2 273	2 982	3 921	6 674	12 514	16 268	25 028	52
	.96 - 8.96	1124	1 618	2 449	3 213	4 224	7 191	13 482	17 527	26 965	56
0000	13.79	1096	1578	2 389	3 134	4 120	7 013	13 150	17 095	26 300	54
20.00	12.07	1196	1722	2 607	3 420	4 497	7 654	14 351	18 656	28 702	59
	1.03 - 9.79	1220	1758	2 661	3 491	4 589	7 811	14 646	19 040	29 292	61
	17.10	1205	1735	2 627	3 446	4 530	7 711	14 453	18 789	28 907	
24.13	15.51 13.79	1 309 1 404	1 885 2 022	2 854 3 061	3 744 4 016	4 922 5 279	8 379 8 986	14 668 16 844	20 419 21 898	31 415 33 689	
	1.24 - 11.02	1 404	2 022	3 061	4 016	5 279	9 052	18 094	23 521	33 689 36 187	
	17.10	1679	2 418	3 661	4 803	6 314	10 748	20 146	26 190	40 293	
29.30	15.51	1756	2 528	3 827	5 021	6 601	11 236	21 064	27 383	40 293	
_5.50	1.52 - 13.4	1 814	2 530	3 955	5 189	6 821	11 610	21 816	28 361	43 632	

 $NOTE: Maximum\ pressure\ reduction\ 20:1,\ except\ for\ GD-2000K\ 10:1.\ Minimum\ pressure\ reduction\ is\ 85\%\ of\ inlet\ pressure.$

For 50% reduced port capacities, divide the capacity by 2.

50% reduced port available for sizes 15 - 100 mm.

GP-2000 On/Off—For Steam Service

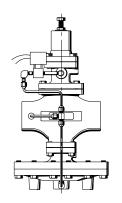


External Pilot Solenoid Operated Valves

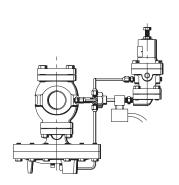
The GP-2000 On/Off option allows for remote shutoff of pressure reducing valves. Automatic shutoff during power failures and shutoff based on set points of pressure, temperature or liquid levels of process fluids. This option is available as an accessory item or may be factory installed on any of the GP-2000 Series valves. The GP-2000 On/Off is designed for a maximum pressure of 150 psig and a maximum temperature of 366°F NEMA IV standard, coil: class H 110V standard. Available with normally open or normally closed solenoids.

Non-Electric Gradient Monitoring Option (Between Water and Steam Pressure)

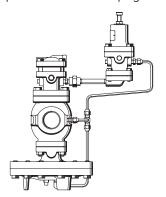
The GP-2000W1P provides a safe and dependable shutdown of steam when the water pressure falls or drops rapidly on a constant pressure, steam-to-water exchanger. Unlike a solenoid option that shuts the steam down when the water pressure drops below a pre-set point, the GP-2000W1P always maintains a constant steam pressure until water pressure drops to within 3 psig above the steam pressure. Lower water pressure will cause the steam pressure to fall, thereby maintaining a minimum 3 psig difference. This will allow the exchanger to produce hot water even when water pressure is low, and ensures that steam pressure will stay functional as long as water pressure is above 15 psig.



GP-2000, GP-2000CS, GP-2000R with On/Off



GP-2000 Remote Mount with On/Off



GP-2000W1P

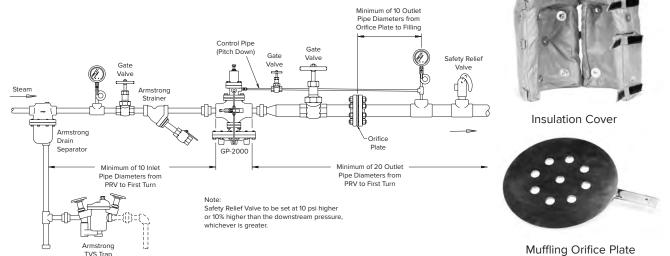
Noise Treatment

OSHA has established limits on the length of time any employee may be exposed to various sound levels. A sound level of 85 Dba or less is the acceptable standard for noise levels through a PRV in most applications. Certain facilities may require much less. Please consult Armstrong PRV Sizing Software or contact the local Armstrong factory representative for Dba levels for each application.

For Dba levels above 85 you can offer a 2" thick insulation cover for thermal conductivity and noise attenuation, a muffling orifice plate to reduce the noise through the PRV, or a combination of both.

A muffling orifice plate consists of a 1/4" thick stainless steel plate installed between mating ANSI flanges. The orifice plate is installed in the enlarged piping downstream of the pressure regulator. Each orifice plate is engineered for specific applications to maximize noise reduction without reducing regulator capacity.

Orifice plates for GP-2000 only.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Armstrong [®]	Notes

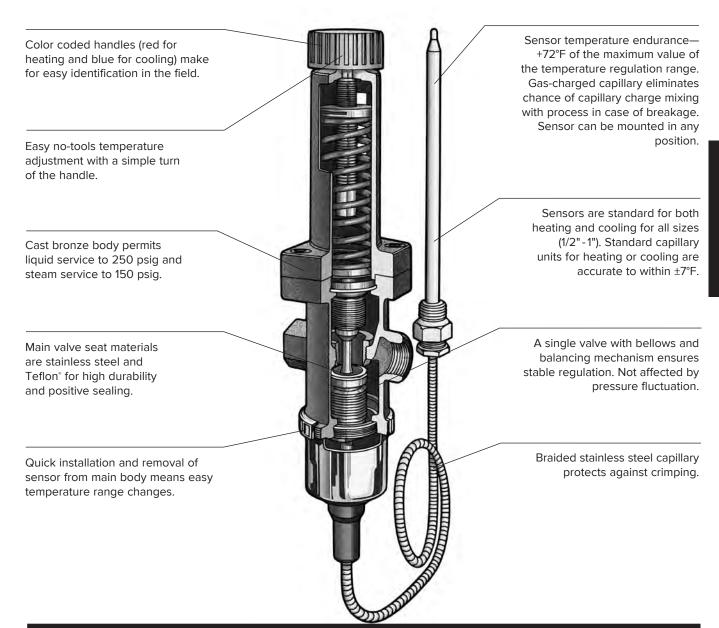
Temperature Regulators



For Steam, Water and Non-Corrosive Liquid Service

Armstrong self-actuated temperature regulators are compact, high performance units that are simple in design and operation—and suitable for a wide variety of applications.

Features including flexible mounting positions of the sensor, interchangeable capillaries and varied temperature ranges make installation, adjustment and maintenance quick and easy.



Temperature	Regulator Valve Se	election					
If the Service Is	If Inlet Pressure is psig (barg)	Type of Control	Temperature Ratings °F (°C)	Temperature Accuracy °F (°C)	If Maximum Capacity Is Less Than	Look for Model	Find on Page
	5 to 150 (.34 to 10)	Self Contained Direct Acting	From 32 to 302 (0 to 150) 5 Ranges	±7 (±3) From set point	1 745 (792)	OB-30	304
Heating	5 to 15 (.34 to 1)	Self Contained	From 18 to 361	±2 (±1)	5 643 (2 565)	OB-2000L	308
	10 to 300	Pilot Operated	(-/ to 183)	From set point	F0 022 /2C 222\	OB-2000	306
	(.69 to 20		· ·		58 032 (26 323)	OB-2000PT	310
Cooling	5 to 250 (.34 to 17)	Self Contained Reverse Acting	From 32 to 302 (0 to 150) 5 Ranges	±7 (±3) From set point	70 gpm (308 m3/hr)	OB-31	304



For Steam, Air and Non-Corrosive Liquids

The Armstrong OB-30/31 is a direct acting temperature regulator that requires no external source for operation. Simple and compact, the unit is suitable for a wide variety of heating/cooling applications. Installing, adjusting or maintaining the OB-30/31 is quick and easy because interchangeable capillaries mount in any position and disconnect by simply loosening the union nut. No stem

packing so there's no leakage. Single composition seat for tight shutoff. The OB-30/31 comes in 1/2", 3/4" or 1" sizes and is available with a choice of five temperature ranges and three capillary lengths.

For a fully detailed certified drawing, refer to CDY #1036.

OB-30/31	OB-30/31 Specifications													
Model	Application	Service	Max. Inlet Pressure psig (barg)	Maximum Diff. psig (barg)	Temperature Ranges °F (°C)	Max. Temp. °F (°C)	Temperature Accuracy °F (°C)	Capillary Lengths feet (meters)						
OB-30	Heating	Steam, Water	Steam 150 (10)	140	32 - 95 (0 - 35) 77 - 158 (25 - 70)	366	±7 (±3)	*6-1/2 (2)						
OB-31	Cooling	Water, Non- Corrosive Liquids	Liquid 250 (17)	(9.6)	104 - 212 (40 - 100) 140 - 266 (60 - 130) 158 - 302 (70 - 150)	(185)	From Set Point	9-1/2 (3) 16-1/2 (5)						

^{*}Standard length.

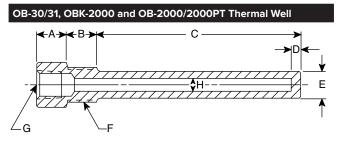
NOTES: Capillary can withstand a maximum of 72°F (40°C) above rated range. If desired set temperature is in temperature range overlap, select lower range.

OB-30/31 Materials					
Body Material	Seat Type & Material	Valve Material	Capillary Material	Bulb Material	Thermal Well Material
Bronze ASTM B584	Single Seat 304 Stainless Steel	Teflon	304 Stainless Steel Armor Shielded Capillary	Copper-Nickel Plated	*304 Stainless Steel or Brass

^{*}Other materials available upon request.

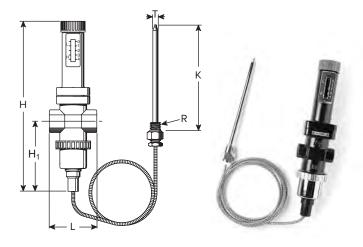
OB-30/31 Dimensions and Weights																
Si	ze	L		H ₁		н		Т		К		R		Weight		
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	CV
1/2	15	3	80	5-1/8	130	12-1/2	315	3/8	10	8	200	1/2	15	6	2.8	3.7
3/4	20	3-1/8	85	5-1/8	130	12-1/2	315	3/8	10	8	200	1/2	15	6	2.8	4.6
1	25	3-1/2	95	5-1/8	130	12-1/2	315	3/8	10	8	200	1/2	15	6-1/2	3.0	5.8

Thermal Well Dimens	Thermal Well Dimensions															
Maralal	Α		E	В		C D)	E		F		G		Н	
Model	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
OB-30/31	3/4	20	1	25	7-1/2	204	1/4	7	.765	20	3/4	20	1/2	15	.380	10
OB-2000/2000PT	1	25	3/4	20	7-3/4	197	1/4	7	.89	23	1	25	3/4	20	.630	16
OBK-2000	1	25	3/4	20	12-1/2	318	1/4	7	.765	20	3/4	20	1/2	15	.515	13



Standard Material: 304 stainless steel or brass. Other materials available upon request.

NOTE: When inserting sensor into thermal well, for best results, it is recommended that heat transfer medium be applied to sensor before installation.





OB-3	0 Capa	cities	Steam						
000	о опри	lb/hr	oteam				kg/hr		
			nection	Size				ection	Size
Inlet	Outlet	COIII	in	JIZC	Inlet	Outlet	Com	mm	J12C
n	sig	1/2	3/4	1	ŀ	arg	15	20	25
	actors	3.7	4.6	5.8		actors	3.7	4.6	5.8
- 0	3	67	83	105		.20	30	38	48
5	2	81	100	127	.35	.14	37	45	58
	0	101	126	159		0	46	57	72
	8	75	94	118		.55	34	43	54
10	6	104	130	164	.7	.41	47	59	75
10	4	125	155	196	./	.28	57	70	89
	0	154	191	241		0	70	87	110
	12	101	125	158		.83	46	57	72
15	9	139	172	218	1.0	.62	63	78	99
13	6	165	205	259	1.0	.41	75	93	118
	0-5	200	249	314		035	91	113	143
	15	139	173	218		1.0	63	79	99
20	10	181	235	296	1.38	.7	82	107	135
20	5	221	275	347	1.50	.35	100	125	158
	0-2	234	290	367		014	106	132	167
	20	149	186	234		1.38	68	85	106
25	15	204	254	320	1.72	1.0	93	115	145
	10	241	300	378	"" =	.7	110	136	172
	0-5	268	333	420		035	122	151	191
	25	159	198	250		1.72	72	90	114
30	15	258	322	406	2.0	1.0	117	146	185
	0-7	302	375	473		048	137	170	215
40	30	244	304	384	276	2.0	111	138	175
40	20	328	408	515	2.76	1.38	149	185	234
	0-12 40	369	459	579 420	-	083	168 122	209 151	263
50	30	268 383	333 451	569	3.45	2.76 2.0	174	205	191 259
50	0-17	437	543	685	3.43	0-1.2	199	247	311
	50	290	360	454		3.45	132	164	206
60	40	395	491	619	4.0	2.76	180	223	281
00	0-22	504	627	791	1 4.0	0-1.5	229	285	360
	60	310	385	486		4.0	141	175	221
	50	328	424	665		3.45	149	193	302
70	40	502	624	787	4.83	2.76	228	284	358
	0-27	572	711	897		0-1.9	260	323	408
	70	329	409	616		4.83	150	186	280
0.0	60	452	562	708		4.0	205	255	322
80	50	537	668	842	5.52	3.45	244	304	383
	0-32	640	795	1 003		0-2.2	291	361	456
	80	346	431	543		5.52	157	196	247
	70	478	694	749		4.83	217	315	340
90	60	570	708	893	6.0	4.0	259	322	406
	50	639	795	1002		3.45	290	361	455
	0-37	707	879	1109		0-2.6	321	400	504
	90	363	452	570		6.0	165	205	259
	80	502	625	788		5.52	228	284	358
100	70	600	747	942	6.9	4.83	273	340	428
	60	676	840	1060		4.0	307	382	482
	0-42	776	963	1 215		0-2.9	353	438	552
	110	489	608	767		7.59	222	276	349
	100	619	770	971		6.9	281	350	441
125	80	798	992	1250	8.62	5.52	363	451	568
	70	863	1073	1353		4.83	392	488	615
	0-55	944	1 174	1480		0-3.8	429	534	673
	130	611	759	958		8.97	278	345	435
150	120	736	915	1154	10.0	8.28	335	416	525
	100	918	1 141	1439		6.9	417	519	654
	0-63	1 113	1384	1745		0-4.3	506	629	793

NOTE: Where it is not possible to calculate pressure drop, 35%

Temperature Regulator Selection Example Parameters:

Fluid	Steam
Maximum inlet pressure	100 psig
Outlet pressure	90 psig
Maximum flow rate	500 lbs/hr
Temperature required	150°F
Distance from regulator to sensing point	5'

To Locate Proper Model:

•	
Enter inlet column at	100 psig
Move to outlet pressure of	90 psig
Locate capacity of 570 lbs/hr under	
connection size	1"
Find capillary temperature range	77-158°F
Select capillary length	

Application Will Require:

OB-30, 1" with 77-158°F Temp. Range, Capillary Length 6-1/2'

OB-30/	31 Capa	cities—V	Vater						
	gr	om			nin				
ΔΡ	Con	nection	Size	ΔР	Con	nection	n Size		
		in		ΔΡ		mm			
psig	1/2	3/4	1	barg	15	20	25		
5	8.1	10.1	12.3	.35	30	38	47		
10	11.9	14.3	18.5	.70	45	55	70		
15	14.3	17.6	22.0	1.00	55	67	83		
20	16.7	20.7	26.4	1.40	63	78	100		
25	18.5	22.0	28.2	1.80	70	83	107		
30	20.3	25.6	31.7	2.00	77	97	120		
50	26.4	33.5	41.4	3.50	100	127	157		
75	32.6	39.6	49.3	5.20	123	150	187		
100	37.9	46.2	57.2	7.00	143	175	217		
125	42.2	52.0	65.6	8.70	160	197	248		
150	46.3	57.25	70.5	10.00	175	217	267		

Capillary Temperature Ranges								
Temperature Ranges °F (°C)								
32 - 95 (0 - 35)								
77 - 158 (25 - 70)								
104 - 212 (40 - 100)								
140 - 266 (60 - 130)								
158 - 302 (70 - 150)								

NOTE: If desired set temperature is in temperature range overlap, select lower range.

⁻ 40% of gauge supply pressure can be used as a reasonable approximation.



Armstrong's OB-2000 is a high performance externally piloted temperature regulator for large capacity applications such as heat exchangers, steam coils, steam dryers, plating tanks and parts washers. It is self-actuated and requires no external energy source. Capillary units mount in any position and can be easily disconnected and interchanged, offering

easy installation and maximum application flexibility. Available in sizes 1/2" through 6" with six temperature ranges and three capillary lengths.

For a fully detailed certified drawing, refer to CDY #1013.

OB-2000L Specification	is				
Application	Inlet Pressure psig (barg)	Reduced Pressure psig (barg)	Temperature Ranges °F (°C)	Temperature Accuracy °F (°C)	Capillary Lengths feet (meters)
Steam	NPT 10 - 300 (.69 - 20) 150 lb Flanged 10 - 185 (.69 - 13 300 lb Flanged 10 - 300 (.69 - 20)	7 (.48)	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	±2 (±1) From Set Point	*6-1/2 (2) 9-1/2 (3) 16-1/2 (5)

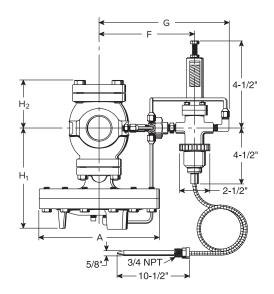
^{*}Standard length.

Note: If desired set temperature is in temperature range overlap, select lower range.

Si				Face-to-	Face					H ₂		A F		G		Weight								
31.	že	NP.	Т	150	#	300	#	H ₁		П2		A				G		NI	PT	15	0#	30	0#	c _v
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	1
1/2	15	5-15/16	150	_	_	_	_	6-3/4	170	2-15/16	74	7-15/16	200	6-5/8	169	8-3/4	222	31	15	33	15	39	18	5.0
3/4	20	5-15/16	150	_	_	_	_	6-3/4	170	2-15/16	74	7-15/16	200	6-5/8	169	8-3/4	222	31	15	33	15	39	18	7.2
1	25	6-15/16	160	5-3/4	147	_	_	6-15/16	175	3-1/16	76	8-15/16	226	6-7/8	174	8-7/8	226	39	19	41	20	47	21	10.9
1-1/4	32	7-1/8	180	6-1/2	166	_	_	7-5/8	192	3-9/16	90	8-5/16	226	7-1/8	182	9-1/4	235	47	22	49	23	54	24	14.3
1-1/2	40	7-1/8	180	7-7/16	189	_	_	7-5/8	192	3-9/16	90	8-15/16	226	7-1/8	182	9-1/4	235	47	22	49	23	54	24	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	8-1/2	216	4-1/16	103	10-15/16	276	7-7/16	189	9-1/2	242	71	33	77	36	78	36	32
2-1/2	65	_	_	10-15/16	278	11-1/2	292	9-13/16	251	4-7/8	122	13-13/16	352	8-1/8	206	10-1/8	259	_	_	138	63	140	64	60
3	80	_	_	11-3/4	298	12-7/16	315	10-7/16	264	5-3/8	135	13-13/16	352	8-9/16	217	10-5/8	270	_	_	149	69	155	71	78
4	100	_	_	13-1/2	343	14-1/8	359	12-5/8	321	6-9/16	167	15-13/16	401	9-1/4	234	11-1/4	287	_	_	234	107	243	110	120

NOTE: For 6" (150 mm) consult factory.

 $^{^*50\%}$ reduced port available for sizes 1/2" - 4". The C $_{
m v}$ value should be divided by 2 to get reduced port C $_{
m v}$.







OB-2000 Sensor and	OB-2000 Sensor and Accessory Specifications												
Capillary Material	Capillary Temperature Ranges °F (°C)	Bulb Material	Bulb Connection	Thermal Well Material	Thermal Well Connection								
Copper Capillary Tube With 304 Stainless Steel Armor Shield	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	Nickel Plated Copper Bulb	3/4" (20 mm) NPT	Brass* 304 Stainless Steel*	1" (25 mm) NPT								

*Standard. Other material available upon request. See page 310 for dimensions of well.

NOTE: Capillary can withstand a maximum of 36°F (20°C) above rated range.

NOTE: If desired set temperature is in temperature range overlap, select lower range.

OB-2000 Materials					
OB-2000	Body Material	Seat Type & Material	Valve Material	Connection	Maximum Temperature °F (°C)
Main Valve	Ductile Iron ASTM A536	Single Seat Stainless Steel	Stainless Steel AISI 420	NPT 150 lb Flanged 300 lb Flanged	450 (232)
Temperature Pilot Valve	Bronze ASTM B584	AISI 420		1/4" (6 mm) NPT]

Valve Sizing
Proper valve selection requires the following information
Steam capacity required for application
Supply pressure of steam
Allowable pressure drop across valve*

 $^{^{*}}$ Where it is not possible to calculate pressure drop, 35% - 40% of gauge supply pressure can be used as a reasonable approximation.

Temperature Regulator Selection Example Parameters:

Fluid	Steam
Maximum inlet pressure	.100 psig
Outlet pressure	75 psig
Maximum flow rate15	00 lbs/hr
Temperature required	180°F
Distance from regulator to sensing point	5'

Application Will Require:

OB-2000, 1" with 131-201°F Temp. Range, Capillary Length 6-1/2'



Armstrong's OB-2000L is a high performance externally piloted temperature regulator for large capacity and low pressure applications. It is self-actuated and requires no external energy source. Capillary units mount in any position and can be easily disconnected and interchanged, offering easy installation and maximum application flexibility.

Available in sizes 1/2" through 4" with six temperature ranges and three capillary lengths.

For a fully detailed certified drawing, refer to CDY #2232.

OB-2000L Specification	s				
Application	Inlet Pressure psig (barg)	Reduced Pressure psig (barg)	Temperature Ranges °F (°C)	Temperature Accuracy °F (°C)	Capillary Lengths feet (meters)
Steam	5 - 15 (.3 - 1)	3 (.21)	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	±2 (±1) From Set Point	*6-1/2 (2) 9-1/2 (3) 16-1/2 (5)

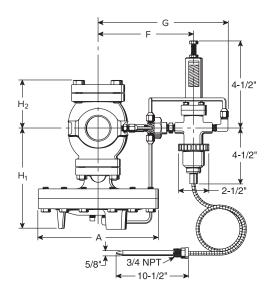
^{*}Standard length.

Note: If desired set temperature is in temperature range overlap, select lower range.

OB-2	20001	Dimens	ions a	nd Weigh	nts															
Siz		F	ace-to-	Face "L"		ш		ш		А		_		G			We	ight		
314	ze	NP1	Г	150#	#	H ₁		H ₂	!	A				G		NI	PT	15	0#	c _v
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	
1/2	15	5-15/16	150	_	_	6-3/4	170	2-15/16	74	7-15/16	200	6-5/8	169	8-3/4	222	31	15	33	15	6.5
3/4	20	5-15/16	150	_	_	6-3/4	170	2-15/16	74	7-15/16	200	6-5/8	169	8-3/4	222	31	15	33	15	9
1	25	6-5/16	160	5-3/4	147	6-15/16	175	3-1/16	76	8-15/16	226	6-7/8	174	8-7/8	226	39	19	41	20	12
1-1/4	32	7-1/8	180	6-1/2	166	7-5/8	192	3-9/16	90	8-15/16	226	7-1/8	182	9-1/4	235	47	22	49	23	19
1-1/2	40	7-1/8	180	7-7/16	189	7-5/8	192	3-9/16	90	8-15/16	226	7-1/8	182	9-1/4	235	47	22	49	23	22
2	50	9-1/8	230	8-9/16	217	8-1/2	216	4-1/16	103	10-15/16	276	7-7/16	189	9-1/2	242	71	33	77	36	38
2-1/2	65	_	_	10-15/16	278	9-13/16	251	4-7/8	122	13-13/16	352	8-1/8	206	10-1/8	259	_	_	138	63	66
3	80	ı	_	11-3/4	298	10-7/16	264	5-3/8	135	13-13/16	352	8-9/16	217	10-5/8	270	_	_	149	69	78
4	100		_	13-1/2	343	12-5/8	321	6-9/16	167	15-13/16	401	9-1/4	234	11-1/4	287		_	234	107	116

^{*50%} reduced port available for sizes 1/2" - 4". The C_v value should be divided by 2 to get reduced port C_v .

For capacities see page 315.







OB-2000L Sensor ar	nd Accessory Specificatio	ns			
Capillary Material	Capillary Temperature Ranges °F (°C)	Bulb Material	Bulb Connection	Thermal Well Material	Thermal Well Connection
Copper Capillary Tube With 304 Stainless Steel Armor Shield	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	Nickel Plated Copper Bulb	3/4" (20 mm) NPT	Brass* 304 Stainless Steel*	1" (25 mm) NPT

^{*}Standard. Other material available upon request. See page 310 for dimensions of well.

NOTE: Capillary can withstand a maximum of 36°F (20°C) above rated range.

NOTE: If desired set temperature is in temperature range overlap, select lower range.

OB-2000L Materials					
OB-2000	Body Material	Seat Type & Material	Valve Material	Connection	Maximum Temperature °F (°C)
Main Valve	Ductile Iron ASTM A536	Single Seat Stainless Steel	Stainless Steel	NPT 150 lb Flanged 300 lb Flanged	450 (232)
Temperature Pilot Valve	Bronze ASTM B584	AISI 420	AISI 420	1/4" (6 mm) NPT	

GP-2000L, OB-2000L

Capacities for Steam Service

					lb/h	r										kg/h	r				
l-al-at	041-4				Co	nnecti	on Size	e			Inlat	041-4				Cor	nnecti	on Siz	:e		
iniet	Outlet					in	1				Inlet	Outlet					mr	n			
р	sig	1/2	3/4	1	1-1/4	1-1/2	2	2-1/2	3	4	b	arg	15	20	25	32	40	50	65	80	100
5	2	218	277	316	495	594	1100	1782	1 881	3 135	0.34	0.14	99	126	143	225	269	499	808	853	1422
10	7 3	161 356	223 435	297 475	471 812	545 920	942 1 518	1 635 2 574	1 933 2 772	2 874 4 598	0.69	0.48 0.21	73 161	101 197	135 215	214 368	247 417	427 689	742 1 168	877 1 257	1304 2 086
15	12 8 3	178 261 416	246 362 482	328 483 594	519 764 970	601 885 1 168		1 803 2 654 3 069		3 169 4 665 5 643	1.03	0.83 0.55 0.21	81 119 189	112 164 219	149 219 269	235 347 440	273 401 530	471 693 768	818 1 204 1 392	966 1423 1527	1 437 2 116 2 560

Note: For reduced port capacity, please divide capacity by 2.



For Steam Service

The OB-2000PT is a diaphragm-operated externally piloted pressure/temperature combination regulator. It is used in applications where maximum pressure should be limited and the temperature of the heated medium is controlled using a single seated main valve. Temperature pilot and capillary unit disconnect, making repairs or temperature range changes

quick and easy. Available in sizes 1/2" through 6" and with a choice of four spring ranges, six temperature ranges and three capillary lengths.

For a fully detailed certified drawing, refer to CDY #1006.

OB-2000PT	Specifications					
Application	Inlet Pressure psig (barg)	Minimum Differ. Pressure psig (barg)	Reduced Pressure & Spring Color psig (barg)	Temperature Ranges °F (°C)	Temperature Accuracy °F (°C)	Capillary Lengths feet (meters)
Steam	NPT 15 - 300 (1 - 20) 150 lb Flanged 15 - 185 (1 - 13) 300 lb Flanged 15 - 300 (1 - 20)	7 (.48)	1.5 - 3 (.1021) Yellow 3 - 21 (.21 - 1.4) Yellow 15 - 200 (1.0 - 13.8) Green	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	±2 (±1) From Set Point	6-1/2 (2)* 9-1/2 (3) 16-1/2 (5)

*Standard length.

OB-2000PT Sensor and Acc	cessory Specifications				
Capillary Material	Capillary Temperature Ranges °F (°C)	Bulb Material	Bulb Connection	Thermal Well Material	Thermal Well Connection
Copper Capillary Tube With 304 Stainless Steel Armor Shield	18 - 59 (-8 - 15) 50 - 97 (10 - 36) 86 - 144 (30 - 62) 131 - 201 (55 - 94) 176 - 260 (80 - 127) 239 - 361 (115 - 183)	Nickel Plated Copper Bulb	3/4" (20 mm) NPT	Brass* 304 Stainless Steel*	1" (25 mm) NPT

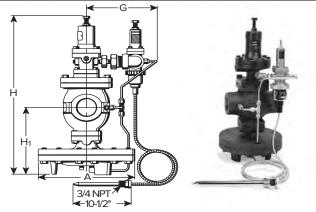
 * Standard. Other material available upon request. See page 310 for dimensions of well.

NOTES: Capillary can withstand a maximum of 36°F (20°C) above rated range. If desired set temperature is in temperature range overlap, select lower range.

00-2	3001	1 Dillici	1310113	and Wei	girts																	
Siz				Face-to-	Face			н						٥				Wei	ghts			
312	e	NPT	г	150#	•	300	*			H ₁		А			,	NI	PT	15	0#	30	0#	c _v
in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg	
1/2	15	5-15/16	150	_	_	_	_	15-3/4	398	6-3/4	170	7-15/16	200	6-1/2	166	47	22	49	23	55	25	5.0
3/4	20	5-15/16	150	_	_	_	_	15-3/4	398	6-3/4	170	7-15/16	200	6-1/2	166	47	22	49	23	55	25	7.2
1	25	6-15/16	160	5-3/4	147	_	_	15-15/16	404	6-15/16	175	8-15/16	226	7	178	57	26	59	28	64	29	10.9
1-1/4	32	7-1/8	180	6-1/2	166	_	_	17-1/8	434	7-5/8	192	8-15/16	226	7-1/4	185	67	31	69	31	74	34	14.3
1-1/2	40	7-1/8	180	7-7/16	189	_	_	17-1/8	434	7-5/8	192	8-15/16	226	7-1/4	185	67	31	69	31	75	34	18.8
2	50	9-1/8	230	8-9/16	217	9-1/8	232	19-5/8	498	8-1/2	216	10-15/16	276	6-1/2	166	89	41	94	43	100	46	32
2-1/2	65	-	-	10-15/16	278	11-1/2	292	21-3/4	552	9-13/16	251	13-13/16	352	6-1/2	166	_	_	158	72	167	76	60
3	80	_	_	11-3/4	298	12-7/16	315	22-5/8	575	10-7/16	264	13-13/16	352	6-1/2	166	_	_	171	78	183	83	78
4	100	_	_	13-1/2	343	14-1/8	359	25-15/16	658	12-5/8	321	15-13/16	401	6-1/2	166	_	_	263	120	281	128	120

Note: For 6" (150 mm) consult factory.

OB-2000PT Ma	terials		
OB-2000PT	Body Material	Valve & Seat Material	Maximum Temperature °F (°C)
Main Valve	Ductile Iron ASTM A536		
Temperature Pilot Valve	Bronze ASTM B584	Stainless Steel AISI 420	450 (232)
Pressure Pilot	Ductile Iron ASTM A536		



OB-2000, OB-2000PT



Capacities for Steam Service

3-2000	, OB-2000P	T Capacitie	s—Steam								
					II	o/hr					
Inlet	Outlet					Connec	ion Size				
	Junet		1			1	n	1		1	
	sig	1/2	3/4	1	1-1/4	1-1/2	2	2-1/2	3	4	6
	actor	5	7.2	10.9	14.3	18.8	32	60	78	120	250
10*	0 - 3	211	304	460	604	794	1352	2 534	3 294	5 068	10 55
15	8 0 - 3	201 250	290 361	438 546	575 716	756 942	1 287 1 603	2 413 3 005	3 137 3 907	4 826 6 010	10 05 12 52
	13	219	316	478	628	825	1404	2 633	3 423	5 267	10 97
20	0 - 3	313	451	683	896	1178	2 006	3 761	4 889	7 521	15 66
25	18	236	340	515	676	889	1 513	2 837	3 688	5 673	11 81
25	0 - 5	339	489	740	971	1 276	2 172	4 073	5 295	8 146	16 97
30	23	252	363	550	721	948	1 614	3 026	3 934	6 052	12 60
	0 - 7	382	550	833	1 093	1 437	2 446	4 586	5 962	9 172	19 10
40	33 25	281 395	405 569	613 861	804 1 130	1 057 1 486	1799 2 529	3 373 4 741	4 385 6 164	6 747 9 483	14 05 19 75
40	0 - 12	468	673	1020	1338	1758	2 993	5 612	7 296	11 224	23 38
	42	327	471	713	936	1230	2 094	3 927	5 105	7 853	16 36
50	30	491	707	1 071	1 405	1847	3 143	5 894	7 662	11 788	24 55
	0 - 17	553	797	1206	1 582	2 080	3 540	6 638	8 630	13 276	27 65
	51	373	537	814	1 067	1 403	2 389	4 479	5 823	8 958	18 66
60	45	471	679	1028	1348	1773	3 017	5 657	7 355	11 315	23 57
	35 0 - 22	586 639	843 920	1 277 1 392	1 675 1 827	2 202	3 748 4 088	7 027 7 664	9 135 9 963	14 053 15 328	29 27
	63	471	678	1026	1346	2 401 1 769	3 012	5 647	7 341	11 295	31 93 23 53
	55	593	854	1292	1696	2 229	3 794	7 114	9 249	14 229	29 64
75	45	703	1 012	1532	2 010	2 643	4 499	8 435	10 966	16 871	35 14
	0 - 30	767	1104	1 672	2 193	2 884	4 908	9 203	11 964	18 406	38 34
	85	595	857	1298	1703	2 239	3 811	7 145	9 289	14 291	29 77
100	75	751	1 081	1636	2 147	2 822	4 804	9 007	11 709	18 014	37 52
	60 0 - 42	914 981	1 316 1 412	1 992 2 138	2 614 2 805	3 436 3 687	5 849 6 276	10 967 11 768	14 257 15 299	21 934	45 69 49 03
	106	739	1064	1 610	2 112	2 777	4 727	8 863	11 522	23 536 17 725	36 92
	100	837	1206	1825	2 395	3 149	5 359	10 048	13 063	20 097	41 86
125	75	1 125	1 619	2 451	3 216	4 228	7 197	13 494	17 543	26 989	56 22
	0 - 55	1 194	1720	2 604	3 416	4 491	7 644	14 333	18 633	28 666	59 72
	127	881	1 269	1922	2 521	3 314	5 641	10 577	13 751	21 155	44 07
150	100	1 241	1 787	2 705	3 549	4 666	7 943	14 893	19 360	29 785	62 05
	0 - 67	1408	2 028	3 070	4 027	5 295	9 012	16 898	21 968	33 796	70 40
	148 125	1 024 1 348	1 475 1 940	2 233 2 938	2 929 3 854	3 851 5 067	6 555 8 624	12 291 16 170	15 978 21 021	24 581 32 341	51 2° 67 37
175	100	1548	2 285	3 459	4 537	5 965	10 154	19 038	24 750	38 076	79 32
	0 - 80	1622	2 336	3 536	4 639	6 098	10 380	19 463	25 302	38 926	81 09
	170	1 149	1655	2 506	3 287	4 322	7 356	13 792	17 930	27 585	57 46
200	150	1 446	2 083	3 153	4 136	5 438	9 256	17 354	22 560	34 708	72 30
200	125	1 712	2 465	3 732	4 896	6 437	10 956	20 542	26 705	41 085	85 59
	0 - 92	1836	2 643	4 002	5 250	6 902	11 748	22 028	28 637	44 056	91 78
	191 175	1 292 1 539	1 861 2 215	2 817 3 354	3 695 4 400	4 858 5 785	8 270 9 847	15 505 18 462	20 157 24 001	31 011 36 925	64 60 76 92
225	150	1829	2 633	3 986	5 230	6 876	11 703	21 944	28 527	43 887	91 43
	0 - 105	2 049	2 951	4 468	5 861	7 706	13 116	24 593	31 971	49 186	102 4
	200	1626	2 341	3 544	4 649	6 112	10 404	19 508	25 360	39 015	81 28
250	175	1938	2 791	4 226	5 544	7 288	12 406	23 261	30 239	46 521	96 9 ⁴
250	150	2 176	3 133	4 743	6 223	8 181	13 925	26 110	33 943	52 219	108 7
	0 - 117	2 263	3 259	4 934	6 473	8 510	14 484	27 158	35 306	54 316	113 15
275	200	2 042	2 941	4 452	5 841	7 679	13 070	24 507	31 859	49 014	102 1
275	175	2 299	3 311	5 012	6 575	8 644	14 714	27 588	35 864	55 176	114 95
	0 - 130 200	2 477 2 416	3 567 3 479	5 400 5 267	7 084 6 910	9 313 9 084	15 852 15 462	29 723 28 991	38 640 37 688	59 446 57 982	123 8 120 7
300	175	2 637	3 797	5 748	7 540	9 084	16 874	31 638	41 130	63 277	131 82
	0 - 142	2 691	3 875	5 866	7 695	10 117	17 220	32 288	41 975	64 576	134 53

 $^{^*}$ Minimum inlet pressure for OB-2000PT is 15 psig (1 barg) because of the pressure pilot.



Armstrong[®] OB-2000, OB-2000PT

Capacities for Steam Service

	, 00 2000	PT Capacitie	3—Steam		l.	g/hr					
					K	Connect	ion Sizo				
Inlet	Outlet					m					
b.)	15	20	25	32	40	50	65	80	100	150
	arg									 	
	actor	5	7.2	10.9	14.3	18.8	32	60	78	120	250
0.69*	021 0.55	96 91	138 131	209 199	274 261	360 343	613 584	1 150 1 095	1 494 1 423	2 299 2 189	4 79 4 56
1.03	0.33	114	164	248	325	427	727	1363	1772	2 726	5 67
	0.90	100	143	217	285	374	637	1 194	1553	2 389	4 97
1.38	021	142	205	310	407	534	910	1706	2 218	3 412	7 10
470	1.24	107	154	234	307	403	686	1 287	1673	2 573	5 36
1.72	034	154	222	336	440	579	985	1848	2 402	3 695	7 69
2.07	1.59	114	165	249	327	430	732	1373	1784	2 745	5 71
2.07	048	173	250	378	496	652	1 109	2 080	2 704	4 161	8 66
	2.28	128	184	278	365	479	816	1530	1 989	3 060	6 37
2.76	1.72	114	165	249	327	430	732	1373	1784	2 745	5 71
	083	173	250	378	496	652	1109	2 080	2 704	4 161	8 66
2.45	2.90 2.07	128	184	278 391	365	479 674	816	1530	1 989 2 796	3 060	6 37
3.45	0 - 1.17	179 212	258 305	462	513 607	798	1 147 1 358	2 151 2 546	3 309	4 301 5 091	8 96 10 60
	3.52	148	214	324	425	558	950	1 781	2 315	3 562	7 42
	3.10	148	214	324	425	558	950	1 781	2 315	3 562	7 42
4.14	2.41	223	321	486	637	838	1426	2 673	3 475	5 347	11 13
	0 - 1.5	251	361	547	718	943	1606	3 011	3 914	6 022	12 54
	4.34	213	307	465	611	803	1366	2 562	3 330	5 123	10 67
5.17	3.79	269	387	586	769	1 011	1 721	3 227	4 195	6 454	13 44
5.17	3.10	319	459	695	912	1 199	2 041	3 826	4 974	7 653	15 94
	0 - 2.1	348	501	758	995	1308	2 226	4 175	5 427	8 349	17 39
	5.86	270	389	589	772	1 016	1729	3 241	4 213	6 482	13 50
6.89	5.17	340	490	742	974	1280	2 179	4 086	5 311	8 171	17 02
	4.14	415	597	904	1186	1559	2 653	4 975	6 467	9 949	20 72
	0 - 2.9 7.31	445 335	641 482	970 730	1 272 958	1 673 1 260	2 847 2 144	5 338 4 020	6 939 5 226	10 676 8 040	22 24 16 75
	6.89	380	547	828	1 086	1 428	2 431	4 558	5 925	9 116	18 99
8.62	5.17	510	735	1 112	1 459	1 918	3 265	6 121	7 957	12 242	25 50
	0 - 3.7	542	780	1 181	1550	2 037	3 467	6 502	8 452	13 003	27 09
	8.76	400	576	872	1 143	1503	2 559	4 798	6 237	9 596	19 9
10.34	6.89	563	811	1 2 2 7	1 610	2 117	3 603	6 755	8 782	13 510	28 14
	0 - 4.6	639	920	1392	1827	2 402	4 088	7 665	9 964	15 330	31 93
	10.20	465	669	1 013	1329	1 747	2 973	5 575	7 247	11 150	23 22
12.07	8.62	611	880	1332	1748	2 298	3 912	7 335	9 535	14 670	30 50
,,	6.89	720	1036	1569	2 058	2 706	4 606	8 636	11 226	17 271	35 98
	0 - 5.5	736	1059	1604	2 104	2 766	4 709	8 828	11 477	17 657	36 78
	11.72	521	751	1 137	1 491	1960	3 337	6 256	8 133	12 512	26 0
13.79	10.34 8.62	656 776	945 1 118	1 430 1 693	1 876 2 221	2 466 2 920	4 198 4 970	7 872 9 318	10 233 12 113	15 744 18 636	32 79 38 82
	0 - 6.3	833	1 199	1 815	2 381	3 131	5 329	9 9 9 9 2	12 113	19 984	41 63
	13.17	586	844	1278	1676	2 204	3 751	7 033	9 143	14 066	29 30
45 57	12.07	698	1005	1 521	1996	2 624	4 466	8 374	10 887	16 749	34 89
15.51	10.34	829	1 194	1808	2 372	3 119	5 309	9 954	12 940	19 907	41 47
	0 - 7.24	930	1 339	2 027	2 659	3 495	5 950	11 155	14 502	22 311	46 4
	13.79	737	1062	1607	2 109	2 773	4 719	8 849	11 503	17 697	36 86
17.24	12.07	879	1 266	1 917	2 515	3 306	5 627	10 551	13 716	21 102	43 96
. / . 4 7	10.34	987	1 421	2 152	2 823	3 711	6 316	11 843	15 396	23 687	49 3
	0 - 8.06	1027	1 478	2 238	2 936	3 860	6 570	12 319	16 015	24 638	51 32
10.00	13.79	926	1334	2 019	2 649	3 483	5 929	11 116	14 451	22 233	46 3
18.96	12.07	1 043	1502	2 273	2 982	3 921	6 674	12 514	16 268	25 028	52 14
	0 - 8.96 13.79	1124	1 618 1 578	2 449 2 389	3 213 3 134	4 224 4 120	7 191 7 013	13 482 13 150	17 527 17 095	26 965	56 17
20.00	12.07	1 096 1 196	1722	2 389	3 134	4 120	7 654	14 351	18 656	26 300 28 702	54 79 59 79
_ 0.00	0 - 9.79	1220	1758	2 661	3 491	4 589	7 811	14 646	19 040	29 292	61 02

^{*}Minimum inlet pressure for OB-2000PT is 15 psig (1 barg) because of the pressure pilot.

OB-30, OB-2000, OB-2000PT



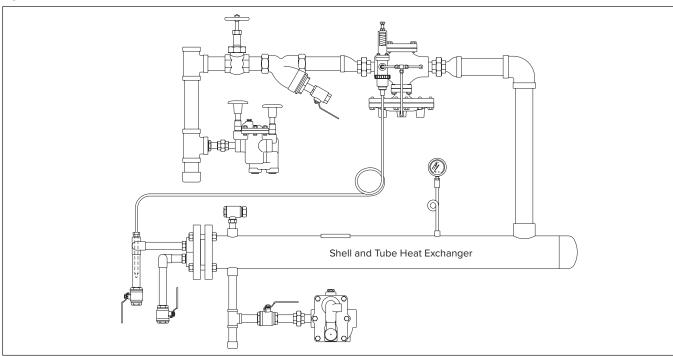
For Steam Service

Points to Remember When Installing

- Drain condensate at inlet of pressure/temperature regulator with inverted bucket steam trap.
- Protect temperature regulating valve from dirt and scale by installing strainer with 100 mesh screen at inlet of valve.
- Install shutoff valves on either side of the regulating valve along with a by-pass line for maintenance purposes.
- Install vacuum breaker after the outlet of equipment and before the steam trap.

- Install sensor so it is fully immersed in the fluid being heated.
- If temperature well is used, apply heat transfer medium to sensor before insertion into well.
- Place thermometer into system in close proximity to temperature sensor for accurate valve adjustment.
- If possible, do not elevate condensate after steam trap.
- Determine pressure setting before temperature setting (OB-2000PT only).

Typical Installation—OB-30, OB-2000



Load Calculations

Heating oil with steam

lb/hr steam =
$$\frac{GPM}{4}$$
 x ΔT x 1.1

Heating water with steam

lb/hr steam =
$$\frac{GPM}{2}$$
 × ΔT × 1.1

Heating air with steam

lb/hr steam =
$$\frac{CFM}{900} \times \Delta T \times 1.1$$

Jacketed kettles or tanks

Ib/hr steam =
$$\frac{\text{Gal x SG x Cp x } \Delta \text{T x 8.3}}{\text{Lat x T}}$$

Where:

GPM = Gallons per minute ΔT = Temperature rise (°F)

CFM = Cubic feet per minute

Cp = Specific heat of liquids (Btu/lb-°F)

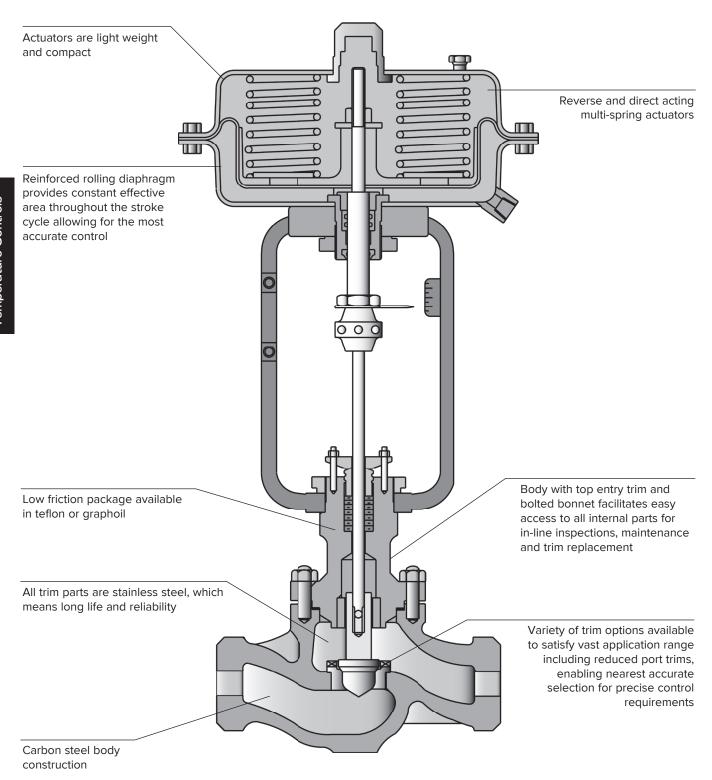
 $\Gamma = Time (hours)$

Lat = Latent heat of steam (Btu/lb)
Gal = Gallons of liquid to be heated

SG = Specific gravity 1.1 = Safety factor



Python - 1100 Series Control Valves



Python - 1100 Series Control Valves



When accurate control is desired from your steam or water applications the Armstrong Python* 1100 Series Control Valve will squeeze every bit of performance out of your system and deliver precise control. With a wide range of materials, sizes, trim, and other features, you are sure to find the Python* can accurately control your system. The Python* 1100 Series Control Valve is constructed and equipped with state of the art materials and is designed to meet the most stringent budget.

Product Features

- Series 1100 valves are Globe two-way single seated body design valves, which satisfy the majority of control applications for HVAC, industrial and commercial markets.
- Body with top entry trim and bolted bonnet facilitates easy access to all internal parts for in-line inspection, maintenance and trim replacement.
- · Stream line flow path provides large flow capacity.
- Variety of trim options are available to satisfy a vast application range including reduced port trims enabling nearest accurate selection for precise control requirements.
- Trims with top bush guided plugs are available with simple construction for stable operation, assuring high rangeability and turndown ratios.
- · Micro trims available for control of minute flow rates.
- Trims with large guide plugs are available for full pressure balancing effect providing an economical choice for high pressure applications.
- All parts are renewable in-line.
- Carbon steel or stainless steel body construction.
- · Reverse and direct acting multi-spring actuators.
- Available in 1/2" 2" NPT and 1/2" 8" ANSI flange design.
- · Rated for class IV shut-off.

Accessories

- Pneumatic Valve Positioner
- Electro-Pneumatic (E/P) Valve Positioner
- Digital Valve Positioners
- Pressure/Temperature Controllers
- · Air Filter Regulator



Python* Series 1100 Control Valve



Python® Series 1100 Control Valve with Positioner



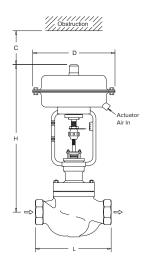
Armstrong Python - 1100 Series Control Valves

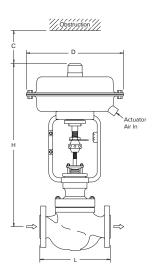
Control Valves - 1100 Series List of Materials	
Valve Body*	Carlhan Stand A 24C Cr. WCD
Bonnet*	Carbon Steel A216 Gr. WCB
Valve/Valve Seat	Stainless Steel AISI 431
Valve Stem	Stainless Steel 316
Gland Packing	V-Teflon - option 1 (366°F Max.) Grafoil - option 2
Yoke	S.G. Iron
Actuator Spring	Chrome Vanadium/Spring Steel
Actuator Diaphragm	Nitrile Reinforced with Nylon Fiber

^{*}Stainless steel available.

Control Valv	es - 1100 Series Specifications	
Flow		Equal Percentage
Leakage		ANSI Class IV
Rangeability		50:1
	1/2" to 1"	11/16" (18 mm)
Travel	1-1/2" to 2"	1-1/8" (28 mm)
Iravei	2-1/2" to 4"	1-1/2" (38 mm)
	6" to 8"	2-1/4" (58 mm)
Maximum Temperature		450°F (232°C)*
Maximum Pressure		300 psig (20 barg)*

^{*}Higher pressure and temperature valves available.





Contro	ol Valv	es - 1100	Serie	s Dimen	sions	and Wei	ghts												
Siz	e.		F	ace-to-F	ace "L	."		"~	,	"D	,	"LI	,			We	ight		
		NP	Т	150)#	300)#		"C" "D"			"H"		NPT		150#		300#	
in	mm	in	mm	in	mm	in	mm	in	mm	in	in mm	in	mm	lb	kg	lb	kg	lb	kg
1/2	15	6-1/2	165	7	178	_	_	4	102	9-7/16	240	18-1/2	470	31	14	34	15	_	_
3/4	20	6-1/2	165	7-1/8	181	_	_	4	102	9-7/16	240	18-1/2	470	31	14	34	15	_	_
1	25	7-3/4	197	7-1/4	184	7-3/4	197	4	102	9-7/16	240	18-1/2	470	33	15	36	16	40	18
1-1/2	40	9-1/4	25	8-3/4	222	9-1/4	235	5	127	11-7/16	290	20-9/32	515	51	23	55	25	60	27
2	50	10-1/2	267	10	254	10-1/2	267	5	127	11-7/16	290	20-9/32	515	60	27	65	30	71	32
2-1/2	65	_	_	10-7/8	276	11-1/2	292	6	127	15	380	25-3/16	640	_	_	120	54	135	61
3	80	_	_	11-3/4	299	12-1/2	318	6	152	15	380	25-3/16	640	_	_	135	61	154	70
4	100	_	_	13-7/8	353	14-1/2	368	6	152	15	380	26-3/8	670	_	_	176	80	220	100
6	150	_	_	17-3/4	451	18-5/8	473	7	175	17-5/8	448	43-1/2	1105	_	_	330	150	396	180
8	200	_	_	21-3/8	543	22-3/8	568	7	175	17-5/8	448	45-1/4	1150	_	_	551	250	650	295

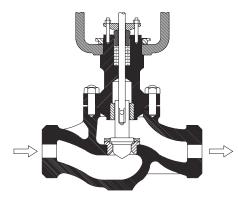
Note: Additional sizes up to 20" available upon request.

Python - 1100 Series Control Valves



Contour Top Guided

The Contour Top Guided trims are the preferred choice for a variety of control applications due to their simple construction. Heavy top guided trim provides maximum support to impart complete stability. The plug shank is guided at the lowest portion of the bonnet minimizing the effect of side thrust on the valve plug and eliminating trim vibration.



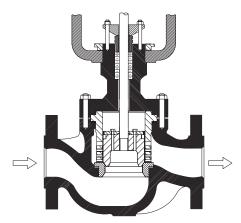
Contoured Top Guided Trim (Unbalanced)

Multi-Hole Cage Guided - Pressure Balanced

The large guide trims with pressure balancing effect enable the valve to handle higher ΔP shut off without employing high power actuators. The flow characteristic is achieved through plug contour. Equalizing holes are opened in the plug which effectively cancel out the unbalanced force impressed on the top and bottom of the valve plug.

Pressure balance sealing is attained; 1) At seating surface 2) Through pressure balance seal rings which are fitted on the plug seal applying pressure along the inner wall of the large guide having a ground, honed and chrome plated surface.

This multi-hole trim also helps with noise attenuation.



Multi-Hole Cage Guided Pressure Balanced Trims

Contoured Top Guided Cv Values

Valve	Size	Trim	Size			
in	mm	in	mm	c _v		
		1	25	13		
		3/4	20	9		
*1/2,	*15, *20, 25	*15,	1/2	15	5	
*3/4, 1		5/16	8	3		
'		1/4	6	2		
		1/8	3	1		
		1-1/2	40	30		
1-1/2	40	1-1/4	32	20		
		1	25	13		
		2	50	50		
2	50	1-1/2	40	30		
		1-1/4	32	20		
		2-1/2	65	80		
2-1/2	65	2	50	50		
		1-1/2	40	30		
		3	80	110		
3	80	2-1/2	65	80		
		2	50	50		
		4	100	200		
4	100	3	80	110		
		2-1/2	65	80		
		6	150	400		
6	150	5	125	300		
		4	100	200		
		8	200	640		
8	200	6	150	400		
		5	125	300		

Note: Additional sizes up to 20" available upon request.

Multi-Hole Cage Guided Cv Values

Valve	Size	Trim	Size	_	
in	mm	in	mm	C _V	
		1-1/2	40	24	
1-1/2	40	1-1/4	32	16	
		1	25	10	
		2	50	40	
2	50	1-1/2	40	24	
		1-1/4	32	16	
		2-1/2	65	64	
2-1/2	65	2	50	40	
		1-1/2	40	24	
		3	80	90	
3	80	2-1/2	65	64	
		2	50	40	
		4	100	160	
4	100	3	80	90	
		2-1/2	65	64	
		6	150	320	
6	150	5	125	240	
		4	100	160	
		8	200	510	
8	200	6	150	320	
		5	125	240	

Note: Additional sizes up to 20" available upon request.

^{*} The trim size must be less than or equal to the valve size.



Python - 1100 Series Control Valve

Multi-Spring Actuators: Series M

The "M" Series control valve actuators are diaphragm actuators with pre-compressed multi-spring construction. They are compact (fewer parts), easy to maintain and quickly reversible. The actuators are suitable for regulating and on/ off applications. Various models are available covering small to larger thrust requirements.

The increasing air pressure supply moves the diaphragm and actuator stem opposing the spring force. With decreasing air pressure supply, the spring force moves the diaphragm in the opposite direction and back to the normal position. To get various loading capacities the number of springs are altered.

Specifications

- Maximum Diaphragm Pressure:
 50 psig (3.5 barg) for Model M and Mp
- Actuator travel:
 11/16", 1-1/8", 1-1/2", 2-1/4"
 (18, 28, 38, 58 mm)
- Diaphragm:

Nitrile reinforced with Nylon fiber

- Operating Temperature Range: -40° to 176°F (-40° to 80°C)
- · Connections:

1/4" NPT (F) for Models 00 and 11 3/8" NPT (F) for Models 22 and 33

Permissible Linearity and Hysterisis:
 ±5% of Signal Pressure Range

Features:

- Utility Applicable for regulating and on-off applications
- High Power Variety of models provide choice for low and high thrust requirements
- Construction Due to multi-spring arrangement the actuators are lightweight and compact
- Reversible The actuators are field reversible without demanding addition or deletion of parts
- Long Service Life Rigid construction and durable components provide a long lasting service life
- Minimum Maintenance The actuators are virtually maintenance free
- Accuracy Rolling diaphragm construction provides constant effective area throughout the stroke

Direct Acting Actuators (Fail Open)

The actuator stem moves downward with increasing diaphragm pressure. When this pressure is reduced the opposing spring force moves the actuator stem upward. On air failure, the actuator stem is pulled to the extreme upward position by spring force.

This actuator is suitable for the following:

Fail Open - For valves with plugs that push down to close Fail Close - For valves with plugs that push down to open

Reverse Acting Actuators (Fail Close)

The actuator stem moves upward with increasing diaphragm pressure. When this pressure is reduced the opposing spring force moves the actuator stem downward. On air failure, the actuator stem is pushed to extreme downward position by spring force.

This actuator is suitable for the following:

Fail Close - For valves with plugs that push down to close Fail Open - For valves with plugs that push down to open

Air Volume Required Per Stroke.	
Model Number	Cubic Feet/Stroke
M-00, Mp-00	0.012
M-11, Mp-11	0.035
M-22, Mp-22	0.082
M-33, Mp-33	0.185

Python - 1100 Series Control Valve



Conto	ıred Top G	uided Shu	t Off Pressure	e														
	Air	Spring Se	etting Range				Maxim	um Diff	erentia	l Pressu	re (PSIC	S) ΔP /	Shut Off	Pressu	ıre			
Model No.	Supply Pres. to Diaph.	Direct Acting Actuator	Reverse Acting Actuator	Diaph. Area						Tri	m Size							
	PSIG	PSIG	PSIG	inch²	1/8"	1/4" - 5/16"	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	2-1/2"	3"	4"	6"	8"	
	20	3 - 15	3 - 15		300	300	206	134	94	–	_	_	_	_	_	_	_	
	23	3 - 13	6 - 18		300	300	300	300	222	_	_	_	_	_	_	_	_	
M-00	34		6 - 30	30	300	300	300	300	222	–	_	_	_	_	_	_	_	
	37	6 - 30	9 - 32		300	300	300	300	300	_	_	_	_	_	_	_	_	
	40		12 - 35		300	300	300	300	300	_	_	_	_	_	_	_	_	
	20	3 - 15	3 - 15		_	_	_	_	_	121	78	43	_	_	_	_	_	
	23		6 - 18		_	_	_	_	_	269	178	102	_	_	_	_	_	
M-11	34		6 - 30	55	_	_	_	_	_	269	178	102	_	_	_	_	_	
	37	6 - 30	9 - 32	9 - 32		_	_	_	_	_	300	279	162	_	_	_	_	_
	40		12 - 35		_	_	_	_	_	300	300	222	_	_	_	_	_	
	20	3 - 15	3 - 15		_	_	_	_	_	_	_	_	51	35	16	_	_	
	23	3-13	6 - 18		_	_	_	_	_	_	_	_	114	80	38	_	_	
M-22	34		6 - 30	95	_	_	_	_	_	_	_	_	114	80	38	_	_	
	37	6 - 30	9 - 32		_	_	_	_	_	_	_	_	178	125	62	_	_	
	40		12 - 35		_	_	_	_	_	–	_	_	240	172	85	_	_	
	20	3 - 15	3 - 15		_	_	_	_	_	–	_	_	_	_	_	10	5	
	23	3-15	6 - 18		_	_	_	_	_	–	_	_	_	_	_	27	14	
M-33	34		6 - 30	140		_	_	_	_	_	_	_	_	_	-	27	14	
	37	6 - 30	9 - 32		-	_	_	_	_	_	_	_	_	_	-	42	25	
	40		12 - 35		_	_	_	_	_	_	_	_	_	_	_	60	32	

Do not exceed 50 PSIG air pressure to the actuator.

Multi-Hole	e Cage Guided S	Shut Off Pres	sure											
	Air Cummbe	Spring	Setting Range		Maximum Differential Pressure (PSIG) ΔP / Shut Off Pressure									
Model No.	Air Supply Pres. to Diaph.	Direct Acting Actuator	Reverse Acting Actuator	Diaph. Area	Trim Size									
	PSIG	PSIG	PSIG	inch²	1-1/2"	2"	2-1/2"	3"	4"	6"	8"			
	20	3 - 15	3 - 15	55	257	150	_	_	_	_	_			
	23	3 - 13	6 - 18		300	300	_	_	_	_	_			
M-11	34		6 - 30		300	300	_	_	_	_	_			
	37	6 - 30	9 - 32		300	300	_	ı	_	-	_			
	40		12 - 35		300	300	_	ı	_	-	_			
	20	3 - 15	3 - 15		_	-	298	190	97	_	_			
	23	3 - 15	6 - 18		_	-	300	300	300	_	_			
M-22	34		6 - 30	95	_	_	300	300	300	_	_			
	37	6 - 30	9 - 32		_	_	300	300	300	_	_			
	40		12 - 35		_	_	300	300	300	_	_			
	20	3 - 15	3 - 15		_	-	_	ı	_	133	21			
	23	3 - 15	6 - 18		_	-	_	ı	_	300	258			
M-33	34		6 - 30	140	_	_	_	_	_	300	258			
	37	6 - 30	9 - 32	1	_	_	_	_	_	300	300			
	40		12 - 35			_		_	_	300	300			

Do not exceed 50 PSIG air pressure to the actuator.



Python - Electric Actuators

When accurate control of your steam or water application is desired and air is not available, the Python* AEL Electric Control Valve will deliver precise control. The electric version of the popular 1100 series control valve is built to out perform and deliver accurate control. The AEL Series Electric Control Valve is constructed and equipped with state of the art industrial materials combined with the standard 1100 series main valve.

Product Features:

- Power: 24v AC (120v AC or 240v AC available)
- · Terminal board connection
- · Pillar mechanical connection
- · Auto/Manual control
- · Control signal 4-20 ma, 0-10 volts
- · Protection class IP 67
- · High thrust capabilities
- · Electronic position control
- · Metal internal gears
- · Compact design
- Mounts to the standard 1100 Series valve body
- · Actuators available from 1/2" to 4"

List of Materials	
Valve Body*	Carbon Steel A216 GR. WCB
Bonnet*	Carbon Steel A216 GR. WCB
Valve/Valve Seat	Stainless Steel AISI 410
Valve Stem	Stainless Steel 316
valve Stem	V-Teflon- Option 1 (366°F max)
Gland Packing	Grafoil-Option 2
Yoke	S.G. Iron
Actuator Housing	Aluminum

^{*}Stainless steel available.



Python® Series 1100 AEL Electric Actuator

Technic	al Data	
Flow		Equal Percentage
Leakage		ANSI Class IV
Rangeab	ility	50:1
	1/2" to 1"	11/16" (18mm)
Travel	1-1/4" to 2"	1-1/8" (28mm)
IIavei	2-1/2" to 4"	1-1/2" (38mm)
	6" to 8"	2-1/4" (58mm)
Maximum	1 Temperature	450°F (232°C)
Maximum	n Pressure	300 psig (20 barg)
Voltage		24v Power Supply

Dime	ensio	ns anc	l We	ights															
Siz	e		Fa	ce-to-F	ace "	L"		"C'	,	"D'	,	"H'	,	Weight					
		NP.	Т	150)#	300)#	C						NPT		150#		300#	
in	mm	in	mm	in	mm	in	mm	in	mm	n in n	mm	in	mm	lb	kg	lb	kg	lb	kg
1/2	15	6-1/2	165	7	178	_	_	7-7/8	200	5	127	14-9/16	370	22	10	34	15	_	_
3/4	20	6-1/2	165	7-1/8	181	_	_	7-7/8	200	5	127	14-9/16	370	22	10	34	15	_	_
1	25	7-3/4	197	7-1/4	184	_	_	7-7/8	200	5	127	24-15/16	633	24	11	36	16	_	_
1-1/4	32	9-1/4	235	8-3/4	222	_	_	6-5/16	160	7-1/4	183	26-1/8	664	39	18	55	25	_	_
1-1/2	40	9-1/4	235	8-3/4	222	_	_	6-5/16	160	7-1/4	183	26-1/8	664	39	18	55	25	_	-
2	50	10-1/2	267	10	254	10-1/2	267	6-5/16	160	7-1/4	183	26-11/16	678	48	22	65	30	71	32
2-1/2	65	_	_	10-7/8	276	11-1/2	292	6-5/16	160	7-1/4	183	26-5/16	668	_	_	120	54	135	61
3	80	_	_	11-3/4	299	12-1/2	318	6-5/16	160	7-1/4	183	28-1/2	724	_	_	135	61	150	68
4	100	_	_	13-7/8	353	14-1/2	368	6-5/16	160	7-1/4	183	31-5/8	803	_	_	176	80	210	95
6	150	_	-	17-3/4	451	18-5/8	473	6-5/16	160	7-1/4	183	34-1/4	870	_	_	322	146	380	172
8	200	_	_	21-3/8	543	22-3/8	568		_	_	_	_	_	_	_	540	245	630	286

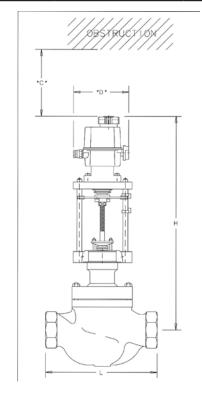
^{*}Refer to images on page 321.

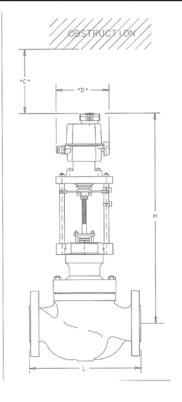
Python® - Electric Actuators



Top Guid	led												
Size	of Valve			NPT				Model					
IN	ММ	Switch-off thrust (N)	Speed (mm/min)	Modulating Model	ON/OFF Model	Switch-off thrust (N)	Speed (mm/ min)			Stroke			
1/2"	15	1900	28	AEL1430	AEL1490	1 900	28	AEL1430	AEL1490	18mm			
3/4"	20	1900	28	AEL1430	AEL1490	1900	28	AEL1430	AEL1490	18mm			
1"	25	1900	28	AEL1430	AEL1490	1900	28	AEL1430	AEL1490	18mm			
1-1/4"	32	3 600	48	AEL1438	AEL1498	1900	48	AEL1438	AEL1498	28mm			
1-1/2"	40	4 600	48	AEL1438	AEL1498	3 600	48	AEL1438	AEL1498	28mm			
2"	50	7 200	48	AEL1438	AEL1431	4 600	48	AEL1438	AEL1498	28mm			
2-1/2"	65	_	_	_	_	4 600	48	AEL1438	AEL1498	_			
3"	80	_	_	_	_	4 600	48	AEL1438	AEL1498	_			
4"	100	_	_	_	_	4 600	48	AEL1438	AEL1498	_			

Multi-Ho	fulti-Hole												
Size	of Valve		15	0# Flg		300# Flg							
IN	N MM Switch-off thrust (N)		Speed (mm/min)	Modulating Model	ON/OFF Model	Switch-off thrust (N)	Speed (mm/ min)	Modulating Model	ON/OFF Model	Stroke			
1-1/2"	40	1900	48	AEL1438	AEL1498	1900	48	AEL1438	AEL1498	28mm			
2"	50	1900	48	AEL1438	AEL1498	1900	48	AEL1438	AEL1498	28mm			
2-1/2"	65	3 600	48	AEL1438	AEL1498	3 600	48	AEL1438	AEL1498	38mm			
3"	80	3 600	48	AEL1438	AEL1498	3 600	48	AEL1438	AEL1498	38mm			
4"	100	3 600	48	AEL1438	AEL1498	3 600	48	AEL1438	AEL1498	38mm			
6"	150	4 600	48	AEL1431	AEL1491	5 800	48	AEL1438	AEL1431	58mm			







Armstrong[®] Python[®] - 1100 Series Control Valve

Capacities for Saturated Steam Service

Contou	red Top G	uided Tri	m											
							lb/hr							
Inlet	Outlet	Trim Size and C _V												
/n	cia)	1/8	1/4	5/16	1/2	3/4	1	in 1-1/4	1-1/2	2	2-1/2	3	4	6
(psig) C _V Factor		1.0	2.0	3.0	5.0	9.0	13.0	20.0	30.0	50.0	80.0	110.0	200.0	400.0
C _V F	3	18	36	5.0 54	91	163	236	363	545	908	1 453	1998	3 632	7 265
5	0-2	32	64	97	161	290	418	643	965	1609	2 574	3 539	6 434	12 868
	5	31	63	94	156	282	407	626	939	1564	2 503	3 442	6 258	12 516
10	0-4	40	81	121	202	363	524	807	1 210	2 017	3 227	4 437	8 067	16 134
	10	35	69	104	173	312	450	693	1039	1732	2 771	3 810	6 927	13 854
15	0 - 6	49	97	146	243	437	631	970	1 455	2 425	3 880	5 335	9 700	19 400
	15	38	75	113	188	339	490	754	1 130	1884	3 015	4 145	7 537	15 073
20	0 - 8	57	113	170	283	510	737	1 133	1700	2 833	4 533	6 233	11 333	22 666
	20	59	118	178	296	533	769	1 183	1775	2 959	4 734	6 509	11 835	23 670
30	0 - 12	73	146	219	365	657	949	1460	2 190	3 650	5 840	8 029	14 599	29 198
	30	66	132	199	331	596	861	1324	1986	3 310	5 297	7 283	13 242	26 483
40	25	79	158	237	395	711	1027	1580	2 371	3 951	6 322	8 692	15 805	31 609
	0 - 16	89	179	268	447	804	1 161	1 787	2 680	4 466	7 146	9 826	17 865	35 730
	40	73	145	218	363	653	943	1 451	2 177	3 628	5 805	7 982	14 513	29 026
50	30	98	196	295	491	884	1 277	1965	2 947	4 911	7 858	10 805	19 646	39 292
	0 - 20	106	211	317	528	951	1374	2 113	3 170	5 283	8 452	11 622	21 131	42 262
	50	78	157	235	392	706	1 019	1568	2 352	3 920	6 272	8 625	15 681	31 362
60	35	117	234	351	586	1054	1522	2 342	3 513	5 856	9 369	12 882	23 422	46 84
	0 - 24	122	244	366	610	1 098	1586	2 440	3 660	6 099	9 759	13 418	24 397	48 794
	65	86	173	259	432	778	1124	1729	2 593	4 322	6 915	9 508	17 286	34 573
75	50	130	261	391	652	1 174	1696	2 609	3 914	6 524	10 438	14 352	26 094	52 188
	0 - 30	146	293	439	732	1 318	1904	2 930	4 394	7 324	11 718	16 113	29 296	58 59
	75	150	300	450	751	1 351	1952	3 002	4 504	7 506	12 009	16 513	30 023	60 04
100	60	183	366	548	914	1 645	2 376	3 656	5 484	9 139	14 623	20 106	36 557	73 114
	0 - 40	187	375	562	937	1 686	2 435	3 746	5 619	9 365	14 984	20 604	37 461	74 922
	100	167	335	502	837	1507	2 177	3 349	5 024	8 374	13 398	18 422	33 495	66 99
125	75	225	450	675	1125	2 024	2 924	4 498	6 747	11 245	17 992	24 740	44 981	89 962
	0 - 50	228	456	684	1 141	2 053	2 966	4 563	6 844	11 407	18 250	25 094	45 626	91 252
	125	183	366	550	916	1 649	2 382	3 664	5 496	9 160	14 656	20 151	36 639	73 278
150	100	248	496	745	1 241	2 234	3 227	4 964	7 446	12 410	19 857	27 303	49 642	99 284
	0 - 60	269	538	807	1345	2 421	3 496	5 379	8 069	13 448	21 516	29 585	53 791	107 58
	150	198	395	593	988	1 779	2 570	3 953	5 930	9 883	15 813	21 743	39 534	79 06
175	110	300	600	901	1 501	2 702	3 903	6 004	9 006	15 010	24 016	33 022	60 041	120 08
	0 - 70	310	620	929	1 549	2 788	4 027	6 196	9 293	15 489	24 782	34 076	61 956	123 91
	150	289	578	868	1 446	2 603	3 760	5 785	8 677	14 462	23 139	31 816	57 847	115 69
200	125	342	685	1 027	1 712	3 081	4 451	6 847	10 271	17 119	27 390	37 661	68 474	136 94
	0 - 80	351	701	1052	1753	3 155	4 558	7 012	10 518	17 530	28 048	38 567	70 121	140 24
	200	325	650	975	1626	2 926	4 227	6 503	9 754	16 256	26 010	35 764	65 025	130 05
250	150	413	827	1 240	2 067	3 721	5 374	8 268	12 402	20 670	33 072	45 474	82 681	165 36
	0 - 100	432	865	1 297	2 161	3 890	5 619	8 645	12 968	21 613	34 580	47 548	86 451	172 90
	250	357	715	1 072	1 787	3 217	4 647	7 149	10 723	17 872	28 595	39 318	71 486	142 97
300	200	483	966	1 450	2 416	4 349	6 281	9 664	14 495	24 159	38 655	53 150	96 637	193 273
	0 - 120	514	1028	1542	2 570	4 625	6 681	10 278	15 417	25 695	41 112	56 530	102 781	205 56

^{*}Capacities based on maximum Cv. It is recommended to operate the valve between 15-85% of the valve opening. See chart on page 333.

Python - 1100 Series Control Valve



Capacities for Saturated Steam Service

							kg/hr							
Inlet	Outlet						Trir	n Size an	d C _V					
			1		1	1		mm		1	1			1
(barg)		3	6	8	15	20	25	32	40	50	65	80	100	150
C _V F	actor	1.0	2.0	3.0	5.0	9.0	13.0	20.0	30.0	50.0	80.0	110.0	200.0	400.
0.34	0.21	8	16	25	41	74	107	165	247	412	659	906	1648	3 29
	0 - 0.14	15	29	44	73	131	190	292	438	730	1 167	1605	2 918	5 83
0.69	0.34	14	28	43	71	128	185	284	426	710	1 135	1 561	2 839	5 67
0.00	0 - 0.28	18	37	55	91	165	238	366	549	915	1 464	2 013	3 659	7 318
1.03	0.69	16	31	47	79	141	204	314	471	785	1257	1728	3 142	6 28
1.03	0 - 0.41	22	44	66	110	198	286	440	660	1 100	1760	2 420	4 400	8 80
1.38	1.03	17	34	51	85	154	222	342	513	855	1367	1880	3 419	6 83
1.30	0 - 0.55	26	51	77	129	231	334	514	771	1 285	2 056	2 827	5 141	10 28
2.07	1.38	27	54	81	134	242	349	537	805	1342	2 147	2 953	5 368	10 73
2.07	0 - 0.83	33	66	99	166	298	430	662	993	1656	2 649	3 642	6 622	13 24
	2.07	30	60	90	150	270	390	601	901	1502	2 403	3 304	6 006	12 01
2.76	1.72	36	72	108	179	323	466	717	1 075	1792	2 868	3 943	7 169	14 33
	0 - 1.10	41	81	122	203	365	527	810	1 216	2 026	3 241	4 457	8 104	16 20
	2.76	33	66	99	165	296	428	658	987	1646	2 633	3 621	6 583	13 16
3.45	2.07	45	89	134	223	401	579	891	1337	2 228	3 565	4 901	8 911	17 82
	0 - 1.38	48	96	144	240	431	623	958	1 438	2 396	3 834	5 272	9 585	19 17
4.14	3.45	36	71	107	178	320	462	711	1067	1778	2 845	3 912	7 113	14 22
	2.41	53	106	159	266	478	691	1062	1594	2 656	4 250	5 843	10 624	21 24
	0 - 1.65	55	111	166	277	498	719	1 107	1660	2 767	4 427	6 087	11 066	22 13
	4.48	39	78	118	196	353	510	784	1 176	1960	3 136	4 313	7 841	15 68
5.17	3.45	59	118	178	296	533	769	1 184	1 775	2 959	4 734	6 510	11 836	23 67
0	0 - 2.07	66	133	199	332	598	864	1329	1993	3 322	5 315	7 309	13 289	26 57
	5.17	68	136	204	340	613	885	1362	2 043	3 405	5 447	7 490	13 619	27 23
6.89	4.14	83	166	249	415	746	1 078	1658	2 487	4 146	6 633	9 120	16 582	33 16
0.03	0 - 2.76	85	170	255	425	765	1 104	1699	2 549	4 248	6 797	9 346	16 992	33 98
	6.89	76	152	228	380	684	988	1 519	2 279	3 798	6 077	8 356	15 193	30 38
8.62	5.17	102	204	306	510	918	1326	2 040	3 061	5 101	8 161	11 222	20 403	40 80
0.02	0 - 3.45	103	207	310	517	931	1345	2 070	3 104	5 174	8 278	11 383	20 696	41 39
	8.62	83	166	249	415	748	1080	1662	2 493	4 155	6 648	9 141	16 619	33 23
10.34	6.89	113	225	338	563	1 013	1 464	2 252	3 378	5 629	9 007	12 385	22 517	45 03
10.54	0.89	122	244	366	610	1013	1586	2 440	3 660	6 100	9 760	13 420	24 399	48 79
	10.34	90	179	269	448	807	1166	1793	2 690	4 483	7 173	9 863	17 932	35 86
12.07	1			1				I		ł		1	1	
12.07	7.58	136	272	409	681	1226	1770	2 723	4 085	6 809	10 894	14 979	27 234	54 46
	0 - 4.83	141	281	422	703	1265	1827	2 810	4 215	7 026	11 241	15 457	28 103	56 20
12.70	10.34	131	262	394	656	1 181	1706	2 624	3 936	6 560	10 496	14 432	26 239	52 47
13.79	8.62	155	311	466	776	1 398	2 019	3 106	4 659	7 765	12 424	17 083	31 060	62 11
	0 - 5.52	159	318	477	795	1 431	2 067	3 181	4 771	7 952	12 723	17 494	31 807	63 61
17.24	13.79	147	295	442	737	1327	1 917	2 950	4 424	7 374	11 798	16 222	29 495	58 99
	10.34	188	375	563	938	1688	2 438	3 750	5 626	9 376	15 001	20 627	37 504	75 00
	0 - 10.3	196	392	588	980	1765	2 549	3 921	5 882	9 803	15 686	21 568	39 214	78 42
	17.24	162	324	486	811	1 459	2 108	3 243	4 864	8 107	12 970	17 834	32 426	64 85
20.00	13.79	219	438	658	1096	1 973	2 849	4 383	6 575	10 959	17 534	24 109	43 834	87 66
	0 - 8.28	233	466	699	1 166	2 098	3 030	4 662	6 993	11 655	18 648	25 642	46 621	93 24

^{*}Capacities based on maximum Cv. It is recommended to operate the valve between 15-85% of the valve opening. See chart on page 333.



Capacities for Saturated Steam Service

				II.	o/hr					
						e and C _v				
Inlet	Outlet		in							
(p	sig)	1	1-1/4	1-1/2	2	2-1/2	3	4	6	
C _v F	actor	10.0	16.0	24.0	40.0	64.0	90.0	160.0	320.0	
	75	1 501	2 402	3 603	6 005	9 607	13 511	24 019	48 037	
100	60	1828	2 925	4 387	7 311	11 698	16 451	29 246	58 49 ⁻	
	0 - 40	1873	2 997	4 495	7 492	11 988	16 857	29 969	59 938	
	100	1 675	2 680	4 019	6 699	10 718	15 073	26 796	53 592	
125	75	2 249	3 598	5 398	8 996	14 394	20 242	35 985	71 970	
	0 - 50	2 281	3 650	5 475	9 125	14 600	20 532	36 501	73 002	
	125	1832	2 931	4 397	7 328	11 724	16 487	29 311	58 622	
150	100	2 482	3 971	5 957	9 928	15 885	22 339	39 713	79 42	
	0 - 60	2 690	4 303	6 455	10 758	17 213	24 206	43 033	86 06	
	150	1 977	3 163	4 744	7 907	12 651	17 790	31 627	63 25	
175	110	3 002	4 803	7 205	12 008	19 213	27 018	48 033	96 06!	
	0 - 70	3 098	4 956	7 435	12 391	19 826	27 880	49 565	99 130	
	150	2 892	4 628	6 942	11 569	18 511	26 031	46 278	92 556	
200	125	3 424	5 478	8 217	13 695	21 912	30 813	54 779	109 55	
	0 - 80	3 506	5 610	8 415	14 024	22 439	31 554	56 097	112 194	
	200	3 251	5 202	7 803	13 005	20 808	29 261	52 020	104 04	
250	150	4 134	6 614	9 922	16 536	26 458	37 206	66 145	132 28	
	0 - 100	4 323	6 916	10 374	17 290	27 664	38 903	69 161	138 32	
•	250	3 574	5 719	8 578	14 297	22 876	32 169	57 189	114 378	
300	200	4 832	7 731	11 596	19 327	30 924	43 486	77 309	154 618	
	0 - 120	5 139	8 222	12 334	20 556	32 890	46 251	82 225	164 45	

^{*}Capacities based on maximum C_{V} . It is recommended to operate the valve between 15-85% of the valve opening. See chart on page 333.

				k	g/hr					
Inlet	Outlet					e and C _v				
						mm				
	arg)	25	32	40	50	65	80	100	150	
C _v I	Factor	10.0	16.0	24.0	40.0	64.0	90.0	160.0	320.0	
	5.17	681	1 089	1 634	2 724	4 358	6 128	10 895	21 790	
6.89	4.14	829	1 327	1 990	3 316	5 306	7 462	13 266	26 531	
	0 - 2.76	850	1359	2 039	3 398	5 438	7 646	13 594	27 188	
	6.89	760	1 215	1823	3 039	4 862	6 837	12 155	24 309	
8.62	5.17	1 020	1 632	2 448	4 081	6 529	9 182	16 323	32 645	
	0 - 3.45	1 035	1 656	2 483	4 139	6 623	9 313	16 557	33 113	
	8.62	831	1 330	1994	3 324	5 318	7 479	13 295	26 591	
10.34	6.89	1126	1 801	2 702	4 503	7 206	10 133	18 014	36 028	
	0 - 4.14	1 220	1952	2 928	4 880	7 808	10 980	19 520	39 039	
	10.34	897	1 435	2 152	3 586	5 738	8 070	14 346	28 692	
12.07	7.58	1362	2 179	3 268	5 447	8 715	12 255	21 788	43 575	
	0 - 4.83	1 405	2 248	3 372	5 621	8 993	12 646	22 482	44 965	
	10.34	1 312	2 099	3 149	5 248	8 397	11 808	20 991	41 983	
13.79	8.62	1 553	2 485	3 727	6 212	9 939	13 977	24 848	49 695	
	0 - 5.52	1590	2 545	3 817	6 361	10 178	14 313	25 445	50 891	
	13.79	1 475	2 360	3 539	5 899	9 439	13 273	23 596	47 193	
17.24	10.34	1 875	3 000	4 500	7 501	12 001	16 877	30 003	60 006	
	0 - 10.3	1 961	3 137	4 706	7 843	12 548	17 646	31 371	62 742	
	17.24	1 621	2 594	3 891	6 485	10 376	14 592	25 941	51 882	
20.00	13.79	2 192	3 507	5 260	8 767	14 027	19 725	35 067	70 134	
	0 - 8.28	2 331	3 730	5 595	9 324	14 919	20 980	37 297	74 594	

^{*}Capacities based on maximum C_V . It is recommended to operate the valve between 15-85% of the valve opening. See chart on page 333.



Valve Sizing

To determine the size of valve you need, calculate the required Cv value for your application. Once you have calculated the required Cv, refer to the valve Cv charts on page 323 to determine the size and trim of valve. Globe style control valves have the best control in the midrange of the valve's capacity. It is best to pick a valve so the calculated Cv is between 15% and 85% of the valve opening, see page 332. See the formulas below for steam and water applications. Consult factory for other types of fluids.

For Saturated Steam Service

Subcritical Flow	Critical Flow			
When $\Delta P < 0.81(P_1/2)$	When $\Delta P \ge 0.81(P_1/2)$			
Cv =W	Cv =W			
2.1√ΔP(P1A+P2A)	1.633 (P _{1A})			

For Liquid Service

$$Cv = \underline{\qquad (GPM) \sqrt{G}}$$

C_v = Valve flow coefficient

W = Maximum flow capacity of steam, lbs/hr P_{1A} = Inlet Pressure, psia (psig + 14.7) P_{2A} = Outlet Pressure, psia (psig + 14.7) ΔP = Pressure drop (P_1 - P_2) psig

GPM = Maximum flow capacity of Liquid, GPM

G = Specific Gravity

Actuator Sizing

To determine the required actuator, you need to determine the differential pressure (shut off pressure). The shut off pressure for a pressure reduction application is the pressure difference between P₁ and P₂. The shut off pressure for a temperature control application is the P₁ pressure.

Once you have calculated your shut off pressure, select the actuator model and spring setting range that exceeds your calculated shutoff pressure with the trim size previously selected. Select reverse acting for air to open (fail close) applications or direct acting for air to close (fail open) applications.

Make sure the required air pressure is available for the spring range selected.

Sizing Example 1:

Fluid: Saturated Steam

P₁ = 140 psig **P**₂ = 20 psig **Flow:** 13 000 lbs/hr

Actuator: Air to open (Fail Close)

Solution:

Valve Selection: Select the correct formula needed to calculate Cv. We need to use the critical flow formula since $\Delta P > .81(P_1/2)$.

$$C_V = \frac{13\ 000}{1.633(140 + 14.7)} = 52$$

Refer to the C_V charts on Page 4. Select a 2-1/2" Multi-hole cage guided with 2-1/2" Trim. Top bush guided would work as well, but multi-hole cage was chosen to help with noise attenuation.

Actuator Selection: Determine your shutoff pressure (ΔP).

$$\Delta P = 140 - 20 = 120 \text{ psig}$$

Refer to chart 6-2 (multi-hole cage guided) and go to the 2-1/2" trim size column. Follow the column until you get to a pressure greater than 120 psig, then follow the row horizontally to determine you need a Model M-22 with the 3-15 psig spring range.

Complete valve selection is 1100 series, 2-1/2" 150# Flange with 2-1/2" Multi-hole cage trim and M-22 actuator with 3-15 psig spring range.

Sizing Example 2:

Fluid: Saturated Steam

Application: Temperature Control

P1: 125 psig **Flow:** 1 750 lbs/hr

Actuator: Air to open (Fail Close)

Solution:

Since this is a temperature control application and we do not know the P_2 pressure, we will size the valve with a 30% pressure drop. We need to use the subcritical flow formula.

$$C_V = \frac{1750}{2.1\sqrt{(37)((125+14.7)+(88+14.7))}} = 8.8$$

Refer to the Cv charts on Page 4. Select a 1" Contoured top guided with full port trim. The 1" is chosen over the 3/4" because the valve will control best between 15% - 85% of maximum valve capacity. The 3/4" valve would be operating at 98% of valve capacity.

Actuator Selection:

For temperature control applications, the shut off pressure is the P_1 pressure. Refer to chart 6-1 (Contoured Top Guided) and go to the 1" trim size column. Follow the column until you get to a pressure greater than 125 psig, then follow the row horizontally to determine you need a Model M-00 with a 6 - 18 psig spring range.

Complete valve selection is 1100 series 1" NPT with 1" contoured top guided trim and M-00 actuator with 6 - 18 psig spring range.



Determine the percentage of 'valve open' at any calculated C_{ν}

You must first solve for a required C_{ν} with one of the formulas on page 331. Using sizing example 2, we calculated a C_{ν} of 8.8 and we chose a 1" contoured top guided valve with a full 1" trim with a maximum C_{ν} of 13.

- Step 1: Locate selected valve trim size in the far right-hand column. The maximum $C_{\rm v}$ for this trim can be found by moving two columns to the left.
- Step 2: Locate the calculated C_{ν} (flow coefficient) on the far left side.
- Step 3: Follow calculated C_{ν} to the right until it intersects with the curve associated with the trim size found in step 1.

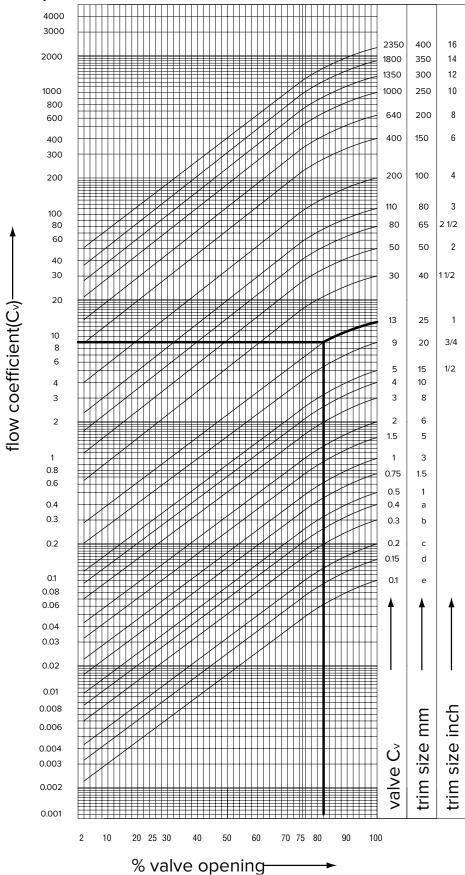
Step 4: From the point of intersection, travel vertically to the bottom of the chart.

This point indicates the percentage of valve open, at the calculated C_{ν} . In this case the valve will operate at 83% of the valves maximum capacity.

The valve has the greatest control between 15 and 85% of the valve opening.



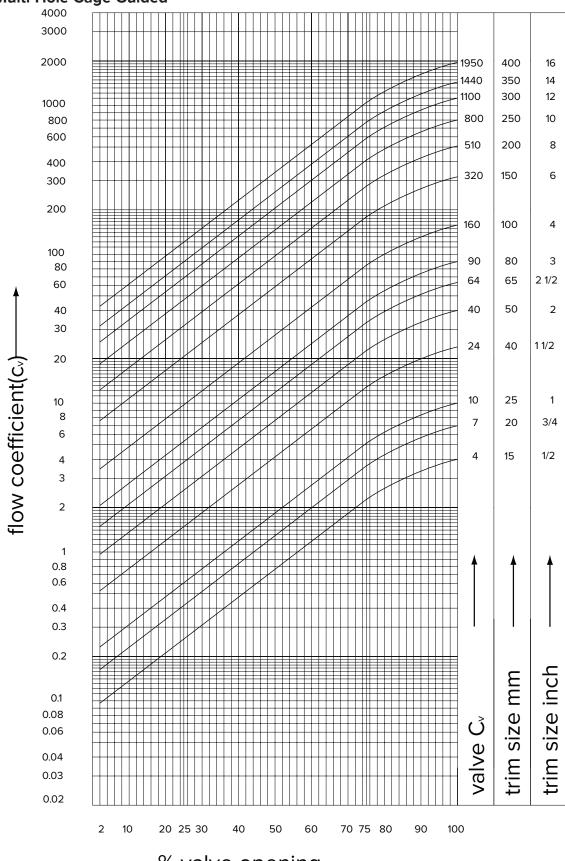
Trim: Contoured Top Bush Guided





Armstrong Python - 1100 Series Control Valve







SRP981 Pneumatic Positioner

The SRP981 positioner is designed to control pneumatic valve actuators with pneumatic control signals. It is used to reduce the adverse effects of valve friction, for higher thrust and shorter positioning time. It offers an easy adjustment by two mechanical screws.

Input:

Signal range: 3 to 15 psig (0.2 to 1 barg) split range down

to Δw 3 psig (0.2 barg)

Response characteristic:

Amplification: adjustable Sensitivity: <0.1% F.S.

Non-linearity (terminal based adjustment): <1.0% F.S.

Hysteresis: <0.3% F.S.

Supply air dependency: <0.3% / 1.5 psig (0.1 barg)

Temperature effect: <0.5% / 10 K

Mechanical vibration: 10-60 Hz up to 0.14 mm 60 - 500 Hz up to 2 g

<0.25% of travel span

Supply:

Supply air pressure: 20 to 50 psig (1.4 to 3.5 barg)

Supply air: free of oil, dust and water according to IEC 654-2

Connection:

Pneumatic: Female threads G 1/8 according to ISO 228

Materials:

Base Plate: Aluminum (Alloy No. 230) finished with

DD varnish

Features

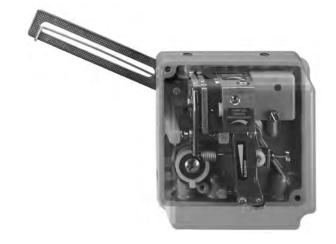
- · Independent adjustment of stroke range and zero
- Adjustable amplification and damping
- Split range up to 4-fold possible
- Input signal from 3-15 psig (0.2-1 barg)
- Supply pressure up to 50 psig (3.5 barg)
- Low vibration effect in all directions
- Ambient temperature -40 to 176°F (-40 to 80°C)
- Protection class IP54 or IP65
- Explosion protection:

II 2 G EEx c (constructive safety) + accessories in

II 2 G EEx i according to ATEX

- · Additional inputs/outputs (optional)
- Position feedback 4 to 20 mA
- Built-in independent inductive limit switches (2-/3 wire) or micro switches
- Accessories
- Booster relay to minimize stroke time
- Gauge manifold
- · Gauges (optional)
- External gauge manifolds
- Integrated gauges
- Indicating ranges:

Input: 0 to 23 psig (0 to 1.6 barg) Output: 0 to 150 psig (0 to 10 barg)





SRI990 Analog Positioner

The analog positioner SRI990 with analog input 4 to 20 mA is designed to control pneumatic valve actuators. The modular structure of this product line enables conversion from an analog to an "intelligent" positioner with HART, Fieldbus or FoxCom.

It offers an easy adjustment by means of switches and potentiometers.

Input

Two wire system

Reverse polarity protection: Built-in standard feature

Signal range: 4 to 20 mA Characteristic of setpoint: linear Operating range: 3 to 21.5 mA

Voltage: DC 6 to 36 V (unloaded circuit)

Load: 300 Ohms, 6 V at 20 mA

Supply

Supply air pressure: 20 to 50 psig (1.4 to 3.5 barg)

Supply air: according to IEC 654-2

Response characteristics

Sensitivity: <0.2% of travel span Non-linearity: <±0.8% of travel span Hysteresis: <0.5% of travel span Temperature effect: <±0.5% / 10 K

Supply air dependence: <0.3% / 15 psig (1 barg)

Mechanical vibration: 10-60 Hz up to 0.14 mm,

60-500 Hz up to 2 g: <0.25% of travel span

Features

- Ambient temperature -40 to 176°F (-40 to 80°C)
- · Additional inputs/outputs (optional):
- Position feedback 4 to 20 mA
- Built-in independent inductive limit switches (2-/3 wire) or micro switches
- Accessories
- Booster relay to minimize stroke time
- Gauge manifold
- Configuration by means of switches and potentiometers
- · Load 300 Ohms
- · Low air consumption
- Supply air pressure up to 50 psig
- · Single acting or double acting
- Mechanical travel indicator
- Reverse polarity protection and interlock diode
- Switch for pneumatic test
- Protection class IP 65 with ATEX and NEMA 4X with FM and CSA
- · Explosion protection:
- II 2 G EEx i/II 2 G EEx n (intrinsic safety) according to ATEX
- Intrinsic safety according to FM and CSA
- Stainless steel housing for offshore or food and beverage applications





SRD991 Intelligent Positioner with HART, PROFIBUS PA, FOUNDATION Fieldbus H1 or FoxCom for EEx ia Intrinsically Safe Applications

The microprocessor controlled positioner SRD991 is designed to control pneumatic valve actuators and can be operated locally or by means of control systems (e.g. the Foxboro I/A Series System). The advanced diagnostic can be partially shown on the local LCD of the positioner or fully on a PC or a DCS workstation with a DTM based software (VALcare or Valve Monitor).

The positioner is available with different communication protocols. This includes versions with analog setpoint (4 to 20 mA) and superimposed HART- or FoxCom signal; digital with FoxCom protocol, or fieldbus communication according to PROFIBUS-PA and FOUNDATION fieldbus H1 according to IEC 1158-2 based on FISCO.

The SRD991 also has the capability to control a Partial Stroke Test(PST) that offers operators a tool to identify the trouble-proof function of ESD (Emergency Shut Down) valves.

Features

Version "Intelligent"

- Autostart with self calibrationg
- Self diagnostic, status and diagnostic messages

Version "Intelligent with Communication"

- Communication HART, FOUNDATION Fieldbus H1, PROFIBUS-PA or FoxCom
- Configuration by means of local keys, Hand Held Terminal, PC or I/A Series system or with an infrared interface by means of IRCOM

Version "Intelligent without Communication"

• Input signal 4-20 mA

Applicable to all SRD991 Models:

- Supply air pressure up to 50 psig (3.4 barg)
- Single or double acting
- Protection class IP 65, NEMA 4X
- Explosion protection:
- II 2 G EEx i / II 2 G EEx n (intrinsic safety) according to ATEX
- Intrinsic safety according to FM and CSA
- Ambient temperature -40 to 176°F (-40 to 80°C)
- Display and Local User Interface:
- Multilingual Full-Text Graphic LCD or LEDs
- Status- and Diagnostic-Messages displayed on LCD
- Easy configuration by means of 3 push buttons
- Mechanical travel indicator
- · Suitable for safety applications up to SIL3
- Partial Stroke Test (PST) for Emergency Shut Down applications
- Infrared Interface for wireless communication
- Stainless steel housing for offshore or food and beverage applications



- · Additional Inputs/outputs (optional):
- 2 binary outputs (limits)
- Position feedback 4 to 20 mA, 1 Alarm output
- 2 binary inputs
- Built-in independent inductive limit switches (2- 3-wire) or micro switches
- Sensors for supply air pressure and output pressure
- Binary Inputs/Outputs dedicated to SIS logic solvers
- Accessories
- Booster relay to minimize stroke time
- Gauge Manifold



43AP Pressure Controller

- 4 to 400% proportional band
- 3-15 psig signal output
- 316 stainless steel spiral pressure element
- Enclosure meets IEC IP53 NEMA Type 3

43AP Temperature Controller

- 4 to 400% proportional band
- 15 Ft. capillary
- 316 stainless steel well with 6" insertion length
- Enclosure meets IEC IP53 NEMA Type 3

Features

- · Wide selection of measuring elements
- · Wide choice of control modes
- Broad range of integral (reset) and derivative adjustments
- Power failures do not influence process driven indication
- Weatherproof construction
- Versatile mounting
- Internal bumpless automatic-manual transfer station

These instruments indicate and control pressure, temperature, vacuum and differential pressure. They provide process industries with a highly dependable and versatile group of instruments.

Accuracy:

Input to pointer: ±0.5% of span for qualified elements. Input to output: Depends on measuring element used.

Repeatability:

0.2% of span

Deadband:

0.1% of span

Ambient Temperature Effect:

Maximum control point shift at midspan per 100°F (55°C) change within normal operating conditions is 1% of input span.

Supply Pressure Effect:

Maximum control point shift at midspan per 1 psig (7 kPa) change within normal operating conditions is 0.2% of input span.





Foxboro/Eckardt Controllers

The 718C Series expands the capability of standard 1/8 DIN controllers with advanced features:

- Modbus serial communication to I/A Series for Windows NT, where data collection capabilities and remote operation are needed.
- · Adaptive Auto-Tune for quick start ups
- Anti-Windup for keeping your batch process under control

The NEMA 4X faceplates allow these units to be used in applications where washdowns and dust conditions exist.

The Soft Start function prevents thermal shock.

Designed specifically for equipment manufacturers who need communications to data aquisition equipment, the light and compact (1/8 DIN size) is able to perform in the most demanding applications with easy yet reliable control.

The 718C Series start-up is as simple as:

- wiring the instrument
- configuring set points and alarm thresholds
- · initiating the autotune function

Engineers, technicians and operators, skilled or unskilled in process control theory, can obtain perfect process control.

Foxboro 718C Electric Controller

- For digital control with universal input and local set point.
 Installed in a fiberglass enclosure with a thermal strip and auto tune instructions.
- One (1) mA output, 3 relays, 2 digital inputs and auxillary power supply for transmitters.
- · No communication
- 24 Vdc, 110 AC, 240 AC power supply



Piston Valves

Description

Armstrong Piston Valves are full port forged steel isolation valves with a maximum operating pressure of 136 Barg/1 973 psig and a maximum operating temperature of 427°C/800°F. The burnished piston and metal reinforced graphite rings provide leak-proof shut off and allow Armstrong Piston Valves to be operated at higher temperatures, while also extending operating life.

Armstrong Piston Valves are available in Socket Weld, BSPT, and NPT end connections. Flanged ends can be supplied upon request.

Armstrong Piston Valves are ideal for saturated and superheated steam, and hot water applications.

Armstrong Piston Valves Feature:

- · Leak-proof isolation
- Sizes from 15mm/1/2" NB to 40mm/1-1/2" NB
- · Choice of socket weld, screwed or flanged end connections
- Compatible with API, ASME, IBR, and DIN standards
- Resistant to cavitation
- All sealing valve components may be easily replaced in-line
- Long-term operation. Piston valve design ensures actuation even after many years without operation
- Fire-proof performance





Ductile Iron hand wheel designed for easy operation.

Four-bolt mechanism with Belleville washers to ensure spring action even in high temperature applications.

Piston stem is fully enclosed to prevent dirt

and corrosion.

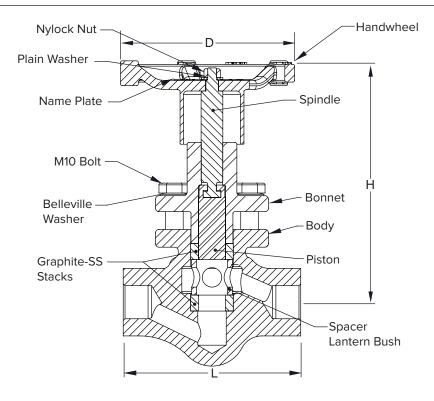
Precision burnished stainless steel pistons provide long-term operation, and ensures actuation even after many years without operation. The piston slides without rotating between the two valve sealing rings, preventing dirt from damaging the surfaces.

ASTM A19 GR B7 bolts for high temperature operation.

Flexible graphite reinforced ring stacks that withstand high temperatures and feature superior mechanical bonding.

Piston Valves





Forged Piston	Valves ANSI Class	A) 008	PI602 &	ASME E	316.34)						
NB/DN	Body Material	ı	L	ŀ	1	D		Minimum	Bolting Type	Approxim	ate Weight
		mm	in	mm	in	mm	in	Thread	0 ,,	kg	lbs
15	A105/LF2	100	3.9	134	5.3	93	3.7	14	4B - SE/SW	1.9	4.2
20	A105/LF2	120	4.7	138.5	5.5	93	3.7	14	4B - SE/SW	3.4	7.5
25	A105/LF2	135	5.3	183	7.2	112	4.4	18	4B - SE/SW	4.8	10.6
40	A105/LF2	185	7.3	226	8.9	112	4.4	19	4B - SE/SW	11.5	25.4

Design Features Forged Steel Piston Valves Class 800 (Sizes 15, 20, 25, 40NB)									
End Connections *	Maximum Pressure at Temperature				Maximum Temperature at Operating Pressure				Hydro Test Pressure at Ambient Temperature
	barg	°C	psig	°F	°C	barg	°F	psig	Ambient lemperature
Socketweld ends	136.20	≤38	1 975.41	100	427	75.84	801	1 099.97	204.30

^{*} Other end connections may have restricted pressure and temperature ratings due to applicable standards.

Design features of Armstrong Piston Valves:

Material of Construction - Body

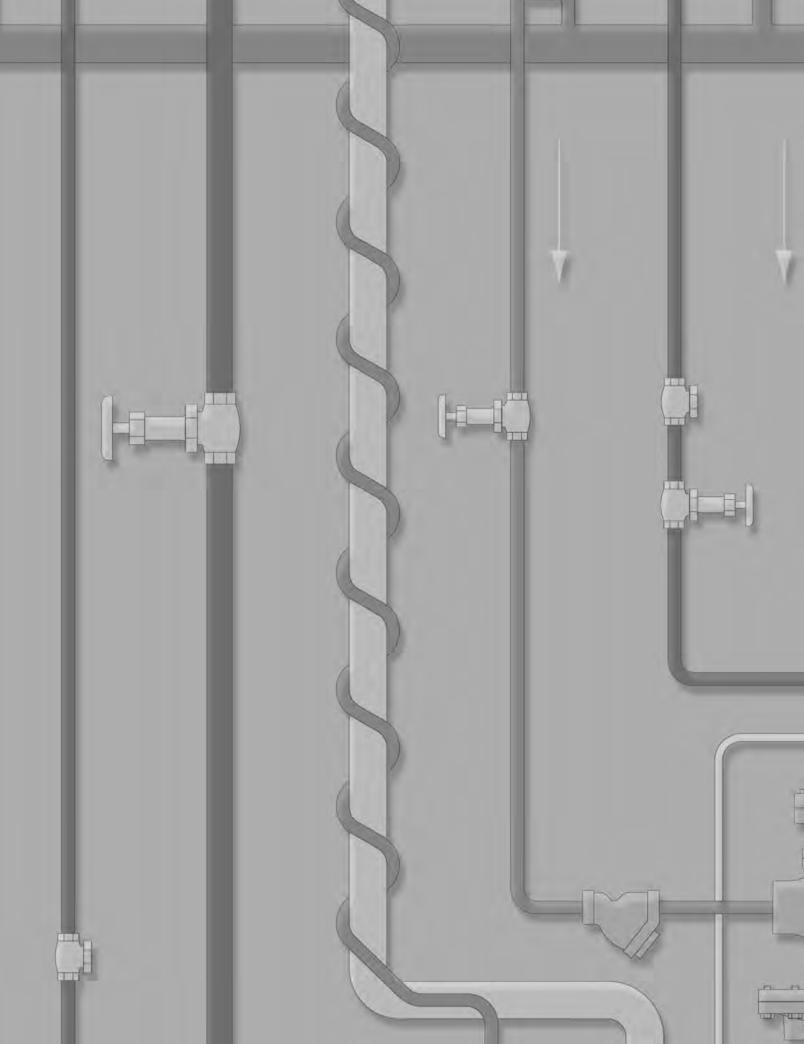
Forged Steel (ASTM A105, ASTM A350 LF2)

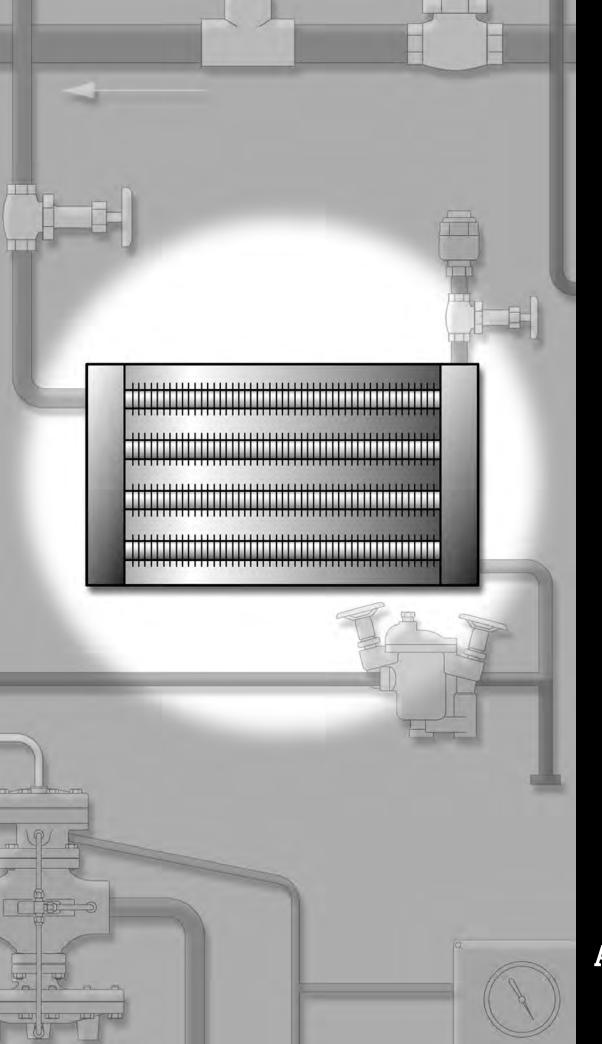
Material of Construction – Graphite Ring Stack

• Flexible Graphite and SS 316

Design Standards

- ASME (B16.34, B16.10, B16.5)
- API (600, 602)
- IBR 1950
- DIN (3202, 10226-1)
- Inspection and testing (API 598)
- · Leak test (ANSI/FCI 70-2)
- Fire test (API SPEC 6FA: 1999)





Heating and Cooling Coils

4rmstrond





Why Leaky Coils Are a Losing Proposition

Leaky coils can be the beginning of the end for efficient heat transfer. Although coils may fail for a variety of reasons, mechanical failure and corrosion are the culprits in the majority of cases. When coils corrode, unwanted moisture and contaminants may foul the air stream or exhaust gases. And a steam leak from a badly corroded coil simply blows precious energy off into the atmosphere.

External corrosion. Contaminants in the airstream cause external corrosion. Dirt buildup intensifies corrosive action by trapping contaminants in concentrated pockets. And it's accelerated when dirt becomes strong airborne mist. Factors such as inappropriate fin pitch, fabricating techniques and material selection may also fuel external corrosion.

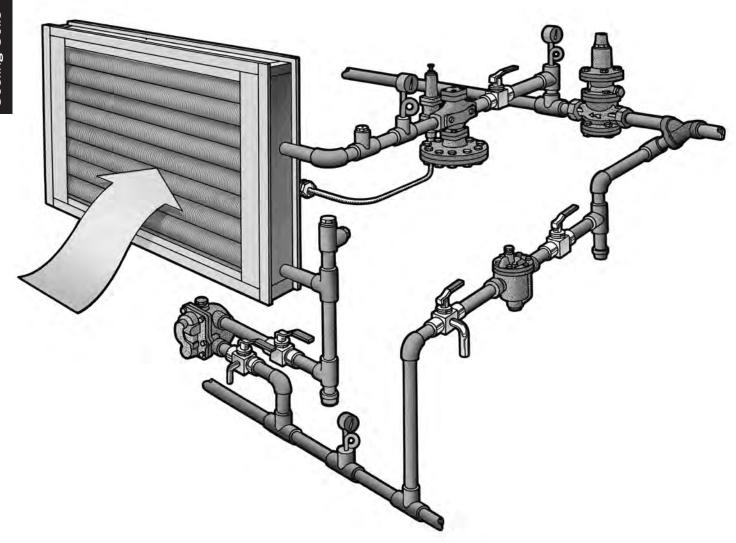
Internal corrosion. Retention of contaminated condensate or inadequate venting of non-condensable gases are major causes of internal corrosion. When CO₂ gas dissolves in condensate that has cooled below steam temperature, it

forms highly corrosive carbonic acid. Likewise, oxygen left to stagnate in the system fosters corrosive action by pitting iron and steel surfaces. Joining pipes/tubes in headers of dissimilar materials may spawn galvanic action. Internal stresses due to improper welding may also hasten corrosion damage.

Armstrong to the Rescue

Armstrong's help in coil selection and design is one of the best defenses against external corrosion. We offer a wide selection of fin pitches to help combat dirt buildup. What's more, sturdy fins lend extra strength to withstand high-pressure cleaning without damage or distortion. As a defense against non-environmental factors, Armstrong fabricates coils in a full range of metals and alloys. You may also specify special coatings to increase external corrosion resistance.

Proper trapping and venting—a specialty of your Armstrong Representative—is where defense against internal corrosion



Why Leaky Coils Are a Losing Proposition



begins. Armstrong reps are steam specialists with more than 75 years of experience in properly sizing, locating and piping steam traps, strainers, vents and related equipment. That's why only Armstrong gives you quality steam coils—plus the installation and trapping help you need to make them work in your total system.

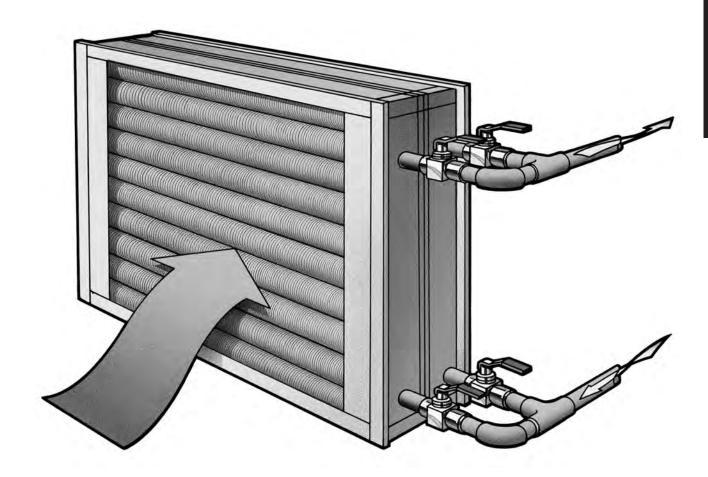
A System to Make Yours More Efficient

Today, the Armstrong "system" merges coil-building experience, practical knowledge and technical know-how from years of trapping coil installations. The result: coils that survive the rigors of high pressures, high temperatures and corrosive conditions.

For example, Armstrong fabricates standard steel heating coils from 1" OD 12 ga ERW Tube (.109" wall) helically

wound with 0.024" thick steel fins at varying fin pitches. Each coil is tested during construction, and the completed unit is again tested hydrostatically to not less than 1.3 times the design pressure with a standard testing pressure at 450 psig for steel or stainless steel cores.

It's this simple: It takes one system to improve another. Exactly how the Armstrong system of product and service carefully matches coils to your specs and applications is the subject of the following pages.





Material Selection for Tubes, Headers and Connections

The choice of tube material depends upon several important factors:

- The corrosive quality of the steam or liquid medium
- The ability to pipe, trap and vent steam coils effectively
- The size and service requirements of the installation
- The external corrosion to which the coils are likely to be subjected

Generally speaking, the heat transfer characteristics of the tube material are of little consequence. The table on the next page illustrates the relative effect of tube materials on overall heat transfer. Because the fin area constitutes the vast majority of the heat transfer surface, it is the most important factor determining heat transfer effectiveness. Therefore, the choice of tube materials should be based on service requirements, not heat transfer efficiency.

Internal corrosion. The base material found in the 6000 Series coils is steel. The minimum wall thickness is .109" for steam coils and liquid coils, which affords both strength and corrosion resistance. All Armstrong coils are of monometallic design, which means that all wetted parts are made of the same materials. This precludes the likelihood of galvanic corrosion often experienced in coils made of dissimilar materials. For most applications, steel will provide very satisfactory service. In order to do this, however, steam coils must be carefully piped, trapped and vented to ensure good condensate and non-condensable gas evacuation.



The cross section of the coil on the right shows how internal corrosion caused by improper piping, trapping and venting may destroy coils from the inside out.

There are many cases where the steam cannot be conditioned enough to be non-corrosive or it is not possible to pipe, trap and vent the coils properly. For those areas, Armstrong recommends stainless steel wetted parts. Choosing which of these is most appropriate depends on the degree and type of problem as well as the steam pressure involved.

External corrosion. In the case of external corrosion, factors concerning the corrosiveness of the airstream enter into the decision. The choice of steel or stainless steel for the wetted parts depends on the compatibility of those materials with the contaminants in the airstream. In addition to the base materials available, Armstrong also offers hot dipped galvanizing, epoxy dip or baked phenolic coatings. These are frequently used when only external corrosion is a consideration.

Service requirements. These may be as important as the above considerations. Coil failures manifest themselves in many forms, but the most prevalent is failure of the tube-to-header joints. This failure occurs as a result of coil design defects, insufficient material at the tube-to-header joints or because of the method of connecting the tubes to the headers.

Armstrong 6000 Series coils are designed to accommodate the service requirements of the particular installation. They are built with enough material at the tube-to-header joints to make them strong. When differential expansion between tubes in steam coils is likely to over-stress the joints, centifeed type coils are recommended. Finally, Armstrong coils are always of welded construction, providing the best method of connecting the two parts together.





Computer-controlled equipment like this simplifies the process of drilling coil headers.

Tube Materials



The best combination of coil materials is the one that delivers maximum heat transfer and service life. Tubes, regardless of material, contribute little to heat transfer in extended-surface coils. It is the fins, fully exposed to the airstream, that provide the greatest contribution to heat transfer. Therefore, choose tube material on the basis of application.

Relative Heat Transfer Capacities of Identical Coils Using Different Tube Materials					
Tube Material	Relative HT Capacity				
Copper	1.00				
Aluminum	1.00				
Steel	.98				
Stainless Steel	.95				

Material Selection for Fins

The heat transfer coil is essentially a tube on which fins are spirally wound or similarly attached. The fins produce an extended surface to improve heat transfer to or from air or other gases passing over the fins. The effective heat transfer of a coil is based on fin pitch (number of fins per inch), fin height, fin material and method of attachment.

Copper fins offer the best heat transfer, but aluminum fins provide the best overall value. Compared to aluminum fins, steel fins reduce heat transfer. Compared to aluminum and steel, stainless steel fins reduce heat transfer significantly. Fins may be of aluminum, copper, steel, or stainless steel, depending on contaminants, operating conditions and economic considerations.

The selection of fin materials should be based upon several considerations:

- · The heat transfer characteristic desired
- The compatibility of the material with the air stream
- The amount and type of particulate matter in the air stream
- The frequency and aggressiveness of coil cleaning

The table below illustrates the heat transfer effectiveness of various fin materials with Armstrong coils. Note that these relative heat transfer capacities are for a specific set of conditions. The factors will vary with different conditions.

The fin/tube combinations available are listed on page 349.

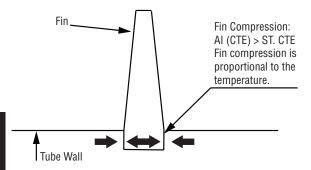
Relative Heat Transfer Capacities of Armstrong Coils With Tubes and Fins of Various Materials*						
Tube Material	Fin Material	Relative HT Capacity				
Steel	Copper Keyfin	1.05				
Steel	Aluminum Keyfin	1.00				
Stainless Steel	Aluminum Keyfin	.94				
Steel	Steel L Fin	.92				
Stainless Steel	Stainless Steel L Fin	.58				

^{*}At 800 ft/min velocity, 7 fins/inch and 300°F steam temperature. Will vary at other conditions.



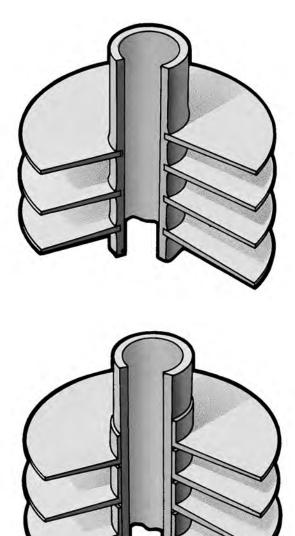
Keyfin

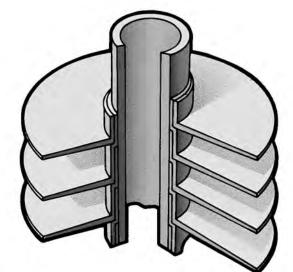
The keyfin is the standard design for Armstrong's most popular coils. Keyfin coils are manufactured by forming a helical groove in the tube surface, winding the fin into the groove and peening the displaced metal from the groove against the fin. This means a tight fit between the fin and the tube, providing for efficient operation over wide temperature ranges. Keyfin is the superior design for dissimilar fin and tube materials.



L Fin

The L fin has a "foot" at its base and is tension wound on knurled tube material. The L-shaped base provides a large contact area between the tube and the fin, ensuring effective, long-lasting heat transfer. The L fin is recommended when tubes and fins are of the same material.





Overlap L Fin

The overlap L fin is simply an L fin with an extended base. Each fin overlaps the foot of the previous fin, completely covering the tube surface. The overlap technique makes it possible to create a completely aluminumized coil for applications where exposed steel would be vulnerable to corrosion.

Why Settle for What's "Available" When You Can Specify Exactly What You Need?



Armstrong manufactures heavy-duty industrial coils in a wide range of sizes and materials to meet virtually any application demand. Dimensionally duplicated to fit your

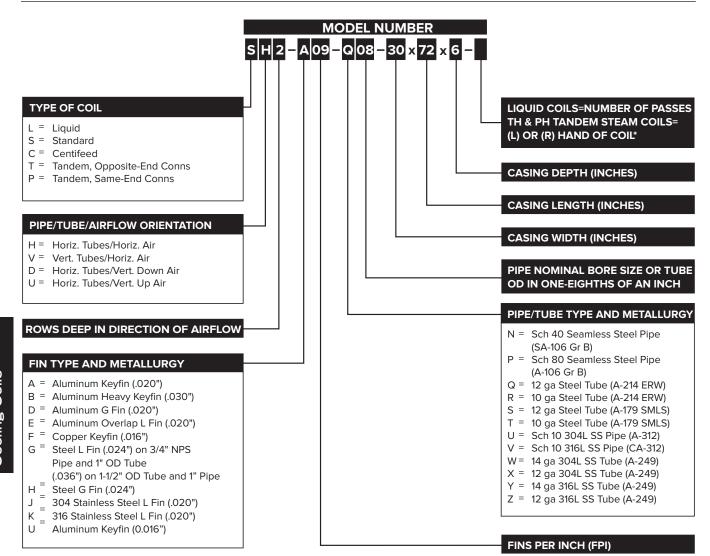
exact requirements, Armstrong coils are what you need. Whether it's off the shelf or off the wall. Other materials will be considered upon request.

		Tubes/Pipes
Carbon Steel Tubes	Standard	12 ga A-214 ERW
	Optional	10 ga A-214 ERW
		12 ga A-179 seamless
		10 ga A-179 seamless
Carbon Steel Pipes	Optional	Sch 80 seamless; A-106 Gr 'B'
Stainless Steel Tubes	Standard	14 ga (1" OD) 12 ga (1-1/2" OD) A-249 type 304L
	Optional	14 ga (1" OD) 12 ga (1-1/2" OD) A-249 type 316L
		Fins
Steel	Standard	0.024" thick on 3/4" NPS pipes
		0.024" thick on 1" OD tubes
		0.036" thick on 1-1/2" OD tubes & 1" NPS & larger pipe
Aluminum	Standard	0.020" thick on all tube sizes
		0.016" thick on 1" OD
	Optional	0.030" heavy keyfin 1" & 1-1/2" OD steel and stainless steel tube
Stainless Steel		0.020" thick type 304 & 316 on all sizes
Copper		0.016" thick on all sizes
		Connections
Steel		Sch 80 (screwed), Sch 40 (flanged)
Stainless Steel		Sch 40 (screwed), Sch 10 (flanged)
		Headers
All coils have headers of the	same material as	tubing and are of welded construction.
		Casing
Galvanized Steel	Standard	Minimum 12 ga galvanized for depth 7-1/2" and over
		Minimum 14 ga galvanized for depth under 7-1/2"
Stainless Steel	Optional	14 ga type 304 & 316 for all depths
Aluminum	Optional	12 ga for all depths
Other gauge material availal	ole on request. All	casings have drilled flanges for duct mounting unless specified otherwise.
		Design Pressure
Standard design pressure for Higher pressure and/or tem -20°F MDMT, lower MDMT a	perature constructi	·
		Testing
All coils are tested hydrosta steel steam coils.	tically to at least 1.3	3 times the working pressure with a standard testing pressure at 450 psig on steel & stainless
-	tically to at least 1.3	3 times the working pressure with a standard testing pressure at 450 psig on steel & stainless Options

epoxy coatings. Coils are available with ASME Section VIII, Division I, "U" stamps or CRN approval.



Model Number Selection Series 6000 Coils



SPECIFY:

Number, Size and Type of Connections

Also call out non-standard items such as: Header Inside or Outside of Casing Special Casing Flange Width and Drilling Airtight Casing

Mounting Plate (removable type)

Coatings, etc.

Number of Inlets

Connection Location

Fluid Circuiting (for Liquid Coil)

*Hand of coil is determined by the position of either the condensate connection or the leaving liquid connection when facing the coil with the airflow to your back.

Steam Coils



For air heating coils, steam is the preferred medium for heat transfer throughout much of industry. It affords advantages over liquids because it is easy and inexpensive to move from the boiler to the point of use and because it gives up so much energy at a constant temperature when it condenses. Process control is easily and quickly accomplished with essentially no lag time as is experienced with liquids.

The selection of coil construction and materials is a multi-step process that must take a number of factors into consideration. Armstrong's line of heavy-duty steam coils is designed and manufactured to provide the long life and efficient heat transfer that pays dividends over a long period of time.

Selection of Steam Coil Circuitry

The following pages show the four types of coil circuits offered by Armstrong and discuss the application parameters of each. The return bend type circuit is not covered because Armstrong feels that one of the four listed circuits is a better choice for most applications.



Armstrong can build coils to a wide variety of material and performance specifications and dimensionally duplicate replacement coils to fit your exact requirements.



Series 6000 Steam Coil Types

Standard Coils (Type S)

This type of coil is used for most applications where entering air temperatures are above 35°F and steam is at constant pressure. It is used extensively in high-temperature process applications and for "reheat" in HVAC systems. It is not, however, recommended where even outlet air temperatures are required immediately after the coil, such as in multi-zone heating systems, or where a modulating steam control valve is used to control temperature.

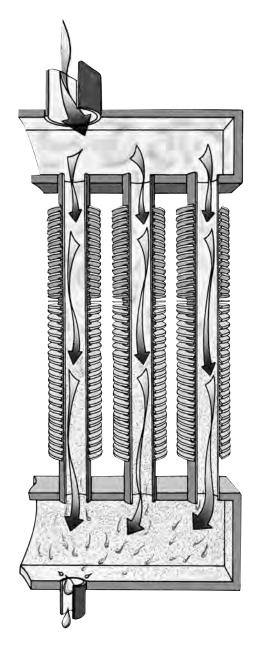
Centifeed Coils (Type C)

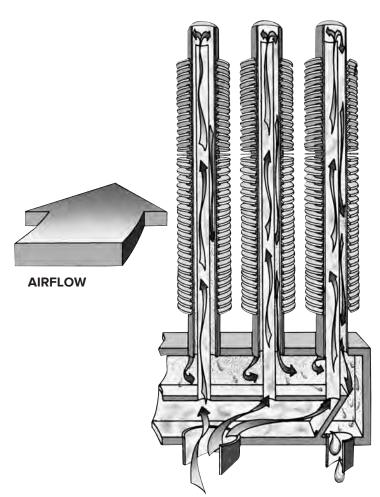
The single-row centifeed coil can be used where air is below freezing and/or modulating control is used. Recommended where:

- A single row delivers the required performance
- B A modulating steam control valve is used
- © Even outlet air temperatures are required over the whole coil face
- D Stainless steel tubes are used

Two-row centifeed coils are available where (B) and (C) are required, but tandem type coils are a better choice with freezing air temperatures.

A centifeed coil is one plain tube—called the inner steam distribution tube—inserted inside an outer finned tube. The center tube is fed with steam, which travels up this distribution tube and is then discharged into the outer tube. It then travels back between the outside wall of the distribution tube and the inside wall of the finned tube to the condensate header. The inner tube acts as a steam tracer to keep the finned tube warm along its total length.





Type S coils are available with opposite-end connections only.

Type C coils are available with same-end connections only.



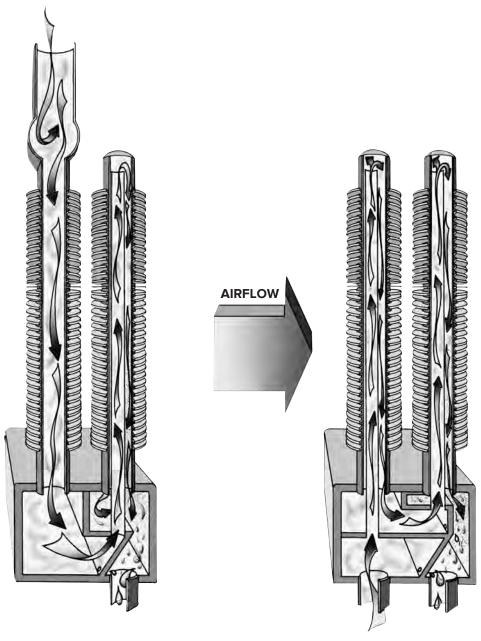
Tandem Coils (Types T and P)

Freezing applications requiring more than one row to achieve the desired final air temperature demand this type of coil.

The coil is designed so that the total amount of steam to be condensed by the whole coil is fed into the first row in the direction of airflow. This purges non-condensable gases and droplets of condensate from that part of the coil exposed to the coldest air. Channeling the steam from the header to the other rows in series has the same purging effect. This design ensures that air passing over the last row is at least 35°F.

The coldest part of the coil will always have steam in sufficient quantity to overcome unequal distribution and "backfeeding" due to differing steam loads and pressure drops in adjacent tubes. This eliminates freezing problems caused by condensate holdup.

The "series" feed characteristic of the tandem coil, as opposed to the "parallel" feed of the two-row centifeed coil, makes it the ideal choice for multi-row coils in freezing applications. If you want a stainless steel tube tandem, specify a P type.



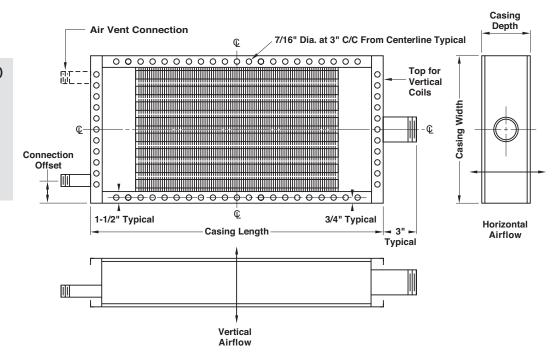
Type T coils have opposite-end connections.

Type P units have same-end connections.

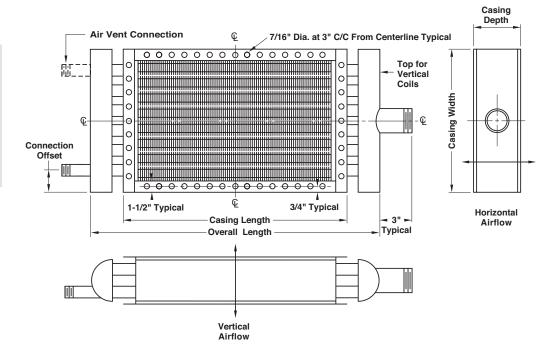


Armstrong Steam Coil Typical Arrangements

- · Standard Coils (Type S)
- · Tandem Coils (Type T)
- For Vertical or Horizontal Airflow
- With Headers Inside the Casing



- · Standard Coils (Type S)
- Tandem Coils (Type T)
- For Vertical or Horizontal Airflow
- With Headers Outside the Casing



NOTES:

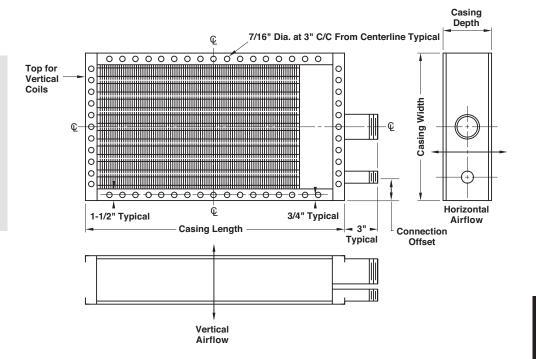
Always specify airflow directions and tube orientation when ordering coils. Specify all dimensions for replacement coils, especially those varying from typicals above. If coils are to be Tandem type, specify coil hand by facing the coil with airflow at your back and pointing to the condensate connection.

Minimum tandem casing depth is 7-1/2", contact factory for details.

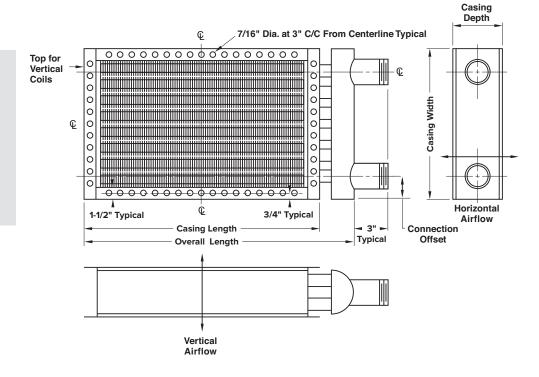
Steam Coil Typical Arrangements



- Centifeed Coils (Type C)
- Centifeed Tandem Coils (Type P)
- For Vertical or Horizontal Airflow
- With Headers Inside the Casing



- Centifeed Coils (Type C)
- Centifeed Tandem Coils (Type P)
- For Vertical or Horizontal Airflow
- With Headers Outside the Casing

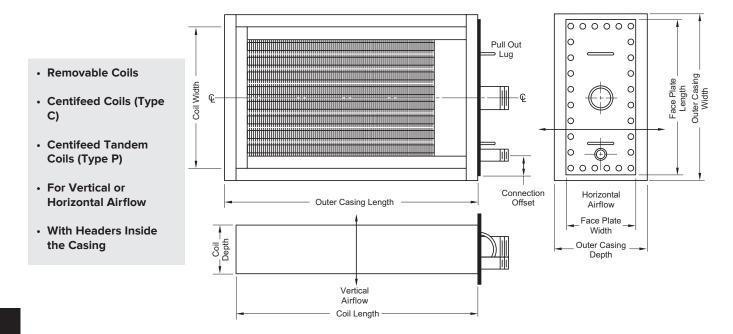


NOTES:

Always specify airflow directions and tube orientation when ordering coils. Specify all dimensions for replacement coils, especially those varying from typicals above. If coils are to be Tandem type, specify coil hand by facing the coil with airflow at your back and pointing to the condensate connection.

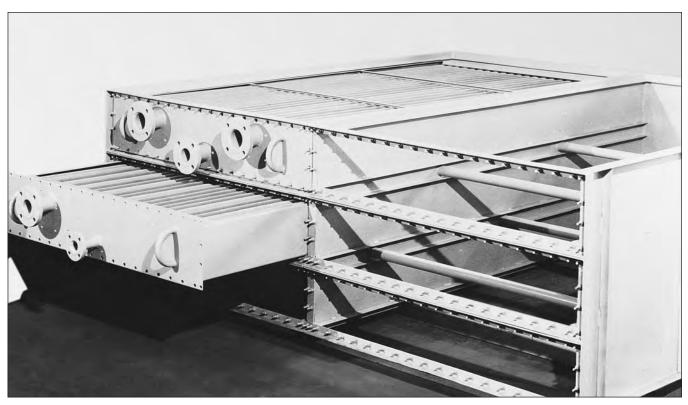


Armstrong Steam Coil Typical Arrangements



NOTES: Always specify airflow directions and tube orientation when ordering coils. Specify all dimensions for replacement coils, especially those varying from typicals above. If coils are to be Tandem type, specify coil hand by facing the coil with airflow at your back and pointing to the condensate connection.

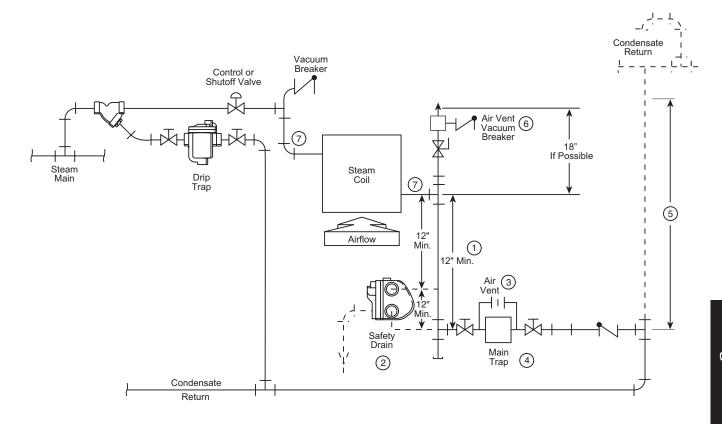
Removable coils can be designed for removal from either connection end or end opposite connections.



Removable coils with outer casing (removable from connections end configuration shown above).

Recommended Piping Practices for Steam Heating Coils





- 1. 24" minimum if safety drain is used.
- Safety drain is used if steam supply is modulated and the condensate system is pressurized or overhead. Armstrong's pumping traps or Posi-Pressure Control system provides additional protection or may substitute for the safety drain, especially if condensate conservation is desired.
- 3. Air venting must be provided on all steam coils except those using low-pressure Posi-Pressure Control systems. The air vent may either be an orifice bleed or a thermostatically operated element, with the orifice bleed being the preferred choice. The air vent or orifice bleed should be piped so that it cannot be valved out independently of the trap.
- 4. The main trap may be either an inverted bucket or a float & thermostatic type depending upon the service conditions. See the chart below for recommendations. Inverted bucket type steam trap required with Posi-Pressure Control system.
- 5. Overhead condensate return system.
- 6. Required only on a modulated system.
- Provide a flexible connection or swing joint at the coil inlet and outlet connections to isolate the coil from vibration, piping stresses and differential expansion within the coil.

NOTE: See Bulletin AH-825 for detailed operation and maintenance procedures. Recommended practice valid for all steam coils (Duralite, Series 6000 and Duramix.)

Armstrong Steam Trap Selection Guide							
Equipment	Selections	Constant	Pressure	Modulated Pressure			
		0 - 30 psig	Above 30 psig	0 - 30 psig	Above 30 psig		
I la it I la ataux	1st Choice	IBLV	IBLV	F&T	F&T		
Unit Heaters	2nd Choice	F&T	F&T	IBLV	IBLV		
Air Handlers	1st Choice	IBLV	IBLV	F&T	F&T		
All Halldleis	2nd Choice	F&T	F&T	IBLV	IBLV		
		0 - 250 psig	Above 250 psig	0 - 30 psig	Above 30 psig		
Dranna Caila	1st Choice	IBLV	IBLV	F&T	F&T		
Process Coils	2nd Choice	F&T	IBLV	IBLV	IBLV		
Duramix	1st Choice	IBLV	IBLV	Not Reco	mmended		



Steam Coil Sizing

		Represent	tative:			
alesperson:		Application:				
ustomer:		Customer	Customer Location:			
erformance Requirem	nents					
Air Flow Quantity	□SCFM	□ACFM	□lb/hr (check o	one)		
Altitude	feet above	sea level				
Humidity Ratio	lb. moisture	e/lb. dry air (prod	cess applications	only)		
Design Entering Temp	perature°I	=				
Design Leaving Temp	erature°I	=				
Steam Pressure at the	coil(s)	_ psig	□psia			
Steam Pressure	■Modulated	□Constan	t			
Maximum Air Pressure	e Drop in wg	J				
Special Requirements	Not Covered Abo	ve				
ystem and Coil Config	guration Requ	uirements				
ystem and Coil Config Air Flow Direction:	guration Requ □Horizontal	uirements □Vertical UP	□Vertical DC	WN (check one)		
•	•	□Vertical UP		WN (check one)		
Air Flow Direction:	□Horizontal □Before Coils	□Vertical UP		,		
Air Flow Direction: Fan Location:	☐ Horizontal ☐ Before Coils ☐ Horizontal	□Vertical UP □After Coils (c □Vertical	heck one) □Optional (c	,		
Air Flow Direction: Fan Location: Coil Tube Orientation:	☐ Horizontal ☐ Before Coils ☐ Horizontal	□Vertical UP □After Coils (c □Vertical	heck one) □Optional (c	heck one)		
Air Flow Direction: Fan Location: Coil Tube Orientation: Type of Coil:	□Horizontal □Before Coils □Horizontal □Standard □C □MPT	□Vertical UP □After Coils (c □Vertical entifeed □Tal □FPT	heck one) Optional (c ndem Centife	heck one)		
Air Flow Direction: Fan Location: Coil Tube Orientation: Type of Coil: Connection Type:	□Horizontal □Before Coils □Horizontal □Standard □C □MPT	□Vertical UP □After Coils (c □Vertical entifeed □Tal □FPT □Same End	heck one) Optional (c ndem Centife	heck one) eed-Tandem □Optional		
Air Flow Direction: Fan Location: Coil Tube Orientation: Type of Coil: Connection Type: Connection Location:	□Horizontal □Before Coils □Horizontal □Standard □C □MPT □Opposite End	□Vertical UP □After Coils (c □Vertical entifeed □Ta □FPT □Same End □304L Stainles	heck one) Optional (c ndem Centife Flanged Optional ss 316L Stainle	heck one) eed-Tandem □Optional ess (check one)		
Air Flow Direction: Fan Location: Coil Tube Orientation: Type of Coil: Connection Type: Connection Location: Tube Material:	□Horizontal □Before Coils □Horizontal □Standard □C □MPT □Opposite End □Steel	□Vertical UP □After Coils (c □Vertical entifeed □Ta □FPT □Same End □304L Stainles	heck one) Optional (c ndem Centife Flanged Optional ss 316L Stainle	heck one) eed-Tandem □Optional ess (check one)		
Air Flow Direction: Fan Location: Coil Tube Orientation: Type of Coil: Connection Type: Connection Location: Tube Material:	□Horizontal □Before Coils □Horizontal □Standard □C □MPT □Opposite End □Steel □0.020" Aluminu □0.016" Copper	□Vertical UP □After Coils (c □Vertical entifeed □Tal □FPT □Same End □304L Stainled Im Keyfin □ Keyfin □	heck one) Optional (condem Centife Planged Optional Stainle Conden Cond	heck one) eed-Tandem		

Cooling Coils

Steam Coil Sizing

Replacement for Existing Coils



Date:	Representative:
Salesperson:	Application:
Customer:	Customer Location:
Performance Requirements	
Air Flow Quantity DS	CFM □ACFM □lb/hr (check one)
Altitude feet al	pove sea level
Humidity Ratio lb. mo	isture/lb. dry air (process applications only)
Design Entering Temperature	°F
Design Leaving Temperature	°F
Steam Pressure at the coil(s)	□psig □psia
Steam Pressure	ted □Constant
Maximum Air Pressure Dropi	in wg
Special Requirements Not Covered	Above
System and Coil Configuration (E	Existing Installation)
Air Flow Direction: ☐Horizontal	□Vertical UP □Vertical DOWN (check one)
Fan Location: ☐Before Coi	ls □After Coils (check one)
Coil Tube Orientation: ☐Horizontal	□Vertical □Optional (check one)
Type of Coil: ☐Standard	□Centifeed □Tandem □Centifeed-Tandem □Optional
Connection Type: ☐MPT ☐F	PT □Flanged Inlet: inches Outlet: inches
Connection Location: ☐Opposite E	End □Same End □Optional
Tube Material:	
Fin Material:; Fin Thickne	ess: in; Fins/in (count spaces)
Fin Type: □Plate	□Spiral Wound □Extruded □Welded
Number of Rows of Tubes in Each O	Coil: □One □Two □Three □Other
Number of Coils of Parallel;	Number of Coils in Deep in Airstream
Coils to be: □Duct Moun	ted □Removable with Outer Case □Core Only(check one)
Special Requirements Not Covered	Above
Cail Barrainana anta (Barria anno ant	L C - 'I'
Coil Requirements (Replacement	·
	□Centifeed □Tandem □Centifeed-Tandem □Optional
Connection Location: Opposite E	
Tube Material: ☐Steel	□304L Stainless □316L Stainless (chek one)
	minum Keyfin
	pper Keyfin □Steel/L-Fin □Stainless Steel/L-Fin
Special Requirements Not Covered	Above



Installation, Operation and Maintenance Instructions

In steam coils, successful operation and a long, trouble-free service life depend on:

- The manner of installation, including the design of coil mounting and piping—with particular emphasis on trapping and air venting.
- 2. Operating conditions that are within design parameters.
- 3. The method of operation.
- 4. The thoroughness and frequency of cleaning required.

Following these simple guidelines will help you achieve maximum coil performance.

Receipt and Storage

- Upon receipt, inspect coils and notify carrier immediately of an damage sustained in transit.
- If coils are not installed immediately, store under cover in a heated area free of potential damage from personnel and/or equipment.

Installation

- Support coils and piping individually to prevent undue strains on the steam and condensate connections. Use swing joints or flexible connections for freedom of movement.
- Steam and condensate pipes should be the same size as coil connections. Maintain connection size from the coil back to the steam main and from the coil to the steam trap takeoff.
- Install a drip trap prior to the coils (and before a control valve if there is one) to prevent the introduction of condensate.
- Install strainers with blowdown valves before all control valves and traps.
- To avoid hunting and maintain control, use only modified linear or equal percentage (vee-port) valves when a modulating control valve regulates the steam supply. Consult Armstrong for proper applications.
- 6. Never oversize control valves. Bigger is NOT better.
- 7. Install a vacuum breaker in the steam piping prior to the coil to prevent retention of condensate during shutdown. Also install a vacuum breaker on the downstream side of the coil when steam pressure is to be modulated. If you use check valves as vacuum breakers, they should be 15-degree swing checks.
- Provide venting of non-condensable gases individually on each coil to ensure maximum heat transfer and minimum internal corrosion. In order of effectiveness, venting can be with a fixed orifice bleed, independent thermostatic vent or by using a float and thermostatic steam trap.
- Trap all coils individually. Locate trap as close to coil as possible. Otherwise, inadequate drainage may damage the coil and/or interfere with effective heat transfer.
- 10. Use only traps such as the inverted bucket or float and thermostatic which drain continuously. When steam to the coils is modulated, a float and thermostatic trap is preferred. See the previous page for selection guidelines.

- 11. Install a dirt pocket prior to the steam trap. You may also install a gate valve at the bottom of the dirt pocket to facilitate drainage during shutdown periods.
- 12. Use the same size trap on all coils when they are in parallel across the duct opening. Coils mounted in series (one behind the other in the direction of the airflow) typically have lower condensing rates at the downstream end of the system. Size traps to handle the maximum calculated load for individual coils. Avoid oversizing. Consult your Armstrong Representative if you need assistance.
- 13. Modulating control valves are best used with gravity flow vented condensate return systems. If the condensate return system is overhead or pressurized, the use of pumps, Armstrong pumping traps or the Armstrong Posi-Pressure Coil Controller System is highly recommended. If this is not possible a safety drain as illustrated on page 357 should be installed.
- 14. Install filters at the coil inlet if possible. Simple filter systems permit easy cleaning or replacement and ensure efficient operation.
- 15. Refer to the previous page for an illustration of piping practices for steam heating coils.
- 16. Provide uniform air velocity and uniform air temperature at the face of the coil. This is very important for good coil performance.

Operation

Once coils are installed properly, their performance and service life depend on a few simple guidelines for maintenance and operation.

- To prevent plugging of tubes, clean the piping system and blow down all strainers prior to initial startup.
- On startup, feed steam to the coils slowly to avoid thermal shock loadings.
- 3. Make sure the steam has been on for a minimum of 15 minutes prior to starting fans or opening dampers.
- 4. Make sure operating pressures are kept within design limits.
- During initial startup, tighten all bolted connections once the system stabilizes at operating temperature.
- To provide maximum freeze protection, maintain a minimum steam pressure of 5 psig to coils exposed to air temperature below 40°F (5°C). If this is impossible, consult your Armstrong Representative.
- 7. Drain during shutdown to prevent internal corrosion.

Maintenance

- If filters are installed, clean regularly to maintain adequate airflow across the coils and to keep fan loadings at design.
- If filters are not used, inspect and clean coils periodically. Clogged filters and plugged coils have the same result.

Liquid Coils



Although steam may be the preferred heating medium for coils, liquids such as water, glycol solutions and high temperature heat transfer fluids are coming into wide use. Some of the reasons for the popularity of water and glycol systems are:

- Heat recovery systems are becoming more popular, and hot water or glycol solutions are ideal for that duty
- Hot water may be readily available from such sources as condensate systems or other processes, and it makes sense to use the available heat from those sources
- Users have a preference for liquids over steam

The use of high temperature heat transfer fluids has a number of practical advantages over water and steam when process air has to be heated to high temperatures. These fluids can operate in the 500°F to 750°F range at or near atmospheric pressure as opposed to steam, which would have to be over 1 500 psig in order to achieve a saturation temperature of 600°F.

Systems capable of operating at high pressures are expensive to construct and maintain. Corrosion caused by steam and water and the need for water treatment to minimize scale formation result in high maintenance costs. The absence of any need for supervisory staff to be on constant duty is a further advantage of the high temperature heat transfer fluid system.

To meet the needs of industry for heavy duty liquid coils, Armstrong has introduced a line of standardized sizes in seven widths from 16-3/4" to 57-3/4" in 21 lengths from 24" to 144". These are available with fin pitches from 5 to 11 FPI and in 2 or 3 rows. Many circuiting options are available.

As with all Armstrong coils, liquid coils are built to withstand the rigors of tough industrial applications in contrast to the commercial grade coils frequently misapplied in industrial environments.

In addition to the standardized line, custom coils in sizes to fit existing installations and in materials to fit particular applications are also available.

Materials of C	Construction
Tubes	1" OD 12 ga (109" wall thickness) A-214 ERW carbon steel tubes (seamless tubes optional), 10 ga tube also available.
Fins	.020" or .030" thick aluminum keyfin (imbedded).
Headers	Schedule 40 steel or fabricated.
Connections	Water and glycol solutions: • Schedule 80 steel screwed MPT (flanges optional) — same end High temperature heat transfer fluids: • Seamless Schedule 40 steel with 300 lb raised face weld neck flanges—same end
Assembly	All wetted parts are welded into a monometallic structure, affording the greatest strength and corrosion resistance.
Design	250 psig at 750°F. Hydrostatically standard testing pressure at 450 psig.
Casing	Minimum 14 ga galvanized steel primed after manufacture.
Coatings	Special coatings such as baked phenolic or epoxy powder are available as options. These coatings are suitable for temperatures up to 400°F.



		_ Represer	ntative:
sperson:		Application:	
mer:		Customer Location:	
ormance Requirem	ents		
Air Flow Quantity	□SCFM	¶ □ACFM	□lb/hr (check one)
Altitude	feet above	sea level	
Humidity Ratio	lb. moistur	e/lb. dry air (pro	ocess applications only)
Design Entering Temp	erature°	F	
Design Leaving Temp	erature°	F	
Liquid Type			
Entering Liquid Tempe	erature°	F	
Leaving Liquid Tempe	rature°	F (or liquid flow	v rate gpm)
Liquid Characteristics	at Average Liquid	Temperature:_	
Specific Gravity:			
Specific Heat:			
Viscocity:		□lb/ft-hr (che	ck one)
Thermal Conductivity			
Special Requirements	Not Covered Abo	ve	
em and Coil Config	guration Requ	uirements	
Air Flow Direction:	□Horizontal	□Vertical UP	□Vertical DOWN (check one)
Fan Location:	☐Before Coils	□After Coils ((check one)
Coil Tube Orientation:	□Horizontal	□Vertical	□Optional (check one)
Tube Material:	□Steel	□304L Stainle	ess 316L Stainless (chek one)
Fin Material:	□0.020" Aluminu	um Keyfin	□0.030" Aluminum Keyfin
	□ 0.016" Copper	Keyfin	□Steel □Stainless Steel
Coils to be:	☐Duct Mounted	■Removable	with Outer Case (check one)

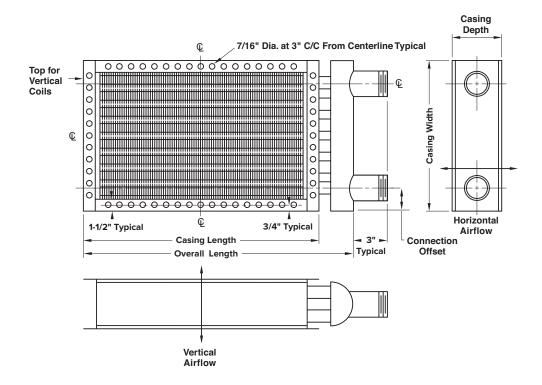
leating and coils

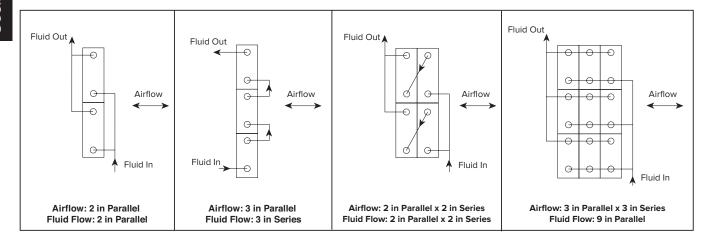
Liquid Coil Sizing

Replacement for Existing Coils



Date:	Representative:	
Salesperson:	Application:	
Customer:	Customer Location:	
Performance Requirements		
Air Flow Quantity □SCFM	□ACFM □Ib/hr (check one)	
Altitude feet above sea	level	
Humidity Ratio lb. moisture/lb.	dry air (process applications only)	
Design Entering Temperature °F		
Design Leaving Temperature °F		
Liquid Type		
Entering Liquid Temperature °F		
Leaving Liquid Temperature°F (or	liquid flow rate gpm)	
Liquid Characteristics at Average Liquid Ten	nperature:	
Specific Gravity:		
Specific Heat:		
Viscocity: □cp □It	o/ft-hr (check one)	
Thermal Conductivity		
Special Requirements Not Covered Above		
System and Coil Configuration (Existing	g Installation)	
Air Flow Direction: ☐Horizontal ☐V	ertical UP □Vertical DOWN (check one)	
Fan Location: ☐Before Coils ☐A	fter Coils (check one)	
Coil Tube Orientation: ☐Horizontal ☐V	retrical □Optional (check one)	
Fluid Circuit:		
Connection Type: ☐MPT ☐FPT ☐F	langed Inlet: inches Outlet: inches	
Connection Location: ☐Same End ☐C	Optional Connection Size: inches	
Tube Material:		
Fin Material:; Fin Thickness:	in; Fins/in (count spaces)	
Fin Type: □Plate □S	piral Wound Extruded Welded	
Number of Rows of Tubes in Each Coil: 🔲 🔾	one □Two □Three □Other	
Number of Coils of Parallel; Number	of Coils in Deep in Airstream	
Coils to be: □Duct Mounted □R	removable with Outer Case	
Special Requirements Not Covered Above		
Coil Requirements (Replacement Coil)		
Type of Coil: □Standard □Centi	feed 🗆 Tandem 🗅 Centifeed-Tandem 🗅 Optional	
Connection Location: Opposite End S	ame End	
	04L Stainless □316L Stainless (chek one)	
Fin Material: □0.020" Aluminum K	eyfin 0.030" Aluminum Keyfin	
	in Steel/L-Fin Stainless Steel/L-Fin	





Casing Width: _____

Casing Depth:_

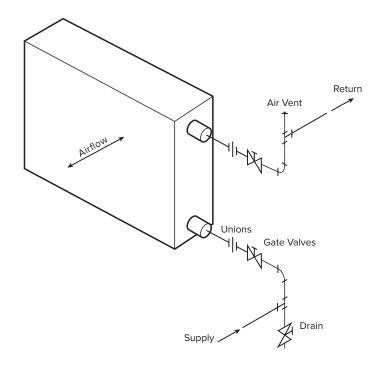
Note: Casing width is always measured along the header.

Casing length is always measured along the tube length

Hole sizes and placement are Armstrong standards. Please not variances.

Piping Diagram for Water and Ethylene Glycol



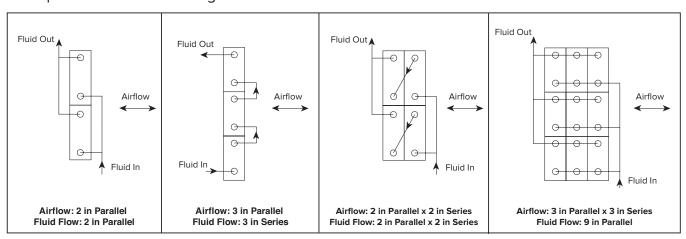


- 1. Install coils level to assure complete drainage.
- 2. Supply water to the bottom connection and return through the top connection.
- Carefully vent coils, either individually or through an air manifold.
- 4. Armstrong recommends that coil isolation valves be fitted to take out coils without disturbing the whole system.
- Ensure that water supply to coils is as clean as possible to avoid potential blockage and excessive fouling. Settling tanks and strainers can be used for this purpose.

- Do not support piping from the coils. Install adequate hangers and expansion joints to prevent undue stresses.
- Armstrong recommends the use of low pressure air or flushing with ethylene glycol to prevent freeze damage when draining.
- 8. Do not use throttling controls in hot water heating service if there is a possibility of below-freezing air passing through the coil. Use an air by-pass system at full water flow rate for control.

NOTE: Keep finned tube surface clean and free of all foreign matter in order to maintain the design heat transfer and pressure drop ratings. Install filters upstream of the coils to keep actual coil maintenance to a minimum.

Examples of Multi-Coil Arrangements





How to Specify Armstrong Series 6000 Steam Coils

Heavy-duty construction/fabrication is why Armstrong Series 6000 coils last longer, saving maintenance and frequent replacement costs.

Think about it. Less expensive coils are also less durable and are commonly misapplied in heavy industrial service. As a result, they actually become more expensive when measured by down time, maintenance and replacement over a period of time. It's really a very simple fact: Higher initial costs are

justified when they secure a lower life cycle cost.

The sample specifications below will help you in detailing coil construction for your heavy-duty application. These samples cover the most popular of the various material combinations. For assistance with other options, consult your Armstrong Representative.

Steel Tube/Aluminum Keyfins

- Tubes-minimum 12 ga carbon steel
- Fins—minimum 0.020" thick aluminum (imbedded type)
- · Headers—minimum Sch 40 carbon steel pipe
- Connections—minimum Sch 80 carbon steel pipe
- · Casings—minimum 14 ga galvanized steel
- Tubes, headers and connections shall be welded together to form monometallic joints.

Steel Tube/Steel Fins

- Tubes-minimum 12 ga carbon steel
- Fins-minimum 0.024" thick carbon steel ("L" fin)
- · Headers-minimum Sch 40 carbon steel pipe
- Connections—minimum Sch 80 carbon steel pipe
- Casings—minimum 14 ga galvanized steel
- Tubes, headers and connections shall be welded together to form monometallic joints.

Stainless Steel Tube/Aluminum Fins

- Tubes-minimum 14 ga 304L stainless steel
- Fins—minimum 0.020" thick aluminum (imbedded type)
- Headers—minimum Sch 10 304L stainless steel pipe
- Connections—minimum Sch 40 304L stainless steel pipe Casings—minimum 14 ga galvanized steel
- Tubes, headers and connections shall be welded together to form monometallic joints.

NOTE: 0.030" thick aluminum keyfin is an available option for imbedded type only.

Typical Coil Applications

Armstrong can manufacture coils in any configuration necessary to meet your requirements.

- Pulp dryer coils
- · Veneer dryer coils
- · Pocket ventilation coils
- · Smokehouse coils
- Yankee hood drying coils
- · Pasteurizer coils
- · Air makeup coils for comfort heating
- · Char coolers
- · Carpet dryer coils
- · Boiler air preheater coils
- · Grain dryer coils
- · Boiler feedwater runaround systems

- Starch dryer coils
- · Textile dryer coils
- Dry kiln coils
- · Paint spray booth coils
- Drying ovens
- Steam condenser coils
- · Unit heaters for comfort heating
- · Door heaters
- Tank heating coils
- · Unit coolers and condensers
- Fluid Bed Dryers
- · Direct Contact Fluid Bed Dryers

Coil Packages Engineered to Your Specifications





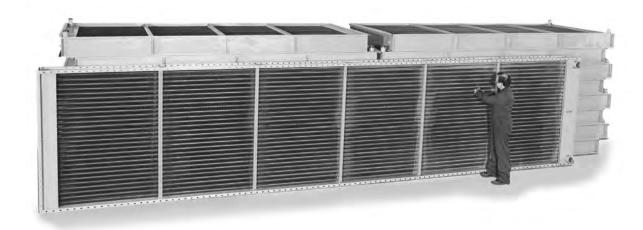


Blast air coolers and heaters.

Air heaters using high pressure steam.



Stainless steel boiler air preheaters used in the pulp and paper industry.



Air heaters using thermal oils.



Quality Construction

"Designed to Perform & Built to Last"

Armstrong Preheat Coils outlast thin-finned and thin-walled lightweights because of superior engineering and robust construction. Thicker tube walls and fins provide greater resistance to coil damage and wear from high pressures, temperatures and corrosive conditions.

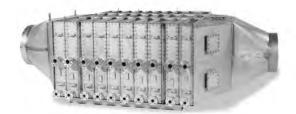
Armstrong's Typical Heavy Duty Air Heater Specifications:

- Fins Keyfin Embedded, Spiral Wound Aluminum or Copper
- Fin Thickness Minimum 0.020" thickness or optional 0.030" Heavy Keyfin
- Tubes 1" OD x 12 Ga Carbon Steel or 14 Ga St.Stl. (1-1/2" OD Available)
- Inner Tubes 1/2" 7/8" OD Carbon or St. Steel (no perforations or holes)
- · Headers Heavy Wall (Carbon Steel or St.Steel) Fabricated
- Tube/Header Joints All Welded Multi-Pass Full Penetration
- Tube Sheets NC Machined, and Chamfered Tube Holes -Heavy Gauge
- Mono-Metallic Construction on all wetted parts reducing potential for galvanic corrosion
- Coil Casings Min 14ga or 12 Ga Galvanized Steel or St. Steel
- Outer Casings Drawer Type Construction with Airtight Outer Casings for ease of coil removal or replacement
- Cleanout/Inspection/Access Spacer Sections Available on request
- Inlet/Outlet Transitions Per Specification
- Pre-Piped Options On Application
- Extended Warranties Available on Application
- Design and Construction in Accordance with ASME SECTION VIII Div. 1. (All Armstrong 6000 Series Coils are built to this standard whether or not ASME is required - unlike other manufacturers).
- U Stamp Available on request
- Special Materials and Coatings available on request
- Manufacturing done in Armstrong factories, not subcontracted. Armstrong controls all QA/QC in-house.

Whether you need a standard replacement coil or custom-built unit, you'll get the same built-in quality.

During construction each section of the coil is checked for compliance with detailed, written QA/QC procedures available for your review. And, finally the complete coil is tested hydrostatically to ASME standards.

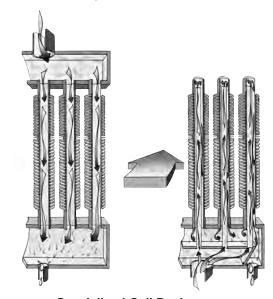
Armstrong offers total steam expertise and manufacturing capability that can help you identify and solve coil problems. In addition, Armstrong's steam system package approach is a blueprint for blending superior products, knowledge and judgment into plans for effective energy management and pinpointing Heat Rate improvements.



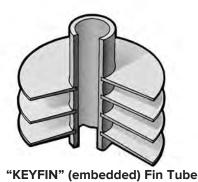
Full Systems with Transitions



Drawer Type Air Preheat Coils



Specialized Coil Designs





Solutions Through Experience.

For power and large industrial plants, producing electricity, generating steam, energy efficiency, air preheating and protection of important heat transfer equipment and systems, go hand in hand. Coordinating design and performance of various system components requires a review of the entire energy usage loop from turbine extraction, through air preheating, to condensate collection, return, and re-use of available flash energy and hot condensate.

Combustion and boiler air preheating is no longer just a simple need to heat air to prevent dew point issues on tubular or regenerative air pre-heater surfaces. The advent of SCR's, SNCR's, WET/DRY SCRUBBERS – FGD'S, BAGHOUSE UPGRADES, AND STACK GAS REHEATING, have positioned the steam or fluid coil air pre-heater as a key component to the overall combustion efficiency and equipment life extension planning.

For more than a century, Armstrong has been synonymous with steam system innovation and solutions. Armstrong understands efficient generation and effective use of steam throughout the power/utility, large industrial boiler operations, from Coal/Fossil fired, through Biomass, Hog Fuels, Black Liquor Recovery (B.L.R.B.) and Fluid Bed designs to packaged fire tube boiler requirements.

Combustion air preheating heat source options we work with include, extraction or auxiliary steam source, thermal oils, glycol or hot water (from d/a etc.).

Armstrong leads the industry in rugged, robust coil designs that extend life of equipment and reduce downtime and lost energy production hours. With reduced staffing in most facilities, you can relax and focus on your base operations and be assured that the systems we provide will deliver years of continuous, optimized performance.

ARMSTRONG IS ALSO THE ONLY GLOBAL
MANUFACTURER WITH THE ABILITY TO SUPPLY KEY
SYSTEM COMPONENTS INCLUDING STEAM SUPPLY
CONTROL VALVES, HEAVY DUTY COILS, CONDENSATE
TRAPPING, VENTING COLLECTION AND RETURN SYSTEMS
FROM THE SAME CORPORATE SOURCING! THIS MAKES
ARMSTRONG YOUR ONE-STOP SOLUTION SOURCE!

Armstrong partners are air preheat and coil system specialists.

Combine our combustion air preheat coil-building know-how with the expertise of a decades-old steam specialist and what do you get? Preheat coils specifically designed for the rigors of power plant applications.

Armstrong: The power to improve on every energy front.

Why add Armstrong to your energy team? Our applications expertise in the key areas of combustion air preheating and efficient use of extraction steam and flash recovery is well documented. Our steam trapping and condensate recovery/ handling knowledge in both saturated and superheated steam applications extends over 100 years. Even your HVAC, plant heating/cooling and hot water requirements are within the scope of the products and services from Armstrong.

Armstrong is a problem solver.

At Armstrong, we consider the entire system. We don't simply duplicate the coils within it. Flexibility—in material, engineering and construction—is the key to Armstrong's problem-solving. We carefully match coil characteristics to specific applications, on a case-by-case basis.

You can depend on Armstrong for custom engineering and quality construction.

Coil problem: Armstrong solution. We can manufacture coils in a range of sizes and in a variety of metals and alloys, including steel, stainless steel, copper, copper-alloy and other metals. A blend of custom engineering and quality construction results in an extended life cycle for your combustion air or process system coil/service package with a focus on heat rate improvement for power generation applications.

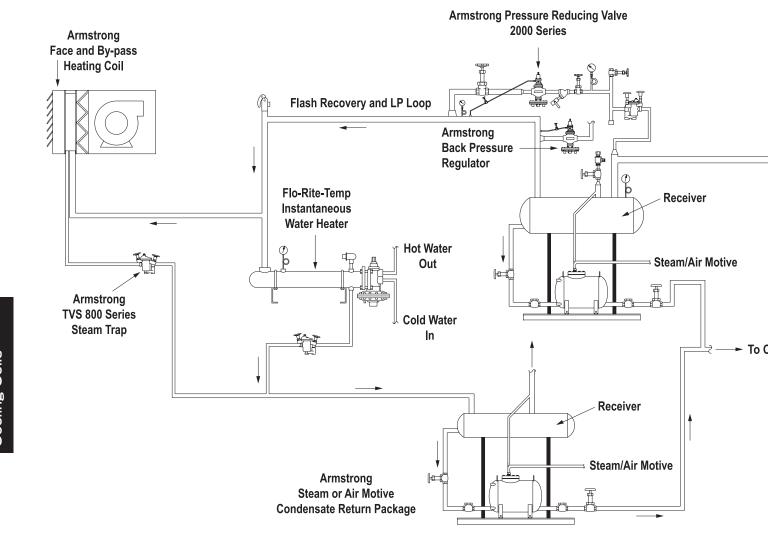
Armstrong has a complete range of service options.

Specialists from Armstrong can visit your location for walkthroughs and follow up with comprehensive system assessments. While there may be more than one course of action for you, we will recommend and—if you choose—implement the one(s) that will deliver the greatest benefit.

Although the cost of fossil fuels fluctuates, Armstrong can help you use it more efficiently. Our experience and total coil air preheating system capability can be the beginning of your transition from necessary parasitic load preheating to maximizing your combustion air preheating system's effect on improving overall system efficiency and reliability.

CONTACT US TODAY!





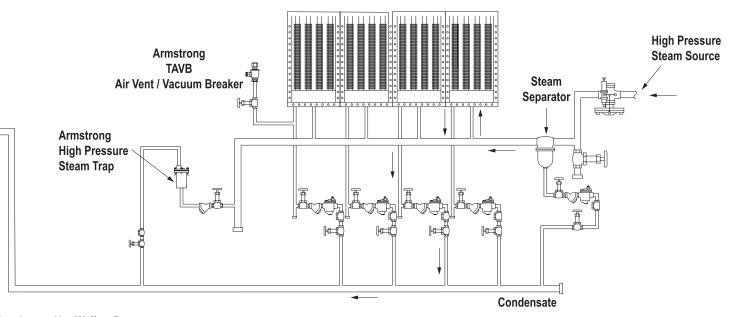




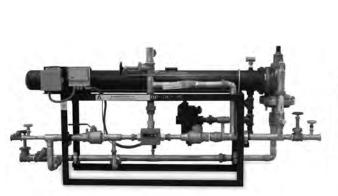


Heavy Duty Steam and Fluid Unit Heaters & Door Heaters





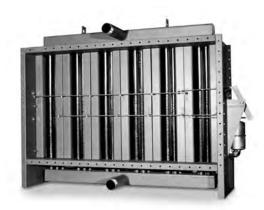
Condenser Hot Well or Deaerator



Flo-Rite-Temp Instantaneous Water Heater



Condensate Recovery
Systems



Heavy Duty Face & Bypass Steam Coil Pre-Heating Systems

If you are NOT following Best Practices, you may not be getting the Most out of your Air Preheating System!



Armstrong Duralite Plate Fin Coils

Armstrong is a full-line coil supplier with application knowledge and experience you'll find nowhere else in the industry. For nearly half a century, our heavy-duty industrial coils have been serving the process needs of heavy industry. Building on that tradition of quality and dependability, our plate fin coils meet the diverse needs of the HVAC and light industrial markets.

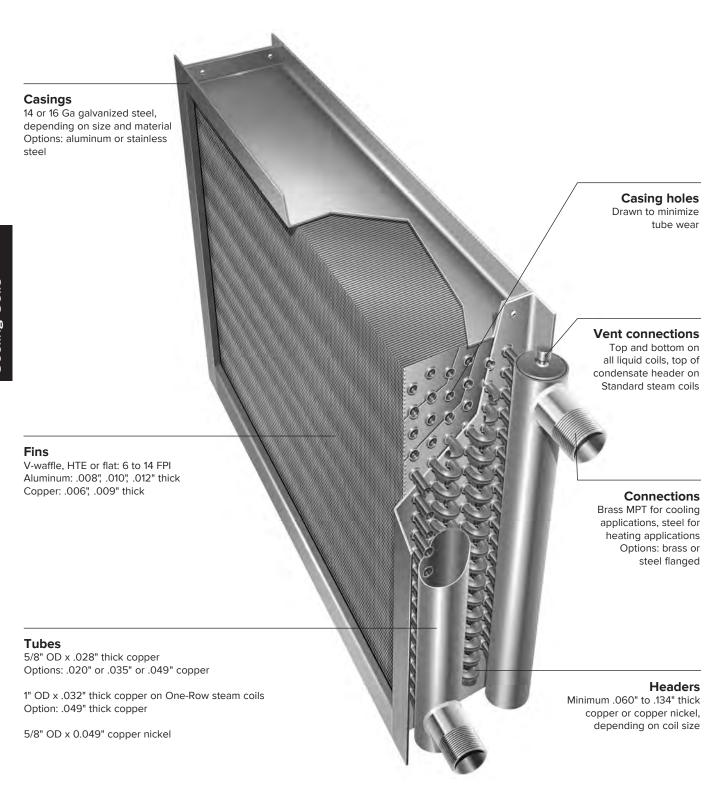
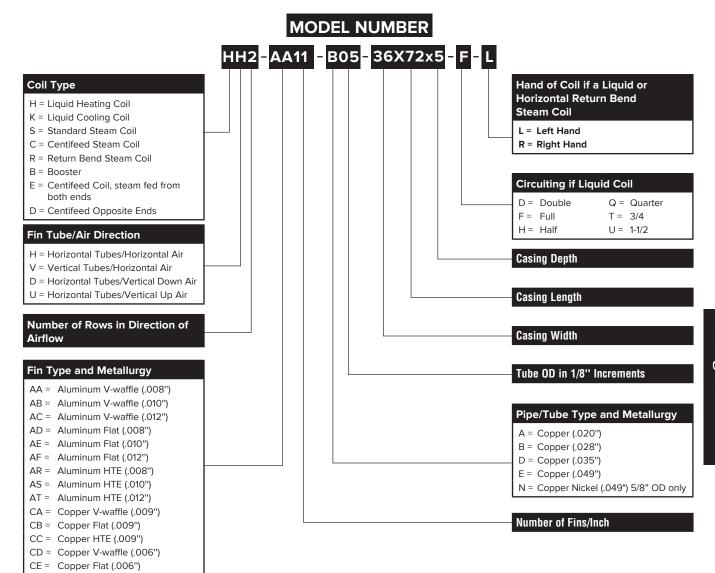


Plate Fin Coil Model Numbers





How to Identify the Circuiting of a Return Bend Coil

CF = Copper HTE (.006")

- Identify the inlet header and count the number of tubes fed from it.
- 2. Count the number of tubes in the face of the coil.
- 3. Divide the number of tubes fed from the header by the number of tubes in the face.
- 4. The result is the identification of the coil's circuit.

How to Identify the Hand of a Return Bend Coil

- 1. Face the coil with the airflow at your back (or imagine this).
- 2. Point to the outlet connection (it will be at the top of a liquid coil and should be closest to you). On a return bend steam coil, it will be the condensate return connection and should be farthest from you. If the reverse of the above exists, the coil may be installed incorrectly.
- 3. The connection on your right indicates a right-hand coil.
- 4. The connection on your left indicates a left-hand coil.

Coil-A-ware Sizing Program

Armstrong coils, both heavy duty and plate fin, are available on a Windows*-based computer program that is extremely user friendly. To obtain a copy through your Armstrong Representative, visit our Web site at armstronginternational. com and supply the requested information. Your local representative will personally deliver it to you. Updates will be available and downloadable from the Web site.

^{*}Windows is a registered trademark of Microsoft.



How To Order Armstrong Duralite Plate Fin Steam Coils

Armstrong Duralite" Plate Fin Steam Coils are available in Centifeed (Steam Distributing Tube Type), Standard (Opposite End Connections) and Two-Row Return Bend Construction.

Centifeed, Standard and Return Bend coils are made of 5/8" OD tubes as a standard.

One-Row coils are available optionally with 1" OD tubes.

Depending upon steam flow, long Centifeed coils may require steam to be fed from both ends to eliminate cold tube ends and subsequent freezing potential.

To ensure that a replacement coil will fit in the same location, and that it will perform the same as the coil it replaces, the dimensions and other data requested below must be obtained prior to sizing and pricing.

Dimensions

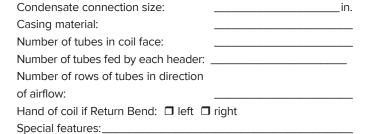
Tube wall:

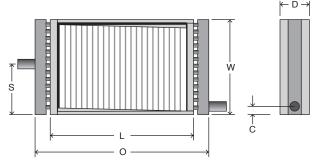
Steam connection size:

W	L	D	0	S*	C*

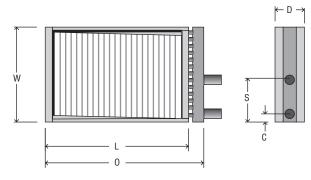
^{*}Not required if Armstrong Standard Dimensions are acceptable.

Perrorma	nce ir	itorma	tion		
Airflow rate:					
☐ Fan CFM	☐ SCF	M 🗖 lb/	hr		
Fan location:	☐ befo	re coil(s)	□ aft	er coil(s)	
Steam pressu	ıre:				psig
Entering air to	emperat	ure:			° F
Leaving air te	emperati	ıre:			° F
Altitude:					ft. above MSL
Coil Infor	matio	n			
Coil type (spe	ecify): _				
Fin type:	☐ flat	■ V-war	ffle 🗆	HTE	
Fin material:					
Fin thickness	:				in
Fins per inch	:				
Tube materia	ıl:				
Tube OD:					in

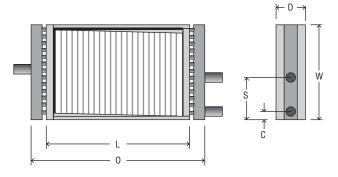




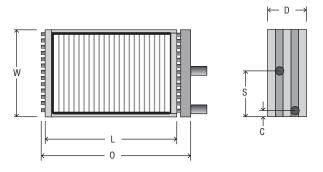
Standard Steam Coils



Centifeed Steam Coils



Centifeed Steam Coils Fed From Both Ends



Return Bend Steam Coils

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

in.

How To Order Armstrong Duralite Plate Fin Liquid Coils



Armstrong Duralite™ Plate Fin Heating Coils are available in Return Header design in one- or two-row configurations and Return Bend design in two or more rows. Liquid coils are made of 5/8" OD copper tube.

Cooling coils can be built from 2 to 12 rows and with double, full or 1/2 circuits. Custom circuits are also available.

To ensure that a replacement coil will fit in the same location, and that it will perform the same as the coil it replaces, the dimensions and other data requested below must be obtained prior to sizing and pricing.

Dimensions

W	L	D	0	S*	C*

^{*}Not required if Armstrong Standard Dimensions are acceptable.

Performance Information

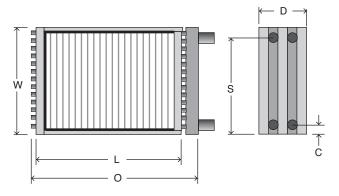
Airflow rate:	
☐ Fan CFM ☐ SCFM ☐ Ib/hr	
Fan location: \square before coil(s) \square after	r coil(s)
Entering air temperature:	°F
Wet bulb or RH (if cooling):	
Leaving air temperature:	°F
Heating or cooling medium:	
Entering liquid temperature:	°F
Leaving liquid temperature:	°F
or liquid flow rate:	GPM
Altitude:	ft. above MSL

Coil InformationCoil type (specify):

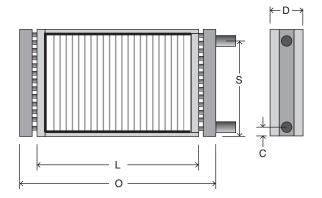
in
in
in
in
in
r:

Hand of coil if Return Bend: ☐ left ☐ right

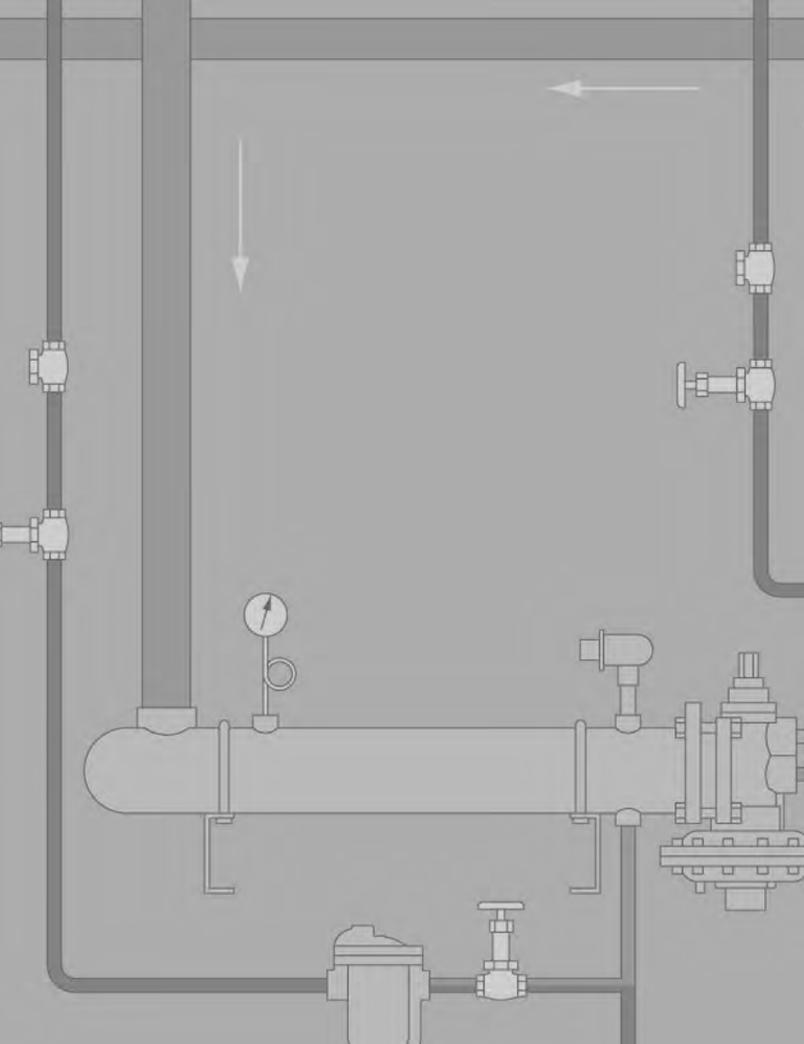
Special features:_____

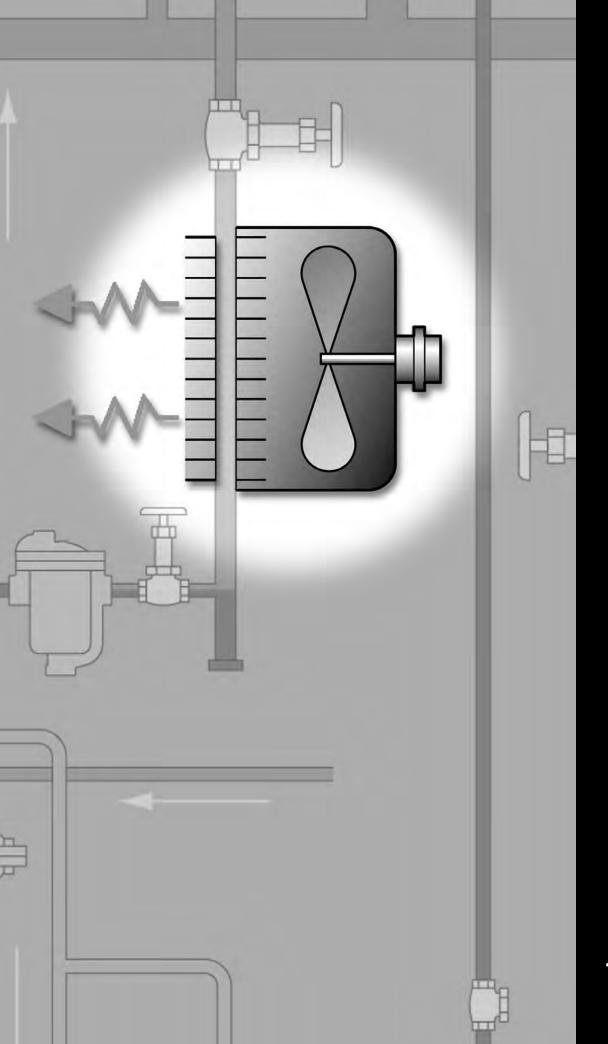


Return Bend Heating & Cooling Coils



Return Header Heating Coils





Unit Heaters

Armstrong





Longer Life in the Harshest Environments

When it comes to long life under tough industrial conditions, Armstrong is all you need to know about unit heaters. Even in the most severe environments, where coil leaks and corrosion are costly problems, Armstrong coils maintain high efficiency and output.

Armstrong: Why and How

The ability to maintain heat transfer efficiency and resist corrosion—both internally and externally—is why Armstrong unit heaters are uniquely dependable. *How* we construct them is your assurance of lasting performance, even in severe operating environments.

Consider these measurable benefits at work in your facility:

- **Heavy gauge enclosures:** Fabricated from 14-gauge steel for protection and durability.
- Corrosion-resistant heating cores: Cores are fabricated in a full range of materials, including steel, stainless steel, copper and others. Special coatings may be applied to increase resistance to external corrosion. Cores feature all-welded construction for durability and ease of repair. Cores can be steam or liquid compatible and can be used for steam, hot water or glycol heating mediums.

- Standard NEMA frame TEFC ball bearing motors: Supplied on all sizes, these heavy-duty motors are totally enclosed to lock out dirt for smooth performance. Quick access to the motor permits easy replacement.
- Thick fins and tubes: Constructed of high-strength, corrosion-resistant materials. Fins are available in a wide variety of thicknesses and pitches to withstand high pressure cleaning without damage or distortion.
- Customizing to your needs: Fans range in size from 10" to 48", and the wide selection of component materials means long, trouble-free service life.



Lightweight coils don't stand a chance in harsh environments. Armstrong coils survive because they're built as tough as your meanest application.



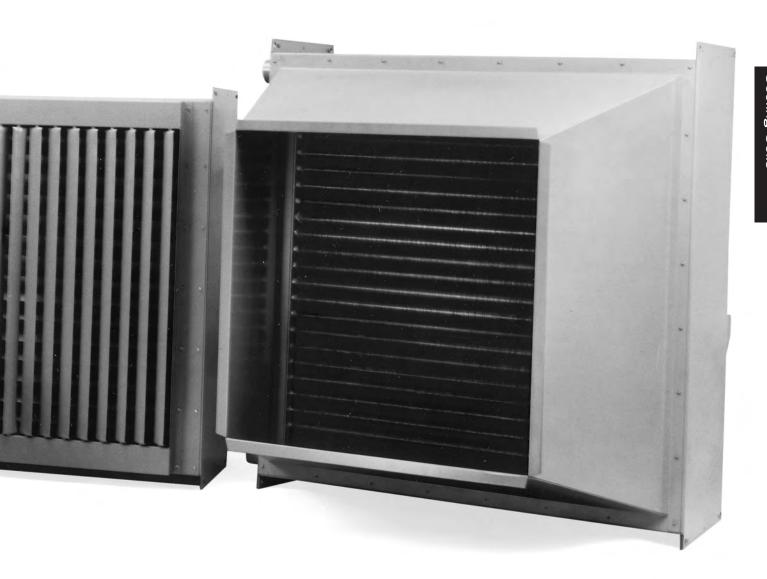


Your Steam Specialist

The first step toward ensuring trouble-free operation is proper unit selection. Your Armstrong Representative will help you select the right unit heater or door heater for any given application.

Our expertise as a manufacturer of unit heaters and door heaters is backed by over 70 years' experience in steam trapping, venting and condensate removal. To you, that means a superior product and an Armstrong Representative who understands how to make it work in your steam system.

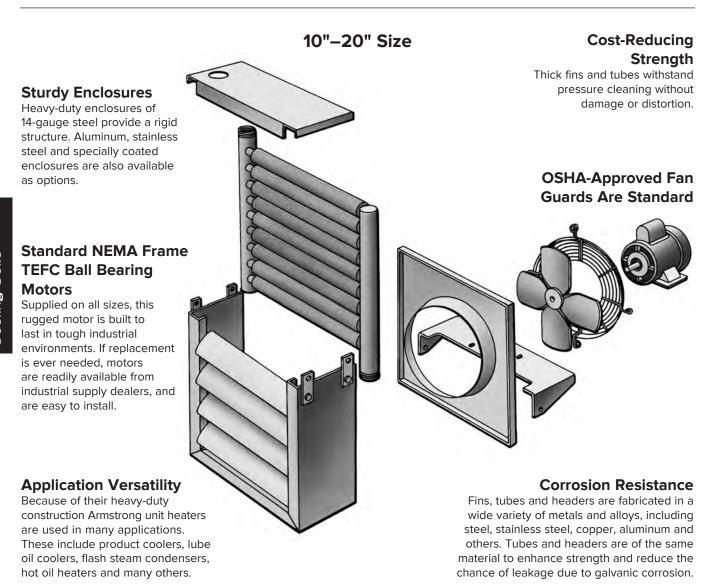
If you're losing heat transfer due to deteriorating coils, contact your Armstrong Representative for a complete application analysis. You'll receive top-quality, reliable products from experts who know how to maximize your steam system efficiency.





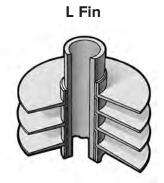
Compare the Benefits You Can't See

Many of the best reasons to insist on Armstrong unit heaters and door heaters are ones you never even see. Components like motors, bearings, tubes, enclosures and fins are built heavy-duty to ensure lasting performance. Armstrong's options for fin material, pitch, height and type, for example, help explain why our heating cores last longer and perform with greater efficiency. These factors all have a bearing on heat transfer. Knowing how to balance these and other factors is the key to a cost-effective solution. That knowledge is perhaps the most important of Armstrong's many hidden benefits.





The L fin has a foot at its base and is tension wound on knurled tube material. The L-shaped base provides a large contact area between the tube and the fin, ensuring effective, long-lasting heat transfer. The L fin is recommended when tubes and fins are of the same material.



The keyfin is manufactured by forming a helical groove in the tube surface, winding the fin into the groove and peening the displaced metal from the groove against the fin. This means a tight fit between the fin and the tube. The keyfin is the superior design for dissimilar tube and fin material.



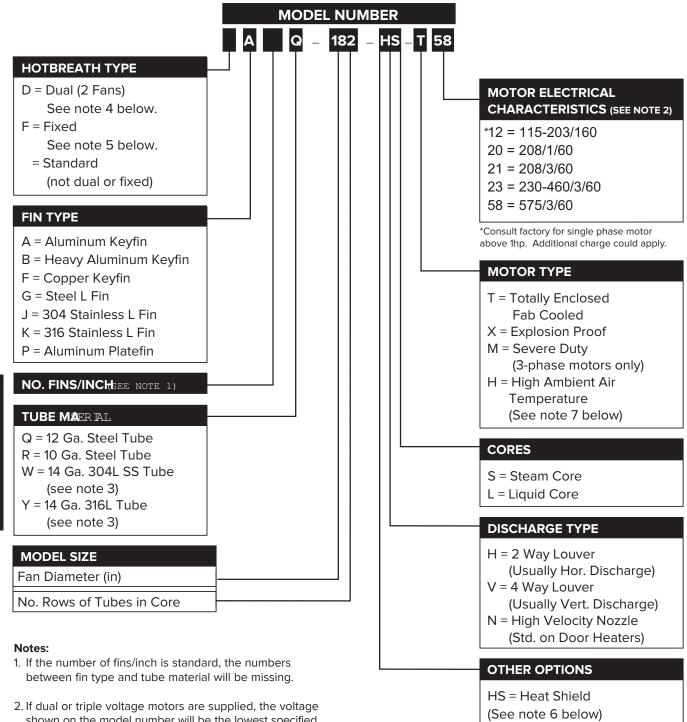
Steam or Liquid Compatible Mounting Flexibility 24"-48" Size Cores are available for steam or Basic units may be used in either liquid, allowing units to be applied horizontal or two-way vertical in different plant areas where discharge configurations. The various heating mediums may exist. addition or substitution of a four-way vertical louver section produces a square discharge pattern. An optional high-velocity discharge nozzle allows the unit to be used as a door heater to temper cold air admitted through open loading-dock doors. Highvelocity nozzles may also be used in applications requiring greater mounting heights. **High Velocity** Nozzle Fan Size Flexibility Armstrong unit heaters and door heaters are available in fan sizes ranging from 10" to 48". Vertical Unit Heater Heat Shield for **High Temperature Applications** Special purpose motor: 3b

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

(see page 383)



Model Number Selection



- 2. If dual or triple voltage motors are supplied, the voltage shown on the model number will be the lowest specified. It is the responsibility of the installer to ensure that the motor is wired correctly in accordance with the motor manufacturer's instructions to preclude damage.
- 3. May be substituted with Sch. 10 SS pipe.
- 4. Add prefix 'D' for dual units (2 fans on wider core).

 For standard unit with one fan, the Hotbreath type will be missing.
- F Models includes larger motors, cleanout lip, ports for sensors.
- 6. Required for vertical airflow or if heating medium temperature is above 300°F.
- Required for ambient air above 104°F and only available with 3-phases motors.

Material Specifications



Unit Heater	Core Material	Specifications											
1" OE	Tubes		Fins			Hea	ders	Conne	ections				
Material Min. Wall Thickness		Material	Туре	FPI	Minimum Thickness	Material	Minimum Thickness	Material	Minimum Thickness				
Standard M	Standard Materials												
Steel	.109"	Steel	L-Foot	11	.024"	Steel	.145"	Steel	.133"				
Steel	.109"	Aluminum	Keyfin	11	.020"	Steel	.145"	Steel	.133"				
Steel	.109"	Aluminum	Keyfin	13	.016"	Steel	.145"	Steel	.133"				
Special Ord	er Materials												
Steel	.109"	Copper	Keyfin	12	.016"	Steel	.145"	Steel	.133"				
Stainless	.083"	Steel	L-Foot	11	.024"	Stainless	.109"	Stainless	.109"				
Stainless .083"		Stainless	L-Foot	10	.020"	Stainless	.109"	Stainless	.109"				
Stainless .083"		Aluminum	Keyfin	11	.020"	Stainless	.109"	Stainless	.109"				
Stainless .083"		Copper	Keyfin	11	.016"	Stainless	.109"	Stainless	.109"				

NOTE: Stainless tubes available in either 304L or 316L.

Options:

- Special coatings such as powder coat epoxy, baked phenolic or hot dip galvanizing.
- Thicker tube walls.

Design Pressures and Testing Specifications

Core design pressure is 350 psig @ saturated steam temperature. (650°F for carbon steel and 500°F for stainless steel). Standard testing pressure at 525 psig. Higher pressure ratings are available upon request.

Enclosures

Enclosures, louvers and high-velocity nozzles are fabricated from 14 ga galvanized steel, finished in gray enamel. Available material options include stainless steel or aluminum. Epoxy coatings and other protective finishes are available.

Fans

Fans are of stamped aluminum with steel hubs and spiders on unit sizes 30" and smaller. Cast aluminum fans are furnished on unit sizes 36" and larger.

Fan guards are OSHA-approved and constructed of bright zinc plated steel wire.

Motor Specifications

Standard Motors

Construction:

TEFC, NEMA frame, rigid mount, continuous duty, NEMA B design, Class B insulation, 1.0 service factor, sealed ball bearings and steel frame.

Electrical Characteristics:

Single Phase (standard through 3/4 HP—optional extra cost 1-1/2 HP) 115, 208 & 230 volts. Three Phase (all sizes)—208, 230, 460 & 575 volts.

Special Purpose Motors

- Explosion-proof motors are available in all horsepowers and voltages. They are suitable for Class I Group D and Class II Groups F & G service.
- 2. Environmentally Protected. Known as "Mill & Chemical," "Severe" and "Hostile" duty motors.
 - a. Three phase 1/2 & 3/4 HP. Available with 1.15 service factor, Class F insulation, steel frame, cast iron end bells and conduit box, phosphatized or stainless steel shaft, shaft flingers and stainless steel nameplate.

- b. Three phase integral HP. Available with 1.15 service factor, Class F insulation, cast iron frame, end bells, fan cover and conduit box, stainless steel shaft, shaft flingers and stainless steel nameplate, epoxy coated. (Explosion proof motor S.F. = 1.0).
- 3. High Temperature Applications
 - a. For horizontal discharge applications where high ambient temperatures are encountered (typically 140°F–150°F, 165°F maximum), motor HP or insulation class must be increased. Consult factory.
 - b. For vertical units with on/off fan operation:

Heating Medium Temperature 300°F–375°F Class F Insulation & Heat Shield

For explosion proof motor, consult factory. 375°F & Over Class H Insulation & Heat Shield

4. Washdown duty motors also available.



Selecting Unit Heaters

A multi-step process is required to select the proper size, type and number of unit heaters to adequately heat a particular building. The process consists of the following steps:

- 1. Estimate the building heat loss.
- 2. Preliminarily select the number and type(s) of heaters to properly cover the area to be heated.
- Select specific models and calculate the actual performance of equipment selected using actual heating medium conditions and inlet air temperatures.
- Calculate actual throws, spreads and mounting heights and check to see that they will allow for complete coverage of the area to be heated.
- 5. If necessary, adjust selection and repeat steps 2 through 4.

Estimating Heat Loss

The ASHRAE Handbook of Fundamentals should be consulted to determine heat losses, taking into account specific building features. However, for an approximation of the heat loss from a typical modern industrial building, the following formula may be used.

With heated area size and outside design temperatures given:

A. Calculate the volume of the building in cubic feet:

Volume (cu ft) = floor length (ft) x floor width (ft) x average ceiling height (ft) B. Calculate the area of walls and roofs that are exposed to outside temperature:

Exposed area (EA) = wall length (ft) x average ceiling height (ft) + floor area (sq ft)

C. Total heat load (MBH) =

$$\left(\frac{V}{25} + \frac{EA}{4}\right) \times \frac{\Delta T}{1000}$$

Where

V = Building Volume (cu-ft)

EA = Exposed Wall & Roof Area (ft²) ΔT = Inside Design Temperature (F) –

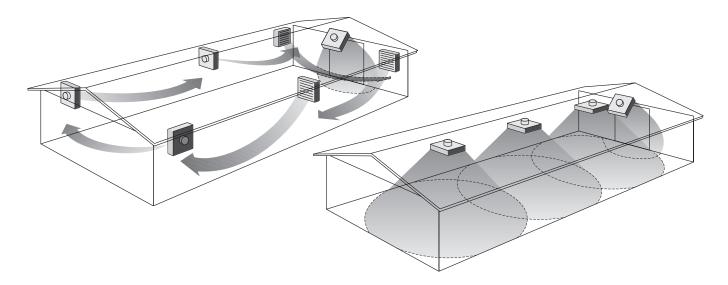
Outside Design Temperature (F)

Selection of Number, Type(s) and Location of Unit Heaters

With the total heat loss calculated, the next step is to determine the number, type(s) and location of unit heaters. First, look at the layout of the building. From that, determine the general arrangement of the unit heaters. Some typical layouts are shown below, but any given arrangement should be tailored to the particular building. Some general rules to consider follow:

 Horizontal unit heaters are used as a means to heat outside walls and should be directed to discharge toward or along walls to provide a wiping effect. Horizontal discharge units are generally sufficient to adequately heat most buildings except those with very large central floor areas or very high ceilings.

Typical Arrangements



Horizontal unit heaters provide a sweeping effect over outside walls and are sufficient to heat most buildings except those with large central floor areas.

Four-way vertical discharge units are used to heat large central areas and buildings with high ceilings or buildings with large heat loss through the ceiling.



2. Vertical unit heaters are used when a direct downward discharge to heat large central areas is needed. They may also be used if the mounting heights and throws allow for wiping of the walls with their discharge air. The discharge may be arranged for two-way airflow or four-way airflow with the addition or substitution of a four-way discharge section. A rectangular building might only need two-way discharge, whereas a square building would be better covered with a four-way arrangement.

Vertical units are also used in buildings with high ceilings or where roof heat losses are exceptionally high. Hot air from the roof area is drawn into the units and directed down to floor level, minimizing temperature gradients and reducing fuel consumption.

If fitted with a high-velocity discharge nozzle, units can be used at higher than normal mounting heights.

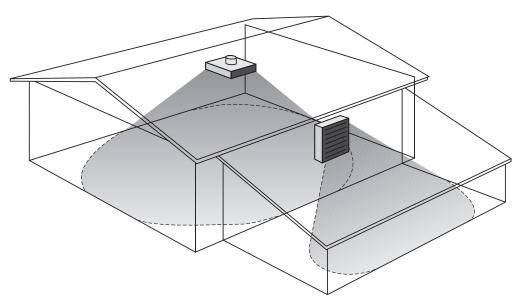
- 3. Door heaters simply use a high-velocity discharge nozzle to increase the air velocity to reach those areas that are hard to heat. These heaters can provide blankets of warm air to heat large open-loading doorways or busy entryways. They are also ideal for heating wide open plant areas. If door heater fans are activated only when doors are open, their Btu output should not be considered as part of the heat loss makeup. See page 386 for door heater selection guidelines.
- Units should be directed toward the areas of greatest heat loss. Outside doorways and exposed windows require more careful consideration.
- 5. Unit heater airstreams should be minimally obstructed to allow for greatest heat distribution.

- Unit heaters should be located to blow into open spaces such as aisles and along exterior walls rather than directly at personnel.
- 7. The mounting heights and throws specified on page 392 and corrected for outlet air temperature should be followed. Improper mounting height distance will result in poor heat distribution and reduced comfort.

Once the general layout has been determined, you can begin selecting the type of model required. First, select any door heaters that may be required. Then, select any vertical unit heaters. If the vertical unit heaters are to be directed toward center floor areas and used in conjunction with horizontal units, calculate the percentage of the total area it is intended to cover and divide that by 2. That will give you the percentage of the total heat that is required from the vertical units.

Lastly, select the horizontal units. The remaining heat load to be provided is divided by the number of units desired. Here your choice may be between a number of smaller units or fewer larger units. Notice that as the units increase in size and heating capacity their throw also increases. Generally, fewer larger units will result in the most economical installation as long as full coverage is provided.

After completing this preliminary selection process, you can calculate the actual throws, spreads and mounting heights to ensure the area will be adequately heated. If you find that the required coverage cannot be met with your initial selections, recalculate coverage by adjusting unit size or number of units.



High-velocity vertical unit heaters and door heaters are used to reach hard-to-heat areas or to provide blankets of warm air to large open areas such as loading dock doors.



Door Heaters

Door heaters are identical in design to unit heaters with the addition of a high-velocity nozzle. This nozzle helps direct airflow precisely to heat the door area required.

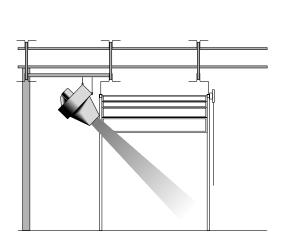
Door Heater Model Si	ze Selection Cl	hart						
Door Size				Outside Desig	n Temperature			
Width x Height (ft)	-40°F	-30°F	-20°F	-10°F	0°F	10°F	20°F	30°F
6 x 8	30	24	24	20	18	18	16	14
8 x 8	36	30	30	24	20	20	18	16
8 x 10	42	36	30	30	24	20	20	18
10 x 12	48	48	42	36	30	30	24	20
12 x 14	Two 42	Two 36	48	42	36	36	30	30
14 x 16	Two 48	Two 42	Two 36	48	42	42	36	30
16 x 18	Two 48	Two 48	Two 42	Two 36	48	48	42	36
18 x 20	Three 48	Three 42	Two 48	Two 42	Two 42	48	48	42
20 x 22	Three 48	Three 48	Three 42	Two 48	Two 42	Two 36	48	48
22 x 24	Four 48	Four 48	Three 48	Three 42	Two 48	Two 42	Two 36	48
24 x 26	Four 48	Four 48	Three 48	Three 48	Two 48	Two 42	Two 42	Two 36

How to Use This Model Size Chart:

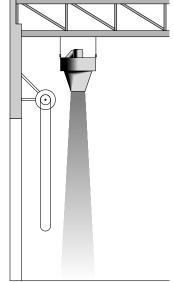
This chart gives the recommended size of door heaters. Select either a single- or double-row heating core from the appropriate performance chart (pages 386 to 392) to give a final air temperature within the 100°F to 130°F range.

- For roll-up or sliding doors, mount unit(s) to discharge vertically with the bottom of the discharge directly above the top of the door. For overhead doors, mount unit(s)
- back into the building at a distance to give sufficient clearance from the door in the open position. Aim the discharge toward the bottom of the door.
- · For doors facing prevailing winds, select one size larger.
- If negative pressure exists in the building, consult factory. Additional capacity could be required.

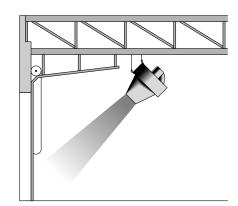
Typical Door Heater Arrangements



Side-mounted 45° discharge for low ceiling applications.



Vertical discharge for roll-up or sliding doors.



Front-mounted 45° discharge for overhead doors.

Unit Heaters



Perforn	nance Dat	ta With 2	psig ^①	Steam, 60	°F Enteri	ng Air Tem	perature						
		Co	ommon [Data	Steel T	ube / Alum 11 FPI	inum Fin		Tube / Ste ss Tube / S		Stainles	s Tube / Sta 10 FPI	inless Fin
	Model Size	Мс	otor	CFM		IIFFI			11 FPI			IU FFI	
	Size	HP	RPM	2	MBH 3	Leaving Air (°F)	Cond. (lb/hr)	MBH ③	Leaving Air (°F)	Cond. (lb/hr)	MBH ③	Leaving Air (°F)	Cond. (lb/hr)
<u>v</u>	101	1/3	1725	810	36	102	38	29	93	30	17	80	18
Models	121	1/3	1725	1350	53	97	55	42	89	44	25	77	26
	141	1/3	1725	2 590	80	89	83	64	83	66	37	73	39
Standard	161	1/2	1725	3 330	102	88	105	87	84	90	51	74	53
auc	181	3/4	1725	4 420	128	87	133	109	83	113	64	73	66
, to	201	3/4	1725	5 430	156	87	161	131	82	136	77	73	79
	241	1-1/2	1 125	7 020	205	87	212	179	84	185	105	74	108
	301	2	1 125	10 660	322	88	333	276	84	286	162	74	168
	361	2	1 125	13 440	406	88	420	351	84	363	206	74	213
	421	3	870	16 530	536	90	555	444	85	459	261	75	270
	481	3	870	22 110	692	89	716	593	85	614	349	75	361
	102	1/3	1725	700	55	133	57	45	119	47	28	98	29
in in	122	1/3	1725	1320	88	122	91	71	110	74	44	91	45
rat	142	1/3	1725	1 980	122	117	126	100	107	103	61	88	63
l du	162	1/2	1725	2 910	166	113	171	143	106	148	87	88	90
Te Se	182	3/4	1725	3 900	212	110	219	182	103	189	110	86	114
t Air Te Models	202	3/4	1725	4 560	253	111	262	217	104	224	131	87	136
High Outlet Air Temperature Models	242	1-1/2	1 125	6 000	343	113	355	304	107	315	186	89	192
ort	302	2	1 125	9 400	548	114	567	477	107	494	291	89	301
l dg	362	2	1 125	12 160	722	115	747	622	107	643	380	89	393
Ĭ	422	3	870	15 160	950	118	983	802	109	830	492	90	509
	482	3	870	20 040	1 234	117	1 277	1063	109	1 100	652	90	675

NOTES

① Steam pressure as supplied to unit heater. Valve and line losses must be subtracted from steam main pressure.

② Standard CFM measured at 70°F with density of .075 lb/cu ft.

3 Heat load in thousands of Btu/hr.

NOTE:

Leaving air temperature and MBH from table above must be corrected for steam pressures other than 2 psig and entering air temperatures other than 60°F.

Table below lists the correction factors. To determine correction factors falling between those shown, use the next lowest steam pressure and the next highest air temperature shown.

MBH (corrected) = MBH (above) \times Correction Factor LAT (corrected) = EAT + (MBH [corrected] \times 926/CFM) Condensate Load = MBH (corrected) \times 1000/Latent Heat of Steam

Correction Factors Based on 2 psig ① Steam, 60°F Entering Air														
Steam ①					Temper	ature of	Entering	a Air (°F)					Saturated	Steam
Pressure (psig)	-10	0	10	20	30	40	50	60	70	80	90	100	Steam Temp. (°F)	Latent Heat (Btu/lb)
2	_	_	_	_	_	1.16	1.08	1.00	0.93	0.85	0.78	0.71	219	966
5	1.64	1.55	1.46	1.37	1.29	1.21	1.13	1.05	0.97	0.90	0.83	0.76	227	960
10	1.73	1.64	1.55	1.46	1.38	1.29	1.21	1.13	1.06	0.98	0.91	0.84	239	953
15	1.80	1.71	1.61	1.53	1.44	1.34	1.28	1.19	1.12	1.04	0.97	0.90	250	945
20	1.86	1.77	1.68	1.58	1.50	1.42	1.33	1.25	1.17	1.10	1.02	0.95	259	939
30	1.97	1.87	1.78	1.68	1.60	1.51	1.43	1.35	1.27	1.19	1.12	1.04	274	929
40	2.06	1.96	1.86	1.77	1.68	1.60	1.51	1.43	1.35	1.27	1.19	1.12	286	920
50	2.13	2.04	1.94	1.85	1.76	1.67	1.58	1.50	1.42	1.34	1.26	1.19	298	912
60	2.20	2.09	2.00	1.90	1.81	1.73	1.64	1.56	1.47	1.39	1.31	1.24	307	906
70	2.26	2.16	2.06	1.96	1.87	1.78	1.70	1.61	1.53	1.45	1.37	1.29	316	898
75	2.28	2.18	2.09	1.99	1.90	1.81	1.72	1.64	1.55	1.47	1.40	1.32	320	895
80	2.31	2.21	2.11	2.02	1.93	1.84	1.75	1.66	1.58	1.50	1.42	1.34	324	891
90	2.36	2.26	2.16	2.06	1.97	1.88	1.79	1.71	1.62	1.54	1.46	1.38	331	886
100	2.41	2.31	2.20	2.11	2.02	1.93	1.84	1.75	1.66	1.58	1.50	1.42	338	880
125	2.51	2.41	2.31	2.21	2.11	2.02	1.93	1.84	1.76	1.68	1.59	1.51	353	868
150	2.60	2.50	2.40	2.30	2.20	2.11	2.02	1.93	1.84	1.76	1.67	1.59	366	857
200	2.75	2.65	2.55	2.45	2.35	2.25	2.16	2.07	1.98	1.89	1.81	1.72	388	837
250	2.87	2.77	2.67	2.57	2.46	2.36	2.27	2.18	2.09	2.01	1.92	1.81	408	820



Per	rforman	ce Da	ta Wi	th 200°	°F® Wa	ter, 60	0°F Ente	ring Air [·]	Temperat	ure									
	Model		mmon	Data	_	Steel ⁻	Γube / Alı 11 FF	uminum F	in			el Tube / : ess Tube 11 FP	/ Steel Fi	n	s	itainles	s Tube / : 10 FP	Stainless I	Fin
	Size	НР	RPM	CFM ②	Water Temp. Drop	мвн ③	Leaving Air (°F)	USGPM	Pressure Drop (ft wg)	Water Temp. Drop	мвн ③	Leaving Air (°F)	USGPM	Pressure Drop (ft wg)	Water Temp. Drop	MBH ③	Leaving Air (°F)	USGPM	Pressure Drop (ft wg)
	102	1/3	1725 I	700	10 20	45 39	119 112	8.9 3.9	2.01 .39	10 20	33 29	104 99	6.7 2.9	1.02 .20	10 20	25 22	93 89	5.0 2.2	.54 .10
					30 10	34 62	106 103	2.3 12.4	.13 4.01	30 10	25 52	93 96	1.7	.07 1.87	30 10	19 38	86 87	1.3 7.6	.04 .95
	122	1/3		1320	20 30	55 49	99 94	5.5 3.2	.79 .27	20 30	46 40	92 88	4.6 2.7	.37 .13	20 30	34 30	84 81	3.4 2.0	.19 .07
	142	1/3		1980	10 20	90 78	102 97	18.0 7.8	1.95 .37	10 20	76 66	96 91	15.2 6.6	.94 .18	10 20	55 48	86 82	11.0 4.8	.46 .09
					30 10	67 119	92 98	4.5 23.9	.12 2.77	30 10	57 97	87 91	3.8 19.3	.06 1.24	30 10	42 70	79 82	2.8 14.0	.03 .62
odels	162	1/2		2 910	20	105	94 89	10.5	.54	20	85 75	87 84	8.5 5.0	.24	20 30	61 54	80 77	6.1 3.6	.12
Standard Models	182	3/4		3 900	10 20	156 137	97 93	31.2 13.7	3.89 .75	10 20	132 116	91 88	26.5 11.6	1.77 .34	10 20	94 83	82 80	18.9 8.3	.85 .17
Stan					30 10	121	89 99	8.1 38.0	.26 4.88	30 10	102	93	6.8 32.2	.12 2.25	30 10	74 115	78 83	4.9 23.1	.06 1.08
"	202	3/4	₩	4 560	20 30	170 150	95 91	17.0 10.0	.97 .34	20 30	144 127	89 86	14.4 8.4	.45 .15	20 30	103 91	81 79	10.3 6.1	.22 .08
	242	1-1/2	1 125 	6 000	10 20 30	284 258 232	104 100 96	56.8 25.8 15.5	8.39 1.73 .62	10 20 30	237 214 196	97 93 90	47.4 21.4 13.1	3.87 .79 .29	10 20 30	169 153 137	86 84 81	33.7 15.3 9.2	1.82 .37 .13
	302	2		9 400	15 20 30	437 416 381	103 101 98	58.2 41.6 25.4	4.10 2.79 1.04	10 20 30	380 345 315	97 94 91	75.9 34.5 21.0	6.36 1.31 .49	10 20 30	267 245 222	86 84 82	53.4 24.5 14.8	2.94 .62 .23
	362	2		12 160	15	575 552 506	104 102 99	76.7 55.2 33.7	5.84 4.19 1.56	10 20 30	491 452 419	97 95 92	98.2 45.3 27.9	9.20 1.96 .74	10 20 30	352 324 297	87 85 83	70.4 32.4 19.8	4.41 .94 .35
	422	3	870 	15 160	10	748 675 603	106 101 97	149.7 67.5 40.2	3.05 .62 .22	10 20 30	612 552 490	97 94 90	122.5 55.2 32.6	1.43 .29 .10	10 20 30	452 406 364	88 85 82	90.4 40.6 24.2	.70 .14 .05
	482	3		20 040	10 20	989 892	106 101	197.8 89.2	4.36 .89	10 20	820 745	98 94	164.1 74.5	1.97 .41	10 20	547 539	88 85	119.5 53.9	.98 .20
	101	1/3	1725	810	30 10 20	28 25	97 92 88	53.4 5.6 2.5	.32 3.80 .74	30 10 20	667 21 19	91 84 82	44.4 4.2 1.9	.14 2.09 .43	30 10 20	487 16 14	83 78 76	32.5 3.1 1.4	.07 .86 .17
	424		1725	1250	30 10	22 41	85 88	1.5 8.2	.26 6.20	30 10	17 32	79 82	6.3	.15 3.54	30 10	12 23	74 76	.8 4.6	.06 1.4
	121	1/3		1350	20 30 10	36 32 60	85 82 81	3.7 2.2 12.0	1.24 .44 3.13	20 30 10	29 25 47	80 77 77	2.9 1.7 9.5	.73 .25 1.85	20 30 10	20 18 33	74 73 72	2.0 1.2 6.6	.28 .10
	141	1/3		2 590	20	52 45	79 76	5.2 3.0	.58 .20	20 30	41 36	75 73	4.1 2.4	.35 .12	20 30	29 25	70 69	2.9 1.7	.13 .04
dels	161	1/2		3 330	10 20 30	76 67 58	81 79 76	15.3 6.7 3.9	4.15 .80 .27	10 20 30	63 57 49	78 76 74	12.7 5.7 3.3	2.19 .44 .15	10 20 30	45 40 35	73 71 70	9.0 4.0 2.3	.84 .16 .06
ture Mc	181	3/4		4 420	10 20	97 86	80 78	19.5 8.6	5.62 1.09	10 20	81 73	77 75	16.1 7.3	3.03 .61	10 20	57 50	72 71	11.4 5.0	1.15 .22
Low Outlet Air Temperature Models	201	3/4		5 430	30 10 20	75 119 106	76 80 78	5.0 23.8 10.6	.37 7.14 1.40	30 10 20	98 88	74 77 75	4.3 19.6 8.8	.21 3.85 .78	30 10 20	45 69 62	69 72 71	3.0 13.7 6.2	.08 1.44 .29
t Air Te			1 125		30 15	94	76 81	6.3 21.4	.49 4.47	30 10	79 136	74 78	5.3 27.1	.28 4.76	30 10	55 95	69 73	3.7 19.0	.10 2.16
Outle	241	1-1/2		7 020	20 30 15	153 137 249	80 78 82	15.3 9.1 33.2	2.28 .80 6.66	20 30 10	123 111 208	76 75 78	12.3 7.4 41.7	.97 .36 7.22	20 30 10	86 78 149	71 70 73	8.6 5.2 29.7	.45 .16 3.41
Low	301	2		10 660	1	236 215	81 79	23.6 14.4	3.37 1.25	20 30	190 173	77 77 75	19.0 11.5	1.50 .55	20 30	137 124	72 71	13.7 8.3	.74 .27
	361	2		13 440	1	327 312	83 82	43.6 31.2	9.87 5.07	10 20	269 247	79 77	53.7 24.7	10.43	10 20	190 177	73 72	38.0 17.7	4.88 1.06
	421	3	870	16 530	i .	285 425 380	80 84 81	19.0 85.0 38.0	1.87 3.74 .75	30 10 20	337 300	76 79 77	15.1 67.5 30.0	.82 1.66 .33	30 10 20	234 211	71 73 72	10.7 46.8 21.1	.39 .74 .15
	481	3		22 110	30 10 20	336 559 502	79 83 81	22.4 111.8 50.2	.26 5.33 1.07	30 10 20	266 451 406	75 79 77	17.7 90.3 40.6	.11 2.30 .46	30 10 20	186 315 284	70 73 72	12.4 63.0 28.4	.05 1.03 .21
	701		♥	22 110	30	451	79	30.2	.39	30	365	75	24.4	.17	30	253	71	16.9	.07

Heating and Coils

Unit Heaters



NOTES:

- ① Water temperature at the unit heater.
- 2 Standard CFM measured at 70°F with density of .075 lb/cu ft.
- ③ Heat load in thousands of Btu/hr.

NOTE

Leaving air temperature and MBH from table on previous page must be corrected for water temperatures other than 200°F and entering air temperatures other than 60°F. Liquid flow rates and pressure drops are not corrected Table below lists the correction factors. To determine correction factors falling between those shown, use the next lowest water temperature and the next highest entering air temperature shown.

MBH (corrected) = MBH (from page 390) x Correction Factor

LAT (corrected) = EAT + (MBH (corrected) x 926/CFM)

Water $\Delta T = MBH$ (corrected) x 2.00/USGPM

Entering Water		Temperature of Entering Air (°F)													
Temp. (°F)	0	10	20	30	40	50	60	70	80	90	100				
160	1.23	1.14	1.05	0.96	0.88	0.80	0.72	0.63	0.57	0.48	0.41				
170	1.31	1.21	1.12	1.04	0.95	0.87	0.79	0.70	0.63	0.55	0.48				
180	1.38	1.29	1.20	1.11	1.02	0.94	0.86	0.77	0.70	0.62	0.55				
190	1.46	1.36	1.27	1.18	1.10	1.01	0.93	0.85	0.77	0.69	0.62				
200	1.54	1.44	1.35	1.26	1.17	1.09	1.00	0.92	0.84	0.76	0.68				
210	1.61	1.52	1.42	1.33	1.25	1.16	1.07	0.99	0.91	0.83	0.75				
220	1.69	1.59	1.50	1.41	1.32	1.23	1.14	1.06	0.98	0.90	0.82				
230	1.77	1.67	1.57	1.48	1.39	1.30	1.22	1.13	1.05	0.97	0.89				
240	1.84	1.75	1.65	1.55	1.47	1.37	1.29	1.20	1.12	1.04	0.96				
250	1.92	1.82	1.72	1.63	1.54	1.45	1.36	1.27	1.19	1.11	1.03				



		Coi	mmon	Data	:	Steel T	ube / Alu 11 FP		in				/ Steel Fi	n	S	tainles	s Tube / :		Fin
	Model Size	HP	tor RPM	CFM ②	Water Temp.	мвн	Leaving	USGPM	Pressure Drop	Water Temp.	мвн	11 FP	USGPM	Pressure Drop	Water Temp.	мвн	Leaving	USGPM	Pressur
		111	KFW		Drop	3	Air (°F)	OSOFIN	(ft wg)	Drop	3	Air (°F)	OSGFW	(ft wg)	Drop	3	Air (°F)	OSGFW	(ft wg
			1725		40	69	151	3.4	.30	40	51	127	2.5	.15	40	38	111	1.9	.08
	102	1/3		700	60 80	64 60	145 140	2.1 1.5	.16 .06	60 80	45 40	119 113	1.5 1.0	.05 .02	60 80	34 30	106 99	1.2 .7	.03
			1		40	96	128	4.8	.61	40	79	116	4.0	.25	40	59	101	2.9	.01
	122	1/3		1320	60	86	120	2.9	.21	60	71	110	2.4	.10	60	53	97	1.8	.05
					80	75	113	1.9	.09	80	62	104	1.6	.04	80	47	93	1.2	.02
	142	1/3		1980	40 60	137 120	124 116	6.8 4.0	.28 .10	40 60	116 101	114 107	5.8 3.4	.14 .05	40 60	84 74	99 95	4.2 2.5	.07
	142	1/3		1960	80	103	108	2.6	.04	80	86	100	2.1	.03	80	63	90	4.6	.02
			1		40	185	119	9.2	.41	30	148	107	7.4	.18	40	108	94	5.4	.09
gels	162	1/2		2 910	60	162	112	5.4	.14	60	131	102	4.4	.06	60	94	90	3.1	.03
ĕ					80	140	105	3.5	.06	80	114	96	2.8	.03	80	82	86	2.1	.01
<u>p</u>	182	3/4		3 900	40 60	240 213	117 111	12.0 7.1	.58 .20	40 60	203 179	108 103	10.2 6.0	.26 .09	40 60	146 129	95 91	7.3 4.3	.13
Standard Models	102	3/4		3 300	80	185	104	4.6	.09	80	158	97	3.9	.09	80	113	87	2.8	.04
Sta					40	296	120	14.8	.74	40	251	111	12.5	.34	40	178	96	8.9	.16
	202	3/4	↓	4 560	60	264	114	8.8	.26	60	224	106	7.5	.12	60	161	93	5.4	.06
			1105		80 40	233	107	5.8	.11	80	197	100	4.9	.05	80	141	89	3.5	.03
	242	1-1/2	1125	6 000	60	444 405	129 123	22.2 13.5	1.00	40 60	373 336	118 112	18.6 11.2	.60 .22	40 60	264 238	101 97	13.2 7.9	.28
	212	1 1/2			80	363	116	9.1	.17	80	301	107	7.5	.10	80	214	93	5.4	.05
					40	721	131	36.0	1.57	40	596	119	29.8	.98	40	421	102	21.1	.46
	302	2		9 400	60	660	125	22.0	.59	60	543	114	18.1	.36	60	383	98	12.8	.17
					80 40	599	119	15.0	.27	80	493	109	12.3	.17	80	348	94	8.7	.08
	362	2		12 160	60	950 873	132 127	47.5 29.1	2.24	40 60	781 714	120 114	39.1 23.8	1.46 .54	40 60	557 511	102 99	27.8 17.0	.69
	302	_	♥	12 100	80	799	121	20.0	.40	80	654	110	16.4	.25	80	465	95	11.6	.12
			870		40	1 167	131	58.4	.32	40	956	118	47.8	.22	40	704	103	35.2	.11
	422	3	l i	15 160	60	1 048	124	34.9	.12	60	856	112	28.5	.08	60	632	99	21.1	.04
			{ 		80 40	933	117 131	23.3 77.2	.05 .45	80 40	763 1 294	107 120	19.1 64.7	.03	80 40	560 939	94	14.0 47.0	.02
	482	3		20	60	1392	124	46.4	.16	60	1 158	114	38.6	.31	60	848	99	28.3	.05
			•	040	80	1255	118	31.4	.07	80	1045	108	26.1	.05	80	753	95	18.8	.02
			1725		40	43	109	2.1	.56	40	33	98	1.7	.32	40	24	88	1.2	.13
	101	1/3	1	810	60	38	104	1.3	.20	60	30	94	1.0	.11	60	21	85	.7	.05
			{ 		80 40	34 63	98 103	.8 3.2	.09	80 40	26 49	90 94	.7 2.5	.05 .53	80 40	19 35	82 84	.5 1.8	.02
	121	1/3		1350	60	57	99	1.9	.33	60	45	91	1.5	.20	60	32	82	1.1	.08
					80	50	95	1.3	.15	80	39	87	1.0	.08	80	28	79	.7	.03
					40	91	93	4.6	.45	40	71	86	3.6	.26	40	50	78	2.5	.10
	141	1/3		2 590	60	80	89	2.7	.15	60	63	83	2.1	.09	60	44 38	76	1.5	.03
			ł I		80 40	69 117	85 93	1.7 5.8	.06 .61	80 30	55 98	80 87	1.4 4.9	.04	80 40	69	74 79	1.0 3.5	.01
8	161	1/2		3 330	60	103	89	3.4	.21	60	87	84	2.9	.12	60	61	77	2.0	.04
ğ					80	89	85	2.2	.09	80	77	81	1.9	.05	80	54	75	1.4	.02
e ≤					40	150	91	7.5	.83	40	126	86	6.3	.46	40	87	78	4.4	.17
ξţ	181	3/4		4 420	60	133	88	4.4	.29	60	112	83	3.7	.16	60	78	76	2.6	.06
Ser			ł I		80 40	117 185	92	2.9 9.2	.18 1.07	80 40	99 153	81 86	2.5 7.6	.07 .58	80 40	69 107	74 78	1.7 5.4	.03
Low Outlet Air Temperature Models	201	3/4		5 430	60	164	88	5.5	.38	60	138	84	4.6	.21	60	96	76	3.2	.08
Ĕ			V		80	144	85	3.6	.16	80	122	81	3.1	.09	80	84	74	2.1	.03
Ā			1125		40	263	95	13.2	1.68	40	214	88	10.7	.74	40	149	80	7.4	.33
HE	241	1-1/2		7 020	60 80	239 212	92 88	8.0 5.3	.62 .27	60 80	192	85 83	6.4 4.3	.26 .12	60 80	135 121	78 76	4.5 3.0	.05
0			 		40	408	96	20.4	2.53	40	329	89	16.7	1.13	40	234	80	11.7	.54
٥	301	2		10 660		372	92	12.4	.93	60	298	86	9.9	.41	60	213	79	7.1	.20
					80	334	89	8.4	.42	80	269	83	6.7	.19	80	192	77	4.8	.09
	264			42.446	40	537	97	26.9	3.75	40	425	89	21.3	1.64	40	302	81	15.1	.77
	361	2	₩	13 440	60 80	494 447	94 91	16.5 11.2	1.41 .65	60 80	389 356	87 85	13.0 8.9	.61 .29	60 80	276 250	79 77	9.2 6.2	.29
			870		40	661	97	33.0	.57	40	528	90	26.4	.25	40	362	80	18.1	.13
	421	3		16 530	60	586	93	19.5	.20	60	466	86	15.5	.09	60	323	78	10.8	.04
					80	520	89	13.0	.09	80	411	83	10.3	.04	80	286	76	7.1	.02
	404	_		22.446	30	876	97	43.8	.82	40	700	89	35.0	.35	40	492	81	24.6	.16
	481	3	₩	22 110	60 80	783 693	93 89	26.1 17.3	.29 .13	60 80	630 564	86 84	21.0 14.1	.12 .06	60 80	442 392	79 76	14.7 9.8	.06 .02

Heating and Cooling Cooling

Unit Heaters



NOTES:

 $\ensuremath{\textcircled{\scriptsize 1}}$ Water temperature at the unit heater.

2 Standard CFM measured at 70°F with density of .075 lb/cu ft.

3 Heat load in thousands of Btu/hr.

NOTE:

Leaving air temperature and MBH from table on previous page must be corrected for water temperatures other than 300°F and entering air temperatures other than 60°F. Liquid flow rates and pressure drops are not corrected.

Table below lists the correction factors. To determine correction factors falling between those shown, use the next lowest water temperature and the next highest entering air temperature shown.

MBH (corrected) = MBH (from page 390) x Correction Factor

LAT (corrected) = EAT + (MBH [corrected] x 926/CFM)

Water $\Delta T = MBH$ (corrected) x 2.08/USGPM

Entering Water					Temperati	are of Enter	ing Air (°F)				
Temp. (°F)	0	10	20	30	40	50	60	70	80	90	100
260	1.15	1.10	1.04	0.99	0.94	0.88	0.83	0.78	0.73	0.69	0.64
270	1.19	1.14	1.08	1.03	0.98	0.93	0.88	0.82	0.78	0.73	0.68
280	1.23	1.18	1.13	1.08	1.02	0.97	0.92	0.87	0.82	0.77	0.72
290	1.27	1.22	1.17	1.12	1.07	1.01	0.96	0.91	0.86	0.81	0.76
300	1.31	1.26	1.21	1.16	1.11	1.05	1.00	0.95	0.90	0.85	0.80
310	1.35	1.30	1.25	1.21	1.15	1.10	1.04	0.99	0.94	0.89	0.84
320	1.41	1.36	1.30	1.26	1.19	1.14	1.09	1.03	0.98	0.93	0.88
330	1.45	1.40	1.34	1.30	1.23	1.18	1.13	1.07	1.02	0.97	0.92
340	1.49	1.44	1.39	1.34	1.27	1.22	1.17	1.11	1.06	1.01	0.95
350	1.54	1.48	1.43	1.38	1.33	1.26	1.21	1.15	1.10	1.05	1.00
360	1.58	1.52	1.47	1.42	1.36	1.30	1.25	1.20	1.14	1.09	1.04
370	1.62	1.57	1.51	1.46	1.40	1.35	1.29	1.24	1.18	1.13	1.08
380	1.66	1.61	1.55	1.50	1.44	1.39	1.33	1.28	1.22	1.17	1.12
390	1.71	1.65	1.60	1.54	1.49	1.43	1.37	1.32	1.27	1.21	1.16
400	1.74	1.69	1.63	1.57	1.53	1.47	1.42	1.36	1.31	1.25	1.20

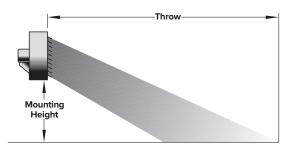


Mounting Heights, Throws and Spreads

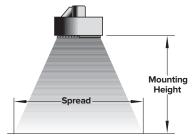
The mounting heights, throws and spreads listed below are based on an air temperature rise (ΔT) of 40°F. To arrive at these values for temperature rises other than 40°F, first determine the actual temperature rise from the appropriate performance data page. Then multiply the values from table below by the correction factors shown.

NOTES:

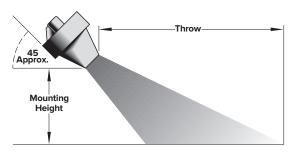
- 1. Minimum mounting height is 7 feet.
- 2. Mounting height is measured from bottom of unit to floor.
- 3. Values in the table were determined with louvers at 45°.
- 4. If four-way discharge louvers are used for horizontal applications, multiply throws by 0.8.
- 5. Values given are based upon average conditions and could be severely affected by such factors as obstructions, cross drafts, etc.



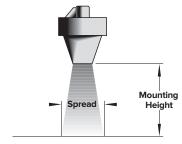
Horizontal Discharge—Standard Louvers



Vertical Discharge—Four-Way Louvers



Horizontal Discharge—High-Velocity Nozzle



Vertical Discharge—High-Velocity Nozzle

Discharge T Correction F	
Actual ∆T	Correction
10	1.18
20	1.12
30	1.06
40	1.00
50	0.94
60	0.88
70	0.82
80	0.76
90	0.70
100	0.64
110	0.58
120	0.51
130	0.45
140	0.39
150	0.33

Unit Hea	ter Mounti	ng Heights, T	hrows ar	nd Spreads								
	Hori	izontal Louvere	d	Ve	ertical Louvered	d	Horizo	ntal High Velo	city	Verti	cal High Veloc	ity
Model Size	Outlet Velocity FPM	Max. Mounting Height (ft)	Throw (ft)	Outlet Velocity FPM	Max. Mounting Height (ft)	Spread (ft)	Outlet Velocity FPM	Max. Mounting Height (ft)	Throw (ft)	Outlet Velocity FPM	Max. Mounting Height (ft)	Spread (ft)
101	600	10	30	660	10	25	2 310	12	40	2 310	17	15
121	750	12	44	820	13	38	2 050	14	58	2 050	22	20
141	1 090	14	53	1200	16	48	2 620	17	72	2 620	27	25
161	1 110	15	66	1220	17	52	2 290	18	88	2 290	29	27
181	1200	16	72	1320	18	55	2 270	19	94	2 270	31	29
201	1220	17	76	1340	18	56	2 380	20	101	2 380	31	29
241	1360	18	82	1500	19	59	2 340	22	109	2 340	32	30
301	1340	20	84	1500	20	62	2 270	24	112	2 270	34	32
361	1220	21	88	1340	21	65	2 210	25	122	2 210	36	34
421	1 110	21	118	1 230	21	66	2 180	25	158	2 180	36	34
481	1140	22	118	1 270	22	70	2 210	26	160	2 210	37	35
102	550	9	22	600	9	24	2 000	11	30	2 000	15	13
122	730	12	37	800	13	38	2 000	14	49	2 000	22	20
142	840	13	45	920	15	46	2 000	16	62	2 000	26	24
162	970	15	56	1060	17	51	2 000	18	75	2 000	29	27
182	1 050	16	66	1 160	18	55	2 000	19	86	2 000	31	29
202	1 030	16	69	1 130	18	56	2 000	19	92	2 000	31	29
242	1 170	17	73	1 280	19	59	2 000	20	97	2 000	32	30
302	1 180	19	74	1320	20	62	2 000	23	98	2 000	34	32
362	1 100	20	78	1 210	20	62	2 000	24	110	2 000	34	32
422	1 020	21	110	1 130	21	66	2 000	25	145	2 000	36	34
482	1 040	22	110	1 150	22	70	2 000	26	147	2 000	37	35

Dimensions and Weights



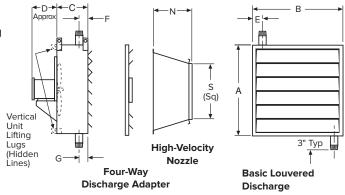
Sound Data

Since unit heaters use fans and motors to move air, sound is a natural result. The sound rating of a particular unit may limit its use in a given application. The following sound rating table is presented to allow you to select a unit based upon an acceptable sound level.

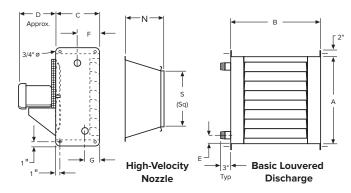
Sound Data	
Unit Heater Size	dBA Sound * Pressure Level at 3 Feet from Unit
101	63
102	63
121	63
122	63
141	66
142	65
161	74
162	73
181	77
182	76
201	81
202	81
241	82
242	82
301	84
302	83
361	85
362	85
421	84
422	83
481	85
482	85

^{*} Per fan.

10"-20" Units



24"-48" Units



NOTE: Connections are MPT

(Four-way louver section replaces basic louver section)

Dimensi	ons and \	Weights												
Model					Dimen	sions (in)				V	nit With Hor ertical Louv s by Core 1	ers	Additional Weight for High-Velocity
Size	Α	В	С	D	E	F	G	Conn. MPT	N	s	ST/AL	ST/ST	SS/SS	Discharge Nozzle (lb)
101 102	15	17-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	10	7	95 135	105 155	95 145	11
121 122	17-1/4	19-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	10-3/4	9-3/4	105 150	120 180	110 165	14
141 142	19-1/2	21-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	11-1/2	11-3/4	120 175	140 210	125 190	16
161 162	22	23-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	12-1/4	14-1/4	135 195	165 240	145 220	19
181 182	24-1/4	25-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	13	16-3/4	150 220	185 280	160 250	22
201 202	26-1/2	27-3/4	12	9	1-3/8	4-1/2	4-1/4	1-1/2	13-3/4	18	170 245	210 315	180 285	24
241 242	32	34-1/4	18	12	2-7/16	6-3/4	4-1/4	2	14-1/2	20-3/4	290 360	350 470	320 420	17
301 302	39-1/4	40-1/4	18	12-1/2	1-13/16	6-3/4	4-1/4	2	18-13/16	26	360 460	460 650	410 550	31
361 362	361 45-1/4	46-1/4	18	12-1/2	2-5/8	6-1/2	4-1/2	2-1/2	22-7/8	29-1/2	440 550	560 800	500 680	47
421 422	421 52-1/4	52-1/4	22	15	2-5/8	6-1/4	4-3/4	3	29-3/8	33	680 830	850 1 150	770 1 010	35
422 481 482 59-1/4	58-1/4	22	15	2-3/8	6-1/4	4-3/4	3	31-1/4	38	800 990	1 030 1 430	920 1 240	47	

^{*} Dual units have two fans and two motors and, therefore, have twice the width and weight.



Installation Guidelines

Below are some abbreviated installation guidelines. Consult Armstrong for more detailed installation, operation and maintenance instructions.

General Piping Guidelines

- 1. Provide adequate support from the building structure to eliminate piping stresses.
- 2. Allow movement of the piping to provide for expansion and contraction. Use swing joints where possible.
- Adequately support all piping. Do not use unit heater for this purpose.

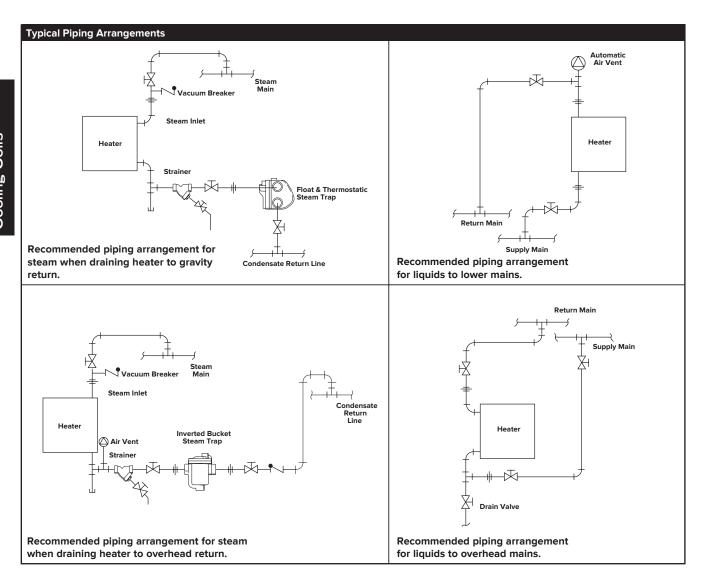
Steam Piping

- Slope steam piping under 10' long toward the steam main.
 If steam pipe is longer than 10', slope toward the unit and install a drip trap before the unit.
- All steam and condensate lines must be of the proper size to carry the calculated loads.

- 3. Only continuously draining traps such as inverted bucket or float and thermostatic types should be used. If an inverted bucket trap is used, an air vent should be installed downstream of the unit and before the trap.
- 4. Maintain the unit heater outlet size to the trap takeoff.
- 5. If condensate is to be lifted or if the return system is pressurized, use a check valve after the steam trap and provide a gate valve on the strainer to drain the heater in the off season.

Liquid Piping

- 1. Supply return mains must be sloped for adequate venting.
- 2. Provide air vents at all high points.
- Circulating pumps must be of adequate size to provide the required liquid flow and to overcome the system pressure drops.



Sample Specifications



Unit heaters supplied shall be manufactured with the methods and materials specified as follows:

General

Enclosures and Louvers—Shall be of minimum 14 ga galvanized steel and finished in gray enamel. (Epoxy coatings and other protective finishes are available.) Fans shall have aluminum alloy blades with steel hubs. (Epoxy coatings and other protective finishes are available.)

Motors—Shall be heavy-duty industrial type TEFC, ball bearing, standard NEMA frame motors. Electrical supply shall be _____ phase ____ volts 60 Hz. (Explosion-proof and other motor types available.)

Fan Guards—Shall be provided with each unit and be OSHA approved.

Core Type Specific

Steel tube/steel fin:

Tubes—Shall be 1" OD 12 ga steel tube. Minimum wall thickness shall be .109".

Fins—Shall be helically wound L-footed and of minimum .024" thick steel.

Headers—Shall be of carbon steel not less than .145" thick.

Connections—Shall be of Schedule 80 carbon steel pipe.

Assembly—Shall be welded to form a monometallic, internally wetted surface. Standard testing pressure at 525 psig. Pressure parts all welded.

Steel tube/aluminum fin:

Tubes—Shall be of 1" OD 12 ga steel tube. Minimum wall thickness shall be .109".

Fins—Shall be helically wound embedded type and of minimum .020" thick aluminum.

Headers—Shall be of carbon steel not less than .145" thick.

Connections—Shall be of Schedule 80 carbon steel pipe.

Assembly—Shall be welded to form a monometallic, internally wetted surface. Standard testing pressure at 525 psig.

Stainless steel tube/stainless steel fin:

Tubes—Shall be 304 L (or 316 L) 1" OD 14 ga stainless steel tube. Minimum wall thickness shall be .083".

Fins—Shall be helically wound L-footed and of minimum .020" thick 304 (or 316) stainless steel.

Headers—Shall be of the same stainless steel as the tubes not less than .109" thick.

Connections—Shall be of Schedule 40 stainless steel pipe.

Assembly—Shall be welded to form a monometallic, internally wetted surface. Standard testing pressure at 525 psig.

Stainless steel tube/steel fin:

Tubes—Shall be 304 L (or 316 L) 1" OD 14 ga stainless steel tube. Minimum wall thickness shall be .083".

Fins—Shall be helically wound L-footed and of minimum .024" thick steel.

Headers—Shall be of the same stainless steel as the tubes not less than .109" thick.

Connections—Shall be of Schedule 40 stainless steel pipe.

Assembly—Shall be welded to form a monometallic, internally wetted surface. Standard testing pressure at 525 psig.



Rotabreath High Mounted Series

Product Features

- Designed for steam, water or glycol
- 500 MBH (146 kW) to 1500 MBH (440 kW)
- One or two fans
- · Rotating of fixed discharge
- · High velocity nozzle
- · Custom designs available

Product Benefits

- · Less piping, wiring and controls
- Ideal in a low temp heat recovery loop (single point)
- · Ease of maintenance
- · Redued installation/shutdown time
- Simple installation, fewer units to install
- One unit averages 300 feet diameter of coverage
- Reduced temperature stratification

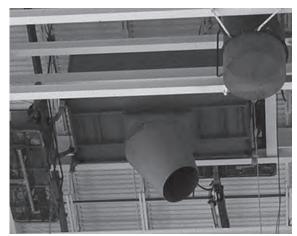
Typical Applications:

- Ideal for open space (ex. Aircraft Hangars)
- Used for high mounting (high ceiling) applications
- Ideal for low glycol temperatures
- Heat recovery application (single source)

Available in:

- Heavy Duty Series 6000
- Plate Fin Duralite









Hot Breath "/Hot Bin" Portable Heaters



Armstrong offers their Heavy Duty Industrial Unit Heaters mounted on a Heavy Duty custom Service Cart with Pre-Piped Assemblies. This design offers the customer portable, on demand, spot heat treatment to any area or equipment within their facility.

Applications

- Integrated Pest Management Heat Treatment for insect control. Dry Controlled Heat up for Structural (CAQ) and Targeted (Bin/Silo) areas (BAQ)
- Critical Area Heating during general plant shutdowns
- Temporary Comfort Heat
- Freeze Protection
- Construction Site work for Concrete Curing with controlled, low humidity, clean air

Purchase or Rent

• Purchase, Rental or Rent-To-Own Options

TEFC or Exp. Proof: (Industrial Rated)

- CAQ in Standard TEFC or Exp. Proof /FC options
- CAQ 115/230/1/60 1 HP (de-rated) with Prop Fan
- BAQ in Standard Exp. Proof options
- BAQ 230/460/3/60 3 HP with Centrifugal Fan

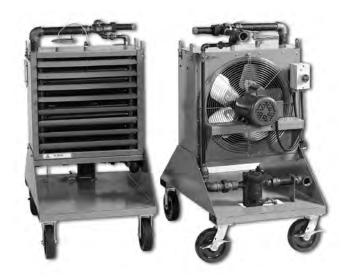
Pre-Assembled and Piped Package

Standard (150 PSIG Max. Steam Service Rating)

- Units designed to fit through 36" Doorways
- Armstrong Heavy Duty Full Size Y-Strainer w/Blow down
- Armstrong Adjustable Temp. Control Valve w/Capillary
- Armstrong Heavy Duty Industrial Finned Heating Coil
- Armstrong Inverted Bucket Steam Trap with Drain
- Heavy Duty Casing Material
- Industrial Prop Fan (CAQ) or Centrifugal Fan (BAQ) with OSHA Guard
- Steam & Condensate Piping interconnected
- Inlet/Outlet Dixon "BOSS" Steam / Condensate Fittings
- · Heavy Duty Steel Cart, welded and bolted
- Heavy Duty Industrial Caster/Wheels with (2) Locks
- Heavy Duty Wood Shipping Containers (Rental Units supplied with Re-Usable Shipping Containers)
- 2 Way Adjustable Discharge Louvers (CAQ)
- 12" Discharge Nozzle with 25Ft Hi-Temp Flex Duct & Clamps (BAQ)
- Dixon "Boss" Clamps / Fittings for Field Connections
- \bullet Heavy Duty, Steam Rated (250dgF) Hose (2 50ft)
- Heavy Duty Electric Cable. Plugs and Disconnect Pre-Wired on Single Phase (only).(Exp. Proof Shipped Loose)

Options

 Custom Options are available for Purchased Units to meet specific customer demands.



CAQ-202-HS-T12 (380 MBH - 50 psig @ 60°F EAT)

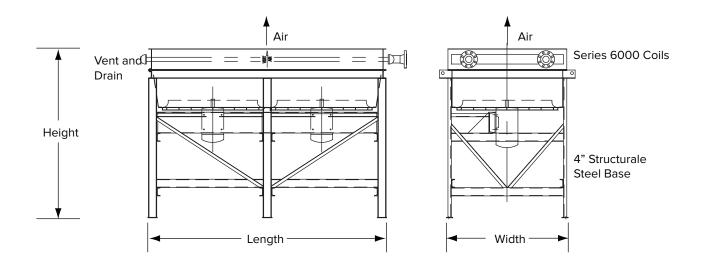


BAQ-300-HS-X23 Custom Packaged System



HI-Temp Steam Rated Hose and Quick Connectors

Armstrong Steam Condenser and Liquid Cooler

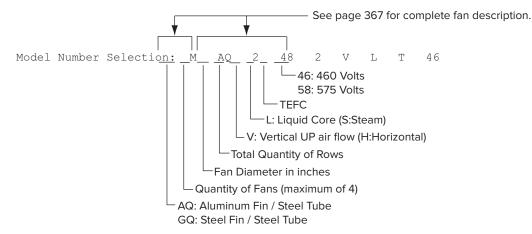


Available Options

- TEMA and API 661 design available
- ASME Section VIII Div. 1 available on pressure parts consult factory
- TEMA and API 661 design available
- Epoxy coating available
- Hail Guard
- Removable Covers
- Removable Coils contact factory

Dimensions										
	Unit Dimensions	3			Length					
	NA/7 -14	ı.			Quantity of F	ans			H	eight
Fan Size	Widt	n		2	3	}		4		
	in	mm	in	mm	in	mm	in	mm	in	mm
36"	49-1/4	1 251	96-1/2	2 451	142-3/4	3 626	189	4 801	46	1168
42"	56-1/4	1 429	108-1/2	2 756	160-3/4	4 083	213	5 410	54	1372
48"	63-1/4	1607	120-1/2	3 061	178-3/4	4 540	237	6 020	60	1524

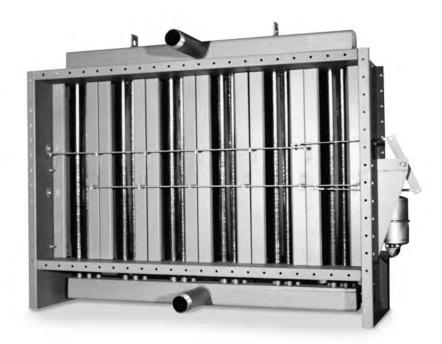
Note: Custom and larger dimensions available. Consult factory.



For sound pressure level, contact factory.

Duramix Face and By-pass Heating Coil





The Armstrong Duramix heating coil controls air temperature while operating at full steam pressure. Once set, the desired leaving air temperature is maintained by Duramix regardless of variations in the entering air temperature. The Armstrong Duramix heating coil is simple, yet very effective, and it is easy to install and maintain.

How Does It Work?

Special dampers, operated by a pneumatic or electric actuator connected to a temperature sensor, adjust the leaving air temperature by channeling the appropriate amount of entering air across the heating coils and diverting the remaining air through by-pass channels. As entering air temperature gets closer to or farther from the set point, the dampers are closed or opened accordingly.

Typical Applications

- HVAC air preheat systems
- Make-up air systems
- Combustion air preheat systems

Advantages

- Maximum freeze protection
- · Accurate temperature control
- Even leaving air temperature

Why Choose Armstrong Duramix*?

The Armstrong Duramix heating coil combines the advantages of a face and by-pass system with the quality, heavy-duty construction inherent in all Armstrong coils. From an all-welded, monometallic coil to corrosion-resistant linkages to a tough casing assembly, the Armstrong Duramix coil is built to provide long-lasting, trouble-free service.

Materials

• Heavy-Duty Tubes: 12 ga steel (type Q)

10 ga steel (type R)

14 ga 304L stainless steel (type W) 14 ga 316L stainless steel (type Y)

• Heavy-Duty Fins: 0.020" thick aluminum (type A)

0.030" thick aluminum (type B) 0.024" thick steel (type G)

0.020" thick 316L stainless steel (type K)

0.016" thick copper (type F)

- Monometallic Coil Design: Prevents galvanic corrosion
- · Welded Tube-to-Header Joints: Prevent leaks
- All Stainless Steel Damper Linkage Assembly: Prevents dampers from "freezing up" due to corrosion
- 12 ga steel casing provides a strong, durable frame Optional: 12 ga 304L stainless steel
- 16 Ga. Louvers

Design Limit

150 psig @ 400°F (10 barg @ 204°C)

Custom-built Duramix face and by-pass heating coils are also available. Please consult factory.

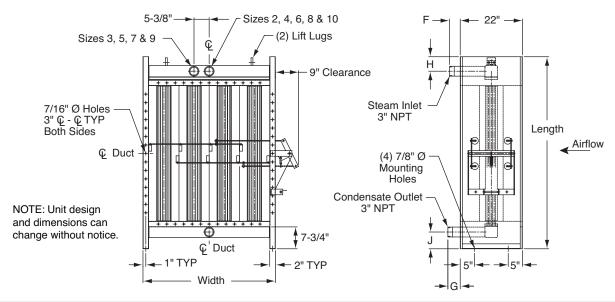
Coil Type

 Available also in centifeed, tandem and centifeed tandem, consult factory.



Duramix Sizing and Selection

All sizes are for vertical tubes and horizontal airflow only. For help in selecting the right size for either a new or retrofit application, please call us. Left hand Duramix shown below.



1-Ro	w Units																									
	No.	of Tub	e Bundl	les	2	2	3	3	4	1	Ę	5	6	j	-	7	8	3	9)	1	0	1	1	12	2
	С	asing V	Vidth (in)	25-	3/8	36-	1/8	46-	7/8	57-	5/8	68-	1/4	7	9	89-	-3/4	100	-1/2	111-	-1/8	121-	-7/8	132-	5/8
Size		F (in)		3-3	3/4	3-3	3/4	3-3	8/4	3-3	8/4	2-1	/8	2-	1/8	2-	1/8	2-	1/8	2-	1/8	2-	1/8	2-1	1/8
	Casing	(in)	11(in)	J (in)	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT
	Length	Length G (in) H (in) J				lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb
А	44"				2.27	268	3.41	331	4.54	390	5.68	458	6.81	540	7.95	607	9.09	706								
В	56"				3.41	308	5.11	374	6.81	448	8.52	526	10.22	614	11.92	693	13.63	788								
С	68"	4-3/8	5-1/8	5-15/16	4.54	339	6.81	420	9.09	501	11.36	587	13.63	681	15.90	769	18.17	867	20.44	930	22.71	1 013	25.09	1 096	27.37	1 179
D	80"	4-3/0	J-1/0	3-13/10			8.52	460	11.36	546	14.20	647	17.03	753	19.87	844	22.71	958	25.55	1037	28.39	1 130	31.37	1230	34.22	1330
Е	93-11/16"								14.76	627	18.45	738	22.15	849	25.84	961	29.53	1084	33.22	1 183	36.91	1284	40.77	1385	44.48	1 487
F	116"										22.81	825	27.38	940	31.94	1 070	36.50	1195	41.06	1320	45.63	1430	50.19	1540	54.75	1667

2-Ro	w Units																									
	No.	of Tub	e Bundl	es	2	2	3	3	4	1	Ę	5	6)	7	7	8	3	9)	10	С	1	1	13	2
	С	asing V	Vidth (in)	25-	3/8	36-	1/8	46-	7/8	57-	5/8	68-	1/4	7	9	89-	3/4	100	-1/2	111-	1/8	121-	7/8	132-	-5/8
Size		F (i	in)		3-1	1/4	3-1	/4	3-1	1/4	3-	1/4	5-1	/4	5-	1/4	5-	1/4	5-	1/4	5-1	1/4	2-	1/8	2-	1/8
	Casing	G (in)	LI (in)	l (in)	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT
	Length	G (III)	H (in)	J (in)	ft²	lb	ft²	lb	ft²	lb	ft ²	lb	ft²	lb	ft²	lb	ft²	lb	ft²	lb	ft²	lb	ft²	lb	ft²	lb
А	44"				2.27	308	3.41	382	4.54	456	5.68	538	6.81	578	7.95	756	9.09	735								
В	56"				3.41	351	5.11	431	6.81	520	8.52	613	10.22	719	11.92	839	13.63	977								
С	68"	3-1/4	3-3/8	3-1/8	4.54	383	6.81	482	9.09	580	11.36	682	13.63	795	15.90	905	18.17	1 016	20.44	1126	22.71	1 237	25.09	1348	27.37	1 459
D	80"	3-1/4	3-3/0	3-1/0			8.52	528	11.36	632	14.20	752	17.03	877	19.87	1 048	22.71	1193	25.55	1 318	28.39	1420	31.37	1522	34.22	1624
Е	98"								14.76	723	18.45	856	22.15	1044	25.84	1 196	29.53	1337	33.22	1 472	36.91	1598	40.77	1724	44.48	1850
F	116"										22.81	960	27.38	1 211	31.94	1344	36.50	1 481	41.06	1626	45.63	1 873	50.19	1926	54.75	2 076

Consult factory for additional size options.

Design Limits: 150 psig @ 400F

Model Number Selection:

BV1 - 2A A AllH/R@08 - T

Left Hand / Right Hand (LH Shown Above)

Thermostat (T), Pneumatic (P), Electric (E), Actuator (A—If Supplied)

Tube Type, Gauge/Schedule, OD - See page 342

Fin Type, Fins per Inch - See page 342

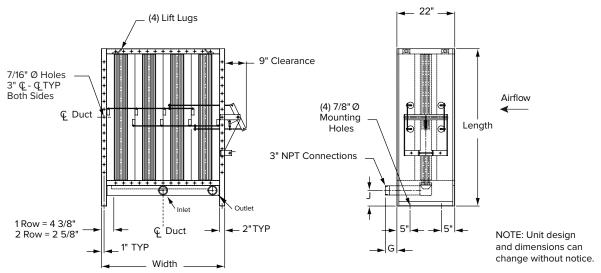
No. of Tube Bundles, Casing Width / Casing Length

By-pass, Vertical, No. of Rows

Centifeed Duramix Sizing and Selection



All sizes are for vertical tubes and horizontal airflow only. For help in selecting the right size for either a new or retrofit application, please call us. Left hand Centifeed Duramix shown below.



1-Rov	w Units																									
	No.	of Tube	e Bundl	es	2	2	3		4	ŀ	Ę	5	6		-	7	8	3	S)	10	Э	1	11	1.	2
	С	asing V	Vidth (in)	25-	3/8	36-	1/8	46-	7/8	57-	5/8	68-	1/4	7	9	89-	3/4	100	-1/2	111-	1/8	121-	-7/8	132-	-5/8
Size		F (i	in)		3-3	3/4	3-3	/4	3-3	3/4	3-3	3/4	2-1	/8	2-	1/8	2-	1/8	2-1	/8	2-1	1/8	2-	1/8	2-1	1/8
	Casing	((in)	III (im)	l (in)	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT
	Length G (in) H (in) J (ii				ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb
А	36"				2.27	268	3.41	331	4.54	390	5.68	458	6.81	540	7.95	607	9.09	706								
В	48"				3.41	308	5.11	374	6.81	448	8.52	526	10.22	614	11.92	693	13.63	788								
С	60"	4-3/8	5-1/8	5-15/16	4.54	339	6.81	420	9.09	501	11.36	587	13.63	681	15.90	769	18.17	867	20.44	930	22.71	1 013	25.09	1096	27.37	1 179
D	72"	4-3/6	5-1/8	5-15/16			8.52	460	11.36	546	14.20	647	17.03	753	19.87	844	22.71	958	25.55	1 037	28.39	1 130	31.37	1230	34.22	1330
Е	90"								14.76	627	18.45	738	22.15	849	25.84	961	29.53	1084	33.22	1 183	36.91	1284	40.77	1385	44.48	1 487
F	108"										22.81	825	27.38	940	31.94	1 070	36.50	1 195	41.06	1320	45.63	1 430	50.19	1540	54.75	1667

2-Ro	w Units																									
	No.	of Tub	e Bundl	es	2	2	3	3	2	1	Ĺ	5	6	;	7	7	8	3	ç)	10)	1	1	1:	2
	Ca	asing V	Vidth (in)	25-	3/8	36-	1/8	46-	7/8	57-	5/8	68-	1/4	7	9	89-	3/4	100	-1/2	111-	1/8	121-	7/8	132	-5/8
Size		F (i	in)		3-1	1/4	3-1	/4	3-1	1/4	3-	/4	5-1	/4	5-'	1/4	5-	1/4	5-1	/4	5-1	1/4	2-	1/8	2-	1/8
	Casing	(::)	11(:0)	J (in)	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT	FA	WT
	Length	Length G (in) H (in) J				lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb	ft ²	lb
Α	36"				2.27	308	3.41	382	4.54	456	5.68	538	6.81	578	7.95	756	9.09	735								
В	48"				3.41	351	5.11	431	6.81	520	8.52	613	10.22	719	11.92	839	13.63	977								
С	60"	24/4	2 2/0	3-1/8	4.54	383	6.81	482	9.09	580	11.36	682	13.63	795	15.90	905	18.17	1 016	20.44	1126	22.71	1 237	25.09	1348	27.37	1 459
D	72"	3-1/4	3-3/8	3-1/8			8.52	528	11.36	632	14.20	752	17.03	877	19.87	1 048	22.71	1 193	25.55	1 318	28.39	1 420	31.37	1522	34.22	1624
Е	90"								14.76	723	18.45	856	22.15	1 044	25.84	1 196	29.53	1337	33.22	1 472	36.91	1 598	40.77	1724	44.48	1850
F	108"										22.81	960	27.38	1 211	31.94	1344	36.50	1 481	41.06	1626	45.63	1 873	50.19	1926	54.75	2 076

Consult factory for additional size options.

Design Limits: 150 psig @ 400°F

Model Number Selection: CBV1 - 4C - A11 - Q08 - TA - LH/RH

Left Hand / Right Hand (LH Shown Above)

Thermostat (T), Pneumatic (P), Electric (E), Actuator (A - If Supplied)

Tube Type, Gauge/Schedule, OD - See page C-7

Fin Type, Fins per Inch - See page C-7

No. of Tube Bundles, Casing Width / Casing Length

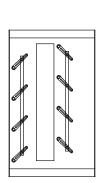
Centifeed By-pass, Vertical, No. of Rows

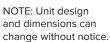


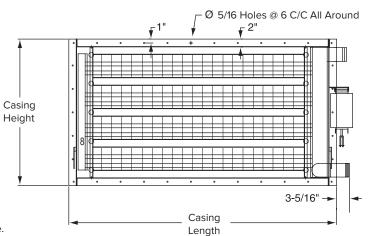
Horizontal Duramix Sizing and Selection

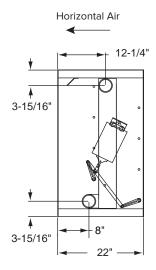
All sizes are for horizontal tubes and horizontal airflow only.

For help in selecting the right size for either a new or retrofit application, please call us. Left hand horizontal Duramix shown below.









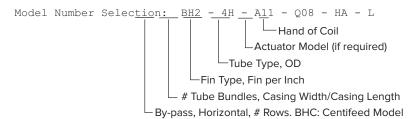
:	Size		A		В		С		D
Casing	Length (in)	26-1/2		32-1/2		38	3-1/2	44-1/2	
Size	Casing Height (in)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)
2	20-3/4	0.96	239	1.43	262	1.91	285	2.38	308
3	29-1/8	1.43	263	2.15	345	2.86	380	3.57	414
4	37-1/2	1.68	287	2.52	429	3.35	475	4.19	521
5	45-7/8	_	_	3.58	512	4.76	570	5.95	627
6	54-1/4	_	_	_	_	5.72	664	7.14	733
7	62-5/8	_	_	_	_	_	_	8.33	840
8	71	_	_	_	_	_	_	9.53	946

Reference weight only using steel tube 12 Ga. A-214 and aluminum keyfin 0.020" thick.

Si	ize	E		ı	F		3	Н	
Casing L	ength (in)	50-1/2		56-1/2		62-1/2		68-1/2	
Size	Casing Height (in)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)	Face Area Ft. ²	Weight (lb)
2	20-3/4	2.86	331	3.33	354	3.81	377	4.28	400
3	29-1/8	4.28	449	5.00	483	5.71	517	6.42	552
4	37-1/2	5.71	566	6.66	612	7.61	658	8.56	704
5	45-7/8	7.14	684	8.33	742	9.52	799	10.71	856
6	54-1/4	8.57	802	10.00	871	11.42	940	12.85	1 008
7	62-5/8	10.00	920	11.66	1000	13.32	1 080	14.99	1 161
8	71	11.43	1 038	13.33	1129	15.23	1 2 2 1	17.13	1 313

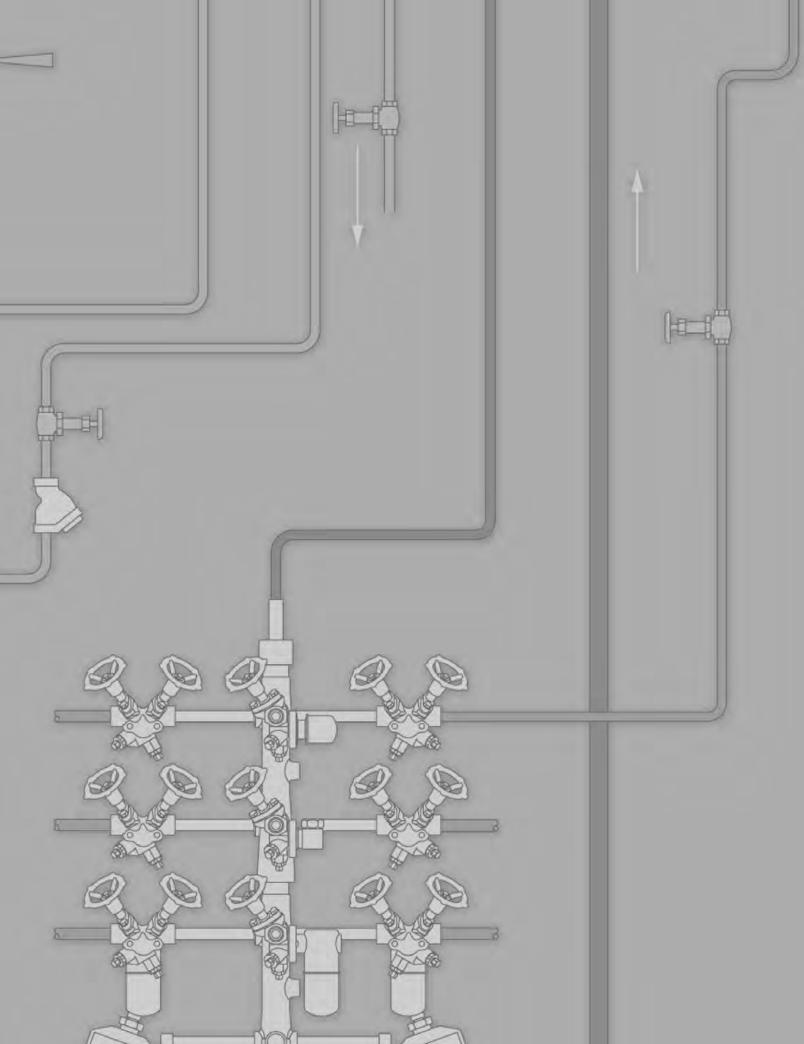
Reference weight only using steel tube 12 Ga. A-214 and aluminum keyfin 0.020" thick.

Design Limits: 150 psig @ 400°F



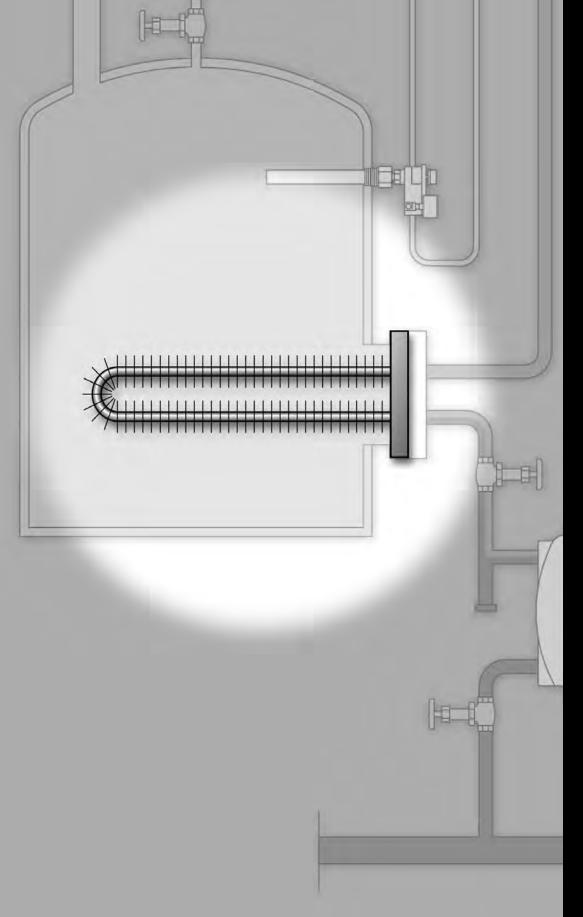
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Notes	Armstron
Designs materials weights and performance ratings are approximate and subject to	change without notice. Visit armstronginternational.com for up-to-date information.



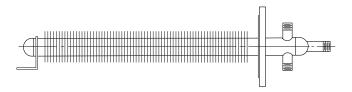








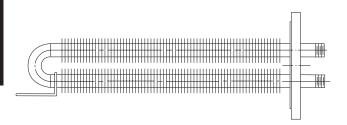
Features/Benefits of Armstrong Tank Heaters



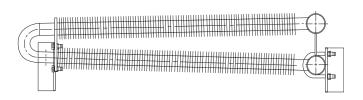
Flange Mounted Bayonet Type FBC and FBS



Base Mounted Direct Type BD



Flange Mounted Hairpin Type FHC and FHS



Base Mounted Hairpin Type BHC and BHS

Application Flexibility

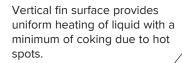
Four types of tank heaters are offered in several materials and sizes to suit your specific requirements. Several heaters are custom built, consult factory.

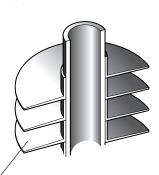
Space Savings

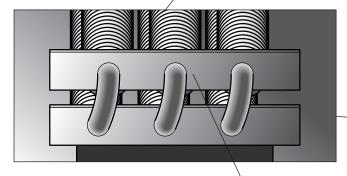
Flange mounted heaters are installed on various standard manhole sizes. You save internal space because only the heating element itself is inside. Steam and condensate connections are outside of the tank.

Heat Transfer Efficiency

Stiff, helically wound L fin design for an efficient and longlasting heat transfer surface.

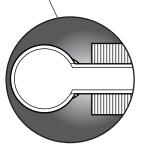






Durability Over Long Life

Pipes and headers are of heavy construction (minimum Sch. 40 pipe for steel). Greater thickness means a stronger, more corrosion-resistant design that lasts longer.



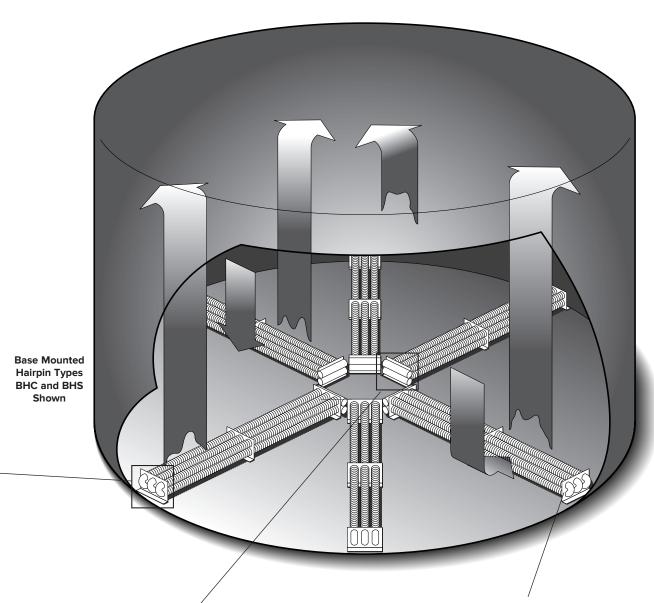
Corrosion Resistance

Pipes, headers and connections are welded together for a tough, single material joint. Eliminating dissimilar materials precludes galvanic corrosion, thereby lengthening service life.

Several heaters are custom built - consult factory.

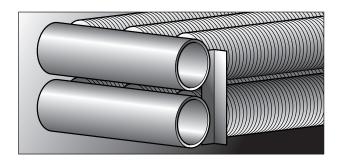
Typical Tank Heater Arrangement





Fast, Direct Connection

Heaters are ready for connection to the steam and condensate systems as supplied. Numerous types of connections are available.



Base mounted heaters come with supports to allow for a proper distance between the tank bottom and the heating surface. This also helps to minimize the need for internal welding. Longer units are provided with mid-support members to further minimize inside welding and ensure rigid footing.

Minimum Installation Welding

Armstrong base-mounted tank heaters are installed and removed easily through manholes, eliminating the need for time-consuming welding inside the tank.



Tougher on the Job

Armstrong tank heaters are built to withstand the rigorous demands encountered in industrial installations. The heavy-duty features of our units were developed in response to a need for tank heaters that could provide efficient heat transfer without sacrificing structural integrity. These features include heavy-wall pipes and headers, thick L footed fins and all welded construction. In addition, the mono-metallic construction of our units precludes galvanic corrosion, and the finned surface is rigid enough to withstand high-pressure cleaning.

Experience gained over 80 years backs every Armstrong tank heater. As a steam system specialist, your Armstrong Representative can provide assistance with everything from the boiler to the condensate return system.

Quality products from Armstrong, plus the practical knowledge to integrate them into your total steam system, ensure an efficient and trouble-free installation.

Efficient Heat Transfer

Finned pipe tank heaters are easier than bare pipe units to install, remove and repair. They are also more compact and provide superior efficiency in product heating. Finned pipe tank heaters provide up to 10 times as much heat transfer as an equivalent length of bare pipe, resulting in lower film or "skin" temperatures. This reduces coking of the product on the heat transfer surface and discoloration of heat-sensitive products. This buildup of deposits on the heater requires that more frequent cleanings be carried out to maintain maximum efficiency and original heat transfer design conditions.

This helically wound finned pipe is best suited for horizontal units, with the fins being in the vertical plane. This increases the natural convection currents, which increases heat transfer and continuously wipes the coil surface to maintain cleanliness.

Options to Match Your Applications

Armstrong tank heaters are available in four standard configurations:

- Flange Mounted Hairpin—Types FHC and FHS
- Flange Mounted Bayonet—Types FBC and FBS
- Base Mounted Hairpin—Types BHC and BHS
- Base Mounted Direct—Type BD

These four configurations offer a range of choices to suit most area coverage and thermal performance requirements. Each type includes a number of length, width and fin pitch options. All units are available in seamless carbon steel pipe construction. The hairpin and bayonet types are available in stainless steel. Liquid heated units and custom designs are also available.

Critical to the heating and maintenance of temperatures for a broad variety of products, Armstrong tank heaters are widely used in breweries, chemical and food processing plants, oil refineries, paper mills, tank storage farms, and in shipping and other industries.

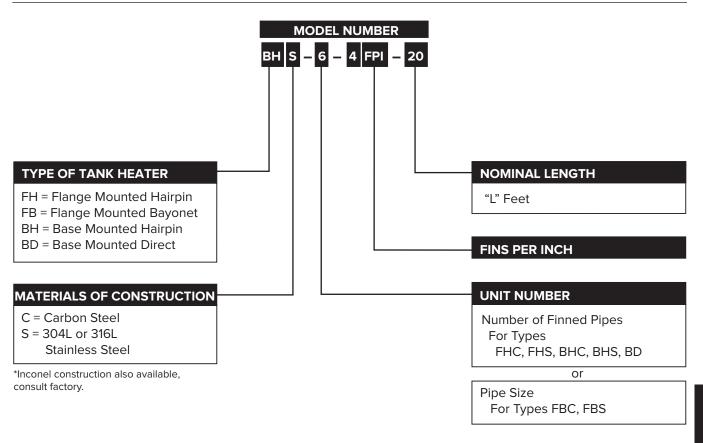


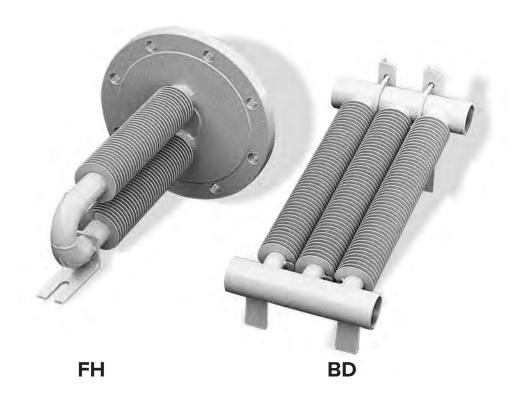
BH FB

From left to right, Base Mounted Hairpin, Flange Mounted Bayonet, Flange Mounted Hairpin and Base Mounted Direct.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

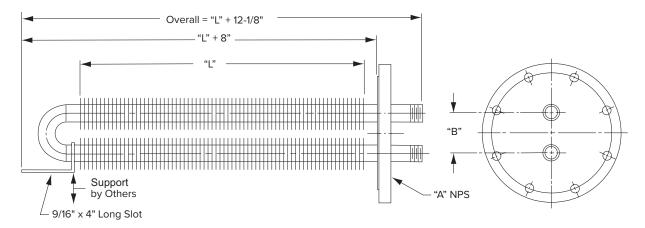








Flange Mounted Hairpin Type FHC and FHS



Standard Sizes

FHC Carbon Steel Units														
Туре	A Flange	В	Nominal Length	Surfac	e Area	(sq ft)	w	eight (l	b)					
	Size (in)	(in)	L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 FPI	5 FPI					
			2	11.6	14.9	18.1	71	74	77					
			3	17.4	22.3	27.2	81	86	90					
			4	23.2	29.8	36.3	91	97	103					
	C-2 8		5	29.0	37.2	45.4	102	109	116					
FHC-2		8 3-3/4	6	34.8	44.6	54.4	112	120	129					
			7	40.6	52.1	63.5	122	132	142					
			8	46.4	59.5	72.6	132	144	155					
			9	52.3	67.0	81.6	142	155	168					
			10	58.1	74.4	90.7	153	167	181					
			2	21.8	27.9	34.0	124	130	135					
								3	33.4	42.8	52.2	144	153	161
			4	45.0	57.7	70.3	165	176	187					
			5	56.6	72.5	88.5	185	200	213					
FHC-4	10	5-5/16	6	68.2	87.4	106.6	206	223	239					
			7	79.8	102.3	124.7	226	246	265					
			8	91.4	117.2	142.9	246	269	291					
			9	103.1	132.1	161.0	267	292	317					
			10	114.7	146.9	179.2	287	316	343					

Materials of Construction

 $\textbf{Pipes:} \ 1\text{-}1\text{/}4\text{" NPS Sch. 80 Seamless Steel (1.66\text{" OD x 0.191" Wall)}}$

Fins: 0.036" Thick Helically Wound Steel "L" Foot

Return Bends: A-234 Long Radius Forged Steel Sch. 80 Mounting Flange: A-105 Forged Steel, 150 lb Raised Face

Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

FHS S	tainless	Steel U	Inits						
Туре	A Flange	В	Nominal Length	Surfac	e Area	(sq ft)	Weight (lb)		
	Size (in)	(in)	L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 FPI	5 FPI
			2	8.8	11.1	13.4	60	61	62
		3-3/4	3	13.1	16.6	20.1	65	67	69
			4	17.5	22.2	26.9	71	73	75
			5	21.9	27.7	33.6	76	79	82
FHS-2	8		6	26.3	33.3	40.3	82	85	88
			7	30.6	38.8	47.0	87	91	95
			8	35.0	44.4	53.7	92	97	101
			9	39.4	49.9	60.4	98	103	108
			10	43.8	55.5	67.2	103	109	114
			2	17.5	22.2	26.9	100	102	105
			3	26.3	33.3	40.3	111	114	118
			4	35.0	44.4	53.7	122	126	131
			5	43.8	55.5	67.2	132	138	144
FHS-4	10	5-5/16	6	52.5	66.6	80.6	143	150	157
			7	61.3	77.7	94.0	154	162	170
			8	70.0	88.8	107.5	165	174	183
			9	78.8	99.9	120.9	176	186	196
			10	87.6	111.0	134.3	186	198	209

Materials of Construction

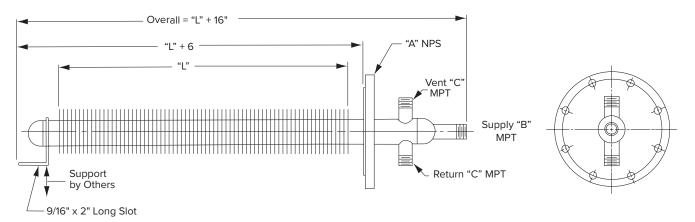
Pipes: 1-1/4" NPS Sch. 10, 304L SS (1.66" OD \times 0.109" Wall) Fins: 0.020" Thick Helically Wound 304 SS "L" Foot Return Bends: A-403 Long Radius 304L SS Sch. 10 Mounting Flange: A-182 304L SS, 150 lb Raised Face

Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

NOTE: Type 316L SS Construction is available.

Flange Mounted Bayonet Type FBC and FBS





Standard Sizes

FBC Carbon Steel Units											
Туре	A Flange	В	С	Nominal Length	Sur	face A (sq ft)		W	eight (lb)	
Турс	Size (in)	(in)	(in)	L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 PFI	5 FPI	
				2	5.8	7.4	9.1	33	34	35	
				3	8.7	11.2	13.6	39	41	42	
				4	11.6	14.9	18.1	45	47	50	
-FD-0	4			5	14.5	18.6	22.7	51	54	57	
FBC- 125		3/4	3/4	6	17.4	22.3	27.2	57	60	64	
.20				7	20.3	26.0	31.8	63	67	72	
				8	23.2	29.8	36.3	69	74	79	
				9	26.1	33.5	40.8	75	80	86	
				10	29.0	37.2	45.4	81	87	93	
	6	1	1	2	7.9	10.1	12.3	50	52	54	
				3	11.8	15.1	18.4	59	62	65	
				4	15.7	20.2	24.6	67	71	75	
				5	19.7	25.2	30.7	76	81	86	
FBC- 200				6	23.6	30.2	36.9	85	91	96	
				7	27.6	35.3	43.0	94	101	107	
				8	31.5	40.3	49.2	102	110	118	
				9	35.4	45.4	55.3	111	120	128	
				10	39.4	50.4	61.5	120	130	139	
				2	9.2	11.8	14.3	60	62	65	
				3	13.8	17.7	21.5	72	75	79	
				4	18.4	23.5	28.7	84	89	94	
FDC				5	23.0	29.4	35.8	97	102	108	
FBC- 250	6	1-1/4	1	6	27.6	35.3	43.0	109	115	123	
				7	32.2	41.2	50.2	121	129	137	
				8	36.8	47.1	57.4	133	142	151	
				9	41.4	53.0	64.5	145	155	166	
				10	46.0	58.9	71.7	158	168	180	

Materials	of	Construction
Materiais	v	Constituction

FBC-125 Pipes: 1-1/4" NPS Sch. 40 Seamless Steel (1.66" OD \times 0.140" Wall) FBC-200 Pipes: 2" NPS Sch. 40 Seamless Steel (2.375" OD \times 0.154" Wall) FBC-250 Pipes: 2-1/2" NPS Sch. 40 Seamless Steel (2.875" OD \times 0.203" Wall)

Fins: 0.036" Thick Helically Wound Steel "L" Foot Inner Distributing Pipe: Sch. 80A-53F Steel End Caps: A-234 Forged Steel Sch. 40

Mounting Flange: A-105 Forged Steel, 150 lb Raised Face

Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

NOTE: Sch. 80 Construction is available.

FBS Stainless Steel Units											
Туре	A Flange	В	С	Nominal Length	Sui	face A (sq ft)		w	eight (lb)	
туре	Size (in)	(in)	(in)	L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 PFI	5 FPI	
				2	4.4	5.5	6.7	27	28	29	
				3	6.6	8.3	10.1	31	32	33	
				4	8.8	11.1	13.4	34	36	37	
				5	10.9	13.9	16.8	38	39	41	
FBS-125	4	3/4	3/4	6	13.1	16.6	20.1	41	43	45	
				7	15.3	19.4	23.5	45	47	50	
				8	17.5	22.2	26.9	48	51	54	
				9	19.7	25.0	30.2	52	55	58	
				10	21.9	27.7	33.6	55	58	62	
		1	1	2	6.0	7.5	9.1	41	42	43	
				3	8.9	11.3	13.6	46	48	49	
				4	11.9	15.0	18.2	51	53	55	
ED0				5	14.9	18.8	22.7	57	59	61	
FBS- 200	6			6	17.9	22.6	27.3	62	64	67	
200				7	20.8	26.3	31.8	67	70	73	
				8	23.8	30.1	36.4	72	76	79	
				9	26.8	33.8	40.9	77	81	85	
				10	29.8	37.6	45.5	83	87	91	
				2	6.9	8.7	10.5	46	47	48	
				3	10.4	13.0	15.7	53	54	56	
				4	13.8	17.4	21.0	59	61	63	
				5	17.3	21.7	26.2	66	69	71	
FBS- 250	6	1-1/4	1	6	20.7	26.1	31.5	73	76	78	
200				7	24.2	30.4	36.7	80	83	86	
				8	27.6	34.8	42.0	86	90	94	
				9	31.1	39.1	47.2	93	97	101	
				10	34.5	43.5	52.5	100	105	109	

Materials of Construction

 $\label{eq:FBS-125 Pipes: 1-1/4" NPS Sch. 10, 304L SS (1.66" OD x 0.109" Wall)} $$ FBS-200 Pipes: 2" NPS Sch. 10, 304L SS (2.375" OD x 0.109" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2" NPS Sch. 10, 304L SS (2.875" OD x 0.120" Wall) $$ FBS-250 Pipes: 2-1/2"$

Fins: 0.020" Thick Helically Wound 304 SS "L" Foot

Inner Distributing Pipe: Sch. 10, 304L SS **End Caps:** A-403, 304L SS, Sch. 10

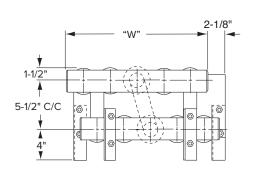
Mounting Flange: A-182, 304L SS, 150 lb Raised Face

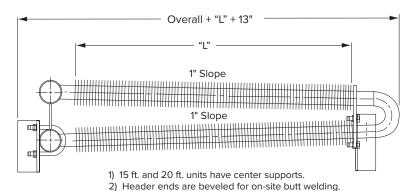
Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

NOTE: Type 316L SS Construction is available.



Base Mounted Hairpin Type BHC and BHS





Standard Sizes

BHC Car	rbon Steel	Units								
Туре	Minimum Manhole	w	Nominal Length	Sur	Surface Area (sq ft)			Weight (lb)		
Type	Size (in)	(in)	L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 FPI	5 FPI	
			5	59	76	93	108	123	138	
BHC-4	16	7-1/8	10	118	152	186	198	228	258	
BHC-4	BHC-4 16	7-1/8	15	178	228	278	293	338	383	
			20	237	304	371	384	444	503	
	18	10-1/4	5	89	114	139	158	180	203	
BHC-6			10	178	228	278	294	339	383	
BHC-6			15	266	342	418	435	502	569	
			20	355	456	557	570	660	749	
			5	118	152	186	208	238	268	
BHC-8	22	13-3/8	10	237	304	371	389	449	508	
BHC-8	22	13-3/8	15	355	456	557	576	666	755	
			20	473	608	742	757	877	995	
			5	148	190	232	258	295	332	
BHC-10	24	16 1/2	10	296	380	464	484	559	633	
	24	16-1/2	15	444	570	696	717	830	941	
			20	592	760	928	943	1 093	1 241	

Materials of Construction

Pipes: 1-1/4" NPS Sch. 40 Seamless Steel (1.66" OD x 0.140" Wall)

Fins: 0.036" Thick Helically Wound Steel "L" Foot

Headers:~2"~NPS Sch.~40~Seamless Steel~(2.375"~OD~x~0.154"~Wall)

Return Bends: A-234 Long Radius Forged Steel Sch. 40

Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

NOTE: Sch. 80 Construction is available.

BHS Stai	nless Stee	el Units	;							
Туре	Minimum Manhole	W (in)	Nominal Length	Sur	Surface Area (sq ft)			Weight (lb)		
Туре	Size (in)		L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 FPI	5 FPI	
	16		5	44	55	67	70	76	81	
BHS-4		7-1/8	10	88	111	134	124	135	147	
БПЭ-4	10	7-1/0	15	131	166	201	182	199	217	
			20	175	222	269	236	256	282	
BHS-6	18	10-1/4	5	66	83	101	101	110	119	
			10	131	166	201	182	199	217	
DH3-0			15	197	250	302	268	294	320	
			20	263	333	403	349	384	418	
			5	88	111	134	133	144	156	
BHS-10	24	16-1/2	10	175	222	269	240	264	287	
БП3-10	24	10-1/2	15	263	333	403	354	389	424	
			20	350	444	537	462	508	555	
			5	109	139	168	164	179	193	
BHS-8	22	12 2/0	10	219	277	336	299	328	357	
	22	13-3/8	15	328	416	504	440	484	527	
			20	438	555	672	575	633	691	

Materials of Construction

Pipes: 1-1/4" NPS Sch. 10, 304L SS (1.66" OD x 0.109" Wall)

Fins: 0.020" Thick Helically Wound 304 SS "L" Foot

Headers:~2" NPS Sch.~40, 304L~SS~(2.375" OD~x~0.154" Wall)

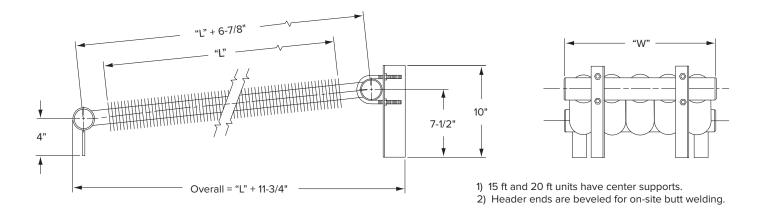
Return Bends: A-403 Long Radius 304L SS Sch. 10

Mechanical Design: 450 psig, 650°F, Standard Testing Pressure 675 psig

NOTE: Type 316L SS Construction is available.

Base Mounted Direct Type BD





Standard Sizes

BD Carbon Steel Units											
Time	Minimum Manhole	w	Nominal	Surface Area (sq ft)			Weight (lb)				
Type	Size (in)	(in)	Length L (ft)	3 FPI	4 FPI	5 FPI	3 FPI	4 FPI	5 FPI		
	14		5	30	38	47	60	68	75		
BD-2		7-1/8	10	59	76	93	104	121	135		
DD-2		7-1/8	15	89	114	140	156	179	201		
			20	118	152	186	201	231	261		
	16	10-1/4	5	45	57	70	86	97	109		
			10	89	114	139	154	177	199		
BD-3			15	134	171	209	227	261	294		
			20	178	228	278	295	340	384		
			5	59	76	93	112	127	142		
BD-4	20	13-3/8	10	118	152	186	203	233	262		
BD-4	20	13-3/6	15	177	228	279	298	343	388		
			20	237	304	371	389	449	508		
			5	74	95	116	138	157	175		
BD-5	22	16 1/2	10	148	190	232	251	288	325		
	22	16-1/2	15	222	285	348	369	425	481		
			20	296	380	464	482	557	631		

Materials of Construction

Pipes: 1-1/4" NPS Sch. 40 Seamless Steel (1.66" OD x 0.140" Wall)

Fins: 0.036" Thick Helically Wound Steel "L" Foot

Headers: 2" NPS Sch. 40 Seamless Steel (2.375" OD x 0.154" Wall)

Mechanical Design: 450 psig, 650°F, Standard Testing Prsesure 675 psig

NOTE: Sch. 80 Construction is available.

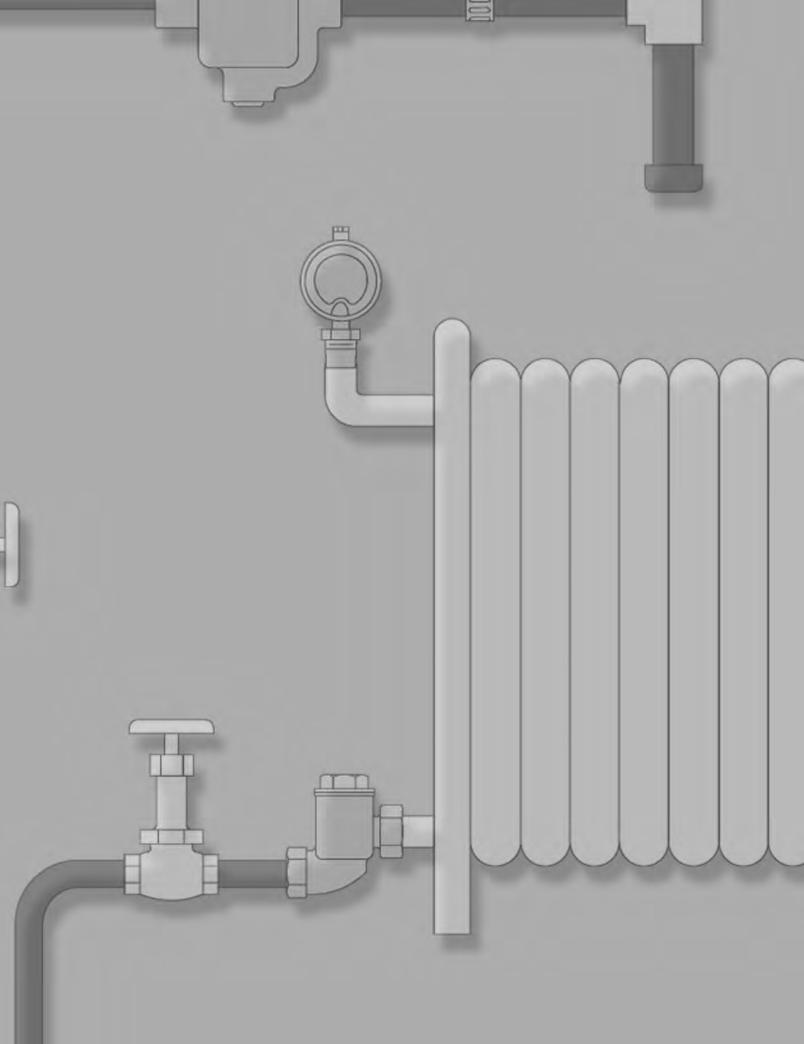
These units are available only in Carbon Steel.

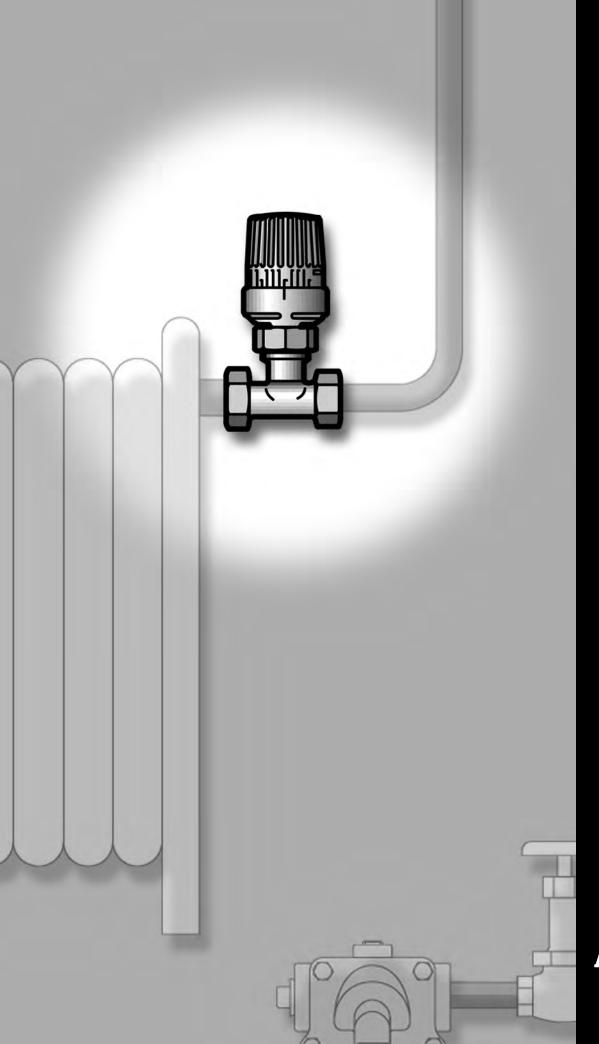


Armstrong® Tank Heater Selection Work Sheet

Tank I	Information				
	Tank Reference Number			-	
	Tank Type			-	
	Tank Material			-	
	Dimensions			_ feet	
	Insulated?	-			
	Open Top?				
	Tank Level (% full) or Flu				
	Design Ambient Air Tem				
	Design Wind Velocity (if	outside and not ir	nsulated)	_ mpn	
Steam	Information				
	Steam Pressure	psig			
	Saturated?		emperature?	_ °F	
Fluid I	Information				
	Type of Fluid				
	Properties (not required				
	Specific Gravity			°F	
	or Density	lb/cu ft at		- · °F	
	or Density				
	2. Specific Heat	- °F			
	Viscosity (at least one units	value required, p		-	
				_ °F	
Heatir	ng Requirements				
ricatii	A. Through Load		LISGPM at	°F	not annlicable
	B. Heat-Up Load from _	°F to	0501 W at	hours	not applicable
	C. Maintenance Load to			nours	not applicable
	D. Total Heat Load (if kn		_ ·		
	D. Total Fleat Load (ii kii		Btu/III		
Tank I	Heater Requirement 1. Materials of Construct	ion			
	A. Carbon Steel			-	
	B. Type 304L Stainles C. Type 316L Stainles			-	
	2. Type of Unit				
			(preference? Hairpi	n	Rayonet
			(preference? Hairpi		
			OK?If not,		
	3. Maximum tank openin	g to insert heater	into the tank:	inches	s.
Other	Information				

Notes	Armstrong
Designs, materials, weights and performance ratings are approximate and subject t	o change without notice. Visit armstronginternational.com for up-to-date information.





Radiator Products

Armstrond



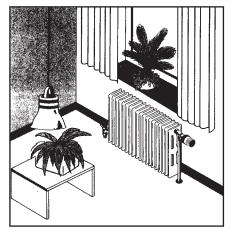


Armstrong® Radiator ID Chart

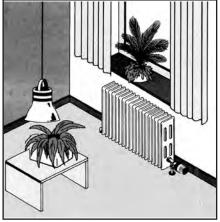
III. and an all a se	T	Body	Conn.	Max. Allow.	TMA	Body	Madal	Max. Oper.		Connecti	on Size		Located
Illustration	Type	Pattern	Туре	Press. psig	°F	Material	Model	Press. psig	1/8"	1/4"	1/2"	3/4"	on Page
	SV-12 Steam Radiator System Air Vents	Straight Angle (1/8" only)	NPT	15	250	Nickel Plated Brass	SV-12	15	•	•	•	•	422
	AV-11, AV-13 Hydronic			200 Hydronic			AV-11	50	•				
	System Air Vents	Straight	NPT	350 Hydronic	210	Brass	AV-13	150			• Female	• Male	423
											remale	Iviale	
Illustration	Туре	Body	Conn.	Max. Allow.	ТМА	Body	Model	Max. O	per. Press.	Co	nnection \$	Size	Located
illustration	Туре	Pattern	Туре	Press. psig	°F	Material	Woder	ŀ	psig		3/4"	1"	on Page
	Series TS-2/TS-3 Radiator	Straight		50	300		TS-2		50	•	•		
	Trap Capacities to 1 600 lb/hr	Angle	Threaded	65	315	Bronze	TS-3		65		•	•	424
Illustration	Туре	Body	Conn.	Max. Allow.	тма	Body	Model	Max. Oper.		Connecti	on Size		Located
mustration	.,,,,,	Pattern	Туре	Press. psig	°F	Material	Model	Press. psig	1/2"	3/4"	1"	1-1/4"	on Page
	RV-4 Radiator Valves	Straight Angle Reverse Angle	NPT Solder (1/2 & 3/4)	15 Steam 150 Water	250	Nickel Plated Brass	RV-4	15 Steam 150 Water	•	•	•	•	420
	LV-4, WV-4, MV-3, LV-4W, EV-4 Radiator Operators Remote Sensors Available	_	_	_	250	Plastic (Luron)	LV-4 WV-4 MV-3 LV-4W EV-4	_	Us	sed with a	bove RV-4	ı	421

Typical Radiator Valve Applications

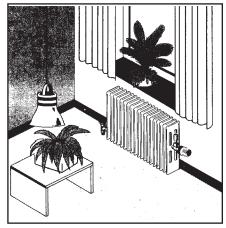




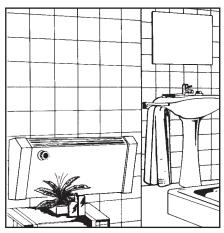
LV-4 with RV-4 reversed angle body, on free standing two-pipe steam radiator.



LV-4 with RV-4 reversed angle body on forced hot water radiator.



LV-4 with RV-4 one-pipe steam body on free standing radiator.



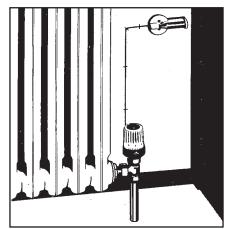
Convector with accessible thermostat. A LV-4 is shown, and in some cases a remote sensor is available.



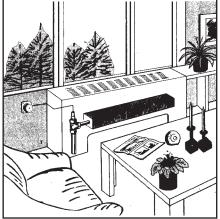
LV-4 with remote sensor. Valve is covered by a curtain; remote sensor has been mounted away from the curtain.



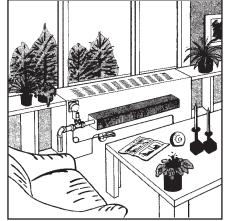
LV-4 with remote sensor. The sill creates a heat pocket; in this case a thermostat with remote sensor is necessay.



LV-4 remote sensor with RV-4 angle body. Vertically installed thermostats require a remote sensor.



LV-4W with a RV-4 angle body. An inaccessible radiator valve requiring a remote control and adjuster unit.

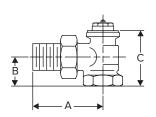


LV-4W remote sensor with RV-4 straight body to insulate sensor from heat influence or cover, remote sensor is necessary.

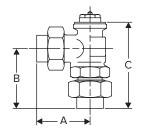
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



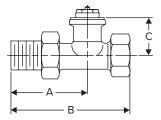
RV-4 Thermostatic Radiator Valves



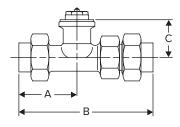
RV-4 Angle



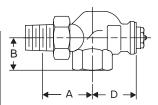
RV-4 Angle Solder



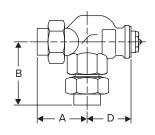
RV-4 Straight



RV-4 Straight Solder



RV-4 Reversed Angle



RV-4 Reversed Angle Solder

For Hot Water and Low Pressure Steam

Armstrong's thermostatic radiator valves are offered in straight, angle and reversed angle patterns. Thermostatic operators provide accurate and automatic control of space temperature. They are ideal for hot water and low pressure steam heated convectors, radiators, thermostatically controlled hydronic or low pressure heat exchangers. Five styles of thermostatic operators are available with liquid, liquid remote or low density wax sensors.

For a fully detailed certified drawing, refer to:

RV-4 Angle CDY #1049 RV-4 Straight CDY #1050 RV-4 Reversed Angle CDY #1051

Physical Dat	Physical Data—Valve Bodies																					
Pattern	Angle									Straight						Reversed Angle						
Pipe Conn.	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
FPT x MPT	1/2	15	3/4	20	1	25	1-1/4	32	1/2	15	3/4	20	1	25	1-1/4	32	1/2	15	3/4	20	1	25
"A"	2-5/16	59	2-5/8	66	2-15/16	59	3-7/16	65	2-15/16	59	2-1/2	64	3-1/8	73	3-9/16	90	2-3/8	60	2-5/8	66	3	76
"B"	1	25	1-1/8	28	1-5/16	33	1-9/16	39	3-3/4	95	4-3/16	106	4-15/16	78	6	150	1-1/16	27	1-3/4	44	1-5/16	33
"C"	1-15/16	49	2-1/16	52	2-3/8	60	2-3/4	70	1-1/8	28	1-1/8	28	1-1/8	28	1-3/8	35	_	-	_	-	_	-
"D"	-	-	-	-	_	_	_	-	_	-	_	-	_	-	-	-	1-9/16	40	1-3/8	35	1-1/2	38
Weight, Ib (kg)		3/4 (0).34)		1-1/2 (0	.68)	1-3/4 (0.79)	3/4 (0.	34)	1 (0.	45)	1-1/2 (0	.68)	1-3/4 (0).79)	1 (0.4	-5)	1-1/4 (0).56)	1-1/2 (0).68)

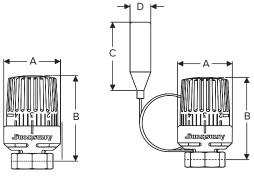
Physical C	ata—	Sold	er Val	ve B	odies								
Pattern		Ang	gle			Stra	ight		Reversed Angle				
Pipe	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	
Connection Solder	1/2	15	3/4	20	1/2	15	3/4	20	1/2	15	3/4	20	
"A"	1-7/8	47	2-1/4	57	1-7/8	47	2-5/32	55	1-3/4	44	2-1/4	57	
"B"	2-5/32	55	2-1/2	64	4-7/16	113	5-1/4	133	2-3/16	56	3-1/8	79	
"C"	3	76	3-1/2	89	1-1/4	32	1-5/32	29	-	-	-	-	
"D"	-	-	-	-	-	-	-	-	1-1/2	38	1-1/2	38	
Weight, lb	3/4 (0).34)	1(0.4	45)	3/4 (0	.34)	1 (0.4	15)	1-1/4 (0	0.56)	1-1/3 (0	0.60)	

Pressure/Temperatures	Pressure/Temperatures										
Model	"A" Insert (Standard On All Valves)	"S" Insert (Provides Longer Life on Steam Service)									
Maximum Steam, psig (barg)	15 (1)										
Maximum Temp. °F (°C)	250 (121)										
Max. Diff.—Water, psig (barg)		15 (1)									
Max. Static Pressure, psig (barg)		150 (10)									

NOTE: Normally closed insert available.

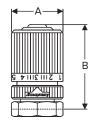
Thermostatic Operators



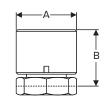


LV-4 Operator Liquid Sensor

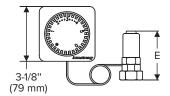
LV-4 Operator Remote Sensor



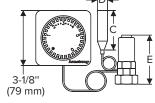
WV-4 Operator Low Density Wax Sensor



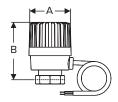
MV-3 Operator*



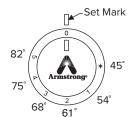
LV-4W Operator (Wall Mount)



LV-4W w/Remote Sensor



EV-4 Electric Operator 24 VAC N.C. or N.O.



Thermostatic Radiator Valve In-Service Repair Tool for Valve Repair Without Interrupting Operation

Failures of thermostatic radiator valves are frequently caused by solid matter suspended in the heating medium, such as weld or solder beads, dirt particles, etc. This results in the loss of the shut-off function of the valve through damage to the sealing surface of the valve and seat.

The use of an Armstrong In-Service Repair Tool provides a quick and easy way to remove the valve insert from an Armstrong radiator valve. Valve repair can then be accomplished without draining the heating system or interrupting its operation.



The LV-4 can be easily adjusted to a comfortable temperature. The temperature to scale relationship is shown to the left. The lowest setting provides freeze protection at approximately 45°F with a high setting of 82°F. Temperature settings on all LV-4 Operators may be limited or locked.

For a fully detailed certified drawing, refer to:

LV-4 Operator Liquid Sensor CDY #1053
LV-4 Operator Remote Sensor CDY #1054
MV-3 Operator CDY #1058
LV-4W Operator (Wall Mount) CDY #1055
LV-4W w/Remote Sensor CDY #1056
EV-4 Electric Operator CDY #1056
WV-4 Operator Low Density Wax Sensor CDY #1062

Specifications—Val	Specifications—Valve Bodies and Operators										
Name of Part	Name of Part Material										
Valve Body	Brass (nickel plated)										
Main Valve	"A" insert - Brass	"S" insert									
Main Valve Seat	"A" insert - EPDM	chrome nickel plated									
Operator Body	Lı	uron									
O-rings	EF	PDM									

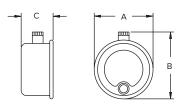
Physical Data—Thermos	tatic Op	erators	5											
Туре	LV-4 O Operator w/Li w/Liquid Rem		LV-4 Op w/Liq Remo	uid Operator w/ Low Density		MV-3 Operator*		LV-4W Operator (Wall Mount)		LV-4W Operator w/Remote Sensor		EV-4 Electric Operator		
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
"A"	2-1/8	54	2-1/8	54	1-7/16	37	1-1/2	38	_	_	_	_	2	50
"B"	3-5/16	84	3-5/16	84	2-9/16	65	1-1/2	38	_	_	_	_	2-3/4	70
"C"	_	_	2-7/8	73	_	_	_	_	_	_	2-7/8	28	_	_
"D"	_	_	3/4	20	_	_	_	_	_	_	3/4	20	_	-
"E"	_	_	_	_	_	_	_	_	3	76	3	76	_	_
Remote Operator	_	_	-	_	_	_	-	_	3-1/8 x 3-1/8	79 x 79	3-1/8 x 3-1/8	79 x 79	_	_
Capillary Length, ft (m)	_		6-1/2 or (2 or		-	_	-	-	_		6-1/2 or 16-1/2 (2 or 5)		_	
Weight, lb (kg)	1/3 (0).15)	1/2 or (0.23 or		1/4	(0.11)	1/8 (0).05)	3/4 (0.3	4)	1 or 1-1/ (0.45 or 0		3/4 (0).34)

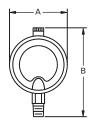
^{*}For on-off service—not thermostatic.

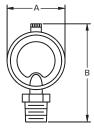
Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Armstrong SV-12 Steam Radiator Air Vent







SV-12 Straight Main Air Vent

SV-12 Angle Air Vent

SV-12 Straight Air Vent

For a fully detailed certified drawing, refer to CDY #1042.

A vent port size for every room location with the largest size for the coldest rooms and the smallest size for the "too hot" rooms. SV-12 air vents are easy to install on

For Steam Service

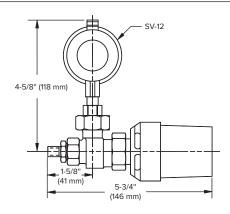
any steam radiator.



Material
Nickel plated brass
Polypropylene
Brass
Stainless steel

Physical Data							
Pattern	Angle Co	onnection	Straight C	Connection	Straight Main Connection		
Dina Cannastian Cina	in	mm	in	mm	in	mm	
Pipe Connection Size	1/8	3	1/8, 1/4	3, 6	1/2, 3/4	15, 20	
"A"	2-3/16	56	2-3/16	56	2-3/16	56	
"B"	2-5/16	59	3-1/4	83	3-1/2	89	
"C"	1-3/16	30	1-3/16	30	1-3/16	30	
Max. Operating Pressure, psig (barg)			15 (1)				
Vent Port Designation and Port Size	Each air ve	_	6 = .0935" C = .1285" .1850" all five of the abov	re vent ports	,	850" vent port provided	

RV-4 One Pipe Steam Radiator Valve



RV-4 One Pipe Steam Radiator Valve

For Steam Service

The Armstrong RV-4 One Pipe Radiator Valve is a state-of-the-art thermostatic radiator valve for low pressure steam service. The valve provides accurate and automatic control of space temperature in individual rooms through automatic air venting.

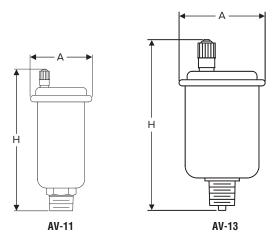
Specifications		
Name of Part	Ma	terial
Valve Body	Brass (ni	ckel plated)
Main Valve	"A" insert - Brass	"S" insert
Main Valve Seat	"A" insert - EPDM	chrome nickel plated
Operator Body	Lı	uron
O-rings	EI	PDM

Pressure/Temperatures Model	"A" Insert (Standard On All	"S" Insert (Provides Longer Life on Steam					
	Valves)	Service)					
Maximum Steam, psig (barg)	15 (1)						
Maximum Temp. °F (°C)	250 (121)						
Max. Diff.—Water, psig (barg)	15 (1)						
Max. Static Pressure, psig (barg)		150 (10)					

NOTE: Normally closed insert available.

For a fully detailed certified drawing, refer to CDY #1052.







For Hot or Cold Water and Non-viscous Liquids

Air vent models AV-11 and AV-13 are compact float-type valves for the removal of air and other gases from hydronic heating and cooling systems, liquid chilling operations and other light liquid services.

For a fully detailed certified drawing, refer to: AV-11 CDY #1047 AV-13 CDY #1048

Specificat	Specifications												
Madal	Annlination	Workin	g Pressure	Maximum Te	mperature	Connection	Hydraulic 1	Test Body					
Model	Application	psig	barg	°F	°C		psig	barg					
AV-11	Hot or	1 - 50	0.06 - 3.4	240	00	NDT Coroused	200	14					
AV-13	Cold Water	1 - 150	0.06 - 10.3	210	99	NPT Screwed	350	24					

Capacit	Capacities										
	AV	-11			AV	-13					
	ΔP Capacities				ΔP	Capacities					
psig	barg	cfm	m³/hr	psig	barg	cfm	m³/hr				
3.5	0.24	0.5	0.84	16	1.1	1	1.7				
10	0.69	1.0	1.7	48	3.3	2	3.4				
24	1.7	1.5	2.5	84	5.8	3	5.1				
35	2.4	1.9	3.2	120	8.3	4	6.8				
50	3.4	2.0	3.4	150	10	4.9	8.3				

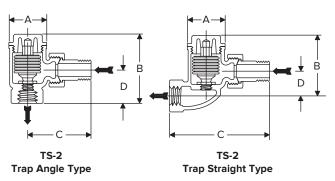
Materials		
Valve	Float	Disc
Brass	Polypropylene	Nitrila

Physical Data				
Model	AV	'-13		
Connection Size	in	mm	in	mm
	1/8 v	3	1/2 Female	15 Female
	1/6 V	3	3/4 Male	20 Male
"A"	1-3/4	44	2-1/8	54
"H"	3-3/8	86	4-5/8	118
Weight, lb (kg)	1/4 (0.11) 1/2 (0.23)			0.23)

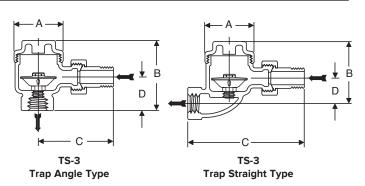


TS-2/TS-3 Radiator Traps

For Pressures to 65 psig (4.5 barg)...Capacities to 1 600 lb/hr (726/kg)



Armstrong Series TS radiator traps are offered in both angle and straight patterns. The TS-2 has a balanced pressure thermostatic element with a high quality multiple-convolution bellows. It's ideal for draining equipment such as steam radiators and convectors, small heat exchangers, unit heaters and steam air vents. The TS-2 comes with a strong cast bronze body and a stainless seat. The valve and seat are renewable in-line. The TS-3 is a heavy duty wafer type trap for the drainage of all types of steam radiators and convectors. Its wafer design is well suited to systems prone to water hammer, which may damage conventional bellows type units. The TS-3 is repairable in-line and has an all-stainless steel wafer element.





For a fully detailed certified drawing, refer to: TS-2 CDY #1045

TS-3 CDY #1046

Physical Data																				
Model		TS-2												TS	-3					
Pattern		Ang	gle			Stra	ight				An	gle					Stra	ight		
Dina Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1/2	15	3/4	20	1/2	15	3/4	20	1	25	1/2	15	3/4	20	1	25
"A" Diameter	1-5/8	41	1-5/8	41	1-5/8	41	1-5/8	41	2	50	2	50	2-3/8	86	2	50	2	50	2-3/8	86
"B" Height	2-15/16	75	3	76	2-11/16	68	2-7/8	73	2-7/8	73	3-5/8	92	3-7/8	98	2-5/8	61	3-3/8	86	3-1/2	89
"C"	2-9/16	65	2-7/8	73	4	102	4-1/2	114	3-1/8	79	3-1/2	89	4-1/8	105	4-7/8	124	5-1/4	133	6-1/2	165
"D"	1-3/8	35	1-5/8	41	1-1/8	28	1-5/16	33	1-3/8	35	1-5/8	41	2	50	1-1/8	28	1-3/8	35	1-5/8	41
Weight, lb (kg)	1-1/2 (0	0.68)	1-3/4	(0.79)	1-1/2 (0	0.68)	2 (0	.91)	1-1/2	0.68)	2 (0).91)	2-1/2	2 (1.1)	1-1/2	(0.68)	2-1/	4 (1)	3 (1	.4)
Maximum Allowable Pressure (Vessel Design)		50 psig @ 300°F (3.4 barg @ 149°C)					65 psig @ 315°F (4.5 barq @ 157°C)													
Pressure, psi (barg)		50 (3.4)					65 (4.5)													
Vacuum Ratings				25" M	ercury									10" M∈	ercury					

Materials				
Name of Part	TS-2	TS-3		
Cap	Bro	nze, ASTM B-62		
Body	Bro	nze, ASTM B-62		
Union Nipple	Brass, ASTM B-584			
Valve	Brass	Stainless Steel		
Valve Seat	Stainless steel	Stainless steel		
Element	Phosphor-bronze bellows	T-316 SS Wafer with T-304 SS housing		

Capacities	S				
Orifice	Size, in	5/	16	1/	8
Differentia	Differential Pressure		Mode	el No.	
Differential Pressure		TS	5-2	TS	-3
psig	barg	lb/hr	kg/hr	lb/hr	kg/hr
1	0.07	275	125	160	73
3	0.21	395	179	280	127
5	0.34	475	215	360	162
10	0.69	630	286	515	233
20	1.4	1000	454	625	283
30	2.0	1 200	544	720	327
45	3.1	1 475	669	825	374
50	3.4	1600	726	870	395
65	4.5	_	_	960	435

Capacities given are continuous discharge capacities in lb/hr (kg/hr) of hot condensate at pressure differential indicated.

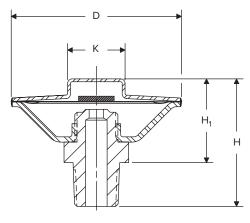
T-Wafer Radiator Trap Replacement Capsule



For Steam Service

The T-Wafer capsule is a compact, easy to install, welded wafer element. The capsule is designed so that it can be easily adapted to almost any of the popular radiator traps currently in use.

For a fully detailed certified drawing, refer to CDY #1077.



T-Wafer Capsule



Specifications and Materials									
Application	Max. Max. Oper. Oper. psig Temp. (barg) °F (°C)		Materials						
			Body	Seat	Wafer				
Steam	65 (4)	312 (156)	T-304 SS	T-316 SS	T-316 SS				

Physica	l Data						
- 1	_	*	Н	H	1,	K	
in	mm	in	mm	in	mm	in	mm
1-1/2	38	1-3/16	30	3/4	20	1/2 Hex	15

*When using adapter extension or using extra tall adapter, add 1/2" (15 mm).

For a complete listing of popular models adaptable to the T-Wafer, contact your Armstrong Representative.

Specify the following when ordering T-Wafers

Trap Manufacturer — Trap Model Number — Trap Connection Size — Trap Pattern (on some models)



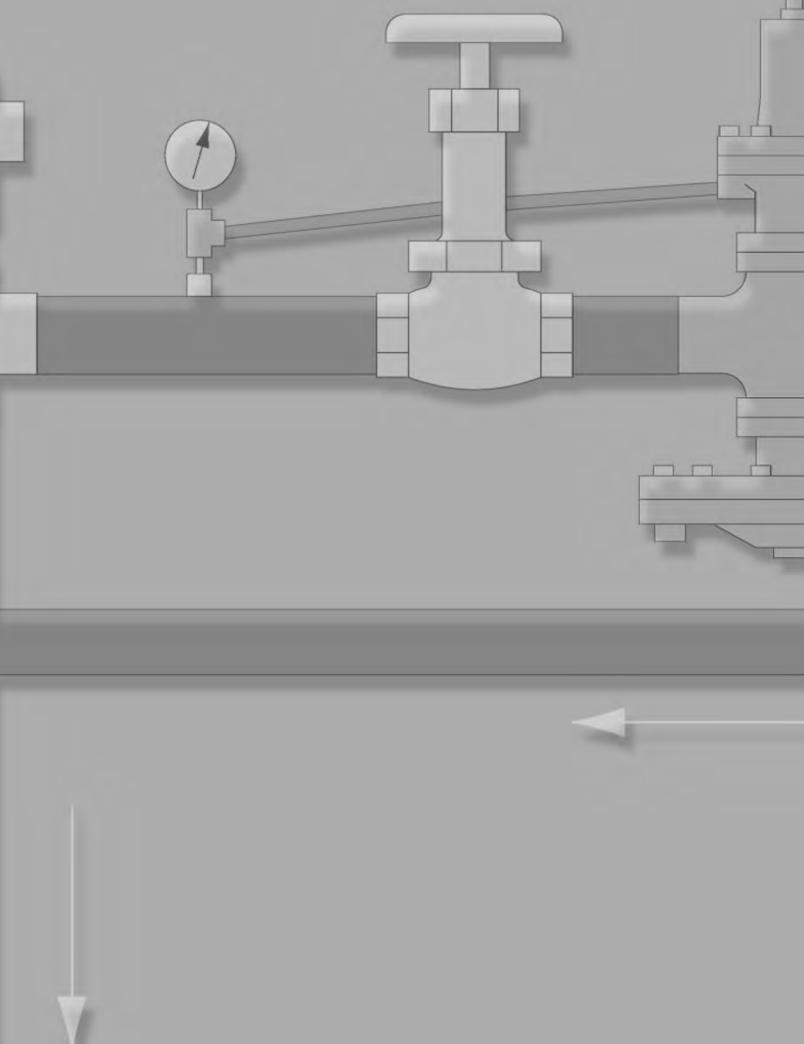
Armstrong T-Wafer Radiator Trap Replacement Capsule

Tron Manufacture	to the T-Wafer	Tron Comment :	Association Post No.	Make -		
Trap Manufacturer	Trap Model	Trap Connection	Armstrong Part No.	Notes		
-	122 3045	1/2"	B7413			
Barnes & Jones	6	+	B7418	Integral Seat		
-	134	3/4"	B7437	_		
	TH2A	- 3/4	B7412			
-	1E		B7430	Removable Seat		
Dunham Bush	1E	1/2"	B7415			
Julilalii Busii	2E	3/4"	B7413	Integral Seat		
	V1B	3/4	B7415	Integral Seat		
	17C	1/2"	B7416			
	8	1 "2	B7432			
loffman	8C		B7416			
	9	3/4"	B7432			
		1/2"	B7409			
linois	3G		B7431			
	2-7	3/4"	B7411			
	1		B7409	Removable Seat		
1arsh -	2	1	B7403	Kemovable Seat		
-	2 1N	1/2"	B7427			
	30	- " ²	B7409			
lonash-Younker	34	1	B7403			
	E		B/41/			
-	Н	1/2" & 3/4"	B7409			
Sarco	<u> </u>	1"	B7428			
-	S65	1/2" & 3/4"	B/428	Trap Rated @ 65 psi		
	B1	1/2 & 3/4	B7409	Removable Seat/Non-vertical		
	B1	1	B7424	Integral Seat/Vertical Config.		
-		1/2"		Removable Seat/Vertical Config.		
rane	B1	1/2"	B7423			
	B1	-	B7426	Integral Seat/Non-vertical		
	B2		B7415	Integral Seat		
	B3	3/4"	B7412	Removable Seat		
	B3		B7436	Integral Seat		
-	02H & 02V	-	B7411	_		
-	12H5		B7419			
-	22H5	1/2"		_		
-	502	-	D7444			
-	502V-1	0/4"	B7411			
-	503	3/4"		_		
-	512, 512H & 512G	1/2"	_			
-	513	3/4"	4			
-	522H	1/2"	B7419			
-	522HB	1/2"				
-	524HB	1	4			
	533	3/4"		Removable Seat		
	5993					
	702	1/2"				
	702V-1		B7411			
Varren Webster	703	3/4"				
	712	1/2"				
	712HB	,,2	B7419			
	713	3/4"	B7411			
ļ	713HB		4			
ļ	722HB	1/2"	B7419			
	724AH & 724HB	1"	D/ =13			
	734					
	780	3/8"	B7411	High Press. Heavy Load Trap		
	781	1/2"				
	782		B7428			
	783	3/4"	D/420	Pemovahle Seat		
	784	1"	L Domovable Seat			
	902	1/2"	B7425			
	902V	1/2"	B7411			
	733H	3/4"	B7419	Heavy Load Trap		

NOTE: This is not a complete listing of adaptable traps—For a complete listing, contact your Armstrong Representative. When ordering, please specify: 1. Trap Manufacturer 2. Trap Model Number 3. Trap Connection Size 4. Trap Pattern (on some models)

NOTES	Armstrong

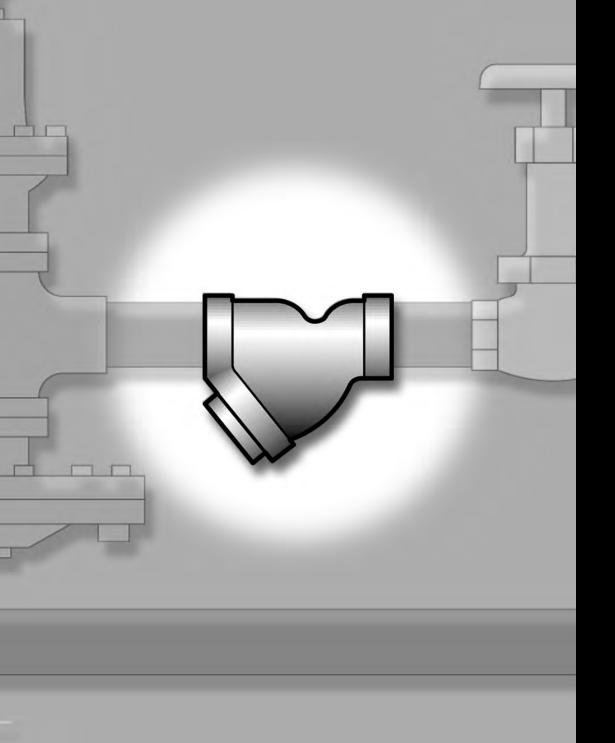
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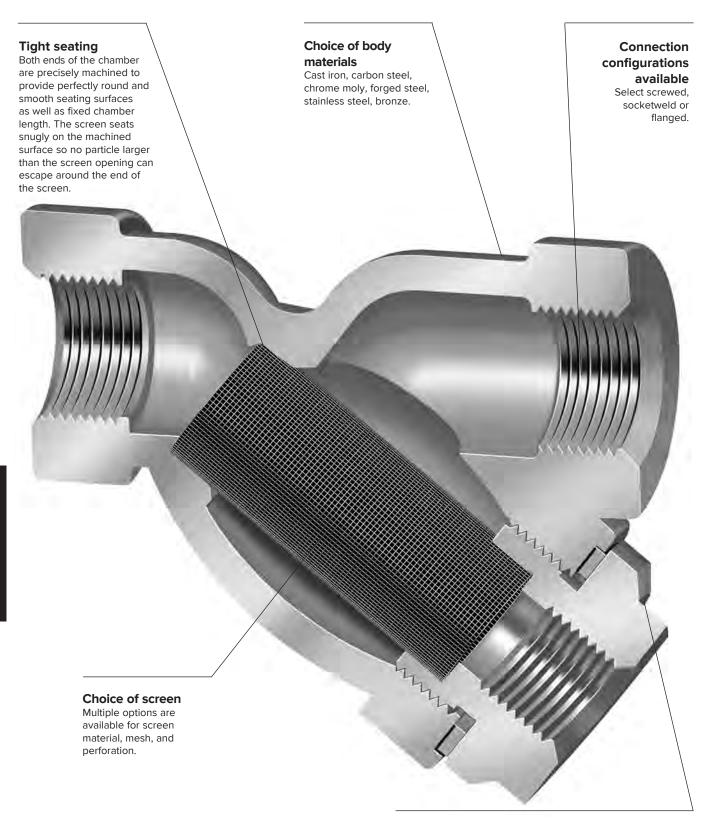
Strainers

Armstrone









Easy-in, easy-out screwed screen retainers

Straight threads mean less torque is required to obtain a tight seal with proper gasket compression, and less torque is required to remove the retainer. The danger of "freezing in" is considerably less than with hard-to-break tapered pipe threads.

Armstrong Y-Type Strainers



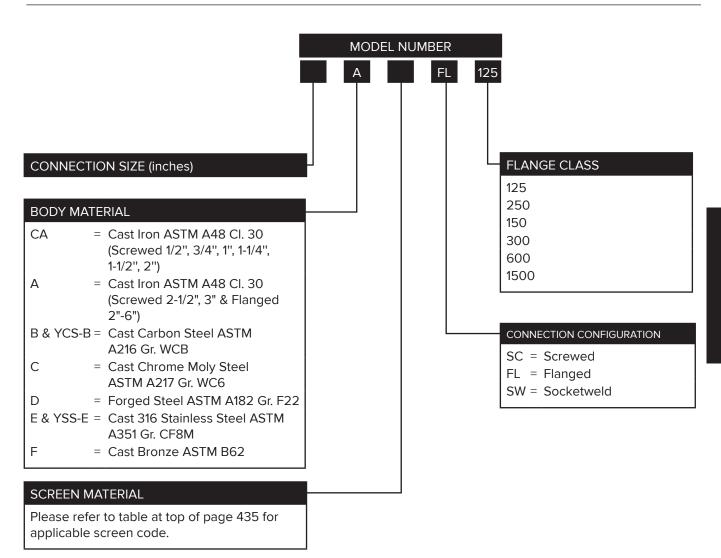
Design Advantages

No-Leak, No-Crush Screen Chambers are assured by precise machining of both ends of the chamber to provide perfectly round and smooth seating surfaces as well as fixed chamber length. The screen seats snugly on the machined surface so no particle larger than the screen opening can escape around the end of the screen.

Easy-In, Easy-Out Screwed Screen Retainers have straight threads. Less torque is required to obtain a tight seal with proper gasket compression. Less torque is required to remove the retainer. The danger of "freezing in" is considerably less than with hard-to-break tapered pipe threads.

Off-Center Blowdown Connections for 2-1/2" and 3" size strainers. The off-center drain permits nearly complete removal of liquid and dirt when blowing down the strainer. And less liquid spills when removing the screen retainer.

How To Order





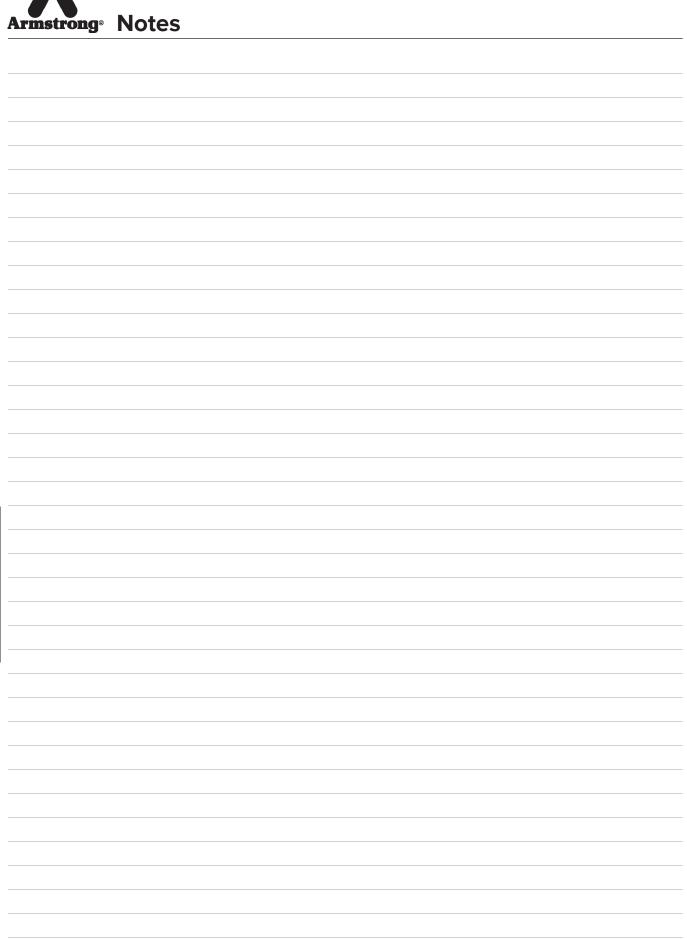
Armstrong Strainers ID Charts

				B 1 ** · · ·	Pressure Tempe	erature Ratings	Located
Illustration	Model	Connection Size	Connection Type	Body Material	Steam Non-shock	Cold Non-shock	on Page
	CA	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	Coround		250 psig @ 406°F	400 psig @ 150°F	436
	А	2-1/2", 3"	Screwed	Cast Iron ASTM-A48	250 psig @ 406 F	400 psig @ 150 F	436
пп	А	2"		Class 30			437
	Α	2-1/2" - 6"	125 Flanged		125 psig @ 353°F	175 psig @ 150°F	437
	Α	2"					437
	А	2-1/2" - 6"	250 Flanged		250 psig @ 400°F	400 psig @ 150°F	437
	В	1/2", 3/4", 1"	Screwed & Socketweld 900 lb	d Cast Carbon Steel ASTM-A216 Gr. WCB	1635 psig @ 609°F	2 220 psig @ 100°F	438
	В	1-1/4", 1-1/2", 2", 3"	Screwed & Socketweld 600 lb		1 135 psig @ 562°F	1 480 psig @ 100°F	438
	В	1/2", 3/4", 1"					439
	В	1-1/4", 1-1/2"	Class 150 Flanged		205 psig @ 390°F	285 psig @ 100°F	439
В	YCS-B	2" - 12"					440
	В	1/2", 3/4", 1"					439
	В	1-1/4", 1-1/2"	Class 300 Flanged		605 psig @ 490°F	740 psig @ 100°F	439
	YCS-B	2" - 12"					440
di la la la la la la la la la la la la la	В	1/2", 3/4", 1"			1135 psig @ 562°F	1 480 psig @ 100°F	439
YCS-B	В	1-1/4", 1-1/2"	Class 600 Flanged				439
	YCS-B	2" - 12"					440
	С	1/2", 3/4", 1"	Screwed &		2 090 psig @ 643°F	3 000 psig @ 100°F	441
	С	1-1/4", 1-1/2", 2"	Socketweld 1 500	Cast Chrome Moly	2 515 psig @ 670°F	3 600 psig @100°F	441
	С	1/2", 3/4", 1"	Class 1 500	Steel ASTM-A217 Gr. WC6	2 090 psig @ 643°F	3 000 psig @ 100°F	442
	С	1-1/4", 1-1/2", 2"	Flanged		2 515 psig @ 670°F	3 600 psig @ 100°F	441
	D	1/2", 3/4", 1", 1-1/4", 1-1/2", 2"	Socketweld 2 500 lb	Forged Steel ASTM-A182 Gr. F22	2 500 psig @ 1 025°F	6 000 psig @ 100°F	442

Strainers ID Charts



Illustration	Madel	Composition Si	Connection T	Dedy Meteric!	Pressure Tempe	erature Ratings	Located
Illustration	Model	Connection Size	Connection Type	Body Material	Steam Non-shock	Cold Non-shock	on Page
	Е	1/2", 3/4", 1"	Screwed & Socketweld 1 500 Ib		2 090 psig @ 643°F	3 000 psig @ 100°F	443
	Е	1-1/4", 1-1/2", 2", 3"	Screwed & Socketweld 600 lb		935 psig @ 538°F	1 140 psig @ 100°F	443
	Е	1/2", 3/4", 1"			200 psig @ 386°F	275 psig @ 100°F	444
	Е	1-1/2"	Class 150 Flanged	Cast Stainless Steel			444
	YSS-E	2" - 12"		ASTM-A351 Gr. CF8M			445
	Е	1/2", 3/4", 1"					444
	Е	1-1/2"	Class 300 Flanged		495 psig @ 467°F	720 psig @ 100°F	444
	YSS-E	2" - 12"					445
U	E	1/2", 3/4", 1"			935 psig @ 540°F		444
	Е	1-1/2"	Class 600 Flanged			1 440 psig @ 100°F	444
YSS-E	YSS-E	2" - 12"					445
	F 1/2", 3/4", 1", 1-1/4"					446	
	F	1-1/2", 2"	Screwed 300 lb	Cast Bronze ASTM-B62	300 psig @ 422°F	500 psig @ 150°F	446



Screen Data



Screen Material Availability and Particle Retention Size													
	Screen Specification		Back-Up Screen	Materials									
Screen Sp			Required	304 SS	Monel	Brass	316 SS						
	1/64"	0.016	3" - 10"	Code 10	Code 18	_	_						
	1/32"	0.031	None	Code 11	Code 19	_	Code 31						
	.045 (3/64")	0.045	None	Code 1	Code 3	Code 4	Code 7						
Perforated	1/16"	0.062	None	Code 12	Code 12 – -		Code 32						
	1/8"	0.125	None	Code 8	Code 21	Code 28	Code 33						
	3/16"	0.188	None	Code 13	Code 22	_	Code 34						
	1/4"	0.25	None	Code 14	Code 23	_	Code 35						
	20 x 20	0.034	6" - 10"*	Code 15	Code 5**	_	_						
	24 x 110	0.0056	5" - 10"	_	Code 24	_	Code 2						
Maala	40 x 40	0.015	1-1/2" - 10"	Code 16	Code 6	_	Code 37						
Mesh	100 x 100	0.0055	All sizes	Code 9	Code 25	_	Code 38						
	150 x 150	0.0041	All sizes	Code 40	_	_	_						
	200 x 200	0.0029	All sizes	Code 17	_	_	Code 39						

^{*}Except 6" - 125 lb cast iron

Shade indicates only available screen choices for CA Series Strainers.

(1) A back-up screen is required for all YCS-B and YSS-E strainers with mesh screens. No back ups are used on perforated screens for the YCS-B and YSS-E.

(2) 24 x 110 mesh screen not available for YCS-B and YSS-E Strainers.

Ratio of C	atio of Open Area of Screen to Inside Area of Pipe Ratio—Perforated Screens Ratio—Wire Mesh Screens														
Strainer	Total Screen	Inside Area		Ra	tio—Pe	erforate	d Screer	ıs			Ratio-	Wire Me	sh Screens	5	
Size	Area, sq in	of Pipe, sq in	1/64"	1/32"	.045"	1/16"	1/8"	3/16"	1/4"	24 x 110	20 x 20	40 x 40	100 x 100	200 x 200	
1/2"	7.2	0.30	5.2	5	6.4(5)	5.2	6.9(5.4)	8.8	10	4.8(3.8)	6.6	5.2(4.1)	2.2(1.8)	2.5	
3/4"	7.2	0.53	4	3.9	5	4	5.4	6.9	7.8	3.8	5.3	4.1	1.8	2	
1"	11	0.86	3.8	3.7	4.7	3.8	5.1	6.5	7.4	3.7	5.2	4	1.7	1.9	
1-1/4"	15.9	1.49	3.2	3	3.9	3.2	4.2	5.4	6.1	3.2	4.4	3.4	1.5	1.6	
1-1/2"	23.6	2.03	3.4	3.3	4.3	3.4	4.6	5.9	6.7	3.5	4.8	2.8	1.6	1.8	
2"	34.4	3.35	3	2.9	3.8	3	4.1	5.2	5.9	3.2	4.4	2.6	1.5	1.6	
2-1/2"	54.4	4.78	3.4	3.3	4.2	3.4	4.5	5.8	6.6	3.3	3.5 ⁺	2.7	1.7	1.9	
3" 125#	74	7.39	1.7	2.9	3.7	3	4	5.1	5.8	2.9	3.1 ⁺	2.3	1.5	1.7	
3" 250#	87	7.39	2	3.4	4.3	3.5	4.7	6	6.8	3.5	3.8 ⁺	2.8	1.8	2	
4" 125#	123	12.7	1.7	2.8	3.5	2.9	3.8	4.9	5.6	2.8	3 ⁺	2.3	1.5	1.6	
4" 250#	145	12.7	2	3.3	4.2	3.4	4.5	5.8	6.6	3.4	3.7 ⁺	2.1	1.8	2	
6" 125#	272	28.9	1.6	2.7	3.4	2.8	3.1	4.8	5.4	1.6	3	1.8	1.5	1.6	
6" 250#	317	28.9	1.9	3.1	4	3.2	4.3	5.5	6.3	1.9	2.7	2.1	1.7	1.9	
Pe	rcentage Ope	n Area	30%*	29%	37%	30%	40%	51%	58%	33%*	46%*	36%*	_	_	

NOTES: Cast steel, stainless steel and bronze strainers have the same ratios as 250 lb cast iron. This table does not apply to the YCS-B, Forged Steel F22, and YSS-E strainers (pages 440, 442, and 445).

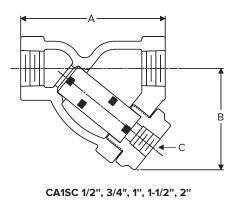
Numbers in parentheses apply to CA cast iron series only. A back-up screen is required for all YCS-B and YSS-E strainers with mesh screens. *For unbacked screens.

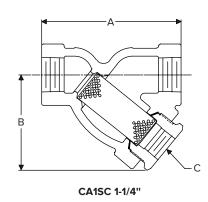
Shade indicates that back-up screens are required.

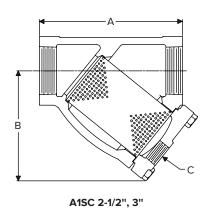
^{**}On Code 5—2-1/2" thru 10" require back-up screens

[†]Back-up required, Monel only.

Cast Iron 250 lb Screwed 1/2" - 3"



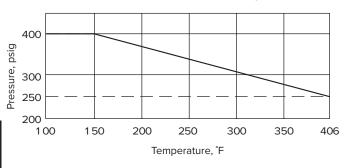




For a fully detailed certified drawing, refer to: CA1SC 1/2", 3/4", 1", 1-1/4", 1-1/2", 2" A1SC 2-1/2", 3"

CD #1111 CD #1043

Pressure/Temperature Rating





Materials: 250	Materials: 250 lb Screwed 1/2" - 3" (15 - 80 mm)													
Connections Size		Dodu	Standard Screen	Screen	Coolean	Dolkina								
in	mm	Body	Retail		Gasket	Bolting								
1/2, 3/4	15, 20													
1, 1-1/2, 2	25, 40,	ASTM A48 Class 30	304 SS .045" perforated [†]	ASTM A48	Spiral Wound	N/A								
1, 1 1/2, 2	50	Cast Iron	304 33 :043 periorated	Class 30		IV/A								
1-1/4	32	Cast IIOII		Cast Iron	Soft Steel									
2-1/2, 3	65, 80		304 SS .045" perforated [†]		Non-asbestos	Cap Screws ASTM A193 Gr. B7								

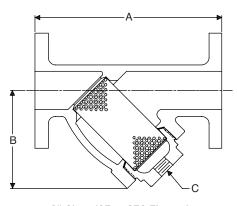
[†]NOTE: Other screen materials available. See page 435.

Physica	Physical Data: 250 lb Screwed 1/2" - 3" (15 - 80 mm)																					
		Ordering				Dimensions							n Press	ure	_							
Siz	e	Code, Standard	Weight		Weight		Weight		Weight		Α	Ĺ	В		(2	Satur Ste		ı	(66°C) shock	Screen Retainer Type	Connections
in	mm	Screen	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Type							
1/2	15		3	1.1	4.4/4	100	3	70	3/8	9.5												
3/4	20		3	1.4	4-1/4	108	3	76				17	400		Threaded	ANSI B1.20.1 Screwed						
1	25	CA466	4-1/2	2	5	127	3-3/4	95														
1-1/4	32	CA1SC	7	3	5-1/2	140	3-7/8	98	1/2	15	250			28								
1-1/2	40		10	4.5	6-5/16	160	4-7/16	113			250		400	28								
2	50		15	6.8	7-1/2	191	5-7/16	138														
2-1/2	65	A1SC	24-1/2	11	8-1/2	216	6-7/16	164	3/4	20					Doltod							
3	80	AISC	45-1/2	21	10-1/2	267	8	203	1-1/4	32					Bolted							

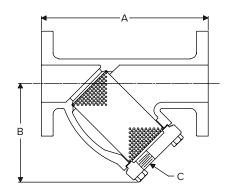
Cast Iron

Class 125 Flanged 2"-6" and Class 250 Flanged 2"-6" Armstrong





2" Class 125 or 250 Flanged



2-1/2" - 6" Class 125 Flanged, 2-1/2" - 6" Class 250 Flanged

For a fully detailed certified drawing, refer to list below:
2" Class 125 or 250 Flanged CD #1044
2-1/2" - 6" Class 125 Flanged CD #1045
2-1/2" - 6" Class 250 Flanged CD #1046



Materials: Class 125 Fl	Materials: Class 125 Flanged 2" - 6" (50 - 150 mm) and Class 250 Flanged 2" - 6" (50 - 150 mm)													
Connect	Body Screen		Gasket	Bolting	Standard Screen									
in	mm		Retainer											
2	50	ASTM		Soft Steel	N/A									
2-1/2, 3, 4, 6	65, 80, 100, 150	30	Class Cast on	Non-asbestos	Cap Screws ASTM A193	304 SS .045" perforated [†]								

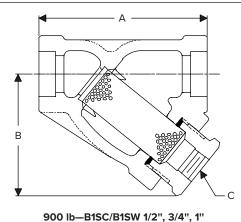
[†]NOTE: Other screen materials available. See page 435.

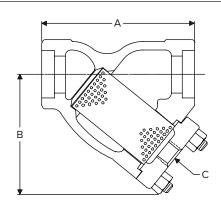
Physica	Physical Data: Class 125 Flanged 2" - 6" (50 - 150 mm) and Class 250 Flanged 2" - 6" (50 - 150 mm)															
		Ordering	Ordering				Dimensi	ions			Ма	aximu	m Press	ure		
Size Cod		Code, Standard	-,		A		В		С		Saturated Steam		1		Screen Retainer Type	Conn.
in	mm	Screen	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Туре	
2	50		22	10	9-3/4	248	5-1/8	130	1/2	15					Threaded	
2-1/2	65		36	16	11-1/16	281	6-7/16	164	3/4	20					Bolted	Class 125
3	80	A1FL125	49	22	12-1/4	311	7-1/4	184	1-1/4	32	125	8.6	175	12		ANSI B16.1 Flat Faced
4	100		83	38	14-7/8	378	9-1/2	241	1-1/4	32						
6	150		187	85	20-7/16	519	13-7/8	353	1-1/2	40						
2	50		25	11	10-1/4	260	5-1/8	130	1/2	15					Threaded	
2-1/2	65		42	19	11-11/16	297	6-7/16	164	3/4	20						Class 250
3	80	A1FL250	70	32	14-1/8	283	8-1/2	216	1-1/4	32	250	17	400	28	Poltod	ANSI B16.1
4	100		125	57	17-1/8	435	10-3/4	273	1-1/4	32					Bolted	1/16" RF
6	150		294	133	23-1/2	597	15-3/4	400	1-1/2	40						



Cast Carbon Steel (WCB)

600 lb and 900 lb Screwed or Socketweld 1/2" - 3"





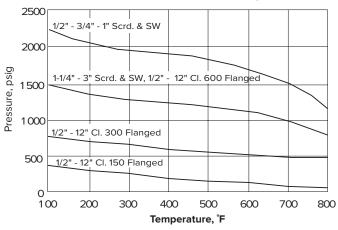
600 lb-B1SC/B1SW 1-1/4", 1-1/2", 2", 3"

For a fully detailed certified drawing, refer to: 900 lb—B1SC/B1SW 1/2", 3/4", 1"

600 lb—B1SC/B1SW 1-1/4", 1-1/2", 2", 3"

CD #1047 CD #1048

Pressure/Temperature Rating





Materials: 600 lb	and 900 lb :	Screwed or So	ocketweld 1/2" - 3" (15	- 80 mm)		
Connection	Size	Dody	Screen Retainer	Gasket	Dolting	Standard Screen
in	mm	Body	Screen Retainer	Gasket	Bolting	Standard Screen
1/2, 3/4	15, 20		ASTM A108 Gr. 1045	Coft Ctool	N/A	
1	25	ASTM A216	ASTM A108 Gr. 1040	Soft Steel	IN/A	304 SS
1-1/4, 1-1/2, 2	32, 40, 50	Gr. WCB		304 SS Spiral Wound	Studs ASTM A193 Gr. B7	.045" perforated
1-1/4, 1-1/2, 2	32, 40, 50	GI. WCB	ASTM A216 Gr. WCB	Non-asbestos	Nuts ASTM A194 Gr. 2H	.045 periorateur
3	80			Non-asbestos	Cap Screws ASTM A193 Gr. B7	

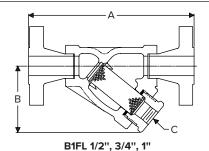
[†]NOTE: Other screen materials available. See page 435.

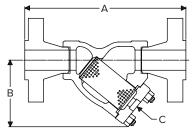
		Orderin	g Code					Dimensi	ons			Ma	aximu	m Press	ure		
Siz	:e	Stand Scre		Weig	ght	А		В		C	:	Satur Ste			(38°C) shock	Screen Retainer	Connections
in	mm	Scr'd	sw	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Type	
1/2	15			2-1/2	1	3-3/4	95	2-11/16	68	3/8	9.5						
3/4	20			3-1/2	1.6	4-3/16	106	2-15/16	75			1635	113	2 220	153	Threaded	ANSI B1.20.1
1	25			6	2.7	5	127	3-1/2	89								Screwed
1-1/4	32	B1SC	B1SW	9	4	5-1/2	140	4-3/16	106	1/2	15						
1-1/2	40			11	5	6-5/16	160	4-13/16	122			1 135	78	1 480	102	Bolted	ANSI B16.11
2	50			19	9	7-3/4	197	5-5/8	143			1 135	78	1 480	102	Boiled	Socketweld
3	80			46	21	11-3/8	289	8-3/16	208	1-1/4	32						

Cast Carbon Steel (WCB)

Class 150, 300 Flanged, and 600 Flanged 1/2" - 1-1/2"







B1FL 1-1/4", 1-1/2"

For a fully detailed certified drawing, refer to:

B1FL 1/2", 3/4", 1" CD #1050

B1FL 1-1/4", 1-1/2" CD #1051

Materials: Class	s 150, 300, aı	nd 600 Flang	ed 1/2" - 1-1/2"	(15 - 40 mm)		
Connection	on Size	Dodu	Screen	Cooket	Dalking	Standard
in	mm	Body	Retainer	Gasket	Bolting	Screen
1/2, 3/4	15, 20		ASTM A108	Soft Steel	N/A	
1	25	ASTM A216	Gr. 1045	Soft Steel	N/A	304 SS .045"
1-1/4, 1-1/2	32, 40	Gr. WCB	ASTM A216 Gr. WCB	304 SS Spiral Wound Non-asbestos	Studs ASTM A193 Gr. B7 Nuts ASTM A194 Gr. 2H	perforated [†]

[†]NOTE: Other screen materials available. See page 435.

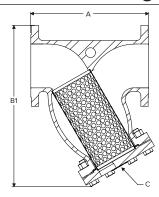
		Ordering					Dimensio	ons			Ma	aximu	m Pressu	ıre		
Siz	е	Code, Standard	Weig	ıht	Α		В		c	;	Satur Stea		100°F (non-s	•	Screen Retainer Type	Flanges
in	mm	Screen	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Туре	
1/2	15		5	2.3	6-7/8	175	2-11/16	68	3/8	9.5						
3/4	20		10	4.5	7-3/8	187	2-15/16	75							Threaded	Class 150
1	25	B1FL 150	10-1/2	4.8	8-1/2	216	3-1/2	89	1/2	15	205	14	285	20		ANSI B16.5
1-1/4	32		15	7	9	229	4-3/16	106	1/2	15					Bolted	1/16" RF
1-1/2	40		20	9	10-1/4	260	4-13/16	122							Boiled	
1/2	15		6-1/2	3	7-1/4	184	2-11/16	68	3/8	9.5						
3/4	20		12	5	7-3/4	197	2-15/16	75							Threaded	Class 300
1	25	B1FL 300	13-1/2	6	8-7/8	226	3-1/2	89	1/2	15	605	42	740	51		ANSI B16.5
1-1/4	32		17-1/2	8	9-5/8	244	4-3/16	106	1/2	15					Bolted	1/16" RF
1-1/2	40		26	12	10-3/4	273	4-13/16	122							Boiled	
1/2	15		11	5	7-11/16	195	2-11/16	68	3/8	9.5						
3/4	20		12	5.4	8-1/4	210	2-15/16	75							Threaded	Class 600
1	25		13-1/2	6	9-3/8	238	3-1/2	89	1/2	15	1135	78	1480	102		ANSI B16.5
1-1/4	32		18-1/2	8.5	10-1/4	260	4-3/16	106	1/2	15					Daltad	1/4" RF
1-1/2	40		28	13	11-5/16	287	4-13/16	122							Bolted	

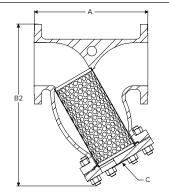
NOTE: For pressure/temperature ratings, see page 438.



Cast Carbon Steel (WCB)

Class 150, 300 Flanged, and 600 Flanged 2" - 12"





YCS-B 2"-12" (Bolts) YCS-B 2"-12" (Studs)

	Materials: Class	s 150, 300, ar	nd 600 Flang	ed 2" - 12" (50	- 300 mm)		
	Connection	on Size	Body	Screen	Gasket	Politing (P.) / Stude (P.)	Standard Screen
	in	mm	Бойу	Retainer	Gasket	Bolting (B ₁) / Studs (B ₂)	Standard Screen
ſ		50 - 300	ASTM A216	ASTM A105N	304 SS Spiral Wound Graphite	Bolts / Studs ASTM A193 Gr. B7	304 SS .045"
1		30 - 300	Gr. WCB	ASTIVI ATUSIN	304 33 Spirai Woulld Grapfille	Nuts ASTM A194 2H Zinc Plated	perforated [†]

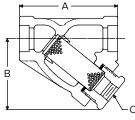
[†]NOTE: Other screen materials available. See page 435.

							Dimen	sions				Ma	aximun	n Pressu	ıre		
Si	ize	Wei	ght	А		B ₁ (bol	ts)	B ₂ (stu	ıds)	c	;		rated am		(38°C) shock	Screen Retainer Type	Flanges
in	mm	lb	kg	in	mm	in	mm	in	mm	in	mm	psig	barg	psig	barg	Турс	
2	50	40	18	8	203	8-3/32	205	8-19/32	218	1/2	15						
3	80	55	25	9-1/2	241	9-19/32	245	9-29/32	252	1	25						
4	100	104	47	11-1/2	292	11-19/32	294	11-15/16	303	1-1/2	40						Class 150
6	150	173	78	16	406	16-13/32	417	17	432			205	14	285	20	Bolted	ANSI B16.5
8	200	299	135	19-1/2	495	20-13/16	529	21-1/4	540	2	50						1/16" RF
10	250	458	208	24-1/2	622	24-19/32	625	25-1/8	638		50						
12	300	767	348	27-1/2	699	29	736	29-19/32	752								
2	50	45	21	10-1/2	267	8-7/32	207	8-1/2	216	1/2	15						
3	80	77	35	12-1/2	318	10-3/32	256	10-13/32	264	1	25						
4	100	135	61	14	356	11-13/16	300	12-7/32	310	1-1/2	40						Class 300
6	150	254	115	17-1/2	445	16-23/32	424	17-1/8	435			605	42	740	51	Bolted	ANSI B16.5
8	200	446	202	22	559	21-13/32	543	21-7/8	555	2	50						1/16" RF
10	250	650	295	24-1/2	622	25-7/32	639	25-10/16	651		30						
12	300	981	445	28	711	29-13/16	757	30-11/32	771								
2	50	64	29	11-1/2	292	9-3/32	230	9-13/32	239	1/2	15						
3	80	106	48	14	356	11-7/32	284	11-23/32	298	1	25						
4	100	211	96	17	432	13-1/2	342	14	356	1-1/2	40						Class 600
6	150	453	205	22	559	19-7/32	487	19-23/32	501			1 135	78	1480	102	Bolted	ANSI B16.5
8	200	721	327	26	660	23	585	24-1/4	603	2	50						1/4" RF
10	250	1227	556	31	787	27-13/16	707	28-15/32	723		50						
12	300	1663	754	33	838	32-29/32	835	33-10/16	854								

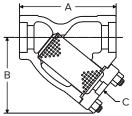
NOTE: For pressure/temperature ratings, see page 438.

Cast Chrome Moly Steel (WC6)

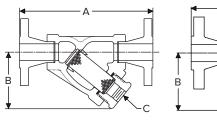
1 500 lb Screwed, Socketweld and Cl. 1 500 Flanged 1/2"- 2"Armstrong



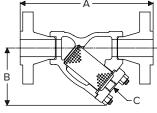
C1SC/C1SW 1/2", 3/4", 1" C



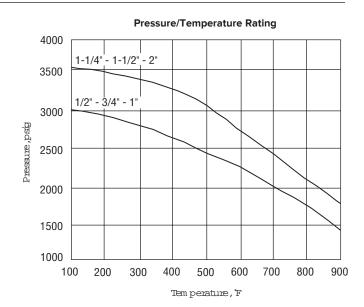
C1SC/C1SW 1-1/4", 1-1/2", 2"







C1FL 1-1/4", 1-1/2", 2"



For a fully detailed certified drawing, refer to list below:

C1SC/C1SW 1/2", 3/4", 1" CD #1055 C1SC/C1SW 1-1/4", 1-1/2", 2" CD #1056 C1FL 1/2", 3/4", 1" CD #1057 C1FL 1-1/4", 1-1/2", 2" CD #1058

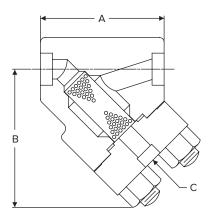
Materials: 1 500 lb	Screwed, Soc	ketweld and Cl	. 1 500 lb Flanged 1/2" -	2" (15 - 50 mm)		
Connectio	n Size	Body	Screen Retainer	Gasket	Bolting	Standard
in	mm	Войу	Screen Retainer	Gasket	Boiting	Screen
1/2, 3/4, 1	15, 20, 25	ASTM A217	ASTM A276	Soft Steel	N/A	304 SS .045"
1-1/4, 1-1/2, 2	32, 40, 50	Gr. WC6	ASTM A217 Gr. WC6	316L SS Spiral Wound Non-asbestos	Studs ASTM A193 Gr. B16 Nuts ASTM A194 Gr. 2H	perforated [†]

[†]NOTE: Other screen materials available. See page 435.

Physica	al Data	: 1 500	lb Screwe	ed, Sock	etwel	d and Cl	. 1 500) Ib Flang	ed 1/2'	" - 2 "	(15 - 5	0 mm)					
		Orderi	ng Code					Dimensio	ns			М	aximu	m Pressu	ire	6	
Siz	e		ndard reen	Weig	ht	А		В		,	С	Satur Ste		100°F (non-s	•	Screen Retainer Type	Connections
in	mm	Scr'd	SW	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Туре	
1/2	15	C1SC	C1SW	2-1/2	1.1	3-3/4	95	2-11/16	68	3/8	9.5						ANSI
3/4	20	C1SC	C1SW	3-1/2	1.6	4-3/16	106	2-15/16	75	1/2	15	2 090	144	3 000	207	Threaded	B1.20.1
1	25	C1SC	C1SW	5-1/2	2.5	5	127	3-1/2	89	1/2	15						Screwed
1-1/4	32	C1SC	C1SW*	17	8	6-3/4	171	6	152	3/4	20						
1-1/2	40	C1SC	C1SW*	17	8	6-3/4	171	6	152	3/4	20	_	173	3 600	248	Bolted	ANSI B16.11
2	50	C1SC	C1SW*	25	11	8-1/4	210	7-7/16	189	1	25						Socketweld
1/2	15	C1F	L1500	12	5	8-1/4	210	2-11/16	68	3/8	9.5						
3/4	20	C1F	L1500	15-1/2	7	9-3/8	238	2-15/16	75	1/2	15	2 090	144	3 000	207	Threaded	
1	25	C1F	L1500	22-1/2	10	10-1/4	260	3-1/2	89	1/2	15						Class 1500
1-1/4	32	C1FL	_1500*	37	17	12-1/8	308	6	152	3/4	20						ANSI B16.5 1/4" RF
1-1/2	40	C1FL	_1500*	45	20	12-7/8	327	6	152	3/4	20		173	3 600	248	Bolted	,
2	50	C1FL	_1500*	78	35	15-5/8	397	7-7/16	189	1	25						

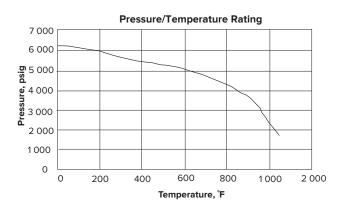
^{*}Socketweld Blowdown Connections.

Forged Steel (F22) 2 500 lb Socketweld 1/2" - 2"



D1SW 1/2" - 2"

For a fully detailed certified drawing, refer to CD #1059.





ĺ	Materials: 2 500 II	b Socketweld 1/	2" - 2" (15 - 50 ı	nm)			
	Connection	on Size	Body	Screen	Gasket	Bolting	Standard Screen
ı	in	mm	Бойу	Retainer	Gasket	Вошпу	Standard Screen
ı	1/2, 3/4, 1, 1-1/4,	15, 20, 25, 32,	ASTM A182	ASTM A182	347 SS Spiral Wound	Studs ASTM A193 Gr. B16	304 SS .045"
ı	1-1/2, 2	40, 50	Gr. F22	Gr. F22	Non-asbestos	Nuts ASTM A194 Gr. 2H	perforated [†]

[†]NOTE: Other screen materials available. See page 435.

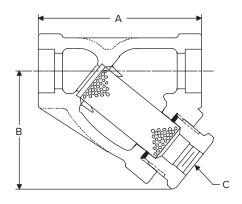
Physic	al Data	: 2 500 lb Socketwe	eld 1/2	" - 2" (15 - 50	mm)										
							Dimens	ions			М	aximu	m Press	ure		
Si	ze	Ordering Code, Standard Screen	Wei	ight	Α		В	l		C*	Satur Ste		100°F non-s		Screen Retainer Type	Connections
in	mm		lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Type	
1/2	15	D1SW -														
3/4	20		26	12	5-1/8	130	5-5/8	143								
1	25								1/2	15	2 500	172	6 000	414	Bolted	ANSI B16.11
1-1/4	32								1/2	15	2 500	1/2	8 000	414	Boiled	Socketweld
1-1/2	40		56	25	6-5/8	168	7-3/8	187								
2	50															

^{*}Socketweld blowdown connections for 1/2" (15 mm) pipe.

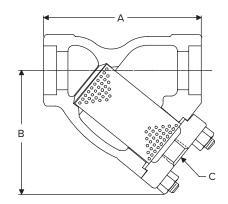
Cast Stainless Steel (CF8M)

1 500 lb and 600 lb Screwed, Socketweld 1/2" - 3"



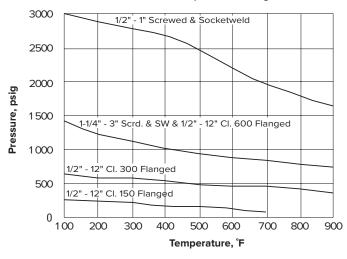


1500 Lb. E7SC/E7SW 1/2", 3/4", 1"



600 Lb. E7SC/E7SW 1-1/4", 1-1/2", 2", 3"

Pressure/Temperature Rating



For a fully detailed certified drawing, refer to: E7SC/E7SW 1/2", 3/4", 1" CD #1060 E7SC/E7SW 1-1/4", 1-1/2", 2", 3" CD #1061



Materials: 1 500 lb	Materials: 1 500 lb and 600 lb Screwed or Socketweld 1/2" - 3" (15 - 80 mm)														
Connectio	n Size	Body	Screen	Gasket	Bolting	Standard									
in	mm	Воду	Retainer	Gasket	Boiting	Screen									
1/2, 3/4, 1	15, 20, 25		ASTM A276	316 SS Flat	N/A										
1-1/4, 1-1/2, 2	32, 40, 50	ASTM A351 Gr. CF8M	ASTM A351 Gr. CF8M	304 SS Spiral Wound Non-asbestos	Studs ASTM A193 Gr. B7 Nuts ASTM A194 Gr. 2H	316 SS .045" perforated [†]									
3	80		Gr. CF8W	Non-asbestos	Cap Screws ASTM A193 Gr. B7										

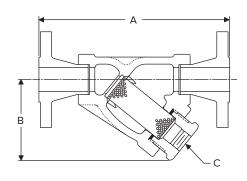
[†]NOTE: Other screen materials available. See page 435.

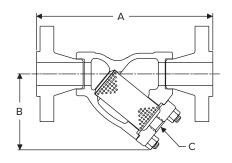
Physic	al Da	ta: 1 500	lb and 6	600 lb S	crew	ed or So	cketw	eld 1/2" - :	3" (15 -	· 80 mn	n)						
		Orderin	g Code					Dimensi	ons			Ma	ximu	ท Pressเ	ıre		
Siz	e	Stan Scr		Weig	ht	А		В		c	;	Satur Stea		100°F (non-s		Screen Retainer Type	Connections
in	mm	Scr'd	sw	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Туре	
1/2	15	4500"	4500"	2-1/2	1.1	3-3/4	95	2-11/16	68	3/8	9.5						
3/4	20	1500# E7SC	1500# E7SW	3-1/2	1.6	4-3/16	106	2-15/16	75			2 090	144	3 000	207	Threaded	ANSI B1.20.1
1	25	E/3C	E/3W	6	3	5	127	3-1/2	89								Screwed
1-1/4	32			9	4	5-1/2	140	4-3/16	106	1/2	15						
1-1/2	40	600#		11	5	6-5/16	160	4-13/16	122			025	C 4	1 110	00	Daltad	ANSI B16.11
2	50	E7SC		19	9	7-3/4	197	5-5/8	143			935	64	1 440	99	Bolted	Socketweld
3	80			50	23	11-3/8	289	8-3/16	208	1-1/4	32						



Cast Stainless Steel (CF8M)

Cl. 150, 300, and 600 Flanged 1/2" - 1-1/2"





E7FL 1/2", 3/4", 1"

E7FL 1-1/2"

For a fully detailed certified drawing, refer to list below: E7FL 1/2", 3/4", 1" CD #1071 E7FL 1-1/2" CD #1063

Materials: Class	150, 300, and 6	600 Flanged 1/2	2" - 1-1/2" (15 - 40	0 mm)		
Connection	on Size	Body	Screen	Gasket	Bolting	Standard
in	mm	Войу	Retainer	Gasket	Вошія	Screen
1/2, 3/4, 1	15, 20, 25	ASTM A351	ASTM A276	316 SS Flat	N/A	246 66 045"
1-1/2	1-1/2 40		ASTM A351 Gr. CF8M	304 SS Spiral Wound Non-asbestos	Studs ASTM A193 Gr. B7 Nuts ASTM A194 Gr. 2H	316 SS .045" perforated [†]

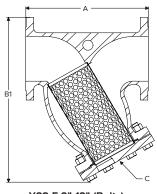
[†]NOTE: Other screen materials available. See page 435.

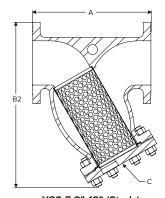
Physic	al Data	: Class 150, 30	00, and 6	00 Fl	anged 1/2	" - 1-1 /:	2" (15 - 40	mm)								
		Ordering					Dimensi	ons			М	aximu	m Press	sure		
Siz	e	Code, Standard	Weig	ıht	А		В		c	;	Satur Ste	rated am	100°F non-s		Screen Retainer Type	Flanges
in	mm	Screen	lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Туре	
1/2	15		5	2.3	6-7/8	175	2-11/16	68	3/8	9.5						
3/4	20	E7FL 150	10	4.5	7-3/8	187	2-15/16	75			200	14	275	19	Threaded	ANSI B16.5
1	25	E/FL 150	11	5	8-3/8	213	3-1/2	89	1/2	15	200	14	2/5	19		1/16" RF
1-1/2	40		20	9	10-1/8	257	4-13/16	122							Bolted	
1/2	15		6-1/2	3	7-1/4	184	2-11/16	68	3/8	9.5						
3/4	20	E7FL 300	9-1/2	4.3	7-3/4	197	2-15/16	75			495	34	720	50	Threaded	ANSI B16.5
1	25	E/FL 300	13-1/2	6	8-7/8	226	3-1/2	89	1/2	15	495	34	/20	50		1/16" RF
1-1/2	40		22	10	10-3/4	273	4-13/16	122							Bolted	
1/2	15		8-1/2	4	7-11/16	195	2-11/16	68	3/8	9.5						
3/4	20	E7FL 600	9-1/2	4.3	8-1/4	210	2-15/16	75			935	64	1 440	99	Threaded	ANSI B16.5
1	25	E/FL 600	13-1/2	6	9-3/8	238	3-1/2	89	1/2	15	935	04	1 440	99		1/4" RF
1-1/2	40		27	12	11-5/16	287	4-13/16	122							Bolted	

NOTE: For pressure/temperature ratings, see page 443.

Cast Stainless Steel (CF8M) Class 150, 300 Flanged, and 600 Flanged 2" - 12"







YSS-E	2"-12"	(Bolts)
-------	--------	---------

YSS-E 2"-12" (Studs)

Materials: C	Class 150, 30	00, and 600 F	langed 2" - 12"	(50 - 300 mm)		
Connect	tion Size	Body	Screen	Gasket	Bolting (B ₁) / Studs (B ₂)	Standard
in	mm	Body	Retainer	Odsket	Boiting (B1) / Stads (B2)	Screen
					Bolts ASTM A193 Gr. B7 Zinc Plated	
2 - 12	50 - 300	ASTM A351	ASTM A182	304 SS Spiral Wound Graphite	Nuts ASTM A194 2H Zinc Plated	316 SS .045"
2 - 12	50 - 300	Gr. CF8M	Gr. F316	304 33 Spiral Woulld Grapflite	Studs ASTM A193 B8M	perforated [†]
					Nuts ASTM A194 8M	

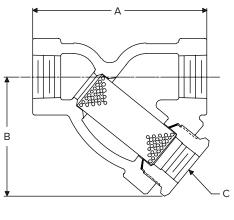
[†]NOTE: Other screen materials available. See page 435.

Phys	ical Da	ıta: Cla	ıss 150	, 300, and	d 600	Flanged 2 '	- 12"	(50 - 300	mm)								
						C	imens	sions				Ма	ximur	n Pres	sure		
Si	ize	Wei	ight	А		B ₁ (bol	ts)	B ₂ (st	uds)		;			100°F		Screen Retainer	Flanges
<u> </u>						•		_					am		shock	Type	
in	mm	lb	kg	in	mm	in	mm	in	mm	in	mm	psig	barg	psig	barg		
2	50	40	18	8	203	8-3/32	205	8-19/32	218	1/2	15						
3	80	55	25	9-1/2	241	9-19/32	245	9-29/32	252	1	25						
4	100	104	47	11-1/2	292	11-19/32	294	11-15/16	303	1-1/2	40						Class 150
6	150	173	78	16	406	16-13/32	417	17	432			200	14	275	19	Bolted	ANSI B16.5
8	200	299	135	19-1/2	495	20-13/16	529	21-1/4	540	2	50						1/16" RF
10	250	458	208	24-1/2	622	24-19/32	625	25-1/8	638		30						
12	300	767	348	27-1/2	699	29	736	29-19/32	752								
2	50	45	21	10-1/2	267	8-7/32	207	8-1/2	216	1/2 15		<u> </u>					
3	80	77	35	12-1/2	318	10-3/32	256	10-13/32	264	1	25]					
4	100	135	61	14	356	11-13/16	300	12-7/32	310	1-1/2	40						Class 300
6	150	254	115	17-1/2	445	16-23/32	424	17-1/8	435			495	34	720	50	Bolted	ANSI B16.5
8	200	446	202	22	559	21-13/32	543	21-7/8	555	2	50						1/16" RF
10	250	650	295	24-1/2	622	25-7/32	639	25-10/16	651] ~	50						
12	300	981	445	28	711	29-13/16	757	30-11/32	771	1							
2	50	64	29	11-1/2	292	9-3/32	230	9-13/32	239	1/2	15						
3	80	106	48	14	356	11-7/32	284	11-23/32	298	1	25]					
4	100	211	96	17	432	13-1/2	342	14	356	56 1-1/2 40]					Class 600	
6	150	453	205	22	559	19-7/32	487	19-23/32	501		935	64	1 440	99	Bolted	ANSI B16.5	
8	200	721	327	26	660	23	585	24-1/4	603]							1/4" RF
10	250	1227	556	31	787	27-13/16	707	28-15/32	723	2	50						
12	300	1663	754	33	838	32-29/32	835	33-10/16	854								

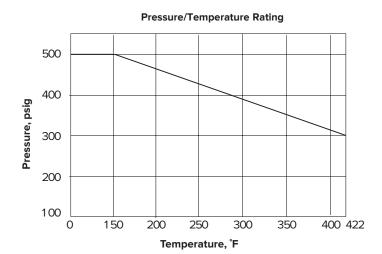
NOTE: For pressure/temperature ratings, see page 443.



Cast Bronze 300 lb Screwed 1/2" - 2"







For a fully detailed certified drawing, refer to CD #1064.



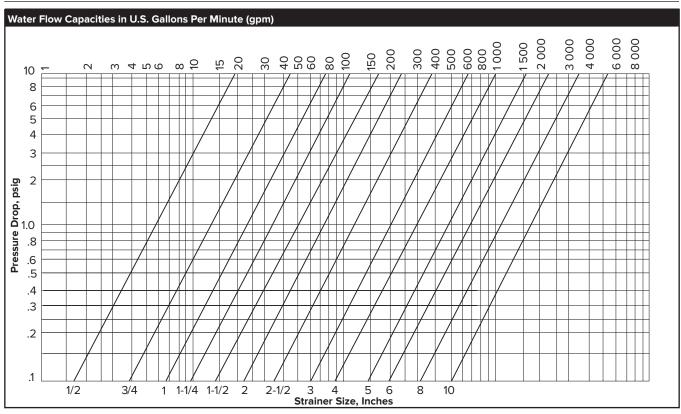
Ν	Materials: 300 lb Screwed 1/2" - 2	2" (15 - 50 mm)					
	Connection	Size	Body	Screen	Gasket	Bolting	Standard Screen
Г	in	mm		Retainer			
Г	1/2, 3/4, 1, 1-1/4, 1-1/2, 2	15, 20, 25, 32, 40, 50	ASTM B62	Brass C	Copper	N/A	Brass .045" perforated [†]

[†]NOTE: Other screen materials available. See page 435.

		Ordering					Dimen	sions			М	laximu	m Press	ure		
Siz	e	Code, Standard	Wei	ight	A	\	В		c	;	Satur		150°F non-s		Screen Retainer	Connections
in	mm		lb	kg	in	mm	in	mm	in	mm	psig	barg	psig	barg	Type	
1/2	15		1-1/2	0.68	3-1/2	89	2-1/2	64	3/8	9.5						
3/4	20		2	0.91	4	102	2-7/8	73								
1	25	F466	3-1/2	1.6	4-3/4	121	3-5/16	84			200	24	F00	24	Tl	ANSI B1.20.1
1-1/4	32	F4SC	5	2.3	5-1/4	133	4	102	02 1/2 15 300	21	500	34	Threaded	Screwed		
1-1/2	40		7-1/2	3.4	6	152	4-3/8	111								
2	50		12	5.4	7	178	5-1/2	140								

Water Flow Capacities





Armstrong Y-Type Strainers—Master Selection Table

Master Selec	tion Table						
		Siz	es	Pressure - Temp	erature Ratings	Pressure - Temp	erature Ratings
Material	Connections	in		Stand	dard	Met	ric
		III	mm	Steam, Non-Shock	Cold, Non-Shock	Steam, Non-Shock	Cold, Non-Shock
Cast Iron	Screwed - 250 lb	1/2 - 3	15 - 80	250 psig @ 406°F	400 psig @ 150°F	17 barg @ 208°C	28 barg @ 66°C
ASTM A48	Class 125 Flanged	2 - 6	50 - 150	125 psig @ 353°F	175 psig @ 150°F	8.6 barg @ 178°C	12 barg @ 66°C
Class 30	Class 250 Flanged	2 - 6	50 - 150	250 psig @ 406°F	400 psig @ 150°F	17 barg @ 208°C	28 barg @ 66°C
	Screwed & Socketweld - 900 lb	1/2 - 1	15 - 25	1 635 psig @ 609°F	2 200 psig @ 100°F	113 barg @ 321°C	153 barg @ 38°C
Cast Carbon	Screwed & Socketweld - 600 lb	1-1/4 - 3	32 - 80	1135 psig @ 562°F	1 480 psig @ 100°F	78 barg @ 294°C	102 barg @ 38°C
Steel ASTM	ASTM Class 150 Flanged		15 - 150	205 psig @ 390°F	285 psig @ 100°F	14 barg @ 199°C	20 barg @ 38°C
A216 Gr. WCB	Class 300 Flanged	1/2 - 12	15 - 150	605 psig @ 490°F	740 psig @ 100°F	42 barg @ 254°C	51 barg @ 38°C
	Class 600 Flanged	1/2 - 12	15 - 100	1135 psig @ 562°F	1 480 psig @ 100°F	78 barg @ 294°C	102 barg @ 38°C
Cast Chrome	Screwed & Socketweld - 1500 lb	1/2 - 1	15 - 25	2 090 psig @ 643°F	3 000 psig @ 100°F	144 barg @ 339°C	207 barg @ 38°C
Moly Steel	Screwed & Socketweld - 1500 lb	1-1/4 - 2	32 - 50	2 515 psig @ 670°F	3 600 psig @ 100°F	173 barg @ 354°C	248 barg @ 38°C
ASTM A217	Class 1 500 Flanged	1/2 - 1	15 - 25	2 090 psig @ 643°F	3 000 psig @ 100°F	144 barg @ 339°C	207 barg @ 38°C
Gr. WC6	Class 1 500 Flanged	1-1/4 - 2	32 - 50	2 515 psig @ 670°F	3 600 psig @ 100°F	173 barg @ 354°C	248 barg @ 38°C
Forged Steel ASTM A182 Gr. F22	Socketweld - 2 500 lb	1/2 - 2	15 - 50	2 500 psig @ 1 025°F	6 000 psig @ 100°F	172 barg @ 552°C	414 barg @ 38°C
	Screwed & Socketweld - 1 500 lb	1/2 - 1	15 - 25	2 090 psig @ 643°F	3 000 psig @ 100°F	144 barg @ 339°C	207 barg @ 38°C
Cast SS	Screwed & Socketweld - 600 lb	1-1/4 - 3	32 - 80	935 psig @ 538°F	1 400 psig @ 100°F	64 barg @ 281°C	97 barg @ 38°C
ASTM A351	Class 150 Flanged	1/2 - 12	15 - 150	200 psig @ 388°F	275 psig @ 100°F	14 barg @ 198°C	19 barg @ 38°C
Gr. CF8M	Class 300 Flanged	1/2 - 12	15 - 150	495 psig @ 467°F	720 psig @ 100°F	34 barg @ 242°C	50 barg @ 38°C
	Class 600 Flanged	1/2 - 12	15 - 100	935 psig @ 540°F	1 440 psig @ 100°F	64 barg @ 282°C	99 barg @ 38°C
Cast Bronze ASTM B62	Screwed - 300 lb	1/2 - 2	15 - 50	300 psig @ 422°F	500 psig @ 150°F	21 barg @ 217°C	34 barg @ 66°C



Armstrong Custom Fabricated Strainers



Y-Type Strainers - Forged/Cast

*Class 150 lbs. up to 24"

*Class 300 lbs. up to 24"

*Class 600 lbs. up to 24"

*Class 900 lbs. up to 16"

*Class 2 500 to 4 500 lbs. up to 8"

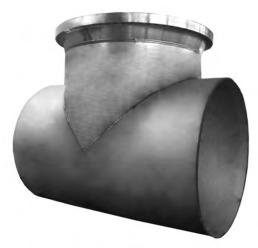




Basket Strainers

Simplex or duplex type up to 96" body and 72" connections.

Sizes and classes per customer requirements.



T-Type Strainers - Carbon Steel/Stainless Steel

*Class 150 lbs. 2" to 24"

*Class 300 lbs. 2" to 24"

*Class 600 lbs. 2" to 24"

*Class 900 lbs. 2" to 24"

*Class 1 500 lbs. 2" to 24"

*Class 2 500 lbs. 2" to 24"

Strainers are designed bolted bonnet as standard, however, pressure seal design is available for class 600 lbs. and over upon request.



^{*} Larger sizes are available upon request.

^{*} Larger sizes are available upon request.

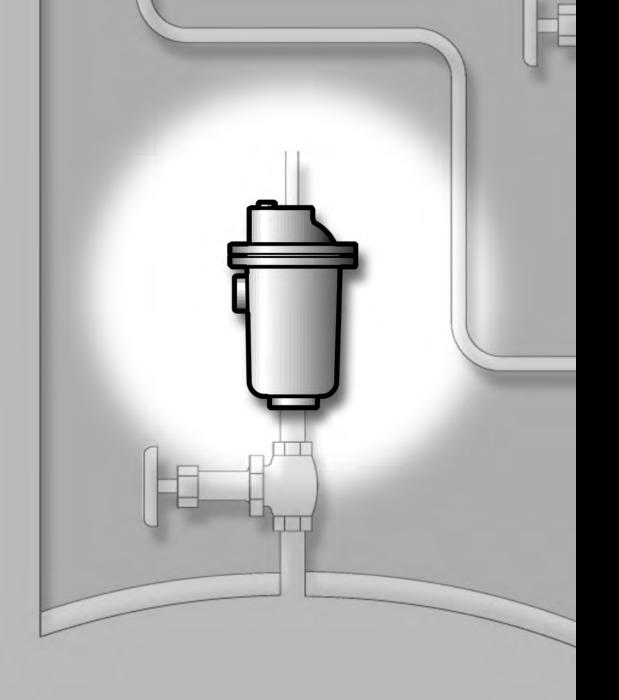
Notes	Armstrong



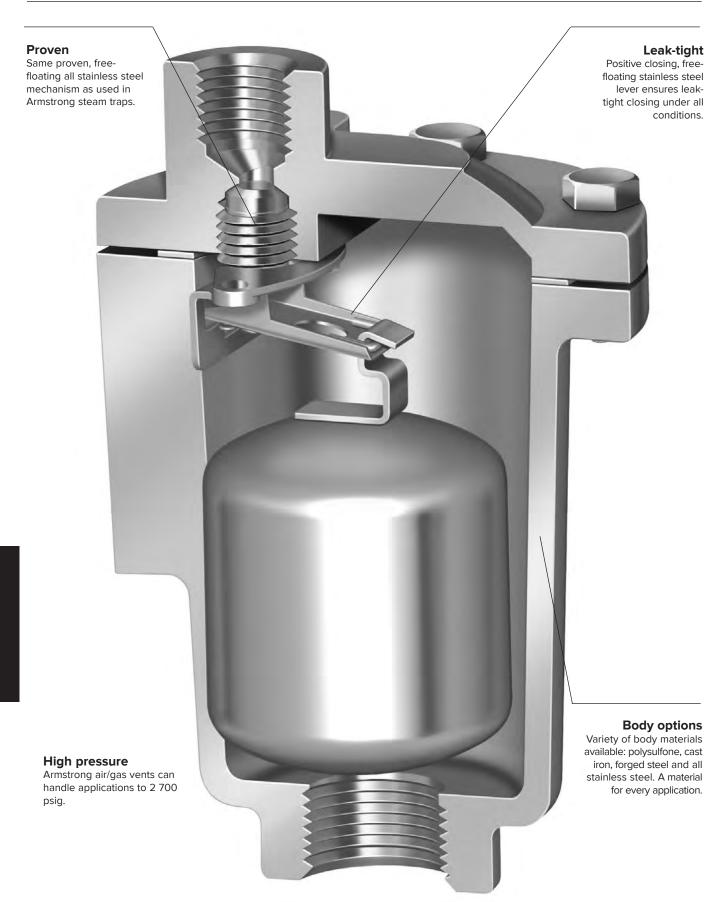


Armstrong









Selecting The Armstrong Air/Gas Vent



With the desired CFM capacity known, find the orifice size required from the table on this page. Then find the vent or vents with the correct orifice size on pages 457, 459, 461 or 469 that will operate at the required pressure with a liquid of the specific gravity being handled.

Example—Find a model number that will vent 52 cfm of air (including safety factor of 1.5 - 2.0) from a liquid with a specific gravity of 0.93 at 250 psig. Using the table below, follow the 250 psig line across to the number 60.9. Orifice size is 5/32". Now go to pages 457, 459, 461 or 469 checking the 5/32" orifice lines to locate a vent for 250 psig or higher with 0.90 gravity liquid.

NOTE: Since specific gravity falls between 0.95 and 0.90, use 0.90 gravity data. The model 3-AV on page 456 is the one to use.

For Venting During Filling Only

If a vent is required only for getting rid of air when a system is started up, such as when starting up a deep well pump or filling an empty pipe, tank or other vessel, ability of the vent to open at operating pressure can be ignored. In these cases, a model number with a large orifice for fast venting may be selected, but the vent will not open after air is expelled and the system reaches operating pressure.

$$V = \frac{W}{d} = \frac{2.05 \text{ C A P}_2 \times 60}{d} \sqrt{\left(\frac{P_1}{P_2}\right)^{.283} \left[\left(\frac{P_1}{P_2}\right)^{.283}\right]}$$

Where:

V = Volume flow rate, ft³/min W = Mass flow rate, lb/min

d = Density, 0.07494 lb/ft³ at standard conditions

C = Flow coefficient = 0.65

A = Orifice area, in²

P1 = Upstream pressure, psia

P2 = Pressure at throat orifice or downstream pressure = greater of 0.53 P1 or 14.7 psia

T = Upstream temperature = 530°R

Ref: Baumeister & Marks, Standard Handbook for Mechanical Engineers, 7th edition.

Discriure	je or A	AII IIII	rougn	an O	rifice	ın Sta	naaro	Cubi	c reet	•					ospnei	ic Pre	ssure	ot 14.	/ psia a	and 70	ľΕ	
pressure										10	ifice D	iamete	r, inche	es								
psig	1/16	5/64	3/32	#38	7/64	1/8	9/64	5/32	3/16	7/32	1/4	9/32	5/16	11/32	3/8	7/16	1/2	9/16	5/8	3/4	7/8	1-1/16
5	0.64	1.00	1.44	1.54	1.96	2.56	3.24	4.00	5.76	7.84	10.2	13.0	16.0	19.4	23.0	31.4	41.0	51.9	64.0	92.2	125	185
6	0.70	1.09	1.57	1.69	2.14	2.80	3.54	4.37	6.30	8.57	11.2	14.2	17.5	21.2	25.2	34.3	44.8	56.7	70.0	101	137	202
7	0.75	1.18	1.70	1.82	2.31	3.02	3.82	4.71	6.78	9.23	12.1	15.3	18.8	22.8	27.1	36.9	48.2	61.1	75.4	109	148	218
9	0.85	1.33	1.91	2.05	2.61	3.40	4.31	5.32	7.66	10.4	13.6	17.2	21.3	25.7	30.6	41.7	54.4	68.9	85.1	122	167	246
12	0.98	1.52	2.19	2.35	2.99	3.90	4.94	6.10	8.78	11.9	15.6	19.8	24.4	29.5	35.1	47.8	62.4	79.0	97.5	140	191	282
15	1.09	1.70	2.44	2.62	3.33	4.34	5.50	6.79	9.78	13.3	17.4	22.0	27.2	32.9	39.1	53.2	69.5	88.0	109	156	213	314
20	1.27	1.98	2.86	3.06	3.89	5.08	6.42	7.93	11.4	15.5	20.3	25.7	31.7	38.4	45.7	62.2	81.2	103	127	183	249	367
25	1.45	2.27	3.27	3.50	4.45	5.81	7.35	9.07	13.1	17.8	23.2	29.4	36.3	43.9	52.3	71.1	92.9	118	145	209	285	420
30	1.63	2.55	3.68	3.94	5.01	6.54	8.28	10.2	14.7	20.0	26.2	33.1	40.9	49.5	58.9	80.1	105	132	163	235	320	472
35	1.82	2.84	4.09	4.38	5.57	7.27	9.20	11.4	16.4	22.3	29.1	36.8	45.4	55.0	65.4	89.1	116	147	182	262	356	525
40	2.00	3.13	4.50	4.82	6.13	8.00	10.1	12.5	18.0	24.5	32.0	40.5	50.0	60.5	72.0	98.0	128	162	200	288	392	578
45	2.18	3.41	4.91	5.26	6.69	8.73	11.1	13.6	19.6	26.7	34.9	44.2	54.6	66.0	78.6	107	140	177	218	314	428	631
50	2.37	3.70	5.32	5.70	7.25	9.46	12.0	14.8	21.3	29.0	37.9	47.9	59.2	71.6	85.2	116	151	192	237	341	464	684
60	2.73	4.27	6.15	6.58	8.37	10.9	13.8	17.1	24.6	33.5	43.7	55.3	68.3	82.6	98.3	134	175	221	273	393	535	790
70	3.10	4.84	6.97	7.46	9.49	12.4	15.7	19.4	27.9	37.9	49.6	62.7	77.4	93.7	112	152	198	251	310	446	607	895
80	3.46	5.41	7.79	8.34	10.6	13.9	17.5	21.6	31.2	42.4	55.4	70.1	86.6	105	125	170	222	281	346	499	679	1 001
90	3.83	5.98	8.62	9.2	11.7	15.3	19.4	23.9	34.5	46.9	61.3	77.5	95.7	116	138	188	245	310	383	551	750	1 107
100	4.19	6.55	9.44	10.1	12.8	16.8	21.2	26.2	37.8	51.4	67.1	84.9	105	127	151	206	268	340	419	604	822	1 212
110	4.56	7.13	10.3	11.0	14.0	18.2	23.1	28.5	41.0	55.9	73.0	92.4	114	138	164	223	292	369	456	657	894	1 318
125	5.11	7.98	11.5	12.3	15.6	20.4	25.9	31.9	46.0	62.6	81.7	103	128	155	184	250	327	414	511	736	1 0 0 1	1 477
150	6.02	9.41	13.6	14.5	18.4	24.1	30.5	37.6	54.2	73.8	96.4	122	151	182	217	295	385	488	602	867	1 181	1 741
200	7.85	12.3	17.7	18.9	24.0	31.4	39.8	49.1	70.7	96.2	126	159	196	238	283	385	503	636	785	1 131	1539	2 269
250	9.68	15.1	21.8	23.3	29.6	38.7	49.0	60.5	87.1	119	155	196	242	293	348	474	620	784	968	1394	1897	2 798
300	11.5	18.0	25.9	27.7	35.2	46.0	58.3	71.9	104	141	184	233	288	348	414	564	737	932	1 151	1657	2 256	3 326
400	15.2	23.7	34.1	36.5	46.4	60.7	76.8	94.8	136	186	243	307	379	459	546	743	971	1228	1 517	2 184	2 973	4 383
500	18.8	29.4	42.4	45.3	57.6	75.3	95.3	118	169	231	301	381	471	569	678	922	1205	1525	1882	2 711	3 689	5 440
600	22.5	35.1	50.6	54.1	68.8	89.9	114	141	202	275	360	455	562	680	809	1102	1 439	1821	2 248	3 237	4 406	6 497
750	28.0	43.7	62.9	67.4	85.6	112	142	175	252	343	447	566	699	846	1007	1370	1790	2 265	2 797	4 027	5 481	8 082
1000	37.1	58.0	83.5	89.4	114	148	188	232	334	455	594	751	928	1123	1336	1 818	2 375	3 006	3 711	5 344	7 273	10 725



Armstrong[®] Air Vent ID Charts

			Flow	Connection	Max. Allow.	TMA			Max. Oper.			Con	nectio	n Siz	e	1	Located
Scriet AlvCw Scrieved 150 150 Replications 1.4VC 150 150	Illustration	Туре	1		Press.		Body Material	Model	Press.	1/8"	1/4"	1/2"	3/4"	1"	1-1/2"	2"	1
Ser-Intru Free Ser-		See-Thru Free Floating Lever	-	Screwed	150	150	Polycarbonate	1-AVC	150			•	**				454
Fixed Pivot Ball Fixe		See-Thru Free Floating Lever Air Vents for Ozone	-	Screwed	150	150	(Polybutylene Terephthalate) Polycarbonate	1-AVCW	150			•					455
Fixed Plvot Ball Float Air/Gas Vents Series 1, 2, 3, 6 Free Floating Lever Air/Gas Vents Screwed Socketweld Flanged 100 or 750 75		Fixed Pivot Ball Float Air/Gas	1	Screwed	250	450	Class 30 Cast	21-AR	250			•	•				459
Free Floating Lever Air/Gas Vents Screwed Vents Screwed Screwed Vents Screwed Vents Screwed Vents Screwed Vents Screwed Vents Screwed Socketweld Flanged m Screwed Soc		Fixed Pivot Ball Float Air/Gas		Socketweld	1	or						•	•				459
Lever Air/Gas Vents Screwed Vents Screwe			A		300	200		1-AV [†]	300			*	1				
Series 30 Free Floating Lever Air/Gas Vents Screwed Socketweld Flanged 100 or 600 750 100 or 600 750 100 or 600 100 o		Lever Air/Gas		Screwed	250	450	Class 30	3-AV	250			•		•	•		456
Socketweld Flanged 1000 or 600 750		Free Floating			1	or						•	•				
Series 10 Free Floating Lever Air/Gas Vents Screwed Socketweld Flanged *** Screwed Air/Gas Vents Screwed Air/Gas Vents Screwed Socketweld Flanged *** S		Vents		Socketweld		or		33-AV	900			•	•	•			458
Screwed Socketweld (22 and 13 only)						or		36-AV	1000						•	•	
Socketweld (22 and 13 only) Stainless Stai		Free Floating	A		I	or		11-AV **	400			•	**				
Series HLAR High Leverage Air/Gas Vents Screwed Socketweld Flanged *** Screwed Socketweld F		Vents	[Socketweld (22 and 13		or	Stainless	22-AV	555				•				460
High Leverage Air/Gas Vents Screwed Socketweld Flanged *** 100 or 750 100 or 750 2315 HLAR 1000 2315 HLAR 1000 2315 HLAR 1000 2316 HLAR 1000 2316 HLAR 1000 2316 HLAR 1500 2316 HLAR 1500 2413 HLAR 1500 2413 HLAR 1500 2415 HLAR 1800				Only)		or		13-AV	570					•			
Socketweld Flanged 100 or 750 ASTM A105 2315 HLAR 1000 1-1/4		High Leverage	A					2313 HLAR				•	•	•			
Series HLAR High Leverage Air/Gas Vents Screwed Socketweld Flanged *** 1500 or 900 or 850		Air/Gas Vents		Socketweld		or			1000					•	1-1/2 •	_	462
High Leverage Air/Gas Vents Screwed Socketweld Flanged *** 1800 0 or 900		Series HLAR			4===	100		2316 HLAR							•	•	
Flanged *** 1800 100 Forged Steel 2415 HLAR 1800 • 1-1/2 •		High Leverage	•		1	or		2413 HLAR	1500			•	•	•	1 1/4		462
2410 TILAK 1 300						l								•	1-1/2 •		402

^{★ 1/4&}quot; outlet connection

^{★★ 1/2&}quot; outlet connection

[†] Side connection available

[▲] Alternate inlet 1/2"

^{††} Side connection not available

^{†††} Flange selection may limit pressure and temperature rating.

Air Vent ID Charts



		Flow	Connection	Max. Allow.	TMA			Max. Oper.			Coni	nectio	n Size	e		Located
Illustration	Туре	Direction	Туре	Press. psig	°F	Body Material	Model	Press. psig	1/8"	1/4"	1/2"	3/4"	1"	1-1/2"	2"	on Page
	Series HLAR High Leverage Air/Gas Vents	A		2 120 or 1 700	100 or 900		25133G- HLAR	2 125			•	•	•			
			Screwed Socketweld Flanged ***	2 520 or 2 000	100 or 900	ASTM A182 Gr. F22 Forged Steel	25155G- HLAR	2 500				•	•	1-1/4		462
				3 700 or 3 000	100 or 900		26155G- HLAR	2 700					•	1-1/4		
	Series TTF Thermostatic Air Vents	<u></u>	Straight-Thru Right Angle	300	450	304-L Stainless Steel	TTF-1	300			•	•				464
	Series TV-2 Thermostatic Air Vents	†	Screwed	125	350	ASTM B62 Cast Bronze	TV-2	125			•					465
	Series TS-2 Thermostatic Air Vents	•	Threaded	50	300	ASTM B62 Bronze	TS-2	50			•	•				466
	AV-11, AV-13 Air Vents	†	Screwed	50 150	210	Brass	AV-11 AV-13	50 150	•		•	•				467
	SV-12 Steam Radiator Air Vent		Threaded	15	250	Nickel Plated Brass	SV-12	15	•	•	•	•				468

^{★ 1/4&}quot; outlet connection

^{★★ 1/2&}quot; outlet connection

[†] Side connection available

[▲] Alternate inlet 1/2"

^{††} Side connection not available

^{†††} Flange selection may limit pressure and temperature rating.



1-AVC See-Thru Air Vent

For Pressures to 150 psig (10 barg) or Specific Gravity Down to 0.80

A See-Thru Body-So You'll Know When It's Working

Now, you can literally see what you've been missing—the early warning signs of a system problem. Since you'll know the operating condition of the air vent, you won't have to waste time and money scheduling maintenance that isn't needed. In other words, you will be able to react to a condition before it becomes a problem.

A simple ball float mechanism requiring no electricity to operate, the new Armstrong 1-AVC discharges automatically only when air/gas are present. That means no liquid loss as with manual venting.

An Inside Look

See-thru body means you can observe changing conditions as they occur. See a problem in the making—instead of having to deal with it after the fact.

Efficient Operation

Simple ball float mechanism discharges only when air is present so it doesn't waste liquid.

Positive Seating

Free-floating valve mechanism assures positive seating so it prevents liquid loss. There are no fixed pivots to wear or create friction, and wear points are heavily reinforced for long life.

Reduced Maintenance

Stainless steel internals mean corrosion resistance and reduced maintenance.

Corrosion Resistance

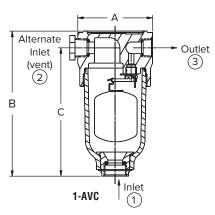
Long-lasting polysulfone body and reinforced nylon cap resist corrosion and provide long, trouble-free service life.

List of Materials	
Name of Part	Material
Cap	Reinforced Nylon*
Body	polysulfone
O-Rings (Body Cap and Fitting)	Nitrile Elastomer Compound
Float Lever and Screws	Stainless Steel
Valve & Seat	Stainless Steel
Fitting & Pipe Plug	Reinforced Nylon
Retainer Ring	Zinc Plated Steel

*UV sensitive.

Physical Data							
	in	mm					
Inlet Connection	1/2, 3/4	15, 20					
Outlet Connection	1/2	15					
"A" Face-to-Face	3-1/2	89					
"B" Height	6-3/4	171					
"C" Bottom to Q	6	552					
Maximum Allowable Pressure	150 psig @ 150°F						
(Vessel Design)	(10 barg	@ 65°C)					
Maximum Operating Pressure	150 psig	(10 barg)					
Specific Gravity Range	1.00 to 0.80						
Weight, lb (kg)	1 (.45)						





How to Order

Inlet ①	Alternate Inlet ②	Outlet ③
3/4"	1/2"	1/2"
1/2" or 3/4"	1/2" or 3/4"	1/2"

NOTE: The Armstrong 1-AVC should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.

For a fully detailed certified drawing, contact Armstrong.

Model 1-AVC C	apacity			
Differentia	l Pressure	Orifice		
psig	barg	Size	scfm	m³/hr
15	1.0		4.3	7.3
30	2.0		6.5	11.0
50	3.5		9.5	16.1
75	5.0	1/8"	13.1	22.2
100	7.0		16.9	28.7
125	8.5		20.5	34.8
150	10.5		24.2	41.3

NOTE: Discharge of air through an orifice in scfm (standard cubic feet of free air per minute) at a standard atmospheric pressure of 14.7 psig (1 barg) and 70°F

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

1-AVCW See-Thru Air Vent for Ozone Applications

For Pressures to 150 psig (10 barg) or Specific Gravity Down to 0.80



What Is Ozone?

Ozone is a gas that forms naturally during thunderstorms when lightning converts normal oxygen molecules (O2) into ozone (O3). The fresh, sweet smell in the air after a storm is the smell of ozone. The unstable ozone molecule reacts rapidly with most substances and is an extremely strong natural oxidant.

How Is Commercial Ozone Produced?

Ozone can be formed by exposing air to ultraviolet light; however, the most common method of generating ozone is by passing air through an electrical discharge. Because ozone has strong oxidizing properties, its production requires corrosion-resistant equipment.

How Is Ozone Used in Water Filtration and Purification?

Because ozone is such an effective oxidant, it kills viruses, bacteria, mold, mildew, fungus and germs. Passing ozone through water achieves high purification rates without any chemical residue. Oxygen is the only by-product.

Typical Customer Applications:

- Purifying standing ground water in Third World countries.
- · Conditioning water for poultry and livestock.
- · Purifying water in the bottled water industry.
- · Filtering and purifying water for process applications.

A See-Thru Body Shows You It's Working

Now, you can literally see what you've been missing. The Armstrong 1-AVCW See-Thru Air Vent lets you easily check its operating condition. You won't have to waste time and money scheduling maintenance that isn't needed, and you can quickly react to a condition before it becomes a problem.

Efficient Operation

Simple ball-float mechanism doesn't need electricity to operate. The air vent automatically discharges only when air or gas is present. No liquid is lost, as with manual venting.

Positive Seating

Free-floating valve mechanism ensures positive seating and prevents liquid loss. There are no fixed pivots to wear or create friction. Wear points are heavily reinforced for long life.

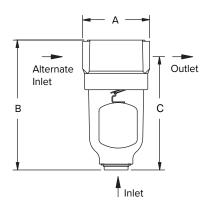
Corrosion Resistance

Long-lasting CPVC cap and polysulfone body provides trouble-free operation. T316 stainless steel internal parts resist corrosion and reduce maintenance.

Compare-and Save the Difference

Seeing really is believing—especially when you compare the Armstrong 1-AVCW See-Thru Air Vent with manual venting. Measure the time and money you can save with a more efficient, easier-to-maintain system. For more information or technical assistance, contact your local Armstrong Representative.

NOTE: The Armstrong 1-AVCW should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.



1-AVCW

List of Materials	
Name of Part	Material
Cap	CPVC
Body	Polysulfone
O-Rings (Body Cap and Fitting)	Aflas
Float Lever and Screws	T316 Stainless Steel
Valve & Seat	T316 Stainless Steel
Fitting	CPVC
Retainer Ring	Zinc Plated Steel

Physical Data						
	in	mm				
Inlet Connection (In Body)	3/4	20				
Inlet Connection (Alternate)	1/2	15				
Outlet Connection	1/2	15				
"A" Face-to-Face	3-1/2	89				
"B" Height	6-13/16	172				
"C" Bottom to Q	6	152				
Maximum Allowable Pressure (Vessel Design)	150 psig @ 150°F (10 barg @ 66°C)					
Maximum Operating Pressure	150 psig	(10 barg)				
Specific Gravity Range	1.00 to 0.80					
Weight, lb (kg)	1 (.5)				

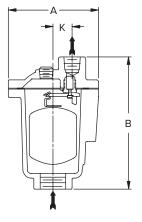
Model 1-AVC	CW Capacity			
Differentia	al Pressure	Orifice Size	scfm	m³/hr
psig	barg	Offlice Size	SCIIII	1117111
15	1.0		4.3	7.3
30	2.0		6.5	11.0
50	3.5		9.5	16.1
75	5.0	1/8"	13.1	22.2
100	7.0		16.9	28.7
125	8.5		20.5	34.8
150	10.5		24.2	41.3

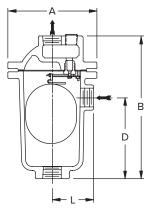
NOTE: Discharge of air through an orifice in scfm (standard cubic feet of free air per minute) at a standard atmospheric pressure of 14.7 psig (1 barg) and 70°F (21°C).



Free Floating Lever Air/Gas Vents—Cast Iron

For Pressures to 300 psig (21 barg) or Specific Gravity Down to 0.40









Model 1-AV

Model 2-AV, 3-AV and 6-AV

Armstrong free floating lever Air/Gas Vents use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service.

Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for vent size and weight. The hemispherical valve, seat and leverage are identical in design, materials and workmanship to those for saturated steam service up to 1000 psig, with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

1-AV—A cast iron air vent that uses a positive-closing free floating lever to ensure leaktight closing under all conditions. This vent is good for low capacity air/gas venting up to 300 psig.

For a fully detailed certified drawing, refer to CD #1070.

2-AV, 3-AV and 6-AV—Cast iron vents using the same proven free floating lever mechanisms used in Armstrong steam traps. For applications where high air/gas venting capacity is required up to 250 psig.

For a fully detailed certified drawing, refer to CD #1034.

Physical Data												
Model No.			C	ast Iron								
Wiodel No.	1-AV	**	2-4	AV	3-	AV	6-AV					
Pipe Connections	in	mm	in	mm	in	mm	in	mm				
Pipe Connections	1/2*, 3/4*	15, 20	1/2, 3/4	15, 20	3/4, 1	20, 25	1-1/2, 2	40, 50				
"A"	3-3/4	89	5-1/4	133	6-3/8	162	10-3/16	259				
"B"	5-1/2	140	8-3/4	222	11-1/2	292	18	457				
"D"	-	-	5-1/8	130	7	188	9-3/8	238				
"K"	13/16	21	-	-	-	-	-	-				
"L"	-	-	2-7/16	62	2-7/8	73	4-5/8	-				
Weight, lb (kg)	4 (1.8	3)	12 (!	5.5)	21 (9.5) 78 (35.5)							
Max. Allowable Pressure (Vessel Design)	300 psig @ 200°F (250 psig @ 450°F (1		250 psig @ 450°F (17 barg @ 232°C)									

*Outlet connection 1/4" (7 mm). **1-AV available with side connection if specified on order. On models 2-AV, 3-AV and 6-AV, pipe size of side connections is same as that of inlet and outlet connections. Some floats are oil filled. Consult factory for details.

List of Materi	als						
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket	Bolts	Nuts
1-AV						ASTM A193 Gr. B7	
2-AV		Ctaimlean Ctanl		ASTM A48	Non sebestes		ASTM A563
3-AV		Stainless Steel		Class 30 Cast Iron	Non-asbestos	SAE Gr. 2	Gr. A
6-AV				Cast iion			

Free Floating Lever Air/Gas Vents—Cast Iron

Armstrong®

For Pressures to 300 psig (21 barg) or Specific Gravity Down to 0.40

1-AV Maximum Operating Pressures											
Minimum Specific Gravity	0.80										
Ovifica Sina (in)	Maximum Operating Pressure										
Orifice Size (in)	psig	barg									
1/8	146	10									
7/64	173	12									
#38	219	15									
5/64	300	21									

Specific Gravity*	1.0	00	0.	95	0.90		0.	85	0.8	0.80		75	0.7	70	0.0	65	0.6	60	0.55		0.50	
Float wt., oz (g)	7.7 (217)	7.3 (206)	6.9	(195)	6.5	(184)	6.1 (174)	5.7 (163)	5.4 (152)	5.0	(141)	4.6 ((130)	4.2	(119)	3.8	(109)
Ovifice Cine (in)									M	aximur	т Оре	rating	Pressu	re								
Orifice Size (in)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	bar
5/16	27	1.8	25	1.8	24	1.7	23	1.6	22	1.5	20	1.4	19	1.3	18	1.2	16	1.1	15	1.0	14	0.9
1/4	44	3.0	42	2.9	40	2.7	38	2.6	35	2.4	33	2.3	31	2.1	29	2.0	27	1.8	24	1.7	22	1.5
3/16	97	6.7	92	6.4	88	6.0	83	5.7	78	5.4	73	5.0	68	4.7	64	4.4	59	4.1	54	3.7	49	3.4
5/32	167	12	159	11	151	10.4	142	9.8	134	9.3	126	8.7	118	8.1	110	7.6	101	7.0	93	6.4	85	5.8
1/8	250	17	250	17	250	17	244	17	230	16	216	15	202	14	187	13	173	12	159	11	145	10.
7/64	250	17	250	17	250	17	250	17	250	17	250	17	250	17	240	17	222	15	204	14	186	13
#38	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	231	16
5/64	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17

3-AV Maximum Operati	ng Pre	ssures																
Specific Gravity*	1.00 0.95		0.90		0.85		0.80		0.75		0.	70	0.65		0.60			
Float wt., oz (g)	14.9 (423) 14.2 (402)				13.4 (381)		12.7	360)	12.0	(339)	11.2	(318)	10.5	(296)	9.7 (275)		9.0 (254)
Orifico Sizo (in)								Maximu	ıт Оре	rating P	ressure							
Orifice Size (in)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1/2	21	1.5	20	1.4	19	1.3	18	1.3	17	1.2	16	1.1	15	1.0	14	1.0	13	0.9
3/8	45	3.1	43	3.0	41	2.8	38	2.7	36	2.5	34	2.3	32	2.2	30	2.0	27	1.9
5/16	72	5.0	69	4.7	65	4.5	61	4.2	58	4.0	54	3.8	51	3.5	47	3.3	44	3.0
9/32	96	6.6	91	6.3	87	6.0	82	5.6	77	5.3	72	5.0	68	4.7	63	4.3	58	4.0
1/4	144	9.9	137	9.4	130	8.9	123	8.5	116	8.0	109	7.5	102	7.0	94	6.5	87	6.0
7/32	206	14	196	13	186	13	176	12	165	11	155	10.7	145	10.0	135	9.3	125	8.6
3/16	250	17	250	17	250	17	250	17	249	17	234	16	218	15	203	14	188	13
5/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17

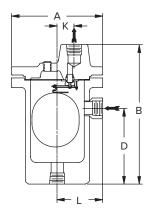
6-AV Maximu	m Op	erati	ng P	ressı	ıres																					
Specific Gravity*	1.0	00	0.	95	0.9	90	0.	85	0.	80	0.	75	0.	70	0.6	65	0.	60	0.	55	0.!	50	0.	.45	0.	40
Float wt., oz (g)		3.5 084)		9.8 979)	66 (1.8	5.2 75)		2.5 771)		3.8 67)	55 (1 5	5. 1 63)	_	1.5 159)		7.8 (54)	1	4.1 250)).4 46)		6.8 (42)	33.1	(938)	29.4	(833)
Orifice Size (in)											Ma	ximur	n Ope	erating	Press	sure										
Offlice Size (III)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1-1/16	22	1.5	21	1.5	20	1.4	19	1.3	18	1.2	17	1.2	16	1.1	14	1.0	13	0.9	12	0.8	11	0.8	10	0.70	9	0.62
7/8	35	2.4	33	2.3	31	2.2	30	2.0	28	1.9	26	1.8	24	1.7	23	1.6	21	1.5	19	1.3	18	1.2	16	1.1	14	1
3/4	50	3.5	48	3.3	45	3.1	43	3.0	40	2.8	38	2.6	35	2.4	33	2.3	30	2.1	28	1.9	25	1.8	23	1.6	20	1.4
5/8	77	5.3	73	5.0	69	4.8	66	4.5	62	4.3	58	4.0	54	3.7	50	3.5	46	3.2	43	2.9	39	2.7	35	2.4	31	2.2
9/16	102	7.0	97	6.7	92	6.3	87	6.0	82	5.6	77	5.3	72	4.9	67	4.6	62	4.2	57	3.9	51	3.6	46	3.2	41	3.9
1/2	148	10.2	140	9.7	133	9.2	126	8.7	119	8.2	111	7.7	104	7.2	97	6.7	89	6.2	82	5.6	75	5.1	67	4.6	60	4.1
7/16	210	14	200	14	189	13	179	12	168	12	158	11	148	10.2	137	9.5	127	8.7	116	8.0	106	7.3	96	6.6	85	5.9
3/8	250	17	250	17	250	17	250	17	250	17	249	17	233	16	216	15	200	14	184	13	167	12	151	10.4	134	9.3
11/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	245	17	223	15	201	14	179	12
5/16	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	230	16
9/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
1/4	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17

 $^{^*}$ If specific gravity falls between those shown, use next lowest: e.g., if actual gravity is 0.73, use 0.70 specific gravity data.

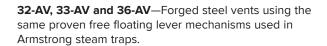


Free Floating Lever Air/Gas Vents—Forged Steel

For Pressures to 1 000 psig (69 barg) or Specific Gravity Down to 0.40



Model 32-AV, 33-AV and 36-AV





For applications where high air/gas venting capacity is required up to 1 000 psig. Available with screwed, socketweld or flanged connections.

For a fully detailed certified drawing, refer to CD #1035.

List of Material	s					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket	Bolting
32-AV				ACTN A405		D II ACTA A400 C D7
33-AV		Stainless Steel		ASTM A105 Forged Steel	Non-asbestos	Bolts ASTM A193 Gr. B7 Nuts ASTM A194 Gr. 2H
36-AV				1 orged Steel		INULS ASTIVI A194 GI. 2H

Physical Data						
Model No.			Forged	l Steel		
Model No.	32-	AV [†]	33-	AV [†]	36-	AV [†]
Pipe Connections	1/2, 3/4, 1	15, 20, 25	3/4, 1	20, 25	1-1/2, 2	40, 50
"A"	6-3/4	171	8	203	11-7/8	301
"B"	10-3/16	259	11-9/16	294	17-1/8	435
"D"	5-9/16	141	6-1/16	154	9	229
"K"	1-1/4	32	1-7/16	37	2-1/8	54
"L"	3-3/8	86	3-7/8	98	6-1/16	154
Approx. Wt. lb (kg)	31 (14)		49 (22)		163 (74)	
Max. Allow. Pressure	600 psig @ 100°F	(41 barg @ 38°C)		1 000 psig @ 100°	F (69 barg @ 38°C)	
(Vessel Design)	500 psig @ 750°F	(34 barg @ 399°C)		600 psig @ 750°F	(41 barg @ 399°C)	

†Available in Type 316 SS. Consult factory. Pipe size of side connections if provided is same as that of inlet and outlet connections. Some floats are oil filled. Consult factory for details.

Free Floating Lever Air/Gas Vents—Forged Steel

For Pressures to 1 000 psig (69 barg) or Specific Gravity Down to 0.40



High-Temperature Service

Maximum allowable working pressures of floats decrease at temperatures above 100°F. Allow for approximately:

- 10% decrease at 200°F
- 15% decrease at 300°F
- 20% decrease at 400°F

The float is not always the limiting factor, however. Consult with Armstrong Application Engineering if you have a high-temperature application that also requires maximum operating pressures.

Sour Gas Service

Forged steel and stainless steel traps can be modified to resist hydrogen sulfide stress corrosion. These modifications involve annealing the float, which will reduce the maximum working pressure of the float to about half of its normal value. Consult Armstrong Application Engineering for allowable working pressures.

Maximum Operating Pressures of free floating lever vents with weighted floats for different orifice sizes, and the specific gravities on which they can be used.

32-AV Maximum O	peratin	g Pressi	ures													
Specific Gravity*	1.0	00	0.9	95	0.	90	0.	85	0.	80	0.	75	0.	70	0.	65
Float wt., oz (g)	11.8 ((335)	11.2	(318)	10.6	(301)	10.0	(285)	9.4 (268)	8.9	(251)	8.3 (234)	7.7 (218)
Orifico Sizo (in)							Maxim	um Ope	rating P	ressure						
Orifice Size (in)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
5/16	41	2.8	39	2.7	37	2.6	35	2.4	33	2.3	31	2.1	29	2.0	27	1.9
1/4	68	4.7	64	4.4	61	4.2	58	4.0	54	3.7	51	3.5	47	3.3	44	3.0
3/16	149	10.3	142	9.8	134	9.3	127	8.8	120	8.2	112	7.7	105	7.2	97	6.7
5/32	257	18	244	17	231	16	219	15	206	14	193	13	180	12	168	12
1/8	439	30	417	29	396	27	374	26	352	24	330	23	309	21	287	20
7/64	562	39	534	37	506	35	478	33	450	31	423	29	395	27	367	25
#38	600	41	600	41	600	41	595	41	561	39	526	36	491	34	457	31
5/64	600	41	600	41	600	41	600	41	600	41	600	41	600	41	600	41

33-AV Maximum Opera	ting Pr	essure	s															
Specific Gravity*	1.0	00	0.9	95	0.9	90	0.	85	0.	80	0.	75	0.	70	0.0	65	0.0	60
Float wt., oz (g)	14.9	(423)	14.2	(402)	13.4	(381)	12.7	(360)	12.0	(339)	11.2	(318)	10.5	(296)	9.7 (275)	9.0 (254)
Orifice Size (in)							M	laximuı	n Ope	rating I	Pressu	re						
Offlice Size (III)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1/2	21	1.5	20	1.4	19	1.3	18	1.3	17	1.2	16	1.1	15	1.0	14	1.0	13	0.9
3/8	45	3.1	43	3.0	41	2.8	38	2.7	36	2.5	34	2.3	32	2.2	30	2.0	27	1.9
5/16	72	5.0	69	4.7	65	4.5	61	4.2	58	4.0	54	3.8	51	3.5	47	3.3	44	3.0
9/32	96	6.6	91	6.3	87	6.0	82	5.6	77	5.3	72	5.0	68	4.7	63	4.3	58	4.0
1/4	144	9.9	137	9.4	130	8.9	123	8.5	116	8.0	109	7.5	102	7.0	94	6.5	87	6.0
7/32	206	14	196	13	186	13	176	12	165	11	155	10.7	145	10.0	135	9.3	125	8.6
3/16	309	21	294	20	279	19	264	18	249	17	234	16	218	15	203	14	188	13
5/32	484	33	460	32	437	30	413	28	389	27	365	25	342	24	318	22	294	20
1/8	900	62	900	62	883	61	835	58	787	54	739	51	691	48	643	44	595	41
7/64	900	62	900	62	900	62	900	62	900	62	900	62	883	61	822	57	760	52

36-AV N	/laxim	um C	Operat	ting I	Pressu	ıres																				
Specific Gravity*	1.0	00	0.9	15	0.9	0	0.8	5	0.8	30	0.7	75	0.7	70	0.6	65	0.6	60	0.5	55	0.	50	0.	45	0.4	40
Float wt., oz (g)	73 (2 0		69. (1 97	-	66. (1 87		62. (1 7		58 (1 6		55 (1 5)	5.1 63)	51 (1 4		47.8 35	- 1	44 (1 2!	l.1 50)	40 (1 1			5.8 (42)		3.1 38)		9.4 33)
Orifice											Max	imum	Opera	iting P	ressur	е										
Size (in)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1-1/16	22	1.5	21	1.5	20	1.4	19	1.3	18	1.2	17	1.2	16	1.1	14	1.0	13	0.9	12	0.8	11	0.8	10	0.70	9	0.62
7/8	35	2.4	33	2.3	31	2.2	30	2.0	28	1.9	26	1.8	24	1.7	23	1.6	21	1.5	19	1.3	18	1.2	16	1.1	14	1
3/4	50	3.5	48	3.3	45	3.1	43	3.0	40	2.8	38	2.6	35	2.4	33	2.3	30	2.1	28	1.9	25	1.8	23	1.6	20	1.4
5/8	77	5.3	73	5.0	69	4.8	66	4.5	62	4.3	58	4.0	54	3.7	50	3.5	46	3.2	43	2.9	39	2.7	35	2.4	31	2.2
9/16	102	7.0	97	6.7	92	6.3	87	6.0	82	5.6	77	5.3	72	4.9	67	4.6	62	4.2	57	3.9	51	3.6	46	3.2	41	3.9
1/2	148	10.2	140	9.7	133	9.2	126	8.7	119	8.2	111	7.7	104	7.2	97	6.7	89	6.2	82	5.6	75	5.1	67	4.6	60	4.1
7/16	210	14	200	14	189	13	179	12	168	12	158	11	148	10.2	137	9.5	127	8.7	116	8.0	106	7.3	96	6.6	85	5.9
3/8	331	23	315	22	299	21	282	19	266	18	249	17	233	16	216	15	200	14	184	13	167	12	151	10.4	134	9.3
11/32	441	30	419	29	398	27	376	26	354	24	332	23	310	21	288	20	266	18	245	17	223	15	201	14	179	12
5/16	567	39	539	37	511	35	483	33	455	31	427	29	399	27	371	26	342	24	250	17	250	17	250	17	230	16
9/32	743	51	706	49	669	46	633	44	596	41	559	39	522	36	485	33	449	31	250	17	250	17	250	17	250	17
1/4	1 000	69	1000	69	979	67	925	64	871	60	817	56	763	53	710	49	656	45	250	17	250	17	250	17	250	17
7/32	1 000	69	1000	69	1000	69	1 000	69	1000	69	1000	69	1000	69	1000	69	926	64	250	17	250	17	250	17	250	17
3/16	1 000	69	1000	69	1000	69	1 000	69	1000	69	1000	69	1 000	69	1000	69	1 000	69	250	17	250	17	250	17	250	17

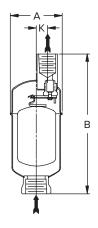
^{*}If specific gravity falls between those shown, use next lowest: e.g., if actual gravity is 0.73, use 0.70 specific gravity data.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

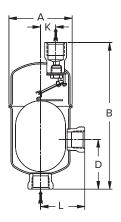


Free Floating Lever Air/Gas Vents—All Stainless Steel

For Pressures to 600 psig (41 barg) or Specific Gravity Down to 0.50



Model 11-AV



Model 22-AV and 13-AV



The Armstrong stainless steel free floating lever air vents have been developed to provide positive venting of air/gases under pressure.

The body and cap and all working parts of the No. 11-AV, 22-AV and 13-AV are made of high strength, corrosion resistant stainless steel. Body and caps are welded together to form a permanently sealed, tamperproof unit with no gaskets. Elliptical floats and high leverage provide up to 115 SCFM capacity for these compact air/gas vents. Lever action is guided to assure proper seating of the valve under all operating conditions.

11-AV, 22-AV and 13-AV—All stainless steel construction where exposure to either internal or external corrosion is a problem. These air/gas vents have the same proven free floating mechanisms used in other Armstrong steam traps. Pressures to 600 psig @ 100°F (41 barg @ 38°C).

For a fully detailed certified drawing, refer to list below: 11-AV CD #1066 13-AV and 22-AV CD #1086

Physical Data						
Model No.	11-A	V	22-	AV	13-4	AV
Pipe Connections	1/2, 3/4**	15, 20**	3/4	20	1	25
"A"	2-3/4	70	3-7/8	99	4-1/2	114
"B"	7-1/4	184	8-13/16	224	11-3/8	289
"D"	_	_	3-3/8	86	6-1/8	156
"K"	9/16	14	7/8	22	1-3/16	30
"L"	_	_	2-5/8	67	3-1/4	83
Weight, lb (kg)			5 (2	2.3)	7-1/2	(3.4)
Max. Allow. Pressure	500 psig @ 100°F (34 barg @ 38°C)	600 psig @ 100°F	(41 barg @ 38°C)	570 psig @ 100°F	(39 barg @ 38°C)
(Vessel Design)	440 psig @ 500°F (3	30 barg @ 260°C)	475 psig @ 500°F ((33 barg @ 260°C)	490 psig @ 500°F (34 barg @ 260°C)

^{** 1/2&}quot; (15 mm) outlet.

List of Ma	iterials			
Model No.	Valve & Seat*	Leverage System*	Float*	Body & Cap*
11-AV	Hardened	303/304	304	
22-AV	chrome	Stainless	Stainless	Sealed Stainless
13-AV	steel—17- 4PH	Steel	Steel	Steel 304-L

^{*}Type 316 SS valve and seat available. Consult factory.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

^{*11-}LD available in all-316SS. Consult factory.

Free Floating Lever Air/Gas Vents—All Stainless Steel



For Pressures to 600 psig (41 barg) or Specific Gravity Down to 0.50

11-AV Maximum Operating	Pressures			
Minimum Specific Gravity	0.75	5	0.	50
Float wt., oz (g)	2.90 (82) S	standard	2.08 (59) Special
Orifico Sizo (in)	Maxim	um Opera	ating Pres	sure
Orifice Size (in)	psig	barg	psig	barg
1/8	178	12	118	8
#38	267	18	177	12
5/64	400	28	311	21

Specific Gravity*	1.0	00	0.5	95	0.9	90	0.	85	0.	80	0.	75	0.	70	0.	65	0.	60	0.	55	0.	50
Float wt., oz (g)	10.0	(282)	9.5 (268)	9.0 (254)	8.5	(240)	8.0 (226)	7.5 (212)	5.4 ((152)	5.0	(141)	4.6	(130)	4.2	(119)	3.8	(109
Orifice Size (in)									М	aximur	n Ope	rating	Pressu	ıre								
Office Size (iii)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	ba
5/16	35	2.4	33	2.3	31	2.2	30	2.0	28	1.9	26	1.8	19	1.3	18	1.2	16	1.1	15	1.0	14	0
1/4	57	3.9	54	3.7	51	3.5	49	3.4	46	3.2	43	3.0	31	2.1	29	2.0	27	1.8	24	1.7	22	1
3/16	126	8.7	120	8.2	113	7.8	107	7.4	101	7.0	95	6.5	68	4.7	64	4.4	59	4.1	54	3.7	49	3
5/32	217	14.9	206	14.2	195	13.5	185	12.7	174	12.0	163	11.2	118	8.1	110	7.6	101	7.0	93	6.4	85	5
1/8	371	25.6	352	24.3	334	23.0	316	21.8	297	20.5	279	19.2	202	13.9	187	12.9	173	12.0	159	11.0	145	10
7/64	474	32.7	451	31.1	427	29.5	404	27.9	380	26.2	357	24.6	258	17.8	240	16.5	222	15.3	204	14.0	186	12
#38	590	40.7	561	38.7	532	36.7	503	34.7	473	32.7	444	30.6	321	22.1	298	20.6	276	19.0	253	17.5	231	1!
5/64	600	41.4	600	41.4	600	41.4	600	41.4	600	41.4	600	41.4	473	32.6	440	30.3	407	28.1	374	25.8	341	2

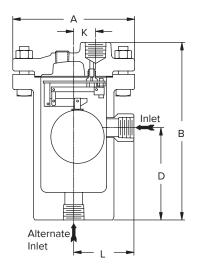
13-AV Maximum O	peratin	g Press	sures															
Specific Gravity*	1.0	00	0.	95	0.9	90	0.	85	0.	80	0.	75	0.	70	0.	65	0.	60
Float wt., oz (g)	14.9	(423)	14.2	(402)	13.4	(381)	12.7	(360)	12.0	(339)	11.2	(318)	10.5	(296)	9.7 (275)	9.0 ((254)
Orifice Size (in)								Maximu	ıт Оре	rating P	ressure							
Offlice Size (III)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1/2	21	1.5	20	1.4	19	1.3	18	1.3	17	1.2	16	1.1	15	1.0	14	1.0	13	0.9
3/8	45	3.1	43	3.0	41	2.8	38	2.7	36	2.5	34	2.3	32	2.2	30	2.0	27	1.9
5/16	72	5.0	69	4.7	65	4.5	61	4.2	58	4.0	54	3.8	51	3.5	47	3.3	44	3.0
9/32	96	6.6	91	6.3	87	6.0	82	5.6	77	5.3	72	5.0	68	4.7	63	4.3	58	4.0
1/4	144	9.9	137	9.4	130	8.9	123	8.5	116	8.0	109	7.5	102	7.0	94	6.5	87	6.0
7/32	206	14	196	13	186	13	176	12	165	11	155	10.7	145	10.0	135	9.3	125	8.6
3/16	309	21	294	20	279	19	264	18	249	17	234	16	218	15	203	14	188	13
5/32	484	33	460	32	437	30	413	28	389	27	365	25	342	24	318	22	294	20
1/8	570	39	570	39	570	39	570	39	570	39	570	39	570	39	570	39	570	39
7/64	570	39	570	39	570	39	570	39	570	39	570	39	570	39	570	39	570	39

^{*}If specific gravity falls between those shown, use next lowest: e.g., if actual gravity is 0.73, use 0.70 specific gravity data.



High Leverage Ball Float Type Air Relief Traps

For Low Flows at Pressures to 2 700 (186 barg) or Specific Gravity Down to 0.49



The Armstrong High Leverage Series of Air Relief traps were developed especially for venting gases from low specific gravity fluids at high pressures. They use standard Armstrong forged steel bodies with very high leverage air relief mechanisms. Available with screwed, socketweld or flanged connections.

NOTE: Models 2313-HLAR, 2316-HLAR, 2413-HLAR and 2415-HLAR are also available with cast T-316 stainless steel body and all-stainless steel internals. Consult factory.

Sour Gas Service

Forged steel and stainless steel traps can be modified to resist hydrogen sulfide stress corrosion. These modifications involve annealing the float, which will reduce the maximum working pressure of the float to about half its normal value. Consult Armstrong Application Engineering for allowable working pressures.

Physical D	ata—Hi	igh Le	verage	Ball Fl	oat Ty	pe Ai	r Relief	Traps										
Model No.	2313-H	HLAR†	2315-H	HLAR	2316-H	HLAR	2413-	HLAR†	2415-l	HLAR	2416-H	LAR	25133G	-HLAR	25155G	-HLAR	26155G	-HLAR
Dina	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4	20, 25, 32	1, 1-1/4	25, 32
"A"	8	203	9-3/4	248	11-7/8	302	8-5/8	219	10-3/4	273	12-1/2	318	8-1/2	216	10-3/8	263	11-3/4	298
"B"	11-9/16	294	15-1/16	383	17-1/8	435	11-7/8	302	15	381	17-3/4	451	14-1/4	362	16-7/32	412	24-1/8	613
"D"	6-1/16	154	7-13/16	198	9	229	5-3/8	137	7-1/4	184	9	229	3	75	4	102	5	127
"G"	5-1/8	130	6-7/8	175	8-3/8	213	5-3/8	137	6-7/8	175	8-5/8	219	5-3/4	146	7-3/8	187	8-3/8	213
"K"	1-7/16	37	1-3/4	44	2-1/8	54	1-7/16	37	1-3/4	44	2-1/8	54	1-5/16	33	1-3/4	44	1-3/4	44
"L"	3-7/8	98	4-11/16	119	5-3/4	146	4	102	4-13/16	122	5-13/16	148	-	-	-	-	-	-
Weight, lbs (kg)	46	(21)	98 (44)	160 ((73)	69	(31)	130 ([59)	210 (9	95)	113 (51)	171 (78)	325 ((147)
Maximum Allowable Pressure (Vessel Design)		46 (21) 98 (44) 160 (73 1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)					(103 barg 900 psig	g @ 100°F g @ 38°C) g @ 850°F @ 454°C)	(1 9)	300 psig 25 barg 00 psig @ 2 barg @	900°F		(146 barg ([®] 38°C) 1 [®] 900°F	2 520 psig (174 barg @ 000 psig (138 barg @	9 38°C) 2 @ 900°F		@ 38°C) g @ 900°F

†Available with cast 316 stainless steel body and all stainless steel internals. Consult factory.

List of Materia	als					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket	
2313-HLAR				ASTM		
2315-HLAR				A105 Forged		
2316-HLAR				Steel	Compressed	
2413-HLAR					Asbestos-free	
2415-HLAR	Sta	inless Steel		ASTM		
2416-HLAR				A182		
25133G-HLAR					Spiral Wound	
25155G-HLAR				Forged Steel	Stainless Steel	
26155G-HLAR					non-asbestos	

2315-HLAR Maximum Operating Pressures							
Specific Gravity	1.00 -	- 0.61	0.60	- 0.51			
Float Weight, oz (g)	9.0 (255)	7.1 (2	201)			
Orifice	Maximum Operating Pressure						
Offlice	psig	barg	psig	barg			
3/16	825	56					
5/32			600	41			
1/8	1000	69	600	41			
3/32							

2313-HLAR Maximum Operating Pressures							
Specific Gravity	1.00	- 0.69	0.68	- 0.54			
Float Weight, oz (g)	6.75	(191)	4.75	(135)			
Orifice size (in)	1	Maximum Ope	rating Pressu	re			
Orifice size (in)	psig	barg	psig	barg			
1/8			475	33			
7/64							
3/32	1000	69					
5/64							
1/16							

2316-HLAR Maximum Operating Pressures							
Specific Gravity	1.00 -	- 0.70	0.69 -	- 0.55			
Float Weight, oz (g)	22 (624)	15.5	(439)			
Orifice	N	Maximum Ope	rating Pressur	е			
Offfice	psig	barg	psig	barg			
7/32			475	33			
3/16							
5/32	1 000	69					
1/8							
3/32							

High Leverage Ball Float Type Air Relief Traps



For Low Flows at Pressures to 2 700 (186 barg) or Specific Gravity Down to 0.49

2413-HLAR Maximum Operating Pressures							
Specific Gravity	1.00 -	0.90	0.89 -	- 0.69	0.68 - 0.54		
Float Weight, oz (g)	9.375	(266)	6.75 (191)		4.75	(135)	
Orifice size (in)		Maximum Operating Pressure					
Offlice Size (III)	psig	barg	psig	barg	psig	barg	
1/8							
7/64							
3/32	1500	103	1000	69	475	33	
5/64							
1/16							

Specific Gravity	1.00 - 0.70		0.69 - 0.55		
Float Weight, oz (g)	22 (624)	15.5	(439)	
Orifice	Ma	ximum Ope	rating Press	ure	
Office	psig	barg	psig	barg	
7/32					
3/16					
5/32	1400	96	475	33	
1/8					
3/32					

2415-HLAR Maximum Operating Pressures							
Specific Gravity	1.00 -	- 0.85	0.84	- 0.61	0.60 - 0.51		
Float weight, oz (g)	13.75 (390) 9.0 (255) 7.1 (200)		9.0 (255)		7.1 (2	(01)	
Orifice	Maximum Operating				essure		
Office	psig	barg	psig	barg	psig	barg	
3/16	1200	83	825	56			
5/32	1725	119	1150	80	600	41	
1/8	1800	124	1200	83	600	41	
3/32	1 600	124	1 200	03			
2/16-HI AP Maximum Operating Prossures							

2416-HLAR Maximum	Operating Pressures

25133G HLAR Maximum Operating Pressures								
Specific gravity	1.00 -	- 0.98	0.97 -	0.97 – 0.90		- 0.69	0.68 - 0.54	
Float weight, oz (g)	10.5 (298)		9.375 (266)		6.75 (191)		4.75 (135)	
Orifice	Maximum Operating Pressure							
Offlice	psig	barg	psig	barg	psig	barg	psig	barg
7/64								
3/32	2.425	446	440		1 000	69	475	33
5/64	2 125	146	1 500	103				
1/16								

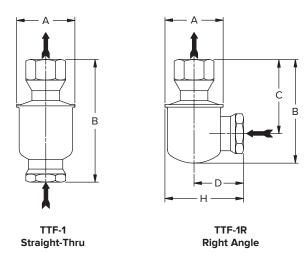
25155G HLAR Maximum Operating Pressures								
Specific gravity	1.00 -	- 0.95	0.94 -	0.94 - 0.86		0.85 - 0.63		- 0.52
Float weight, oz (g)	15.4 (437)		13.75	13.75 (390) 9.25 (262)		7.1 (201)	
Orifica		Maximum Operating Pressure						
Orifice	psig	barg	psig	barg	psig	barg	psig	barg
3/16	1350	93	1200	83	825	58		
5/32	1925	132	1725	119	1200	82		44
1/8	2.500	170	2,000	120	1 200	02	600	41
3/32	3/32 2 500	172 2 000	2 000	138	1 200	83		

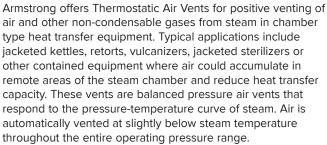
26155G HLAR Maximum Operating Pressures								
Specific gravity	1.00 -	- 0.95	0.94 – 0.86		0.85 - 0.63		0.85 – 0.63	
Float weight, oz (g)	15.4 (437)		13.75 (390)		9.25 (262)		7.1 (201)
Orifice		Maximum Operating Pressure						
Offlice	psig	barg	psig	barg	psig	barg	psig	barg
3/16	1350	93	1200	83	825	58		
5/32	1925	132	1725	119	1 200	82	600	41
1/8	1/8 3/32 2 700 186	2.700 400 2.000	120	1200	83	600	41	
3/32		100	2 000	138	1200	0.5		



Armstrong Stainless Steel Thermostatic Air Vents

For Pressures to 300 psig (20 barg)...Capacities to 104 scfm







Features

- Suitable for pressures from 0 300 psig
- All 304-L stainless steel bodies—sealed, tamper-proof
- Balanced pressure thermostatic element vents air at slightly below steam temperature over the entire pressure range—no adjustments required
- Dependable, proven phosphor-bronze bellows caged in stainless steel with bronze valve and stainless steel seat
- Available in straight-thru or right-angle connections

Armstrong thermostatic air vents should be installed at the highest point on a steam chamber, with the air vent located above the chamber. This will minimize the possibility of any liquid carryover, and air can be vented at atmosphere without a drain line.

For a fully detailed certified drawing, refer to CD #1018.

List of Materials	
Name of Part	Material
Body	304-L Stainless steel
Connections	304 Stainless steel
Balanced Pressure Thermostatic Air Vent	Stainless steel and bronze with phosphor-bronze bellows, entire unit caged in stainless steel
Gasket	Copper clad non-asbestos

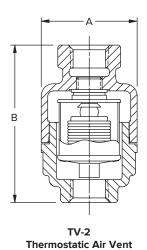
Optional: All stainless steel thermostatic air vent.

Physical Data								
Model No.	St	raight-Thru C	onnections TT	F-1	Ri	ight-Angle Con	nections TTF-1	R
Dina Connections	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2	15	3/4	20	1/2	15	3/4	20
"A" Diameter	2-1/4	57	2-1/4	57	2-1/4	57	2-1/4	57
"B" Height	4-1/2	114	4-11/16	119	3-3/4	95	3-15/16	100
"C" & inlet to face of outlet	_		_		2-5/8	67	2-13/16	71
"D" © outlet to face of inlet	_		_		1-15/16	49	1-7/8	48
"H"	_			_	3-1/16	78	3	76
Weight, lb (kg)	3/4 (0.4)	1 (0.5)	3/4	(0.4)	1 (0	.5)
Maximum Allowable Pressure (Vessel Design)		300 psig @ 450°F (20 barg @ 232°C)						
Maximum Operating Pressure, psig (barg)		300 (20)						
Discharge Orifice Size				3/	16"			

TV-2 Thermostatic Air Vent

For Pressures to 125 psig (9 barg)...Capacities to 46 scfm





Armstrong offers the Model TV-2 Balanced Pressure Thermostatic Air Vent for positive venting of air from chamber type heat transfer equipment with no loss of steam. Typical applications include jacketed kettles, retorts, vulcanizers, jacketed sterilizers or other contained equipment where air could accumulate at the top of the steam chamber and reduce heat transfer capacity.

The Model TV-2 is a balanced-pressure thermostatic air vent that responds to the pressure-temperature curve of steam at any pressure from light vacuum to maximum operating pressure. Air is automatically vented at slightly below steam temperature throughout the entire operating pressure range.

The thermostatic element is a charged multi-convolution phosphor bronze bellows caged in stainless steel. Valve and seat are also stainless steel designed to meet the most rigid cycling specifications known for this type of service.



Features

- Stainless steel hemispherical valve and seat
- Thermostatic element comprises a multi-convolution phosphor bronze bellows caged in stainless steel
- Thermostatic element is charged with water to provide positive opening of the valve at slightly below steam temperature and positive closing in the presence of steam throughout the operating pressure range
- · ASTM B62 cast bronze body

Armstrong Model TV-2 Thermostatic Air Vents should be installed at the highest points of steam chambers with inlet connections to the vents higher than the highest points of the chambers. Thus installed there is a minimum hazard of any liquid carryover and air can be vented to atmosphere with no drain line necessary.

For a fully detailed certified drawing, refer to CD #1032.

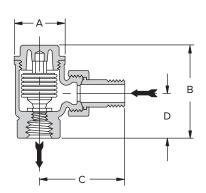
TV-2 Physical Data			
Dina Cannastiana	in	mm	
Pipe Connections	1/2	15	
"A" (Diameter)	2-3/16	56	
"B" (Height)	3-1/2	89	
Weight, lb (kg)	1-1/2 (0.8)		
Maximum Operating Pressure	125 psig	(9 barg)	
Temperature Maximum, °F (°C)	350°F (177°C)		

TV-2 Materials	
Name of Part	Material
Body & Cap	Cast bronze ASTM B62
Gasket	Compressed non-asbestos
Thermostatic Unit	
Bellows	Phosphor bronze
Cage and Cover	Stainless steel
Thermostatic Unit Gasket	Copper clad

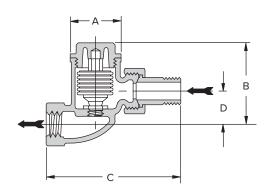


TS-2 Thermostatic Air Vent

For Pressures to 50 psig (3.4 barg)...Capacities to 25.9 scfm



TS-2 Air Vent Angle Type



TS-2 Air Vent Straight Type



Armstrong TS thermostatic air vent is offered in both angle and straight patterns. The TS-2 has a balanced pressure thermostatic element with a high quality multiple-convolution bellows. It's ideal for venting air from equipment such as steam radiators and convectors, small heat exchangers, and unit heaters. The TS-2 comes with a strong, cast bronze body and a stainless steel seat. The valve and seat are renewable in-line.

Materials

Cap: Bronze, ASTM B62
Body: Bronze, ASTM B62
Union Nipple: Brass, ASTM B584

Valve: Brass

Valve Seat: Stainless steel

Element: Phosphor-bronze bellows

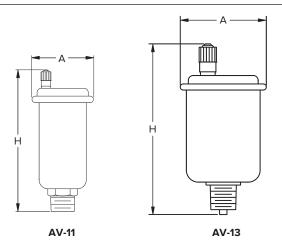
For a fully detailed certified drawing, refer to CDY #1045.

Physical Data										
Model		TS-2								
Pattern		Aı	ngle			Stra	aight			
Dina Connections	in	mm	in	mm	in	mm	in	mm		
Pipe Connections	1/2	15	3/4	20	1/2	15	3/4	20		
"A" Diameter	1-5/8	41	1-5/8	41	1-5/8	41	1-5/8	41		
"B" Height	2-15/16	75	3	76	2-11/16	68	2-7/8	73		
"C"	2-9/16	65	2-7/8	73	4	102	4-1/2	114		
"D"	1-3/8	35	1-5/8	41	1-1/8	28	1-5/16	33		
Weight, lb (kg)	1-1/2 (0.68)	1-3/4	(0.79)	1-1/2	(0.68)	2 (0	0.91)		

AV-11/AV-13 Air Vents

For Pressures to 150 psig (10 barg)







For Hot or Cold Water and Non-Viscous Liquids

Air vent models AV-11 and AV-13 are compact float-type valves for the removal of air and other gases from hydronic heating and cooling systems, liquid chilling operations and other light liquid services.

Physical Data						
Model	AV-	AV-11 AV-13				
Connection	in	mm	in	mm	in	mm
Size	1/8	3	1/2 Female	15 Female	3/4 Male	20 Male
"A"	1-3/4	44	2-1/8	54	2-1/8	54
"H"	3-3/8	86	4-5/8	118	4-5/8	118
Weight, lb (kg)	1/4 (0	D.11)	1/2 (0.23)			

Capaci	ties						
AV-11					AV	'-13	
	ΔP	Capa	cities	Δ	·P	Capa	cities
psig	barg	cfm	m³/hr	psig	barg	cfm	m³/hr
3.5	0.24	0.5	0.84	16	1.1	1	1.7
10	0.69	1.0	1.7	48	3.3	2	3.4
24	1.7	1.5	2.5	84	5.8	3	5.1
35	2.4	1.9	3.2	120	8.3	4	6.8
50	3.4	2.0	3.4	150	10	4.9	8.3

Specifications									
Model	Application	Workin	ng Pressure	Maximum Te	mperature	Connection	Hydraulic Test Body		
Model	Application	psig	barg °F °C		°C	Connection	psig	barg	
AV-11	Hot or Cold	1 - 50	0.06 - 3.4	210	00	NDT Coroused	200	14	
AV-13	Water	1 - 150	0.06 - 10.3	210	99	NPT Screwed	350	24	

Materials		
Valve	Float	Disc
Brass	Polypropylene	Nitrile

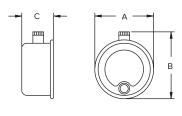


Materials

Valve Seat

Body Float

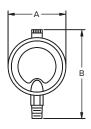
Armstrong SV-12 Steam Radiator Air Vent





Name of Part

Bimetal Thermostatic Element



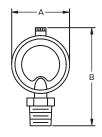
SV-12 Straight Air Vent

Material

Nickel plated brass

Polypropylene

Brass Stainless steel



SV-12 Straight Main Air Vent

For Steam Service

A vent port size for every room location with the largest size for the coldest rooms and the smallest size for the "too hot" rooms. SV-12 air vents are easy to install on any steam radiator.

For a fully detailed certified drawing, refer to CDY #1042.

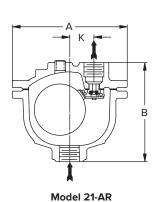


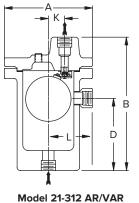
Physical Data								
Pattern	Angle Co	onnection	Straight C	Connection	Straight Mair	Straight Main Connection		
Dia - Canadatian Cia	in	mm	in	mm	in	mm		
Pipe Connection Size	1/8	3	1/8, 1/4	3, 6	1/2, 3/4	15, 20		
"A"	2-3/16	56	2-3/16	56	2-3/16	56		
"B"	2-5/16	59	3-1/4	83	3-1/2	89		
"C"	1-3/16	30	1-3/16	30	1-3/16	30		
Max. Operating Pressure, psig (barg)			15 (1)					
Vent Port Designation and Port Size	Each air ve	_	6 = .0935" C = .1285" .1850" all five of the abov	e vent ports	Only one	850" vent port provided		

Fixed Pivot Ball Float Air/Gas Vents

For Pressures to 600 psig (41 barg) or Specific Gravity Down to 0.83









Cast	Iron	Forged Steel		
21-4	AR .	21-312 AF	R/VAR	
in	mm	in	mm	
1/2, 3/4	15, 20	1/2, 3/4	15, 20	
6-3/16	157	6-3/4	171	
5-1/4	133	10-1/4	260	
-	-	5-9/16	141	
1-5/16	33	1-1/4	32	
-	-	3-5/16	84	
8 (4	4)	30 (14	4)	
250 psig @ 450°F** (17 barg @ 232°C**)		600 psig @ 100°F (41 barg @ 38°C) 500 psig @ 750°F** (34 barg @ 399° C**)		
	21-A in 1/2, 3/4 6-3/16 5-1/4 - 1-5/16 - 8 (4	1/2, 3/4 15, 20 6-3/16 157 5-1/4 133 1-5/16 33 8 (4) 250 psig @ 450°F**	21-AR 21-312 AF in mm in 1/2, 3/4 15, 20 1/2, 3/4 6-3/16 157 6-3/4 5-1/4 133 10-1/4 5-9/16 1-5/16 33 1-1/4 3-5/16 8 (4) 30 (1-4) 250 psig @ 450°F** (41 barg @ 232°C**) 500 psig @ 500 psig	

21-AR—A small, high-quality economical air vent. It employs a single lever with a fixed pivot and viton seat, ensuring a tight shut-off.

For a fully detailed certified drawing, refer to CD #1037.

21-312 AR/VAR —Forged steel version of the Model 21 with a larger float and higher leverage. Available with screwed, socketweld or flanged connections.

For a fully detailed certified drawing, refer to CD #1106.

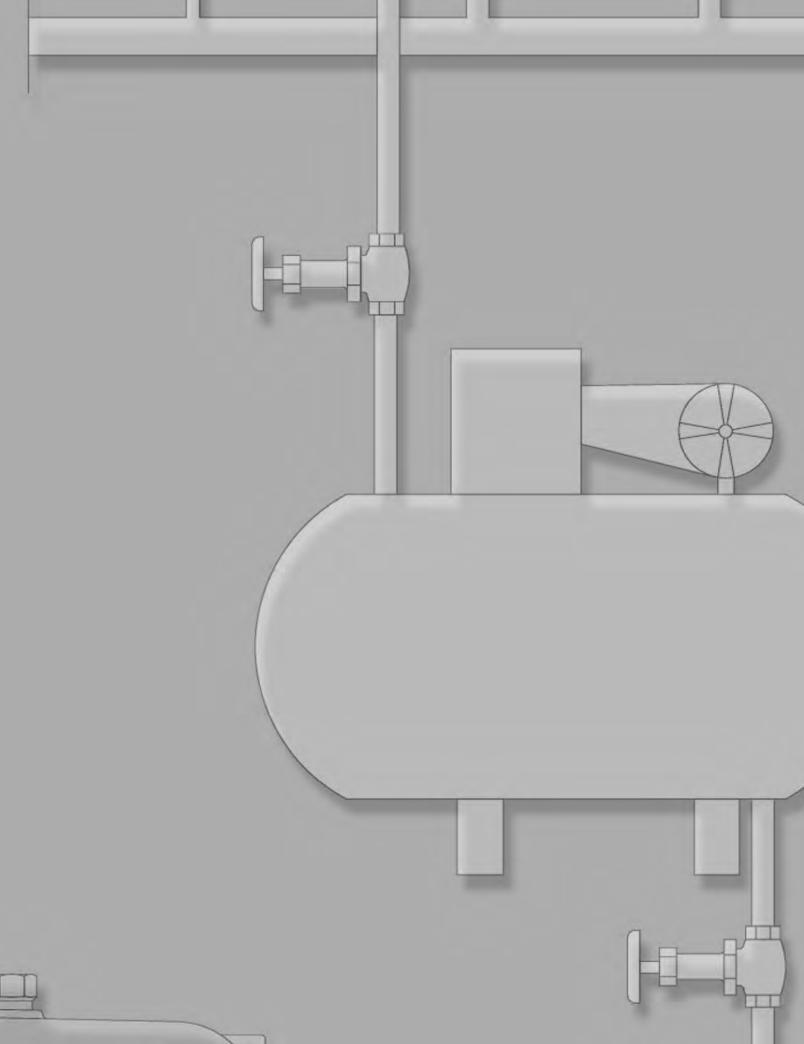
**Viton valve seat insert limited to 400°F (204°C	2).
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21-AR Maximum Operating Pressures								
Minimum Specific Gravity	0.4	.9	0.8	4				
Float Weight, oz (g)	2.25	(64)	4.12 (118)				
Orifice (in)	Maxim	num Ope	rating Pres	sure				
Office (iii)	psig	barg	psig	barg				
7/32	17	1.2	-	-				
3/16	23	1.6	-	-				
5/32	33	2.3	-	-				
9/64	41	2.8	-	-				
1/8	52	3.6	-	-				
3/32	92	6.4	-	-				
5/64	133	9.2	-	-				
1/16	208	14	-	-				
1/16	-	-	250	17				

21-312 AR/VAR Maximum Operating Pressures									
Model	Minimum Specific Gravity	0.83							
	Float Weight, oz (g)	5 (143)							
		Maximum Operating							
	Orifice (in)	Pressure							
		psig	barg						
21-312AR	1/4	22	1.5						
	7/32	28	1.9						
	3/16	38	2.7						
	5/32	55	3.8						
	9/64	68	4.7						
21-312VAR	1/8	173	12						
	3/32	308	21						
	5/64	443	31						
	1/16	600	41						

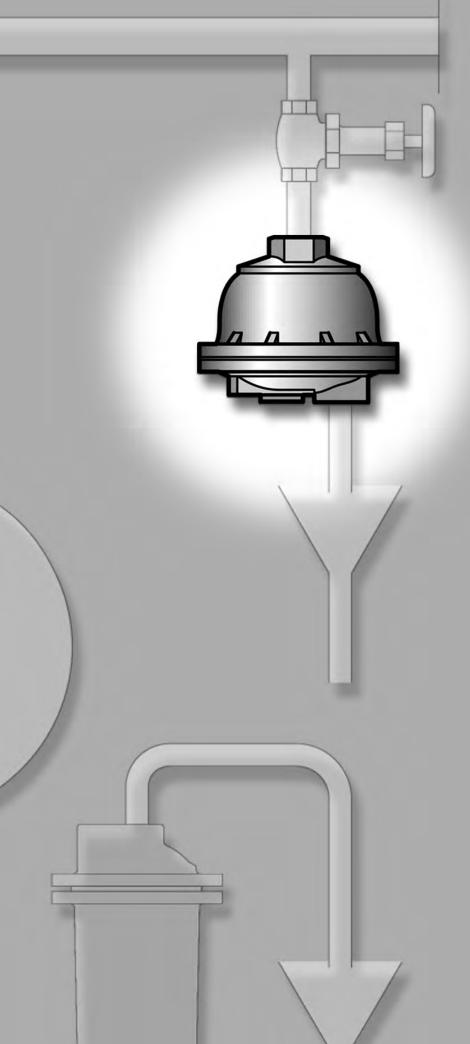
List of Materials										
Model No.	Valve	Seat	Leverage System	Float	Body & Cap	Gasket	Bolting			
21-AR	Stainless Steel	Steel with	Stainless	Stainless Steel	ASTM A48 Class 30 Cast Iron	Non- Asbestos	Bolts SAE Gr. 2 Nuts ASTM A563 Gr. A			
21-312 AR 21-312 VAR			Steel		ASTM A105 Forged Steel		Bolts and Nuts ASTM B633 Type 1			

NOTE: Above vents available in T-316 SS bodies and caps and all SS internals. Aluminum body and cap available for Model 21-AR only. *Other seat insert materials available. Consult factory.



Strong









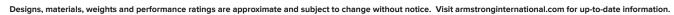


1-LD Cast Iron Free Floating Lever Drain Trap



11-LD Stainless Steel Free Floating Lever Drain Trap





Liquid Drainers ID Charts



Armstrong Liqui	d Drainers														
				Max.				Max.			Conn	ection S	ize		
Illustration	Туре	Flow Direction	Connection Type	Allow. Press. psig	TMA °F	Body Material	Model	Oper. Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	Located on Page
	Series 1-LDC See-Thru Free Floating Lever Drain Traps Capacities to 1 500 lb/hr	—	Screwed	150	150	Nylon Cap Polycarbonate Body	1-LDC	150	•	**					502
Ō	Series 1-LDCW See-Thru Free Floating Lever Drain Traps for Ozone Applications	—	Screwed	150	150	PBT Cap (Polybutylene Terephthalate) Polycarbonate Body	1-LDCW		A	**					505
	Series 200 BVSW Inverted Bucket Drain Traps Capacities to 7 000 lb/hr	1	Screwed	250	450	ASTM A48 Class 30 Cast Iron	211 212 213	250	•	•	•				506
	Series 800 BVSW Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	800 811 812 813	150 250 250 250	•	•	•				506
	Series 880 BVSW Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	880 881 882 883	150 250 250 250	•	•	•				
	Series 300 BVSW Inverted Bucket Drain Traps Capacities to 7 000 lb/hr	1	Screwed Socketweld Flanged [†]	600	650 650	ASTM A105 Forged Steel	312 313	600	•	•	•				506
	Series 900 BVSW Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed Socketweld Flanged [†]	600	650	ASTM A216 WCB Cast Steel	981 983	300 600	•	•	•				
	Series 1, 2, 3, 6 Free Floating Lever			300	200		1-LD	300	*						
	Drain Traps Capacities to 49 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	2-LD 3-LD 6-LD	250	•	•	•		•	•	509

^{★ 1/4&}quot; outlet connection

^{★★ 1/2&}quot; outlet connection

[†] Flange selection may limit pressure and temperature rating.

^{††} Side connection not available.



Armstrong Liquid Drainers ID Charts

Armstrong Liqu	id Drainers			Max.				Max.			Conn	ection S	ize		
Illustration	Туре	Flow Direction	Connection Type	Allow. Press. psig	°F	Body Material	Model	Oper. Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	Located on Page
	Series 11, 22, 13 Free Floating Lever		Screwed Socketweld	500 or 440	100 or 500		11-LD**	400	•	**					
	Drain Traps		Screwed Socketweld	600 or 475	100 or 500	304-L Stainless Steel	22-LD	533		•					510
	Capacities to 9 500 lb/hr	\	(22 and 13 Series Only)	570 or 490	100 or 500		13-LD	570			•				
	180-LD/181-LD Free Floating Lever Drain Traps		Screwed	500 or	100 or	304L Stainless	180-LD	229	•						512
	Capacities to 1 100 lb/hr	→	Socketweld	440	500	Steel	181-LD	350		•					
	Series 30 Free Floating Lever Drain Traps			600 or 500	100 or 750		32-LD	600	•	•	•				
			Screwed Socketweld Flanged [†]	1 000 or 600	100 or 750	ASTM A105 Forged Steel	33-LD	900	•	•	•				511
	Capacities to 42 000 lb/hr	+		1 000 or 600	100 or 750		36-LD	1000					•	•	
	Series 21 Fixed Pivot Drain Trap Capacities to 2 700 lb/hr	•	Screwed	250	450	ASTM A48 Class 30 Cast Iron	21	250	•	•					
	Series 21-312 Fixed Pivot Drain Traps Capacities to 3 900 lb/hr		Screwed Socketweld Flanged [†]	600 or 500	100 or 750	ASTM A105 Forged Steel	21-312 21-312V	74 600	•	•	•				
	Series 71-A Snap Action Drain Trap Capacities to 1 950 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	71-A	250		•	•				514
	Series 71-315 Snap Action Drain Trap Capacities to 1 950 lb/hr		Screwed Socketweld Flanged [†]	1000 or 600	100 or 750	ASTM A105 Forged Steel	71-315	1000		•	•	•			
	Series 2300 High Leverage Spring-Loaded Float Type Drain Trap Capacities to 14 500 lb/hr		Screwed Socketweld Flanged [†]	1000 or 600	100 or 750	ASTM A105 Forged Steel	2313-HLS 2315-HLS 2316-HLS	1000	•	•	•	•	•	•	516

[†] Flange selection may limit pressure and temperature rating.

Liquid Drainers ID Charts



Armstrong Liqu	ld Drainers											Connec	tion Size	9			
Illustration	Туре	Flow Direction	Connection Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	2-1/2"	3"	Located on Page
	Series 2400 High Leverage Spring-Loaded		Screwed	1500 or 900	100 or 850	ASTM A182	2413-HLS	1500	•	•	•						516
	Float Type Drain Traps Capacities to 16 250 lb/hr		Socketweld Flanged [†]	1800 or 900	100 or 900	Gr. F22 Forged Steel	2415-HLS 2416-HLS	1800			•	•	•	•			516
	Series 2500/2600 High Leverage Spring-Loaded			2 120 or 1 700	100 or 900		25133G HLS	2 120		•	•	•					
	Float Type Drain Traps		Screwed Socketweld Flanged [†]	2 520 or 2 000	100 or 900	ASTM A182 Gr. F22 Forged	25155G HLS	2 520			•	•	•				516
	Capacities to 11 000 lb/hr	+		3 700 or 3 000	100 or 900	Steel	26155G HLS	3 700				•	•				
	Series 2, 3, 6 Free Floating Lever Dual Gravity Drain					ASTM	2-DG	190	•	•							
	Traps Capacities to 40 000 lb/hr		Screwed	250	450	A48 Class 30 Cast Iron	3-DG 6-DG	250 250		•	•		•	•			
	Series 30 Free Floating Lever Dual	1 1		600 or 500	100 or 750		32-DG	325	•	•	•						518
	Gravity Drain Traps Capacities to		Screwed Socketweld Flanged [†]	1 000 or 600	100 or 750	ASTM A105 Forged Steel	33-DG	700		•	•						
	40 000 lb/hr	+		1000 or 600	100 or 750		36-DG	1000					•	•			
	Series JD&KD Ultra-Capacity Drain Traps Capacities to 302 000 lb/hr	*	Screwed	300	650	ASTM A395 Ductile Iron	JD8 KD8 KD10 KD12	300*						•	•	•	
	Series L&M Ultra-Capacity Drain Traps Capacities to 700 000 lb/hr	—	Screwed	250	450	ASTM A48 Class 30 Cast Iron	L8 L10 M12	250*						•	•	•	520
	Series LS&MS Ultra-Capacity Drain Traps Capacities to 700 000 lb/hr	—	Screwed Socketweld Flanged [†]	450	650	ASTM A216 WCB Cast Steel	LS8 LS10 MS12	450*						•	•	•	
	ADP-1 Pneumatically Operated Liquid Drainer Capacities to 1.5 lb liquid per cycle	-	Screwed	180	150	Aluminum ASTM B221 6061- T6511	ADP-1	180		•							524

^{*}For different specific gravities, see table LD-33 on page LD-49.

[†]Flange selection may limit pressure and temperature rating.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Bringing Energy Down to Earth

Say energy. Think environment. And vice versa.

Any company that is energy conscious is also environmentally conscious. Less energy consumed means less waste, fewer emissions and a healthier environment.

In short, bringing energy and environment together lowers the cost industry must pay for both. By helping companies manage energy, Armstrong products and services are also helping to protect the environment.

Armstrong has been sharing know-how since we invented the energy-efficient inverted bucket steam trap in 1911. In the years since, customers' savings have proven again and again that knowledge not shared is energy wasted.

Armstrong's developments and improvements in drain trap design and function have led to countless savings in energy, time and money. This section has grown out of our decades of sharing and expanding what we've learned. It deals with the operating principles of drain traps and outlines their specific applications to a wide variety of products and industries.

This section also includes Recommendation Charts that summarize our findings on which type of drain trap will give optimum performance in a given situation and why.

Terminology

Drain traps, as described in this section, have many other names in industry. A drain trap is an automatic loss prevention valve that opens to discharge liquids and closes to prevent air or gas loss. In industry, drain traps are also known as:

- Compressed air drains
- Condensate drainers
- Air traps
- Water traps

- Dump valves
- Float traps
- Liquid drainers
- Compressed air traps

This section should be utilized as a guide for the installation and operation of drain trapping equipment by experienced personnel. Selection or installation should always be accompanied by competent technical assistance or advice. We encourage you to contact Armstrong or its local representative for complete details.

Instructions for Using the Recommendation Charts



Quick reference Recommendation Charts appear throughout the "HOW TO DRAIN" pages of this section, pages LD-17 to LD-28

A feature code system (ranging from A to N) supplies you with "at-a-glance" information.

The chart covers the type of drain traps and the major advantages that Armstrong feels are superior for each particular application.

For example, assume you are looking for information concerning the proper trap to use on an aftercooler. You would:

1. Turn to the **"How to Drain Aftercoolers"** section, pages LD-21 and LD-22, and look in the lower left-hand corner of page LD-21. (Each application has a Recommendation Chart.) The Recommendation Chart LD-7 from page LD-21 is reprinted below as Chart LD-1 for your convenience.

2. Find "Aftercooler" in the first column under "Equipment
Being Drained" and read to the right for Armstrong's
"1st Choice and Feature Code". In this case, the first
choice is an IB and the feature code letters F, G, J, K, M are
listed.

- 3. Now refer to the chart below, titled "How Various Types of Drain Traps Meet Specific Operating Requirements" and read down the extreme left-hand column to each of the letters F, G, J, K, M. The letter "F," for example, refers to the trap's ability to handle oil/water mix.
- **4.** Follow the line for "F" to the right until you reach the column that corresponds to our first choice, in this case the inverted bucket. Based on tests, actual operating conditions, and the fact that the discharge is at the top, the inverted bucket trap handles oil/water mixtures extremely well. Follow this same procedure for the remaining letters.

Chart LD-1. Recommendation Chart (See below for "Feature Code" references.)								
Air Gas								
Equipment Being Drained	1st Choice and Feature Choice Code Alternate Choice Code Alternate Choice Code							
Aftercooler	IB	FF	*FF	FP				
Intercooler	F, G, J, K, M							

*Since IBs vent gas to operate, an FF is suggested because gas venting may not be desirable.

Chart LD	Chart LD-2. How Various Types of Drain Traps Meet Specific Operating Requirements										
Feature Code	Characteristic	IB	FF	FP	FS	D	TV	MV			
А	Method of Operation (Intermittent- Continuous)	I	С	С	I	I	I	С			
В	Energy Conservation in Operation	Good	Excellent	Excellent	Excellent	Fair	Poor	Excellent			
С	Energy Conservation Over Time	Good	Excellent	Excellent	Excellent	Poor	Fair	Poor (5)			
D	Resistance to Wear Fair	Excellent	Excellent	Fair	Good	Poor	Good	Excellent			
Е	Corrosion Resistance	Excellent	Excellent	Excellent	Excellent	Excellent	Excellent	Excellent			
F	Ability to Handle Oil/Water Mix	Excellent	Fair	Fair	Fair	Good	Excellent	Excellent			
G	Ability to Prevent Sludge Buildup	Excellent	Poor	Poor	Fair	Good	Good	Excellent			
Н	Resistance to Damage from Freezing (1)	Good (2)	Poor	Poor	Poor	Good	Fair	Good			
I	Performance to Very Light Loads	Good	Excellent	Excellent	Excellent	Poor	Poor	Poor			
J	Responsiveness to Slugs of Liquid (3)	Good	Excellent	Excellent	Excellent	Poor	Poor	Poor			
K	Ability to Handle Dirt	Excellent	Fair	Fair	Excellent	Poor	Excellent	Good			
L	Comparative Physical Size	Large	Large	Large	Large	Small	Small	Small			
М	Mechanical Failure (Open-Closed)	Open	Closed	Closed	Closed	Open	(4)	(4)			
N	Noise Level of Discharge (Loud-Quiet)	Quiet	Quiet	Quiet	Quiet	Loud	Loud	(4)			

IB = Inverted Bucket

FF = Float-Free Linkage

FP = Float-Fixed Pivot Linkage

FS = Float-Snap Acting Linkage

D = Disc

TV = Timed Solenoid Valve

MV = Manual Valve

- (1) Cast iron not recommended.
- (2) Sealed stainless steel = good.
- (3) Float traps should be back vented = excellent.
- (4) Can be either.
- (5) Usually end up "cracked open."



Moisture is always present in compressed air, and oil can be present at some points in a compressed air system. For the efficient operation and long life of gaskets, hoses and air tools, this excess moisture and the oil must be removed from the system.

The removal of moisture and oil from a system involves more than just traps. To maintain high efficiency and avoid costly problems, a compressed air system also requires:

- Aftercoolers to bring the compressed air down to ambient or room temperature.
- Separators to knock down suspended droplets of water or fog. Separators are installed downstream from aftercoolers or in air lines near point of use, or both.
- 3. Drain traps to discharge the liquid from the system with a minimum loss of air.

Table LD-1. \	Weight of Wa	iter Per Cubic	Foot of Air a	at Various Te	mperatures					
						of Saturation	I			
Temp. °F	10	20	30	40	50	60	70	80	90	100
	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains
-10	.028	.057	.086	.114	.142	.171	.200	.228	.256	.285
0	.048	.096	.144	.192	.240	.289	.337	.385	.433	.481
10	.078	.155	.233	.310	.388	.466	.543	.621	.698	.776
20	.124	.247	.370	.494	.618	.741	.864	.988	1.112	1.235
30	.194	.387	.580	.774	.968	1.161	1.354	1.548	1.742	1.935
32	.211	.422	.634	.845	1.056	1.268	1.479	1.690	1.902	2.113
35	.237	.473	.710	.946	1.183	1.420	1.656	1.893	2.129	2.366
40	.285	.570	.855	1.140	1.424	1.709	1.994	2.279	2.564	2.849
45	.341	.683	1.024	1.366	1.707	2.048	2.390	2.731	3.073	3.414
50	.408	.815	1.223	1.630	2.038	2.446	2.853	3.261	3.668	4.076
55	.485	.970	1.455	1.940	2.424	2.909	3.394	3.879	4.364	4.849
60	.574	1.149	1.724	2.298	2.872	3.447	4.022	4.596	5.170	5.745
62	.614	1.228	1.843	2.457	3.071	3.685	4.299	4.914	5.528	6.142
64	.656	1.313	1.969	2.625	3.282	3.938	4.594	5.250	5.907	6.563
66	.701	1.402	2.103	2.804	3.504	4.205	4.906	5.607	6.308	7.009
68	.748	1.496	2.244	2.992	3.740	4.488	5.236	5.984	6.732	7.480
70	.798	1.596	2.394	3.192	3.990	4.788	5.586	6.384	7.182	7.980
72	.851	1.702	2.552	3.403	4.254	5.105	5.956	6.806	7.657	8.508
74	.907	1.813	2.720	3.626	4.533	5.440	6.346	7.253	8.159	9.066
76	.966	1.931	2.896	3.862	4.828	5.793	6.758	7.724	8.690	9.655
78	1.028	2.055	3.083	4.111	5.138	6.166	7.194	8.222	9.249	10.277
80	1.093	2.187	3.280	4.374	5.467	6.560	7.654	8.747	9.841	10.934
82	1.163	2.325	3.488	4.650	5.813	6.976	8.138	9.301	10.463	11.625
84	1.236	2.471	3.707	4.942	6.178	7.414	8.649	9.885	11.120	12.326
86	1.313	2.625	3.938	5.251	6.564	7.877	9.189	10.502	11.814	13.137
88	1.394	2.787	4.181	5.575	6.968	8.362	9.756	11.150	12.543	13.997
90	1.479	2.958	4.437	5.916	7.395	8.874	10.353	11.832	13.311	14.780
92	1.569	3.138	4.707	6.276	7.844	9.413	10.982	12.551	14.120	15.639
94	1.663	3.327	4.990	6.654	8.317	9.980	11.644	13.307	14.971	16.624
96	1.763	3.525	5.288	7.050	8.813	10.576	12.338	14.101	15.863	17.676
98	1.867	3.734	5.601	7.468	9.336	11.203	13.070	14.937	16.804	18.661
100	1.977	3.953	5.930	7.906	9.883	11.860	13.836	15.813	17.789	19.766

Based on atmospheric pressure of 14.7 psia.



Water carried with air into tools or machines where air is being used will wash away lubricating oil. This causes excess wear to motors and bearings and results in high maintenance expense. Without adequate lubrication, the tools and machines run sluggishly and their efficiency is lowered. This effect is particularly pronounced in the case of pneumatic hammers, drills, hoists and sand rammers, where the wearing surfaces are limited in size and the excessive wear creates air leakage.

Where air is used for paint spraying, enameling, food agitation and similar processes, the presence of water and/or oil cannot be tolerated, nor can particles of grit or scale. In instrument air systems, water will tend to cling to small orifices and collect dirt, causing erratic operation or failure of sensitive devices.

Pipeline Troubles

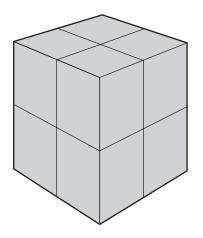
When water accumulates at low points in the pipeline, the air-carrying capacity of the line is reduced. Eventually, airflow over the pool of water will begin to carry the water along at high velocity. This produces "water hammer" along the line, and may even carry over a slug of water into a tool. In cold weather, accumulations of water may freeze and burst pipelines.

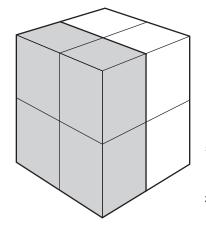
Air's Capacity to Hold Moisture

At atmospheric pressure (14.7 psia), 8 cu ft of air with an RH of 50% and a temperature of 70°F will contain 32 grains of moisture vapor.

When the pressure is doubled (without increasing the temperature) the volume is cut in half (4 cu ft), but there are still 32 grains of moisture. This means the relative humidity is now 100%—all the moisture in vapor form that it can handle.

Increasing the pressure to 100 psig (114.7 psia), the volume of air is further reduced to approximately 1 cu ft. This 1 cu ft of compressed air still at 70°F can hold a maximum eight grains of moisture.





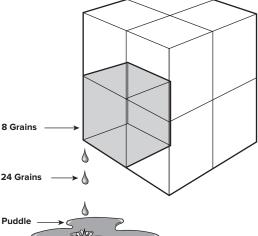


Figure LD-1.

Pressure: 0 psig (14.7 psia)
Temp: 70°F
Air = 8 CF
Moisture = 32 Grains
Max Possible = 64 Grains

Figure LD-2.

Pressure: 15 psig (29.7 psia)
Temp: 70°F
Air = 4 CF
Moisture = 32 Grains
Max Possible = 32 Grains

Figure LD-3.

 Pressure: 100 psig (114.7 psia)

 Temp: 70°F

 Air = 1 CF

 Moisture = 32 Grains

 Max Possible = 8 Grains

 24 Grains

24 Grains of Liquid



Drainage Problems and How to Avoid Them

Oil. A critical drainage problem exists at points where oil may be present in the compressed air (principally at intercoolers, aftercoolers and receivers).

Two facts create this problem:

- 1. Oil is lighter than water and will float on top of water.
- Compressor oil when cooled tends to become thick and viscous.

The beaker simulates any drain trap that has its discharge valve at the bottom, Fig. LD-4. Like the beaker, the trap will fill with heavy oil that may be thick and viscous.

Compare with Fig. LD-5, which shows an identical beaker except that the discharge valve is at the same level as the oil. Oil will escape until the oil level is so thin that for every 19 drops of water and one of oil that enter the beaker, exactly 19 drops of water and one drop of oil will leave. The beaker always will be filled with water.

The conclusion is obvious. When there is an oil-water mixture to be drained from an air separator or receiver, use a trap with the discharge valve at the top.

Dirt and Grit. While scale and sediment is seldom a problem between the compressor and receiver, it is encountered in the air distribution system, particularly when the piping is old. In this situation, scale will be carried to a drain trap along with the water. If the drain trap is not designed to handle dirt and grit, the trap may fail to drain water and oil, or the trap valve may not close.

Air Loss. Often in compressed air systems, the solution to one problem may also cause another problem. For example, a common method of draining unwanted moisture is to crack open a valve; however, this also creates a leak. The immediate problem is solved, but the "solution" has an obvious, and usually underestimated, cost of continual air loss

How much air is lost depends on orifice size and line pressure (see Table LD-2). The overall result is a decrease in line pressure, the loss of up to a third of the system's compressed air, and the cost of compressing it.

Leak control involves:

- Looking for leaks during shut-down with an ultrasonic leak detector
- Determining total leakage by observing how fast pressure drops with the compressor off, both before and after a leak survey
- Fixing leaks at joints, valves and similar points
- Replacing cracked-open valves with drain traps
- Checking the system regularly

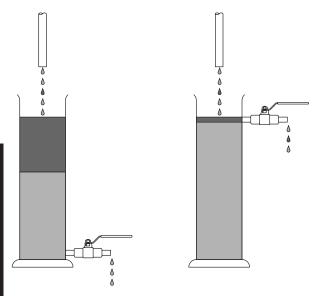


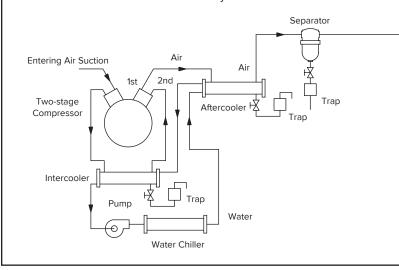
Figure LD-4.

If a beaker collecting oil and water is drained from the bottom at the same rate that oil and water enter, it will eventually fill entirely with oil because oil floats on water.

Figure LD-5.

If a beaker collecting oil and water is drained from the top at the same rate that oil and water enter, it soon will be entirely filled with water because the oil floats on the water.

Figure LD-6. Drain Trap Locations in a Compressed Air System The use of drain traps is an effective way to remove water that collects in many places in a compressed air system. Each trap location must be considered individually.



475 I N-9



Drainage Methods

Manual. Liquid may be discharged continuously through cracked-open valves, or periodically by opening manually operated drain valves.

Open drains are a continuous waste of air or gas—and the energy to produce it. A valve manually opened will be left open until air blows freely. Frequently, however, the operator will delay or forget to close the valve, and precious air or gas is lost.

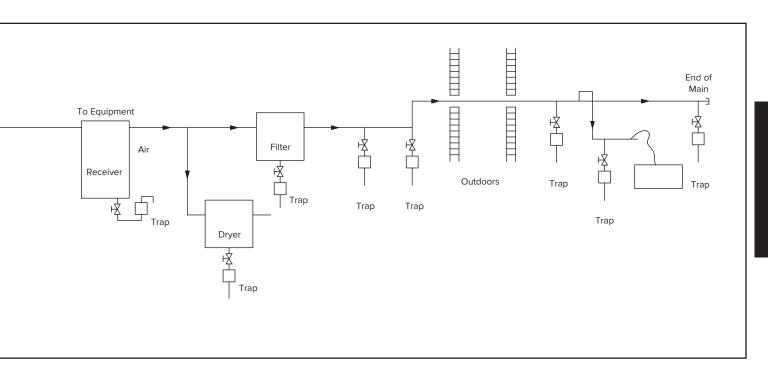
Automatic. Automatic drainage equipment that is adequate for the system is seldom included in the original system. However, subsequent installation of automatic drain traps will significantly reduce energy and maintenance costs.

Drain Traps. Water collected in separators and drip legs must be removed continuously without wasting costly air or gas. In instances where drain traps are not part of the system design, manual drain valves are usually opened periodically or left cracked open to drain constantly. In either case, the valves are opened far enough that some air and gas are lost along with the liquid. To eliminate this problem, a drain trap should be installed at appropriate points to remove liquid continuously and automatically without wasting air or gas.

The job of the drain trap is to get liquid and oil out of the compressed air/gas system. In addition, for overall efficiency and economy, the trap must provide:

- Operation that is relatively trouble-free with minimal need for adjustment or maintenance
- Reliable operation even though dirt, grit and oil are present in the line
- Long operating life
- Minimal air loss
- Ease of repair

Table LD-2. Cost of Various Size Air Leaks at 90 psig									
Orifice Diameter (in)									
3/8	138.00	\$1 207.50	\$14 490						
1/4	61.00	533.75	6 405						
1/8	15.40	134.75	1 617						
7/64	11.80	103.25	1 239						
5/64	6.00	52.50	630						
1/16	3.84	33.60	403						





Inverted Bucket Drain Traps

For Heavy Oil/Water Service

BVSW inverted bucket drain traps are designed for systems with heavy oil or water services.

An inverted bucket is used because the discharge valve is at the top, so oil is discharged first and the trap body is almost completely filled with water at all times.

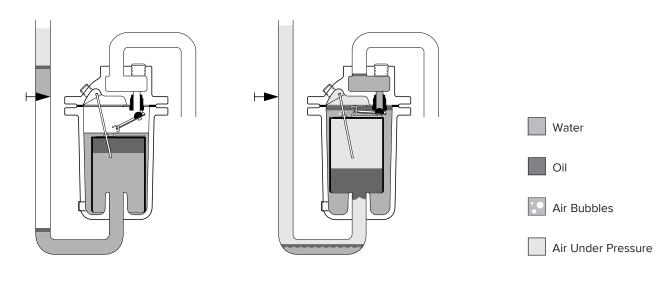
BVSW stands for Bucket Vent Scrubbing Wire. This 1/16" dia. wire swings freely from the trap cap and extends through the bucket vent. Its function is to prevent reduction of vent size by buildup of solids or heavy oil in the vent itself. The up-and-down motion of the bucket relative to the vent scrubbing wire keeps the vent clean and full size.

Operation of Inverted Bucket Drain Traps

- Since there is seldom sufficient accumulation of water to float the bucket and close the valve, the trap must be primed on initial start-up or after draining for cleaning. Step 1 shows "after operating" primed condition with oil in the top of bucket and a very thin layer of oil on top of water in the trap body.
- When valve in line to trap is opened, air enters bucket, displacing liquid. When bucket is two-thirds full of air, it becomes buoyant and floats. This closes the discharge valve. As bucket rises, the vent scrubbing wire removes oil and any dirt from bucket vent.

Both liquid and air in trap are at full line pressure, so no more liquid or air can enter trap until some liquid or air escapes through the discharge valve. Static head forces air through bucket vent. The air rises to top of trap and displaces water that enters bucket at bottom to replace air that passes through vent. Just as soon as bucket is less than two-thirds full of air, it loses buoyancy and starts to pull on valve lever as shown in Step 3.

Figure LD-7. Operation of the BVSW Inverted Bucket Drain Trap



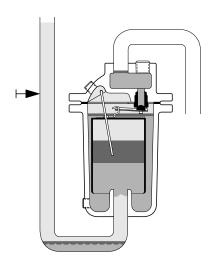
- 1. Trap primed, air off, bucket down, trap valve open.
- 2. Trap in service, bucket floating. Air passes through bucket vent and collects at top of trap.

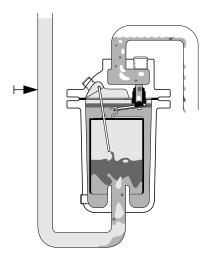


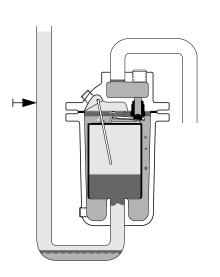
Inverted Bucket Drain Traps



- 3. Note that liquid level at top of trap has dropped and the liquid level in the bucket has risen. The volume of water displaced by air exactly equals the volume of water that entered the bucket. During this valve-closed part of the operating cycle—Steps 2 and 3—water and oil are collecting in the horizontal line ahead of the trap. When the bucket is about two-thirds full of liquid, it exerts enough pull on lever to crack open the discharge valve.
- 4. Two things happen simultaneously. a) The accumulated air at top of trap is discharged immediately, followed by oil and any water that enters the trap while the valve is cracked. b) Pressure in trap body is lowered slightly, allowing accumulated liquid in horizontal line to enter the trap. Air displaces liquid from the bucket until it floats and closes the discharge valve, restoring the condition shown in Step 2.
- 5. When full buoyancy is restored, the trap bucket is twothirds full of air. Oil that has entered while trap was open flows under bottom of bucket and rises to top of water in trap body. The trap normally discharges small quantities of air several times per minute.







- Water enters bucket to replace air passing through bucket vent. This increases weight of bucket until...
- ...pull on lever cracks valve. Air at top of trap escapes, followed by oil and water. Liquid in pipe ahead of trap enters bucket followed by air.
- Air displaces liquid and excess oil from bucket, restoring condition shown in Step 2.



Float Type Drain Traps

Closed Float

Hollow, thin-wall metal floats are attached through linkages to valves at the trap bottom, and a seat with an appropriately sized orifice is inserted at the trap outlet. Floats are selected to provide adequate buoyancy to open the valve against the pressure difference. Discharge usually is to atmosphere, so the pressure drop is equal to the system air pressure. The float and linkage are made of stainless steel, and the valve and seat are hardened stainless steel for wear resistance and long life. The body is cast iron, stainless steel, or cast or forged steel depending on gas pressure. Bodies may be made of stainless steel to resist corrosive gas mixtures.

Entering liquid drops to the bottom of the body. As liquid level rises, the ball is floated upward, thereby causing the valve to open sufficiently that outlet flow balances inlet flow. Subsequent change of incoming flow raises or lowers water

level further opening or throttling the valve. Thus discharge is proportionally modulated to drain liquid completely and continuously. However, gas flow may be constant or it may abruptly change depending on system demand characteristics. Liquid formation may be sporadic, or the nature of flow generation may cause surges. At times, flow will be very low, requiring operation to throttle the flow or even tight shut-off. Tightness of closure, gas leakage and trap cost will depend on the design of linkage and valve.

Free Floating Lever

The discharge from the No. 1-LD is continuous. The opening of the valve is just wide enough to remove the liquid as fast as it comes to the trap. Thus, at times, the valve is barely cracked from its seat.

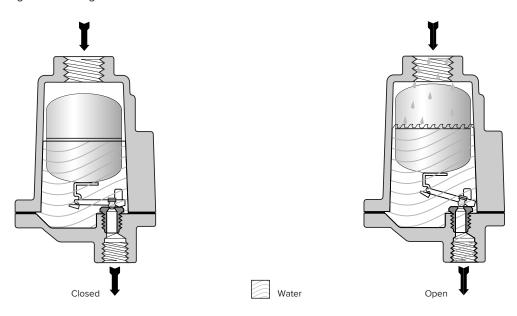


Figure LD-8. Operation of the No. 1-LD Free Floating Lever Drain Trap
As water begins to fill the body of the trap, the float rises, opening the
discharge valve. Motion of the free floating valve lever is guided to
provide precise closure.

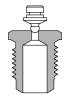
Free Floating Linkage Valve

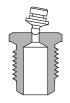
A hemispherical ball-shaped valve is attached to linkage which is suspended freely on two guide pins. There is no fixed pivot or rigid guides; therefore, the attachment is loose. There are no critical alignments, and the lever and valve may move in all directions. Consequently, the lever may move the

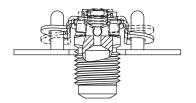
valve to the seat in any alignment. As the valve approaches the seat, the pressure pushes the round valve into the square edge orifice of the seat, effecting a line seal to attain bubble-tight closure.

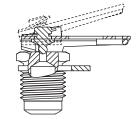
Figure LD-9. Free Floating Linkage



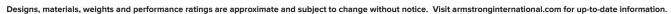








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Float Type Drain Traps



Fixed Pivot Conical Valve

A conically shaped valve is attached to a fixed pivot leverage system. The fixed pivot does not allow the valve to move

freely to conform to the seat for tight closure. Thus, it may not seal tightly, and some loss of air or gas may be expected.

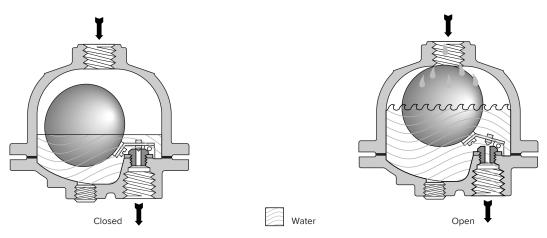


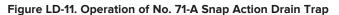
Figure LD-10. Operation of No. 21 Fixed Pivot Drain Trap

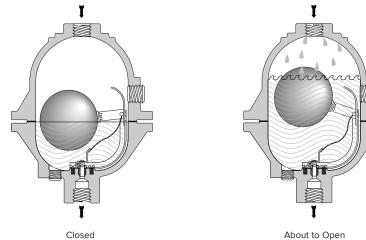
As the water level rises, the ball float cracks the valve to drain liquid at the same rate that it reaches the trap. Changes in the rate of flow to the trap adjust the float level and the degree of opening of the valve.

Snap Action Valve

Because of the sporadic liquid flow, much of the time the valve in a standard float-type drainer is only slightly opened. If there is fine dirt or grit in the liquid, particles may accumulate and clog the partially open valve, or they may lodge between the valve and seat, preventing closure. To overcome this, a special toggle-spring operated valve is used.

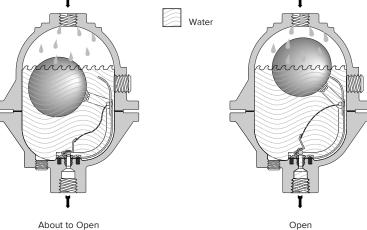
A flat spring attached to the leverage system holds the valve closed until liquid level is high enough for the buoyancy to exceed the spring force. Then the valve is snapped open, and the accumulated dirt and grit can be flushed through the wide open valve. When the body is nearly empty, buoyancy is reduced enough to permit the spring to snap the valve closed.





Filling Cycle. Trap valve has just closed. Spring bowed to right. Float and sprides high in water because no force is exerted on spring. As water enters, float rises, storing energy in spring.

This increases submergence of float.



Float now is more than half submerged and spring has assumed a "handlebar mustache" shape. Energy stored in spring is due to increased displacement of water. A very slight rise in water level causes spring to snap to the left... ...Instantly the valve opens wide. This releases energy from spring and float again rides high in water. As water level drops, weight of float bends spring to right, causing snap closing of valve before all the water has been discharged.



Drain Trap Selection

To obtain the full benefits from the traps described in the preceding section, it is necessary that the correct size and pressure of drain trap be selected for each job, and that it be properly installed and maintained.

Rely on Experience. Most drain traps are selected on the basis of experience. This may be:

- Your personal experience
- The experience of your Armstrong Representative or distributor
- The experience of thousands of others in draining identical equipment

Do-It-Yourself Sizing is required at times. Fortunately, drain trap sizing is simple when you know or can figure:

- 1. Liquid loads in lbs/hr.
- 2. Pressure differential.
- 3. Maximum allowable pressure.
- **1. Liquid Load.** Each "How To" section of this handbook contains formulas and useful information on proper sizing procedures and safety factors.

2. Pressure Differential. Maximum differential is the difference between main pressure, or the downstream pressure of a PRV, and return line pressure. See Fig. LD-12. The drain trap must be able to open against this pressure differential.

Operating differential. When the plant is operating at capacity, the pressure at the trap inlet may be lower than main pressure. And the pressure in the return header may go above atmospheric.

If the operating differential is at least 80% of the maximum differential, it is safe to use maximum differential in selecting traps.

IMPORTANT: Be sure to read the discussion on page LD-16, which deals with less common, but important, reductions in pressure differential.

3. Maximum Allowable Pressure. The trap must be able to withstand the maximum allowable pressure of the system, or design pressure. It may not have to operate at this pressure, but it must be able to contain it. As an example, the maximum inlet pressure is 150 psig and the return line pressure is 15 psig. This results in a differential pressure of 135 psig; however, the trap must be able to withstand 150 psig maximum allowable pressure. See Fig. LD-12.

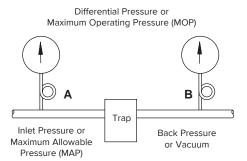


Figure LD-12. "A" minus "B" is Pressure Differential: If "B" is back pressure, subtract it from "A." If "B" is vacuum, add it to "A"



Drain Trap Selection



Factors Affecting Pressure Differential

Pressure Differential in Detail

Inlet pressure can be:

- 1. Air main pressure.
- Reduced pressure controlled by a pressure reducing valve station.

Discharge can be:

- 1. Atmospheric.
- Below atmospheric—under vacuum. Add vacuum to inlet pressure to get pressure differential.
 Hq vacuum = approximately 1 psiq of pressure
 - below atmospheric.
- 3. Above atmospheric due to:
 - a. Pipe friction
 - b. Elevating liquid

Every 2' lift reduces pressure differential by approximately 1 psig, when the discharge is only liquid.

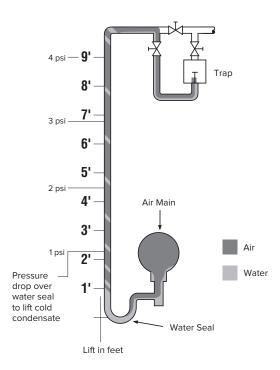


Figure LD-13. Liquid from gravity drain point is lifted to trap by a syphon. Every 2' of lift reduces pressure differential by approximately 1 psig. Note seal at low point and the trap's internal check valve to prevent back flow.

Special Considerations

Drain traps are available for services other than those found on standard compressed air systems.

High Pressure

Spring-loaded mechanisms allow float type drain traps to operate on pressures above 3 000 psig.

Fluids Other Than Water

Different fluids, such as oils and liquid, can be compensated for with specially weighted floats or lower operating pressure ratings. Fluids with specific gravities down to 0.4 will work with float type drain traps.

Materials of Construction

Service requirements for stainless steel or other corrosionresistant materials can be met by float and inverted bucket type drain traps.

NACE Sour Gas Service

Special materials and construction are required for hydrogen sulfide service.

High Capacity for Large Flow Rates

Ultra-capacity type drain traps allow float type drain traps to be used on service requiring capacities up to 700 000 lbs/hr.

Dual Gravity

Float type drain traps can be modified to drain a heavier fluid from a lighter fluid.



Air distribution systems make up the vital link between compressors and the vast amount of air-utilizing equipment. They represent the method by which air is actually transported to all parts of the plant to perform specific functions.

The three primary components of air distribution systems are air mains, air branch lines, and air distribution manifolds. They each fill certain requirements of the system, and together with separators and traps, contribute to efficient air utilization. Common to all air distribution systems is the need for drip legs at various intervals. These drip legs are provided to:

- 1. Let liquid escape by gravity from the fast-moving air.
- 2. Store the liquid until the pressure differential can discharge it through the drain trap.
- 3. Serve as dirt pockets for the inevitable dirt and grit that will accumulate in the distribution system.

Air mains are one of the most common applications for drain traps. These lines need to be kept free of liquid to keep the supplied equipment operating properly. Inadequately trapped air mains often result in water hammer and slugs of liquid, which can damage control valves and other equipment. There is also a freeze potential wherever water is allowed to accumulate. In areas where air is moving slowly, the accumulation of water can effectively reduce the pipe size, thereby increasing the pressure drop and wasting energy.

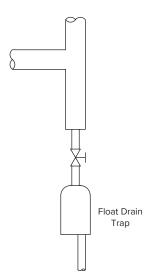


Figure LD-14.Drain trap installed straight under a low point.

Chart LD-3. Recommendation Chart

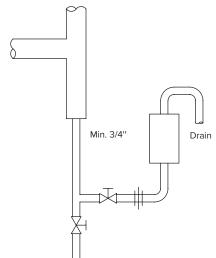


Figure LD-15.
Series 200 or 300 inverted bucket drain traps installed on compressed air line contaminated by oil.

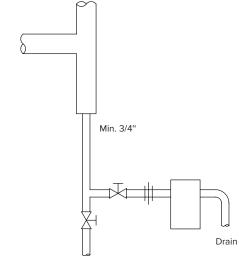


Figure LD-16.
Series 800 or 900 inverted bucket drain traps installed on compressed air line contaminated by oil.

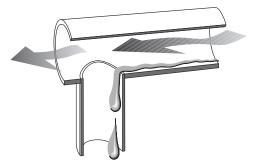


Figure LD-17. Drip leg length should be at least 1-1/2 times the diameter of the main and never less than 10". Drip leg diameter should be the same size as the main, up to 4" pipe size and at least 1/2 of the diameter of the main above that, but never less than 4".

(See chart on page LD-6 for "Feature Code" references.)

Air Mains

1st Choice and Feature Code

FF B, C, D, J, M

Alternate Choice and Feature Code

Alternate Choice and Feature Code

Feature Code

^{*}IB is a good alternative where heavy oil carryover is likely.



Selection of Drain Traps and Safety Factor for Air Mains

Traps should be selected to discharge a volume of liquid normally produced when the system is up and running. Liquid loads can be estimated if actual CFM or air volume flow is not known. If cold temperatures are possible, the dew point at supply pressure must be known. Once this maximum is determined, the safety factor used to size the trap will be only 10% of the total potential liquid load. Ten percent of the total is used because most of the liquid has been removed in the aftercooler and receiver. The drain trap must handle only the small remaining amount of 10% of the total possible load.

If actual airflow rate is not known, it can be estimated using Chart LD-4, titled "Pressure Drop in Compressed Air Pipe." Using an assumed pressure drop of 1/4 (.25) psig per 100 ft, and 100 psig gauge pressure of air through a 4" line, it can be seen that approximately 1 000 cu ft of free air per minute are flowing through the line. Taking this figure to the chart titled "Water Condensed From Compressed Air," Chart LD-6 on page LD-20, it can be seen that if 80°F, 90% RH air is delivered at 100 psig, then 1.2 lbs of water will be condensed per minute at 1 000 CFM. This number will be multiplied by 60 to convert from minutes to hours, which equals 72 lbs/hr. For this air main then, take 10% of this figure, or 7.2 lbs/hr, to be the flow rate to the drainer.

Rule of Thumb for Calculating Compressor Liquid Loads

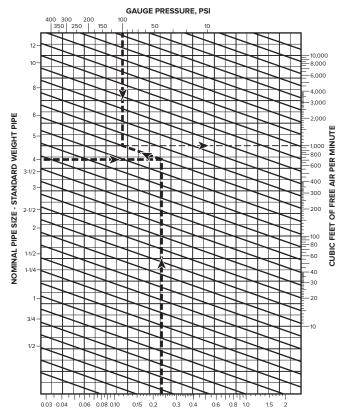
 $\frac{\text{CFM x 20 gr/cu ft x 60 min/hr}}{7\ 000\ \text{gr/#}} = \#/\text{hr}$

- Assuming worst condition: 100°F @ 100% RH For other conditions, see page LD-7
- 2. Using air main safety factor of: Load x 10%

Installation of Drain Traps on Air Mains

Drip Legs. All air mains should utilize drip legs and traps at all low spots or natural drainage points, such as ahead of risers, end of mains, ahead of expansion joints or bends, and ahead of valves and regulators (see installation Fig. LD-17).

Where there are no natural drainage points, drip legs and drain traps should still be provided. These should normally be installed at intervals of about 500 ft.



PRESSURE DROP, PSI PER 100 FT

Chart LD-4. Pressure Drop in Compressed Air Pipe

Chart gives pressure drop in compressed air piping in pounds per square inch per 100 ft of pipe. Initial pressure, flow and size of pipe must be known or assumed.



Branch Lines

Branch lines are takeoffs of the air main supplying specific areas of air-utilizing equipment. Branch lines must always be taken from the top of the air main. The entire system must be designed and hooked up to prevent accumulation of liquid at any point. If a specific process area requires it, an air dryer will be installed on the branch line.

Trap Selection and Safety Factor for Branches

The formula for computing liquid load in branch lines is the same as that used for air mains. Branch lines also have a recommended safety factor of 10% of total air load. Drip legs must be installed ahead of risers and at the end of branch lines, especially when branch line runouts exceed 50 ft. There are usually several branches off the air main, and in many cases they experience a high liquid load when they run against cold outside walls. This cooling causes more moisture to condense in the branch line than would be seen in the air main.

Distribution Manifolds

A distribution manifold is a terminal for a branch line from which several air users are taken off. They are particularly common in manufacturing facilities for pneumatic tool hookups or takeoffs to cylinder actuators. Like branch lines, it is common for distribution manifolds to be installed against cool walls where low temperatures cause condensation and the accumulation of liquid.

Distribution manifolds are often equipped with filters and regulators. Regulators may also be found at the termination before the air-using device.

Since the air distribution manifold is usually one pipe size larger than the branch line, it is common for air velocity to drop when coming from the branch line. With this decrease in velocity, often combined with lower ambient temperatures, it is common for a liquid to accumulate in the distribution manifold. For this reason, the use of filter-drainer combinations or separate drain traps is recommended. Trapping the liquid in the distribution manifold is important to protect the regulators on air-using equipment and orifices in air-using instruments.

This is a location where manual valves are commonly misused due to their accessibility. To drain the liquid and keep it from fouling an instrument or pneumatic tool, manual valves will often be cracked to atmosphere. When they are left this way, the result is a large air loss due to the unrestricted free blow of air to atmosphere.

Trap Selection and Safety Factor for Distribution Manifolds Normally the smallest drain trap is practical for distribution manifolds up to manifold diameters of 2". Above 2", the distribution manifold should be considered a branch, and then the sizing procedure from the Air Main section would apply.

Chart LD-5. Recommendation Chart (See chart on page LD-6 for "Feature Code" references.)							
Equipment Being Drained 1st Choice and Feature Code Alternate Choice							
Branch Lines	FF B, C, D, J, M	FP*					
Distribution Manifolds	FF B, C, D, I, M	FP					

*IB is a good alternative where heavy oil carryover is likely.





Installation

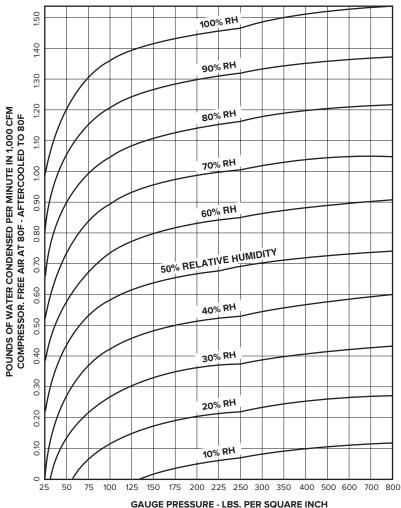
The ABCs of trap installation must be followed: "A" for accessible, "B" for below the point being drained, and "C" for close to the point being drained. If the discharge point for this drain trap is some distance away from the drain point, the discharge line from the trap should be run out—not the inlet to the trap.

When installing traps on the drain connection of filters, particular care should be taken to the connection size. Normally outlet connections on filters are 1/4" in size or less. This connection size is normally not large enough to allow anything but slugs of liquid to flow into the trap housing. If a float trap is utilized, it should be either back vented or the connection size must be increased to 3/4" minimum. For additional installation recommendations, see pages LD-51 and LD-52.

Table L	Table LD-3. Correction Factors										
F	For lbs water condensed at temperatures other than 80°F, find wt condensed at 80°F and multiply by factors shown.										
°F	°F Factor °F Factor °F Factor °F Factor										
10	.070	50	.373	100	1.81	140	5.15				
20	.112	60	.525	110	2.39	150	6.52				
30	.176	70	.729	120	3.12	160	8.19				
40	.259	90	1.35	130	4.02	170	10.2				

Chart LD-6. Water Condensed From Compressed Air





NOTE: Amount of water condensed is in direct ratio to compressor rating. For example, for 500 CFM compressor, multiply determined amount of condensate by 0.50; for 200 CFM compressor, multiply amount of condensate by 0.20.





How to Drain Intercoolers, Aftercoolers, and Aftercooler Separator Combinations

Aftercooler

An aftercooler serves as the primary means of moisture removal on industrial air systems. It increases the efficiency of air distribution by reducing pressure drop created when air flows through the system. It does this by using cooling water to reduce the specific volume of the air which, in turn, allows the air to flow through the system with less pressure drop. Aftercoolers are found on most industrial compressors over 10 hp in size. In addition to removing the heat of compression, aftercoolers also remove approximately two-thirds of the liquid found in the air, and help in the removal and knock-down of oil carryover from the compressor.

Intercooler

Compressor intercoolers are designed to increase the efficiency of compression by reducing the temperature and specific volume of air between stages of compression. This allows the compressor to do more work at a lower temperature than would normally occur. Because some condensing will occur in the intercooler, a drain trap is required to protect compressor parts.

If liquid were to carry over from the intercooler, it could also carry dirt or scale into the compressor and/or also cause corrosion within the compressor, both of which are undesirable for efficient compressor operation. If slugs of liquid were to pass from the intercooler into the compressor, it would make the compressor operation erratic. Efficient trapping is required at this point to deliver dry air to the next stage of the compressor.

An intercooler is typically a shell and tube heat exchanger. Liquid condensate flow out of the heat exchanger is usually irregular, causing slugs to accumulate and pass into the drain trap. Because of this, a drip leg is required on the intercooler, and full size outlet piping from the intercooler must be used into a dirt pocket. The drip leg allows the slug of condensate to be handled by the drain trap and handles some small backup while the drain trap is discharging the liquid.

The intercooler may also experience oil carryover if the compressor is not of the oil-less or sealed type. As air enters the intercooler, it carries a mist or tiny droplets of oil along with it. Because the air is at a relatively high temperature, this oil is fairly thin. Then, as the intercooler cools the air and oil, the oil may thicken. The drain trap must be able to discharge this oil before it thickens and negatively affects the drain trap and intercooler operation. Trap selection is very important in this type of application where a water and oil mix must be handled by the trap and the oil must be discharged first.

Since the aftercooler removes approximately two-thirds of the total moisture load, traps here will normally be much larger than those found on the rest of the system.

Trap Selection and Safety Factor Intercooler

Select the proper trap for:

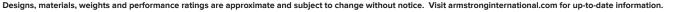
- 1. Entering water temperature into the intercooler.
- 2. Airflow rate through the intercooler.
- Intermediate pressure at which the intercooler is operated.

Use Chart LD-6 on page LD-20, "Water Condensed From Compressed Air," to determine the pounds of water condensed per minute in 1 000 CFM. Then multiply by 60 to convert minutes to hours and use a safety factor of 2:1.

Chart LD-7. Recommendation Chart (See chart on page LD-6 for "Feature Code" references.)								
Air Gas								
Equipment Being Drained	1st Choice and Feature Code	Alternate Choice	1st Choice and Feature Code	Alternate Choice				
Aftercooler	IB F	FF	*FF					
Intercooler	tercooler , G, J, K, M		B, E, J	FP				

^{*}Since IBs vent gas to operate, an FF is suggested because gas venting may not be desirable.





How to Drain Intercoolers, Aftercoolers, and Aftercooler Separator Combinations



When selecting the type of trap, consider the failure mode and the ability of the trap to respond to slugs of liquid. In most cases, an "open" failure mode will be desirable as it is vital to protect the compressor from slugs of liquid. A quick response to slugs is important so there is no delay between the time the liquid accumulates and the trap discharges the liquid.

Aftercooler

When the aftercooler condensing rate is not known, there are two typical methods for calculating condensate load. The first method is to calculate total airflow through the system. Then using Chart LD-6 on page LD-20, titled "Water Condensed From Compressed Air," determine pounds of water condensed per minute in 1 000 CFM. Multiply this by 60 to convert minutes to hours for required trap capacity in pounds per hour (the entering maximum incoming summertime temperature and relative humidity must be known to use this chart). This load is then multiplied by 2 to determine required trap capacity.

The second method of calculating trap capacity is to look at maximum allowable flow rate through the aftercooler. Use the "Water Condensed From Compressed Air" chart on page LD-20 in the same manner as described in Method 1. Although this method will normally yield a larger trap size, it allows for the addition of another compressor or the interconnection of several compressors to the system in the event of unplanned by-passes.

In the second method, it's important to estimate the average

water temperature within the aftercooler as closely as possible. Not all air actually comes in contact with the water tubes; therefore, the air is not uniformly cooled to the water temperature. If actual leaving air temperature is known, this is by far the most accurate figure to use. A properly sized aftercooler will normally cool compressed air down to within 15°F of entering air temperature.

Installation

When installing drain traps on aftercoolers or aftercooler separator combinations, the "ABCs" of trap installation should be followed:

- Accessible for maintenance and repair.
- Below the point being drained.
- Close to the drip point as possible.

Be sure to follow manufacturer's instructions on trap installation. Most aftercoolers are equipped with a separate separator. However, if a separator is not furnished, the aftercooler must be trapped individually. In the case of the aftercooler/ separator combination, only the separator normally requires a trap. See Fig. LD-18 or LD-19. But again, it is important to follow manufacturer's instructions. For additional installation recommendations, see pages LD-51 and LD-52.

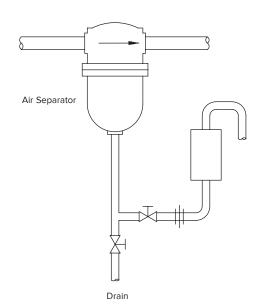


Figure LD-18. Installation of a 200 Series inverted bucket drain trap on compressed air contaminated by oil.

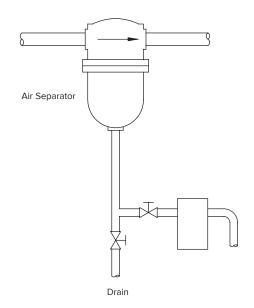


Figure LD-19. 800 Series inverted bucket drain trap

installed on compressed air contaminated by oil.



How to Drain Separators, Separator Filter Combinations

Separators serve an important function within the compressed air system. Separators may also be known as knockout pots, knockout drums or demisters. Their function is to remove liquid that may be moving at a high speed from the flowing air, and they normally perform this function in a two-step process.

- Separators increase the flow area and volume of the gas, thereby reducing its velocity. Air within the system may flow at velocities exceeding 100 mph. At this velocity any liquid will be entrained as droplets and will not be flowing along the bottom of the pipe. To remove these liquid droplets, it is necessary to reduce the velocity of the gas; otherwise, the droplets accumulate and again become entrained with the flowing gas.
- 2. The second step is to change direction and impinge the liquid. As the velocity of the gas is reduced, the velocity of the fast-moving droplets can be reduced even further by causing the air to take either 90-degree turns or to centrifugally flow within a chamber. Both of these methods serve to "sling" the droplets up against baffles, plates or the wall of the separator.

Because the droplets have a relatively high mass and are incompressible, their velocity will drop dramatically. At this point, gravity will take over, causing the drops to accumulate and flow into the bottom of the separator. Liquid will often fall in sheets down the wall of the separator and collect at the outlet piping in slugs. The immediate drainage of the slugs is important since the separator is normally a final opportunity to protect an air-using device downstream.

If liquid is allowed to accumulate for any amount of time, it may undermine the entire purpose and function of the separator. Therefore, if the separator does not do its job efficiently, it can actually become a reservoir that accumulates condensate and forms slugs to be transmitted down the air line and into the device being protected. In this case, the use of a separator may be worse than no protection at all.

Locations

Separators are normally located on the leaving side of aftercoolers and before the compressed air receiver. They are often integral with filters located before sensitive air-using equipment or as part of the filter on a distribution manifold. In this case there may be a combination filter, oiler, regulator and separator drainage point for liquids to accumulate.

Trap Selection and Safety Factor

If the separator is part of an aftercooler combination installed between the compressor and the receiver, you should refer to the section on Aftercoolers and Aftercooler Separators for trap selection.

Trap selection is fairly critical, especially on equipment with larger than 1" air lines feeding it, since slug formation can wash scale into the air-using equipment and become a serious dirt problem. Therefore, on larger than 1" separators, the flow should be calculated by totaling the air consumption of the devices downstream and using Chart LD-6, "Water Condensed From Compressed Air," on page LD-20. Use the full water load expected and the safety factor of 3:1 to figure trap capacity.

Chart LD-8. Recommendation Chart (See chart on page LD-6 for "Feature Code" references.)								
Equipment Being Drained 1st Choice and Feature Code Alternate Choice								
Separator Line Size > 1"	FF*	IB						
Separator Inlet Pipe < 1"	J, B, C, E	FP*						

*IB is a good alternative when heavy oil carryover is likely.



How to Drain Separators, Separator Filter Combinations



To determine proper trap capacity for separators with a pipe size of **less than** 1", the flow can be estimated by using Chart LD-6, "Water Condensed From Compressed Air," on page LD-20, and then calculating 20% of full load.

The safety factor for both selection procedures is 3:1 since separators must respond to surges of liquid from the inlet. In this case, the trap must handle far more liquid than would be experienced under normal operation.

Installation

When installing ball float type traps on separators 1" and above, it's important to back vent the trap (refer to the section on how to hook up ball floats for the purpose and function of back vent lines, page LD-51). All other types of drainers should be coupled as closely as possible to the drain leg. The drain leg should be the same size as the drain connection on the separator and extend 6" below the separator with another 6" allowed for a dirt pocket. The trap is then tee'd off this line (see Figs. LD-20 and LD-21). This piping is crucial because, as noted above, if the separator does not receive full drainage, it can be worse than no separator at all. For this reason, the "ABCs" are critical:

Accessible for inspection and maintenance.

Below the equipment being drained.

Close to the drain point.

The line size leading from the drip leg to the inlet of the unit should be kept the same size as the trap inlet for good drainage into the trap. Again, when slugs are being handled it's important that the trap begin draining immediately. Back vents on float type traps should be a minimum of 1/2" in pipe size with 3/4" preferred. Any valves used in this back-vent piping should be full ported to allow free gas flow out of and liquid flow into the drain trap. For additional installation recommendations, see pages LD-50 to LD-52.

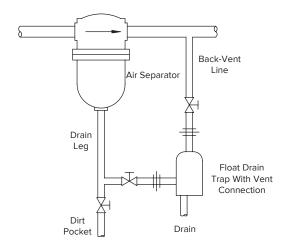


Figure LD-20. Installation of a drain trap with equalizing line downstream of the separator in order to assure a quick and regular flow to the drainer. Note side inlet connection from separator.

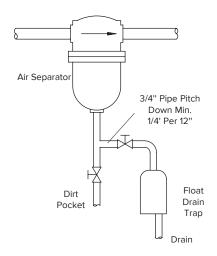


Figure LD-21. Installation of a drain trap on side of separator.



How to Drain Receivers

Receivers perform the vital function of storing air for the system. The receiver dampens pressure fluctuations in the system and provides a very short storage time in the event of compressor failure. It also functions as a liquid knockout drum to prevent entrained liquid (which may carry over) from entering the compressed air dryer or the air mains. The receiver should be sized to provide enough storage time for an orderly shutdown, particularly in the case of instrumentation air systems. Receiver volume is what provides the amount of air required for storage periods.

The receiver should be located close to the compressor. Fallout of liquid is normal due to low velocity within the receiver. Velocity is at the lowest point it will reach in any other part of the operating system. The air has a high dwell time within the receiver and is more likely to cool to ambient. This cooling of the air is what causes moisture to condense.

The receiver is equipped with a drain port at the bottom to allow liquids to flow to drain traps. In many cases, because receivers are so large and located adjacent to the compressor, they are installed close to the floor. When this happens, the drain point is relatively inaccessible, making trap piping difficult and gravity flow into the trap often impossible. To avoid this, the receiver should be located on a small concrete pad, which will facilitate efficient drain trap installation and operation.

For several reasons, it's good to keep the receiver drained. When receiver volume is lost, the dampening of the compressed air pressure is reduced and the storage time between compressor failure and system shutdown is greatly reduced. Corrosion within the receiver can also take place when liquid is allowed to accumulate.

Manual valves are commonly used to drain receivers since they are typically installed close to the floor. The resulting loss of receiver volume is seldom noticed in the day-to-day operation of the system. However, with any manual system, the valve can be forgotten and not opened. Then, when the weather changes from a relatively dry, low moisture load to a warm, high moisture load, the receiver will lose volume and the dampening effect and accumulator effect are decreased. The compressor can short cycle under these conditions, increasing the wear and tear on the compressor. In addition, the only reminder to open the manual valve is when carryover occurs. In this case, an air dryer can be damaged, liquid can be introduced into the air mains and surge through the system, causing scale to be washed into the system, water hammer and/or freeze damage.

Trap Selection and Safety Factor

To select the proper trap for the receiver, it is necessary to calculate total system load using Chart LD-6, "Water Condensed From Compressed Air," on page LD-20. Once this total potential load is known, it will be multiplied by the following factors: With an aftercooler, multiply the load by 50%, with an aftercooler separator combination, multiply the total load by 40%, and if no aftercooler is present, multiply the total load by 70%. Once this load is known, a safety factor of 2:1 is applied.

Table LD-4. Total System Load Multipliers							
Calculate Total System Load with	Aftercooler	Aftercooler Separator	None				
Multiply by	50%	40%	70%				

Chart LD-9. Recommendation Chart (See chart on page LD-6 for "Feature Code" references.)					
Equipment Being Drained Seature Code Alternate Choice					
Receivers	FS* C, E, I, J, K	IB D			

*FF for over 120 lbs/hr load.



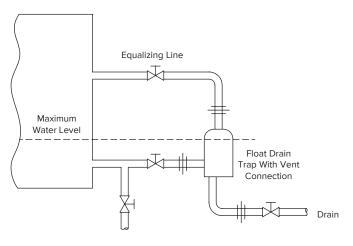
How to Drain Receivers



Installation

When a float type drain trap is used with a receiver, the level will run at about the inlet connection on the trap. Therefore, it is important to locate the trap as close to the floor as feasible and with no dips in the piping. See Figs. LD-22 thru LD-25. If there is a piping dip with a float type unit and the vent connection is not back vented, the unit will fail to operate. In the case of a back-vented unit, the dip in the piping will be flooded at all times. An inverted bucket trap can be installed above floor level since it will operate above the drain point. An

internal check valve, tube and coupling should be installed to prevent the liquid seal from flowing backward on system shutdown. A snap action type float unit should be used when any amount of grit is expected in the system. In this case, the spring life can be extended by moving the drain trap slightly upward to allow liquid to accumulate both within the receiver and within the trap body between trap cycles. For additional installation recommendations, see pages LD-50 to LD-52.



Receiver

3/4" Pipe Pitch
Down Min.
1/4' Per 12"

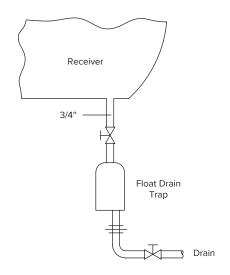
Float Drain
Trap

Drain

Figure LD-22.Drain trap installed at side of a receiver, close to floor. Water will rise to broken line before drain trap opens.

Figure LD-23.

Install the drain trap on side to get better access or compensate for lack of space under the receiver (particularly for drain trap used under compressors).



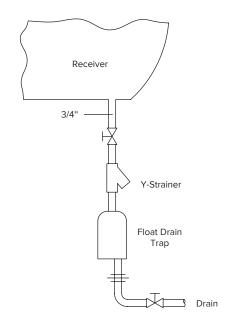


Figure LD-24.

Installation **not recommended** because of the dirt problem that can occur with a drain trap installed straight under the receiver.

Figure LD-25.

Same installation but with a strainer protecting the drain trap.



How to Drain Dryers

The function of dryers is to eliminate liquid in applications where freezing or any moisture accumulation can cause serious problems with the air-consuming equipment. Dryers should always be installed on instrument quality air systems.

Two basic dryer types are dessicant and refrigerated. In the dessicant type, the dessicant chemical absorbs the liquid by chemically bonding with the water molecules. Dessicant dryers can achieve very low dew points and are often installed with a pre-dryer of the refrigerant type. Refrigerant dryers work the same as aftercoolers by circulating cold fluid, causing the moisture to condense. However, their ability to reach low dew points is limited by the temperature at which frost will form on the heat exchanger tubing (greatly reducing heat transfer).

This leads to a discussion of air dew point. Dew point is the temperature at which moisture will condense out from the air due to its relative humidity increasing above 100%; see Chart LD-11. When this happens, the moisture condenses out and can be drained to a drain trap. Dew point is also important when considering air that has left the dryer, because if the air is ever exposed to temperatures below its dew point, moisture will form. Therefore, when applying air dryers, it is important to consider two features of compressed air usage that will impact dryer selection.

- When air is compressed, the dew point is increased. Also, the dew point under pressurized conditions must be known. For example, even though a -40°F dew point is achieved at atmospheric conditions, this becomes a dew point of about 10°F once the air has been compressed to 100 psig. In outdoor systems, when the temperature drops below 10°F, condensing and freezing of that moisture will result.
- 2. When compressed air is expanded through instruments or air tools, its volume increases, pressure decreases and a temperature drop is usually experienced. If the temperature drops below the dew point of the air, undesirable moisture forms in the equipment. The air would never be subjected to that temperature under any conditions other than when expanding.

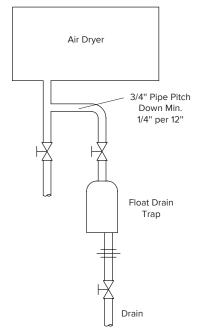


Figure LD-26.Drain trap installation with dirt leg for purging the dirt.

Chart LD-10. Recommendation Chart (See chart on page LD-6 for "Feature Code" references.)					
Equipment Being Drained 1st Choice and Feature Code Alternate Choice					
Dryers	FF B, C, J, N	IB FP			

How to Drain Dryers



Drain traps are usually required on refrigerated type dryers only. Here the refrigerant chills air and creates moisture that the drain trap can discharge. In the case of the dessicant type air dryer, the chemical grabs the moisture and bonds chemically with the water molecules, and no liquid accumulates. These bonded water molecules are then usually driven off in a regeneration cycle the dryer must periodically undergo.

Trap Selection and Safety Factor

In most cases, the dryer manufacturer will rate the dryer for a given moisture removal rate. The safety factor should still be applied to this load, however. If the manufacturer's ratings are not known, then it's necessary to calculate the moisture content of the air at aftercooler conditions and the moisture content at ambient conditions. Using the lower moisture content between these two, compare that figure to the moisture content at the dew point of the air leaving the dryer. The difference in these moisture contents is then multiplied by the airflow through the dryer to determine the moisture load. The safety factor applied to the load is 2:1 since liquid should be drained immediately from the dryer and the liquid tends to flow into the drain trap in slugs.

Installation

The dryer should come with a drain port of a given pipe size sufficient to handle the liquid coming out of the dryer. In this pipe size, a drain leg should be piped up 6" below the dryer with another 6" below that as a dirt pocket. Teeing off this line and into the trap with the same inlet size as the trap will allow for gravity drainage into the trap. Again, the ABCs of trap installation should be followed:

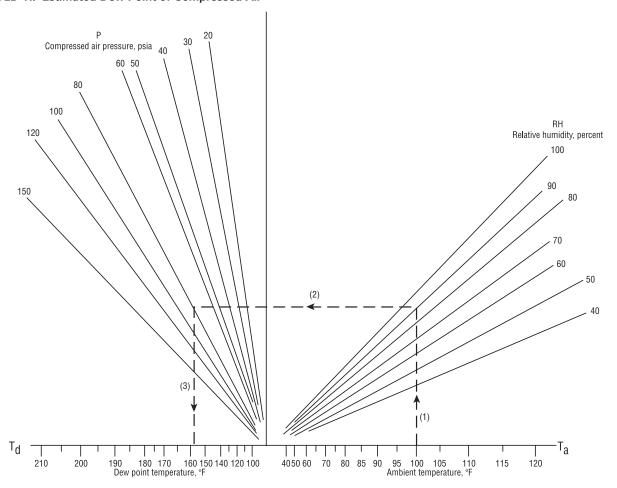
Accessible.

Below the point being drained.

Close to the drain leg as possible.

If the trap is too close to the floor to allow the use of a ball float trap, an inverted bucket trap should be considered. For additional installation recommendations, see pages LD-50 to LD-52.

Chart LD-11. Estimated Dew Point of Compressed Air



Nomograph estimates dew point of compressed air.



Armstrong How to Select and Size Armstrong Drain Traps

For Draining Liquids From Gases Under Pressure

Armstrong liquid drain traps are offered in a wide variety of sizes and types to meet the most specific requirements. The most widely used models and sizes utilize bodies, caps and some operating parts that are mass produced for Armstrong steam traps. The proven capabilities of these components, along with volume production economies, enable us to offer you exceptionally high quality at attractive prices. You can choose the smallest and least costly model that will meet your requirements with confidence.

Selection Procedure for Draining Liquid From Gas

- Multiply the actual peak liquid load (lbs/hr) by a safety factor of at least 1-1/2 or 2. See paragraph headed "Safety Factors."
- From Orifice Capacity Chart LD-12, find the orifice size that will deliver the required cold water capacity at the maximum operating pressure. If a light liquid is to be drained, convert light liquid capacity in lbs per hour to water capacity using factors in Table LD-5. Then find orifice size from Chart LD-12.
- From the Orifice Size Operating Pressure tables on the product model pages, find the drain trap(s) capable of opening the required orifice size at a specific pressure (and specific gravity if other than cold water—specific gravity 1.0).

NOTE: If specific gravity falls between those shown in the tables, use next lower. Example: If specific gravity is 0.73, use 0.70 gravity data.

Safety Factors

Safety factor is the ratio between actual continuous discharge capacity of the drain trap and the amount of liquid to be discharged during any given period. Chart LD-12 shows the maximum continuous rate of cold water discharge of the drain trap. However, you must provide capacity for peak loads and, possibly, lower-than-normal pressures. A safety factor of 1-1/2 or 2 is generally adequate if applied to the peak load and the minimum pressure at which it occurs. If the load discharge to the trap is sporadic, a higher safety factor may be required. Contact your Armstrong Representative for details.

Selection Examples

EXAMPLE No. 1: Find a drain trap to drain 1 000 lbs of water per hour from air at 500 psig pressure differential.

Multiply 1 000 lbs/hr by 2 (if not already done) to provide a safety factor; thus, a 2 000 lbs/hr continuous discharge capacity is required. In Capacity Chart LD-12, the 2 000 lb capacity line intersects the 500 psig pressure line directly below the No. 38 drill orifice curve. This orifice is available in the No. 1-LD or No. 11-LD drain trap, but for much lower pressures. Moving to the 32-LD, a #38 orifice is good to 489 psig. This is the trap/orifice combination to use.

Table LD-14, page LD-37, shows the No. 32-LD drain trap with #38 orifice will operate at pressures up to 489 psig and, therefore, is suitable for the job. Further checking shows the No. 2313 HLS drain trap with a 7/64" orifice could also handle the job, but it is designed particularly for low gravity liquids and is more costly than the No. 32-LD, so the No. 32-LD is a better choice.

EXAMPLE No. 2: Find a drain trap to drain 6 400 lbs/hr (safety factor included) of .80 specific gravity liquid from gas at 400 psig pressure differential.

Since Capacity Chart LD-12 is based on water capacity, the known light liquid capacity requirement must be converted to its equivalent water capacity with the factor given in Table LD-5: $6\,400\,x\,1.12=7\,168=$ water capacity required for using Chart LD-12.

Chart LD-12 shows that 7 168 lbs/hr and 400 psig calls for a 7/32" orifice. Entering the .80 specific gravity column of Table LD-14, page LD-37, shows that a No. 36-LD forged steel drain trap will open a 7/32" orifice at pressures up to 707 psig. As a matter of fact, this drain trap will open a 1/4" orifice at 501 psig and would be the one to use.

NOTE: While drain traps are sized on the basis of pressure differential, steel must be used whenever gauge pressure in the drain trap exceeds 250 psig.

Where Not to Use

Float type drain traps are not recommended where heavy oil, sludge or considerable dirt are encountered in lines. Dirt can prevent the valve from seating tightly, and cold oil can prevent float traps from opening. Where these conditions exist, Armstrong inverted bucket BVSW traps should be used.

How to Order Drain Traps

Specify:

- · Drain trap size by number
- Orifice size
- · Pipe connections—size and type
- Maximum operating pressure

If the correct drain trap cannot be determined, tell us capacity required, maximum pressure, and SPECIFIC GRAVITY of liquid.

Table LD-5. Conversion Factors to Find Cold Water Capacity Equivalents for Light Liquids

Specific Gravity	Multiply Light Liquid Capacity in Pounds Per Hour by:
.95	1.03
.90	1.06
.85	1.09
.80	1.12
.75	1.16
.70	1.20
.65	1.24
.60	1.29
.55	1.35
.50	1.42
.45	1.49
.40	1.58

How to Select and Size Armstrong Drain Traps



For Draining Water From a Light Liquid

Armstrong dual gravity drain traps for draining water from a light liquid are described on pages LD-47 and LD-48. All models shown are identical to corresponding models of traps used to drain liquid from a gas except that float weights are modified to make them suitable for draining water from a light liquid.

Dual gravity drain trap* selection requires that you know the peak heavy liquid load, maximum operating pressure, and specific gravity of the light liquid. With this information you can determine the orifice size required from Chart LD-12 and find the specific drain trap that will meet your conditions from the pressure tables on the dual gravity pages.

Selection Procedure for Draining Water from a Light Liquid

- Assume a required safety factor of 2:1. Multiply the peak load in pounds per hour by 2. (See paragraph on "Safety Factors.")
- From Capacity Chart LD-12, find the intersection of actual load times safety factor and the minimum operating pressure differential.
 Follow the pressure line immediately above this point to intersect the next higher orifice capacity curve. Then follow this curve downward and to the left to get the orifice size.
- Inspect the tables on pages LD-47 and LD-48 to find the smallest trap that can open the predetermined orifice size at the maximum operating pressure differential. Do not oversize dual gravity drain traps. Oversizing will cause excessive fluctuation of the interface between the two liquids.

NOTE: While drain traps are sized on the basis of operating pressure differential, forged steel must be used when total pressure in the drain trap exceeds 250 psig.

How to Order Dual Gravity Drain Traps

Specify:

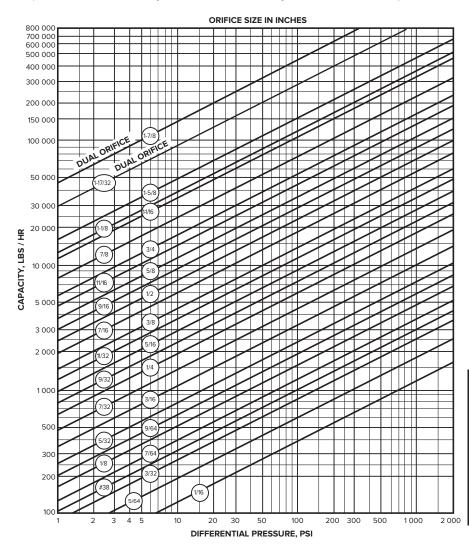
- Drain trap size by number
- Orifice size
- Pipe connections—size and type
- · Specific gravity of light liquid
- Weight of water discharge per hour
- · Maximum operating pressure

If you are not sure of the drain trap size to use, then specify:

- Specific gravity of light liquid
- Capacity in pounds of water per hour with safety factor included
- Working pressure—maximum and minimum

Chart LD-12. Calculated Cold Water Capacity of Armstrong Drain Trap Orifices at Various Pressures

Actual capacity also depends on trap configuration, piping and flow to trap. It is important to allow for safety factors and fluid density variations due to temperature.



^{*} Floats for dual gravity drain traps are weighted with quenching oil which, in the unlikely possibility of float failure, may be dispersed through the system. If this is a hazard, consult the Armstrong Application Engineering Department.





1-LDC—A See-Thru Body So You'll Know When It's Working

Benefits You Can See



Stainless steel internals mean corrosion resistance and reduced maintenance.

Efficient operation

Simple ball float mechanism discharges only when liquid is present so it doesn't waste air.

Positive seating

Free-floating valve mechanism assures positive seating so it prevents air loss. There are no fixed pivots to wear or create friction, and wear points are heavily reinforced for long life.

In-line repairability

In-line connections and an O-ring seal make for quick, easy repairs without dismantling piping. Just unscrew and remove the body for maintenance.

Reduced need for cleaning

Recessed dirt pocket gives dirt a place to accumulate away from the valve seat. Valve seat is 1-1/4" above the dirt pocket. Compared to other ball float drain traps, the Armstrong 1-LDC reduces dirt fouling and needs less frequent cleaning.

An inside look

See-thru body means you can observe changing conditions as they occur. See a problem in the making—instead of having to deal with it after the fact.

Corrosion resistance

Long-lasting polysulfone body and reinforced nylon cap weigh less than 20% of cast iron liquid drain traps. Rugged polysulfone resists corrosion and provides long, trouble-free service life.

Simplified installation

Optional horizontal or vertical inlet with horizontal outlet eliminates the need for extra fittings. Makes installation in existing systems easier. Vertical inlet is 3/4" to accommodate air venting. Requires no electricity.

NOTE: The Armstrong 1-LDC is not recommended for extremely dirty systems or those with heavy oil carryover. The drain trap should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.

1-LDC—A See-Thru Body So You'll Know When It's Working



Now, you can literally see what you've been missing—the early warning signs of a drain trap or system problem. Since you'll know the operating condition of a drain trap, you won't waste time and money scheduling maintenance that isn't needed. In other words, you will be able to react to a condition before it becomes a problem.

A simple ball float mechanism requiring no electricity to operate, the new Armstrong 1-LDC discharges automatically only when liquid is present. That means no air loss as with timed devices, which open even when liquid is not present.

Moisture in a compressed air system causes a variety of problems— everything from dirt fouling and potential corrosion to water hammer. Getting the water out—automatically, reliably—builds greater efficiency into your system. In short, pay attention to your compressed air system, and you'll probably pay less to compress air.

Compare...and Save the Difference

Seeing really is believing—especially when you compare the Armstrong see-thru drain trap with cast iron units. Measure the differences in the time and money you can save with a more efficient, easier-to-maintain compressed air system. For more information or technical assistance, contact your local Armstrong Representative.







1-LDC See-Thru Liquid Drainer

For Loads to 1 500 lb/hr (690 kg/hr)...Pressures to 150 psig (10 barg)

Now, you can literally see what you've been missing—the early warning signs of a drain trap or system problem. Since you'll know the operating condition of a drain trap, you won't waste time and money scheduling maintenance that isn't needed. In other words, you'll be able to react to a condition before it becomes a problem.

A free floating mechanism needs no electricity to operate, the 1-LDC discharges automatically only when liquid is present. That means no air loss as with timed devices that open even when liquid is not present. Moisture in a compressed air system causes problems. Getting the water out—automatically, reliably—builds greater efficiency into your system.

List of Materials

Table LD-6.	
Name of Part	Material
Cap and Fitting	Reinforced Nylon*
Body	Polysulfone
O-Rings (Cap, Body and Fitting)	Nitrile Elastomer Compound
Float, Lever and Screws	Stainless Steel
Valve & Seat	Stalliless Steel
Retainer Ring	Zinc-Plated Steel

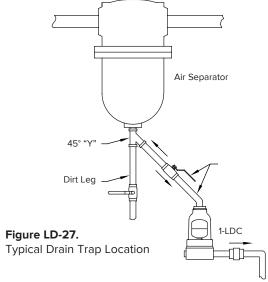
^{*}UV sensitive

Maximum Operation Pressures and Capacities

Table LD-7.									
Specific 1.0						0.9	95		
Orifice Size	Oper	Operating Capacity Ope		Capacity Operat		ating	Capacity		
	psig	barg	lb/hr	kg/hr	psig	barg	lb/hr	kg/hr	
1/8	121	8.3	1500	690	109	7.6	1400	640	
#38	150	10.0	1100	510	150	10.0	1100	490	

Capacities given are continuous discharge capacities in lb/hr or kg/hr of liquid at pressure differential indicated.

For a fully detailed certified drawing, contact Armstrong.

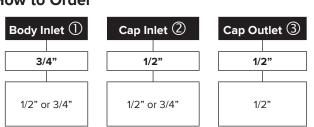


Drain traps dispose of water that collects in many places in a compressed air system. Each drain trap arrangement must be considered individually.

Physical Data

Table LD-8.		
Inlet Connections	in	mm
inlet Connections	1/2, 3/4	15, 20
Outlet Connection	1/2	15
Alternate Inlet or Vent Connection	1/2, 3/4	15, 20
"A"	3-1/2	89
"B"	6-7/8	175
"C"	6-3/32	155
Weight lbs (kg)	1 (0.45)
Maximum Allowable Pressure (Vessel Design)	150 psig @ 150°	F (10 barg @ 65°C)
Maximum Operating Pressure psig (barg)	15	0 (10)

How to Order



Body Inlet 1
Vent when alternate inlet is used.

Cap Inlet 2

1-LDCW See-Thru Air Liquid Drainer for Ozone Applications

For Pressures to 150 psig (10 barg) or Specific Gravity 1.0



What Is Ozone?

Ozone is a gas that forms naturally during thunderstorms when lightning converts normal oxygen molecules (O^2) into ozone (O^3). The fresh, sweet smell in the air after a storm is the smell of ozone. The unstable ozone molecule reacts rapidly with most substances and is an extremely strong natural oxidant.

How Is Commercial Ozone Produced?

Ozone can be formed by exposing air to ultraviolet light; however, the most common method of generating ozone is by passing air through an electrical discharge. Because ozone has strong oxidizing properties, its production requires corrosion-resistant equipment.

How Is Ozone Used in Water Filtration and Purification?

Because ozone is such an effective oxidant, it kills viruses, bacteria, mold, mildew, fungus and germs. Passing ozone through water achieves high purification rates without any chemical residue. Oxygen is the only by-product.

Typical Customer Applications:

- Purifying standing ground water in Third World countries.
- Conditioning water for poultry and livestock.
- · Purifying water in the bottled water industry.
- · Filtering and purifying water for process applications.

A See-Thru Body Shows You It's Working

Now, you can literally see what you've been missing. The Armstrong 1-LDCW See-Thru Liquid Drainer lets you easily check its operating condition. You won't have to waste time and money scheduling maintenance that isn't needed, and you can quickly react to a condition before it becomes a problem.

Efficient Operation

Simple ball-float mechanism doesn't need electricity to operate. The liquid drainer automatically discharges liquid when it is present. No air or gas is lost, as with manual draining.

Positive Seating

Free-floating valve mechanism ensures positive seating and prevents liquid loss. There are no fixed pivots to wear or create friction. Wear points are heavily reinforced for long life.

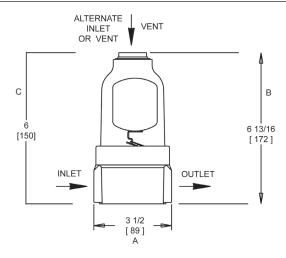
Corrosion Resistance

Long-lasting CPVC cap and polysulfone body provides trouble-free operation. T316 stainless steel internal parts resist corrosion and reduce maintenance.

Compare-and Save the Difference

Seeing really is believing—especially when you compare the Armstrong 1-LDCW See-Thru Air Liquid Drainer with manual drainage. Measure the time and money you can save with a more efficient, easier-to-maintain system. For more information or technical assistance, contact your local Armstrong Representative.

NOTE: The Armstrong 1-LDCW should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.



1-LDCW

List of Materials	
Name of Part	Material
Cap	CPVC
Body	Polysulfone
O-Rings (Body Cap and Fitting)	Aflas
Float Lever and Screws	T316 Stainless Steel
Valve & Seat	T316 Stainless Steel
Fitting	CPVC
Retainer Ring	Zinc Plated Steel

Physical Data			
	in	mm	
Inlet Connection (In Body)	3/4	20	
Inlet Connection (Alternate)	1/2	15	
Outlet Connection	1/2	15	
"A" Face-to-Face	3-1/2	89	
"B" Height	6-13/16	172	
"C" Bottom to C	6	152	
Maximum Allowable Pressure (Vessel Design)	150 psig (10 barg	-	
Maximum Operating Pressure	150 psig (10 barg)		
Specific Gravity Range	1.00 to 0.80		
Weight, lb (kg)	1 (.5)	



Inverted Bucket Drain Traps (BVSW Model)

For Loads to 7 000 lb/hr (3 175 kg/hr)...Pressures to 650 psig (45 barg)

Armstrong inverted bucket drain traps are designed for systems where heavy oil and dirt may be encountered. The enlarged bucket vent equipped with a scrub wire (BVSW) keeps the drain trap operating under dirty conditions.

List of Materials

Table LD-9.						
BVSW Model No.	Body & Cap	Valve & Seat	Bucket & Leverage System	Gasket		
800, 811, 812, 813, 880, 881, 882, 883, 211, 212, 213	Cast Iron ASTM A48 Class 30					
312, 313	Forged Steel ASTM A105	I Stainless Steel I '		Stainless Steel 1 '		Compressed Asbestos-free
981, 983	Cast Steel ASTM A216 Grade WCB					



Physical Data

Model No. Orifice Size		800 BVSW 880 BVSW		811 BVSW 881 BVSW 211 BVSW		812 BVSW 882 BVSW 212 BVSW		VSW*	813 BVSW 883 BVSW 883 BVSW 213 BVSW 313 BVSW* 983 BVSW*		981 B	VSW*
in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1/4	_	_	_	_	_	_	_	_	125	8.5	_	_
7/32	_	_	_	_	_	_	_	_	180	12.5	_	_
3/16	_	_	_	_	_	_	_	_	250	17	50	3.5
5/32	_	_	_	_	125	8.5	_	_	450	31	85	6
1/8	80	5.5	125	8.5	200	14	_	_	600	41	170	11
7/64	125	8.5	200	14	250	17	600	41	_	_	250	17
#38	150	10.5	250	17	_	_	_	_	_	_	330	22.

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

^{*} Use steel traps for pressures above 250 psig (17 barg).

Table LD-11. Armstrong 800 Series Drain Traps									
Model No.	800 8	BVSW	811 E	BVSW	812 BVSW		813	BVSW	
Din a Compostions	in	mm	in	mm	in	mm	in	mm	
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1	20, 25	
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20	
"A"	3-3/4	95	3-3/4	95	5-5/8	143	7	178	
"B"	5-7/16	138	6-7/8	175	9-1/16	230	11-3/4	298	
"C"	5	127	5	127	6-1/2	165	7-3/4	197	
"D"	2-3/4	70	4-1/4	108	5-3/8	137	7-1/32	179	
Number of Bolts	(6	(6	(5	6		
Weight lbs (kg)	5 (2	2.3)	6 (2.7)	15 (6.8)	27-1/2 (13)		
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)								
Max. Operating Pressure psig (barg)	150	(10.5)			250 (17)			

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.



Inverted Bucket Drain Traps (BVSW Model)

Armstrong

For Loads to 7 000 lb/hr (3 175 kg/hr)...Pressures to 650 psig (45 barg)

Physical Data

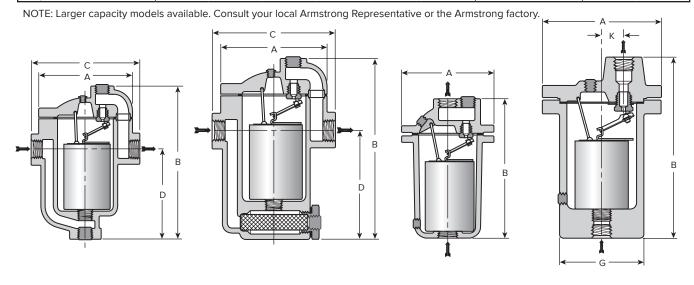
Figure LD-29.

Series 800

Table LD-12. Armstrong 880-	980 Seri	es Drai	in Traps Wi	th Integral	Strainer	s (See p	pages LD-29	and LD-30) for capa	acity.)			
Model No.	Cast Iron								Cast Steel				
	880 BVSW		881 BVSW		882 BVSW		883 BVSW		981 BVSW		983 BVSW		
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1, 1-1/4	20, 25, 32	1/2, 3/4	15, 20	3/4, 1	20, 25	
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20	1/2	15	3/4	20	
"A"	3-3/4	95	3-3/4	95	5-5/8	143	7	178	4-1/2	114	7-1/4	184	
"B"	6-1/16	154	7-1/16	179	9-3/8	244	12-3/8	314	8-5/8	219	12-15/32	313	
"C"	5	127	5	127	6-1/2	165	7-7/8	200	5-3/8	137	7-3/4	197	
"D"	3-7/16	87.3	4-7/16	113	5-3/4	146	7-3/8	187	4-13/16	122	7-9/16	192	
Number of Bolts	6		6		6		6		6		6		
Weight lbs (kg)	5-1/2	-1/2 (2.5) 6 (2.7)		2.7)	15-1/2 (7)		31 (14)		11-1/2 (5)		43 (20)		
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)							600 psig @ 650°F (41 barg @ 343°C)					
Max. Oper. Pressure psig (barg)	150 (10.5)				250	250 (17)				330 (22.5)		600 (41)	

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

Table LD-13. Armstrong 200-300 Series Drain Traps (See pages LD-29 and LD-30 for capacity.)												
Model No.	Cast Iron							Forged Steel				
	211 BVSW		212 BVSW		213 BVSW		312 BVSW		313 BVSW			
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm		
	1/2	15	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25		
Test Plug	1/8	3	3/8	10	1/2	15	_	_	_	_		
"A"	4-1/4	108	5-1/4	133	6-3/8	162	6-3/4	171	8	203		
"B"	6-3/8	162	8-3/4	222	10-3/4	273	10-3/16	259	11-1/2	292		
"G"	_	_	_	_	_	_	4-3/4	121	5-1/8	130		
"K" (C Outlet to C Inlet)	_	_	_	_	_	_	1-1/4	31.7	1-7/16	36.5		
Number of Bolts	6		8	8	6		6		8			
Weight lbs (kg)	6 (2.7)		11-1/2 (5.2)		20-1/4 (9.2)		30 (14)		50 (23)			
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)						600 psig @ 650°F (41 barg @ 343°C)		1 080 psig @ 650°F (75 barg @ 343°C)			
Max. Oper. Pressure psig (barg)	250 (17)						600	(41)	650 (45)			



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Figure LD-31.

Series 200

Figure LD-30.

Series 880 & 980

Figure LD-32.

Series 300



For Loads to 50 000 lb/hr (22 679 kg/hr)...Pressures to 1 000 psig (69 barg)

Table LD-14. Maxin LD-30.)	num Operati	ng Pres	sures f	or Hand	lling Di	fferent	Specif	ic Grav	ity Liqu	ids Wit	h Orific	es Ava	ilable ii	n Guide	d Free	Floatin	g Leve	r Drain	Traps. ((See pa	iges LD	-29 and	d
	Sp. Grav	1.0	00	.9	5	.9	0	3.	35		80		75		0	.6	5	.6	60	.5	55	.5	50
Model No.	Orifice in	psig	barg	psig	barg	psig	barg	psig	barg	Maxim psig	um Op barg	erating psig	Pressu barg	re psig	(barg) barg	psig	barg	psig	barg	psig	barg	psig	barg
	1/8	121	8.3	109	7.6	98	6.8	87	6.0	75	5.2	64	4.4	52	3.6	41	2.8	29	2.0	18	1.2	6	0.4
1-LD	7/64	143	9.9	130	9.0	116	8.0	103	7.1	89	6.1	75	5.2	62	4.3	48	3.3	35	2.4	21	1.4	7	0.5
1 25	#38	182	12.5	164	11	147	10.2	130	9.0	113	7.8	95	6.6	78	5.4	61	4.2	44	3.0	26	1.8	9	0.6
	5/64 1/8	300 176	20.7 12.1	289 161	19.9 11.1	259 146	17.8 10.1	228 130	15.7 9.0	198 115	13.7 7.9	168 100	11.6 6.9	137 85	9.5 5.8	107 69	7.4 4.8	77 54	5.3 3.7	47 39	3.2 2.7	16 24	1.1
44.1.0	7/64	209	14	191	13	173	12	155	10.7	137	9.4	119	8.2	100	6.9	82	5.7	64	4.4	46	3.2	28	1.9
11-LD	#38	264	18	242	17	219	15	196	14	173	12	150	10.4	127	8.8	104	7.2	81	5.6	59	4.0	36	2.5
	5/64 5/16	400	28 1.5	400 20	28 1.4	384 18	27 1.3	344 17	24 1.1	304 15	1.0	264 13	0.9	224	15 0.8	183 10	13 0.7	143	9.9	103	7.1 0.4	63	0.3
	1/4	36	2.5	33	2.3	30	2.1	27	1.9	24	1.7	22	1.5	19	1.3	16	1.1	13	0.5	10	0.4	7	0.5
2-LD to 250 psig	3/16	79	5.5	73	5.0	67	4.6	60	4.2	54	3.7	47	3.3	41	2.8	35	2.4	28	2.0	22	1.5	16	1.1
(17 barg)	5/32	137	9.4	126	8.7	115	7.9	104	7.2	93	6.4	82	5.6	71	4.9	60	4.1	49	3.4	38	2.6	27	1.8
22-LD to 533 psig	1/8	234	16.1	215	14.8	196	13.5	178	12.2	159	10.9	140	9.6	121	8.4	102	7.1	83	5.8	65	4.5	46	3.2
(37 barg)	7/64 #38	299 372	20.6 25.7	275 342	19 23.6	251 313	17.3 21.6	227 283	15.7 19.5	203 253	14 17.4	179 223	12 15	155 193	10.7 13	131 163	9.0 11.2	107	7.4 9.2	83 103	5.7 7.1	59 73	4.0 5.0
	5/64	533	37	475	33	461	32	417	29	372	26	328	23	284	20	240	17	196	14	152	10.5	108	7.4
	5/16	29	2.0	26	1.8	23	1.6	21	1.4	18	1.2	15	1.0	12	0.9	10	0.7	7	0.5	4	0.3	2	0.1
	1/4	47	3.3	43	3.0	38	2.6	34	2.3	29	2.0	25	1.7	20	1.4	16	1.1	12	0.8	7	0.5	3	0.2
	3/16 5/32	104 180	7.2 12	94 163	6.5 11	85 146	5.8 10	75 129	5.2 8.9	65 112	4.5 7.7	55 95	3.8 6.5	45 78	3.1 5.4	35 61	2.4 4.2	25 44	1.8 3.0	16 27	1.1 1.9	6 10	0.4
32-LD	1/8	307	21	278	19	249	17	220	15	191	13	162	11	133	9	104	7.2	75	5.2	46	3.2	17	1.2
	7/64	393	27	356	25	319	22	282	19	245	17	207	14	170	12	133	9	96	6.6	59	4.1	22	1.5
	#38	489	34	443	31	397	27	351	24	304	21	258	18	212	15	166	11	120	8	73	5.1	27	1.9
3-LD to 250 psig	5/64 1/2	600 16	41 1.1	600 14	1.0	585 13	40 0.9	517 12	36 0.8	449 10	31 0.7	381 9	26 0.6	313 7	0.5	244 6	17 0.4	176 5	0.3	108 3	7 0.2	40	2.8 0.1
(17 barg)	3/8	33	2.3	31	2.1	28	1.9	25	1.7	22	1.5	19	1.3	16	1.1	13	0.9	10	0.7	7	0.5	4	0.3
(Cast Iron)	5/16	54	3.7	49	3.4	44	3.0	39	2.7	35	2.4	30	2.1	25	1.7	20	1.4	16	1.1	11	0.8	6	0.4
13-LD to 570 psig	9/32	71	4.9	65	4.5	59	4.0	52	3.6	46	3.2	40	2.7	34	2.3	27	1.9	21	1.4	15	1.0	8	0.6
(39 barg)	1/4 7/32	107 153	7.4 10.5	97 139	6.7 9.6	88 126	6.1 8.7	79 112	5.4 7.7	69 99	4.8 6.8	60 85	4.1 5.9	50 72	3.5 5.0	41 59	2.8 4.0	32 45	2.2 3.1	22 32	1.5 2.2	13 18	0.9
(Stainless)	3/16	230	16	209	14	189	13	169	12	149	10.3	129	8.9	108	7.5	88	6.1	68	4.7	48	3.3	27	1.9
33-LD to 900 psig	5/32	359	25	327	23	296	20	264	18	233	16	201	14	169	12	138	9.5	106	7.3	74	5.1	43	2.9
(62 barg)	1/8	726	50	662	46	598	41	534	37	470	32	406	28	342	24	278	19	214	15	150	10.3	86	5.9
(Steel)	7/64 1-1/16	900	62 1.4	847 19	58 1.3	765 18	53 1.2	683 16	47 1.1	601 15	1.0	519 13	36 0.9	437 12	30 0.8	356 10	25 0.7	274 9	19 0.6	192 7	13 0.5	110	7.6
	7/8	32	2.2	30	2.1	28	1.9	26	1.8	23	1.6	21	1.4	19	1.3	16	1.1	14	1.0	12	0.8	9	0.6
	3/4	47	3.2	44	3.0	40	2.8	37	2.5	34	2.3	30	2.1	27	1.9	24	1.6	20	1.4	17	1.2	14	0.9
	5/8	72	4.9	67	4.6	61	4.2	56	3.9	51	3.5	46	3.2	41	2.8	36	2.5	31	2.1	26	1.8	21	1.4
	9/16 1/2	95 138	6.5 9.5	88 128	6.1 8.8	81 118	5.6 8.1	75 108	5.2 7.5	68 99	4.7 6.8	61 89	4.2 6.1	55 79	3.8 5.4	48 69	3.3 4.8	41 59	2.8 4.1	34 50	2.4 3.4	28 40	1.9 2.8
6-LD	7/16	196	13	182	13	168	12	154	11	140	10	126	8.7	112	7.7	98	6.8	85	5.8	71	4.9	57	3.9
Cast Iron	3/8	250	17	250	17	250	17	243	17	221	15	199	14	177	12	155	11	133	9.0	111	7.7	90	6.2
	11/32 5/16	250 250	17 17	250 250	17 17	250 250	17 17	250 250	17 17	250 250	17 17	250 250	17 17	236 250	16 17	207 250	14 17	178 228	12	148 191	10 13	119 153	8.2 11
	9/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	16 17	250	17	201	14
	1/4	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
	7/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
	3/16	250	17	250	1.01	250	17 0.91	250	17 0.81	250	17 0.71	250	0.6	250 7	17 0.5	250	17 0.4	250	17	250	17	250	17 0.1
	1-1/16 7/8	16 25	1.7	15 23	1.6	13 21	1.4	12 18	1.3	10 16	1.1	9	0.95	11	0.5	6 9	0.4	7	0.3	3 5	0.2	1 2	0.16
	3/4	36	2.5	33	2.3	30	2.1	27	1.8	23	1.6	20	1.4	17	1.1	13	0.91	10	0.68	7	0.45	3	0.22
	5/8	56	3.9	51	3.5	46	3.1	41	2.8	35	2.4	30	2.1	25	1.7	20	1.4	15	1.05	10	0.69	5	0.34
	9/16	74 107	5.1 7.4	67	4.6 6.7	60 88	4.2 6.0	54 78	3.7	47 68	3.2	40 58	2.8	34	2.3	27	1.8	20	1.4	13	0.92	7 10	0.46
36-LD	1/2 7/16	107 152	7.4 10.5	97 138	6.7 9.6	88 125	6.0 8.6	78 111	5.4 7.6	68 97	4.7 6.7	58 83	4.0 5.7	49 69	3.4 4.8	39 55	2.7 3.8	29 41	2.0	19 27	1.3	14	0.66
Forged Steel	3/8	240	17	218	15	197	14	175	12	153	10.5	131	9.0	109	7.5	87	6.0	65	4.5	43	3.0	21	1.5
-	11/32	320	22	291	20	262	18	233	16	203	14	174	12	145	10	116	8.0	87	6.0	58	4.0	29	2.0
	5/16	411	28	374	26	336	23	299	21	262	18	224	15	187	13	149	10.3	112	7.7	74	5.1	37	2.5
	9/32 1/4	539 788	37 54	490 716	34 49	441 644	30 44	392 573	27 39	343 501	24 35	293 429	20 30	244 357	17 25	195 286	13 20	146 214	10.1 15	97 142	6.7 9.8	48 70	3.3 4.9
	7/32	1000	69	1 000	69	910	63	808	56	707	49	606	42	505	35	403	28	302	21	201	9.8	99	6.9
	3/16	1000	69	1000	69	1000		1000	l	1000		992	68	826	57	660	46	494	34	328	23	163	11.2
Specific Gra	avity	1.0	00	.9	5	.9	0	3.	35	3.	80	.7	75	.7	0	.6	5	.6	0	.5	55	.5	50

NOTE: If specific gravity falls between those shown in the chart, use the next lower gravity. For example, if specific gravity is 0.73, use 0.70 gravity data.

High Temperature Service

Maximum allowable working pressures of floats decrease at temperatures above 100°F (37.8°C). Allow for approximately:

- 10% decrease at 200°F (93.3°C)
- 15% decrease at 300°F (148.9°C)
- 20% decrease at 400°F (204.4°C)

The float is not always the limiting factor, however. Consult with Armstrong Application Engineering if you have a high-temperature application that also requires maximum operating pressures.

For Loads to 49 000 lb/hr (22 226 kg/hr)...Pressures to 300 psig (21 barg)



Armstrong's cast iron, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

List of Materials

Table LI	Table LD-15.											
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket							
1-LD				Cook Iron ACTM	Compressed							
2-LD 3-LD	Sta	inless Steel		Cast Iron ASTM A48 Class 30	Asbestos-							
6-LD					free							

For information on special materials, consult the Armstrong Application Engineering Department.

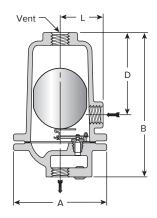


Figure LD-33.

No. 2-LD, 3-LD and 6-LD cast iron guided lever drain traps. No. 1-LD has standard top inlet and optional side connection. The hemispherical valve, seat and leverage of the 1-LD, 2-LD, 3-LD and 6-LD cast iron traps are identical in design, materials and workmanship to those for saturated steam service up to 300 psig (21 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

For a fully detailed certified drawing, refer to:

1-LD CD #1070 2-LD, 3-LD, 6-LD CD #1034



Physical Data

Mardal Na	Cast Iron											
Model No.	1-	LD	2-	LD	3-	LD	6-LD					
Dina Cannastiana	in	mm	in	mm	in	mm	in	mm				
Pipe Connections	1/2*	15*	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50				
"A"	3-3/4	95	5-1/4	133	6-3/8	162	10-3/16	259				
"B"	5-1/2	140	8-3/4	222	11-1/2	292	18	457				
"D"	2-7/8	73	5-1/8	130	7	188	9-3/8	238				
"K" (C Outlet to C Inlet)	13/16	21	_	_	_	_	_	_				
"L"	1-7/8	48	2-7/16	62	2-7/8	73	4-5/8	117				
Approx. Wt. lb (kg)	4	(2)	12 (5.5)	21 (9.5)	78 (35.5)					
Max. Allow. Pressure (Vessel Design)		@ 200°F† @ 93°C)	250 DSIG (a) 450°F (17 Darg (a) 232°C)									

NOTE: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

*For pressures not exceeding 250 psig (17 barg), a maximum temperature of 450°F (232°C) is allowed.

*1/4" (6 mm) outlet.



For Loads to 9 500 lb/hr (4 309 kg/hr)...Pressures to 570 psig (39 barg)

Armstrong's stainless steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

List of Materials

Table Li	D-17.				
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
11-LD 22-LD 13-LD	Sta	inless Steel	k	Sealed Stainless Steel, 304L*	_

^{*11-}LD available in all-316SS. Consult factory.

For information on special materials, consult the Armstrong Application Engineering Department.

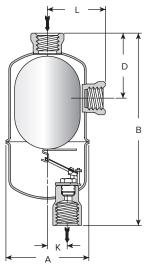


Figure LD-34.

No. 22-LD and 13-LD stainless steel guided lever liquid drain trap with sealed, tamperproof construction.

The hemispherical valve, seat and leverage of the 11-LD, 22-LD and 13-LD stainless steel traps are identical in design, materials and workmanship to those for saturated steam service up to 570 psig (39 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

For a fully detailed certified drawing, refer to list below:

11-LD CD #1066 13-LD and 22-LD CD #1086



Physical Data

Madal Na	Stainless Steel											
Model No.	11-I	_D**	22	-LD	13	-LD						
Pipe Connections	in	mm	in	mm	in	mm						
	3/4*	20*	3/4	20	1	25						
"A"	2-3/4	70	3-15/16	100	4-1/2	114						
"B"	7-1/4	184	8-13/16	224	11-3/8	289						
"D"	_	_	3	76	6-1/8	156						
"K"	9/16	14	7/8	22	1-3/16	30						
"L"	_	_	2-5/8	67	3-9/32	83						
Approx. Wt. lbs (kg)	1-3/4	(0.79)	3-1/4	1 (1.5)	7-1/2 (3.4)							
Max. Allowable Pressure (Vessel Design)		(35 barg @ 38°C) (30 barg @ 260°C)	1 5 -	= (41 barg @ 38°C) (33 barg @ 260°C)	570 psig @ 100°F (39 barg @ 38°C) 490 psig @ 500°F (34 barg @ 260°C							

Note: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

*1/2" (15 mm) outlet. **No side connection.



For Loads to 42 000 lb/hr (19 050 kg/hr)...Pressures to 1 000 psig (69 barg)



Armstrong's forged steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight. The hemispherical valve, seat and leverage of the 32-LD, 33-LD and 36-LD forged steel traps are identical in design, materials and workmanship to those for saturated steam service up to 1 000 psig (69 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

List of Materials

Table LD-21.											
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket						
32-LD 33-LD 36-LD	Sta	ainless Steel		Forged Steel ASTM A105	Compressed Asbestos- free						

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to CD #1035.

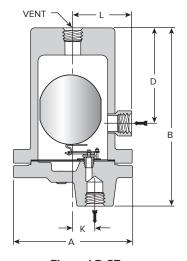


Figure LD-37.

No. 32-LD, 33-LD and 36-LD forged steel guided lever drain trap. Socketweld or flanged connections are also available.



Physical Data

Table LD-22. Armstro		Forged Steel											
Model No.	32	?-LD⁺	33	-LD⁺	36-	·LD†							
Diag Commentions	in	mm	in	mm	in	mm							
Pipe Connections	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50							
"A"	6-3/4	171	8	203	11-7/8	302							
"B"	10-3/16	259	11-9/16	294	17-1/8	435							
"D"	5-9/16	141	6-1/16	154	9	229							
"K"	1-1/4	32	1-7/16	37	2-1/8	54							
"L"	3-3/8	86	3-9/16	90	6-1/16	154							
Approx. Wt. lbs (kg)	31	(14)	49	(22)	163 (74)								
Max. Allowable Pressure (Vessel		F (41 barg @ 38°C) - (35 barg @ 400°C)		1 000 psig @ 100°F 600 psig @ 750°F	,								

Note: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

[†]Available in Type 316 stainless steel. Consult factory.



180 Series Free Floating Lever Drain Traps

All Stainless Steel for Horizontal Installation

For pressures to 400 psig (28 barg) . . . Capacities to 2 000 lb/hr (907 kg/hr)

Armstrong's stainless steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats as Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

The hemispherical valve, seat and leverage of the 180-LD and 181-LD stainless steel traps are identical in design, materials and workmanship to those for saturated steam service up to 570 psig (39 barg), except that the 180 Series traps have a guidepost to ensure a positive, leak-tight valve closing under all conditions. The 180 Series is designed for situations where mounting a drainer close to the floor is critical. A back vent connection is required.

For a fully detailed certified drawing, refer to list below: 180-LD CD #1276

List of Materials

Table LD-19.				
Model No.	Valve & Seat	Leverage System	Float	Body & Cap
180-LD 181-LD	S	tainless Steel		Sealed Stainless Steel 304L

Physical Data

Table LD-20. Armstrong 180 Se	ries Free Floa	iting Leve	r Drain Traps	;		
Model No.	180-L	.D	181-LD			
Dina Cannastiana	in	mm	in	mm		
Pipe Connections	1/2	15	3/4	20		
"A" (Diameter)	2-11/16	68	2-11/16	68		
"B" (Height)	6	152	7-1/4	184		
"C" (Face to Face)	4-5/16	110	4-5/16	110		
"D" (Bottom to C Inlet)	5-1/8	130	6-9/32	160		
"P"	1/2	15	3/4	20		
Weight, lb (kg)	1-3/4 (0).8)	2-3/8	(1.1)		
Max. Allowable Pressure (Vessel Design)	500 psig @ 100°F (35 barg @ 38°C) 440 psig @ 500°F (30 barg @ 260°C)					

 $\label{thm:continuous} \textbf{Note:} \ \ \text{Vessel design pressure may exceed float collapse pressure in some cases. Pipe size of vent is same as that of inlet and oulet connections.}$



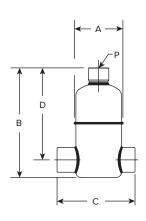


Figure LD-35. Model 180-LD

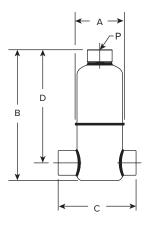
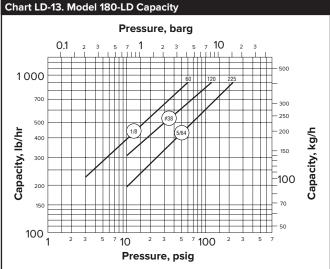
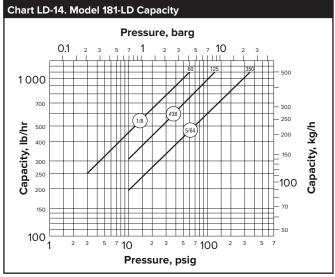


Figure LD-36. Model 181-LD





Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Notes	Armstrong





Fixed Pivot and Snap Action Drain Traps

For Loads to 3 900 lb/hr (1769 kg/hr)...Pressures to 1000 psig (69 barg)

Continuous Flow or On-Off Float Type Drain Traps

Armstrong's line of fixed lever and snap action drain traps includes two basic models available in cast iron and forged steel. The floats are light enough to handle light liquids.

No. 21—A small, high-quality, economical drain trap for use on drainage jobs where dirt and oil are not encountered. It employs a single lever with a fixed pivot.

No. 21-312—Forged steel version of the No. 21 with larger float and higher leverage.

No. 71-A—Wide open, tight-shut drain trap for use where fine dirt and grit may be present or where liquid load is light. A flat spring in the leverage system holds the valve closed until the trap body is nearly full of water. Then it snaps open, washing dirt through. When the trap body is nearly empty, the spring snaps the valve shut.

No. 71-315—Forged steel version of No. 71-A.

CAUTION: Ball float drain traps are not recommended where heavy oil, sludge or considerable dirt are encountered in lines. Under these circumstances use Armstrong inverted bucket BVSW traps.

		Sp. Grav.	1.0	00	.9	5	.9	0	3.	5	.8	0	.7	' 5	.7	0	.6	5	.6	0	.5	5	.5	50
М	odel No.	Orifice size (in)		Maximum Operating Pressure psig (barg) at 100°F (38°C)																				
		psig	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	bar
		1/4	22	1.5	20	1.4	18	1.3	16	1.1	15	1.0	13	0.9	11	0.8	10	0.7	8	0.5	6	0.4	4	0.3
		7/32	28	1.9	26	1.8	24	1.6	21	1.5	19	1.0	17	1.2	15	1.0	12	0.9	10	0.7	8	0.6	6	0.4
		3/16	38	2.6	35	2.4	32	2.2	29	2.0	26	1.8	23	1.6	20	1.4	17	1.2	14	1.0	11	0.7	8	0.5
		5/32	54	3.8	50	3.5	46	3.2	41	2.9	37	2.6	33	2.3	29	2.0	24	1.7	20	1.4	16	1.1	11	0.8
	21	9/64	67	4.6	62	4.2	56	3.9	51	3.5	46	3.1	40	2.8	35	2.4	30	2.1	24	1.7	19	1.3	14	1.0
		1/8	84	5.8	78	5.4	71	4.9	64	4.4	58	4.0	51	3.5	44	3.0	37	2.6	31	2.1	24	1.7	17	1.2
		3/32	148	10.2	136	9.4	124	8.6	112	7.7	101	6.9	89	6.1	77	5.3	66	4.5	54	3.7	42	2.9	30	2.1
		5/64	210	14	193	13	176	12	160	11	143	9.9	126	8.7	110	7.6	93	6.4	77	5.3	60	4.1	43	3.0
		1/16	250	17	250	17	250	17	245	17	220	15	194	13	168	12	143	9.9	117	8.1	92	6.3	66	4.6
	2.2/0	1/4	42	2.9	39	2.7	36	2.5	33	2.3	30	2.1	28	1.9	25	1.7	22	1.5	19	1.3	16	1.1	13	0.9
	3-3/8 oz (96 g)	7/32	54	3.8	51	3.5	47	3.2	43	3.0	40	2.7	36	2.5	32	2.2	28	2.0	25	1.7	21	1.5	17	1.2
	Float	3/16	74	5.1	69	4.7	64	4.4	59	4.0	54	3.7	49	3.4	44	3.0	39	2.7	34	2.3	28	2.0	23	1.6
*.		5/32	200	14	197	14	182	13	168	12	153	10.6	139	9.6	125	8.6	110	7.6	96	6.6	82	5.6	67	4.6
21-312*	4-1/2 oz	9/64	229	16	211	15	200	14	200	14	189	13	171	12	153	10.6	136	9.4	118	8.1	100	6.9	83	5.7
7	(128 g)	1/8	288	20	266	18	243	17	221	15	200	14	200	14	193	13	171	12	148	10.2	126	8.7	104	7.2
	Float	3/32	500	34	465	32	426	29	387	27	348	24	309	21	270	19	231	16	200	14	200	14	182	13
	6 oz	5/64	589	41	533	37	500	34	500	34	495	34	440	30	384	27	329	23	274	19	218	15	200	14
	(170 g) Float	1/16	600	41	600	41	600	41	600	41	563	39	500	34	500	34	500	34	420	29	335	23	250	17
		1/4	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	_	_	_	_	_	T -
71-	4 & 71-315	3/16	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	_	_	_	_	_	_
	**	1/8	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	_	_	_	_	_	_
		7/64	200	14	200	14	200	14	200	14	200	14	200	14	200	14	200	14	_	_	_	_	_	_
	71-A	5/64	250	17	250	17	250	17	250	17	_	_	_	_	_	_	_	_	_	_	_	_	_	-
		5/64	500	35	500	35	500	35	500	35	_	_	_	_	_	_	_	_	_	_	_	_	_	-
	71-315	1/16	1 000	69	1 000	69	1 000	69	1 000	69	_	_	_	_	_	_	_	_	_	_	_	_	_	_

NOTE: If actual specific gravity falls between those shown in above table, use next lower. For example, if actual gravity is 0.73, use 0.70 gravity data.

^{*5/32&}quot; orifice (and smaller) utilizes higher leverage mechanism designated 21-312V.

^{**}Use 6 1/4 oz. float for 0.85 - 1.0 S.G. Use 3 3/8 oz. float for 0.65 - 0.80 S.G.

Fixed Pivot and Snap Action Drain Traps

For Loads to 3 900 lb/hr (1769 kg/hr)...Pressures to 1 000 psig (69 barg)



Physical Data

Table LD-24. Arms	trong Fixed I	Lever and Sn	ap Action Dr	ain Traps							
MadalNa		Cast	Iron		Forged Steel						
Model No.	2	.1 [†]	71	- A *	21-3	12 [†]	71-31	71-315*			
Dina Connections	in	mm	in	mm	in	mm	in	mm			
Pipe Connections	1/2, 3/4 15, 20 3/4, 1 20, 2		20, 25	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4, 1-1/2	20, 25, 32, 40				
"A"	6-3/16	157 8-1/2 216 6-3/4 171		9-3/4	248						
"B"	5-1/4	133	10-3/4 273 10-3/16 259		259	15-5/8	397				
"D"	_	_	4-1/4	108	5-9/16	141	7-13/16	198			
"K"	1-5/16	33	_	_	1-1/4	32	_	_			
"L"	_	_	3-1/2	89	3-5/16	84	4-5/8	117			
Weight, Ibs (kg)	8 (4)		29 (13)		30 (14)		92 (42)				
Maximum Allowable Pressure (Vessel Design)	250	psig @ 450°F	(17 barg @ 23	32°C)	600 psig @ 100°F 500 psig @ 750 400	0°F (34 barg @	1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)				

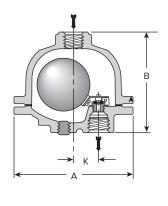
[†] Cast 316 stainless steel body and cap with all stainless steel internals available. Aluminum body and cap available for Model 21 only. Consult factory.

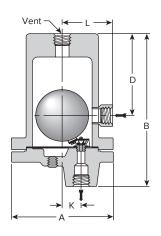
List of Materials

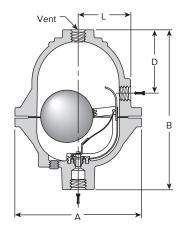
Table LD-2	5.							
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket			
21				Cast Iron ASTM A48				
71-A	Stai	nless Steel	Compre					
21-312 71-315				Forged Steel* ASTM A105	free			











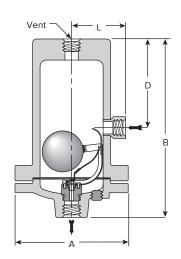


Figure LD-38.

No. 21 cast iron fixed lever drain trap.

Figure LD-39.No. 21-312 forged steel fixed lever drain trap.

Figure LD-40.No. 71-A cast iron snap action drain trap.

Figure LD-41.

No. 71-315 forged steel snap action drain trap.

For a fully detailed certified drawing, refer to list below: No. 21 CD #1037 No. 71-A CD #1038

No. 21-312 CD #1106 No. 71-315 CD #1107

^{*}Snap action drain traps should not be used where load exceeds 120 lb/hr (54 kg/hr). Use on greater loads shortens spring life.



High Leverage Spring-Loaded Ball Float Type Drain Traps

For Low Flows at Pressures to 3 700 psig (255 barg) and Specific Gravity Down to 0.40

The Armstrong High Leverage Series of liquid drain traps was developed especially for draining low specific gravity fluids from gases at high pressures. They use standard Armstrong forged steel bodies with very high leverage systems and spring assist.

NOTE: Models 2313-HLS, 2316-HLS, 2413-HLS and 2415-HLS are also available with cast T-316 stainless steel body and all-stainless steel internals. Consult factory.

Because of design considerations in this drain trap, it is essential that a safety factor of at least 2 be applied to the peak liquid load for sizing purposes.

Do not use HLS drain traps on steam service.

Sour Gas Service

Forged steel and stainless steel traps can be modified to resist hydrogen sulfide stress corrosion. These modifications involve annealing the float, which will reduce the maximum working pressure of the float to about half its normal value. Consult Armstrong Application Engineering for allowable working pressures.

Table LD-26. Re	eference Data	
Model No.	Float Diameter	Unbalanced Float Weight
2313-HLS 2413-HLS 25133G-HLS	3-1/2" (89 mm)	4 oz (113 g)
2315-HLS 2415-HLS 25155G-HLS 26155G-HLS	4" (102 mm)	4-1/2 oz (128 g)
2316-HLS 2416-HLS	5" (127 mm)	6 oz (170 g)

	Sp. Grav.	1.0	0	.9	5	.9	0	.8	5	.8	0	.7	5	.7	0	.6	5	.6	0	.5	5	.5	0	.4	5	.4	10
Model	Orifice											Opera						00°F (3	8°C)								
No.	in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	<u> </u>	barg		barg		barg	psig	barg								
	1/16	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	630	43
2242	5/64	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	940	65	670	47	410	29
2313- HLS	3/32	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	850	58	660	46	480	33	290	20
TILS	7/64	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1000	69	910	63	770	53	630	44	490	34	360	25	220	15
	1/8	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	920	63	810	56	700	48	600	41	490	34	380	26	280	19	170	11.7
	3/32	1 000	69	1 000	69	1 000	69	1 000	69	1 000		1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	1 000	69	960	66
2315-	1/8	1 000	69	1000	69	1 000	69	1 000	69	1 000	69	1000	69	1000	69	1 000	69	1 000	69	1000	69	900	62	730	50	550	38
HLS	5/32	1000	69	1000	69	1 000	69	1 000	69	1 000		1000	69	1000	69	930	64	810	56	700	48	590	40	470	33	360	25
	3/16 3/32	1000	69 69	1000	69 69	1 000	69 69	970	67 69	890 1 000	61 69	810 1 000	56 69	730 1 000	50 69	650 1 000	45 69	570 1 000	39 69	490 1 000	34 69	410 1 000	28 69	330 1 000	23 69	250 1 000	17 69
	1/8	1000	69	1000	69	1 000	69	1 000	69	1 000		1000	69	1000		1000	69	1 000	69	1 000	69	1 000	69	1000	69	1 000	69
2316-	5/32	1000	69	1000	69	1 000	69	1 000	69	1 000	69	1000	69	1000	69	1000	69	1 000	69	1 000	69	1000	69	1000	69	1 000	69
HLS	3/16	1000	69	1000	69	1 000	69	1000	69	1 000		1000	69	1000		1 000		1 000	69	1000	69	1 000	69	1000	69	830	57
	7/32	1 000	69	1000	69	1 000	69	1 000	69	1 000	69	1000	69	1000	69	1000	69	1 000	69	1000	69	880	61	750	52	620	43
	1/16	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500		1500	103	1500	103	1420	98	1020	71	630	43
2413-	5/64	1500	103	1500	103	1 500	103	1 500	103	1 500	103	1500	103	1 500	103	1 500	103	1 460	101	1 200	83	940	65	670	47	410	29
HLS	3/32	1500	103	1500	103	1 500	103	1500	103	1500	103	1500	103	1 400	97	1220	84	1 030	71	850	58	660	46	480	33	290	20
	7/64	1500	103	1500	103	1500	103	1 460	101	1320	91	1180	82	1050	72	910	63	770	53	630	44	490	34	360	25	220	15
	3/32	1800	124	1800	124	1 800	124	1800	124	1 800		1800	124	1800	124	1 800	124	1 800	124	1800	124	1560	108	1260	87	960	66
2415-	1/8	1800	124	1800		1 800	124	1800	124	1 800		1780	122	1600		1 430	98	1 250	86	1 080	74	900	62	730	50	550	38
HLS	5/32	1720	119	1 610	111	1 490	103	1380	95	1 270	87	1150	80	1 040	72	930	64	810	56	700	48	590	40	470	33	360	25
	3/16	1 210 1 600	83 110	1 130 1 600	78 110	1 050	72 110	970 1 600	67 110	890 1600	61 110	810 1 600	56 110	730	50 110	650 1600	45 110	570 1600	39 110	490 1600	34 110	410 1 600	28 110	330 1600	23 110	250 1600	17 110
	1/8	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600 1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110
2416-	5/32	1600	110	1600		1600	110	1600	110	1600		1600	110	1600	-	1600		1600	110	1600	110	1600	110	1480	102	1 220	84
HLS	3/16	1600	110	1600	110	1600	110	1600	110	1600		1600	110	1600	110	1600	110	1580	109	1 400	97	1 220	84	1 040	72	860	59
	7/32	1600	110	1600	110	1600	110	1600	110	1600		1 570	108	1 440	99	1300	90	1 170	81	1040	71	900	62	770	53	640	44
	1/16	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	1820	125	1420	98	1020	71	630	43
25133G-	5/64	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	1 980	137	1720	119	1 460	101	1 200	83	940	65	670	47	410	29
HLS	3/32	2 120	146	2 120	146	2 120	146	1960	135	1 770	122	1 590	110	1 400	97	1220	84	1 030	71	850	58	660	46	480	33	290	20
	7/64	1870	129	1740	120	1600	110	1 460	101	1320	91	1180	82	1050	72	910	63	770	53	630	44	490	34	360	25	220	15
	1	2 520		2 520	l	2 520	174	2 520		2 520		2 520		2 520	174	2 520		2 520	174	2 520	174	2 210	152	1780	123	1350	93
25155G-	1	2 520		2 520	l	2 520	174	2 520		2 520		2 520		2 520	174	2 470	170	2 170	150	1870	129	1560	108	1260	87	960	66
HLS	1	2 520		2 470	l	2 300	159	2 130	147	1950	1	1780	122	1600	110	1 430		1 250	86	1 080	74	900	62	730	50	550	38
	5/32	1720	119	1 610	111	1 490	103	1380	95	1 270	87	1150	80	1 040	72	930	64	810	56	700	48	590	40	470	33	360	25
	3/16 5/64	1 210 3 700	83 255	1 130 3 700	78 255	1 050 3 700	72 255	970 3 700	67 255	890 3 700	61 255	810 3 700	56 255	730 3 700	50 255	650 3 490	45 241	570 3 060	39 211	490 2 630	34 182	410 2 210	28 152	330 1780	23 123	250 1350	17 93
		3 700 3 700		3 700 3 700		3 700	255	3 680	255	3 380		3 080	255	3 700 2 770	191	2 470	170	2 170	150	1870	129	1560	108	1 260	87	960	66
26155G-		3 700 2 650		3 700 2 470		2 300	159	2 130	147	1 950	135	1780	122	1600	110	1430		1 250	86	1 080	74	900	62	730	50	550	38
HLS	5/32	2 030 1 720	119	1 610	111	1 490	103	1380	95	1 270	87	1 150	80	1 040	72	930	64	810	56	700	48	590	40	470	33	360	25
	3/16	1 210	83	1130	78	1 050	72	970	67	890	61	810	56	730	50	650	45	570	39	490	34	410	28	330	23	250	17
Specific	Gravity	1.0		.9		.9		.8		.8		.7		.70		.6		.6		.5	_	.5	_	.4			10

Table LD-27. Maximum Operating Pressures for Handling Different Specific Gravity Liquids With Orifices Available in High Leverage Drain

NOTE: If actual specific gravity falls between those shown in above table, use next lower. For example, if actual gravity is 0.73, use 0.70 data.

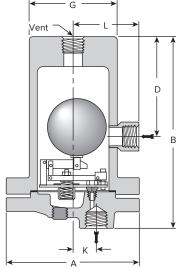
High Leverage Spring-Loaded Ball Float Type Drain Traps

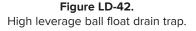
For Low Flows at Pressures to 3 700 psig (255 barg) and Specific Gravity Down to 0.40

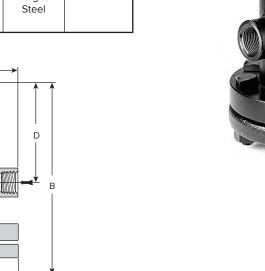


List of Materials

Table LD-28.					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
2313-HLS 2315-HLS 2316-HLS				ASTM A105 Forged Steel	
2413-HLS 2415-HLS 2416-HLS 25133G-HLS 25155G-HLS 26155G-HLS	Staiı	nless Steel		ASTM A182 Grade F22 Forged Steel	Compressed Asbestos- free







For a fully detailed certified drawing, refer to CD #1074.

Physical Data

Model No.	2313-	HLS [†]	2315-	HLS	2316-	HLS	2413-	HLS [†]	2415-	HLS†	2416-1	HLS	25133	G-HLS	25155	G-HLS	26155G	-HLS
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4	20, 25, 32	1, 1-1/4, 1-1/2	25, 32 40
"A"	8	203	9-3/4	248	11-7/8	302	8-5/8	219	10-3/4	273	12-1/2	318	8-1/2	216	10-3/8	263	11-3/4	298
"B"	11-9/16	294	15-1/16	383	17-1/8	435	11-7/8	3 002	15	381	17-3/4	451	14-1/4	362	16-7/32	412	24-1/8	613
"D"	6-1/16	154	7-13/16	198	9	229	5-3/8	137	7-1/4	184	9	229	3	75	4	102	5	127
"G"	5-1/8	130	6-7/8	175	8-3/8	213	5-3/8	137	6-7/8	175	8-5/8	219	5-3/4	146	7-3/8	187	8-3/8	213
"K"	1-7/16	37	1-3/4	44	2-1/8	54	1-7/16	37	1-3/4	44	2-1/8	54	1-5/16	33	1-3/4	44	1-3/4	44
"L"	3-7/8	98	4-11/16	119	5-3/4	146	4	102	4-13/16	122	5-13/16	148	_	_	_	_	_	_
Weight, lbs (kg)	46	(21)	98 (4	14)	160 (73)	69 (31)	130 (59)	210 (9	95)	113	(51)	171 ((78)	325 (14	47)
Maximum Allowable Pressure (Vessel Design)			g @ 100°F @ 750°F (1 500 psig (103 barg 900 psig (62 barg (@ 38°C) @ 850°F		38°)°F (62 bar		2 120 psig (146 barg 1 700 psig (117 barg)	@ 38°C) @ 900°F	2 520 psig (174 barg 2 000 psig (138 barg	@ 38°C) g @ 900°F	3 700 psig (255 barg (3 000 psig ((207 barg @	@ 38°C) @ 900°F

Note: Available with screwed, socketweld or flanged connections.

[†] Available with cast 316 stainless steel body and all stainless steel internals. Consult factory.



Free Floating Lever Dual Gravity Drain Traps

For Pressures to 1 000 psig (69 barg)

Armstrong free floating lever dual gravity drain traps are identical to the units described on pages LD-38 and LD-40 except float weights are modified to make them suitable for draining water from a light liquid. If you wish to use them for draining any liquid with specific gravity other than 1.00, consult the Armstrong Application Engineering Department.

Floats for dual gravity drain traps are weighted with quenching oil which, in the unlikely possibility of float failure, may be dispersed through the system. If this is a hazard, consult the Armstrong Application Engineering Department.

NOTE: Armstrong can design dual gravity traps for venting light liquids from above heavier liquids. Consult the Armstrong Application Engineering Department.

Viscosity Considerations for Dual Gravity Traps

The operation of dual gravity traps depends upon a float that will sink in the light liquid and float in the heavy liquid. When the specific gravities of the two liquids are very close, the available operating forces are, therefore, also very small. Viscous fluids may impair the ability of the trap to respond to changing liquid levels.

Consult Armstrong's Application Engineering Department if your application involves fluids more viscous than 70 cs, which is approximately the viscosity of a light machine oil.

Table ID 20 M	avimum Ona	ratina	Dress	uroo fo	r Droi	nina W	latar F		ifforon	+ Snor	isia Cr	ovity (iousida	\A/:+b	Orifica	. A.	ilabla i	n Dual	
Table LD-30. Ma Gravity Drain To		_				ning w	ater r	-rom L	irreren	it Spec	inc Gr	avity i	_iquias	with	Ornice	es Ava	паріе і	n Duai	
	Sp. Grav.	.5	50	.5	5	.6	0	.6	55	.7	70		75		30	.8	85		
	Float Wt, oz		.0		.5		0		.5		.0		.5	_	9.1	_	0.6		
Model No.	Float Wt, g		70	18		19		•	13		28		42		57	_	71		
								Maximu	ım Ope	rating F	ressure								
	Orifice (in)	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg		
	5/16	15	1.0	12	0.9	10	0.7	9	0.6	7	0.5	5	0.35	-	_	-	_		
	1/4	25	1.6	20	1.4	18	1.2	15	1.0	12	0.8	9	0.6	6	0.4	-	-		
2-DG	3/16	50	3.6	45	3.0	40	2.6	30	2.2	25	1.8	20	1.4	12	0.9	7	0.45		
2-00	5/32	90	6.0	75	5.5	65	4.6	55	3.8	45	3.0	35	2.4	22	1.6	12	0.8		
	1/8	150	10	130	9.0	110	8.0	90	6.5	75	5.0	55	4.0	40	2.6	20	1.4		
	7/64	190	13	170	12	150	10	120	8.5	100	6.5	75	5.0	50	3.4	25	1.8		
	Sp. Grav.		0		5		0		55		70		75		80		85		
	Float Wt, oz		.8	9		10			1.1		.9		2.7	_	3.5	_	4.3		
	Float Wt, g	24	48	2	71	29	93		15		38		60	3	82	4	05		
	Orifice (in)	25	1.0	20	1.4	10	12		ım Ope				0.7	7	0.5	Ι_	1		
32-DG	5/16	25	1.6	20	1.4	18	1.2	15	1.0	12	0.9	10	0.7	7	0.5	8	0.5		
	1/4 3/16	40 90	2.6 6.0	35 75	2.4 5.0	30 65	2.0	25 55	1.8 3.8	22 45	1.4 3.2	18 35	1.2 2.6	12 25	0.8 1.8	18	0.5 1.2		
	<i>3</i> /16 5/32	150	10	130	9.0	110	4.6 8.0	100	3.8 6.5	80	3.2 5.5	65	2.6 4.4	45	3.2	30	2.0		
	1/8	250	17	225	15	200	13	170	0.5	140	9.5	110	7.5	80	5.5	50	3.4		
	7/64	325	22	275	20	250	17	225	15	180	9.5 12	140	9.5	100	7.0	65	4.4		
	Sp. Grav.		50		5	-	0		55		70		75		30		85	.9	0
	Float Wt, oz	11		12		13			1.2		5.2		5.1	_	7.1	_	B.1	19	
2.00	Float Wt, g	3	17	34	1 5	37	73	4	01	4:	30	4	58	4	86	5	14	54	2
3-DG	Orifice (in)								Maxim	um Ope	erating I	Pressur	e						
to 250 psig* (17	1/2	12	0.8	10	0.7	9	0.6	8	0.5	6	0.45	5	0.35	-	_	-	_	_	_
barg)	3/8	25	1.8	22	1.6	20	1.4	15	1.2	12	0.9	10	0.7	7	0.5	-	_	_	_
Cast Iron	5/16	40	2.8	35	2.4	30	2.2	25	1.8	22	1.4	15	1.2	12	0.8	7	0.5	_	-
Cast IIOII	9/32	55	3.6	45	3.2	40	2.8	35	2.4	30	2.0	22	1.6	15	1.0	9	0.6	_	-
	1/4	80	5.5	70	4.8	60	4.2	50	3.6	40	3.0	35	2.2	25	1.6	15	1.0	_	
33-DG	7/32	110	8.0	100	7.0	90	6.0	75	5.0	60	4.2	45	3.2	35	2.4	20	1.4	7	0.45
for all pressures	3/16	170	12	150	10	130	9.0	110	7.5	90	6.5	70	4.8	50	3.4	30	2.0	10	0.7
·	5/32	275	19 38	225	16	200	14	170	12	140	10	110	7.5 15	80	5.5	45	3.2	15	1.0
	1/8 7/64	550 700	48	475 600	34 42	425 525	28 36	350 450	24 32	300 375	20 26	225 275	20	160 200	11 14	100	6.5 8.5	30 40	2.2 2.8
	Sp. Grav.		i 40 60	.5			0 0		<u> </u>		<u> </u>		<u> ∠∪ </u>		1 14 30		<u>0.5</u> 8 5	.9	
	Float Wt, oz	-	2	5			2		5 5 57		2		77	_	32	_	37 37	9	
	Float Wt, g		83	16		17		1	399		-)38		177		316	1	455	25	
6-DG	Orifice (in)										erating I								
to	1-1/16	12	0.9	12	0.8	10	0.7	9	0.6	8	0.5	6	0.4	_	_	l –	_	_	_
250 psig* (17	7/8	22	1.4	18	1.2	18	1.2	15	1.0	12	0.8	10	0.7	7	0.5	5	0.35	_	_
barg)	3/4	30	2.2	25	1.8	25	1.6	20	1.4	18	1.2	15	1.0	10	0.7	7	0.5	_	_
Cast Iron	5/8	45	3.2	40	2.8	35	2.6	30	2.2	25	1.8	22	1.4	15	1.2	12	0.8	6	0.4
	9/16	60	4.2	55	3.8	50	3.4	40	2.8	35	2.4	30	2.0	22	1.4	15	1.0	8	0.5
	1/2	90	6.0	80	5.5	70	4.8	60	4.2	50	3.4	40	2.8	30	2.2	22	1.4	12	0.8
36-DG	7/16	130	9.0	110	8.0	100	7.0	90	6.0	70	5.0	60	4.0	45	3.0	30	2.0	15	1.2
to	3/8	200	14	180	12	160	11	140	9.5	110	8.0	90	6.5	70	4.8	50	3.2	25	1.8
1000 psig (69	11/32	275	18	250	16	200	14	180	12	150	10	120	8.5	90	6.5	65	4.4	35	2.4
barg)	5/16	350	24	300	22	275	19	225	16	190	13	160	11	120	8.0	80	5.5	45	3.0
Steel	9/32	450	32	400	28	350	24	300	20	250	18	200	14	160	11	110	7.5	60	4.0
	1/4	650	46	575	40	525	36	450	30	375	26	300	20	225	16	160	11	80	6.0
	7/32	950	65	850	55	750	50	650	44	525	36	425	30	325	22	225	15	120	8.5
	3/16	1000	69	1000	69	1 000	69	1 000	69	850	60	700	48	525	36	350	24	200	14

NOTE: If actual specific gravity falls between those shown in the above table, use the next higher gravity. For example, if actual gravity is 0.73, use 0.75 gravity data. *For vessel pressures above 250 psig (17 barg), always use steel drain traps.

Free Floating Lever Dual Gravity Drain Traps

For Pressures to 1 000 psig (69 barg)



List of Materials

Table LD	-31.				
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
2-DG 3-DG 6-DG	C+=:	mlana Chanl		Cast Iron ASTM A48 Class 30	Compressed
32-DG 33-DG 36-DG	Stai	nless Steel		Forged Steel ASTM A105	Asbestos-free

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to:
No. 2-DG, 3-DG, 6-DG
CD #1034
No. 32-DG, 33-DG, 36-DG
CD #1035



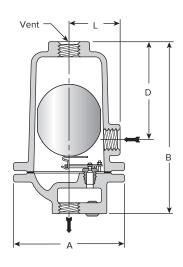


Figure LD-43.

No. 2-DG, 3-DG and 6-DG cast iron dual gravity drain traps.

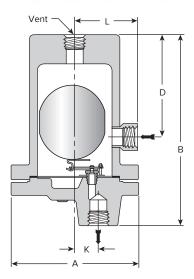


Figure LD-44.

No. 32-DG, 33-DG and 36-DG Forged steel dual gravity drain traps. Socketweld or flanged connections are also available.

Physical Data

Table LD-32. Armstron	g Free F	loating	Lever D	ual Grav	ity Drain	Traps						
Madalbia			Cas	t Iron				Forge	d Steel			
Model No.	2-0)G	3-1	DG	6-DG		32-0	OG*	33-0	G*	36-0	G*
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Pipe Connections	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50
"A"	5-1/4	133	6-3/8	161	10-3/16	259	6-3/4	171	8	203	11-7/8	302
"B"	8-3/4	222	11-1/2	292	18	457	10-3/16	259	11-9/16	297	17-1/8	435
"D"	5-1/8	103	7	188	9-3/8	238	5-9/16	141	6-1/16	154	9	229
"K"	_	_	_	_	_	_	1-1/4	32	1-7/16	37	2-1/8	54
" <u>L</u> "	2-7/16	62	2-7/8	73	4-5/8	117	3-3/8	86	3-7/8	98	6-1/16	154
Approx. Wt. lbs (kg)	12 (5.5)	21 (T (9.5) 78 (35.5		5.5)	31 (14)		49 (22)		163 (74)
Maximum Allowable Pressure (Vessel Design)		250 psi	g @ 450°F	(17 barg @	⊋ 232°C)		600 psig @ 100°F (41 barg @ 38°C)					

^{*} Available in Type 316 stainless steel. Consult factory.



Ultra-Capacity Drain Traps

Capacities to 700 000 lb/hr (317 520 kg/hr)... Pressures to 450 psig (31 barg)

Armstrong ultra-capacity ball float drain traps are designed to meet exceptionally large capacity needs in draining water and other liquids from air or other gases under pressure.

Options. L and M Series drain traps are available with armored gauge glass with a maximum allowable pressure of 250 psig @ 425°F (17 barg @ 218°C). When ordering, be sure to specify "Liquid Drainer" or "LD." Example, LS-series LD, 2" (50 mm) NPT, 7/8"

For a fully detailed certified drawing, refer to: L and M Series, CD #1010 JD and KD Series, CD #1302

Table LD-33	3. Maximum Op	eratin	g Pres	sures	for Ha	ndling	g Diffe	rent S	pecific	Gravi	ty Liqı	ıids W	ith Ori	fices A	vailab	ole in l	Jltra-C	apaci	ty Dra	in Tra _l	ps		
Model No.	Specific Gravity	1.0	00	.9	5	.9	0	3.	35	.8	80	.7	' 5	.7	0	.6	55	.6	50	.5	55	.5	50
Wiodel No.	Orifice Size									Ma	ximun	Oper	ating	Pressu	re								
	in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
	1-1/16	16	1.0	15	1.0	13	0.89	12	0.82	11	0.75	10	0.69	9	0.62	7	0.48	6	0.41	5	0.34	4	0.28
	3/4	35	2.4	32	2.2	30	2.0	27	1.8	24	1.6	22	1.5	19	1.3	16	1.0	14	0.97	11	0.75	9	0.62
	9/16	87	6.0	81	5.5	75	5.0	68	4.6	61	4.2	55	3.8	48	3.3	41	2.8	35	2.4	28	1.8	22	1.5
JD	1/2	146	10	135	9.0	125	8.5	113	8.0	102	7.0	91	6.2	81	5.5	69	4.8	59	4.0	47	3.2	37	2.6
	7/16	175	12	175	12	175	12	175	12	158	11	141	10	125	8.5	107	7.3	91	6.2	73	5.0	57	3.9
	3/8	250	17	232	16	214	15	195	13	177	12.2	159	10.9	140	9.7	122	8.4	103	7.1	85	5.9	67	4.6
	5/16	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	279	19.2	219	15.0
30KD	1-7/8 dual	30	2	30	2	30	2	30	2	_	_	_	_	_	_	_	_	_	_	_	_	_	_
50KD	orifice	50	3.5	50	3.5	50	3.5	50	3.5	_	_	_	_	_	_	-	_	_	_	_	_	_	_
300KD	Offlice	300	21	300	21	300	21	300	21	_	_	_	_	_	_	_	_	_	_	_	_	_	_
L	1-5/8	35	2.4	32	2.2	30	2.0	27	1.8	25	1.6	23	1.6	20	1.4	18	1.2	15	1.0	13	0.89	10	0.69
to 250 psig	1-1/8	116	8.0	108	7.4	100	7.0	92	6.3	84	5.8	76	5.2	68	4.7	60	4.1	52	3.6	44	3.0	36	2.5
(17 barg)	7/8	174	12	162	11	150	10.5	138	9.5	126	8.6	114	7.9	102	7.0	90	6.2	78	5.4	65	4.5	53	3.7
LS	11/16	*315	*22	*294	*20	*272	*19	250	17	228	16	206	14	184	13	162	11	141	9.7	119	8.2	97	6.7
For all Pressures	1/2	*450	*31	*450	*31	*450	*31	*450	*31	*450	*31	*400	*28	*354	*24	*298	*21	248	17	197	14	147	10
M to 250 psig (17 barg)	1-7/8 dual orifice	250	17	250	17	250	17	250	17	_	_	_	_	_	_	_	_	_	_	_	_	_	_
MS For all Pressures	1-17/32 dual orifice	*450	*31	*450	*31	*450	*31	*450	*31	*450	*31	_	_	_	_	_	_	_	_	_	_	_	_

^{*}These pressures applicable only to LS and MS models.

List of Materials

Table LD-34.								
Nama	-f David	Material						
Name o	т Рагт	Series JD, KD, L & M	Series LS & MS					
Can & Bady	JD, KD	ASTM A395 Ductile Iron	ASTM A216 Grade WCB					
Cap & Body	L, M	ASTM A48 Class 31						
Cap	L, LS	304 Stainless Steel, ASTM A351 Grade CF8						
Extension*	KD, M, MS	17-4 Ph, ASTM A7-	47 Grade CB7Cu-1					
Cap Bolting		ASTM A193 Grade B 7**	ASTM A193 Grade B 7					
Cap Gaskets		Flexible Graphite						
Float Mechanis	sm	Stainles	ss Steel					

^{*} JD Series does not have cap extension.

Physical Data

Table LD-36. Ultra-Ca	pacity Dra	ain Traps					
Tuan Carias	JD 8	k KD	L 8	М	LS 8	MS	
Trap Series	in	mm	in	mm	in	mm	
"B"	13-1/16	332	20-1/4	514	20	508	
"C"	9-5/8	244	14-3/4	375	15-1/4	387	
"H"	13-7/8	352	19-3/4	502	20	508	
"M"	6-1/2	165	11-5/16	287	11-5/16	287	
"D"	3	76	4-3/16	106	4-3/16	106	
"S"	_	_	3-3/4	95	3-3/4	95	
"T"	_	_	12	305	12	305	
Weight lbs (kg)	100	(45)	196	(89)	290	(132)	
Max. Allow. Pressure (Vessel Design)	65	osig @ 0°F @ 343°C)	250 p 450 (17 barg)	0°F	450 psig @ 650°F (31 barg @ 338°C)		

JD, KD, L and M Series also may be used for steam service as float and thermostatic traps and as condensate controllers. Steam service capacities for all configurations are given in the Steam Trapping section of this catalog.

Connections Available

Table LD-35	5 .					
Model	Si	ze	NPT	BSPT	sw	FLG
Wiodei	in	mm	INFI	D3F1	300	FLG
JD	2	50	X	X	_	*
KD	2, 2-1/2, 3	50, 65, 80	Х	X	_	*
L	2, 2-1/2	50, 65	Х	Х	_	Х
М	3	80	Х	Х	_	X
LS	2, 2-1/2	50, 65	Х	Х	Х	Х
MS	3	80	Х	Х	Х	X

*Flanged connections available. Consult factory.

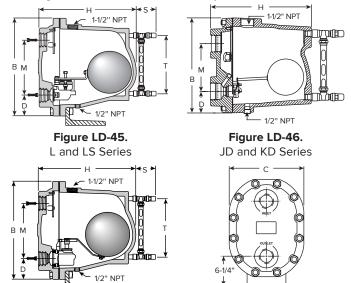


Figure LD-47.

M and MS Series

515 LD-49

^{**}JD and KD Series - ASTM A307 Grade B.

Installation and Maintenance of Drain Traps

For Draining Liquid From Gas...for Draining Water From Light Liquid



Installation Procedures

Pipe Fitting. Adhere to good piping practice. Clean pipes carefully after cutting and threading before hooking up traps. Before connecting traps to system, blow down at full pressure to clear the pipes of dirt, pipe cuttings and other foreign objects.

Strainers are necessary if there is a chance scale and sediment can be carried to the trap.

Blowdown Valves may prove useful.

Shutoff Valves & Unions should be provided so the drain trap can be examined and/or serviced without shutting down the unit drained.

Operation. Maximum operating pressure is stamped on the trap. Do not exceed this pressure.

- **A.** Ball float drain traps must be located below the drain point.
- **B.** Make inlet piping as short as possible with a minimum of elbows and other restrictions.
- C. Back venting usually required on ball float drain traps.
 - 1. Pressure vessels should be vented back to any convenient point above the liquid level. Use a full-ported valve in the back-vent line. On larger traps (6 and 36-LD and larger) use a minimum of 3/4" (20 mm) nominal pipe for back venting—1" (25 mm) or larger preferred for heavy loads. Remember, the pressure in the unit drained and in the drain trap are the same—only the difference in liquid levels produces flow.
 - Separators and drip points should be vented to the downstream side of the unit.
 - On very light loads, venting is not necessary, but use at least a 3/4" (20 mm) connection between the vessel and the trap. Make sure inlet line is vertical or pitched to trap.
 - 4. Float type drain traps do not require priming.

Typical installations of drain traps are shown in drawings in "Installation and Maintenance of Drain Traps" section.

Drain Trap Testing and Troubleshooting Testing Schedule

A regular schedule should be set up for testing and preventive maintenance. Size and operating pressure determine how frequently drain traps should be checked. Units on normal industrial applications should be checked as follows:

High Pressure Drain Traps—250 psig (17 barg) and up. Test daily to weekly.

Medium Pressure Drain Traps—60 to 250 psig (4 to 17 barg). Test weekly to monthly.

Low Pressure Drain Traps—1 to 60 psig (0.07 to 4 barg). Test monthly to annually. Large traps on high capacity jobs can be tested more frequently to good advantage.

Drain Traps on gas and other critical applications should be checked at the same time valves and other line equipment are inspected. Your own experience will determine the required testing schedule.

Troubleshooting

- A. Drain trap does not discharge.
 - Insufficient liquid coming to drain trap to permit discharge. Continue operation.
 - Drain trap filled with dirt or sludge. Remove cap and mechanism; clean thoroughly. Install strainer in inlet side of drain trap.
 - 3. Differential pressure across drain trap too high. Check inlet and outlet pressure. If the difference exceeds the maximum operating pressure stamped on the drain trap, the valve will remain closed. Reduce differential pressure if possible, or install properly sized mechanism in drain trap if possible.
 - 4. Worn valve seat. As the seat becomes worn, the seating surface area enlarges, lowering the trap's maximum operating pressure. Replace with new parts.
 - 5. Inlet or outlet line valves closed. Open valves.
 - 6. Strainer clogged. Clean strainer screen.
 - 7. Float defective or collapsed. Replace float.
- **B.** Drain trap discharges continuously.
 - If drain trap discharges full stream of liquid continuously and vessel fills full of liquid
 - a. Drain trap too small for job. Replace with correct size.
 - Abnormal amounts of liquid coming to drain trap.
 Remedy cause or replace with drain trap that has a larger capacity and will handle peak loads.
- C. Drain trap blows through.
 - 1. Dirt or scale on valve or seat. Remove cap, clean drain trap, as well as valve and seat.
 - 2. Worn valve, or seat that is wire-drawn. Remove cap, replace mechanism.
 - 3. IB trap may lose its prime.
 - a. Close the inlet valve for a few minutes. Then gradually open. If the drain trap catches its prime, the chances are that the trap is all right.
 - Frequent loss of prime may require an internal check valve or, if trap is old, valve and seat may be worn.

In the event of any unusual maintenance or operational difficulty, consult your Armstrong Representative, or the Armstrong International Application Engineering Department.



Installation and Maintenance of Drain Traps

For Draining Liquid From Gas...for Draining Water From Light Liquid

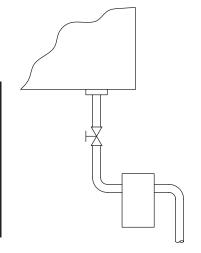
Installation of Armstrong drain traps for the most satisfactory operation requires that a few simple rules be observed:

Clean Piping. First install piping and valve ahead of trap, then blow down at full air pressure to remove loose dirt. Last of all, screw the trap into position.

Location. Compressed drain traps should be located below and close to the unit being drained (See Figs. LD-48 and LD-50), or as directed by the equipment manufacturer. When headroom is inadequate, inverted bucket drain traps can be installed above the unit drained, but they must be equipped with a check valve in the inlet line (See Fig. LD-49). They should be accessible for maintenance.

Priming. Prime bodies of inverted bucket drain traps before turning on the air. Ball float traps do not require priming.

Back Venting (Ball Float Traps Only). Ordinarily a drain trap has little water to handle, and a single line to the top of the trap is sufficient. However, if a ball float trap must be installed at some distance from the drip point, or if there are large quantities of water to be discharged, back venting is good insurance for positive and fast flow of water to the drain (See Fig. LD-52). Be sure there are no pockets in the vent line in which water could collect and prevent venting (See Fig. LD-54). If high water level is objectionable, raise the receiver, or dig a pit so top of trap can be at the same level as the bottom of the drain line (See Fig. LD-53). Otherwise, use an inverted bucket trap that can be installed above the drip point (See Fig. LD-49).



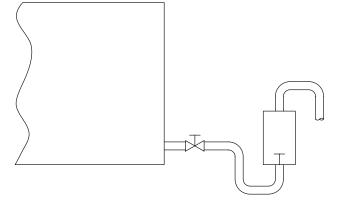


Figure LD-48. Standard hookup for inverted bucket

drain trap BVSW. Be sure to fill trap body with water before opening the valve.

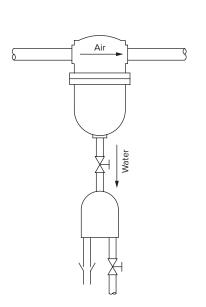
Figure LD-49.

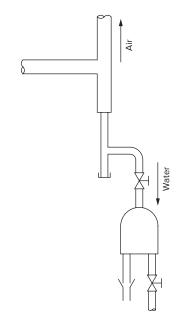
The inverted bucket trap draining an air receiver where space limitations prevent installation below the receiver. Note trap should either have internal check valve or a swing check to prevent prime loss when air pressure drops.

Installation and Maintenance of Drain Traps

For Draining Liquid From Gas...for Draining Water From Light Liquid







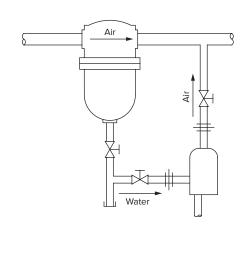


Figure LD-50.

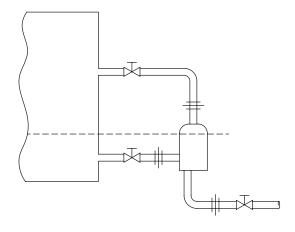
Drain trap installed below an air line separator. Keep the pipe as short as possible.

Figure LD-51.

Drain trap draining air line drip pocket. Be sure to use a gate valve and blow down the assembly before installing trap.

Figure LD-52.

Drain trap with vent line to downstream side of air separator to assure positive and fast flow of water to the trap. Note side inlet connection from separator.





Drain trap installed at side of receiver, close to floor. Water will rise to broken line before trap opens.

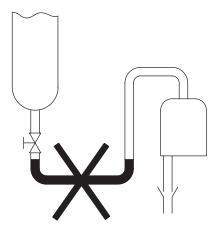


Figure LD-54.

Do not install a ball float trap above the drip point or put a loop or pocket in the line to the trap. The water seal prevents air from leaving trap body and allowing liquid to enter.



Armstrong ADP-1 Pneumatically Operated Liquid Drainer

Armstrong's pneumatically operated liquid drainer with press-to-test actuator for compressed air wastes no air, and it provides automatic operation in a see-thru vessel. This liquid drainer is ideal for draining oil/water separators. Its low profile makes it easy to mount on base-mounted compressors, remote cooler packs, refrigerated air dryers and filters.

Features:

- Convenient press-to-test actuator
- Large 100-oz. see-thru reservoir
- Fully pneumatic
- · No wasted air
- · Extremely low profile
- · Ideal for oil/water separators
- Non-clogging ball valve
- · No strainers to clean
- Automatic operation
- · Vent valve provided
- · Easy to retrofit

Options:

- Legs
- · Mechanical cycle counter
- Heater

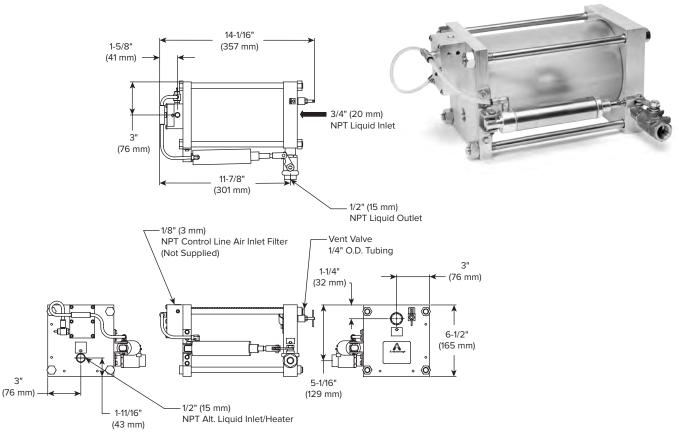
For a fully detailed certified drawing, refer to CD #1271.

List of Materials

Table LD-37.	
Name of Part	Material
Inlet and Outlet Heads	Aluminum ASTM B221 6061-T6511
Float and Leverage System	Stainless Steel
Reservoir	Fiberglass
Outlet Ball Valve	Bronze with Stainless Steel Ball and Stem
Air Cylinder	Stainless Steel
Optional Floor/Wall Mounts	Stainless Steel

Physical Data

Table LD-38. Armstrong ADP-1 P Drainer	neumatically Ope	erated Liquid
Specifications	in	mm
Liquid Outlet	1/2	15
Liquid Inlet	3/4	20
Alternate Liquid Inlet/Heater	1/2	15
Control Air Inlet	1/8	3
Vent Valve Connection	1/4" OD	Tubing
Weight, lb (kg)	14 (6.4)
Maximum Operating Pressure	180 psig	(12 barg)
Maximum Operating Temperature	150°F	(66°C)
Capacity	1.5 lb liquid	d per cycle
Maximum Control Air Pressure	80 - 12 (6 - 8.3	





Notes	Armstrong





Ancillary Products

Armstrone







DS Series Drain Separators

Condensate in steam and air piping reduce thermal efficiency, cause water hammer, corrode equipment such as valves and pipes, and cause other problems.

Armstrong drain separators separate condensate efficiently by using the centrifugal force of steam or air created by introducing it into a specifically shaped path. Because of the simple structure of the drain separators, pressure loss is minimized, enabling clean, dry steam or air to be fed to equipment.

With correct sizing and proper drainage, the separators are designed to eliminate 98% of all entrained liquids and particles that are 10 microns and larger in size.

Features

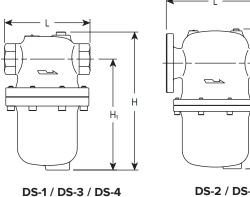
- A cyclone structure maximizes liquid separation efficiency
- · Pressure loss is extremely low
- No moving parts means no breakdowns

Operating Principle

When steam or air flow enters the drain separator, centrifugal force is generated in the fluid because of the device's internal structural design. The fluid drains along the wall because of the difference in specific gravity with steam or air, eventually striking the baffle. The baffle guides the fluid to the drain outlet and to the trap, which drains it. As a result, both small dirt particles and condensate are separated and removed from the system through the bottom drain.

For fully certified drawings refer to:

DS-1 / DS-2 **CDY1102 DS-3** CD2126 **DS-4 CD2127**



DS-2 / DS-3 / DS-4

DS Ser	ies Specifica	ntions					
Model	Application	Maximum Pressure psig	Maximum Temp.	Materials			
		(barg)	°F (°C)	Body	Nozzle		
DS-1		NPT 300 (20)					
		150 lb. Flanged 185 (13)	430 (221)	Ductile Iron ASTM	Cast Iron ASTM		
DS-2	Steam	300 lb. Flanged Steam 300 (20)		A536	A48		
	Air	NPT 300 (20)	650 (343)	SS304			
DS-3 DS-4		150 lb. Flanged 150 (10)	450 (232)	(DS-3) Carbon Steel (DS-4)			
D3-4		300 lb. Flanged 500 (34)	650 (343)				

D3 3e	ies Dili	nensi	on and \	weign																
	Siz				Face-to-	Face "L	**		н		н	11	Dra	in			We	ight		
Model	312		NPT		150#		300#				<u> </u>		Diani		NPT		15	0#	30	0#
	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	lb	kg	lb	kg	lb	kg
	1/2	15	5-15/16	150	-	_	_	_	9-9/16	243	7-5/8	193	3/4	20	16	7.3	-	_	_	_
	3/4	20	5-15/16	150	-	_	_	_	9-9/16	243	7-5/8	193	3/4	20	16	7.3	-	_	_	_
DS-1	1	25	5-15/16	150	-	_	_	_	9-9/16	243	7-5/8	193	3/4	20	16	7.3	-	_	_	_
D3-1	1-1/4	32	7-1/2	190	-	_	_	_	11-1/8	243	8-3/8	213	1	25	28	12.7	-	_	_	_
	1-1/2	40	7-1/2	190	-	_	_	_	11-1/8	243	8-3/8	213	1	25	28	12.7	-	_	_	_
	2	50	8-5/8	219	-	_	_	_	13-15/32	243	10-1/4	260	1	25	45	20.5	-	_	_	_
	2-1/2	65	_	_	11-1/2	292	11-15/16	303	16-15/32	418	12-3/8	314	1	25	_	_	45	20.5	77	35
DS-2	3	80	_	_	13-1/2	343	14-1/64	356	19	484	14-1/2	361	1-1/4	32	_	_	77	35	99	45
	4	100	_	_	15-13/16	402	16-7/16	418	23-3/8	594	17-1/2	445	1-1/4	32	_	_	99	45	143	65
	1/2	15	5-1/2	140	9	229	9	229	16	356	9	229	1	25	28	12.7	30	13.6	32	14.5
	3/4	20	5-1/2	140	9	229	9	229	16	356	9	229	1	25	28	12.7	30	13.6	32	14.5
	1	25	6-3/8	162	10-1/2	267	10-1/2	267	16	356	10-1/2	267	1	25	30	13.6	33	15	35	15.9
	1-1/4	32	6-3/8	162	10-1/2	267	10-1/2	267	16	356	10-1/2	267	1	25	32	14.5	35	15.9	37	16.8
	1-1/2	40	7-5/8	194	11-1/2	292	11-1/2	292	19	483	12-1/2	318	1	25	46	20.9	50	22.7	56	25.4
DS-3	2	50	7-7/8	200	11-1/2	292	11-1/2	292	19	483	12-1/2	318	1	25	51	23.1	55	24.9	59	26.8
	2-1/2	65	_	_	16	406	16	406	22	559	15	381	1	25	_	_	100	45.4	110	49.9
DS-4	3	80	_	_	18	457	18	457	26	660	18	457	1	25	_	_	140	63.5	150	68
	4	100	_	_	20	508	20	508	31	787	22	559	1-1/2	40	_	_	195	88.4	220	99.8
	6	150	_	_	24	610	24	610	41	1 041	30	762	1-1/2	40	_	_	350	159	380	172
	8	200	_	_	28	711	28	711	50	1 270	37	940	2	50	_	_	475	215	610	278
	10	250	_	_	34	864	34	864	70	1 778	55	1397	2	50	_	_	780	354	1 180	535
	12	300	_	_	38	965	38	965	75	1905	58	1 473	2-1/2	65	_	_	940	426	1 510	685

DS Series Drain Separators



Capacities for Steam Service

DS-1/DS-2 Se	eries Steam Ca	pacities (lb/hr))						
Size	5 psig	10 psig	25 psig	50 psig	100 psig	150 psig	200 psig	250 psig	300 psig
1/2"	34	43	69	113	200	287	374	461	548
3/4"	60	75	121	198	351	503	656	809	962
1"	98	122	197	320	568	816	1 063	1 311	1559
1-1/4"	169	212	340	555	983	1 412	1 840	2 269	2 698
1-1/2"	230	288	463	755	1 338	1922	2 505	3 088	3 672
2"	379	475	763	1 244	2 206	3 167	4 129	5 090	6 052
2-1/2"	541	678	1 089	1775	3 147	4 519	5 891	7 263	8 635
3"	835	1 046	1 682	2 741	4 860	6 978	9 096	11 215	13 333
4"	1 437	1802	2 896	4 720	8 368	12 016	15 664	19 312	22 960

DS-1/DS-2 Se	eries Steam Ca	pacities (kg/hr	.)						
Size	0.34 barg	0.69 barg	1.7 barg	3.4 barg	6.9 barg	10.3 barg	13.8 barg	17.2 barg	20.7 barg
1/2"	16	20	31	51	91	130	170	209	249
3/4"	27	34	55	90	159	228	298	367	436
1"	44	55	89	145	258	370	482	595	707
1-1/4"	77	96	154	252	446	640	835	1029	1 224
1-1/2"	104	131	210	342	607	872	1 136	1 401	1 665
2"	172	215	346	564	1 001	1 437	1 873	2 309	2 745
2-1/2"	245	307	494	805	1 428	2 050	2 672	3 294	3 917
3"	379	475	763	1 243	2 204	3 165	4 126	5 087	6 048
4"	652	817	1 314	2 141	3 796	5 450	7 105	8 760	10 414

DS-3/DS-4 Se	eries Steam Ca	apacities (lb/hr)						
Size	5 psig	10 psig	25 psig	50 psig	100 psig	150 psig	200 psig	250 psig	300 psig
1"	190	225	295	390	550	675	780	860	1000
1-1/4"	320	345	460	620	860	1 050	1125	1 140	1 160
1-1/2"	460	500	680	880	1 225	1 550	1800	2 000	2 250
2"	790	910	1 050	1 550	2 200	2 700	3 150	3 700	4 000
2-1/2"	1 075	1120	1 585	2 400	3 400	4 300	5 000	5 375	6 400
3"	1950	2 300	2 950	3 750	5 250	6 600	7 600	9 000	10 000
4"	3 250	3 800	4 975	6 100	9 000	11 100	13 000	11 500	11 650
5"	4 975	5 850	7 650	9 250	11 400	11 700	12 000	23 000	25 000
6"	7 700	8 990	10 100	10 450	21 500	26 500	31 000	36 000	39 000
8"	10 750	11 450	12 000	23 750	34 000	43 000	51 000	58 000	66 000
10"	20 000	22 500	29 500	37 000	54 500	68 000	78 000	90 000	100 000
12"	29 500	34 000	44 000	54 000	81 000	100 000	105 000	112 000	114 000

Size	0.34 barg	0.69 barg	1.7 barg	3.4 barg	6.9 barg	10.3 barg	13.8 barg	17.2 barg	20.7 barg
1"	86	102	134	177	249	306	354	390	454
1-1/4"	145	156	209	281	390	476	510	517	526
1-1/2"	209	227	308	399	556	703	816	907	1 021
2"	358	413	476	703	998	1 2 2 5	1 429	1 678	1 814
2-1/2"	488	508	719	1 089	1 542	1 950	2 268	2 438	2 903
3"	885	1 043	1 338	1 701	2 381	2 994	3 447	4 082	4 536
4"	1 474	1724	2 257	2 767	4 082	5 035	5 897	5 216	5 284
5"	2 257	2 654	3 470	4 196	5 171	5 307	5 443	10 433	11 340
6"	3 943	4 078	4 581	4 740	9 752	12 020	14 061	16 329	17 690
8"	4 876	5 194	5 443	10 773	15 422	19 504	23 133	26 308	29 937
10"	9 072	10 206	13 381	16 783	24 721	30 844	35 380	40 823	45 359
12"	13 381	15 422	19 958	24 494	36 741	45 359	47 627	50 802	51 710



Stainless Steel Sump Ejector

Armstrong Condensate Management Group offers a stainless steel sump ejector for use in draining unwanted water from steam pits, steam tunnels or enclosed spaces. The stainless steel sump ejector uses a snap-acting Inconel X-750 spring-assisted mechanism, which engages a steam motive valve, turning the pump on or off as the float rises and falls. The all stainless steel design will ensure long life in the rather harsh environment of a steam pit.

The stainless steel sump ejector is designed to eliminate maintenance headaches and safety issues surrounding steam pits, tunnels and enclosed spaces.

Features

- All stainless steel construction and design guard against corresion
- True steam-on, steam-off operation
- Heavy duty Inconel X-750 springs provide a long, troublefree service life
- The small, compact and unique cast stainless steel design is unlike anything on the market today

For a fully detailed certified drawing, refer to list below.

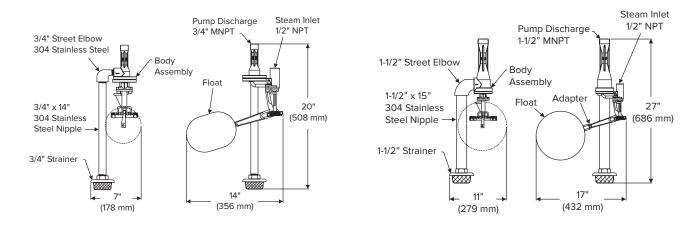
3/4" CDF #1052 1-1/2" CDF #1065

Stainless Steel Sump Ejector	Materials
Name of Part	Material
Mechanism	ASTM A351 CF8M
Springs	Inconel X-750
Spring Ends	304 Stainless Steel
Clevis Pins	304 Stainless Steel
Body	ASTM A351 CF8M
Nozzle	308 Stainless Steel
Seal Retainer	308 Stainless Steel
Motive Ball	440-C Stainless Steel
Motive Valve	316 Stainless Steel
Rod Seal	PTFE
Seal Spring	Hastelloy C-276
Rod Wiper	Nitrile
O-Ring	EPDM
Bolts	18-8 Stainless Steel
Strainer Body	Glass Filled Nylon
Strainer Mesh	Stainless Steel
Fittings	304 Stainless Steel
Pipe	304 Stainless Steel



Stainless Steel Sump Ejector





3/4" Model 1-1/2" Model

3/4" Stainl	ess Ste	el Sump	Ejecto	r Capaci	ities in g	gallons	per min	ute (gpr	n)									
		Wate	er Temp	erature	60°F			Water Temperature 100°F						Water Temperature 140°F				
Discharge Head (ft)		Motive	Steam	Pressur	e (psig)		Motive Steam Pressure (psig)						Мо	Motive Steam Pressure (psig)				
Tieau (II)	40	60	80	100	120	150	40	60	80	100	120	150	60	80	100	120	150	
0	6.0	9.3	11.6	12.2	12.8	12.9	6.0	9.0	9.2	8.6	8.0	8.0	5.5	5.3	5.4	5.5	5.5	
5	4.0	7.3	9.9	11.1	11.9	12.4	3.0	7.1	8.2	8.1	7.8	7.8	4.5	4.5	5.3	5.4	5.4	
10	2.0	5.2	8.3	10.0	11.0	11.9	-	5.2	7.2	7.7	7.6	7.6	3.5	3.5	5.2	5.2	5.2	
15	_	3.2	6.6	8.9	10.0	11.5	-	3.3	6.2	7.2	7.3	7.4	_	_	5.1	5.1	5.1	
20	_	_	5.0	7.8	9.2	11.0	-	_	5.2	6.7	7.1	7.3	_	_	5.0	4.9	4.9	
25	_	_	_	6.7	8.3	10.5	_	_	_	6.2	6.8	7.1	_	_	4.9	4.8	4.8	
30	_	_	_	5.6	7.4	10.0	_	_	_	5.7	6.6	6.9	_	_	4.8	4.6	4.6	
35	_	_	_	_	6.5	9.5	_	_	_	_	6.4	6.7	_	_	_	4.5	4.5	
40	_	_	_	_	5.6	9.1	_	_	_	_	6.1	6.6	_	_	_	4.3	4.3	
45	_	_	_	_	_	8.6	_	_	_	_	_	6.4	_	_	_	_	4.2	
50	_	_	_	_	_	8.1	_	_	_	_	_	6.2	_	_	_	<u> </u>	4.0	

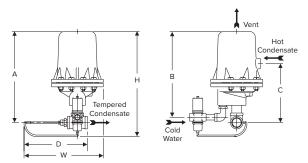
Note: Maximum operating pressure is 175 psig (12 barg). No increase in capacity with motive pressure over 150 psig (10 barg).

1-1/2" Stair	1-1/2" Stainless Steel Sump Ejector Capacities in gallons per minute (gpm)																	
District		Wate	r Temp	erature	60°F			Water	r Tempe	erature	100°F		Water Temperature 140°F					
Discharge Head (ft)		Motive	Steam	Pressur	re (psig))		Motive	Steam F	Pressur	e (psig)		Motive	Steam	Pressur	e (psig)
nead (it)	60	80	100	120	150	175	60	80	100	120	150	175	60	80	100	120	150	175
5	23.0	34.0	42.2	48.4	56.8	55.8	23.2	34.1	42.2	49.9	55.3	56.0	26.3	36.1	46.3	46.2	41.1	41.0
10	_	28.4	38.0	43.2	51.0	51.2	_	28.9	37.2	44.5	52.1	54.8	_	28.9	38.2	43.5	41.1	40.9
15	_	_	35.0	37.9	46.5	50.4		_	31.3	39.3	48.9	53.1	_		30.7	38.1	41.1	40.9
20	_	_	26.1	33.5	44.4	49.5		_	_	35.0	44.7	51.4	_		23.6	33.4	41.2	40.8
25	_	_		29.0	39.5	48.0		_	_	30.9	40.3	47.2	_	_		_	41.4	40.5
30	-	_		-	35.2	43.5	_	_	_	_	36.5	43.9	_		_			-
35	_		_		31.1	38.8		_		_	32.3	39.1	_					_
40						34.3		'				35.7			_		_	_

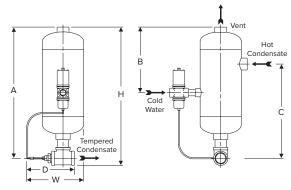


CC Series Condensate Coolers

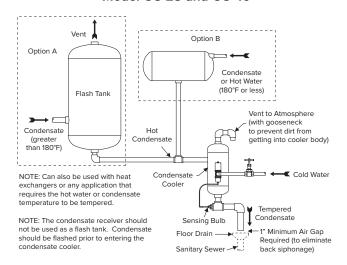
Drain Tempering Service



Model CC-5 and CC-12



Model CC-25 and CC-40



Typical Installation

Description

Armstrong's Condensate Cooler is a device that mixes hot condensate or hot water with a cold water supply to reduce the temperature to acceptable discharge drain temperatures as required by city and state codes. It is a pre-assembled package that is suitable for any plumbing system. When hot condensate or hot water is drained into the condensate cooler body, the tempering valve opens and allows cold water to enter the chamber and mix with hotter liquid, cooling it to a preset temperature level of 135°F (57°C) or to a desired field set temperature.

Capacities (Total of condensate and cooling water combined)

CC-5 5 gpm (19 lpm) CC-12 12 gpm (45 lpm) CC-25 25 gpm (95 lpm) CC-40 40 gpm (151 lpm)

To determine condensate load, use the following formula:

$$\frac{(B-C)}{(H-C)}$$
 x Model = gallons of hot liquid or condensate

Where: B = Set point of tempering valve (preset to 135°F)

C = Cold water temperature

H = Hot water temperature or condensate temperature

Example: $\frac{(135 - 50)}{(180 - 50)}$ x 5 (CC-5) = 3.25*

3.25 gal x 8.33 lbs per gallon x 60 = 1 624 lbs per hour

Tempered Condensate Range

Factory preset 135°F (57°C)

Field adjustable range 115 to 180°F (46 to 82°C) Maximum cold water pressure 150 psig (10 barg)

Materials

Body:

CC-5 and CC-12 ASTM A48 cast iron
CC-25 and CC-40 Carbon steel
Pipe and Fittings: Malleable iron
Body (Controller): Brass
Sensing Bulb: Bronze

Physical Data								
Model	CC	C-5	cc	:-12	СС	-25	CC-40	
Pipe Connection	in	mm	in	mm	in	mm	in	mm
Vent	3/4	20	1-1/2	40	1-1/2	40	2	50
Hot Condensate Inlet	3/4	20	1-1/2	40	1-1/2	40	2	50
Tempered Condensate Outlet	1-1/4	32	1-1/2	40	2	50	2-1/2	65
Cold Water Inlet	3/8	10	3/4	20	1	25	1	25
"H"	13	330	23	584	29	737	32-13/16	833
"W"	12-1/2	318	14-3/16	361	13	330	14-1/2	368
"A"	10-13/16	275	20-5/16	516	27-1/2	698	31	787
"B"	9-1/2	241	19-3/16	487	13-13/16	351	15-5/16	389
"C"	6-1/2	165	11-7/8	302	19-13/16	503	21-9/16	548
"D"	11	279	11	279	11	279	12	305
Weight, lb (kg)	15 (6.8)	77	(35)	81	(37)	93 (42)	

^{*} In the example, Model CC-5 (5 gpm) can handle 3.25 gpm of 180°F liquid. If cold water temperature or discharge temperature changes, the capacity will change.

Armstrong MS-6 Noiseless Heater



The use of hot water is indispensable in food processing, cleaning, and plating operations. Although the simplest and most efficient way to provide the water is by direct steam sparging, such a format often results in vibration and noise caused by steam blowing into the water tank. These problems can be greatly reduced by mounting an MS-6 noiseless heater at the end of the pipe.

Features

- Stainless steel construction for greater durability
- Mounting is simple and economical
- Maintenance free

Formula for Calculating Steam Load to Heat Water in Tank

lbs/hr = $\frac{\text{Gal x } \Delta \text{T x 8.3}}{\text{Lat x T}}$

Gal = Gallons of water to be heated

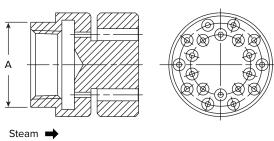
 ΔT = Temperature rise °F

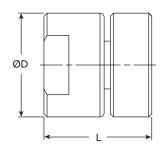
Lat = Latent heat of steam (Btu/lb)

T = Time in hours

Specifications	
Fluid	Steam
Pressure Range	7 - 100 psig (0.5 - 7 barg)
Silencing Limit Temperature	190°F (90°C)
Material	304 Stainless Steel
Connection	NPT







Dimensions and Weights												
Connection Size	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
Connection Size	1/2	15	3/4	20	1	25	1-1/4	32	1-1/2	40	2	50
"L"	1-15/16	49	1-15/16	49	2-1/16	52	2-3/16	55	2-5/16	59	2-9/16	65
"D"	1-3/8	35	1-1/4	45	2	50	2-3/8	60	2-3/4	70	4-1/8	105
"A"	1-3/16	30	1-7/16	36	1-5/8	41	2	50	2-3/8	60	3-9/16	90
Weight, lb (kg)	0.55 (0.25)		0.88 (0.40)		1.15 (0.52)		1.70 (0.77)		2.54 (1.15)		6.59	(2.99)

pacities - Steam, lb/hr (kg/hr)													
Connection Size													
Inlet, psig (barg)	1/	1/2"		3/4"		1"		1-1/4"		1-1/2		2	
	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	lb/hr	kg/hr	
7 (0.50)	54	25	129	58	157	71	190	86	291	132	362	164	
10 (0.70)	65	30	147	67	179	81	222	101	323	147	413	187	
15 (1.00)	84	38	177	80	214	97	276	125	376	171	498	226	
20 (1.38)	103	46	208	94	250	113	330	150	430	195	582	264	
30 (2.00)	140	63	269	122	321	146	439	199	536	243	751	341	
40 (2.76)	177	80	330	149	392	178	547	248	643	292	921	418	
50 (3.45)	214	97	390	177	463	210	655	297	749	340	1090	494	
60 (4.14)	251	114	451	205	534	242	764	346	856	388	1259	571	
70 (4.83)	289	131	512	232	605	275	872	395	963	437	1 428	648	
80 (5.52)	326	148	573	260	676	307	980	445	1069	485	1 597	725	
90 (6.20)	363	165	634	288	748	339	1 088	494	1 176	533	1767	801	
100 (6.90)	400	181	695	315	819	371	1 197	543	1282	582	1936	878	



Armstrong Armstrong Exhaust Head - AEH Series

Description

Armstrong's AEH series carbon steel exhaust heads should be used when there is a risk of water carryover up an atmospheric vent pipe. The internal knock-out plate and stainless steel mesh screening effectively contains water carry-over and discharges it through the bottom drain leaving dry flash steam to vent through the top of the vessel.

Connections

Flanged ASME B16.5 CL 150

Drain FNPT

How To Order

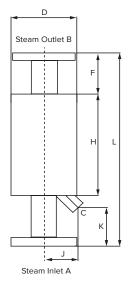
Exhaust heads are typically sized to match existing vent line connections. Choose the Armstrong model below which best fits your application.

(**Note:** 1. Excessive carryover could be caused by leaking steam traps or undersized vents. 2. Not for use on Safety Relief Valves.)

Materials								
Part Name	AEH Series							
Body	Carbon Steel							
Baffle Plate	Carbon Steel							
Screens	304 Stainless Steel							
Flange	Carbon Steel							
Connection Pipe	Carbon Steel							



Dimensions									
	(Connection Size)	D	Н	L	F	К	J
Model	Steam Inlet A In (mm)	Steam Outlet B In (mm)	Drain C In (mm)	In (mm)	In (mm)	In (mm)	In (mm)	In (mm)	In (mm)
AEH20592-2	2 (50)	2 (50)	3/4 (19)	6-1/4 (159)	9-13/16 (250)	18-1/2 (470)		3-5/8 (92)	3-1/4 (82)
AEH20592-3	3 (80)	3 (80)	3/4 (19)	8-5/8 (219)	11-13/16 (300)	21-5/8 (550)		4-13/16 (122)	4-1/8 (105)
AEH20592-4	4 (100)	4 (100)	1 (25)	10-3/4 (273)	13-3/4 (350)	24-13/16 (630)	4 (100)	5-11/16 (145)	5-3/16 (132)
AEH20592-6	6 (150)	6 (150)	1-1/2 (38)	12-13/16 (325	15-3/4 (400)	27-9/16 (700)		6-1/2 (165)	6-1/4 (158)
AEH20592-8	8 (200)	8 (200)	2 (50)	16-3/4 (426)	17-3/4 (450)	30-11/16 (780)		7-3/8 (188)	8 (204)
AEH20592-10	10 (250)	10 (250)	2 (50)	20 (508)	19-11/16 (500)	33-7/16 (850)		8-3/16 (208)	9-3/8 (238)



Notes	Armstrong